by the Smoake doth infect the Aer, and so incorporate with it, that though the very Bodies of those corrosive particles escape our perception, yet we soon find their effects, by the destruction of all things they do but touch; with their fuliginous qualities." Evelyn not only implicated combustion, but also inferred that the cause was from small particles.

This section discusses the ongoing research into the health effects of particulate air pollution, with an emphasis on the toxicological hypotheses that relate to specific types of combustion-generated particles. Table 8 summarizes combustion particle characteristics that are suspected to be important for health effects and the results of selected epidemiology and toxicology studies that have addressed these physical and chemical characteristics.[6,8,25,213,305,308,312–348] Recent reviews discuss the toxicologic and epidemiologic evidence for health risks from gasoline and diesel engine emissions;[324,349] the toxicology of ultrafine anthropogenic atmospheric aerosols;[345] and the relationship of particle air pollution to asthma.[350] The proceedings of recent conferences are sources of more detailed coverage of current health-related research.[351,352]

Table 8. Combustion particle characteristics investigated in toxicology studies.

Characteristic	Relation to Combustion	Epidemiology Studies	Toxicology Studies
Mass	Filterable combustion aerosols are a minor component of urban aerosol, which is dominated by organic, secondary, and geological PM.[305]	Health outcomes have been associated with ambient PM mass.[340]	Exposure of young, healthy adults to concentrated ambient particle does not cause acute effects.[323,336]
Particle Size	Combustion is the major source of submicron and ultrafine PM. (This review.)	Coarse particles are not associated with mortality,[338,341] but health outcomes are associated with fine PM.[318]	Iron mobilization from coal fly ash in cell culture increases with decreasing particle size.[343] Mutagenic activity is associated with fine PM.[333]
Ultrafine and Nanoparticles	Inorganic ultrafines are formed by mineral vaporization during combustion followed by nucleation and condensation. (This review.)	Respiratory effects associated with ultrafine PM number.[335,345]	Differences between fine and ultrafine particles of the same material.[319,331,332,346]
Transition Metals	Submicron particles from combustion are enriched in transition metals. Fe is more bioavailable from coal fly ash than from geological dust with similar size and total Fe.[348]	Associations of health outcomes and transition metals were found in some studies,[327,334] but not in others.[325]	Transition metals catalyze formation of reactive oxygen species.[326,342] Metals from ambient PM[314,322] and coal fly ash[344] induce synthesis of proinflammatory cytokines in cells and lung inflammation in rats.[317]
EC (Soot)	Combustion produces 10- to 50-nm diameter carbon-rich primary particles. (This review.) Diesel exhaust is the major source of urban soot.[308]	Weak association between diesel exhaust and cancer risk[324] but uncertain dose-response relationship.[347]	Carbon black and whole diesel exhaust produced similar lung lesions in rats.[330] Ultrafine carbon causes lung inflammation.[329]
OC	Incomplete combustion produces a wide range of organic species.[213,312]	Exposure studies[324] to whole diesel exhaust include the soluble organic fraction.	PAH compounds include known and suspected carcinogens and mutagens.[324,328]
Secondary SO_4^{2-} and NO_3^-	Most of the urban ambient $PM_{2.5}$ is secondary aerosol formed from combustion-generated SO_2 and NO_x.[6,8]	SO_4^{2-} and NO_3^- are implicated by studies that correlated risk with PM mass.[318]	NO_3^- not toxic at 1 mg/m^3 agricultural worker exposure.[313] High levels of SO_4^{2-} associated with increased airway resistance.[315]
Acidity	Cl and S in fuels produce HCl and SO_2 in the combustion products.	Some evidence for a correlation of health outcomes with H^+.[340]	Various responses reported to laboratory inhalation of acid aerosols.[321]
Synergistic Effects	Combustion emissions contain EC, OC, metal-rich particles, CO, and acid gases.	Epidemiologic studies are confounded by the complex mixture of pollutants in ambient air.[337,339]	Exposure to pairs of pollutants can produce greater effect than either one alone: ultrafine PM and O_3,[320] coal fly ash and H_2SO_4,[25] benzo[a]pyrene and carbon black.[316]

Epidemiology

Epidemiology, the medical science that investigates the quantitative factors controlling the frequency and distribution of disease, provided the initial evidence that the PM_{10} ambient air standard did not meet the legal criteria in the Clean Air Act to "protect the public health" while "allowing an adequate margin of safety."[353] The current emphasis on the health effects of particulate air pollution was set in motion by the seminal studies of Pope, Schwartz, and Dockery. Pope compared hospital records for years when a steel mill in Utah was operating and closed and showed that elevated PM_{10} concentration was associated with increased hospital admissions for pneumonia, pleurisy, bronchitis, and asthma.[354] Schwartz and Dockery showed that variation in total suspended PM correlated with the number of deaths per day in Steubenville, OH, over an 11-year period.[340] Dockery et al. showed that fine-particulate air pollution, or a factor correlated with fine PM, contributed to excess mortality in six U.S. cities.[318]

The methods used in recent air pollution epidemiology studies have been reviewed,[355,356] and these methods are based on general correlation models described in advanced statistics texts.[357] Several studies have involved reexamining previous results by an independent group of investigators to verify the conclusions by alternative statistical methods.[358,359] The statistical association of fine PM and various health end points appears to be robust, that is, independent of the specific correlation model used. Pope reviewed epidemiology studies of particulate air pollution from 1953–1996 and listed approximate ranges of estimated effects.[337,355] For a 10-$\mu g/m^3$ increase in PM_{10}, the effects were a 1.5–4.0% increase in respiratory mortality, a 0.5–2.0% increase in cardiovascular mortality, a 0.5–4.0% increase in respiratory hospital admissions, and a 1.0–4.0% increase in grade-school absences. Detecting such a small increase requires an extremely sensitive statistical method. Since the average death rate in the United States is about 20 deaths/day/million persons, a 1% increase in mortality represents 1–2 excess deaths above the daily average in a metropolitan area containing 5 million people.

Epidemiology methods have limitations. These studies can only correlate data that have been consistently measured over a sufficient geographical area or period of time to show detectable variation. For example, to test for the effect of geological particles, studies have had to use indirect measures of wind-blown dust such as the dates of dust storms[341] or the atmospheric clearing index.[338] Epidemiologists have not correlated health effects with either ultrafine ambient particles or with the ambient concentration of biologically available transition metals because these suspect particle characteristics have not been routinely measured. Although epidemiology can show a correlation, it cannot prove causality. Two well-correlated factors may both be individually correlated with a third unknown factor that is the actual cause. There have been frequent suggestions that the observed health effects that have been correlated with particles are actually due to another pollutant that correlates with PM. Stagnant air conditions in urban areas can lead to the simultaneous buildup of multiple pollutants including PM, O_3, SO_2, CO, soot, and numerous gas-phase and particle-bound organic species, so this is a reasonable hypothesis. As will be discussed in the measurements section of this review, a need exists for the development of robust, precise, economical methods for measuring the various particle characteristics that are possible factors for health studies.

Epidemiology studies in Spokane, WA,[341] and in Utah[338] suggest that coarse, wind-blown particles are not the cause of the observed health effects. This implies that some other component of the urban PM, such as fine particles from combustion, is related to the observed effects. An important distinction must be made between chronic and acute health effects. Some health effects, such as chronic bronchitis, emphysema, pneumoconiosis, fibrosis, and lung cancer, are associated with many years of exposure to the combustion emissions or other inhalable toxic agents. The acute effects of particle inhalation include hospital admissions associated with asthma, bronchitis, pleurisy, pneumonia, and cardiovascular disease. Time-series epidemiology studies show that these effects typically lag the changes in PM level by 1–5 days.[355] During the 1952 London Fog event, a temperature inversion trapped the air pollution, allowing the buildup of combustion emissions to lethal concentrations over a period of four days in December. The increase in deaths was almost 4-fold during the episode, and the effects started within a day of the onset of the pollution increase.

The mass concentration increments addressed by ambient air epidemiology studies are orders of magnitude below the inhalable particle concentrations for PM in occupational settings. Average concentrations of diesel PM ranging up to 1400 $\mu g/m^3$ have been reported in studies of underground mines.[360] Typical allowable 8-hr concentrations for general "nuisance dusts" in occupational settings range from 2000 to 10,000 $\mu g/m^3$, and these measurements are usually stated in mg.[361] Few papers have proposed toxicological mechanisms that are based on particle mass alone at ambient concentrations. Particle mass, which has been the focus of most ambient PM epidemiology, is likely to be a surrogate for the real agent. However, Harrison and Yin,[362] in a review of PM health effects, discussed the uniformity of epidemiologic correlations between PM concentration and health end points observed in different regions of the world with different proportions of SO_4^{2-}, NO_3^-, crustal material, and other major PM components. They concluded that the available data provides little support for the idea that any single major or trace component of PM is responsible for adverse effects, but acknowledged that there is evidence that particle size rather than mass may be the appropriate measure to correlate with health effects.

Respiration and Particle Inhalation

The respiratory system will be briefly discussed to provide a background for the discussion of human population, whole animal, and cell culture studies of combustion particles. Concise descriptions of the human respiratory system, written in the context of air pollution engineering, include those by Carel[363] and Degobert.[248] Guyton and Hall's textbook is recommended for a comprehensive introduction to cardiopulmonary physiology,[364] while Netter's collection of illustrations is recommended for visualizing respiratory anatomy.[365]

The observed statistical associations of ambient PM mass concentration with morbidity and mortality lead to the mechanistic question: How can a small increase in the mass of inhaled particles deposited cause sickness or premature death? A person inhales from 6 to over 12 m^3/day of ambient air, depending on age and physical activity. This air contains a wide variety of natural particles from geological and biological sources as well as anthropogenic pollutants. The deposition of supermicron particles by inertial impaction and of submicron particles by diffusion depends on the gas velocity and residence time in various sections of the airway and lung. A widely used model of size-dependent deposition in the nasopharyngeal, tracheo-bronchial, and pulmonary regions of the respiratory system[366] is reproduced in many references, for example, Wilson and Spengler.[367] Most of the PM_{10} mass is deposited in the nose and throat, while ~60% of inhaled $PM_{0.1}$ is deposited in the lung. Actual size-dependent particle deposition depends on age, health, and especially on nasal versus oral breathing.[368]

Assuming typical values for respiratory volume and alveolar deposition efficiency, a calculation shows that a 10-μg/m^3 increment in ambient $PM_{2.5}$ results in an increment of 0.02–0.05 mg of particles deposited in the lung per day. This has lead to the opinion that either some component of ambient PM is highly toxic or that some individuals are highly susceptible. Alternatively, particle number may be considered. Assuming typical values for ventilation rate, lung surface area, and epithelial cell size, a calculation indicates that a typical urban, near-highway concentration of 10^5 particles/cm^3 results in an alveolar deposition rate of ~1 particle per cell per day. Figure 17 shows the relative size of the microscale structures in the alveolar region of the lung compared to a range of ambient particles.[364,365,369] The accompanying graphs in Figure 17 show a typical urban aerosol mass distribution and the calculated number of particles deposited per alveolus per day as a function of size. The calculated deposition assumes an ambient concentration of 100 μg/m^3 of PM_{10}, with 40% of the mass being smaller than 2.5 μm, and 2% being smaller than 0.1 μm. The deposition is calculated using the size-dependent deposition fraction[366] and assumes uniform deposition to all alveoli. This analysis shows that fewer than 1 in 1000 alveoli has a coarse particle deposited per day, but that a typical alveolus may be exposed to several hundred ultrafine particles per day.

The body has defenses to rapidly remove inhaled particles. A mucus layer, moved upward by cilia on the cells lining the airways, transports particles from the respiratory system to the throat, where they can be coughed up or swallowed. The terminal airways and alveoli lack ciliated cells. Mobile macrophage cells take up particles by phagocytosis and remove the particles from the alveoli by active transport into the ciliated airways. Particles are also removed from the lung by dissolution and by transport into the lymphatic drainage system. A fraction of the inhaled particles is retained for a long time in the respiratory system, either in the airways or in the interstitial spaces. The process of clearing particles from the lungs can induce secondary physiological responses including coughing and inflammation. The mammalian respiratory system is likely to have evolved clearance mechanisms that are appropriate for the natural background particle number concentrations. A plausible hypothesis is that the large numbers of ultrafine particles in the urban aerosol may simply overload the ability to clear particles from the lungs. Alternatively, some specific types of inhaled particles may interact with the body's nervous and biochemical signaling pathways, resulting in an amplified response.

Identification of specific particle types in the ambient mixture that are biologically active for specific health effects is an active area of research.[2,3] The effects of inhaled particles may increase with decreasing particle size due to several factors: finer particles are deposited in the lung rather than in the upper airway; finer particles have greater surface area per unit mass, which enhances solubility; and finer particles can enter cells more readily and can be transported from the lung to other organs. The living cell interacts with the surface of a particle, so surface chemistry, not the volume average composition, is likely to be most relevant for biological effects of low-solubility particles.

Controlled Exposure to Concentrated Ambient Particles

Inhalation exposure studies complement the results of epidemiology studies. The effect of particulate air pollution

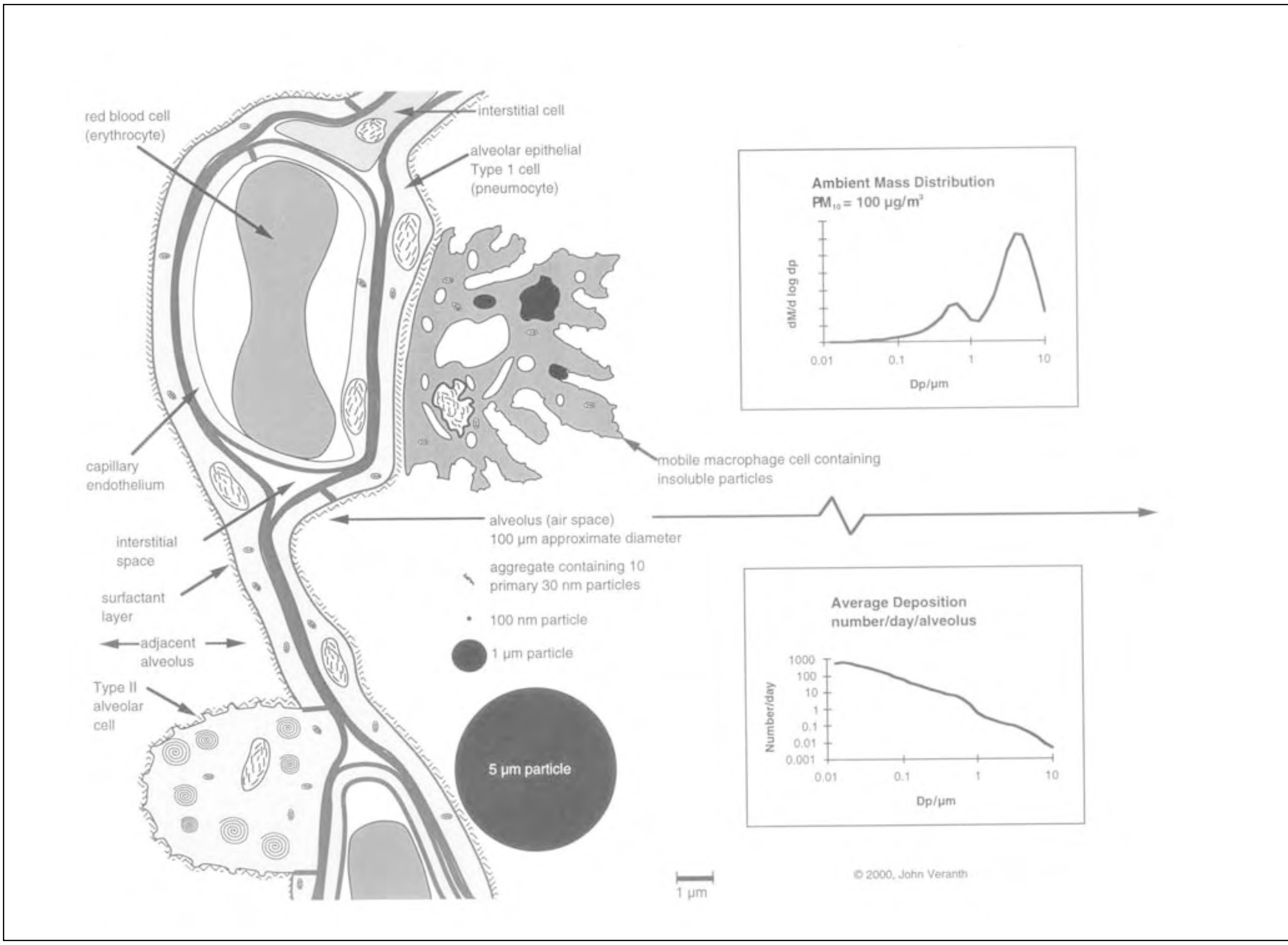

Figure 17. Scale drawing comparing ambient particles to structures in the aveoli of the human lung. The graphs show a typical ambient PM mass distribution and the expected number of particles of each size deposited per alveolus per day. Submicron particles are suspected to be important for health effects because of the large number deposited in the lung and because these particles can move into the interstitial space and blood stream. Compiled from information in refs 364, 365, 369.

can be amplified by conducting controlled inhalation exposure studies with concentrated ambient PM. This has been facilitated by the development of virtual impactor particle concentrators[370–372] and centrifugal particle concentrators[373] that keep the aerosol suspended while separating the gas from the particles. These particle concentrators can be staged to supply an inhalation chamber with air containing a 10-fold or higher concentration of ambient PM. Studies of this type are being conducted with both human volunteers[323] and with laboratory animals.[374,375] An early conclusion is that healthy adults show no adverse impacts from short duration exposure to concentrated ambient particles.[323,326]

Laboratory Studies with Surrogate Particles

A disadvantage of both epidemiologic studies and studies using concentrated ambient PM is that the subject is exposed to a complex mixture containing contributions from many sources, most of which are unknown or poorly characterized. An alternative is to conduct studies with laboratory-generated surrogate particles from well-characterized sources. This approach is most appropriate for conducting mechanistic hypothesis-based toxicological experiments, since the investigator can specify the particle characteristics used for the test and control condition pairs. An example of this type of study involved supplying fresh laboratory-generated coal fly ash particles to animal inhalation chambers as part of a study of the combined effects of H_2SO_4 and coal fly ash.[25,376] Inhalation studies involving ultrafine and nanoparticle PM also require having a laboratory particle generator connected to the inhalation chamber due to the rapid transformation of the particles by coagulation.[377] Surrogate particle inhalation studies require close cooperation between the life sciences and aerosol team members as well as physical proximity of the animal care and combustion facilities. Due to the cost and complexity of conducting animal inhalation studies at combustion facilities, alternative experimental methods are common.

Inhalation of resuspended particles allows the particle generation and collection to be separated from the exposure studies. There is little difficulty in resuspending 2.5- to 10-μm aerosol particles, and resuspension is also suitable for testing hypotheses related to particle chemical composition if particles with size-independent composition are available. Surface forces make the dispersion of submicron particles difficult, so resuspension has serious disadvantages if the hypothesis involves testing size-dependent effects. Improved methods for particle resuspension have been developed.[378–380]

Alternatively, particles may be instilled into the lung as a suspension in saline solution. Despite the artifacts introduced by this invasive procedure, instillation studies have been used to investigate combustion particle effects.[317,329,331,381] Cell culture studies involve mammalian cells or bacteria growing in an appropriate medium. Normally, the cells grow as a layer on the bottom of the culture dish or flask. The cells can be systematically exposed to various types of combustion particles or particle extracts to test specific biochemical hypotheses.[314,382] The biochemistry of single cells, especially cell lines derived from tumors, can differ from the responses that occur in the normal whole animal. Also, cell culture studies do not include any effects related to the interaction of the respiratory tract and nervous system with the particles.

In vitro experiments performed with purified chemicals under cell-free conditions can isolate specific mechanism steps such as the rate of mass transfer of a potentially toxic component from a combustion particle. But even experiments that simulate physiologically relevant conditions simulate only a fraction of the biochemistry that takes place in a living organism.

Laboratory experiments with surrogate particles can be conducted in vitro, using cell-free models of selected biochemical steps; in cell culture, using established cell lines; and in animal models of the human respiratory system. Specific mechanistic hypotheses can be tested by using well-characterized particles from known sources. These types of studies provide an important link between fundamental biochemistry and human population studies. The next section will discuss some of the hypotheses that are topics of current PM research.

Cardiopulmonary Effects of Particles

An active hypothesis is that the observed cardiac symptoms associated with particle inhalation may be mediated by the nervous system. Certain nervous system-activated changes in heart rate, blood pressure, blood viscosity, and heart-rate variability are associated with an increased likelihood of sudden cardiac death.[383] A study of 90 elderly subjects showed that changes in blood oxygen saturation were not associated with exposure to particle air pollution, but increased pulse rate was associated with exposure to particle air pollution on the previous 1–5 days.[384] A decline in heart-rate variability is a quantitative indication of impairment of the autonomic function, that is, a decline in the ability of the cardiorespiratory system to respond to changes. A decrease in heart-rate variability has been observed for persons exposed to increased ambient PM_{10} in Utah[385] and to increased $PM_{2.5}$ in the Boston area.[386] Cardiac monitoring may provide a sensitive indication of acute response that will be useful in identifying the relative importance of different components of ambient aerosol. Exposure of dogs with induced coronary occlusion to concentrated ambient particles affected one of the major electrocardiogram signs of myocardial ischemia,[375] and other cardiac and respiratory parameters were also affected. This suggests a plausible mechanism by which persons with existing heart disease may become more susceptible to serious cardiac effects when they are exposed to some component of ambient PM.

Biochemical Signaling

The nervous system and other biological signaling pathways can result in enormous amplification of a stimulus. Persons with hay fever or asthma are familiar with the massive response that can occur within minutes of exposure to an allergen. Cytokines are intracellular signaling molecules that mediate many protective physiological functions such as increasing the blood circulation and recruiting leukocytes (white blood cells) at the site of an infection. Cytokines can also induce potentially harmful responses such as prolonged tissue inflammation and development of fibrosis in response to irritants.[387,388] Lung inflammation has been associated with exposure to elevated ambient PM,[389,390] and a number of studies are focusing on the relationship of inhalable particles to the biochemical events leading to lung inflammation.[158,317,326,344,391–394] Combustion particles may contain specific chemical species that are able to activate biological signaling pathways, and a number of these hypotheses involve transition metals.

Transition Metals and Biochemical Processes

Particles provide a vehicle for metals to enter the body in inappropriate amounts. Much of the literature on the toxicity of solid-phase metal compounds is based on ingestion rather than on inhalation.[395] Ingestion dose-response relationships may be relevant for the effects of larger particles that are deposited in the upper airways but are rapidly cleared from the respiratory system to the throat, where they are swallowed. However, submicron particles are deposited deep in the lung, and ultrafine particles are able to pass from the lung directly into the body.[331] There is increasing evidence that the same element has very different behavior when inhaled than when ingested. Mn, a necessary trace mineral in the diet and a controversial octane-boosting additive in gasoline,[396] provides an example. Dietary Mn is homeostatically regulated by the liver, and ~3% of ingested Mn is absorbed.[397] Inhalation bypasses the digestive system, and up to 40% of inhaled Mn is absorbed.[398]

The dose of a particle-bound element that is available to the body depends on the entry route, the particle size and morphology, and the mineral species in the particle. When conducting laboratory experiments on metal bioavailability, it is necessary to distinguish between in vitro, extracellular, and intracellular behavior, since the solubility of transition metals from a given combustion ash mineral species depends on the pH and the presence of chelators. Many chelators are present in cells, and some, such as citrate, are present at millimolar concentrations.

Transition metals on inhaled particles may act as biochemical catalysts that can induce other biochemical responses. Transition metals, such as V, Cu, Fe, and Pt, can catalyze the generation of ROS[399] that have been associated with both direct molecular damage and with the induction of biochemical synthesis pathways. Coal fly ash and residual oil fly ash have been studied as examples of combustion particles enriched in transition metals. Residual oil fly ash has been shown to induce inflammatory cytokines in human bronchial epithelial cells[314] and both lung inflammation[326] and cardiac arrhythmia[158] in inhalation studies with rats. Coal fly ash has been shown to be a source of bioavailable iron[343] and can also induce inflammatory cytokines in human lung epithelial cells.[344] Generation of ROS and induction of cytokines in human bronchial cells has also been reported in studies of diesel exhaust particles.[400] The amount of bioavailable transition metals contained in particles has been associated with acute lung inflammation from both combustion and ambient particles.[317] Studies have considered the water-soluble transition metals,[159] metals associated with organic material,[392] and metals that can be mobilized by an intracellular chelator at physiological conditions.[342]

A study of ROS generation in polymorphonuclear leukocytes (a white blood cell type frequently found in the airways of persons exposed to particles) using oil fly ash, coal fly ash, carbon black, natural dust, and ambient particles reported that the ROS correlated with the fraction of Si, Fe, Mn, Ti, and Co that was not removed by distilled-water washing.[401] In studies with coal fly ash and geological dusts,[402] the amount of bioavailable Fe under physiologically relevant in vitro conditions did not correlate with the total Fe in the particles, as shown in Figure 18.[342,343,403,404] Cultured human lung epithelial cells (Type A549) were exposed to PM_1-enriched coal fly ash

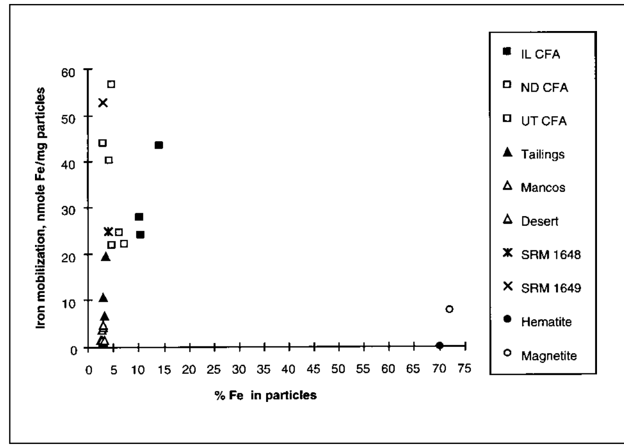

Figure 18. Iron mobilized by the chelator citrate and physiological pH from three types of coal fly ash, two types of dust from unpaved desert roads, mine tailings, urban particles, and pure iron oxides. The mobilized iron does not correlate with the total iron in the particles. Data sources: urban particles,[342] CFA,[343] geological dusts,[403] iron oxides.[404]

both as-collected and after pretreatment with the chelator desferrioxamine B. The chelator removed the ability of the coal fly ash to induce the synthesis of the proinflammatory cytokine IL-8.[344] Mössbauer spectroscopy of the coal fly ash before and after the desferrioxamine B treatment showed that Fe in an aluminosilicate glass phase was preferentially removed.[348] Fe in aluminosilicate glass occurs in combustion ash that is produced by rapid quenching from high temperature, but is not commonly found in dusts with similar elemental composition that have been produced by geological weathering.

Traditional mass transfer and heterogeneous chemical reaction theory[405] was applied to analysis of the measured rate of Fe mobilization from various sizes of coal fly ash by the chelator citrate. The rate of Fe mobilization was consistent with solid-phase-limited diffusion mass transfer, but the final values were consistent with size-dependent differences in initial composition.[402] Such size-dependent composition differences are expected from the mechanism of coal fly ash formation described in the fundamentals section above. These results show the importance of particle size and chemical speciation in the activation of specific biochemical pathways and suggest mechanistic reasons for differences in the response of the body to combustion and geological particles.

Soot and Biochemical Processes

Soot is the major type of combustion-derived ultrafine PM, and associated organic and inorganic compounds cause soot to have mutagenic, carcinogenic, and irritant properties. A study of size-fractionated urban PM showed that the mutagenic activity increased with decreasing particle size,[333] which is consistent with expectations for organic compounds condensed on submicron combustion particles. The indeterminate chemical composition of the EC and OC mixture emitted from combustion, ranging from fuel-like hydrocarbons to primary particles formed from graphite-like fused aromatic rings, greatly complicates biochemical studies. Carbon black is often used as a surrogate for the EC component of real combustion soot.[329,330] Various solvent extracts of soot, or isolated compounds such as specific PAH species, have been used as surrogates in toxicological studies of the OC fraction of combustion soot. Many PAHs are suspected carcinogens and mutagens,[406] and there has been considerable controversy regarding the role of nitroaromatic compounds because of the differing results in bacteria and mammalian cells.[407] Quantified compounds account for only a fraction of the observed mutagenicity of real soot mixtures.

Chlorinated polycyclic aromatic compounds, especially polychlorinated dibenzo-p-dioxins, and furans are also associated with combustion emissions. These compounds are fat-soluble, accumulate up the food chain, and have been suspected to disrupt or mimic the action of developmental hormones.[408] The most-studied effects involve chronic exposure, but the possibility of acute effects from these compounds cannot be ruled out. The chlorinated dioxin and furan compounds are a special concern for municipal and medical waste incineration.[231] Emissions of chlorinated dioxin and furan compounds do not appear to be a problem when burning fuels that contain more sulfur than chlorine, such as coal.

Ultrafines

Ultrafine particles and nanoparticles have been proposed by some health researchers[377] as the biologically important ambient particle. Ultrafine particles are deposited by diffusion deep in the lung and have been found by Oberdörster et al.[331] to be retained in the lungs. Ultrafine particles can also pass through the cells lining the lung and enter the interstitial space. Table 9 summarizes studies with micron-sized and ultrafine particles of the same compound.[319,329,331,409–411] The data show that ultrafine particles often have a greater biological effect than an equal mass of larger particles of the same substance.

For slightly soluble particles, the high surface area of ultrafine and nanoparticles can result in a faster release of toxic compound than would result from larger particles of the same composition. The concentration of a toxic substance reached in cells or in body fluids is the dynamic result of the relative rates of release from the particle and of clearance of the toxic material from the body.

Synergistic Effects

The combination of multiple toxic substances often has a much greater effect than the sum of the effects of the individual substances. Historically, emissions of combustion particle and sulfur oxides have been closely linked. Separating the effects of these pollutants was difficult since both were produced from burning coal. Coal was used extensively in urban areas for both industrial steam engines and domestic heating in Europe and North America prior to the 1950s, when natural-gas pipelines, automobiles, and regulations for large industrial sources changed the emission pattern. European regulations treated these pollutants as a combination and set a limit on SO_2 that varied with the smoke concentration (roughly a measure of EC).[362,412] The assumption underlying this approach was that acid gases adsorbed on the surface of particles could be transported into the lung, whereas vapor-phase acid would diffuse to the wall of the upper respiratory tract. Amdur and coworkers conducted extensive studies of the health effects of H_2SO_4 aerosols, both as a pure component and in combination with coal fly ash.[25,26,413]

Amdur[25,26] reported that a 10-fold increase in dose with acid aerosol alone was required to match the effect on lung-diffusing capacity caused by inhalation of H_2SO_4 condensed on PM. A concentration of 310 mg/m^3 of H_2SO_4 mist corresponded to the same change in diffusion capacity as occurred when the H_2SO_4 was surface-layered on a coal fly ash particle at a concentration of 30 mg/m^3. In addition, the type of particle was also important. Amdur found that with lignite, which has higher Ca and Na than does bituminous coal, the H_2SO_4 reacted with the alkali to form sulfates. With bituminous coal, which has Al, Si, and Fe-rich ash, H_2SO_4 persisted on the particles. Synergistic effects between other combustion-generated pollutants occurring on the same particle have been studied. For example, the combination of benzo[a]pyrene adsorbed on carbon black caused release of tumor necrosis factor-alpha and caused programmed cell death of lung macrophages, but neither carbon black nor benzo[a]pyrene had this effect alone.[316] Other synergistic effects involve particles plus a gas-phase pollutant, such as O_3.[320]

Importance of Chemically Speciated PM Sampling

Equal mass doses of sea salt, desert dust, and diesel exhaust are unlikely to have the same effect on the body. The startup of a large number of air monitoring sites that will routinely report individual chemical categories of PM (EC, OC, SO_4^{2-}, NO_3^-, other inorganic) and the funding of EPA particulate research centers and Supersites will provide input data for epidemiology studies. Improved characterization of combustion and other PM sources will provide data needed to relate the chemical speciation at receptor sites to the major sources. Controlled toxicology studies using exposure to well-characterized components

Table 9. Studies of ultrafine vs. larger particles of the same substance.

Material	Dose/Method	References	Results
Titanium dioxide 20-nm and 200-nm	Rat, instillation	331	Increased pulmonary toxicity of ultrafines related to surface area and the ability to enter interstitial spaces. Alveolar macrophage involvement.
Titanium dioxide 20-nm and 250-nm	Rat, inhalation, 22 mg/m^3, 6 hr/day for 6 months	410	Greater inflammatory response at equal dose with 20-nm particles.
Titanium dioxide 21-nm and 120-nm	Rat explants in vitro	411	Ultrafine particles were able to induce procollagen expression, which is related to development of airway fibrosis.
Carbon black 14-nm and 260-nm	Rat, instillation	329	Ultrafine carbon black had greater ability to produce lung inflammation at low dose.
Carbon black 14-nm and 260-nm	Rat, inhalation 1 mg/m^3, 7 hr one-time	319	No effect with 260-nm particles. Ultrafine produced proinflammatory response, oxidative stress, increased procoagulant blood factor.
Magnesium dioxide UF, 28% < 0.1 µm F, 98% < 2.5 µm	Human, inhalation	409	No significant differences in bronchoalveolar lavage cell concentration or cytokine concentration. Suggested that particle composition, not size alone, is significant.

of ambient aerosol will be needed to develop a mechanistic understanding of how particles affect the body.

AIR QUALITY REGULATIONS

The preceding discussion of the respiratory system and air pollution health effects sets the framework for discussing air quality regulations. These regulations have the primary purpose of protecting human health and the secondary purpose of reducing other environmental impacts of pollution. Environmental laws must be unambiguous for the regulated sources, the enforcement agencies, and the affected public. A prerequisite to developing a rule is that a means must exist to measure the component(s) to be regulated so that compliance monitoring can take place. This monitoring must be cost-effective and reproducible. As a result, the existing regulations focus on regulating ambient concentrations of pollutants for which reasonable cost, robust, and precise measurement methods are available.

Three sections of the U.S. Clean Air Act apply directly to PM. The most important of these are the NAAQS, which include PM_{10} and the newly implemented $PM_{2.5}$ regulations. The EPA[301] has indicated that the PM_{10} trend is improving, with a decrease of 26% in average ambient concentrations from 1988 to 1997. In 1987, the original NAAQS for total suspended PM was replaced by a PM_{10} standard set at 150 µg/m^3 24-hr average and 50 µg/m^3 annual average. The legal requirement to periodically review the standards, combined with growing epidemiologic evidence and a citizen lawsuit, lead to further rulemaking. In 1997, the EPA revised its existing PM standards by adding the $PM_{2.5}$ standard.[414] The annual standard is set at 15 µg/m^3, with a new 24-hr standard set at 65 µg/m^3. The PM_{10} annual standard was retained, but the statistical method of determining compliance with the 24-hr average was modified. The scientific evidence considered by the EPA in setting the standard was compiled into a criteria document.[305]

It should be noted that the standard was recently (May 14, 1999) challenged, and a panel of the U.S. Court of Appeals for the District of Columbia remanded the new standards for $PM_{2.5}$ and O_3. In a summary of the decision, the EPA points out that the court did not question the health evidence for the standard; rather, the decision required more explanation of the process used to set the standard. Congress has required the National Research Council to form a committee to guide the PM research and monitoring agenda. This committee is charged to write four reports between 1998 and 2002, when EPA is to complete a 5-year scientific review of the standards, leading to possible revision. Two of the four reports have been completed.[415,416] The current regulation is based on $PM_{2.5}$ measured by the Federal Reference Method. This mass is dominated by secondary SO_4^{2-} and NO_3^- aerosol and by EC and OC. Submicron inorganic ash and ultrafines from combustion are a small part of the $PM_{2.5}$ mass in many locations. However, the mass measurements do not directly relate to the previously discussed mechanistic toxicological hypotheses. Other characteristics, such as the morphology and chemistry of ultrafine particles, may be more important than simple mass. The EPA is attempting to address this fact by its ambitious Supersite program. These Supersites intend to support the on-going health studies by obtaining chemical- and time-resolved data using a range of research methods. However, one must realize that cost-effective, robust, and simple monitoring methods must be available before any change in the present standards can be realistically promulgated and implemented.

The second regulation can be found in the regional haze rule.[417] Decreased visibility occurs due to the scattering and absorption of light by particles. This is of particular concern in the 156 National Parks and Wilderness Areas that are designated as mandatory Class I air quality areas in the United States. Since fine particles are transported over hundreds of miles, all 50 states will have to participate in planning, analysis, and, in some cases, emission control programs. Since submicron particles scatter light efficiently, combustion-generated PM has a large impact on visibility, even when the primary combustion PM represents a small part of the total $PM_{2.5}$ mass. The EC, which results in light absorption rather than light scattering, is particularly important for visibility. In addition, secondary PM, not covered by this review, is important. Regulations to control acid rain precursors and photochemical smog precursors also reduce the ambient particle concentration, since SO_2 and NO_x are also the precursors of secondary SO_4^{2-} and NO_3^- particles. Visibility rules may prove to be more stringent than health standards in controlling the emission of submicron particles from combustion sources.

Finally, the Clean Air Act Amendments of 1990 require the EPA to address 188 hazardous air pollutants (HAPs). Included in this list are As, Be, Cd, Co, Cr, Hg, Ni, Mn, Pb, Sb, and Se, which are contained in fuels. The accumulation of toxic metals, such as Se and Hg, and the accumulation of persistent organic compounds, such as chlorinated dioxins and furans, in ecosystems is a concern that affects standards for combustion particle emissions. Current regulations focus on sources emitting greater than 25 tons/year, and electric utility steam-generating boilers are temporally exempt from the regulations. Due to amplification in the food chain, and to public concern for wildlife and endangered species, these indirect effects of particles may also result in more stringent regulation of sources. Complying with the ecological goals of the HAP regulations will require an understanding of the relationship between combustion conditions and the emissions of these trace elements.

Adverse health effects originally identified by epidemiology studies motivated the public perceptions and legal actions that have resulted in new regulations for ambient PM. Current air quality standards are based on the mass of particles smaller than a specified size; however, toxicological studies may eventually identify specific categories of ambient PM that need stricter control to protect public health. Advances in understanding the formation and transformation of combustion aerosols and advanced monitoring techniques must take place to meet the challenge of setting and complying with regulatory standards.

TIME- AND SIZE-RESOLVED PARTICLE MEASUREMENTS

The ability to test various health-related hypotheses is closely linked to which PM characteristics can be measured at combustion sources and in the ambient air. The particle measurement issues that are especially relevant for testing current health effects hypotheses regarding metals, ultrafines, and soot from combustion sources include

- *Measurement Artifacts*. This includes all the particle transformations that can be different between a sampling train and the ambient air. Due to the effects of temperature-dilution history on the partitioning of chemical species between the gas phase and the particles, the PM that is measured in the laboratory may have a different size-dependent composition than the PM to which the population is exposed. Also, transformation of the particle size distribution due to coagulation, surface condensation, chemical reactions, and size-selective removal may occur as a result of the sampling methodology.
- *Instrument Limitations*. Methods are needed to measure particle-to-particle variation, which provides information that is lost in the bulk average properties of the PM collected by filter sampling. Rapid response instruments are needed to quantify short duration transients in particulate air pollution that may have significant health effects. Many methods for measuring aerosols that were developed for supermicron particles need to be modified or extended for ultrafine PM.

Measurement Artifacts

The historic regulation of the total PM mass smaller than a given size has produced precise mass measurement techniques. Since the largest particles dominate the mass, there has been an emphasis on isokinetic sampling. There has also been concern about equilibrating the samples to constant humidity before weighing, even though the mass of particle-bound water is unlikely to have biological importance. The techniques that yield precise mass measurements may, however, introduce serious artifacts if the goal is to obtain data on submicron particle composition and size distribution. For example, allowing air of variable temperature, pollutant concentration, and humidity to pass over the accumulating filter deposit for 1–6 days can strip the more volatile species from the collected particles before the sample is weighed. This has led to the development of samplers that can quantify the volatile PM.[418,419] While there is uncertainty regarding the significance of the mass of volatiles adsorbed on particles, this serves as an example of the importance of using appropriate particle measurement methods when testing a given toxicological hypothesis.

Condensable PM, that is, material that condenses into a liquid or solid within a few seconds of leaving the stack, can be comparable in mass to the filterable PM_{10} measured in the stack of a power plant.[420] Currently, U.S. regulations do not require measuring condensable PM when stack-testing stationary sources. This is another example of how measurement protocols developed for regulatory compliance do not collect the data that is most needed for health and environmental studies.

Dilution tunnels were developed for measuring condensable particulate, including both SO_4^{2-} aerosol and organic compounds from vehicle exhaust and stationary sources of VOCs.[278,421] The dilution tunnel process involves mixing the hot combustion emissions with filtered air, allowing a short residence time, then extracting a particulate sample for either on-line analysis or for collection on a filter. Dilution tunnels were developed to measure mass and chemical composition of PM. The possibility that a laboratory dilution tunnel could create a different particle size distribution than the size distribution that occurs during natural dilution was pointed out by Kittelson and Dolan 20 years ago.[422] Since then, many papers have discussed the artifacts that can occur in dilution tunnels.[265,423–428]

The formation of particles during dilution depends on the opposing effects on condensation of the decreasing saturation pressure of the volatile species due to cooling and the decreasing partial pressure of the volatile species due to mixing. The saturation reaches a peak in the dilution range of 5:1 to 50:1, depending on the boiling point of the volatile species and the initial temperatures of the exhaust and dilution gases. Particles will be formed by nucleation if the mixture stays in this dilution range for sufficient time for significant mass transfer to take place. Typical dilution tunnels operate in the range of 3:1 to 20:1 and have residence times on the order of seconds, so critical supersaturation may be exceeded long enough for formation of nuclei particles followed by rapid growth from condensation. The formation of H_2SO_4/H_2O particles is an example in which dilution conditions influence the measured particle number both in dilution tunnels[429] and in the atmosphere.[430]

Unlike mass, particle number is not conserved, and the effect of dilution conditions makes it difficult to compare the particle number size distributions measured by different investigators. This is especially important when using combustion source measurements for investigating the health effects of ultrafines and nanoparticles. Changes in particle number of up to 2 orders of magnitude have been reported when conditions were varied over the typical range used in laboratory dilution systems.[429] Initial combustion exhaust conditions, dilution history, dilution gas temperature and relative humidity, and the residence time interact to affect nucleation and surface growth. Careful interpretation of conditions used for experiments is required. For example, diesel exhaust studies have reported that high dilution ratio both increases[426] and decreases[429] formation of particles below 50 nm.

Research studies of the particulate emissions from IC engines fall into two groups: studies of the transient mixing and chemical reactions inside the cylinder, and studies of the tailpipe emissions to the atmosphere. Between these points is the exhaust system in which the undiluted exhaust cools and ages, but is not diluted. The gas residence time in the engine cylinder is 10–30 msec, depending on engine speed. The time from the cylinder to the atmosphere for a typical heavy-duty truck engine exhaust system is 100–300 msec, about 10 times greater. The extractive particle sampling systems used by various investigators can add another 0.25–1 sec or more to the age of the aerosol before dilution begins. The dilution of tailpipe exhaust under highway conditions starts at the tailpipe and is about 1000:1 after 1 sec.[423] The coagulation of equal size particles is proportional to n^2, so most particle growth by coagulation takes place prior to the onset of exhaust dilution. Under urban conditions, once combustion exhaust is diluted more than ~100:1, the collisions between accumulation mode particles from the ambient air and ultrafines from the combustion source become significant compared with the coagulation between ultrafine particles originating from a single source.

The ultrafine particle size distribution formed from hot diesel exhaust in a laboratory dilution tunnel operating with filtered air may be very different from the size distribution formed under roadway dilution conditions with ambient air. Ambient air contains accumulation mode particles that, due to the increased collision rate between particles of different size, increase the rate at which the nuclei and condensation mode ultrafines are depleted. A novel approach to studying dilution effects involves the simultaneous use on a moving truck of both a dilution tunnel extracting from the tailpipe and an in-plume sampler with the inlet mounted on the rear of the trailer.[431] For these experiments, the dilution system measurement showed a smaller accumulation mode mean size than did the in-plume measurement.[432]

Nanoparticles are difficult to measure because they are rapidly transformed by coagulation, surface growth, and transport to the walls of the equipment. Internal combustion engine particle number measurements may contain artifacts from the sampling lines due to both desorption of condensed material and reentrainment of deposits. A dynamometer study comparing tailpipe and dilution tunnel measurements of gasoline vehicle exhaust particle concentration found that a heated and insulated transfer line resulted in a very intense nanoparticle mode when the drive cycle involved operation at high vehicle speed.[433] This ultrafine mode was not detected under identical operating conditions with an unheated transfer line. This artifact was attributed to the hot exhaust increasing the transfer line temperature above 180–250 °C, resulting in desorption/pyrolysis of organic material in the line.

There is a need for improved technology for making laboratory measurements of combustion PM that can be related to the real behavior of particles in the combustor exhaust, the initial plume, and the atmosphere. Computer simulations of the fundamental mechanisms of aerosol formation and transformation can be used to interpret and compare particle size distribution data collected under various dilution configurations. Rapid dilution is essential if the ultrafines generated in combustion are to be measured. Likewise, ultrafines are most likely to survive from the combustion source to inhalation exposure when there is rapid dilution with relatively clean ambient air.

The commonly used instruments have limitations that may introduce artifacts into measurements of ultrafine particles. Many published graphs of combustion particle number distributions show the highest concentration in the smallest size range measured by an SMPS. This makes the integrated total particle number suspect since there may be extremely high concentrations of undetected nuclei particles present. Some authors explicitly acknowledge this measurement truncation problem by stating the results as the total number within the range of the SMPS. Another approach, for example, that used by Khalek et al.,[262] is to fit a lognormal distribution to the data with an algorithm that allows for truncated measurements. Truncation of the measured size distribution is an important issue both when using experimental data as the input to a coagulation model calculation and when testing toxicological hypotheses related to ultrafine particle number.

Characterization of particle number and chemical composition from combustion and other PM sources is important for both source apportionment studies of the submicron ambient aerosol and for designing controlled tests of particular toxicological hypotheses regarding ultrafines, metals, and synergistic effects between particle components. The size distribution measured from dilution tunnel sampling shows artificially high numbers of particles. However, there is also the possibility that a substantial portion of the nuclei is below the detection limit of the instruments used.

Instrumentation Needs

To understand what particle characteristics affect human health, we must develop ways to make inexpensive, robust measurements of particle size distribution, morphology, and chemical speciation. The important variables have not yet been identified, but the current inhalation toxicology research direction suggests that a better understanding of health effects will require more time-resolved, size-segregated, chemically speciated data from both combustion sources and ambient monitors. Testing of epidemiologic hypotheses requires wide-scale, long-term measurement of PM characteristics. The characteristics selected for measurement should be economical to quantify under field conditions and should be well correlated with the factors that are suspected to be biologically significant.

Filter samples provide only time-averaged aerosol properties, but individual particle composition contains information that is important for both source apportionment and toxicology studies. The urban aerosol contains contributions from nearby and regional sources, both natural and anthropogenic, that have aged in the atmosphere from minutes to days. A typical ambient particle that is inhaled consists of coagulated primary combustion particles or geological particles, coated with some mixture of condensable organic species, secondary SO_4^{2-} and NO_3^-, and H_2O at equilibrium with local humidity. The particle-to-particle variation reflects different sources and transformation histories. The different particle types within the ambient mixture are likely to have different effects when inhaled. The information on particle-to-particle variation is preserved by single particle techniques, such as electron microscopy and aerosol mass spectrometry. However, it is necessary to efficiently measure a statistically large population of particles to obtain meaningful ensemble averages of the ambient PM as a function of time and place.

The wide variation in the physical and chemical characteristics of combustion PM emissions as operating conditions change creates a need for near-real-time measurements that can capture both the transient emissions and the variation between individual sources in a category. For IC engines, toxicological hypotheses motivate a desire to characterize the soot, the soluble organic compounds including individual PAH, the ultrafine particle number, and the metal speciation with various fuels at various speeds and loads. Likewise, measurements of a few boilers, gas turbines, or fireplaces cannot be expected to fully describe the emissions from all similar sources. One of the most challenging combustion PM problems is to characterize highly variable sources such as open burning and domestic biomass combustion. Compliance monitoring methods such as filter sampling of an automobile over the FTP drive cycle, or a 2- to 4-hr steady-state stack test of a boiler, cannot measure the transients. Collecting statistical data on a representative sample of in-service sources is slow and very expensive using compliance methods. This section will discuss some of the research instruments that may offer improved capability to make time- and size-resolved measurements of $PM_{2.5}$ and ultrafine PM.

Desirable instrument characteristics for testing epidemiologic hypotheses include low cost per data point to allow collection of sufficient data to perform statistical analysis, rapid response to allow tracking of transients, reliability and ruggedness to allow use under field conditions, and reproducibility to allow comparisons between investigators. Desirable characteristics for source apportionment and toxicology studies are the ability to provide information on detailed morphology and chemical composition that is relevant to the origin of the particle and its behavior inside the body.

Chemical analysis techniques for source apportionment rely on variation in the concentration of specific compounds that provide individual “markers” or “fingerprints” (i.e., characteristic patterns) for identification of sources. The pioneering studies used elemental composition: Pb for gasoline engines, V for oil-burning power plants, Se for coal-fired boilers, and Al for geological materials.[306] This allowed identification of only a few categories, and changes in technology, such as the phase-out of leaded gasoline, have eliminated some of the markers. Compared with less than 50 elements that are potential markers of combustion particles, organic compounds provide tens of thousands of potential markers, allowing detailed identification of combustion sources.[156,298,434,435] A “memory” of the original fuel is preserved in the detailed composition of the products of incomplete combustion. A limitation of these organic markers is the time needed to collect and analyze a sample by conventional solvent-extraction and gas chromatography. An alternative technique, currently being tested in research programs, is thermal desorption gas chromatography (TD-GC),[436] which involves controlled heating of a lightly loaded particulate filter. This method has been shown to provide composition data with 2-hr time resolution that are nearly identical to collocated 24-hr samples that were analyzed by conventional solvent-extraction, GC/MS methods. Prototypes indicate that TD-GC has the potential to be fully automated in a field-transportable unit.

Another option for rapid organic analysis is the photoelectric aerosol sensor (PAS),[437,438] which provides a real-time indication of changes in the amount of particle-bound PAH. This instrument is compact and has a sensitivity of about 1 ng PAH/m^3.[439] The value of rapid time-resolved PAH measurement is illustrated by a study in which a PAS was installed near the runway of an Air Force base. The spikes in the signal could be correlated with flight logs showing the activity of specific aircraft, as indicated in Figure 19.[440] The PAS signal is a weighted sum from many chemical species. Some research has been completed to quantify the relationship between the PAS instrument reading and conventional measurements of individual PAH by traditional methods for a range of sources. The ability to make rapid semi-quantitative measurements of PAH is extremely valuable for characterization of the variation in the emissions from large populations of similar sources, and to study the effect of combustion transients on the time-averaged emissions. Ongoing research includes developing methods to use the PAS to monitor for high PM-emitting equipment in an operational fleet through edge-of-roadway or edge-of-runway real-time measurements.

Soot is a functional definition and actual combustion particulate emissions are a complex mixture of organic compounds ranging from unburned fuel to graphite-like polycyclic structures, making an arbitrary division into composition categories necessary. These divisions are based on behavior in an analytical procedure. The measured split between OC and EC is based on the light-adsorbing properties of a filter punch as a function of temperature, first under a helium atmosphere and then under an oxygen/helium atmosphere.[441] Changes in the procedure, for example, the NIOSH and IMPROVE methods, give different results.[442] The fuel- and lubricant-derived hydrocarbons are alternatively distinguished from the graphite-like carbon structures in soot by measuring the soluble organic fraction using dichloromethane or a similar solvent.[443] Further separation of the soluble organic compounds usually involves extraction with aqueous and organic solvents, acidic and basic solvents, and polar and non-polar solvents until various classes such as paraffins, aromatics, and oxygenates are isolated for analysis by gas chromatography.[275,276,444,445]

EC, or soot, is an important class of particulate air pollution, and the ability to economically make near-real-time measurements of EC is valuable for characterizing transient emissions from combustion sources. The photoacoustic analyzer detects light-absorbing particles (black carbon) by the transient heating resulting from a pulsating laser beam passing through the sample chamber.[446,447] A preliminary study of IC engine exhaust showed that the photoacoustic instrument response and the EC analyzed on filter samples by thermal/optical reflectance[441] correlated as shown in Figure 20.[448] This technique provides a rapid signal, making time-resolved measurements of events, such as sudden acceleration of

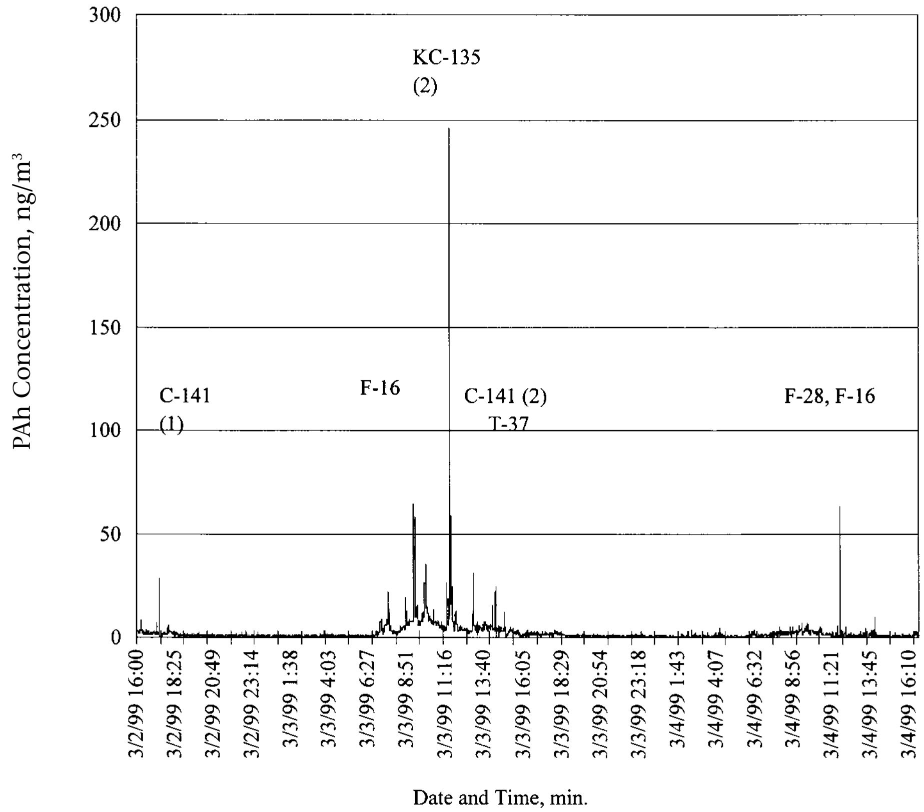

Figure 19. Time-trend data obtained by a PAS sampling at an Air Force base. The spikes in PAH concentration can be correlated with aircraft operations and with local ground traffic. Courtesy of G. Palmer.[440]

the engine, feasible. The instrument also has a wide dynamic range, making it suitable both for studies of transient emissions from combustion sources and for monitoring spikes in ambient concentration. The lower limit of detection for EC is 40 ng/m^3.[447] When developing alternative methods for measuring the health and visibility impacts of soot and of particle-bound organics, there is a need to compare these methods to existing EC and OC data. However, EC, as currently reported, is a method-dependent definition, so the relationship between methods is only an empirical correlation, not a fundamental relationship.

Electron microscopy, coupled with energy dispersive X-ray analysis, can provide size, shape, and elemental composition information on individual particles. Automated electron microscopy, also called CCSEM, allows the characterization of several hundred particles per hour and provides a powerful technique for characterizing both source and receptor samples for source apportionment studies.[449,450]

Concern over acid rain has motivated studies that have looked for coal particles in lake sediments as a tracer for rain-out from power-plant plumes. The methods used to identify coal fly ash in sediments can also be extended to plume tracking for health studies. An early example of using CCSEM in a health-related combustion particle study involved collecting particles from the plume of a coal-fired power plant using a helicopter. Kim et al.[451] showed that the plume particles could be distinguished from background PM by the characteristic morphology and composition of coal fly ash. Characteristics of combustion ash include large carbonaceous spheroidal particles[452] and glassy aluminosilicate spheres.[453,454] Advanced techniques for single particle analysis by microscopy have been reviewed.[455,456] A limitation to the study of submicron particles is that the spatial resolution of many techniques, such as energy-dispersive X-ray analysis, is comparable to the size of the particles.

The aerosol time-of-flight mass spectrometer (ATOFMS) is the most sensitive technique currently available for on-line measurement of the size and chemical composition, both organic and inorganic, of individual aerosol particles. The size and chemical composition of hundreds of particles per minute can be obtained. Fundamentals of the ATOFMS technique and recent advances in aerosol mass spectrometry are discussed in a review,[457] which lists the contributions of 17 research groups. Figure 21 illustrates the capabilities of an ATOFMS research

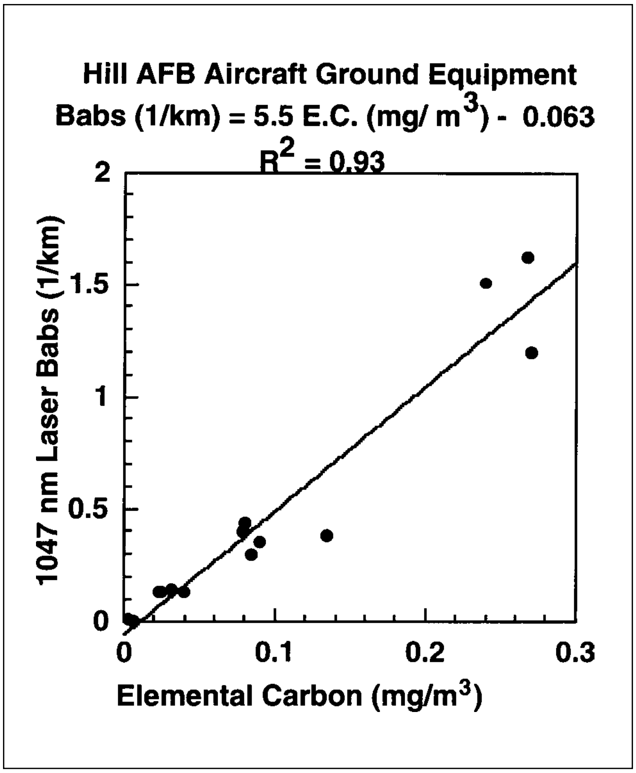

Figure 20. Comparison of near-real-time light absorption measured by the photoacoustic analyzer (PA) and EC measured by thermal-optical reflectance (TOR) of filter samples.[448] The two techniques show good correlation for a range of IC engine sources. Courtesy of P. Arnott.

instrument similar to a design that is now commercially available. Studies have compared the composition of source PM and of ambient PM by cascade impactor time-averaged samples and by time trend data from the ATOFMS.[458] Real-time characterization of aerosol time-of-flight mass spectroscopy has also been used in studies of diesel exhaust to study PAH composition under various operating conditions.[459]

Figure 21 illustrates four single particle mass spectra sampled using an on-line single particle mass spectrometer developed at the University of California, Riverside.[457,460] These four single particles are representative of (a) diesel- and (b) gasoline-powered vehicular OC-containing particulate emissions, (c) coal combustion, and (d) ambient dust. Figures 21a–c show single particles collected during controlled source characterization studies utilizing a dilution sampler.[276,278] These illustrate how single particle source characterization studies allow for the identification and differentiation of PM sources. Figures 21a-1 and 21a-2 are the cation and anion spectra, respectively, of an OC-containing particulate emitted from a 1994 Ford E350 diesel truck. The cation spectrum contains many low mass organic fragments, as well as nitrogen-containing species. Peaks of interest from the cation spectrum include m/z 12 (C^+), m/z 18 (NH_4^+), m/z 27 ($C_2H_3^+$), m/z 43 ($C_3H_7^+$, $C_2H_3O^+$, $CHNO^+$) m/z 86, and m/z 101. The

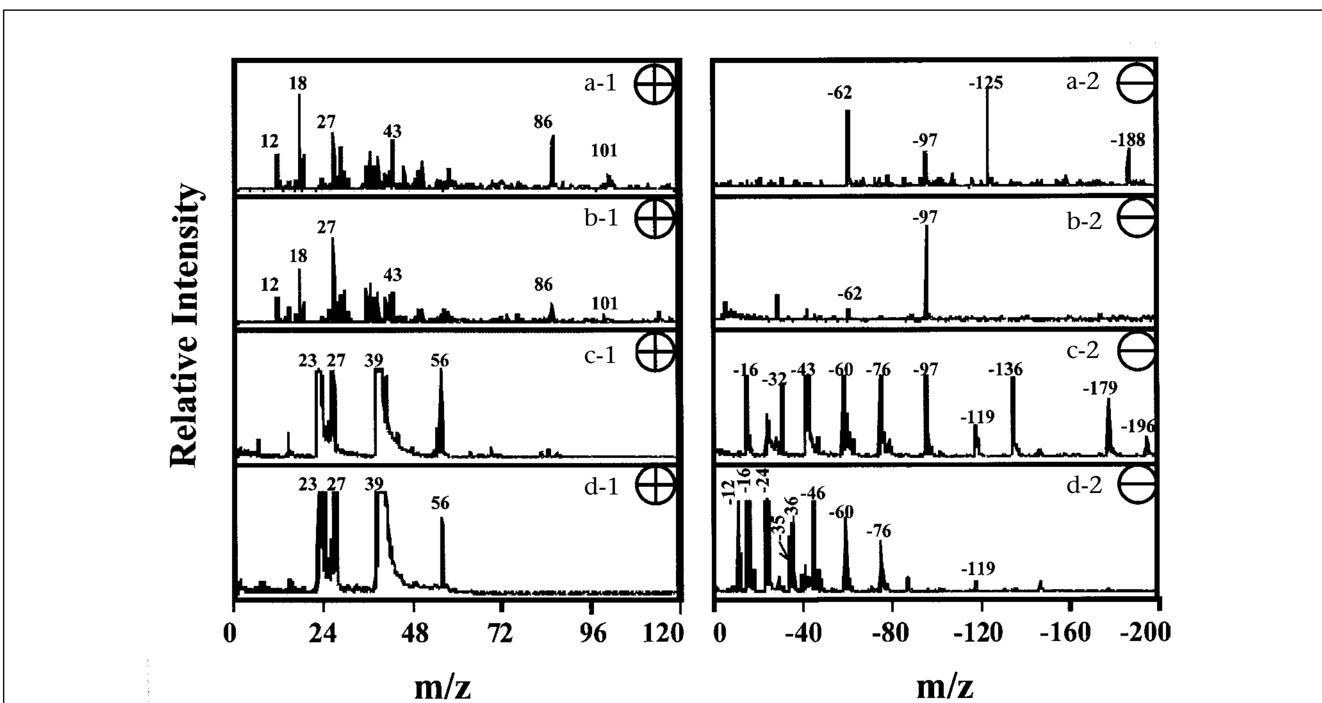

Figure 21. Mass spectra from four different single aerosol particles. a-1 through d-1 are single particle cation spectra and a-2 through d-2 are their associated anion spectra. a-1 and a-2 are from a single particle emitted from a diesel-powered 1994 Ford E350 truck. b-1 and b-2 represent a single particle emitted from a gasoline-powered 1993 Honda Civic. c-1 and c-2 represent a single particle emitted from the combustion of Illinois coal. d-1 and d-2 represent an ambient Riverside, CA, dust particle collected on Oct. 7, 1999. Each of these single particles is representative of its specific source or type. Courtesy of K. Prather and D. Suess.

anion spectrum contains fewer signals, and these are dominated by sulfur- and nitrogen-containing species including m/z –62 (NO_3^-), m/z –97 (HSO_4^-), m/z –125 ($HN_2O_6^-$) and m/z –188 ($H_2N_3O_9^-$).

Figures 21b-1 and 21b-2 are representative OC-containing single particles emitted from a gasoline-powered 1993 Honda Civic. The cation spectrum, Figure 21b-1, contains very similar low-mass organic fragments to those observed from the diesel-powered vehicle, 21a-1. Therefore, differentiating OC-containing single particles from gasoline- and diesel-powered vehicles solely by their positive spectra is not possible. However, with additional information from the anion spectra, these OC-containing single particles can be differentiated. Figure 21b-2 does not contain signals at m/z –125 or m/z –188. As shown in Figure 21a-2, signals at these m/z values are associated with diesel-powered OC vehicular emissions.

Figures 21c-1 and 21c-2 are representative Illinois coal combustion. The cation spectrum contains signals at m/z 23 (Na^+), m/z 27 (Al^+), m/z 39 (K^+) and m/z 56 (Fe^+). In contrast to Figures 21a and b, the complexity of this inorganic particle type lies in the anion spectrum. Chemical species present in Figure 21c-2 include m/z –16 (O_2^-), m/z –32 (S^-, O_2^-), m/z –43 (BO_2^-), m/z –60 (SiO_2^-), m/z –76 (SiO_3^-), m/z –97 (HSO_4^-), m/z –119 ($AlSiO_4^-$), m/z –136 ($Si_2O_5^-$), m/z –179 ($AlSi_2O_6^-$), and m/z –196 ($Si_3O_7^-$). Figures 21d-1 and 21d-2 represent an ambient dust particle sampled in Riverside, CA, on October 7, 1999. The cation ambient dust spectrum is indistinguishable from the coal combustion single particle cation spectrum in Figure 21c-1, but the anion spectra allow for differentiation between these single particle types. Signals in Figure 21d-2 differing from Figure 21c-2 include m/z –12 (C^-), m/z –24 (C_2^-), m/z –35 (Cl^-), m/z –36 (C_3^-), and m/z –46 (NO_2^-). Interestingly, the sulfur-containing species are absent from the ambient dust single particle, as well as from higher mass silicate clusters.

As more single particle source characterization studies are performed, the goal of performing source apportionment of ambient aerosols on a single particle basis becomes more feasible. Data such as these illustrate that it should be possible to distinguish vehicle emission particles from different engine types from other combustion processes such as coal. In addition, the differentiation of coal from ambient dust should be possible using the unique combination of ion markers shown here.

The ATOFMS measurements of single particle composition can provide data on the variation in both source and ambient particles that is lost in filter samples. This allows detailed characterization of both combustion sources and ambient particles on a level of detail that will be suitable for testing of specific toxicological hypotheses; however, this technique has limitations. Large particles are preferentially detected by the ATOFMS, which requires correcting the raw data for the counting efficiency.[461] The current limit of detection is ~0.2 µm. Work is on-going to extend the capability of this technology to characterize ultrafines and nanoparticles.

Both source-based modeling and ambient studies with real-time instruments have demonstrated that the composition of the ambient aerosol has short-term variation as the wind brings in particles from various mixtures of sources. Presently, the relative importance of time-averaged exposure versus short-term exposure to spikes in the ambient aerosol composition is unknown. Some laboratory studies have shown strong responses from short exposures to high particle concentrations.[462] Figure 22 shows the time-resolved PM_{10} and $PM_{2.5}$ measured at an active military base located near an urban area.[440] These transients are suspected to result from nearby sources. The ATOFMS, PAS, and photoacoustic analyzer and similar near-real time instruments provide the analytical tools needed to begin testing hypotheses related to transient exposure. Advances in both data reduction capability and in instrumentation capability, especially with regard to the submicron and nanoparticle components, are still needed.

CONCLUDING COMMENTS

Providing the scientific basis for improved regulation of the emission of combustion particles requires an interdisciplinary approach with interactions between researchers in combustion, air pollution control, atmospheric transport and transformation, exposure assessment, and health effects, together with the regulatory community. The review has touched briefly on relevant information in these areas, providing references for the reader interested in more detailed coverage. Gaps exist in the scientific understanding of all elements of the problem, but the greatest gaps are at the interfaces between the fields. In addition to the need to fill these gaps, there is a need for a better balance between applying the knowledge that has been gained to answer pressing questions and refining the theory to gain better solutions. Significant progress has been made in understanding the processes governing combustion particle formation:

- Particles emitted from combustors are either generated by condensation or, in the case of soot, molecular weight growth reactions that lead to the formation from the gas phase of submicron aggregates of primary particles. Significant progress has been made in understanding the factors controlling the amount, size, and composition of these submicron particles. Their mass is determined primarily in the early stages of combustion for soot, inorganic ash, and condensable hydrocarbons. H_2SO_4 is controlled by

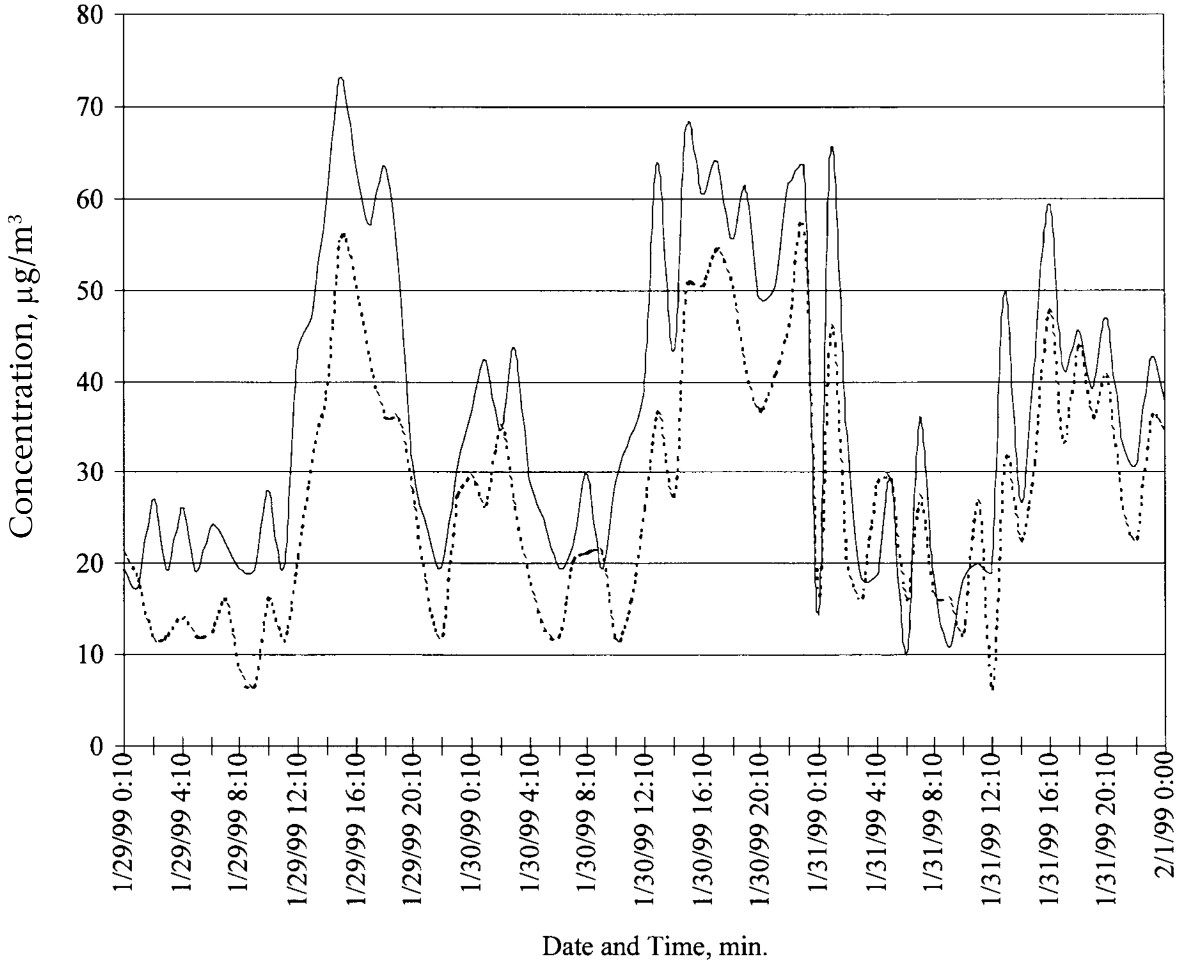

Figure 22. Time trend measurements of PM_{10}(——)and $PM_{2.5}$(------) by a beta attenuation meter show short-term spikes in fine particles, presumably from nearby combustion sources. Courtesy of G. Palmer.[440]

the oxidation of SO_2, primarily catalytically, on tube surfaces, fly ash, and, for certain vehicles, catalytic converters. The number and size distribution of the aggregates is controlled by collision and coagulation processes that are relatively well understood.

- Supramicron combustion-generated particles are produced by the agglomeration of the mineral content in fuels and by the coking of heavy hydrocarbons in fuel oils or coals. The size of these particles is, to an order of magnitude, equal to that of the parent fuel particles for pulverized or atomized fuels. The larger particles will be emitted only in the case of combustion systems not equipped with particulate control equipment. Large particles of carbonaceous material are also important for uncontrolled combustors such as fireplaces and open burning.
- Trace, sometimes toxic, elements are emitted in small enough amounts not to contribute significantly to the mass of the emitted particles. They are distributed between the sub- and supramicron particles emitted by combustors by condensation and surface reaction, sometimes modified by diffusion through pores. The processes governing the distribution of the trace elements are relatively well known; the size dependence of the concentration depends on the controlling mechanism and can provide a means for determining that mechanism.

The particle formation mechanisms have been used mainly in interpreting laboratory data. Although imperfect, they are at a stage where they can be incorporated in computational fluid dynamics simulations of furnaces and boilers to make predictive calculations of the particle size distribution and composition. In order to predict emissions, one needs to combine the information on the size and composition distribution of the particles emerging from combustors with information on the collection efficiency of the APCDs. The penetration of the APCD by particles will vary with the design and operation of the APCD. No control devices are installed on many small combustors or combustors operated with clean fuels, so that the emissions are closely approximated by the combustion emissions.

The limited studies of the PM at the inlet and outlet of APCD devices on full-scale combustion systems show that particle penetration is greatest in the 0.1–1.0 μm range, that is, in the transition of dominance of inertial forces to particle diffusion. There is a need to integrate models of the APCD with those of particle formation. At present, the greatest investment in the measurement of particle emissions has been carried out for compliance purposes and provides data on the total (not size-dependent) penetration efficiency of different elements. Without a mechanistic model, it is not possible to determine how these emission parameters change with changes in fuel, combustion conditions, or the operation and maintenance of the APCD. Further, little effort has been directed at extending the knowledge gained from studies of particle formation in engineered combustion chambers to some of the more mundane sources, such as domestic combustion and open burning. These types of sources are of increasing environmental importance as the emissions from boilers, furnaces, and IC engines become better controlled through improved technology.

Empirical emission factors become quickly dated as regulations are tightened, and as technological changes impact fuel composition and combustor design. The trends in emissions for major combustion sources show decreasing total mass emissions from coal-fired and oil-fired boilers and from on-road diesel engines. Modifications of older stationary sources and the retirement of older vehicles have more than offset the increases due to growing population and economic activity. More attention needs to be focused on biomass sources if these are used to significantly supplant fossil fuel combustors. A major question, however, arises as to whether decrease in mass emission per se achieves the desired impacts of safeguarding human health, since in many cases, the decrease in mass is accompanied by an increase in numbers of smaller particles.

Examination of the size and composition of combustion-generated particles shows that, compared with geologically generated ambient PM, they are smaller and have unique chemical composition and morphology that reflect the fuel composition, the combustion conditions, and the particle transformations between the furnace and the stack. The data generated for compliance purposes provide a starting point, but are not adequate to answer many of the health-related hypotheses being proposed. More characterization studies will be needed for particle sources, including measurements of transient emissions, detailed chemical speciation, and ultrafine particle number. The complex aerosol mixture produced by combustion is further transformed in the atmosphere before human exposure by mechanisms that, though subject to uncertainty, are sufficiently well understood to provide reasonable models of ambient particles from well-characterized emissions.

Epidemiology has demonstrated that susceptible individuals are being harmed by ambient particulate air pollution at levels comparable to the current air quality standards. Based on these findings, new regulations have been proposed for $PM_{2.5}$, but these have been contested. The proposed regulations based on mass loading are to be subject to review as current research leads to better understanding of the mechanism for the health impact of particles and of which specific size fractions and chemicals are responsible for these effects. Controlled studies with surrogate particles are being conducted to help unravel the various hypotheses proposed for the biological effects associated with the exposure to ambient particles. The problem is confounded by the probability that different particle characteristics are associated with different health end points in different susceptible populations. Particle surface area, number of ultrafine particles, and bioavailable transition metals are likely to be found to be more important than particle mass when correlating health effects with air pollution.

The understanding of the effects of particle air pollution on health has benefited from great advances in biochemistry and molecular biology on one side and from improved particle measurement capabilities on the other. Mechanistic toxicology studies are currently looking at the activation of specific genes and the synthesis of specific proteins in response to exposure to particles. Advances in the ability to collect time- and size-resolved research data on the composition of the ambient air will provide valuable input data for health studies and help identify the particle characteristics that are actually responsible for biological responses.

As the particles of importance to human health are identified, time- and size-resolved data will be needed for source apportionment studies both during the development of plans to improve air quality, and for the development of particle-control engineering technology for stationary and mobile sources. The health effects and apportionment studies can be assisted by the knowledge derived from the more fundamental studies on how fuel and combustion conditions affect size and composition of particulate emissions.

The observed association of increased ambient PM with adverse health effects and the lack of a toxicological mechanism provide the dilemma of balancing the added

Table 10. Nomenclature.

APCD	Air pollution control device
ATOFMS	Aerosol time-of-flight mass spectrometer
D_p	Aerodynamic or physical diameter of a particle
EC/OC	Elemental carbon and organic carbon, respectively, as measured by thermal/optical reflectance or a similar method
ESP	Electrostatic precipitator
EPA	United States Environmental Protection Agency
f_v	Volume fraction of a species (metal oxide or soot) per volume of gas
GC	Gas chromatograph
NAAQS	National Ambient Air Quality Standards
PAH	Polycyclic aromatic hydrocarbons
PM	Airborne particulate matter
SMPS	Scanning mobility particle sizer

cost to society of implementing imperfect regulations against the health costs of delaying action. The role of epidemiology during the 1854 cholera outbreak in London is instructive.[463] Dr. John Snow showed a correlation between cholera deaths and water from the Broad Street pump. Discovery of the germ theory of disease by Louis Pasteur was still 11 years in the future, and isolation of the cholera bacteria was 32 years in the future.[464] However, closing the well, based solely on associations and in the absence of a biological mechanism, stopped the epidemic and saved lives. Implementing a stricter fine particle standard can be seen as an analogous to "removing the pump handle." However, closing the offending well had a small cost, since other sources of water were nearby. Major reductions in the emissions of primary particles, especially ultrafines, from stationary and mobile combustion sources will require both advances in engineering practice and major investments of capital.

The cost of the implementation of the regulations can, however, be reduced by contributions provided by advances in the fields of aerosol and combustion science, combined with advances in biochemistry and toxicology. A causal relationship between ambient particles from different sources and specific health end points is needed to provide a sound scientific basis for regulations. These scientific contributions will eventually allow better prioritization of air pollution control resources. The tradeoffs between social costs and health risks are value judgments that need to be resolved through the political process, but that process can be assisted by the clarification of the scientific issues.

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REFERENCES

1. Mauderly, J.L. Summary of the Third Colloquium on Particulate Air Pollution and Human Health, Durham, North Carolina, June 6-8, 1999. In *Third Colloquium on Particulate Air Pollution and Human Health, Durham, North Carolina*; Air Pollution Health Effects Laboratory: University of California, Irvine, 1999; pp 3-9–3-14.
2. Glovsky, M.M.; Miguel, A.G.; Cass, G.R. Particulate Air Pollution: Possible Relevance in Asthma; *Allergy Asthma Proc.* **1997**, *18(3)*, 163-166.
3. Mauderly, J.L. Toxicological Approaches to Complex Mixtures; *Environ. Health Perspect.* **1993**, *101(Suppl. 4)*, 155-165.
4. Albritton, D.; Greenbaum, D.S. Atmospheric Observations: Helping Build the Scientific Basis for Decisions Related to Airborne Particulate Matter. In *PM Measurements Research Workshop;* Health Effects Institute: Chapel Hill, NC, 1998; pp 9-12.
5. Mauderly, J.; Neas, L.; Schlesinger, R. PM Monitoring Needs Related to Health Effects. In *Atmospheric Observations: Helping Build the Scientific Basis for Decisions Related to Airborne Particulate Matter;* PM Measurements Research Workshop; Health Effects Institute: Chapel Hill NC, 1998; pp 9-14.
6. Seinfeld, J.H.; Pandis, S.N. *Atmospheric Chemistry and Physics—From Air Pollution to Climate Change*; Wiley: New York, 1998.
7. Finlayson-Pitts, B.J.; Pitts, J.N.J. *Chemistry of the Upper and Lower Atmosphere: Theory, Experiments, and Applications*; Academic Press: San Diego, CA, 2000.
8. Flagan, R.C.; Seinfeld, J.H. *Fundamentals of Air Pollution Engineering*; Prentice Hall: Englewood Cliffs, NJ, 1988.
9. Ulrich, G.D. Theory of Particle Formation and Growth in Oxide Synthesis Flames; *Combust. Sci. Technol.* **1971**, *4*, 47-57.
10. George, A.P.; Murley, R.D.; Place, E.R. The Formation of TiO_2 Aerosol from the Combustion Supported Reaction of $TiCl_4$ and O_2; *Faraday Symp. Chem. Soc.* **1973**, *7,* 63-71.
11. Oxtoby, D.W. Nucleation. In *Fundamentals of Inorganic Fluids;* Henderson, D., Ed.; Marcel Dekker: New York, 1992; pp 407-442.
12. Oxtoby, D.W. Homogeneous Nucleation: Theory and Experiment; *J. Phys.: Condens. Matter* **1992**, *4*, 7627-7650.
13. Mirabel, P.; Katz, J.L. Binary Homogeneous Nucleation as a Mechanism for the Formation of Aerosols; *J. Chem. Phys.* **1974**, *60*, 1138-1144.
14. Flagan, R.C.; Friedlander, S.K. Particle Formation in Pulverized Coal Combustion–A Review. In *Recent Developments in Aerosol Science;* Symposium on Aerosol Science and Technology, Atlantic City, NJ, August 1976; Shaw, D.T., Ed.; Wiley: New York, 1976; pp 25-59.
15. McNallan, M.J.; Yurek, G.J.; Elliott, J.F. The Formation of Inorganic Particulates by Homogeneous Nucleation in Gases Produced by the Combustion of Coal; *Combust. Flame* **1981**, *42*, 45-60.
16. McLean, W.J.; Hardesty, D.R.; Pohl, J.H. Direct Observations of Devolatilizing Pulverized Coal Particles in a Combustion Environment. In *18th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1981; pp 1239-1248.
17. Seeker, W.R.; Samuelsen, G.S.; Heap, M.P.; Trolinger, J.D. The Thermal Decomposition of Pulverized Coal Particles. In *18th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1981; pp 1213-1226.
18. Timothy, L.D.; Froelich, D.; Sarofim, A.F.; Béer, J.M. Soot Formation and Burnout During the Combustion of Dispersed Pulverized Coal Particles. In *21st Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1986; pp 1141-1148.
19. Helble, J.; Neville, M.; Sarofim, A.F. Aggregate Formation from Vaporized Ash during Pulverized Coal Combustion. In *21st Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1986; pp 411-417.

20. Helble, J.J.; Sarofim, A.F. Factors Determining the Primary Particle Size of Flame-Generated Inorganic Aerosols; *J. Colloid Interface Sci.* **1989**, *128(2)*, 348-362.
21. Neville, M.; Sarofim, A.F. The Stratified Composition of Inorganic Submicron Particles Produced during Coal Combustion. In *19th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1982; pp 1441-1449.
22. Neville, M.; Quann, R.J.; Haynes, B.S.; Sarofim, A.F. Vaporization and Condensation of Mineral Matter during Pulverized Coal Combustion. In *18th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1981; pp 1267-1274.
23. Senior, C.L.; Flagan, R.C. Ash Vaporization and Condensation during Combustion of a Suspended Coal Particle; *Aerosol Sci. Technol.* **1982**, *1*, 371-383.
24. Peshty, A.J.; Flagan, R.C.; Seinfeld, J.H. The Effect of a Growing Aerosol on the Rate of Homogeneous Nucleation of a Vapor; *J. Colloid Interface Sci.* **1981**, *82(2)*, 465-479.
25. Amdur, M.O.; Sarofim, A.F.; Neville, M.; Quann, R.J.; McCarthy, J.F.; Elliot, J.F.; Lam, H.F.; Rogers, A.E.; Conner, M.W. Coal Combustion Aerosols and SO_2: An Interdisciplinary Approach; *Environ. Sci. Technol.* **1986**, *20(2)*, 138-145.
26. Amdur, M. Animal Toxicology. In *Particles In Our Air: Concentrations and Health Effects;* Wilson, R., Spengler, J., Eds.; Harvard University Press: Cambridge, MA, 1996; pp 85-122.
27. Kittelson, D.B. Engines and Nanoparticles: A Review; *J. Aerosol Sci.* **1998**, *29(5/6)*, 575-588.
28. Dobbins, R.A.; Subramaniasivam, H. Soot Precursor Particles in Flames. In *Soot Formation in Combustion;* Bockhorn, H., Ed.; Springer Series in Chemical Physics; Springer-Verlag: Berlin, 1994; pp 290-301.
29. Howard, J.B.; Wersborg, B.L.; Williams, G.C. Coagulation of Carbon Particles in Premixed Flames; *Faraday Symp. Chem. Soc.* **1973**, *7*, 109-119.
30. Bockhorn, H. *Soot Formation in Combustion, Mechanisms and Models*; Springer Series in Chemical Physics; Springer-Verlag: Berlin, 1994; Vol. 59.
31. Palmer, H.B.; Cullis, C.F. *Chem. Phys. Carbon* **1965**, *1*, 265-325.
32. Haynes, B.S.; Wagner, H.G. Sooting Structure in a Laminar Diffusion Flame; *Ber. Bunsen-Ges. Phys. Chem.* **1980**, *84(5)*, 499-506.
33. Haynes, B.S. Soot and Hydrocarbons in Combustion. In *Fossil Fuel Combustion;* Sarofim, A.F., Bartok, W., Eds.; Wiley Interscience: New York, 1991; pp 261-326.
34. Kennedy, I.M. Models of Soot Formation and Oxidation; *Prog. Energy Combust. Sci.* **1997**, *23*, 95-132.
35. Gulder, O.L. Soot Particulate Formation in Combustion; *Trans. Can. Soc. Mech. Eng.* **1999**, *23*, 225-240.
36. Olsen, D.B.; Pickens, J.C. *Combust. Flame* **1984**, *57*, 199-208.
37. Appel, J.; Bockhorn, H.; Frenklach, M. Kinetic Modeling of Soot Formation with Detailed Chemistry and Physics: Laminar Premixed Flames of C2 Hydrocarbons; *Combust. Flame* **2000**, *121*, 122-136.
38. Violi, A.; D'Anna, A. Modeling of Aromatics Formation in Rich Premixed Flames. In *21st Event of the Italian Section of the Combustion Institute;* The Combustion Institute: Naples, Italy, 1998; pp 249-260.
39. Howard, J.B. On the Mechanism of Carbon Formation in Flames. In *12th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1969; pp 877-887.
40. Friedlander, S.K. *Smoke, Dust, and Haze, Fundamentals of Aerosol Behavior*; John Wiley & Sons: New York, 1976.
41. *The Mechanics of Aerosols*; Fuchs, N.A., Ed.; Translated from the Russian by R. E. Daisley and M. Fuchs, Translation edited by C. N. Davies; Macmillian: New York, 1964.
42. Gelbard, F.; Steinfeld, J. Simulation of Multicomponent Aerosol Dynamics; *J. Colloid Interface Sci.* **1978**, *78(2)*, 485-501.
43. Wu, J.J.; Flagan, R.C. A Discrete-Sectional Solution to the Aerosol Dynamic Equation; *J. Colloid Interface Sci.* **1988**, *123(2)*, 339-352.
44. Wu, C.-Y.; Biswas, P. Study of Numerical Diffusion in a Discrete-Sectional Model and Its Application to Aerosol Dynamics Simulation; *Aerosol Sci. Technol.* **1998**, *29*, 359-378.
45. Park, S.H.; Lee, K.W.; Otto, E.; Fissan, H. The Log-Normal Size Distribution Theory of Brownian Aerosol Coagulation for the Entire Particle Size Range: Part I—Analytical Solution Using the Harmonic Mean Coagulation Kernel; *J. Aerosol Sci.* **1999**, *30(1)*, 3-16.
46. Otto, E.; Fissan, H.; Park, S.H.; Lee, K.W. The Log-Normal Size Distribution Theory of Brownian Aerosol Coagulation for the Entire Particle Size Range: Part II—Analytical Solution Using Dahneke's Coagulation Kernel; *J. Aerosol Sci.* **1999**, *30(1)*, 17-34.
47. Landgrebe, J.D.; Pratsinis, S.E. Discrete-Sectional Model for Particulate Production by Gas-Phase Chemical Reaction and Aerosol Coagulation in the Free-Molecular Regime; *J. Colloid Interface Sci.* **1990**, *139(1)*, 63-86.
48. Mick, H.J.; Hospital, A.; Roth, P. Computer Simulation of Soot Particle Coagulation in Low Pressure Flames; *J. Aerosol Sci.* **1991**, *22(7)*, 831-841.
49. Jokiniemi, J.K.; Lazaridis, M.; Lehtinen, K.E.J.; Kauppinen, E.I. Numerical Simulation of Vapour-Aerosol Dynamics in Combustion Processes; *J. Aerosol Sci.* **1994**, *25(3)*, 429-446.
50. Pilinis, C.; Capaldo, K.P.; Nenes, A.; Pandis, S.N. MADM–A New Multicomponent Aerosol Dynamics Model; *Aerosol Sci. Technol.* **2000**, *32(5)*, 482-502.
51. Hinds, W.C. *Aerosol Technology: Properties, Behavior, and Measurement of Airborne Particles*; John Wiley & Sons: New York, 1982.
52. Marlow, W.H. Derivation of Aerosol Collision Rates for Singular Attractive Contact Potentials; *J. Chem. Phys.* **1980**, *73*, 6284-6287.
53. Lai, F.S.; Friedlander, S.K.; Pich, J.; Hindy, G.M. *J. Colloid Interface Sci.* **1972**, *39*, 395-405.
54. Desrosiers, R.E.; Riehl, J.W.; Ulrich, G.D.; Chiu, A.S. Submicron Fly-Ash Formation in Coal-Fired Boilers. In *17th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1978; pp 1395-1403.
55. Taylor, D.D.; Flagan, R.C. The Influence of Combustor Operation on Fine Particles from Coal Combustion; *Aerosol Sci. Technol.* **1982**, *1*, 103-117.
56. *Soot in Combustion Systems and Its Toxic Properties*; Lahaye, J., Prado, G., Eds.; NATO Conference Series, VI Materials Science v. 7; Plenum Press: New York, 1983.
57. Harris, S.J.; Weiner, A.M. *Combust. Sci. Technol.* **1984**, *38*, 75-87.
58. Sethi, V.; Biswas, P. Modeling of Particle Formation and Dynamics in a Flame Incinerator; *J. Air & Waste Manage. Assoc.* **1990**, *40(1)*, 42-46.
59. Linak, W.P.; Wendt, J.O.L. Toxic Metal Emissions from Incineration: Mechanisms and Control; *Prog. Energy Combust. Sci.* **1993**, *19*, 145-185.
60. Flagan, R.C.; Taylor, D.D. Laboratory Studies of Submicron Particles from Coal Combustion. In *18th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1981; pp 1227-1237.
61. Quann, R.J.; Sarofim, A.F. Vaporization of Refractory Oxides during Pulverized Coal Combustion. In *19th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1982; pp 1429-1440.
62. Mims, C.A.; Neville, M.; Quann, R.J.; House, K.; Sarofim, A.F. Laboratory Studies of Mineral Matter Vaporization during Coal Combustion. In *Emission Control from Stationary Power Sources: Technical, Economic, and Environmental Assessments;* Engle, A.J., Slater, S.M., Gentry, J.W., Eds.; American Institute of Chemical Engineers: New York, 1980; pp 188-194.
63. McElroy, M.W.; Carr, R.C.; Ensor, D.S.; Markowski, G.R. Size Distribution of Fine Particles from Coal Combustion; *Science* **1982**, *215*, 13-19.
64. McElroy, M.W.; Carr, R.C. Relationship between NO_x and Fine Particle Emissions. In *Joint Symposium on Stationary Combustion NO_x Control;* Electric Power Research Institute: Palo Alto, CA, 1981; pp 311-329.
65. Lindner, E.R.; Wall, T.F. Sodium-Ash Reactions during the Combustion of Pulverized Coal. In *23rd Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1991; pp 1313-1321.
66. Damle, A.S.; Ensor, D.S.; Ranade, M.B. Coal Combustion Aerosol Formation Mechanisms: A Review; *Aerosol Sci. Technol.* **1982**, *1*, 119-133.
67. Neville, M.; Sarofim, A.F. The Fate of Sodium during Pulverized Coal Combustion; *Fuel* **1985**, *64*, 384-490.
68. Seames, W.S.; Wendt, J.O.L. Partitioning of Arsenic, Selenium, and Cadmium during the Combustion of Pittsburgh and Illinois #6 Coals in a Self-Sustained Combustor; *Fuel Process. Technol.* **2000**, *63*, 179-196.
69. Haynes, B.S.; Neville, M.; Quann, R.J.; Sarofim, A.F. Factors Governing the Surface Enrichment of Fly Ash in Volatile Trace Species; *J. Colloid Interface Sci.* **1982**, *87(1)*, 266-278.
70. Davison, R.L.; Natusch, D.F.S.; Wallace, J.R.; Evans, C.A.J. Trace Elements in Fly Ash Dependence of Concentration on Particle Size; *Environ. Sci. Technol.* **1974**, *8(13)*, 1107-1113.
71. Ondov, J.M.; Ragini, R.C.; Biermann, A.H. Elemental Particle-Size Emissions from Coal-Fired Power Plants: Use of an Inertial Cascade Impactor; *Atmos. Environ.* **1978**, *12*, 1175-1185.
72. Biermann, A.H.; Ondov, J.M. Application of Surface-Deposition Models to Size-Fractionated Coal Fly Ash; *Atmos. Environ.* **1980**, *14*, 289-295.
73. Linak, W.P.; Wendt, J.O.L. Trace Metal Transformation Mechanisms during Coal Combustion; *Fuel Process. Technol.* **1994**, *39(1)*, 173-198.
74. Ondov, J.M.; Ragaini, R.C.; Biermann, A.H. Elemental Emissions from a Coal-Fired Power Plant. Comparison of a Venturi Wet Scrubber System with a Cold-Side Electrostatic Precipitator; *Environ. Sci. Technol.* **1979**, *13(5)*, 598-607.
75. Coles, D.G.; Ragaini, R.C.; Ondov, J.M. Behaviour of Radionuclides in Western Coal-Fired Power Plants; *Environ. Sci. Technol.* **1978**, *12(4)*, 442-446.
76. Gladney, E.S.; Small, J.A.; Gordon, G.E.; Zoller, W.H. Composition and Size Distribution of In-Stack Particulate Material at a Coal-Fired Power Plant; *Atmos. Environ.* **1976**, *10*, 1071-1077.
77. Kaakinen, J.W.; Jorden, R.M.; Lawasani, M.H.; West, R.E. Trace Element Behavior in a Coal-Fired Power Plant; *Environ. Sci. Technol.* **1975**, *9(9)*, 862-869.

78. Shendrikar, A.D.; Ensor, D.S.; Cowen, S.J.; Woffinden, G.J.; McElroy, M.W. Size-Dependent Penetration of Trace Elements through a Utility Baghouse; *Atmos. Environ.* **1983**, *17(8)*, 1411-1421.
79. Klein, D.H.; Andren, A.W.; Carter, J.A.; Emery, J.F.; Feldman, C.; Fulkerson, W.; Lyon, W.S.; Ogle, J.C.; Talmi, Y.; van Hook, R.I.; Bolton, N. Pathways of Thirty-Seven Trace Elements through Coal-Fired Power Plant; *Environ. Sci. Technol.* **1975**, *9(10)*, 973-979.
80. Linak, W.P.; Peterson, T.W. Mechanisms Governing the Composition and Size Distribution of Ash Aerosol in a Laboratory Pulverized Coal Combustor. In *21st Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1986; pp 399-410.
81. Markowski, G.R.; Ensor, D.S.; Hooper, R.G.; Carr, R.C. A Submicron Aerosol Mode in Flue Gas from a Pulverized Coal Utility Boiler; *Environ. Sci. Technol.* **1980**, *14(11)*, 1400-1402.
82. Neville, M.; McCarthy, J.F.; Sarofim, A.F. Size Fractionation of Submicrometer Coal Combustion Aerosol for Chemical Analysis; *Atmos. Environ.* **1983**, *17(12)*, 2599-2604.
83. Smith, R.D.; Campbell, J.A.; Nielson, K.K. Characterization and Formation of Submicron Particles in a Coal-Fired Plant; *Atmos. Environ.* **1979**, *13*, 607.
84. Smith, R.D.; Campbell, J.A.; Nielson, K.K. Volatility of Fly Ash and Coal; *Fuel* **1980**, *59*, 661-665.
85. Senior, C.L.; Bool, L.E.I.; Morency, J.R. Laboratory Study of Trace Element Vaporization from Combustion of Pulverized Coal; *Fuel Process. Technol.* **2000**, *63*, 109-124.
86. Helble, J.J. Trace Element Behavior during Coal Combustion: Results of a Laboratory Study; *Fuel Process. Technol.* **1994**, *39(1)*, 159-172.
87. Senior, C.L.; Bool, L.E.I.; Srinivasachar, S.; Pease, B.R.; Porle, K. Pilot Scale Study of Trace Element Vaporization and Condensation during Combustion of a Pulverized Sub-Bituminous Coal; *Fuel Process. Technol.* **2000**, *63*, 149-165.
88. Linton, R.W.; Loh, A.; Natusch, D.F.S. Surface Predominance of Trace Elements in Airborne Particles; *Science* **1976**, *191*, 852-854.
89. Frandsen, F.; Dam-Johansen, K.; Rasmussen, P. Trace Elements from Combustion and Gasification of Coal—An Equilibrium Approach; *Prog. Energy Combust. Sci.* **1994**, *20(2)*, 115-138.
90. Sandelin, K.; Backman, R. A Simple Two-Reactor Method for Predicting Distribution of Trace Elements in Combustion Systems; *Environ. Sci. Technol.* **2000**, *33(24)*, 4508-4513.
91. Yousif, S.; Lockwood, F.C.; Abbas, T. Modeling of Toxic Metal Emissions from Solid Fuel Combustors. In *27th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1998; pp 1647-1654.
92. Mocellin, A.; Kingery, W.D. Microstructural Changes during Heat Treatment of Sintered Al_2O_3; *J. Amer. Ceram. Soc.* **1973**, *56(6)*, 309-314.
93. Kingery, W.D.; Bowen, H.K.; Uhlmann, D.R. *Introduction to Ceramics*; Wiley: New York, 1976.
94. Ulrich, G.D.; Subramanian, N.S. Particle Growth in Flames-3. Coalescence as a Rate-Controlling Process; *Combust. Sci. Technol.* **1984**, *17* (3-4), 119-126.
95. Pratsinis, S.E. Flame Aerosol Synthesis of Ceramic Powders; *Prog. Energy Combust. Sci.* **1998**, *24*, 197-219.
96. Woolridge, M.S. Gas-Phase Combustion Synthesis of Particles; *Prog. Energy Combust. Sci.* **1998**, *24(1)*, 63-87.
97. Muñoz, R.H.; Charalampopoulos, T.T. Evolution of Compositional and Structural Properties of Soot in Premixed Flames. In *27th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1998; pp 1471-1479.
98. Mulholland, G.W.; Liggett, W.; Koseki, H. Effect of Pool Diameter on the Properties of Smoke Produced by Crude Oil Fires. In *26th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1996; pp 1445-1452.
99. Koch, W.; Friedlander, S.K. Effect of Particle Coalescence on the Surface Area of a Coagulating Aerosol; *J. Colloid Interface Sci.* **1990**, *140*, 419-427.
100. Xiong, Y.; Pratsinis, S.E. Gas Phase Production of Particles in Reactive Turbulent Flows; *J. Aerosol Sci.* **1991**, *22(5)*, 637-655.
101. Reilly, P.T.A.; Whitten, W.B.; Ramsey, J.M. Evidence for the Emergence of Whole Mature Soot Aggregates from Single PAH-Containing Droplets. In *2000 Technical Meeting of the Central State Section of the Combustion Institute;* The Combustion Institute: Pittsburgh, PA, 2000.
102. Biswas, P.; Wu, C.Y. Control of Toxic Metal Emissions from Combustors Using Sorbents: A Review; *J. Air & Waste Manage. Assoc.* **1998**, *48(2)*, 113-127.
103. Goldstein, H.L.; Siegmund, C.W. Influence of Heavy Oil Composition and Boiler Combustion Conditions on Particulate Emission; *Environ. Sci. Technol.* **1976**, *10(12)*, 1109-1114.
104. Senior, C.L.; Zeng, T.; Che, J.; Ames, M.R.; Sarofim, A.F.; Olmez, I.; Huggins, F.E.; Shah, N.; Huffman, G.P.; Kolker, A.; Mroczkowski, S.; Palmer, C.; Finkelman, R. Distribution of Trace Elements in Selected Pulverized Coals as a Function of Particle Size and Density; *Fuel Process. Technol.* **2000**, *63(2-3)*, 215-241.
105. Huggins, F.E.; Huffman, G.P.; Lee, R.J. Scanning Electron Microscope-Based Automated Image Analysis (SEM-AIA) and Mossbauer Spectroscopy: Quantitative Characterization of Coal Minerals. In *Coal and Coal Products: Analytical Characterization Techniques;* Fuller, E.L., Ed.; American Chemical Society: 1982; pp 239-258.
106. Straszheim, W.E.; Markuzewshi, R. Characterization of Mineral Matter in Coal for Prediction of Ash Composition and Particle Size. In *Engineering Foundation Conference on Inorganic Transformations and Ash Deposition During Combustion;* ASME: 1992; pp 165-177.
107. Steadman, E.N.; Erikson, T.A.; Folkedahl, B.C.; Brekke, D.W. Coal and Ash Characterization: Digital Image Analysis Application. In *Engineering Foundation Conference on Inorganic Transformations and Ash Deposition during Combustions;* ASME: 1991; pp 147-164.
108. Yang, N.Y.C.; Baxter, L.L. Instrument and Sample Preparation Considerations for CCSEM Analysis. In *Engineering Foundation Conference on Inorganic Ash Transformations and Ash Deposition during Combustion;* ASME: 1991; pp 191-201.
109. Yu, H.; Marchek, J.E.; Adair, N.L.; Harb, J.N. Characterization of Minerals and Coal/Mineral Associations in Pulverized Coal. In *Engineering Foundation Conference on the Impact of Ash Deposition on Coal Fired Plants;* Taylor and Francis: 1993; pp 361-372.
110. Wigley, F.; Williamson, J.; Gibb, W.H. The Distribution of Mineral Matter in Pulverized Coal Particles in Relation to Burnout Behaviour; *Fuel* **1997**, *76*, 1283-1288.
111. Wilemski, G.; Srinivasachar, S.; Sarofim, A.F. Modeling of Mineral Matter Redistribution and Ash Formation in Pulverized Coal Combustion. In *Engineering Foundation Conference on Inorganic Ash Transformations and Ash Deposition during Combustion;* ASME: 1991; pp 545-564.
112. Sarofim, A.F.; Howard, J.B.; Padia, A.S. The Physical Transformation of Mineral Matter in Pulverized Coal under Simulated Combustion Conditions; *Combust. Sci. Technol.* **1977**, *16*, 187-204.
113. Kang, S.-G.; Helble, J.J.; Sarofim, A.F.; Béer, J.M. Time-Resolved Evolution of Fly Ash during Pulverized Coal Combustion. In *22nd Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1988; pp 231-238.
114. Baxter, L.L. *Coal Char Fragmentation during Pulverized Coal Combustion*; SAND95-8250 UC-1409; Sandia National Laboratories: 1995.
115. Benson, S.A.; Jones, M.L.; Harb, J.N. Ash Formation and Deposition. In *Fundamentals of Coal Combustion for Clean and Efficient Use*; Smoot, L.D., Ed.; Elsevier: New York, 1993; pp 299-373.
116. Barta, L.E.; Toqan, M.A.; Béer, J.M.; Sarofim, A.F. Prediction of Fly Ash Size and Chemical Composition Distributions: The Random Coalescence Model. In *24th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1992; pp 1135-1144.
117. Barta, L.E.; Vámos, G.; Toqan, M.A.; Béer, J.M.; Sarofim, A.F. A Statistical Investigation on Particle-to-Particle Variation of Flyash Using SEM-AIA-EDAX Technique; *Mater. Res. Soc. Symp. Proc.* **1990**, *178*, 67-81.
118. *A Study of Toxic Emissions from a Coal-Fired Power Plant Utilizing an ESP/Wet FGD System*; Batelle Columbus; DOE/PC/93251-T2; DE94017941; U.S. Department of Energy; Pittsburgh Energy Technology Center: 1994; Vol. 1.
119. Charon, O.; Sarofim, A.F.; Béer, J.M. Distribution of Mineral Matter in Pulverized Coal; *Prog. Energy Combust. Sci.* **1990**, *16*, 319-326.
120. Raask, E.; Wilkins, D.M. Volatilization of Silica in Gasification and Combustion Processes; *J. Inst. Fuel* **1965**, *38*, 255-262.
121. Kerstein, A.R.; Edwards, B.F. Percolation Model for Simulation of Char Oxidation and Fragmentation Time-Histories; *Chem. Eng. Sci.* **1987**, *42(7)*, 1629-1634.
122. Kang, S.-G. Fundamental Studies of Mineral Matter Transformation during Pulverized Coal Combustion: Residual Ash Formation. Ph.D. Thesis, Massachusetts Institute of Technology, Cambridge, MA, 1991.
123. Kerstein, A.R.; Niksa, S. Fragmentation during Carbon Conversion: Predictions and Measurements. In *20th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1984; pp 941-949.
124. Seggiani, M.; Bardi, A.; Vitolo, S. Prediction of Fly-Ash Size Distribution: A Correlation between Char Transition Radius and Coal Properties; *Fuel* **2000**, *79*, 999-1002.
125. Hurt, R.H.; Davis, K.A. Near-Extinction and Final Burnout in Coal Combustion. In *25th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1994; pp 561-568.
126. Wu, H.; Bryant, G.; Benfell, K.; Wall, T. Experimental Study on the Effect of System Pressure on Char Structure of an Austrialian Bituminous Coal; *Energy Fuels* **2000**, *14(2)*, 282-290.
127. Fischer, G.L.; Chang, D.P.Y.; Brummer, M. Fly Ash Collected from Electrostatic Precipitators: Micro-Crystalline Structures and the Mystery of Spheres; *Science* **1976**, *192*, 553.
128. Raask, E. *Mineral Impurities in Coal Combustion: Behavior, Problems, and Remedial Measures*; Hemisphere Publishing: New York, 1985.
129. Sloss, L.L.; Smith, I.M.; Adams, D.M.B. Pulverized Coal Ash—Requirements for Utilization; *IEA Coal Research* **1996**, *IEACR/88*.

130. McCarthy, G.J.; Solem, J.K.; Manz, O.; Hassett, D.J. Use of a Database of Chemical, Mineralogical, and Physical Properties of North American Fly Ash to Study the Nature of Fly Ash and Its Use as a Mineral Admixture in Concrete; *Miner. Res. Soc. Symp. Proc.* **1990**, *178*, 2-31.
131. Hering, S.V. *Air Sampling Instruments*; American Conference of Governmental Industrial Hygienists: Cincinnati, OH, 1995.
132. D'Alessio, A.; D'Anna, A.; Gambi, G.; Minutolo, P.; Sgro, L.A.; Violi, A. Combustion-Generated Nanoparticles; *Chim. Ind.* **1999**, *81*, 1001-1006.
133. D'Alessio, A.; D'Anna, A.; Minutolo, P.; Sgro, L.A. Nanoparticles in Combustion Systems: Their Formation and Impact on Climate Change and Health Effects. In *Chemical Engineering, Greetings to Prof. Mario Dente on the Occasion of his 65th Birthday*; AIDIC, Eds.; Milano, Italy, 1999; pp 99-110.
134. Narsimhan, G.; Ruckenstein, E. The Brownian Coagulation of Aerosols over the Entire Range of Knudsen Numbers: Connection between the Sticking Probability and the Interaction Forces; *J. Colloid Interface Sci.* **1985**, *104(2)*, 344-369.
135. Graham, K.A. Submicron Ash Formation and Interaction with Sulfur Oxides During Pulverized Coal Combustion. Ph.D. Thesis, Chemical Engineering, Massachusetts Institute of Technology, Cambridge, MA, 1991.
136. Linak, W.P. The Effect of Coal Type, Residence Time, and Combustion Configuration on the Submicron Aerosol Composition and Size Distribution from Pulverized Coal Combustion. Ph.D. Thesis, University of Arizona, Tucson, AZ, 1985.
137. Miake-Lye, R.C.; Anderson, B.E.; Cofer, W.R.; Wallio, H.A.; Nowicki, G.D.; Ballenthin, J.O.; Hunton, D.E.; Knighton, W.B.; Miller, T.M.; Seeley, J.V.; Viggiano, A.A. SO_x Oxidation and Volatile Aerosol in Aircraft Exhaust Plumes Depend on Fuel Sulfur Content; *Geophys. Res. Lett.* **1998**, *25(10)*, 1677-1680.
138. Park, C.; Appleton, J.P. Shock-Tube Measurements of Soot Oxidation Rates; *Combust. Flame* **1973**, *20*, 369-379.
139. Itkonen, A.O.; Jantunen, M.J. Emissions and Particle-Size Distribution of Some Metallic Elements of Two Peat/Oil-Fired Boilers; *Environ. Sci. Technol.* **1986**, *20(4)*, 335.
140. *Industrial Air Pollution Control Systems*; Heumann, W.L., Ed.; McGraw Hill: New York, 1997.
141. *Handbook of Air Pollution Technology*; Calvert, S., Englund, H.M., Eds.; Wiley: New York, 1986.
142. *Air Pollution,* 3rd Ed.; Stern, A.C., Ed.; Academic Press: New York, 1976.
143. Helble, J.J. A Model for the Air Emissions of Trace Metallic Elements from Coal Combustors Equipped with Electrostatic Precipitators; *Fuel Process. Technol.* **2000**, *63*, 125-147.
144. Soud, H.N. Developments in Particulate Control for Coal Combustion; *IEA Coal Research* **1995**, *IEACR/78*.
145. Zhuang, Y.; Kim, Y.J.; Lee, T.G.; Biswas, P. Experimental and Theoretical Studies of Ultra-Fine Behavior in Electrostatic Precipitators; *J. Electrost.* **2000**, *48(3)*, 245-260.
146. Yoo, K.H.; Lee, J.S.; Oh, M.D. Charging and Collection of Submicron Particles in Two-Stage Parallel-Plate Electrostatic Precipitators; *Aerosol Sci. Technol.* **1997**, *27*, 308-323.
147. Watanabe, T.; Tochikubo, F.; Koizumi, Y.; Tsuchida, T.; Hautanen, J.; Kauppinen, E.I. Submicron Particle Agglomeration by an Electrostatic Agglomerator; *J. Electrost.* **1995**, *34*, 367-383.
148. Kauppinen, E.I.; Pakkanen, T.A. Coal Combustion Aerosols: A Field Study; *Environ. Sci. Technol.* **1990**, *24*, 1811-1818.
149. Miller, S.J.; Ness, S.R.; Weber, G.F.; Erickson, T.A.; Hassett, D.J.; Hawthorne, S.B.; Katrinak, K.A.; Louie, P.K.K. *A Comprehensive Assessment of Toxic Emissions from Coal-Fired Power Plants: Phase I Results from the U.S. Department of Energy Study*; U.S. DOE Pittsburgh Energy Technology Center Contract DE-FC21-93MC30097; Energy & Environmental Research Center; University of North Dakota: 1996.
150. Chow, W.; Miller, M.J.; Torrens, I.M. Pathways of Trace Elements in Power Plants: Interim Research Results and Implications; *Fuel Process. Technol.* **1994**, *39(1)*, 5-20.
151. Moore, T. Hazardous Air Pollutants: Measuring in Micrograms; *EPRI J.* **1994**, *19(1)*, 7-15.
152. Meij, R. Trace Element Behaviour in Coal-Fired Power Plants; *Fuel Process. Technol.* **1994**, *39(1)*, 199-217.
153. *Compilation of Air Emission Factors*; AP-42; EP 4.9:42/985; U.S. Environmental Protection Agency: 1982.
154. Leaderer, B.P.; Naeher, L.; Jankun, T.; Balenger, K.; Holford, T.R.; Toth, C.; Sullivan, J.; Wolfson, J.M.; Koutrakis, P. Indoor, Outdoor and Regional Summer and Winter Concentrations of PM_{10}, $PM_{2.5}$, SO_4^{2-}, H^+, NO_3^- and NH_3 and Nitrous Acid in Homes with and without Kerosene Space Heaters; *Environ. Health Perspect.* **1999**, *107(3)*, 223-231.
155. Hildemann, L.M.; Markowski, G.R.; Jones, M.C.; Cass, G.R. Submicron Aerosol Mass Distributions of Emissions from Boilers, Fireplaces, Automobiles, Diesel Trucks, and Meat-Cooking Operations; *Aerosol Sci. Technol.* **1991**, *14*, 138-152.
156. Hildemann, L.M.; Markowski, G.R.; Cass, G.R. Chemical Composition of Emissions from Urban Sources of Fine Organic Aerosol; *Environ. Sci. Technol.* **1991**, *25(4)*, 744-759.
157. Rogge, W.F.; Hildemann, L.M.; Mazurek, M.A.; Cass, G.R.; Simoneit, B.R.T. Sources of Fine Organic Aerosol. 8. Boilers Burning No. 2 Distillate Fuel Oil; *Environ. Sci. Technol.* **1997**, *31(10)*, 2731-2737.
158. Watkinson, W.P.; Campen, M.J.; Costa, D.L. Cardiac Arrhythmia Induction after Exposure to Residual Oil Fly Ash Particles in a Rodent Model of Pulmonary Hypertension; *Toxicol. Sci.* **1998**, *41*, 209-216.
159. Dreher, K.L.; Jaskot, R.H.; Lehmann, J.R.; Richards, J.H.; McGee, J.K. Soluble Transition Metals Mediate Residual Oil Fly Ash-Induced Acute Lung Injury; *J. Toxicol. Environ. Health* **1997**, *50*, 285-305.
160. Samet, J.M.; Reed, W.; Ghio, A.J.; Devlin, R.B.; Carter, J.D.; Dailey, L.A.; Bromberg, P.A.; Madden, M.C. Induction of Prostaglandin H Synthase 2 in Human Airway Epithelial Cells Exposed to Residual Oil Fly Ash; *Toxicol. Appl. Pharmacol.* **1996**, *141*, 159-168.
161. Miller, C.A.; Linak, W.P.; King, C.; Wendt, J.O.L. Fine Particle Emissions from Heavy Fuel Oil Combustion in a Firetube Package Boiler; *Combust. Sci. Technol.* **1998**, *134*, 477-502.
162. Villasenor, R.; Garcia, F. Experimental Study of the Effects of Asphaltenes on Heavy Fuel Oil Droplet Combustion; *Fuel* **1999**, *78*, 933-944.
163. Urban, D.L.; Huey, S.P.; Dryer, F.L. Evaluation of the Coke Formation Potential of Residual Fuel Oils. In *24th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1992; pp 1357-1364.
164. Linak, W.P.; Miller, C.A.; Wendt, J.O.L. Comparison of the Particle Size Distributions and Elemental Partitioning from the Combustion of Pulverized Coal and Residual Fuel Oil; *J. Air & Waste Manage. Assoc.* **2000**, *50*, 1532-1543.
165. Galbreath, K.C.; Zygarlicke, C.J.; Huggins, F.E.; Huffman, G.P.; Wong, J.L. Chemical Speciation of Nickel in Residual Oil Fly Ash; *Energy Fuels* **1998**, *12*, 818-822.
166. Galbreath, K.C.; Zygarlicke, C.J.; D, L.T.; Huggins, F.E.; Huffman, G.P. Nickel and Chromium Speciation of Residual Oil Combustion Ash; *Combust. Sci. Technol.* **1998**, *134*, 243-262.
167. Huffman, G.P.; Huggins, F.E.; Shah, N.; Huggins, R.; Linak, W.P.; Miller, C.A.; Pumire, R.J.; Meuzelaar, H.L.C.; Seehra, M.S.; Manivannan, A. Characterization of Fine Particulate Matter Produced by Combustion of Residual Fuel Oil; *J. Air & Waste Manage. Assoc.* **2000**, *50*, 1106-1114.
168. Smoot, L.D.; Smith, P.J. *Coal Combustion and Gasification*; Plenum Press: New York, 1985.
169. Smoot, L.D. *Fundamentals of Coal Combustion for Clean and Efficient Use*; Elsevier: New York, 1993.
170. Flagan, R.C. Submicron Particles From Coal Combustion. In *17th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1978; pp 97-104.
171. Fletcher, T.H.; Ma, J.; Rigby, J.R.; Brown, A.L.; Webb, B.W. Soot in Coal Combustion Systems; *Prog. Energy Combust. Sci.* **1997**, *23*, 283-301.
172. Sadakata, M.; Yoshino, A.; Sakai, T.; Matsuoka, H. Formation of Submicron Unburnt Carbon and NO_x from Pulverized Coal Combustion System. In *20th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1984; pp 913-920.
173. Veranth, J.M.; Pershing, D.W.; Sarofim, A.F.; Shield, J.E. Sources of Unburned Carbon in the Fly Ash Produced from Low-NO_x Pulverized Coal Combustion. In *27th Symposium (International) on Combustion, Boulder, CO*; The Combustion Institute: Pittsburgh, PA, 1998; pp 1737-1744.
174. Veranth, J.M.; Fletcher, T.H.; Pershing, D.W.; Sarofim, A.F. Measurement of Soot and Char in Pulverized Coal Fly Ash; *Fuel* **2000**, *79(9)*, 1067-1075.
175. *Characterizing Toxic Emissions from a Coal-Fired Power Plant Demonstrating the AFGD ICCT Project and a Plant Utilizing a Dry Scrubber/Baghouse System*; Final Report Bailly Station Units 7 and 8; SRI Report SRI-ENV-94-827-7960; DOE Contract DE-AC22-93PC93254; U.S. Department of Energy, Pittsburgh Energy Technology Center; Southern Research Institute: 1994.
176. *Assessment of Toxic Emissions from a Coal-Fired Power Plant Utilizing an ESP*; DOE Contract DE-AC22-93PC93252; Energy and Environmental Research Corporation; U.S. Department of Energy; Pittsburgh Energy Technology Center: 1994.
177. Lind, T.; Kauppinen, E.I.; Jokiniemi, J.K.; Maenhaut, W. A Field Study on the Trace Metal Behaviour in Atmospheric Fluidized Bed Combustion. In *25th International Symposium on Combustion;* The Combustion Institute: Pittsburgh, PA, 1994; p 201.
178. Lind, T.; Kauppinen, E.I.; Maenhaut, W.; Shah, A.; Huggins, F. Ash Vaporization in Circulating Fluidized Bed Coal Combustion; *Aerosol Sci. Technol.* **1996**, *24(3)*, 135-150.
179. Mohr, M.; Ylätalo, S.; Klippel, N.; Kauppinen, E.I.; Riccius, O.; Burtscher, H. Submicron Fly Ash Penetration through Electrostatic Precipitators at Two Coal Power Plants; *Aerosol Sci. Technol.* **1996**, *24*, 191-204.
180. Ylatalo, S.I.; Hautanen, J. Electrostatic Precipitator Penetration for Pulverized Coal Combustion; *Aerosol Sci. Technol.* **1998**, *29*, 17-30.
181. Littlejohn, R.F. Mineral Matter and Ash Distribution in "As-Fired" Samples of Pulverized Fuels; *J. Inst. Fuel* **1966**, *39*, 59-67.

182. Ulrich, G.D.; Subramanian, N.S. Particle Growth in Flames III. Coalescence as a Rate-Controlling Process; *Combust. Sci. Technol.* **1977**, *17*, 119-126.
183. Lee, C.M.; Davis, K.A.; Heap, M.P.; Eddings, E.; Sarofim, A. Modeling the Vaporization of Ash Constituents in a Coal-Fired Boiler; *Combust. Inst.*, in press.
184. Linak, W.P.; Peterson, T.W. Effect of Coal Type and Residence Time on the Submicron Aerosol Distribution from Pulverized Coal Combustion; *Aerosol Sci. Technol.* **1984**, *3*, 77-96.
185. Schmidt, E.W.; Gieseke, J.A.; Allen, J.M. Size Distribution of Fine Particulate Emissions from a Coal-Fired Power Plant; *Atmos. Environ.* **1976**, *10*, 1065-1069.
186. Couch, G.R. Power from Coal—Where to Remove Impurities? *IEA Coal Research* **1995**, *IEACR/82*.
187. Smith, K.L.; Smoot, L.D.; Fletcher, T.H.; Pugmire, R.J. *Structure and Reaction Processes of Coal;* Plenum Press: New York, 1994.
188. Zygarlicke, C.J.; Jones, M.L.; Steadman, E.N.; Benson, S.A. *Characterization of Mineral Matter in ACERC Coals*; Advanced Combustion Engineering Research Center and Environmental Systems Research Institute; University of North Dakota: 1990.
189. Itkonen, A.O.; Jantunen, M.J. The Properties of Fly Ash and Fly Ash Mutagenicity. In *Encyclopedia of Environmental Control Technology, Volume 1: Thermal Treatment of Hazardous Wastes;* Cheremisinoff, P.N., Ed.; Gulf Publishing: Houston, TX, 1989; pp 755-789.
190. Hurt, R.H.; Mitchell, R.E. Unified High-Temperature Char Combustion Kinetics for a Suite of Coals of Various Rank. In *24th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1992; pp 1243-1250.
191. Hurt, R.H.; Gibbins, J.R. Residual Carbon from Pulverized Coal-Fired Boilers: 1. Size Distribution and Combustion Reactivity; *Fuel* **1995**, *74(4)*, 471-479.
192. Freeman, E.; Gao, Y.-M.; Hurt, R.; Suuberg, E. Interactions of Carbon-Containing Fly Ash with Commercial Air-Entraining Admixtures for Concrete; *Fuel* **1997**, *76(8)*, 761-765.
193. Ratafia-Brown, J.A. Overview of Trace Element Partitioning in Flames and Furnaces of Utility Coal-Fired Boilers; *Fuel Process. Technol.* **1994**, *39(1)*, 137-154.
194. McLennan, A.R.; Bryant, G.W.; Stanmore, B.R.; Wall, T.F. Ash Formation Mechanisms during pf Combustion in Reducing Conditions; *Energy & Fuels* **2000**, *14*, 150-159.
195. Nathan, Y.; Dvorachek, M.; Pelly, I.; Mimram, U. Characterization of Coal Fly Ash from Israel; *Fuel* **1999**, *78*, 205-213.
196. Huffman, G.P.; Huggins, F.E.; Shah, N.; Shah, A. Behavior of Basic Elements during Coal Combustion; *Prog. Energy Combust. Sci.* **1990**, *16*, 243-251.
197. Nielsen, H.P.; Baxter, L.L.; Sclippab, G.; Morey, C.; Frandsen, F.J.; Dam-Johansen, K. Deposition of Potassium Salts on Heat Transfer Surfaces in Straw-Fired Boilers: A Pilot-Scale Study; *Fuel* **2000**, *79(2)*, 131-139.
198. Jenkins, B.M.; Baxter, L.L.; Miles, T.R.J.; Miles, T.R. Combustion Properties of Biomass; *Fuel Process. Technol.* **1998**, *54(1-3)*, 17-46.
199. Valmari, T.; Lind, T.; Kauppinen, E.I.; Sfiris, G.; Nilsson, K.; Maenhaut, W. Field Study on Ash Behaviour during Circulating Fluidized-Bed Combustion of Biomass. 1. Ash Formation; *Energy Fuels* **1999**, *13*, 379-389.
200. Lind, T.; Valmari, T.; Kauppinen, E.I.; Sfiris, G.; Nilsson, K.; Maenhaut, W. Volatilization of the Heavy Metals during Circulating Fluidized Bed Combustion of Forest Residue; *Environ. Sci. Technol.* **1999**, *33*, 496-502.
201. Chenevert, B.C.; Kramlich, J.C.; Nichols, K.M. Ash Characteristics of High Alkali Sawdust and Sanderdust Biomass Fuels. In *27th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1998; pp 1719-1725.
202. Robinson, A.L.; Junker, H.; Buckley, S.G.; Sclippa, G.; Baxter, L.L. Interactions between Coal and Biomass when Cofiring. In *27th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1998; pp 1351-1359.
203. Dayton, D.C.; Belle-Oudry, D.; Nordin, A. Effect of Coal Minerals on Chlorine and Alkali Metals during Biomass/Coal Cofiring; *Energy Fuels* **1999**, *13(6)*, 1203-1211.
204. Nielsen, L.B.; Jensen, L.S.; Pedersen, C.; Rokke, M.; Livbjerg, H. Field Measurements of Combustion Aerosols from Co-Firing of Coal and Straw; *J. Aerosol Sci.* **1996**, *27(Suppl 1)*, S365-S366.
205. Raunemaa, T.; Yli-Tuomi, T.; Leskinen, A.; Tissari, J.; Alander, T. Wood Combustion Aerosol and Lung Exposure Estimates; *J. Aerosol Sci.* **1999**, *30(Suppl 1*), S735-S736.
206. Amur, G.O.; Bhattacharya, S.C. A Study of Biomass as an Energy Source in Pakistan; *RERIC International Energy J.* **1999**, *21(1)*, 25-36.
207. Albalak, R.; Keeler, G.J.; Frisancho, A.R.; Haber, M. Assesment of PM_{10} Concentrations from Domestic Biomass Fuel Combustion in Two Rural Bolivian Highland Villages; *Environ. Sci. Technol.* **1999**, *33(15)*, 2505-2509.
208. Brauer, M.; Bartlett, K.; Regaldo-Pineda, J.; Perez-Padilla, R. Assessment of Particulate Concentrations from Domestic Biomass Combustion in Rural Mexico; *Environ. Sci. Technol.* **1996**, *30(1)*, 104-109.
209. Rogge, W.F.; Hildemann, L.M.; Cass, G.R.; Simoneit, B.R.T. Sources of Fine Organic Aerosol. 9. Pine, Oak, and Synthetic Log Combustion in Residential Fireplaces; *Environ. Sci. Technol.* **1998**, *32(1)*, 13-22.
210. Rau, J.A. Composition and Size Distribution of Residential Wood Smoke Particles; *Aerosol Sci. Technol.* **1989**, *10*, 181-192.
211. Purvis, C.R.; McCrillis, R.C.; Kariher, P.H. Fine Particulate Matter (PM) and Organic Speciation of Fireplace Emissions; *Environ. Sci. Technol.* **2000**, *34(9)*, 1653-1658.
212. Kozinski, J.A.; Saade, R. Effect of Biomass Burning on the Formation of Soot Particles and Heavy Hydrocarbons. An Experimental Study; *Fuel* **1998**, *77(4)*, 225-237.
213. Oanh, N.T.K.; Reutehgardh, L.B.; Dung, N.T. Emission of Polycyclic Aromatic Hydrocarbons and Particulate Matter from Domestic Combustion of Selected Fuels; *Environ. Sci. Technol.* **1999**, *33(16)*, 2703-2709.
214. Mumford, J.L.; Harris, D.B.; Wilson, W.E.; Chapman, R.S.; Cao, S.; Xian, Y.; Li, X.; Chuang, J.C.; Cooke, W.M. Lung Cancer and Indoor Air Pollution in Xuan Wei, China; *Science* **1987**, *235*, 217-220.
215. Chuang, J.C.; Cao, S.R.; Xian, Y.L.; Harris, D.B.; Mumford, J.L. Chemical Characterization of Indoor Air in Homes from Communes in Xuan Wei, China, with High Lung Cancer Mortality Rate; *Atmos. Environ.* **1992**, *26A(12)*, 2193-2201.
216. Chuang, J.C.; Wise, S.A.; Cao, S.; Mumford, J.L. Chemical Characterization of Mutagenic Fractions of Particles from Indoor Coal Combustion: A Study of Lung Cancer in Xuan Wei, China; *Environ. Sci. Technol.* **1992**, *26*, 999-1004.
217. Mumford, J.L.; Helmes, C.T.; Lee, X.; Seidenberg, J.; Nesnow, S. Mouse Skin Tumorigenicity Studies of Indoor Coal and Wood Combustion Emissions from Homes for Residents in Xuan Wei, China with High Lung Cancer Mortality; *Carcinogenesis* **1990**, *11(3)*, 397-404.
218. Christopher, S.A.; Wang, M.; Berendes, T.A.; Welch, R.M.; Yang, S.-K. 1985 Biomass Burning Season in South America: Satellite Remote Sensing of Fires, Smoke, and Regional Radiative Energy Budgets; *J. Appl. Meteorology* **1998**, *37(7)*, 661-678.
219. *Recommendations for Improving Western Vistas*; Grand Canyon Visibility Transport Commission: 1996.
220. Husar, R.B.; Schichtel, B.A.; Falke, C.R.; Wilson, W.E. Dust and Smoke Events over the USA in 1998. In *Proceedings of PM2000–Particulate Matter and Health,* Charleston, SC, 2000; Air and Waste Management Association: Pittsburgh, PA, 2000; Session 10AS, p 22-23.
221. *Areas Affected by PM10 Natural Events*. Memorandum issued by M.D. Nichols, Assistant Administrator for Air and Radiation to Regional Directors; U.S. Environmental Protection Agency, 1996.
222. Ward, D.E. Factors Influencing the Emissions of Gases and Particulate Matter from Biomass Burning. In *Fire in the Tropical Biota: Ecosystem Processes and Global Challenges;* Goldammer, J.G., Ed.; Ecological Studies; Springer Verlag: Berlin, 1990; pp 418-436.
223. Jenkins, B.M.; Jones, A.D.; Turn, S.Q.; Williams, R.B. Emission Factors for Polycyclic Aromatic Hydrocarbons from Biomass Burning; *Environ. Sci. Technol.* **1996**, *30*, 2462-2469.
224. Jenkins, B.M.; Jones, A.D.; Turn, S.Q.; Williams, R.B. Particle Concentrations, Gas-Particle Partitioning, and Species Correlations for Polycyclic Aromatic Hydrocarbons (PAH) Emitted during Biomass Burning; *Atmos. Environ.* **1996**, *30(22)*, 3825-3835.
225. Walton, W.D.; Evans, D.D.; McGrattan, K.B.; Baum, H.R.; Twilley, W.H.; Madrzykowski, D.; Putorti, A.D.; Rehm, R.G.; Koseki, H.; Tennyson, E.J. In Situ Burning of Oil Spills: Mesoscale Experiments and Analysis. In *16th Arctic and Marine Oil Spill Program Technical Seminar;* Ministry of Supply and Services: Calgary, Alberta, Canada, 1993; pp 679-734.
226. Evans, D.; Walton, W.; Baum, H.; Mulholland, G.; Lawson, J.; Koseki, H. Smoke Emission from Burning Crude Oil. In *14th Arctic and Marine Oil Spill Technical Seminar;* Ministry of Supply and Services: Vancouver, British Columbia, Canada, 1991; pp 421-449.
227. Williams, J.M.; Gritzo, L.A. In Situ Sampling and Transmission Electron Microscope Analysis of Soot in the Flame Zone of Large Pool Fires. In *27th Symposium (International) on Combustion;* The Combustion Institute: Pittsburgh, PA, 1998; pp 2707-2714.
228. Dobbins, R.A.; Megaridis, C.M. Morphology of Flame-Generated Soot as Determined by Thermophoretic Sampling; *Langmuir* **1987**, *3*, 254-259.
229. Benner, B.A.J.; Bryner, N.P.; Wise, S.A.; Mulholland, G.W.; Lao, R.C.; Fingas, M.F. Polycyclic Aromatic Hydrocarbon Emissions from the Combustion of Crude Oil on Water; *Environ. Sci. Technol.* **1990**, *24*, 1418-1427.
230. Barton, R.G.; Clark, W.D.; Seeker, W.R. Fate of Metals in Waste Combustion Systems; *Combust. Sci. Technol.* **1990**, *74*, 327-342.
231. Lighty, J.S.; Veranth, J.M. The Role of Research in Practical Incineration Systems—A Look at the Past and the Future. In *27th Symposium (International) on Combustion, Boulder, CO*; The Combustion Institute: Pittsburgh, PA, 1998; pp 1255-1273.
232. Durlak, S.K.; Biswas, P.; Shi, J. Equilibrium Analysis of the Effect of Temperature, Moisture and Sodium Content on Heavy Metal Emissions from Municipal Solid Waste Incinerators; *J. Hazard. Mater.* **1997**, *56*, 1-20.

233. Holbert, C.; Lighty, J.S. Trace Metals Behavior during Thermal Treatment of Sludge Wastes; *J. Waste Manage.* **1999**, *18*, 423-431.
234. Smith, J.D.; Vandell, R.; Hixon, E.M. Application of Computational Fluid Mechanics to Modeling the Incineration of Chlorinated Hydrocarbon Wastes in Thermal Oxidizers; *Combust. Sci. Technol.* **1994**, *101*, 397-423.
235. Lee, C.C. A Model Analysis of Metal Partitioning in a Hazardous Waste Incineration System; *J. Air Pollut. Control Assoc.* **1988**, *38(7)*, 941-945.
236. Wey, M.-Y.; Hwang, J.-H.; Chen, J.-C. Mass and Elemental Size Distribution of Chromium, Lead, and Cadmium under Various Incineration Conditions; *J. Chem. Eng. Jpn.* **1998**, *31(4)*, 506-517.
237. Eddings, E.G.; Lighty, J.S.; Kozinski, J.A. Determination of Metal Behavior during the Incineration of a Contaminated Montmorillonite Clay; *Environ. Sci. Technol.* **1994**, *28*, 1791-1800.
238. Rink, K.K.; Kozinski, J.A.; Lighty, J.S. Biosludge Incineration in FBCs: Behavior of Ash Particles; *Combust. Flame* **1995**, *100*, 121-130.
239. Biswas, P.; Zachariah, M.R. In Situ Immobilization of Lead Species in Combustion Environments by Injection of Gas Phase Silical Sorbent Precursors; *Environ. Sci. Technol.* **1997**, *31(9)*, 2455-2463.
240. Wendt, J.O.L. Mechanisms Governing the Partitioning of Semi-Volatile Alkali and Toxic Metals during Waste and Waste Fuel Combustion. In *1st International Symposium on Incineration and Flue Gas Treatment Technologies;* Sheffield University, United Kingdom: 1997.
241. Linak, W.P.; Srivastava, R.K.; Wendt, J.O.L. Metal Aerosol Formation in a Laboratory Swirl Flame Incinerator. In *3rd International Congress on Toxic Combustion Byproducts;* Cambridge, MA: 1993.
242. Linak, W.P.; Ryan, J.V.; Wendt, J.O.L. Formation and Destruction of Hexavalent Chromium in a Laboratory Swirl Flame Incinerator; *Combust. Sci. Technol.* **1996**, *116-117(1-6)*, 479-498.
243. Chen, J.-C.; Wey, M.-Y. Simulation of Hexavalent Chromium Formation under Various Incineration Conditions; *Chemosphere* **1998**, *36(7)*, 1553-1564.
244. *Draft Test Report: A Performance Test on a Spray Dryer, Fabric Filter, Wet Scrubber System*; Radian Corporation; Report prepared for Shiva Garg; Office of Solid Waste; U.S. Environmental Protection Agency: 1989.
245. Kauppinen, E.I.; Pakkanen, T.A. Mass and Trace Element Size Distributions of Aerosols Emitted by a Hospital Refuse Incinerator; *Atmos. Environ.* **1990**, *24A*, 423-429.
246. Heywood, J.B. Future Engine Technology. Lessons from the 1980s for the 1990s; *J. Eng. Gas Turbines & Power, Transactions of the ASME* **1991**, *113(3)*, 319-330.
247. Khair, M.K. Progress in Diesel Engine Emissions Control; *J. Eng. Gas Turbines & Power, Transactions of the ASME* **1992**, *114(3)*, 568-577.
248. Degobert, P. *Automobiles and Pollution*; Society of Automotive Engineers: Warrendale, PA, 1995.
249. *Diesel Engines: Combustion and Emissions*; Society of Automotive Engineers: Warrendale, PA, 1999; Vol. SP-1484.
250. *Diesel Combustion, Emissions, and Exhaust Aftertreatment*; EI93010685312; Society of Automotive Engineers: Warrendale, PA, 1992.
251. Johnson, J.H.; Baines, T.M.; Clerc, J.C. *Diesel Particulate Emissions: Measurement Techniques, Fuel Effects and Control Technology*; Society of Automotive Engineers: Warrendale, PA, 1992; Vol. PT-42.
252. *Processes of Diesel Engine Combustion SP-1444*; Society of Automotive Engineers: Warrendale, PA, 1999.
253. Zhao, H.; Ladommatos, N. Optical Diagnostics for Soot and Temperature Measurements in Diesel Engines; *Prog. Energy Combust. Sci.* **1998**, *24(3)*, 221-255.
254. van Beckhoven, L.C. *Effects of Fuel Properties on Diesel Engine Emissions. A Review of Information Available to the EEC-MVEG Group*; SAE Technical Paper Series; Society of Automotive Engineers: Warrendale, PA, 1991.
255. Koltsakis, G.C.; Stametelos, A.M. Catalytic Automotive Exhaust Aftertreatment; *Prog. Energy Combust. Sci.* **1997**, *23(1)*, 1-39.
256. Neeft, J.P.A.; Makkee, M.; Moulijn, J.A. Diesel Particulate Emission Control; *Fuel Process. Technol.* **1996**, *47(1)*, 1-69.
257. Heywood, J.B. *Internal Combustion Engine Fundamentals*; McGraw Hill: New York, 1988.
258. *Handbook of Air Pollution from Internal Combustion Engines Pollutant Formation and Control*; Sher, E., Ed.; Academic Press: Boston, MA, 1998.
259. Flynn, P.F.; Durrett, R.; Hunter, G.; zur Loye, A.; Akinyemi, O.C.; Dec, J.; Westbrook, C. *Diesel Combustion: An Integrated View Combining Laser Diagnostics, Chemical Kinetics, and Empirical Validation*; 1999-01-0509; Society of Automotive Engineers: Warrendale, PA, 1999.
260. Bagley, S.T.; Baumgard, K.J.; Gratz, L.D.; Johnson, J.H.; Leddy, D.G. *Characterization of Fuel and Aftertreatment Device Effects on Diesel Emissions*; Research Report 76; Health Effects Institute: Cambridge, MA, 1996.
261. Ristovski, Z.D.; Morawska, L.; Bofinger, N.D.; Hitchins, J. Submicrometer and Supermicrometer Particulate Emission from Spark Ignition Vehicles; *Environ. Sci. Technol.* **1998**, *32(24)*, 3845-3852.
262. Abdul-Khalek, I.S.; Kittelson, D.B.; Graskow, B.R.; Wei, Q.; Brear, F. *Diesel Exhaust Particle Size: Measurement Issues and Trends*; 980525; Society of Automotive Engineers: Warrendale, PA, 1998.
263. Morawska, L.; Bofinger, N.D.; Kocis, L.; Nwankwoala, A. Submicrometer and Supermicrometer Particles Form Diesel Vehicle Emissions; *Environ. Sci. Technol.* **1998**, *32(14)*, 2033-2042.
264. Graskow, B.R.; Kittelson, D.B.; Abdul-Khalek, I.S.; Ahmadi, M.R.; Morris, J.E. *Characterization of Exhaust Particulate Emissions from a Spark Ignition Engine*; 980528; Society of Automotive Engineers: Warrendale, PA, 1998.
265. Maricq, M.M.; Podsiadlik, D.H.; Chase, R.E. Examination of the Size-Resolved and Transient Nature of Motor Vehicle Particle Emissions; *Environ. Sci. Technol.* **1999**, *33(10)*, 1618-1626.
266. Maricq, M.M.; Podsiadlik, D.H.; Chase, R.E. Gasoline Vehicle Particle Size Distributions: Comparison of Steady State, FTP, and US06 Measurements; *Environ. Sci. Technol.* **1999**, *33(12)*, 2007-2015.
267. Harrison, R.M.; Jones, M.; Collins, G. Measurements of the Physical Properties of Particles in the Urban Atmosphere; *Atmos. Environ.* **1999**, *33*, 309-321.
268. Hitchins, J.; Morawska, L.; Wolff, R.; Gilbert, D. Concentrations of Submicrometre Particles from Vehicle Emissions near a Major Road; *Atmos. Environ.* **1999**, *34*, 51-59.
269. Kittelson, D.B.; Dolan, D.F.; Oliver, R.B.; Aufderheide, E. Diesel Exhaust Particle Size Distributions–Fuel and Additive Effects. In *The Measurement and Control of Diesel Particulate Emissions;* Progress in Techology Series No. 17; Society of Automotive Engineers: Warrendale, PA, 1979; pp 233-244.
270. Kalghatgi, G.T. *Deposits in Gasoline Engines–A Literature Review*; SAE Paper 902108; Society of Automotive Engineers: Warrendale, PA, 1990.
271. Kayes, D.; Hochgreb, S. Mechanisms of Particulate Matter Formation in Spark-Ignition Engines. 2. Effect of Fuel, Oil, and Catalyst Parameters; *Environ. Sci. Technol.* **1999**, *33*, 3968-3977.
272. Sagebiel, J.C.; Zielinska, B.; Walsh, P.A.; Chow, J.C.; Cadle, S.H.; Mulawa, P.A.; Knapp, K.T.; Zweidinger, R.B.; Snow, R. PM10 Exhaust Samples Collected during IM-240 Dynamometer Tests of In-Service Vehicles in Nevada; *Environ. Sci. Technol.* **1997**, *31(1)*, 75-83.
273. Hawley, J.G.; Brace, C.J.; Wallace, F.J.; Horrocks, R.W. Combustion-Related Emissions in CI Engines. In *Handbook of Air Pollution from Internal Combustion Engines;* Sher, E., Ed.; Academic Press: Boston, MA, 1998; pp 280-357.
274. Tanaka, S.; Shimizu, T. A Study of Composition and Size Distribution of Particulate Matter from DI Diesel Engine SAE 1999-01-3487. In *Diesel Engines: Combustion and Emissions;* Society of Automotive Engineers: Warrendale, PA, 1999.
275. Rogge, W.F.; Hildemann, L.M.; Mazurek, M.A.; Cass, G.R. Sources of Fine Organic Aerosol 2. Noncatalyst and Catalyst-Equipped Automobiles and Heavy-Duty Diesel Trucks; *Environ. Sci. Technol.* **1993**, *27(4)*, 636-651.
276. Schauer, J.J.; Kleenam, M.J.; Cass, G.R.; Simoneit, B.R.T. Measurement of Emission from Air Pollution Sources. 2. C1 through C30 Organic Compounds from Medium Duty Diesel Trucks; *Environ. Sci. Technol.* **1999**, *33(10)*, 1578-1587.
277. *Emission Regulations for New Otto-Cycle and Diesel-Cycle Heavy-Duty Engines; Gaseous and Particulate Exhaust Test Procedures;* 40CFR86 Subpart N; Office of the Federal Registrar; U.S. Government Printing Office: 1998.
278. Hildemann, L.M.; Cass, G.R.; Markowski, G.R. A Dilution Stack Sampler for Collection of Organic Aerosol Emissions: Design, Characterization, and Field Tests; *Aerosol Sci. Technol.* **1989**, *10*, 193-204.
279. Ball, J.C. *Emission Rates and Elemental Composition of Particles Collected from 1995 Ford Vehicles Using the Urban Dynamometer Driving Schedule, The Highway Fuel Economy Test, and the US06 Driving Cycle*; SAE 972914; Society of Automotive Engineers: Warrendale, PA, 1997.
280. Cadle, S.H.; Mulawa, P.A.; Ball, J.; Donase, C.; Weibel, A.; Sagebiel, J.C.; Knapp, K.T.; Snow, R. Particulate Emission Rates from In-Use High-Emitting Vehicles Recruited in Orange County, California; *Environ. Sci. Technol.* **1997**, *31(12)*, 3405-3412.
281. Williams, D.J. Particulate Emissions from "In-Use" Motor Vehicles. 1. Spark Ignition Engines; *Atmos. Environ.* **1989**, *23*, 2639-2645.
282. Zayed, J.; Hong, B.; L'Espérance, G. Characterization of Manganese-Containing Particles Collected from the Exhaust Emissions of Automobiles Running with MMT Additive; *Environ. Sci. Technol.* **1999**, *33(19)*, 3341-3346.
283. Rote, D.M. *Impact of Aircraft Emissions on Air Quality in the Vicinity of Airports, Volume III: Air Quality and Emission Modeling Needs*; FAA Report FAA-EE-84-13; USAF Report ESL-TR-84-35; U.S. Department of Transportation Federal Aviation Administration: 1984.
284. Douglas, E. *Effectiveness of Fuel Additives in Reducing Visible Emissions from J79-GE-15A Gas Turbine Engines*; ASEO Report No. 3-96; Aircraft Environmental Support Office; Naval Aviation Depot: 1996.
285. Petzold, A.; Schröder, F.P. Jet Engine Exhaust Aerosol Characterization; *Aerosol Sci. Technol.* **1998**, *28*, 62-76.
286. Anderson, B.E.; Cofer, W.R.; Bagwell, D.R.; Barrick, J.W.; Hudgins, C.H.; Burke, K.E. Airborne Observations of Aircraft Aerosol Emissions I: Total Nonvolatile Particle Emission Indices; *Geophys. Res. Lett.* **1998**, *25(10)*, 1689-1692.
287. Hagen, D.; Whitefield, P.; Paladino, J.; Trueblood, M.; Lilenfeld, H. Particle Sizing and Emission Indices for a Jet Engine Exhaust Sampled at Cruise Altitude; *Geophys. Res. Lett.* **1998**, *25(10)*, 1681-1684.

288. Hagen, D.E.; Trueblood, M.B.; Whitefield, P.D. A Field Sampling of Jet Exhaust Aerosols; *Part. Sci. Technol.* **1992**, *10*, 53-63.
289. Jones, R.E. Gas Turbine Emissions—Problems, Progress, and Future; *Prog. Energy Combust. Sci.* **1978**, *4*, 73-112.
290. Stockham, J.D.; Luebcke, E.H.; Fenton, D.L.; Johnson, R.H.; Campbell, P.P. *Turbine Engine Particulate Emission Characterization*; FAA-RD-79-15; Federal Aviation Administration: 1979.
291. Wilson, W.E.; Mage, D.T.; Grant, L.D. Estimating Separately Personal Exposure to Ambient and Non-Ambient Particulate Matter for Epidemiology and Risk Assessment: Why and How, *J. Air & Waste Manage. Assoc.* **2000**, *50*, 1167-1183.
292. Lillquist, D.R.; Lee, J.S.; Ramsey, J.R.; Boucher, K.M.; Walton, Z.L.; Lyon, J.L. A Comparison of Indoor/Outdoor PM_{10} Concentrations Measured at Three Hospitals and a Centrally Located Monitor in Utah; *Appl. Occup. Environ. Hyg.* **1998**, *13(6)*, 409-415.
293. Whitby, K.T.; Sverdrup, G.M. California Aerosols: Their Physical and Chemical Characteristics. In *The Character and Origins of Atmospheric Aerosols: A Digest of Results from the California Aerosol Characterization Experiment (ACHEX);* Hidy, G.M., et al., Eds.; Advances in Environmental Science and Technology; Wiley: New York, 1980; pp 477-517.
294. Watson, J.G.; Chow, J.C. *Reconciling Urban Fugitive Dust Emissions Inventory and Ambient Source Concentration Estimates: Summary of Current Knowledge and Needed Research*; DRI Document No. 6110.4D2; Desert Research Institute: 1999.
295. Harrison, R.M.; Brimblecombe, P.; Derwent, R.G.; Dollard, G.J.; Eggleston, S.; Hamilton, R.S.; Hickman, A.J.; Holman, C.; Laxen, D.P.H.; Moorcroft, S. *Airborne Particulate Matter in the United Kingdom*; Third Report of the Quality of Urban Air Review Group; Department of the Environment; University of Birmingham, United Kingdom: 1996.
296. Ahuja, K.O.; Paskind, J.J.; Houck, J.E.; Chow, J.C. Design of a Study for the Chemical and Size Characterization of Particulate Matter Emissions from Selected Sources in California. In *Transactions, Receptor Models in Air Resources Management;* Watson, J.G., Ed.; Air & Waste Management Association: Pittsburgh, PA, 1989; pp 145-158.
297. Jaenicke, R. Tropospheric Aerosols. In *Aerosol-Cloud-Climate Interactions;* Hobbs, P.V., Ed.; Academic Press: San Diego, CA, 1993; pp 1-31.
298. Hughes, L.C.; Cass, G.R.; Gone, J.; Ames, M.; Olmez, I. Physical and Chemical Characterization of Atmospheric Ultrafine Particulates in the Los Angeles Area; *Environ. Sci. Technol.* **1998**, *32(9)*, 1153-1161.
299. Penchin, P.M. National PM Study: OPPE Particulate Programs Evaluation System, 1994. In *Particles In Our Air*; Wilson, R., Spengler, J., Eds.; Harvard University Press: 1996.
300. *National Air Quality and Emissions Trends Report, 1997*; EPA 454/R-98-016; U.S. Environmental Protection Agency; Office of Air Quality Planning and Standards: 1998.
301. *Latest Findings on National Air Quality: 1997 Status and Trends*; EPA 454/F-98-009; U.S. Environmental Protection Agency; Office of Air Quality Planning and Standards: 1998.
302. Chen, M.L.; Mao, I.F.; Lin, I.K. The $PM_{2.5}$ and PM_{10} Particles in Urban Areas of Taiwan; *Sci. Total Environ.* **1999**, *226(2-3)*, 227-235.
303. Chen, W.-C.; Wang, C.-S.; Wei, C.-C. Assessment of Source Contributions to Ambient Aerosols in Taiwan; *J. Air & Waste Manage. Assoc.* **1997**, *47(4)*, 501-509.
304. Tuch, T.; Brand, P.; Wichmann, H.E.; Heyder, J. Variation of Particle Number and Mass Concentration in Various Size Ranges of Ambient Aerosol in Eastern Germany; *Atmos. Environ.* **1997**, *31(24)*, 4193-4197.
305. *Air Quality Criteria for Particulate Matter*; EPA/600/P-95-001 aF thru cF; U.S. Environmental Protection Agency: 1996.
306. *Receptor Modeling for Air Quality Management*; Hopke, P.K., Ed.; Data Handling in Science and Technology; Elsevier: New York, 1991.
307. Watson, J.G.; Robinson, N.F.; Fujita, E.M.; Chow, J.C.; Pace, T.G.; Lewis, C.; Coulter, T. *CMB8–Applications and Validation Protocol for $PM_{2.5}$ and VOCS*; DRI Document No. 1980.2D1; Desert Research Institute: 1998.
308. Cass, G.R.; Gray, H.A. *Regional Emissions and Atmospheric Concentrations of Diesel Engine Particulate Matter: Los Angeles as a Case Study in Diesel Exhaust: A Critical Analysis of Emissions, Exposure, and Health Effects*; Health Effects Institute: 1995.
309. Kleeman, M.J.; Eldering, A.; Cass, G.R. Modeling the Airborne Particulate Complex as a Source-Oriented External Mixture; *J. Geophys. Res.* **1997**, *102(D17)*, 21,355-21,372.
310. Kleeman, M.J.; Cass, G.R. Source Contributions to the Size and Composition Distribution of the Urban Particulate Air Pollution; *Atmos. Environ.* **1998**, *32(16)*, 2803-2816.
311. Evelyn, J. Fumigorum or the Inconvenience of the Aer and Smoake of London Dessipated: Together with Some Remdies Hombly Proposed, 1661. Cited in *Advances in Environmental Science*; Pitts, Metcalf, Eds.; Wiley-Interscience: New York, 1969.
312. Bonfanti, L.; De Michele, G.; Riccardi, J.; Lopes-Doriga, E. Influence of Coal Type and Operating Conditions on the Formation of Incomplete Combustion Products. Pilot Plant Experiments; *Combust. Sci. Technol.* **1994**, *10*, 505-525.
313. Busch, R.H.; Buschbom, R.L.; Cannon, W.C.; Lauhala, K.E.; Miller, F.J.; Graham, J.A.; Smith, L.G. Effects of Ammonium Nitrate Aerosol Exposure on Lung Structure of Normal and Elastase-Impaired Rats and Guinea Pigs; *Environ. Res.* **1986**, *39(2)*, 237-252.
314. Carter, J.D.; Ghio, A.J.; Samet, J.M.; Devlin, R.B. Cytokine Production by Human Airway Epithelial Cells after Exposure to an Air Pollution Particle Is Metal-Dependent; *Toxicol. Appl. Pharmacol.* **1997**, *146(2)*, 180-188.
315. Chen, L.C.; Lam, H.F.; Ainsworth, D.; Guty, J.; Amdur, M.O. Functional Changes in the Lungs of Guinea Pigs Exposed to Sodium Sulfite Aerosols; *Toxicol. Appl. Pharamacol.* **1987**, *89*, 1.
316. Chin, B.Y.; Choi, M.E.; Burdick, M.D.; Strieter, R.M.; Risby, T.H.; Choi, A.M. Induction of Apoptosis by Particulate Matter: Role of TNF-Alpha and MAPK; *Am. J. Physiol.* **1998**, *275(5 Pt 1)*, L942-949.
317. Costa, D.L.; Dreher, K.L. Bioavailable Transition Metals in Particulate Matter Mediate Cardiopulmonary Injury in Healthy and Compromised Animal Models; *Environ. Health Perspect.* **1997**, *105(Suppl 5)*, 1053-1060.
318. Dockery, D.W.; Pope, A.C.; Xiping, X.; Spengler, J.D.; Ware, J.H.; Fay, M.E.; Ferris, B.G.; Speizer, F.E. An Association between Air Pollution and Mortality in Six U.S. Cities; *New Engl. J. Med.* **1993**, *329(24)*, 1753-1759.
319. Donaldson, K. Local Inflammatory and Systemic Effects Following Short-Term Inhalation Exposure to Fine and Ultrafine Carbon Black in Rats. In *The Health Effects of Fine Particles: Key Questions and the 2003 Review, Brussels, Belgium*; Health Effects Institute: Cambridge, MA, 1999; pp II-171.
320. Elder, A.C.P.; Gelein, R.; Finkelstein, J.N.; Cox, C.; Oberdörster, G. Endotoxin Priming Affects the Lung Response to Ultrafine Particles and Ozone in Young and Old Rats; *Inhal. Toxicol.* **2000**, *12(Suppl 1)*, 85-98.
321. *An Acid Aerosols Issue Paper: Health Effects and Aerometrics*; EPA-600/8-88-005F, NTIS PB91-125864; U.S. Environmental Protection Agency: 1989.
322. Frampton, M.W.; Ghio, A.J.; Samet, J.M.; Carson, J.L.; Carter, J.D.; Devlin, R.B. Effects of Aqueous Extracts of PM_{10} Filters from the Utah Valley on Human Airway Epithelial Cells; *Lung Cell. Mol. Physiol.* **1999**, *21*, L960-L967.
323. Gong, H.; Sioutas, C.; Linn, W.S.; Clark, K.W.; Terrell, S.L.; Terrell, L.L.; Anderson, K.R.; Kim, S.; Chang, M.-C. Controlled Human Exposures to Concentrated Ambient Fine Particles in Metropolitan Los Angeles: Methodology and Preliminary Health-Effect Findings; *Inhal. Toxicol.* **2000**, *12(Suppl 1)*, 107-119.
324. *Diesel Exhaust: A Critical Analysis of Emissions, Exposure, and Health Effects*; Health Effects Institute: Cambridge, MA, 1995.
325. Hoek, G.; Schwartz, J.D.; Groot, B.; Eilers, P. Effects of Ambient Particulate Matter and Ozone on Daily Mortality in Rotterdam, The Netherlands; *Arch. Environ. Health* **1997**, *52(6)*, 455-463.
326. Kadiiska, M.B.; Mason, R.P.; Dreher, K.L.; Costa, D.L.; Ghio, A.J. In Vivo Evidence of Free Radical Formation in the Rat Lung after Exposure to an Emission Source Air Pollution Particle; *Chem. Res. Toxicol.* **1997**, *10(10)*, 1104-1108.
327. Kennedy, T.; Ghio, A.J.; Reed, W.; Samet, J.; Zagorski, J.; Quay, J.; Carter, J.; Dailey, L.; Hoidal, J.R.; Devlin, R.B. Copper-Dependent Inflammation and Nuclear Factor-kB Activation by Particulate Air Pollution; *Am. J. Respir. Cell Mol. Biol.* **1998**, *19*, 1-14.
328. Lewtas, J. Genotoxicity of Complex Mixtures: Strategies for the Identification and Comparative Assessment of Airborne Mutagens and Carcinogens from Combustion Sources; *Fundam. Appl. Toxicol.* **1988**, *10*, 571-589.
329. Li, X.Y.; Brown, D.; Smith, S.; MacNee, W.; Donaldson, K. Short-Term Inflammatory Responses following Intratracheal Instillation of Fine and Ultrafine Carbon Black in Rats; *Inhal. Toxicol.* **1999**, *11(8)*, 709-731.
330. Nikula, K.J.; Snipes, M.B.; Barr, E.B.; Griffith, W.C.; Henderson, R.F.; Mauderly, J.L. Comparative Pulmonary Toxicities and Carcinogenicities of Chronically Inhaled Diesel Exhaust and Carbon Black in F344 Rats; *Fundam. Appl. Toxicol.* **1995**, *25(1)*, 80-94.
331. Oberdörster, G.; Ferin, J.; Gelein, R.; Soderholm, S.C.; Finkelstein, J. Role of the Alveolar Macrophage in Lung Injury; Studies with Ultrafine Particles; *Environ. Health Perspect.* **1992**, *97*, 193-199.
332. Oberdörster, G.; Ferin, J.; Lehnert, B.E. Correlation between Particle Size, In Vivo Particle Persistence, and Lung Injury; *Environ. Health Perspect.* **1994**, *102(Suppl 5)*, 173-179.
333. Pagano, P.; Zaiacomo, T.D.; Scarcella, E.; Bruni, S.; Calamosca, M. Mutagenic Activity of Total and Particle-Sized Fractions of Urban Particulate Matter; *Environ. Sci. Technol.* **1996**, *30(12)*, 3512-3516.
334. Patterson, E.; Eatough, D.J. Indoor/Outdoor Relationships for Ambient $PM_{2.5}$ and Associated Pollutants: Epidemiological Implications in Lindon, Utah; *J. Air & Waste Manage. Assoc.* **2000**, *50(1)*, 103-110.
335. Peters, A.; Wichmann, H.E.; Tuch, T.; Heinrich, J.; Heyder, J. Respiratory Effects Are Associated with the Number of Ultrafine Particles; *Am. J. Respir. Crit. Care Med.* **1997**, *155(4)*, 1376-1383.

336. Petrovic, S.; Urch, B.; Brook, J.; Datema, J.; Purdham, J.; Liu, L.; Lukic, Z.; Zimmerman, B.; Tofler, G.; Downar, E.; Cory, P.; Tarlo, S.; Broder, I.; Dales, R.; Silverman, F. Cardiorespiratory Effects of Concentrated Ambient $PM_{2.5}$: A Pilot Study Using Controlled Human Exposures; *Inhalation Toxicol.* **2000**, *12(Suppl 1)*, 173-188.
337. Pope, C.A. Epidemiology Investigations of the Health Effects of Particulate Air Pollution: Strengths and Limitations; *Appl. Occup. Environ. Hyg.* **1998**, *13(6)*, 356-363.
338. Pope, A.C.; Hill, R.W.; Villegas, G.M. Particulate Air Pollution and Daily Mortality on Utah's Wasatch Front; *Environ. Health Perspect.* **1999**, *107(7)*, 567-573.
339. Samet, J.M.; Zerer, S.L.; Kelsall, J.E.; Xu, J. Particulate Air Pollution and Mortality: The Particle Epidemiology Evaluation Project; *Appl. Occup. Environ. Health* **1998**, *13(6)*, 364-369.
340. Schwartz, J.; Dockery, D.W. Particulate Air Pollution and Daily Mortality in Steubenville, Ohio; *Am. J. Epidemiol.* **1992**, *135(1)*, 12-19.
341. Schwartz, J.; Norris, G.; Larson, T.; Shepphard, L.; Claiborne, C.; Koenig, J. Episodes of High Coarse Particle Concentrations Are Not Associated with Increased Mortality; *Environ. Health Perspect.* **1999**, *107(5)*, 339- 342.
342. Smith, K.R.; Aust, A.E. Mobilization of Iron from Urban Particulates Leads to Generation of Reactive Oxygen Species In Vitro and Induction of Ferritin Synthesis in Human Lung Epithelial Cells; *Chem. Res. Toxicol.* **1997**, *10(7)*, 828-834.
343. Smith, K.R.; Veranth, J.M.; Lighty, J.S.; Aust, A.E. Mobilization of Iron from Coal Fly Ash Was Dependent upon Particle Size and Source of Coal; *Chem. Res. Toxicol.* **1998**, *11(12)*, 1494-1500.
344. Smith, K.R.; Veranth, J.M.; Hu, A.A.; Lighty, J.S.; Aust, A.E. Interleukin-8 Levels in Human Lung Epithelial Cells Are Increased in Response to Coal Fly Ash and Vary with Bioavailability of Iron, as a Function of Particle Size and Source of Coal; *Chem. Res. Toxicol.* **2000**, *13*, 118-125.
345. Spurny, K.R. On the Physics, Chemistry and Toxicology of Ultrafine Anthropogenic, Atmospheric Aerosols (UAAA): New Advances; *Toxicol. Lett.* **1998**, *96-97*, 253-261.
346. Takenaka, S.; Dornhöfer-Takenaka, H.; Muhle, H. Alveolar Distribution of Fly Ash and of Titanium Dioxide after Long-Term Inhalation by Wistar Rats; *J. Aerosol Sci.* **1986**, *17*, 361-364.
347. Valberg, P.A.; Watson, A.Y. Lack of Concordance between Reported Lung-Cancer Risk Levels and Occupation-Specific Diesel Exhaust Exposures; *Inhalation Toxicol.* **2000**, *12(Suppl 10)*, 199-208.
348. Veranth, J.M.; Smith, K.R.; Rohrbough, J.G.; Huggins, F.; Hu, A.A.; Lighty, J.S.; Aust, A.E. Mossbauer Spectroscopy Indicates that Iron in an Aluminosilicate Glass Phase Is the Source of the Bioavailable Iron from Coal Fly Ash; *Chem. Res. Toxicol.* **2000**, *13*, 161-164.
349. Mauderly, J.L. Toxicological and Epidemiological Evidence for Health Risks from Inhaled Engine Emissions; *Environ. Health Perspect.* **1994**, *102(Suppl 4)*, 165-171.
350. Goldsmith, C.A.; Kobzik, L. Particulate Air Pollution and Asthma: A Review of Epidemiological and Biological Studies; *Rev. Environ. Health* **1999**, *14(3)*, 121-134.
351. Phalen, R.; Bell, Y.M. *Proceedings of the 3rd Colloquium on Particulate Air Pollution and Health*; Air Pollution Health Effects Laboratory; University of California: Irvine, CA, 1999.
352. *PM2000: Particulate Matter and Health—The Scientific Basis for Regulatory Decision-Making, Charleston, SC; Extended Abstract Book;* Air & Waste Management Association: Pittsburgh, PA, 2000.
353. USC, Clean Air Act, Section 109 (b)(1), 42 USC 7401. Public Law 101-549, 1990.
354. Pope, A.C. Respiratory Disease Associated with Community Air Pollution and a Steel Mill, Utah Valley; *Am. J. Pub. Health* **1989**, *89(5)*, 623-628.
355. Dockery, D.W.; Pope, C.A.I. Outdoor Air 1: Particulates. In *Topics in Environmental Epidemiology;* Steenland, K., Savitz, D.A., Eds.; Oxford University Press: New York, 1997; pp 119-166.
356. Samet, J.M.; Jaakkola, J.J.K. The Epidemiologic Approach to Investigating Outdoor Air Pollution. In *Air Pollution and Health;* Holgate, S.T., et al., Eds.; Academic Press: San Diego, CA, 1999; pp 406-460.
357. McCullagh, P.; Nelder, J.A. *Generalized Linear Models*; Chapman and Hall: London, 1989.
358. Samet, J.; Zeger, S.; Xu, J. Particulate Air Pollution and Mortality: The Particle Epidemiology Evaluation Project; *Appl. Occup. Environ. Hyg.* **1998**, *13(6)*, 364-369.
359. *Particulate Air Pollution and Daily Mortality: Analysis of the Effects of Weather and Multiple Air Pollutants*; The Phase I.B Report of the Particle Epidemiology Evaluation Project; Health Effects Institute: Cambridge, MA, 1997.
360. Watts, W.F.J. Assessment of Occupational Exposure to Diesel Emissions. In *Diesel Exhaust: A Critical Analysis of Emissions, Exposure, and Health Effects;* Group, D.W., Ed.; Health Effects Institute: Cambridge, MA, 1995; pp 107-123.
361. *TLVs Threshold Limit Values for Chemical Substances and Physical Agents and Biological Exposure Indices;* American Conference of Governmental Industrial Hygienists: Cincinnati, OH, 2000.
362. Harrison, R.M.; Yin, J. Particulate Matter in the Atmosphere: Which Particle Properties Are Important for Its Effects on Health? *Sci. Total Environ.* **2000**, *249*, 85-101.
363. Carel, R.S. Health Aspects of Air Pollution. In *Handbook of Air Pollution from Internal Combustion Engines;* Sher, E., Ed.; Academic Press: Boston, MA, 1998; pp 42-64.
364. Guyton, A.C.; Hall, J.E. *Textbook of Medical Physiology*; Saunders: Philadelphia, PA, 1996.
365. Netter, F.H. *Respiratory System: A Compilation of Paintings Depicting Anatomy and Embryology, Physiology, Pathology, Pathophysiology, and Clinical Features and Treatment of Diseases*; Divertie, M.B., Ed.; CIBA Pharmaceutical Products: Summit, NJ, 1980.
366. International Commission on Radiological Protection Task Force on Lung Dynamics; *Health Physics* **1966**, *12*, 173-207.
367. Wilson, R.; Spengler, J. *Particles in Our Air: Concentrations and Health Effects*; Harvard University Press: Cambridge, MA, 1996.
368. Lennon, S.; Zhang, Z.; Lessmann, R.; Webster, S. Experiments on Particle Deposition in the Human Upper Respiratory System; *Aerosol Sci. Technol.* **1998**, *28(5)*, 464-474.
369. Matthews, L.R. *Cardiopulmonary Anatomy and Physiology;* Lippincott: Philadelphia, PA, 1996.
370. Sioutas, C.; Koutrakis, P.; Burton, R.M. A High-Volume Small Cutpoint Virtual Impactor for Separation of Atmospheric Particulate from Gaseous Pollutants; *Part. Sci. Technol.* **1994**, *12*, 207-221.
371. Sioutas, C.; Koutrakis, P.; Burton, R.M. A Technique to Expose Animals to Concentrated Fine Ambient Aerosols; *Environ. Health Perspect.* **1995**, *103(2)*, 172-177.
372. Sioutas, C.; Koutrakis, P. Inertial Separation of Ultrafine Particles Using a Condensational Growth/Virtual Impaction System; *Aerosol Sci. Technol.* **1996**, *25*, 424-436.
373. Gordon, T.; Gerber, H.; Fang, C.P.; Chen, L.C. A Centrifugal Particle Concentrator for Use in Inhalation Toxicology; *Inhalation Toxicol.* **1999**, *11(1)*, 71-87.
374. Clarke, R.W.; Catalano, P.; Coull, B.; Koutrakis, P.; Murthy, G.G.K.; Rice, T.; Godleski, J.J. Age-Related Responses in Rats to Concentrated Urban Air Particles (CAPs); *Inhalation Toxicol.* **2000**, *12(Suppl 10)*, 73-84.
375. Godleski, J.; Verrier, R.L.; Koutrakis, P.; Catalano, P. *Mechanisms of Morbidity and Mortality from Exposure to Ambient Air Particles*; Research Report 91; Health Effects Institute: Cambridge, MA, 2000.
376. Amdur, M.O.; Chen, L.C. Furnace-Generated Acid Aerosols: Speciation and Pulmonary Effects; *Environ. Health Perspect.* **1989**, *79*, 147-150.
377. Oberdörster, G.; Gelein, R.M.; Ferin, J.; Weiss, B. Association of Particulate Air Pollution and Acute Mortality: Involvement of Ultrafine Particles? *Inhalation Toxicol.* **1995**, *7*, 111-124.
378. Fonda, M.; Petach, M.; Rogers, C.F.; Huntington, J.; Stratton, D.; Nishioka, K.; Tipo, M. Resuspension of Particles by Aerodynamic Deagglomeration; *Aerosol Sci. Technol.* **1999**, *30(6)*, 509-529.
379. Chow, J.C.; Watson, J.G.; Houck, J.E.; Pritchett, L.C.; Rogers, C.F.; Frazier, C.A.; Egami, R.T.; Ball, B.M. A Laboratory Resuspension Chamber to Measure Fugitive Dust Size Distributions and Chemical Compositions; *Atmos. Environ.* **1994**, *28(21)*, 3463-3481.
380. Kousaka, Y.; Horiuchi, T.; Endo, Y.; Aotani, S. Generation of Aerosol Particles by Boiling Suspensions; *Aerosol Sci. Technol.* **1994**, *21*, 236-240.
381. Terashima, T.; Wiggs, B.; English, D.; Hogg, J.C.; van Eeden, S.F. Phagocytosis of Small Carbon Particles (PM_{10}) by Alveolar Macrophages Stimulates the Release of Polymorphonuclear Leukocytes from Bone Marrow; *Am. J. Respir. Crit. Care Med.* **1997**, *155(4)*, 1441-1447.
382. Liu, W.K.; Wong, C.C. Cytotoxicity of Fly-Ash in Alveolar Macrophages from Hypothyroid Rats; *Toxicol. in Vitro* **1989**, *3(2)*, 95-102.
383. Kennedy, H.L. Beta Blockade, Ventricular Arrhythmias, and Sudden Cardiac Death; *Am. J. Cardiol.* **1997**, *80(9B)*, 29J-34J.
384. Dockery, D.W.; Pope, C.A.; Kanner, R.E.; Villegas, G.M.; Schwartz, J. *Daily Changes in Oxygen Saturation and Pulse Rate Associated with Particulate Air Pollution and Barometric Pressure*; Research Report 83; Health Effects Institute: Cambridge, MA, 1999; p 1-19.
385. Pope, C.A.; Verrier, R.L.; Lovett, E.G.; Larson, A.C.; Raizenne, M.E.; Kanner, R.E.; Schwartz, J.; Villegas, G.M.; Gold, D.R.; Dockery, D.W. Heart Rate Variability Associated with Particulate Air Pollution; *Am. Heart J.* **1999**, *138(5 Pt 1)*, 890-899.
386. Gold, D.R.; Litonjua, A.; Schwartz, J.; Lovett, E.; Larson, A.; Nearing, B.; Allen, G.; Verrier, M.; Cherry, R.; Verrier, R. Ambient Pollution and Heart Variability; *Circulation* **2000**, *101(11)*, 1267-1273.
387. Nelson, S.; Martin, T.R. *Cytokines in Pulmonary Disease: Infection and Inflammation*; *Lung Biology in Health and Disease*; Marcel Dekker: New York, 2000; Vol. 141.
388. Thèze, J. *The Cytokine Network and Immune Functions*; Oxford University Press: New York, 1999.
389. Seaton, A.; MacNee, W.; Donaldson, K.; Godden, D. Particulate Air Pollution and Acute Health Effects; *Lancet* **1995**, *345(8943)*, 176-178.

390. Souza, M.B.; Saldiva, P.H.; Pope, C.A.; Capelozzi, V.L. Respiratory Changes Due to Long-Term Exposure to Urban Levels of Air Pollution: A Histopathologic Study in Humans; *Chest* **1998**, *113(5)*, 1161-1162.
391. Prichard, R.J.; Ghio, A.J.; Lehmann, J.R.; Witsett, D.W.; Tepper, J.S.; Park, P.; Gilmour, M.I.; Dreher, K.L.; Costa, D.L. Oxidant Generation and Lung Injury after Particulate Air Pollutant Exposure Increase with the Concentrations of Associated Metals; *Inhal. Toxicol.* **1996**, *8(5)*, 457-477.
392. Ghio, A.J.; Stonehuerner, J.; Prichard, R.J.; Pintadosi, C.A.; Quigley, D.R.; Dreher, K.L.; Costa, D.L. Humic-Like Substances in Air Pollution Particulates Correlate with Concentrations of Transition Metals and Oxidant Generation; *Inhal. Toxicol.* **1996**, *8*, 479-494.
393. Driscoll, K.E. TNF-alpha and MIP-2: Role in Particle-Induced Inflammation and Regulation by Oxidative Stress; *Toxicol. Lett.* **2000**, *112-113*, 177-183.
394. Ghio, A.J.; Kennedy, T.P.; Whorton, A.R.; Crumbliss, A.L.; Hatch, G.E.; Hoidal, J.R. Role of Surface Complexed Iron in Oxidant Generation and Lung Inflammation Induced by Silicates, *Am. J. Physiol.* **1992**, *263*, L511-L518.
395. Lewis, R.J.J. *Sax's Dangerous Properties of Industrial Materials*; Van Nostrand Reinhold: New York, 1992; Vol. v1-v3.
396. Wallace, L.; Slonecker, T. Ambient Air Concentrations of Fine ($PM_{2.5}$) Manganese in U.S. National Parks and in California and Canadian Cities: The Possible Impact of Adding MMT to Unleaded Gasoline; *J. Air & Waste Manage. Assoc.* **1997**, *47*, 642-653.
397. Mena, I. Trace Minerals. In *Disorders of Mineral Metabolism*; Bronner, F., Coburn, J.W., Eds.; Academic Press: New York, 1981; Vol. 1.
398. Mena, I.; Horiuchi, K.; Burke, K.; Cotzias, G.C. Chronic Manganese Poisoning: Individual Susceptibility and the Absorption of Iron; *Neurology* **1969**, *19*, 1000-1006.
399. Halliwell, B.; Gutteridge, J.M.C. *Free Radicals in Biology and Medicine*; Oxford University Press: Oxford, United Kingdom, 1999.
400. Vogl, G.; Elstner, E.F. Diesel Soot Particles Catalyze the Production of Oxyradicals; *Toxicol. Lett.* **1989**, *47*, 17-23.
401. Prahalad, A.K.; Soukup, J.M.; Inmon, J.; Willis, R.; Ghio, A.J.; Becker, S.; Gallagher, J.E. Ambient Air Particles: Effects on Cellular Oxidant Radical Generation in Relation to Particulate Elemental Chemistry; *Toxicol. Appl. Pharmacol.* **1999**, *158(2)*, 81-91.
402. Veranth, J.M.; Smith, K.R.; Hu, A.A.; Lighty, J.S.; Aust, A.E. Mobilization of Iron from Coal Fly Ash Was Dependent upon the Particle Size and the Source of Coal: Analysis of Rates and Mechanisms; *Chem. Res. Toxicol.* **2000**, *13*, 382-389.
403. Veranth, J.M.; Smith, K.R.; Aust, A.E.; Dansie, S.L.; Griffith, J.B.; Hu, A.A.; Huggins, M.L.; Lighty, J.S. Coal Fly Ash and Mineral Dust for Toxicology and Particle Characterization Studies: Equipment and Methods for $PM_{2.5}$- and PM_1-Enriched Samples; *Aerosol Sci. Technol.* **2000**, *32(2)*, 127-141.
404. Fang, R.; Aust, A.E. Ferritin Induction in Human Lung Epithelial Cells as an Indicator of Intracellular Iron Mobilization from Particulates, submitted for publication.
405. Levenspiel, O. *Chemical Reaction Engineering*; Wiley: New York, 1972.
406. Shirnamé-Moré, L. Genotoxicity of Diesel Emissions Part I: Mutagenicity and Other Genetic Effects. In *Diesel Exhaust: A Critical Analysis of Emissions, Exposure, and Health Effects;* Group, D.W., Ed.; Health Effects Institute: Cambridge, MA, 1995; pp 221-242.
407. Rosenkranz, H.S. Genotoxicity of Diesel Emissions Part II: The Possible Role of Dinitropyrenes in Lung Cancer. In *Diesel Exhaust: A Critical Analysis of Emissions, Exposure, and Health Effects;* Group, D.W., Ed.; Health Effects Institute: Cambridge, MA, 1995; pp 221-242.
408. Peterson, R.E.; Theobald, H.M.; Kimmel, G.L. Developmental and Reproductive Toxicity of Dioxins and Related Compounds: Cross-Species Comparisons; *Crit. Rev. Toxicol.* **1993**, *23(3)*, 285-335.
409. Kuschner, W.G.; Wong, H.; D'Alessardro, A.; Quinlan, P.; Blanc, P.D. Human Pulmonary Responses to Experimental Inhalation of High Concentration Fine and Ultrafine Magnesium Oxide Particles; *Environ. Health Perspect.* **1997**, *105(11)*, 1234-1237.
410. Baggs, R.B.; Ferin, J.; Oberdörster, G. Regression of Pulmonary Lesions Produced by Inhaled Titanium Dioxide in Rats; *Vet. Pathol.* **1997**, *34(6)*, 592-597.
411. Churg, A.; Gilks, B.; Dai, J. Induction of Fibrogenic Mediators by Fine and Ultrafine Titanium Dioxide in Rat Tracheal Explants; *Am. J. Physiol.* **1999**, *277*, L975-L982.
412. *Council Directive of 15 July 1980 on Air Quality Limit Values for Sulphur Dioxide and Suspended Particulates*; O.J. L229/30; Council of the European Communities: 1980.
413. Amdur, M.O. Sulfuric Acid: The Animals Tried to Tell Us. In the 1989 Herbert E. Stokinger Lecture; *Appl. Ind. Hyg.* **1989**, *4(8)*, 189-197.
414. EPA National Ambient Air Quality Standards for Ozone and Particulate. *Fed. Regist.* **1996**, *61(114)*, 29719-29725.
415. *Research Priorities for Airborne Particulate Matter: I. Immediate Priorities and a Long-Range Research Portfolio*; National Research Council; National Academy Press: Washington, DC, 1998.
416. *Research Priorities for Airborne Particulate Matter: II. Evaluating Research Progress and Updating the Portfolio*; National Research Council; National Academy Press: Washington, DC, 1999.
417. EPA Final Regional Haze Regulations for Protection of Visibility in National Parks and Wilderness Areas. *Fed. Regist.* **1999**, *64(126)*, 35713-35774.
418. Tang, H.; Lewis, E.A.; Eatough, D.J.; Burton, R.M.; Farber, R.J. Determination of the Particle Size Distribution and Chemical Composition of Semi-Volatile Organic Compounds in Atmospheric Fine Particles with a Diffusion Denuder Sampling System; *Atmos. Environ.* **1994**, *28(5)*, 939-947.
419. Cui, W.; Eatough, D.J.; Eatough, N.L. Fine Particulate Organic Matter in the Los Angeles Basin–I: Assessment of the High-Volume Brigham Young University Organic Sampling System BIG BOSS; *J. Air & Waste Manage. Assoc.* **1998**, *48(11)*, 1024-1037.
420. Corio, L.A.; Sherwell, J. In-Stack Condensable Particulate Matter Measurements and Issues; *J. Air & Waste Manage. Assoc.* **2000**, *50*, 207-218.
421. Lipkea, W.H.; Johnson, J.H.; Vuk, C.T. The Physical and Chemical Character of Diesel Particulate Emissions–Measurement Techniques and Fundamental Considerations. In *The Measurement and Control of Diesel Particulate Emissions;* Progress in Technology, Number 17; Society of Automotive Engineers: Warrendale, PA, 1979; pp 1-58.
422. Kittelson, D.B.; Dolan, D.F. Diesel Exhaust Aerosols. In *Generation of Aerosols and Facilities for Exposure Experiments;* Willeke, K., Ed.; Ann Arbor Science: Ann Arbor, MI, 1980; pp 337-359.
423. Kittelson, D.B.; Watts, F.W., Jr.; Arnold, M. *Review of Diesel Particulate Matter Sampling Methods: Supplemental Report #2, Aerosol Dynamics, Laboratory, and On-Road Studies*; University of Minnesota, Department of Mechanical Engineering: 1998.
424. Kittelson, D.B.; Arnold, M.; Watts, W.F. *Review of Diesel Particulate Matter Sampling Methods—Final Report*; University of Minnesota; Center for Diesel Research: 1998.
425. Vogt, R.; Scheer, V.; Maricq, M.M. Nanoparticle Artifacts: Comparison of Tailpipe Dilution Tunnel Measurements of Vehicle PM. Presented at International ETH-Workshop on Nanoparticle Measurement, Zurich, Switzerland; ETH Zurich Labortorium für Festkorperphysik: 1999.
426. Shi, J.P.; Harrison, R.M. Investigation of Ultrafine Particle Formation during Diesel Exhaust Dilution; *Environ. Sci. Technol.* **1999**, *33(21)*, 3730-3736.
427. Khalek, I.A. Nanoparticle Growth during Dilution and Cooling of Diesel Exhaust: Experimental Investigation and Theoretical Assessment. Presented at International ETH-Workshop on Nanoparticle Measurement, Zurich, Switzerland; ETH Zurich Labortorium für Festkorperphysik: 1999.
428. Pagán, J. *Study of Particle Size Distributions Emitted by a Diesel Engine*; 1999-01-1141; Society of Automotive Engineers: Warrendale, PA, 1999.
429. Abdul-Khalek, I.; Kittelson, D.; Brear, F. *The Influence of Dilution Conditions on Diesel Exhaust Particle Size Distribution Measurements*; 1999-01-1142; Society of Automotive Engineers: Warrendale, PA, 1999.
430. Chen, J.-P. Particle Nucleation by Recondensation in Combustion Exhausts; *Geophys. Res. Lett.* **1999**, *26(15)*, 2403-2406.
431. Harris, D.B.; King, F.G.J.; Brown, J.E. Development of On-Road Emission Factors for Heavy-Duty Diesel Vehicles Using a Continuous Sampling System. In *The Emissions Inventory: Programs and Progress;* Publication No. VIP-56; Air and Waste Management Association: Pittsburgh, PA, 2000; pp 290-308.
432. Brown, J.E.; Clayton, M.J.; Harris, D.B. Comparison of Particle Size Distribution of Heavy-Duty Diesel Exhaust Using a Dilution Tailpipe Sampler and an In-Plume Sampler On-Road Operation; *J. Air & Waste Manage. Assoc.* **2000**, *50*, 1407-1416.
433. Maricq, M.M.; Chase, R.E.; Podsiadlik, D.H.; Vogt, R. *Vehicle Exhaust Particle Size Distributions: A Comparison of Tailpipe and Dilution Tunnel Measurements*; 1999-01-1461; Society of Automotive Engineers: Warrendale, PA, 1999.
434. Saxena, P.; Cass, G. Designing Atmospheric Experiments to Enable Estimation of Source-Receptor Relationships for Fine Particles. In *Atmospheric Observations: Helping Build the Scientific Basis for Decisions Related to Airborne Particulate Matter;* PM Measurements Research Workshop, Chapel Hill, North Carolina; Health Effects Institute: Cambridge, MA, 1998.
435. Schauer, J.J.; Rogge, W.F.; Hildemann, L.M.; Mazurek, M.A.; Cass, G.R.; Simoneit, B.R.T. Source Apportionment of Airborne Particulate Matter Using Organic Compounds; *Atmos. Environ.* **1996**, *30*, 3837-3855.
436. Meuzelaar, H.; Arnold, N.; Jarman, W. Paso del Norte Air Research Program, Scoping Study, Interim Report; Southwest Center for Environmental Policy and Research. http://www.scerp.org/, accessed 1999.
437. Burtscher, H. Measurement and Characteristics of Combustion Aerosols with Special Consideration of Photoelectric Charging and Charging by Flame Ions; *J. Aerosol Sci.* **1992**, *23(6)*, 549-595.
438. Burtscher, H.; Siegmann, H.C. Monitoring PAH-Emissions from Combustion Processes by Photoelectric Charging; *Combust. Sci. Technol.* **1994**, *101*, 327-332.

439. Burtscher, H.; Schmidt-Orr, A.; Siegmann, H.C. Monitoring Particulate Emissions from Combustion by Photoemission; *J. Aerosol Sci.* **1988**, *18*, 125.
440. Palmer, G.R. Ambient Air Monitoring of Fine Particulate Matter at Hill Air Force Base, UT and the Influence of Mobile Sources. M.S. Thesis, University of Utah, Salt Lake City, UT, 1999.
441. Chow, J.C.; Watson, J.G.; Pritchett, L.C.; Pierson, W.R.; Frazier, C.A.; Purcell, R.G. The DRI Thermal/Optical Reflectance Carbon Analysis System: Description, Evaluation and Application in U.S. Air Quality Studies; *Atmos. Environ.* **1993**, *27A(8)*, 1185-1201.
442. Chow, J.C.; Watson, J.G.; Crow, D.; Lowenthal, D.H.; Merrifield, T. Comparison of IMPROVE and NIOSH Carbon Measurements; *Aerosol Sci. Technol.,* in press.
443. Funkenbusch, E.F.; Leddy, D.G.; Johnson, J.H. The Characterization of the Soluble Organic Fraction of Diesel Particulate Matter. In *Measurement and Control of Diesel Particulates;* Society of Automotive Engineers: Warrendale, PA, 1979; pp 123-143.
444. Fraser, M.P.; Cass, G.R.; Bernd, R.T.S. Gas-Phase and Particle Phase Organic Compounds Emitted from Motor Vehicle Traffic in a Los Angeles Roadway Tunnel; *Environ. Sci. Technol.* **1998**, *32(14)*, 2051-2060.
445. Hildemann, L.M.; Mazurek, M.A.; Cass, G.R. Quantitative Characterization of Urban Sources of Organic Aerosol by High-Resolution Gas Chromatography; *Environ. Sci. Technol.* **1991**, *25(7)*, 1311-1325.
446. Arnott, W.P.; Moosmüller, H.; Rogers, C.F.; Jin, T.; Bruch, R. Photoacoustic Spectrometer for Measuring Light Absorption by Aerosol: Instrument Description; *Atmos. Environ.* **1999**, *33*, 2845-2852.
447. Moosmüller, H.; Arnott, W.P.; Rogers, C.F.; Chow, J.C.; Frazier, C.A.; Sherman, L.E.; Dietrich, D.L. Photoacoustic and Filter Measurements Related to Aerosol Light Absorption during the Northern Front Range Air Quality Study (Colorado 1996/1997); *J. Geophys. Res.* **1998**, *103(D21)*, 28,149-28,157.
448. Arnott, W.P.; Rogers, C.F.; Sagebiel, J.; Zielinski, B.; Fujita, E.; Lighty, J.S.; Sarofim, A.F.; Griffin, J.B. Evaluation of Five Instruments for the Real-Time Measurement of Diesel Particulate Emissions. In *10th CRC On-Road Vehicle Emissions Workshop, San Diego, CA*; Coordinating Research Council, Inc.: Atlanta, GA, 2000.
449. Hopke, P.; Casuccio, G.S. Scanning Electron Microscopy. In *Receptor Modeling for Air Quality Management;* Hopke, P.K., Ed.; Elsevier: New York, 1991; pp 149-208.
450. Spurny, K.R. Review of Applications. In *Physical and Chemical Characterization of Individual Airborne Particles*; Spurny, K.R., Ed.; Ellis Horwood Series in Analytical Chemistry; Wiley: New York, 1986.
451. Kim, D.S.; Hopke, P.K.; Casuccio, G.S.; Lee, R.J.; Miller, S.E.; Sverdrup, G.M.; Garber, R.W. Comparison of Particles Taken from the ESP and Plume of a Coal-Fired Power Plant with Background Aerosol Particles; *Atmos. Environ.* **1989**, *23(1)*, 81-84.
452. Watt, J. Automated Characterization of Individual Carbonaceous Fly Ash Particles by Computer-Controlled Scanning Electron Microscopy: Analytical Methods and Critical Review of Alternative Techniques; *Water, Air, Soil Pollut.* **1998**, *106*, 309-327.
453. Webber, J.S.; Dutkiewicz, V.A.; Husien, L. Identification of Submicrometer Coal Fly Ash in a High-Sulfate Episode at Whiteface Mountain, New York; *Atmos. Environ.* **1985**, *19*, 285-292.
454. Eatough, D.J.; Eatough, M.; Lamb, J.D.; Lewis, L.J.; Lewis, E.A.; Eatough, N.L.; Missen, R. Apportionment of Sulfur Oxides at Canyonlands during the Winter of 1990—I. Study Design and Particulate Chemical Composition; *Atmos. Environ.* **1996**, *2*, 269-281.
455. Anderson, J.R.; Buseck, P.R. 5.3 Special Examples of Applications of Minerology and Geochemistry to Environmental Problems. In *Advanced Minerology*; Marfunin, A.S., Ed.; Springer-Verlag: Berlin, 1998; Vol. 3; pp 300-313.
456. Buseck, P.R.; Anderson, J.R. Analysis of Individual Airborne Mineral Particles. In *Advanced Minerology*; Marfunin, A.S., Ed.; Springer-Verlag: Berlin, 1998; Vol. 3; pp 292-299.
457. Suess, D.T.; Prather, K.A. Mass Spectroscopy of Aerosols; *Chem. Rev.* **1999**, *99*, 3007-3095.
458. Hughes, L.S.; Allen, J.O.; Kleeman, M.J.; Johnson, R.J.; Cass, G.R.; Gross, D.S.; Gard, E.E.; Gälli, M.E.; Morrical, B.D.; Ferguson, D.P.; Dienes, T.; Noble, C.A.; Liu, D.-Y.; Silva, P.J.; Prather, K.A. Size and Composition Distribution of Atmospheric Particles in Southern California; *Environ. Sci. Technol.* **1999**, *33(20)*, 3506-3515.
459. Reilly, P.T.; Gieray, R.A.; Whitten, W.B.; Ramsey, J.M. Real-Time Characterization of the Organic Composition and Size of Individual Diesel Engine Smoke Particles; *Environ. Sci. Technol.* **1998**, *32*, 2672-2679.
460. Gard, E.; Mayer, J.E.; Morrical, B.D.; Dienes, T.; Fergenson, D.P.; Prather, K.A. *Anal. Chem.* **1997**, *69*, 4083-4091.
461. Allen, J.O.; Fergenson, D.P.; Gard, E.E.; Hughes, L.S.; Morrical, B.D.; Kleeman, M.J.; Gross, D.S.; Gälli, M.E.; Prather, K.A.; Cass, G.R. Particle Detection Efficiencies of Aerosol Time of Flight Mass Spectrometers under Ambient Sampling Conditions; *Environ. Sci. Technol.* **2000**, *34(1)*, 211-217.
462. Serita, F.; Kyono, H.; Seki, Y. Pulmonary Clearance and Lesions in Rats after a Single Inhalation Dose of Ultrafine Metallic Nickel at Dose Levels Comparable to the Threshold Limit Value; *Ind. Health* **1999**, *37(4)*, 353-363.
463. Snow, J. *On the Mode of Communication of Cholera*. Reprinted in Snow on Cholera: A Reprint of Two Papers, 1965; Hafner Publ. Co.: New York, 1855.
464. Gertsman, B.B. *Epidemiology Kept Simple: An Introduction to Modern and Classical Epidemiology*; Wiley-LISS: New York, 1998.

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Particle-Size Distributions and Heavy Metal Partitioning in Emission Gas from Different Coal-Fired Power Plants

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ABSTRACT

This study investigated the emission characteristics of particulate matter (PM) and several heavy metals from different Korean coal-fired utility boilers. Emission measurements examined PM and gas emission concentrations, particle size distributions (PSDs), the partitioning of heavy metals, and the concentration of ultrafine particles. The facilities examined included two bituminous coal-fired power plants (pulverized coal combustors) and one anthracite coal-fired power plant (circulating fluidized bed combustor). Measurements were made at locations before the systems' air pollution control devices (APCDs). The PSDs prior to PM control were bimodal from all facilities. The mass ratios of the fine particle modes to larger particle modes were dependent on the ash content of the fuel and the boiler type. Additionally, the overall PM concentration before the APCDs correlates well with the ash content of the coals. Thermodynamic equilibrium predictions indicate that the metal speciation (and volatility) depends not only on the halogen content of the fuel, but also on the localized stoichiometric ratio of combustion.

Key words: heavy metals; particulate matter; coal-fired boiler; particle size distribution; metal partitioning; particle formation mechanisms

INTRODUCTION

In 1997, the U.S. EPA added a standard for ambient concentrations of PM-2.5 (PM smaller than 2.5 μm in aerodynamic diameter). This change was based on health studies indicating PM-2.5 to be hazardous to the human respiratory system (Bachmann *et al.*, 1996; U.S. EPA, 1996a; Wilson and Spengler, 1996; Wolff, 1996; Federal Register, 1997). Coal combustion represents one source of the particles, and information regarding these emis-

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sions, including particle size distributions (PSDs), metal partitioning between different particle sizes, and the relative contribution of ultrafine particles, are likely important parameters that effect emission control strategy and the toxicity of the resulting PM emissions.

PM can be formed via the transformation of ash forming material in the fuel and wastes to form large particles, and through vaporization mechanism to form (ultra-) fine particles through nucleation, coagulation, and condensation processes. The vaporized inorganic matter, including heavy metals, within the high-temperature combustion region undergoes homogeneous condensation to generate particle nuclei. The generated nuclei coagulate with each other by driving forces such as Brownian motion and/or turbulent shear and differential sedimentation. Also, the vaporized inorganic matter may condense on the surfaces of preexisting particles driven by saturation partial pressures. These mechanisms result in distinct submicron mode in the PSD. Linak (2002) showed a trimodal PSD in the coal combustion process with particle size of the finest mode under 0.1 μm.

There have been many research studies investigating the emission characteristics of hazardous air pollutants from fuel combustion, especially bituminous coal combustion. Linak and Wendt (1994) reviewed and investigated the metal transformation mechanisms during bituminous coal combustion. They suggest that metals may become enriched on particles of different size based on different particle formation mechanisms. Helble (2000) predicts metal enrichment to be depended on metal volatility on particles.

To understand the factors affecting ash vaporization, particle formation, and metal partitioning, thermodynamic equilibrium calculations, using the principal of minimizing the total Gibbs free energy of the system were performed. These calculations can be useful to identify the likely dominant species of each element (including heavy metals) in a multicomponent and multiphase system such as combustion. It can also be useful to examine behavior within locally reducing regions around individual coal particles.

In this study, the emission characteristics of three commercial coal-fired boilers were investigated with respect to the PSDs and heavy metal partitioning. This experimental behavior is interpreted through the use of a thermodynamic equilibrium calculation code to predict relative elemental volatilities and stable species and particle formation mechanisms.

FACILITIES AND EXPERIMENTAL METHODS

Facilities tested

Three different types of commercial coal fired power plants were investigated. Two of these units used bituminous coals and the third fired an anthracite coal. The two bituminous pulverized coal-fired power plants are of similar design. Their features are summarized in Table 1. These facilities, Bit1 and Bit2, choose their fuels based on ash contents and heat capacities. The third facility, Ant, was a smaller circulating fluidized bed boiler burning anthracite coal. The properties of the three fuels are summarized in Table 2.

Experimental methods

Sampling of particulate matter. The sampling method for total particulate matter (TPM) used in the experiment was an isokinetic sampling method similar to the U.S. EPA Method 5 (U.S. EPA Method, 2000). However, our approach used a thimble type filter, while Method 5 uses circular paper-type filter. An atmospheric pressure cascade impactor (Anderson Instrument Co. Ltd., Atlanta,

Table 1. Summary of tested facilities.

ID	*Capacity (ton steam/h)*	*Fuel*	*Furnace type*	*Air pollution control devices*
Ant	691	Anthracite coal	Circulating fluidized bed, in bed DeSOx system	Electrostatic precipitator
Bit1	1,720	Bituminous coal	Pulverized coal, Tangential corner firing, low NOx burner, once-through type boiler	Electrostatic precipitator, DeSOx (spray tower)
Bit2	1,720	Bituminous coal	Pulverized coal, Tangential corner firing, low NOx burner, once-through type boiler	Electrostatic precipitator, DeSOx (spray tower)

Table 2. Properties of fuels for three coal fired power plants.

		Anthracite coal	*Bituminous coal 1*	*Bituminous coal 2*
Low heating value, kg/kcal		4,673	6,279	6,262
Proximate	Moisture	4.5	3.7	9.3
Analysis	Fixed carbon	54.5	57.5	56.0
wt. %	Volatile	8.9	29.4	27.2
	Ash	32.2	9.3	7.0
	C	64.4	75.5	75.3
	H	1.2	4.4	3.8
Elemental	O	1.7	13.5	9.3
Analysis, wt. %	N	0.5	1.1	1.4
	S	0.4	0.3	0.5
	Cl	0.07	0.01	0.01
	As	3.0	1.9	<0.3
	Cd	<0.2	<0.2	<0.2
	Cr	4.6	7.5	4.7
Heavy metals,	Cu	27.2	<22.6	<22.6
mg/kg	Ni	12.3	18.5	18.1
	Pb	20.1	<16.8	<16.8
	Zn	27.3	33.4	36.1
	Mn	88.0	88.1	29.1
	Mg	980	525	209

GA, Mark III Stack Sampler) was used for PM-10. PM-2.5 determinations, and PSD analysis (U.S. EPA Method, 1997). The size distributions were calculated using WinCIDRS software (WinCIDRS, Ver. 4.0 Operations and Data Analysis System for Internal Particle Sizing Device), and were based on mass weights determined on each stage of impactor. The sampling points of each facility were the inlet of the electrostatic precipitator (ESP). The locations were after the heat exchangers with average sampling temperatures of 123, 125, and 145 °C for Bit 1, Bit2 and Ant, respectively.

Analysis of heavy metals and inorganic components in particulate matter. The U.S. EPA test method for evaluating solid waste, SW-846 3050B (U.S. EPA Method, 1986), was used for digesting the filters and collected PM for the total filters as well as the PM and substrates of each impactor stage. These extracts were examined for heavy metal and inorganic matter analysis by ICP/MS (Varian Co. Ltd., Palo Alto, CA, Ultra mass 700).

Table 3. Concentration of particulate matters at APCD inlet and their ratios.

	Ant	*Bit1*	*Bit2*
TPM, mg/Sm^3	25,750	12,580	20,798
PM-10, mg/Sm^3	13,043	2,481	1,208
PM-2.5, mg/Sm^3	7,790	274	250
PM-10/TPM	0.51	0.20	0.06
PM-2.5/TPM	0.30	0.02	0.01
PM-2.5/TPM	0.60	0.11	0.21

RESULTS AND DISCUSSIONS

Emission characteristics of PM

The PM concentrations at the inlet of each facility's APCDs are shown in Table 3. The emission concentrations of the PM were strongly related to the ash content in fuel. As showed in Fig. 1, the uncontrolled emission

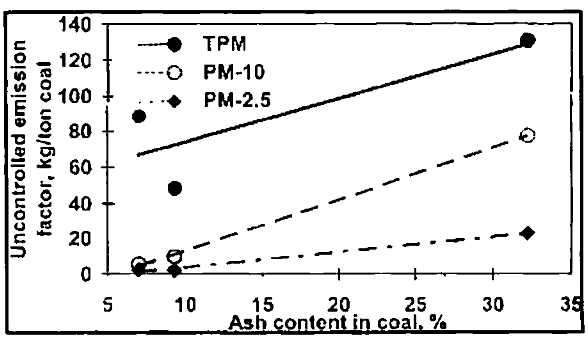

Figure 1. Relationships between uncontrolled emission factors and different ash content in coal.

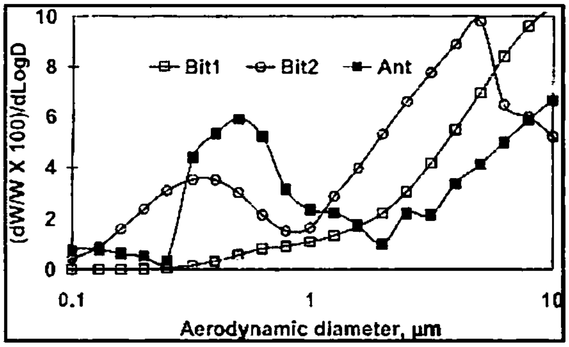

Figure 2. Particle size distribution of PM-10 at the inlet of APCD.

factor, which normalized the amount of pollutant emitted from the furnace by the amount of fuel combusted, increased with the ash content in coal (U.S. EPA, 1995). A detailed discussion on the development of emission factors for these units was described in a previous paper (Yoo *et al.*, 2002). Additionally, as showed in Table 3, the ratio of the fine particles with respect to the coarse particles from the anthracite coal fired boiler are higher than the same ration for the bituminous coal fired boilers. The PSDs of PM-10 from each facility showed bimodal distributions as presented in Fig. 2. The PSD of the anthracite facility showed a higher portion of submicron particles than the bituminous coal fired boilers and showed a distinct mode near 0.1 μm. Therefore, it is assumed that a portion of the inorganic matter, which are

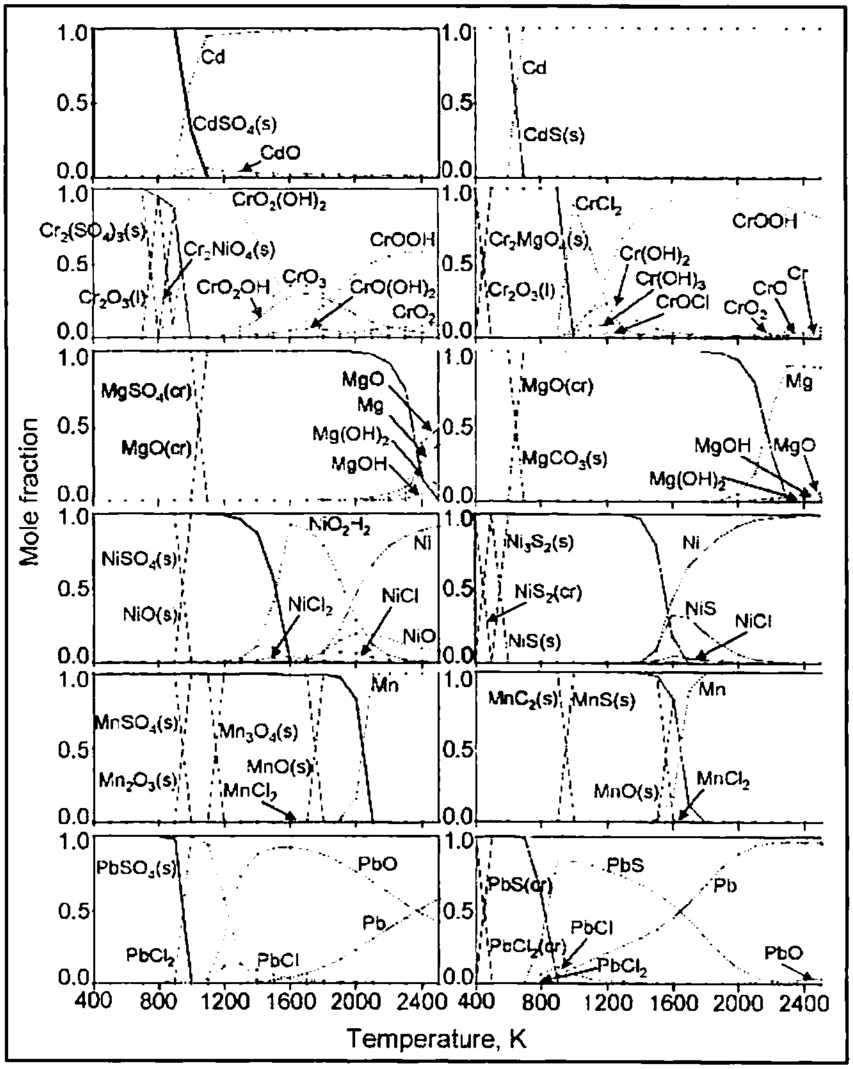

Figure 3. Equilibrium predictions for metal species from anthracite coal-fired boiler using the CEA code.

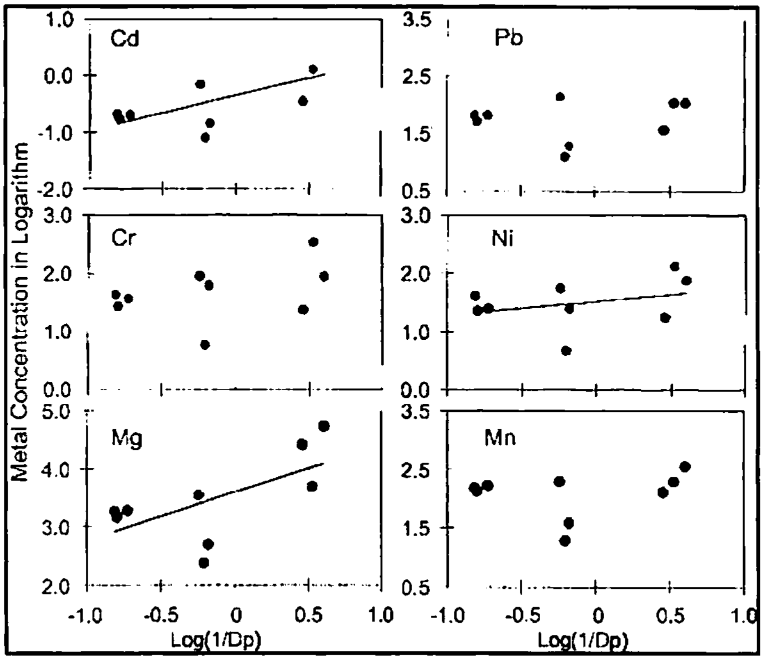

Figure 4. Relationships between particle size and metal concentration for anthracite coal-fired boiler (D_p = μm, metal concentration = μg of metal/g of ash).

main components of ash, were vaporized and formed fine particles by the generation mechanism discussed previously.

Emission characteristics of heavy metals

In a previous paper (Yoo *et al.*, 2002), the emission characteristics of heavy metals were described in detail using a generalized form (i.e., emission factors) to predict emission per unit of heat energy. The emission factor calculation, which was based on the metal content in fuel, has been used in AP-42 U.S. EPA (1995). Using these calculated emission factors, some heavy metals including arsenic, manganese, nickel, and magnesium showed good correlation with their initial concentrations.

Estimation of metal species in the flue gas

In the combustion environment, a portion of the inorganic matter (include heavy metals) were vaporized. The extent of this vaporization is influenced by the temperature, composition, and environment that the ash components experience. Following vaporization, the ash species nucleate, condense, and coagulate following principles of aerosol mechanics. Thus, the chemistry and speciation of heavy metals within the combustion environment is very important to understand of particle generation mechanisms, especially for the fine particles. Additionally, while the overall stoichiometry is always designed to be fuel lean, the microenvironments surrounding and inside a burning coal particle is reducing. Thus, it is important to examine reducing as well as oxidative conditions and its affect on metal vaporization.

The computer simulation code, Chemical Equilibrium Analysis (CEA; Mc Bride *et al.*, 1993), was used to predict the chemical species in the combustion environment with thermochemical data which had been used in Linak *et al.* (1999). The fuels' proximate analyses and heavy metal contents, presented in Table 2, were used in the CEA calculations. Scenarios examining stoichiometric ratios of 0.6 and 1.2 were included to simulate reduction and oxidation conditions, respectively. Reducing conditions are intended to examine stages of early char combustion when the coal particle surface is experiencing an oxidative environment but oxygen has not yet penetrated into its interior. Metals experience this environment may vaporize under reducing conditions (Yan *et al.*, 1999).

Figure 3 presents the results of equilibrium calculations for the anthracite coal-fired boiler. Results for the other bituminous coal-fired boilers showed similar trends but are not presented. The CEA calculations predict element speciation and including the fraction of condensed phase species for the heavy metals of interest as a func-

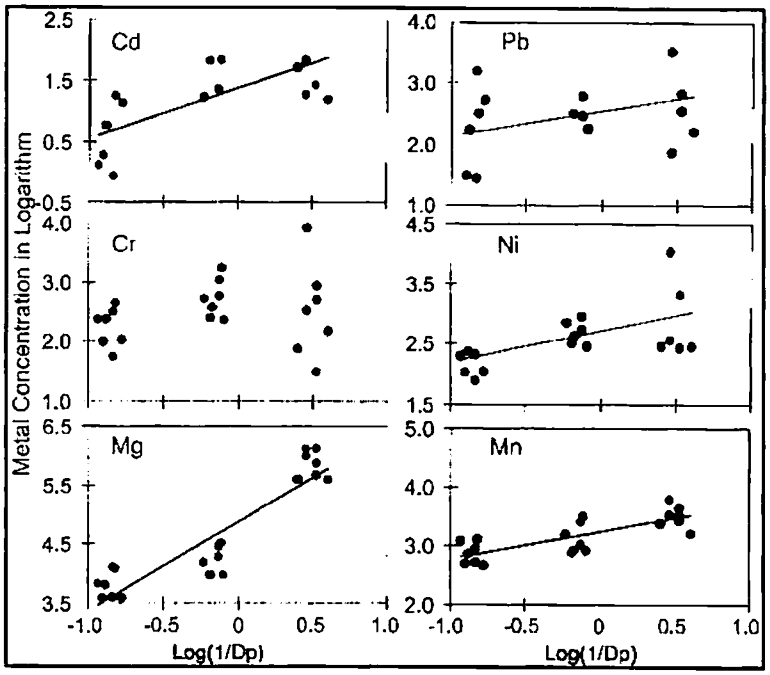

Figure 5. Relationships between particle size and metal concentration for bituminous coal-fired boilers.

tion of temperature. In general, reducing environments enhance the volatility (approximately 200–300 K) compared to oxidation conditions for cadmium, magnesium, and manganese. In contrast, reducing conditions caused very little change in volatility for chromium and nickel, although their predicted speciation is very different between oxidative and reducing environments. These results are consistent with predictions made by Frandsen *et al.* (1994).

Metal partitioning

There have been various investigations, which studied metal enrichment in fly ash samples with the intent of investigating mechanisms controlling particle growth. In this study, the concentration of each metal from each impactor stage was analyzed. The following equation was applied to find a correlation between heavy metal concentration and particle size.

$$\mathrm{Log}(W_i) = m\mathrm{Log}(1/D_p) + b$$

where W_i is the concentration of species i in the particle size range, μg/g; D_p is the representative diameter, μm; and m, b is the experimentally derived slope and intercept.

By plotting $\mathrm{Log}(W_i)$ vs. $\mathrm{Log}(1/D_p)$, a relationship between metal concentration and particles size can be made. The relative slope (m) can be related mathematically to the relative importance of film condensation ($1/D_p^2$ dependence, $m = 2$) and reactive scavenging ($1/D_p$ dependence, $m = 1$) (Linak and Wendt, 1994).

Table 4. Characteristics value for experimental equations of heavy metals in coal fired boilers.

Anthracite coal fired boiler		*Bituminous coal fired boiler*	
Species	*Slope (m)*	*Species*	*Slope (m)*
		Cd	0.82
Cd	0.62	Pb	0.40
Ni	0.24	Ni	0.52
Mg	0.83	Mg	1.50
		Mn	0.46

Figures 4 and Fig. 5 show relationships between particle size and metal concentration for the anthracite and bituminous coal-fired boilers, respectively. The slopes of cadmium and magnesium are close to unity, while the other metals were generally less enriched in the small particle sizes. Table 4 summarizes these slopes for several selected metals, determined by a least mean square method. The results of this study suggest that the mechanism of enrichment for cadmium and magnesium may be pore diffusion controlled diffusion and reactive scavenging on existed particles, respectively (Linak and Wendt, 1993; Linak *et al.*, 1994). This is the case for magnesium, even though the temperature of condensed phase, shown in Fig. 3, was higher than other metals. This may be because of the higher content of magnesium in these coals; the magnesium vaporizes very quickly in the very first stages of combustion.

For the other metals examined, the story is much less clear, and the dominant mechanism of condensation is likely not related to a single mechanism, but to a complex set of mechanisms which occur simultaneously. The thermodynamic prediction indicates that manganese, nickel, and chromium interact with other ash constituent such as silicon, iron, and aluminum (Yan *et al.*, 2001).

CONCLUSIONS

Measurements at three different commercial scale coal fired boilers investigated the characteristics of inorganic PM. Analysis of the PSDs, gaseous inorganic matter, and heavy metals were performed and a computer simulation code was used to predict stable inorganic species within the combustion environment. Several conclusions were derived from the experiment as follows.

1. The emission characteristics of PM depended on the ash content in the fuel. The finer mode in the PSD was clearly related to the ash content of the fuel and relationships of uncontrolled PM emission factor with ash content in the fuel showed more linearity with respect to the fine particles. It is assumed that the ash components in the fuel contributed to the fine particle formation through a mechanism of vaporization, nucleation, condensation, and coagulation.
2. The heavy metals were generally enriched in the finer particles. This was confirmed by computational thermodynamic code. However, magnesium compounds were enriched in the fine particles, even though the calculations indicated that it was not particularly volatile. The halogen content in the fuel was also an important factor for metal partitioning, as it promotes metal vaporization especially under reducing conditions.

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REFERENCES

BACHMANN, J.D., DAMBERG, R.J., CALDWELL, J.C., EDWARDS, C., and KOMAN, P.D. (1996). *Review of the National Ambient Air Quality Standards for Particulate Matter: Policy Assessment of Scientific and Technical Information*, EPA-452/R-96-013 (NTIS PB97-115406). Research Triangle Park, NC: Office of Air Quality Planning and Standards.

FEDERAL REGISTER. (1997). 62 FR 38652, July 18. Author.

FRANDSEN, F., DAM-JOHANSEN, K., and RASMUSSEN P. (1994) Trace elements from combustion and gasification of coal—An equilibrium approach. *Prog. Energy Combust. Sci.* 20, 115.

HELBLE, J.J. (2000). A model for the air emissions of trace metallic elements from coal combustors equipped with electrostatic precipitators. *Fuel Processing Technology* 63, 125–147.

LINAK, W.P. (2002). Fine and ultra-fine ash particles from pulverized coal combustion. *Trace Element Workshop 2002*, Yokohama, Japan.

LINAK, W.P., and WENDT, J.O.L. (1993). Toxic metal emission from incineration: Mechanism and control. *Prog. Energy Combust. Sci.* 19, 145.

LINAK, W.P., and WENDT, J.O.L. (1994). Trace metal transformation mechanisms during coal combustion. *Fuel Process. Technol.* 39, 173.

LINAK, W.P., SRIVASTAVA R.K., and WENDT J.O.L. (1994). Metal aerosol formation in a laboratory swirl flame incinerator. *Combust. Sci. Tech.* 101, 7.

LINAK, W.P., MILLER C.A., and WENDT, J.O.L. (1999). Fine particle emissions from residual fuel oil combustion: Characterization and mechanisms of formation. In *5th International Conference on Technologies and Combustion for a Clean Environment*, July 12–15, 1999, Lisbon, Portugal.

McBRIDE, B.J., GORDON, S., and RENE, M.A. (1993). Coefficients for calculating thermodynamic and transport properties of individual species. *NASA Technical Memorandum* 4513.

U.S. EPA METHOD. (1986). *Test Method for Evaluating Solid Waste, SW-846-3050B Acid Digestion of Sediments, Sludges, and Soils*, 3rd edition. Washington, D.C.:Author.

U.S. EPA. (1995). *Compilation of Air Pollutant Emission Factors*. 5th ed., *vol. I: Stationary Point and Area Sources*. Washington, D.C.:Author.

U.S. EPA. (1996a). *National Ambient Air Quality Standards for Particulate Matter: proposed decision*, 40 CFR, Part 50. Washington, D.C.:Author.

U.S. EPA METHOD. (1997). *EMTIC TM-201A—Determination of PM-10 Emissions*. Washington, D.C.:Author.

U.S. EPA METHOD. (2000). *EMTIC TM-5, Determination of Particulate Matter Emissions from Stationary Sources*. Washington, D.C.: Author.

WILSON, R., and SPENGLER, J.D. (1996). *Particles in Our Air: Concentrations and Health Effects*. Cambridge, MA: Harvard University Press.

WOLFF, G.T. (1996). *Closure by the Clean Air Scientific Advisory Committee (CASAC) on the Staff Paper for Particulate Matter*, EPA-SAB-CASAC-LTR-96-008. Washington, DC: U.S. EPA, Science Advisory Board.

YAN, R., GAUTHIER, D., FLAMANT, G., and BADIE, J.M. (1999). Thermodynamic study of the behavior of minor coal elements and their affinities to sulfur during coal combustion. *Fuel* 78, 1817.

YAN, R., GAUTHIER, D., and FLAMANT, G. (2001). Partitioning of trace elements in the flue gas from coal combustion. *Combust. Flame* 125, 942.

YOO, J.I., LEE, S.J., KIM, K.H., JANG, H.N., SEOK, J.H., SEO, Y.C., SEOK, K.S., HONG, J.H, and KIM, B.H. (2002). Emission factors and emission characteristics of particulate matters and heavy metals from several thermal sources. In 22th *International Conference on Incineration and Thermal Treatment Technologies*, May 13–17, 2002, New Orleans.

Estimating Trace Element Emissions Using USGS Coal Data

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Abstract

The USGS trace element data for Pittsburgh seam coal samples from Pennsylvania were examined to determine correlations of ash and sulfur contents with trace element content. The data indicated moderate to strong correlations occur for the various trace element concentrations of the coals, and the contents of ash and sulfur. CONSOL commercial coal data for the Pittsburgh seam were used to compare the estimated concentrations with coal data at different ash levels. When the USGS data base is analyzed according to the statistical procedures applied here, the predicted values using the developed correlations were considerably closer to the values from the CONSOL data base (from Pennsylvania Pittsburgh seam coals) for most trace elements compared to the EPA estimates (based on state-wide averages). The predicted concentrations for most trace elements were within 60% of the measured product coal concentrations. The state-wide average developed by EPA differed from actual product concentrations by 200% to 400%.[1] Subsequent use of the USGS data base without careful analysis and

treatment of the data will produce misleading estimates for trace element emissions from coal-burning utilities.

Statement of Implications

Using the USGS trace element data base to estimate trace element emissions for coal-fired electric power plants requires attention to the inherent statistical problems. Careful attention must be given to constructing estimates of trace element concentrations that take into account the spatial arrangement of the samples.

Spatially resolved estimates differed by as much as 70% from naive equally weighted averages. Relationships between the trace elements and ash, and sulfur were developed and used to assess the likely reductions in concentration due to coal cleaning. These relationships produce reasonably good estimates of the actual reduction for two CONSOL steam coals in the Pittsburgh seam. Finally, a sampling scheme is suggested for producing national trace element emissions estimates.

Estimation Concerns

The quality of estimates of well-defined regional (global) parameters from point sample data depends on how the sample data were collected. Here quality is measured in terms of accuracy (lack of bias) and precision. Ideally, samples are collected with the estimation of a specific parameter in mind. For example, one could estimate the mercury content of all coal existing in a specific seam regardless of whether it will actually be mined. Samples should ideally be arranged on a uniform systematic grid throughout an area with well-defined borders. Alternatively, one could estimate only coal that will be mined in a given time period. Detailed information on mining activity would be required for this case. Here an estimate should be based on samples only in or near the areas to be mined. (If the grid extends over the entire seam, samples in areas to-be-mined would receive higher weights than samples which are nearby but not directly in an area to-be-mined.)

The USGS coal quality samples were not collected with the thought of estimating any particular parameter. Neither were the samples located on a uniform systematic grid throughout a given seam. The samples cannot even be considered to be uniformly randomly located throughout a given seam. Instead, the samples are irregularly located in clusters. A simple, unweighted average of such samples either represents an estimate of nothing in particular, or a likely highly biased estimate of any particular parameter.

The bottom line is that careful attention must be given to the production of parameter estimates based on the USGS coal quality data base. This paper discusses a few considerations and illustrates several approaches. While the estimates produced are not definitive, they do illustrate the likely improvements that are possible with a little thought and perseverance.

Background

The USGS coal trace element data base is the single largest compilation of trace element data which provides extensive information for virtually all coal seams in the country. This data base has been used by several researchers to estimate the quantity of potential trace element emissions from coal-fired power plants. However, there are several inherent problems when one considers application of the data base to estimate commercial steam coal product trace element concentrations and subsequent power plant emissions.

First, the USGS data base represents trace element concentrations of various channel and core samples collected without a comprehensive sampling strategy appropriate for estimating reserves. In ordinary sampling, a probabilistic scheme is used to tie the sampling to a target population. In spatial sampling, ideally an exhaustive systematic grid of samples is used to ensure unbiased estimates of the deposit characteristics.

The data base also represents the coal deposit prior to any physical cleaning (ash removal). Since 75% - 80% of the coal east of the Mississippi River is cleaned, the USGS coal data do not represent commercial coal products used by power plants. Also, most of the mines from which these samples were collected are closed. In addition, the precision or accuracy of the analytical methods employed in determining the trace element concentrations of these samples is unknown. Therefore, it is necessary to analyze the USGS data carefully and develop factors that would relate the USGS trace element concentrations to currently used commercial coal supplies.

In the present study, USGS trace element data for the Pittsburgh seam coals in Pennsylvania were examined and compared with actual CONSOL steam coal analyses. A good correlation was developed which is described in this report.

Description of the USGS Data Set

The data analyzed in this report consisted of analyses of 71 samples from the USGS coal trace element data base for the Pittsburgh seam (No. 8 coal bed) in Pennsylvania. These samples are almost all channel samples of varying thicknesses and depths obtained at sites accessible to the USGS. The variables considered for the analyses included Btu, ash, sulfur, arsenic, beryllium, cadmium, chlorine, cobalt, bromine, chromium, fluorine, mercury, manganese, molybdenum, nickel, lead, antimony, and selenium concentrations in the coal samples.

Of the 71 original samples, there were 31 unique locations with multiple samples at varying depths in the seam at each location. The 31 unique locations are shown in Figure 1. The spatial locations of the samples in no way represent a random sample of locations throughout the seam, nor are the samples optimally arranged on a uniform systematic grid. In fact, the samples tend to be clustered with the largest cluster in the northwestern part of the geographical area consisting of about 20 samples. At each location, all samples were weight averaged for each parameter using the sample thickness as the weighting factor. Trace element concentrations in parts per million for the 31 locations are shown in Table I.

The symbols A-Z and 1-5 shown in Figure 1 identify the locations of the various samples described in Table I. Note that the concentrations of ash and sulfur are shown to two significant figures (in lb/MM Btu) and that of the trace elements to two significant figures (in ng/Btu). The last column in the table represents total trace element concentrations in ng/Btu for the coals. The minimum, maximum, average, and standard deviation for each of the elements and the element totals are listed at the bottom of the table. A comparison of USGS data with raw and clean coal data[3] for two CONSOL coals (Pennsylvania Pittsburgh seam) is shown in Table II. The measured concentrations for the two CONSOL coals (both raw and clean) are within the minimum and maximum of the USGS data for the elements. However, the simple arithmetic average concentrations of the USGS data differ substantially from the measured values of the CONSOL Pittsburgh coals. The total elemental concentrations for the clean coals are less than half of the USGS averages (as estimated by EPA) for the Pennsylvania Pittsburgh seam coals. Therefore, it appears that the arithmetic averages of the data from any one or several seams can provide substantially misleading estimates for any particular coal within the population used to derive the average.

Analysis of the Unweighted Data

Because the sample locations are highly clustered (Figure 1) and do not represent either a random sample of locations or a systematic grid of locations, summary statistics on the original unadjusted data are not very meaningful. For example, a simple average for coal ash will not tend to be a good estimate of coal ash for the entire seam, because such an estimate will give too much weight to the concentration of samples in the northwestern cluster. The bias in the estimate will be a function of how different the cluster average is from the true seam average. It is relatively simple to decluster the sample data when calculating estimates of seam averages (shown in the next section).

Because of the sparsity of the data (and the fact that the samples only span the northern part of the Pittsburgh seam within Pennsylvania), a simple weighting scheme is not available to help with calculating adjusted correlations and regression functions. Scatterplots illustrating the relationships between ash or sulfur and the various trace elements (those correlating with $r \geq 0.50$) using all 31 locations are shown in Figure 2. A linear fit was used to correlate various trace elements (Cl, Br, F not included) with ash and sulfur. The corresponding correlation coefficients are shown in Table III with correlations at or above $r = 0.5$ shown in bold type. It should be noted that several trace elements do not correlate even this well with either the ash or the sulfur (e.g., antimony and selenium).

Spatial Weighting to Estimate Unbiased Seam Averages

A simple way to decluster samples is to interpolate a closely spaced uniform grid over the area of interest using the polygonal method, triangulation method, or kriging method, and then average the grid.[4] (These methods of interpolation down weight clustered samples when estimating each grid point.) Averaging the grid declusters the global estimate without explicitly calculating weights for each sample that goes into the global estimate (however, weights are calculated for each sample used to estimate each grid point). This effectively down-weights clusters whose individual samples will receive weights which are too high if a simple (equal weights) average is calculated. Ideally, samples should be uniformly distributed over the entire area of interest. When instead, samples are clustered, the more closely-spaced samples tend to be redundant. Giving all samples equal weights then overrepresents the clusters. Similar problems with weighting occur when extrapolation is used to estimate parameters for the seam which lies outside the boundaries of the sample set.

Figure 3 shows shaded maps for each interpolated grid for each trace element shown in Figure 2. Because the area of the interpolated grid roughly approximates the area covered by the Pittsburgh seam in Pennsylvania, the grid averages represent one reasonable way to make concentration estimates for the Pittsburgh seam in Pennsylvania using the USGS data. Ordinary kriging was used. No attempt was made to do a comprehensive geostatistical analysis of the spatial variability as would be required to produce the best possible estimates. Instead, the same arbitrary variogram was specified and used to produce estimates for all parameters in order to illustrate the degree to which the global estimates could differ from naive simple averages.

Table IV compares the kriged grid averages with the simple averages. Twenty-one parameters are shown in Table IV. Using the kriged spatially weighted average as a base, percentage differences for the trace elements ranged from -36% (spatially weighted average exceeds equally weighted average) to +42% (equally weighted average exceeds spatially weighted average). This shows that equally weighted averages can differ substantially from more reasonable spatially weighted averages.

Correlations to Predict Trace Element Concentrations

As mentioned earlier, of 71 original samples there were 31 unique locations with multiple samples at various depths at each location. At each location all samples were weight-averaged for each parameter using sample thickness as the weighing factor. The elements that showed moderate to strong ($r > 0.55$) correlation with ash are beryllium, cadmium, cobalt, chromium, nickel, lead, and selenium. All these elements, except selenium, naturally occur in the inorganic fractions of the coal. The correlations are found in accordance with Finkelman's observations regarding the modes and occurrences of the elements.[5] Therefore, the data was regressed and correlations were developed. Each correlation was checked for goodness of fit, and the residuals were analyzed. The concentrations (Y) of the trace metals (in ng/Btu) as a function of ash content (A) in lb/MM Btu are listed below. The estimated values are then compared with two CONSOL commercial steam coals from the same seam.

Element	Correlation	Coal A		Coal B		EPA
		Estimated	Actual	Estimated	Actual	Estimated
Beryllium	$Y = 32.59 + 2.75\,A$ $r^2 = 0.29$	46	20	50	22	87
Cadmium	$Y = 1.961 + .00164\,A^3$ $r^2 = 0.81$	2	2	2	2	4
Cobalt	$Y = -26.7 + 23.06\,A$ $r^2 = 0.78$	84	64	115	81	280
Chromium	$Y = 67.48 + 68.41\,A$ $r^2 = 0.89$	390	300	490	380	713
Nickel	$Y = 77.98 + 50.37\,A$ $r^2 = 0.59$	320	220	390	220	724
Lead	$Y = -36.7 + 27.722\,A$ $r^2 = 0.74$	96	97	130	130	206
Selenium	$Y = 11.185 + 6.31\,A$ $r^2 = 0.24$	41	36	50	42	178

The elements that showed moderate correlations with sulfur are arsenic and mercury. The data indicated that arsenic and mercury correlated better with total sulfur and pyritic sulfur of the coal, respectively.

Element	Correlation	Coal A		Coal B		EPA
		Estimated	Actual	Estimated	Actual	Estimated
Arsenic	$Y = 110.5 + 85.08\ S^3$ $r^2 = 0.76$	230	200	780	240	1139
Mercury	$\ln Y = 1.85 + 0.77 \ln S_p$ $r^2 = 0.49$	4	3	6	4	10

Trace elements antimony and manganese did not correlate well with either ash or sulfur. The following multiple correlations were made for the two elements as a function of ash, pyritic and organic sulfur forms.

Antimony $Y_{sb} = -12.79 + 0.672\ A - 0.1699\ S_p + 54.728\ S_o$ (1)
$(R^2 = 0.36)$

Manganese $\ln Y_{mn} = 4.796 + 0.8419 \ln A + 0.1676 \ln S_p + 0.7868 \ln S_o$ (2)
$(R^2 = 0.52)$

The total trace element content correlated with both ash and sulfur.

Trace element totals $\ln Y_{total} = 5.9247 + 0.1247 \ln A + 0.0953 \ln S$ (3)
$(R^2 = 0.74)$

	Coal A		Coal B		EPA
Element	Estimated	Actual	Estimated	Actual	Estimated
Antimony	19	21	46	10	67
Manganese	240	350	560	570	834
Totals	1600	1300	2300	1700	4395

The correlations appear to provide better estimates of trace elements for several product coals from the Pittsburgh seam with varying levels of ash and sulfur than the EPA estimates. This appears to agree with one conclusion of the U.S. EPA study[1] in that the trace element correlations with sulfur and ash were stronger when analyzed one seam at a time (or one county at a time) compared to state-wide averages. Therefore, the estimates for most elements using the above correlations are much closer to the measured concentrations compared to EPA's state-wide average estimates for the Pittsburgh seam coals in Pennsylvania. In addition, since the ash and sulfur content of most commercial steam coals (partly or fully cleaned coals) fall within the range of the data base, the correlations can be used to predict the trace element removals during coal cleaning as well.

Estimating Total Emissions

Many factors besides the coal source are involved when estimating the total emissions of trace elements from a power plant. Yet the above analysis shows how easy it is to introduce a substantial bias just in estimating the average amount of trace elements in coals from a particular state. Unlike random errors, bias does not become negligible as the number of samples increases. In the same way, a substantial bias in an estimate of the total national emissions could result even if individual estimates are produced for every single power plant in the country. Rather than devote excessive time and resources to producing estimates for all plants, a statistically designed sampling plan is suggested. Although the exact details of various plans may differ, a reasonable plan would devote more resources to making sure that emissions are accurately estimated for all power plants selected for the sample, rather than spending a small amount of time on each of a large number of power plants.

The simplest possible sampling strategy would be to take a simple random sample of size n from the population of all power plants, each with yearly emission y_i. For example, if there were a total of N = 1400 power plant units[6] (the population), a small percentage would be selected at random to form a sample. The average sample emission

$$\bar{Y} = \sum_{i=1}^{i=n} y_i/n \qquad (4)$$

would be calculated where i goes from 1 to n. An estimate of the total emissions $\hat{Y}$ for the entire population of power plants would be given by:

$$\hat{Y} = N/n\ \bar{Y} \qquad (5)$$

An arbitrary number of power plants will be chosen for the sample (for example, 5% or n = 70). The reliability of the sample estimate cannot be determined until all the sample data is collected and analyzed because the variability of the population is not known. In the simple case of random sampling, if the unknown population variance of all N emissions is S^2_y, then the variance for $\hat{Y}$ is $(1 - n/N)\ N^2\ S^2_y/n$. An approximate 95% confidence interval is given by:

$$Y \pm 2\sqrt{(1 - n/N)}\ NS_y/\sqrt{n}) \qquad (6)$$

The first improvement to this plan might be to do the sampling in two stages, so that the appropriate sample size could be determined for the desired reliability. This strategy would require that a small first phase sample be taken, just large enough to provide a reasonably good estimate of the population variability. For example, 50 to 100 power plants could be randomly selected, data collected and analyzed. The reliability of the first phase sample could then be determined (for example, by calculating a confidence interval for each estimated parameter). If the reliability of any of the estimates was too low, the population variability estimate could then be used to project how many additional samples would be needed in the second phase sampling to achieve the desired level of reliability.

Additional improvements can be made with the goal of achieving a higher reliability with either the same number of samples or less. These sampling strategies are more complex than for the simple random sampling described above, and have different formulas for emission estimates and their corresponding reliability estimates.[7] One approach would be to use stratification of the population.

The ideal (but impractical) variable to use to stratify the population would be plant emissions. If the plant emissions were somehow known, plants could be arranged into nearly homogeneous groups, and these groups would be randomly sampled. For example, plants could be divided into two groups: plants with small emissions and plants with large emissions. Similarly, more than two groupings could be used. Since in each group, the power plants are similar in emissions, the variability of emissions would be low, and this would lead to higher reliability in the estimate of total emissions for the same number of samples compared to pure random sampling. Of course, plant emissions are actually unknown for the entire population of power plants. Stratification can still be performed if another suitable variable related to emissions is available.

Since it would be expected that plants with larger boilers would produce larger total amounts of trace element emissions, boiler size could be used to perform the stratification. For example, the following strata could be used: less than 150 MW, 150 MW to 499 MW, 500 MW to 799 MW, and 800 MW or greater. The result of boiler size and coal ash content may possibly also serve as a good stratification variable. (Effect of coal cleaning may also be usefully included.) The average emissions in each stratum would be calculated and used to estimate total emissions in each stratum. The sum of the total emissions in each stratum would yield an estimate of total emissions. Similarly, the variance of emissions within each stratum could be used to determine the reliability of the total emissions estimate.

A small number of power plants would be considerably larger in terms of boiler size (or the product of boiler size and coal ash content). This small subset would contribute a large portion of total emissions and might tend to be more variable than other groups (since variability often increases with size). Therefore, in this group all power plants would be sampled. This is called a certainty sample. By doing this, a further increase in the reliability of the total emissions estimate may be achieved.

Other improvements can be entertained. For example, if estimates for every state are desired, in addition to national estimates, the sampling plan could be adjusted to allow for sampling within states so that separate state totals could be reliably estimated. In this case, stratification by boiler size might only be usefully applied to states with large numbers of plants. For states with a very small number of plants, all plants may need to be included in the state sample in order to achieve reliable estimates for these states. Providing reliable separate state emission estimates and national estimates will require a larger number of samples than if just national estimates were determined. Dividing the total population of power plants according to their state location while desirable on nonstatistical grounds, is unlikely to be very efficient in the sense of reducing sampling variances within the various states unless power plant sizes within states tend to be similar. To the extent that power plant sizes tend to be the same within each state, and differ between states, the total sampling variance would be reduced.

Sampling

The main emphasis has been on producing national (and possibly state) estimates. Similar principles apply to stratification by any system of classification. However, as discussed previously not all stratification schemes will benefit national estimates to the same degree. Also, the more strata, the larger the total number of samples required to produce individual stratum estimates. If power plants are classified by boiler type and assuming there are twenty boiler types, at least 40 samples would be required to make estimates for each boiler stratum (two samples per stratum). The 20 stratum estimates can be appropriately combined to produce an overall national estimate that may be quite precise. However, the stratum estimates are not likely to be very precise. It could easily take 20 samples per stratum to produce reasonably precise stratum estimates.

It should also be noted that careful attention must be paid to how the samples are collected within each stratum. If the strata are not probabilistically sampled, neither the stratum estimates nor any statistical projections based on stratum estimates are likely to be accurate.

Emissions Estimates for a Typical 500 MW Unit

If the trace element concentrations per unit of heat content in coal are known, trace metal emissions from a unit can be computed in several ways. The information required to compute the emissions includes total annual consumption of coal and emission factors for respective elements. However, emission factors tend to be site-specific and are influenced by boiler design and operating conditions and the type of particulate control device employed. The boiler design and operating conditions influence the split between the bottom ash and fly ash, and the degree of enrichment. Therefore, it is desirable to determine the ash flow rate and trace element concentrations in the fly ash at the inlet of the control device to estimate the total mass flow of trace elements into the particulate control device. Since the retention efficiency of the solid phase trace elements is approximately the same as the overall collection efficiency for typical baghouse/ESP systems, the emission rates can be computed by multiplying the fractional penetration of the control device (1 - retention efficiency) by the total trace element mass input.[2] However, total mass flow of trace elements at the control device inlet is not a readily known factor for many units. In addition, significant mass fractions of some trace elements, such as selenium and mercury, exist in vapor form in the flue gas and are not retained as effectively by baghouse/ESP systems.

Trace element emissions (airborne) for a hypothetical 512 MW pulverized bituminous coal-fired unit (equipped with an ESP) were estimated using predicted trace element concentrations for Coal B, and are shown below. A coal feed rate of 180 t/h, a net capacity factor of 65%, an ESP inlet flue gas temperature of 300°F, and an ESP ash loading of 10.8 t/h were used for the computations.

TRACE ELEMENT (AIRBORNE) EMISSIONS FOR A 512 MW UNIT

Trace Element	Concentration in Coal ng/Btu	Emissions, t/y
As	235	0.07
Be	22	0.01
Cd	2	0.00
Cr	377	0.09
Co	81	0.02
Mn	571	0.14
Ni	216	0.05
Pb	132	0.03
Sb	46	0.01
Se	42	0.81
Hg	4	0.08
Total		1.31

The computations also assume that only 1% of the total trace element mass (for the solid phase elements, i.e, all the elements except Se and Hg) is emitted through the stack. This assumption is quite reasonable considering that the solid phase elements are retained both in the bottom ash (which accounts for 30% of the total ash in most boilers) and ESP hopper ash (collection efficiency of 99% is quite common to most ESPs). It should be noted that the partitioning behavior of selenium is not well understood. If all of the selenium were in elemental form, the trace metal is expected to be in vapor form at typical stack conditions, and the concentrations normally seen in combustion flue gas. Thus, assuming 80% in vapor phase and the rest in solid phase, selenium emissions account for 61% of the total emissions. However, selenium is known to react readily with several other ash constituents forming solid phase compounds that are readily removed in baghouse/ESP systems.(8) Since most of the mercury is reported to be in vapor phase, an emission rate of 0.08 t/y (assuming all of the Hg in vapor form) represents a worst case scenario.(9) Combined solid phase elements and mercury emissions (nonhalogen trace element emissions) do not exceed 0.5 t/y.

References

1. E. Heath, "Review of U.S.G.S Data," U.S. EPA Report, March 1993.
2. N. J. DeIuliis, P. R. Tumati and C. E. Fink, "A Model to Provide Insights Into Trace Element Partitioning Behavior in Coal-Fired Boilers," Tenth EPRI Particulate Control Symposium, Washington, D.C., April 1993.
3. A. G. Fonseca, P. R. Tumati, M. S. DeVito, M. S. Lancet, and G. F. Meenan, "Trace Element Partitioning in Coal Utilization Systems," presented at the SME-AIME Annual Meeting, Reno, Nevada, February 1993.
4. E. H. Isaaks and R. M. Srivastava, "*Applied Geostatistics*," Oxford University Press, New York, 1989.
5. R. B. Finkelman, "Modes of Occurrence of Potentially Hazardous Elements in Coal: Levels of Confidence," Trace Element Transformations in Coal-Fired Power Plants (in print), Elseiver Publications, 1993.
6. T. C. Elliott, "*Power Plants Data Base*," McGraw Hill, New York, 1985.
7. C. E. Särndal, B. Swenson and J. Wretman, "*Model Assisted Survey Sampling*," Springer-Verlag, New York, 1992.
8. E. Dismukes, "Trace Element Control in Electrostatic Precipitators and Fabric Filter," International Trace Elements Workshop, Scottsdale, Arizona, April 1993.
9. P. R. Tumati and M. S. DeVito, "Partitioning Behavior of Mercury During Coal Combustion," IJPGC, Kansas City, Missouri, 1993.

Table I. USGS Trace Element Data for Pittsburgh Seam Coals (Concentrations in ng/Btu)

(Weight averaged concentrations of 71 samples from 31 locations in Pennsylvania)

COAL ID	No. of Samples	Btu/lb	Ash,lb/MMBtu	Sulfur,lb/MMBtu	Arsenic	Beryllium	Cadmium	Cobalt	Chromium	Mercury	Manganese	Molybdenum	Nickel	Lead	Antimony	Selenium	Total (ng/BTU)
A	2	11013	23.2	1.37	250	99	23	460	1,600	10	1,000	98	1,300	710	36	41	5700
B	1	13010	5.07	0.61	100	64	1.4	78	450	0.20	240	53	480	170	12	27	1700
C	2	13633	8.30	1.18	340	49	4.5	290	680	4.8	1,100	43	770	180	21	110	3600
D	1	13498	8.68	0.66	57	41	0.70	120	750	1.7	230	29	480	290	13	60	2100
E	1	13170	9.19	0.91	230	60	2.8	230	720	2.1	350	65	770	250	20	64	2800
F	4	11563	17.6	3.81	790	67	9.5	500	1,200	20	960	62	860	320	42	210	5100
G	2	14110	3.86	0.68	52	48	1.1	81	360	4.6	60	48	460	89	23	37	1300
H	3	12922	6.23	0.91	170	42	1.8	71	480	5.9	210	19	230	210	10	32	1500
I	1	13600	6.15	1.04	200	54	1.5	190	600	0.70	400	54	620	150	20	41	2300
J	3	13005	9.56	2.13	490	75	1.6	150	580	5.6	450	100	640	190	16	60	2800
K	1	12264	12.9	1.23	550	80	2.7	280	930	0.70	530	75	800	240	24	56	3600
L	1	13488	4.67	0.74	180	54	1.2	71	350	2.3	110	62	260	110	10	17	1200
M	1	13564	5.82	1.99	140	18	2.1	94	310	7.7	740	8	120	82	6.7	53	1600
N	3	12823	8.11	1.17	780	46	3.8	150	760	9.1	480	42	440	200	44	60	3000
O	3	12627	9.04	1.81	760	61	3.4	200	790	16	610	99	560	210	29	74	3400
P	1	13232	5.82	1.74	470	95	1.4	120	430	2.7	170	17	570	41	17	19	2000
Q	5	12026	11.9	3.00	3300	95	7.3	230	810	7.7	1,300	200	700	490	46	95	7300
R	3	12866	7.98	1.36	620	55	2.7	140	780	9.7	290	30	380	170	53	52	2600
S	2	11868	12.9	0.86	180	62	4.6	290	1,100	2.4	1,600	21	510	320	29	58	4200
T	1	13514	6.22	2.07	100	19	2.2	44	270	2.2	470	15	170	71	77	47	1300
U	1	11847	12.4	0.51	42	85	2.0	210	950	1.2	430	50	960	200	15	270	3200
V	3	13157	5.27	1.17	250	53	1.5	110	450	7.6	250	48	350	120	10	24	1700
W	2	12678	8.34	1.76	1000	43	4.8	190	660	11	540	83	450	200	27	58	3300
X	2	12618	8.64	2.30	1000	58	6.4	230	640	13	520	22	480	210	31	59	3300
Y	3	12430	9.20	2.66	2300	53	5.1	180	890	10	420	110	540	230	47	69	4800
Z	5	12034	11.6	3.33	730	57	10	170	820	7.8	570	140	480	270	21	120	3400
1	3	12783	7.98	3.10	2300	31	3.5	150	660	5.3	1,100	36	240	130	34	65	4800
2	3	12713	7.75	2.35	3000	35	2.9	110	490	5.9	380	33	230	170	37	68	4500
3	3	13085	6.23	2.42	510	40	2.0	86	390	14	710	91	270	120	13	31	2300
4	4	13091	5.83	1.12	380	80	1.8	130	430	4.9	630	97	690	180	21	41	2700
5	1	13202	5.38	1.74	650	41	2.3	96	360	19	540	24	230	93	14	41	2100
Minimum		*11013*	3.86	0.51	42	18	0.70	44	270	0.20	60	8	120	41	6.7	17	1200
Maximum		*14110*	23.2	3.81	3300	99	23	500	1,600	20	1,600	200	1,300	710	77	270	7300
Average		*12820*	8.77	1.67	710	57	3.9	180	670	7.0	560	61	520	210	26	67	3100
STD		*676*	3.96	0.86	830	20	4.2	100	290	5.2	360	42	260	130	15	52	1400

TABLE II. USGS TRACE ELEMENT DATA FOR PITTSBURGH SEAM COALS
(71 SAMPLES FROM 31 MINES)

	USGS DATA				CONSOL DATA			
	CURRENT STUDY @			EPA STUDY(1)				
	Minimum	Maximum	Average	EPA's Avg * for PA Coals	COAL A Raw	COAL A Clean	COAL B Raw	COAL B Clean
ASH Lb/MMBtu	3.86	23.2	8.76	-	23.0	4.78	12.7	6.15
SULFUR Lb/MMBtu	0.506	3.81	1.67	-	2.03	1.11	2.31	1.99
<u>TRACE ELEMENT CONCENTRATIONS (ng/BTU)</u>								
ARSENIC	42	3300	830	1100	770	200	740	240
BERYLLIUM	18	99	57	87	49	20	37	22
CADMIUM	0.75	23	3.9	3.6	4.9	1.6	3.6	2.0
CHLORINE	0.00	32000	14000	38800	-	-	-	-
COBALT	44	500	18	280	280	64	160	81
CHROMIUM	270	1600	670	710	1100	300	700	380
MERCURY	0.17	20	7.0	10	5.7	2.9	5.4	3.6
MANGANESE	60	1600	560	830	2500	350	1500	570
NICKEL	120	1300	520	720	750	220	490	220
LEAD	41	710	210	380	400	97	230	130
ANTIMONY	6.7	77	26	44	35	21	16	9.8
SELENIUM	17	270	67	180	76	35	46	42
TOTAL METALS	620	9500	2600	4500	6000	1300	4000	1700

@ Using trace element correlations with ash and/or sulfur
* For all seams in Pennsylvania

Table III. Correlation coefficients (r) for the USGS Pittsburgh seam coal samples in Pennsylvania.

	Btu	Ash (lb/MM Btu)	Total Sulfur (lb/MM Btu)	Pyritic Sulfur (lb/MM Btu)	Organic Sulfur (lb/MM Btu)
Arsenic	-0.29	0.11	**0.63**	**0.68**	0.23
Beryllium	-0.55	**0.54**	-0.08	0.04	-0.24
Cadmium	-0.74	**0.84**	0.34	0.29	0.26
Cobalt	-0.72	**0.88**	0.24	0.08	-0.04
Chromium	-0.85	**0.94**	0.15	0.07	0.01
Mercury	-0.30	0.22	**0.56**	**0.54**	0.09
Manganese	-0.53	**0.55**	0.38	0.44	0.40
Molybdenum	-0.42	0.35	0.38	**0.57**	0.09
Nickel	-0.58	**0.77**	-0.10	-0.13	-0.20
Lead	-0.76	**0.86**	0.13	0.13	0.15
Antimony	-0.28	0.28	0.40	0.23	**0.58**
Selenium	-0.49	0.48	0.26	0.05	-0.05
Total	-0.75	**0.74**	0.46	0.47	0.18

Table IV. Comparison of spatially weighted averages and unweighted averages.

Parameters	AVERAGES (ng/Btu, except where noted) Spatially Weighted	Equally Weighted	% Difference
Heating Value, Btu	12,585	12,820	2
Arsenic	497	706	42
Beryllium	59.9	56.8	-5
Cadmium	6.15	3.92	-36
Cobalt	230	175	-24
Chromium	812	667	-18
Mercury	7.42	6.97	-6
Manganese	495	563	14
Molybdenum	61.3	60.8	-1
Nickel	657	519	-21
Lead	278	206	-26
Antimony	31.0	26.4	-15
Selenium	69.8	66.5	-5
Total Trace Elements	2,619	2,824	8
Ash (lb/MM Btu)	11.06	8.77	-21
Sulfur (lb/MM Btu)	1.58	1.67	6
Pyrite Sulfur (lb/MM Btu)	0.57	0.90	58
Organic Sulfur (lb/MM Btu)	0.54	0.60	12

Figure 1. Sample locations in the Pittsburgh seam in Southwestern Pennsylvania (county boundaries shown).

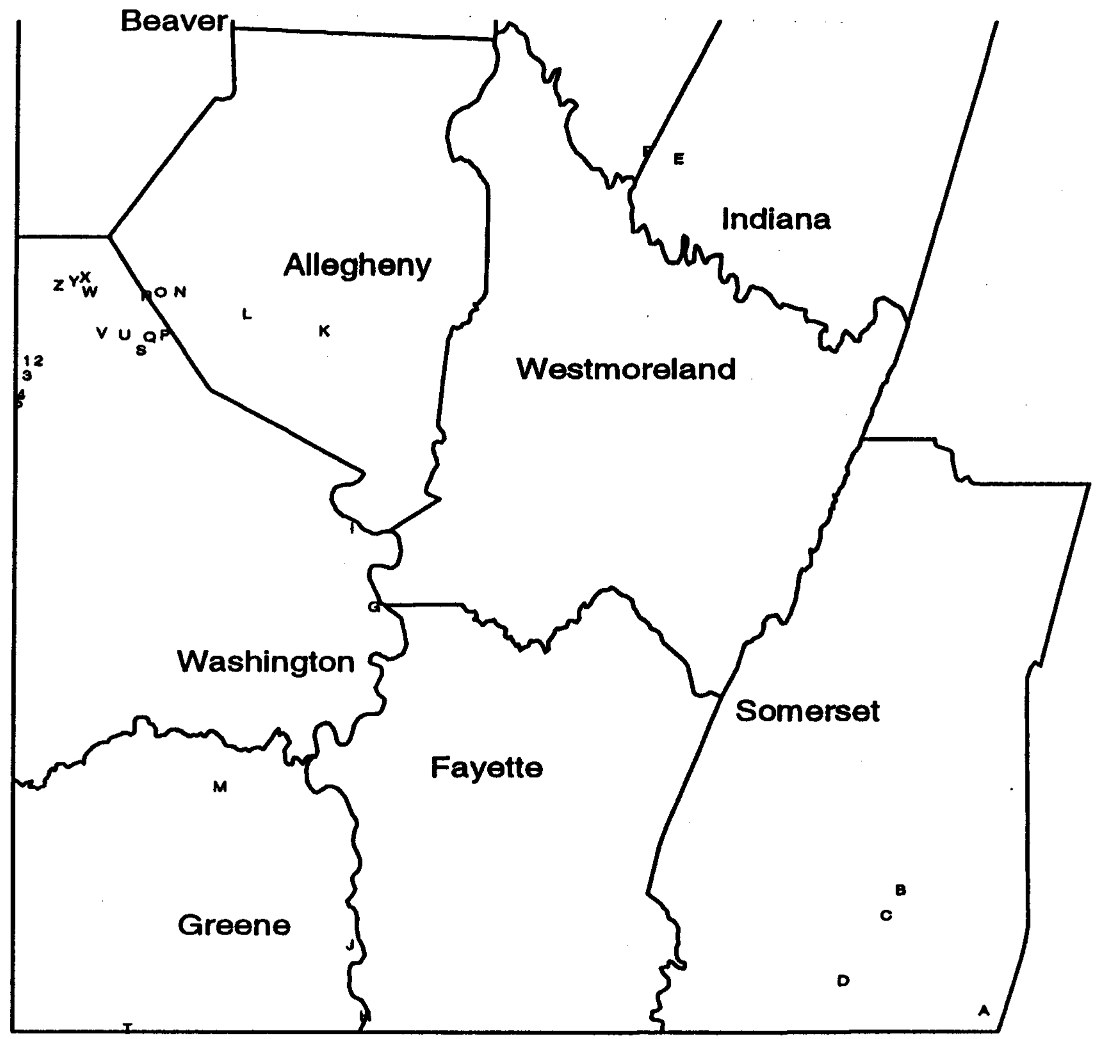


Figure 2. Trace element concentrations as a function of ash or sulfur.

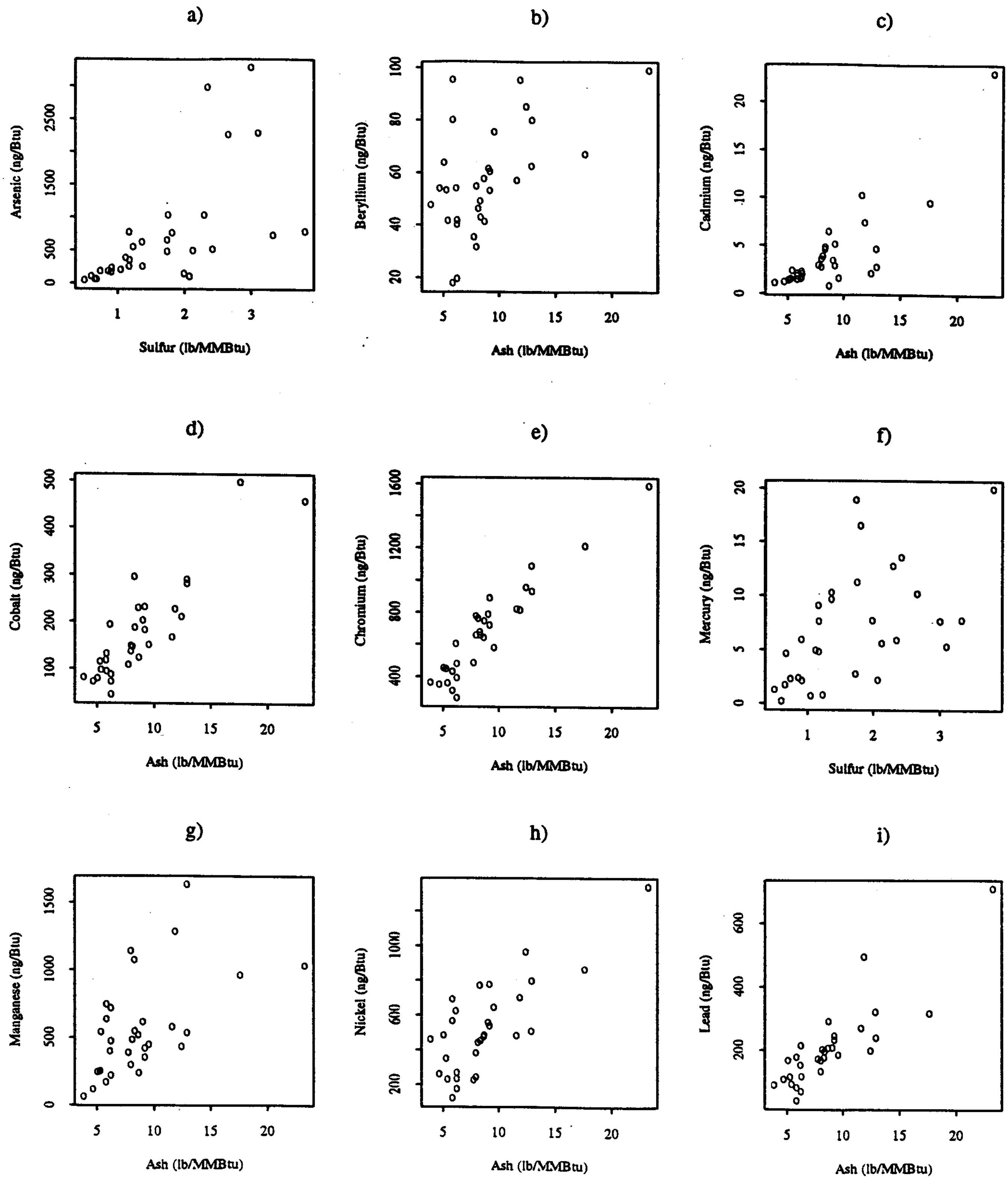
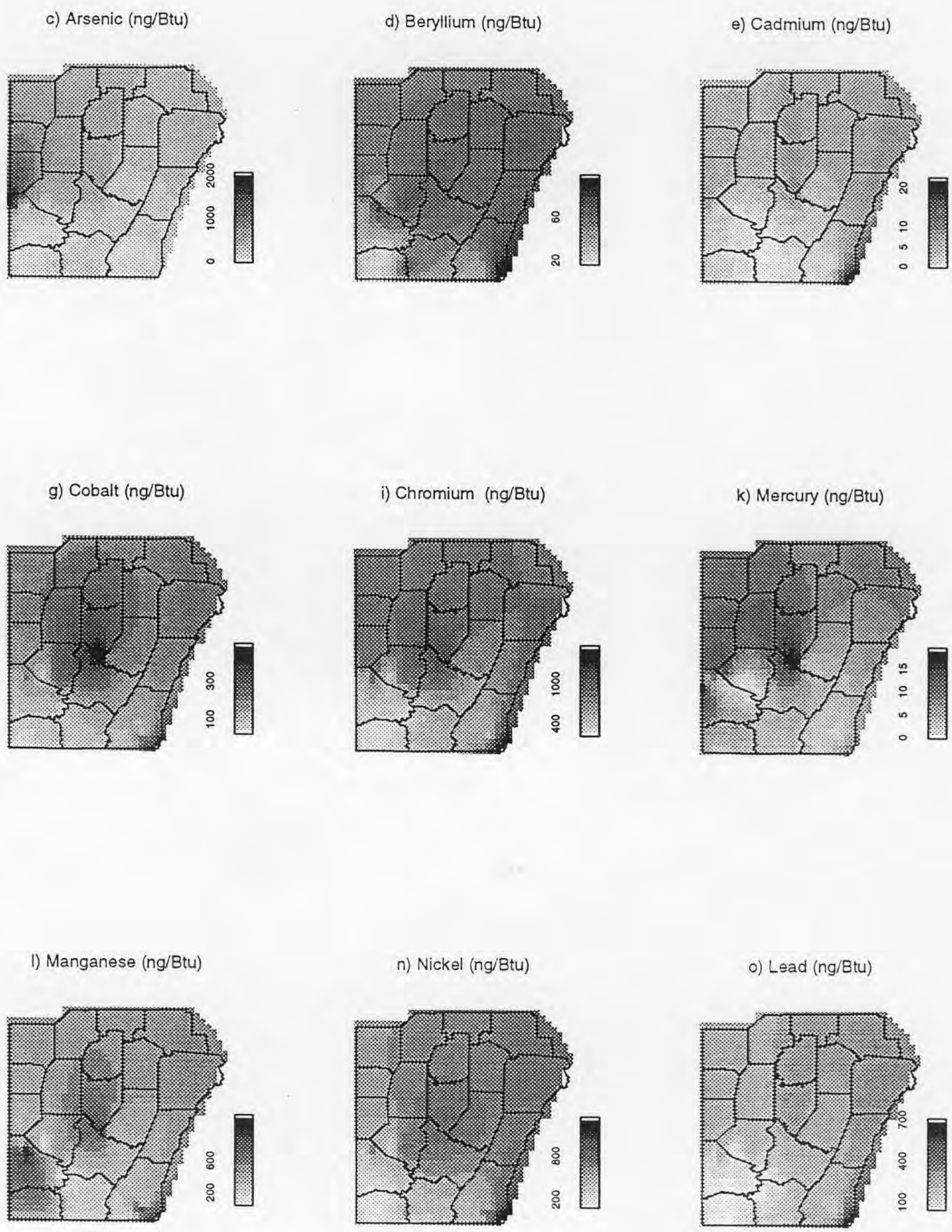


Figure 3. Shaded maps based on USGS samples from Pittsburgh No. 8 coal bed.



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Potentially Carcinogenic Species Emitted to the Atmosphere by Fossil-Fueled Power Plants

by D. F. S. Natusch*

The identities and physicochemical characteristics of potentially carcinogenic species emitted to the atmosphere by fossil-fueled power plants are presented and discussed. It is pointed out that many so-called carcinogens are preferentially concentrated on the surface of respirable fly ash particles thus enabling them to come into intimate contact with lung tissues when inhaled. Relatively little information is available about the identities of particulate polycyclic organic compounds whose emission from coal fired power plants may well be substantially greater than hitherto supposed. The importance of chemical changes, which several species may undergo following emission (but prior to inhalation) in determining their potential carcinogenic impact, is stressed.

Introduction

Production of electric power from the combustion and conversion of fossil fuels represents a ubiquitous and increasing means of obtaining energy in most countries throughout the world. It is now well established that such power plants emit substantial quantities of many carcinogenic and potentially carcinogenic chemical species to the atmosphere. Consequently, it is of considerable importance to establish whether these materials are active in promoting the occurrence of lung cancer in populations resident in the vicinity of fossil-fueled power plants.

In order to make any assessment of risk it is necessary to have knowledge of the nature, concentrations, and physicochemical characteristics of potentially carcinogenic material emitted from the various types of fossil fueled power plants. This paper, therefore, presents a brief survey of the information currently available. Special emphasis is placed on what is known about the physical and chemical characteristics and behavior of each species since these properties may have a profound influence on the inhalation toxicology of individual species (*1*, *2*).

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Fossil-fueled power plants are considered to be those utilizing gases, liquids, or solids as primary fuels derived, respectively, from natural gas, oil, or coal. Some difficulty is encountered in specifying individual pollutant species since definitive data on carcinogenicity are sparse. For the purpose of this paper, therefore, compounds are classified as known carcinogens, suspected carcinogens, and reactants. Compounds classified as reactants are those which are considered likely to be involved in chemical reactions which may result in the production or removal of carcinogenic species or which may interact synergistically with known carcinogens. In Table 1 are given examples of concentrations of known and suspected carcinogens in urban and rural atmospheres.

Gaseous Emissions

Gaseous emissions from fossil-fueled power plants generally contribute more material to the atmosphere than do particulate emissions (except in the now rare case of uncontrolled coal combustion). The major emissions, in terms of mass, involve carbon monoxide (CO), hydrocarbons (HC), nitrogen oxides (NO_x), sulfur oxides (SO_x), and oxygenated species often classified as formaldehyde (HCOH). Representative contributions are indicated in Table 2 (*13*). In addition, minor emissions of mercury occur, and it has been suggested that bromine (Br_2),

Table 1. Concentrations of known and suspected carcinogens in urban and rural atmospheres.

Substance[a]	Status	Urban air[b] Range	Urban air[b] Average[c]	Rural air (range)[b]	References
Inorganic cases, $\mu g/m^3$					
SO_x	Reactant	20–1200	70	0.1–5	(2, 4)
NO_x	Reactant	50–400	100	2–6	(2, 4)
O_3	Reactant	20–400	100	20–100	(2, 4)
Hg	Suspected	0.001–0.20	0.007	—	
Inorganic particulates, ng/m^3					
As	Recognized	2–130	10	< 0.5–5	(5, 6)
Asbestos	Recognized	10–100	20	—	(7)
Be	Recognized	< 0.2–8	5	—	(5, 6)
Cd	Recognized	4–250	10	—	(5, 6, 8)
Co	Suspected	0.5–15	2	< 0.5–2	(5, 8)
Cr	Recognized	5–120	15	< 1–10	(5, 8)
Cu	Suspected	10–4000	60	1–280	(5, 8)
F[d]	Suspected	< 50–2000	300	< 50–150	(5)
Fe	Suspected	1000–2000	1400	10–1000	(5, 8)
Ni	Recognized	10–1000	100	< 10	(5, 6, 8)
Pb[e]	Suspected	500–3000	1500	10–100	(5, 6, 8)
Se[f]	Suspected	< 1–10	1	—	(5)
SO_4^{2-}	Suspected	1000–100,000	5000	—	(2, 5)
U	Recognized	0.01–2	0.2	—	(9)
V[g]	Suspected	50–2000	500	< 1–50	(5, 6, 8)
		1–100	10		
Total particulates	Reactant	$(60–220) \times 10^3$	140×10^3	$(5–60) \times 10^3$	(4, 5)
Radionuclides, Ci/m^3					
^{210}Pb	Recognized	$(1–30) \times 10^{-15}$	20×10^{-15}	$(55–10) \times 10^{-15}$	(9)
^{212}Pb	Recognized	$(0.1–4) \times 10^{-15}$	2×10^{-15}	$(0.03–0.06) \times 10^{-15}$	(9)
^{226}Ra	Recognized	$(50–100) \times 10^{-18}$	—	—	(9)
^{222}Rn	Recognized	$(20–1000) \times 10^{-12}$	200×10^{-12}	$(0.1–20) \times 10^{-12}$	(9)
^{228}Th	Recognized	$10–50) \times 10^{-18}$	30×10^{-18}	—	(9)
^{230}Th	Recognized	$(20–70) \times 10^{-18}$	50×10^{-18}	—	(9)
^{232}Th	Recognized	$(10–50) \times 10^{-18}$	30×10^{-18}	—	(9)
$^{234}U + ^{238}U$	Recognized	$(100–400) \times 10^{-18}$	200×10^{-18}	—	(9)
Gaseous and particulate organic species					
Alkanes, ng/m^3[i]					(3, 4)
n-Butane	Reactant	5–80	10	—	
n-Pentane	Reactant	1–40	15	—	
2-Methylbutane	Reactant	5–60	25	—	
Alkenes, ng/m^3[i]					(4)
2-Butene	Reactant	1–5	6	—	
1,3-Butadiene	Reactant	1–5	2	—	
Propene	Reactant	1–20	6	—	
Aldehydes and ketones, ng/m^3					(3, 7)
Formaldehyde	Suspected	5–100	20	0.5–5	
Acrolein	Suspected	< 1–20	5	—	
Nitrosamines,[j] ng/m^3					(10)
Dimethylnitrosamine	Recognized	20–100	—	—	
Peroxides, ng/m^3					(3, 4)
Peroxyacylnitrates	Suspected	2–30	—	—	
Aromatic hydrocarbons, ng/m^3					(3, 7)
Benzene	Recognized	5–90	20	—	
Toluene	Reactant	10–100	40	—	
1,2-Dimethylbenzene	Suspected	5–100	40	—	
1,3-Dimethylbenzene	Suspected	5–100	40	—	
1,4-Dimethylbenzene	Suspected	5–100	40	—	
Polyaromatic hydrocarbons,[k] ng/m^3					(2, 11, 12)
Anthracene	Reactant	0.5–700	1	—	
Benzo[a]pyrene	Recognized	1–50	10	—	
Benzo[e]pyrene	Suspected	0.1–50	5	—	
1,2-Benzanthracene	Recognized	1–70	20	—	
1,12-Benzperylene	Reactant	0.1–20	3	—	
Coronene	Reactant	0.2–50	1	—	
Chrysene	Suspected	0.5–200	5	—	
Pyrene	Reactant	0.2–50	10	—	

Table 1 (cont'd.)

Polycyclic nitrogen compounds, ng/m³					(2, 12)
Acridine	Suspected	0.1–0.5	—	—	
Fluorene carbonitrile	Suspected	0.02–0.1	—	—	
Lead tetraalkyls, ng/m³					(6)
Tetraethyllead	Suspected	50–2000	75	—	
Benzene-soluble organics, ng/m³	Recognized	1000–20,000	7000	200–3000	(2, 4, 7)

[a]The substances listed include both known and suspected carcinogens for which reasonably reliable atmospheric concentration data are available. Also listed are several compounds which are considered to be capable of promoting carcinogenic activity in noncarcinogenic compounds or modifying that of carcinogens as a result of chemical reaction.

[b]Most values represent 24-hr averages established over periods ranging from several days to one or more years.

[c]Approximate averages values have been estimated for urban air noting that individual areas may exhibit atmospheric concentrations which differ considerably from the average. Due to paucity of data it is considered inappropriate to estimate similar averages for rural atmospheres.

[d]Fluorine is present in the atmosphere as both fluorine gas and particulate fluorides. The values listed refer to the sum of both forms.

[e]Values listed for lead refer to concentrations measured in countries utilizing lead alkyl gasoline additives. Significantly lower values are encountered in countries which do not use leaded gasoline.

[f]Selenium is present in the atmosphere in both gaseous and particulate form. The values listed refer to the sum of both forms. Also, selenium has not been implicated as a causative agent of bronchial carcinoma but only of liver and kidney cancers.

[g]The two sets of values listed for vanadium refer, respectively, to urban areas where considerable use is made of fuel oil for power generation and domestic heating, and to urban areas where oil burning is minimal.

[h]A very large number of organic compounds have been implicated as causative agents for bronchial carcinoma. Only a few of these are listed here, however, since reliable atmospheric concentration data are unavailable. In general, compounds are listed by class with specific examples being given where data are available.

[i]These hydrocarbons are not in themselves considered to be carcinogenic. They may, however, promote formation of photochemical smog which contains several carcinogenic components.

[j]The data for nitrosamines are very tenuous; they are, however, included because of the considerable current interest in these compounds.

[k]Several noncarcinogenic polycyclic compounds are listed, since some of these are known to react photochemically to produce oxygenated derivatives (such as quinones, phthalates, and endoperoxides) which are suspected carcinogens. It will be noted that some very wide concentration ranges are listed for the polyaromatic hydrocarbons. The upper ends of these ranges correspond to values measured in European cities where extensive coal burning is practiced.

Table 2. Average air pollution emissions from power plants according to fuel type.[a]

	Emissions, lb/1000 lb fuel					
Fuel	Particles[a]	CO	HC	NO_2	SO_2	HCOH
Coal	85 (1 - E)[b]	0.25	0.1	10	19 S[c]	0.002
Oil	1.7 (1 - E)	0.07	0.5	17	19 S	0.1
Natural gas	2.7 (1 - E)	neg.	neg.	70	19 S	0.2

[a]Data of Goldstein and Waddams (13).

[b]E is the mass collection efficiency of the control equipment.

[c]As the percent sulfur content of the fuel by weight.

hydrochloric acid (HCl), selenium dioxide (SeO_2), arsenic trioxide (As_4O_6), and organometallics such as nickel carbonyl ($Ni[CO]_4$) may be emitted as vapors (6, 14).

Sulfur Oxides

Sulfur oxides are not, in themselves, thought to be carcinogenic. They are, however, quite reactive and are known to react with, for example, polycyclic aromatic species (2) and to promote lung damage when associated with airborne particles. In the absence of controls the amounts of sulfur oxides emitted from a fossil-fueled power plant are directly related to the sulfur content of the fuel burned (Table 2). In this case, typical SO_x emissions lie in the range 500–3000 ppm with 1000–2000 ppm being most commonly encountered (15). Nowadays, however, most major installations utilize control equipment which typically achieves 85-90 percent removal of SO_x. Generally, about 1–2% of the emitted sulfur oxides are in the form of SO_3, which reacts rapidly with water vapor to produce sulfuric acid mist. A small amount of the SO_2 is also chemisorbed by fly ash particles to form metallic sulfates (primarily calcium sulfate and alkali iron trisulfates) (16).

The rate and extent of sulfur dioxide conversion to sulfuric acid mist and solid particulate sulfate in a power plant plume are unknown; however, current thinking is that these processes occur fairly extensively, so that a significant proportion of the gaseous sulfur oxides produced actually occur in urban atmospheres as sulfuric acid mists or as particulate sulfate (4). This is an important consideration, since it means that the health hazard presented by gaseous sulfur oxides may be partly manifest through inhalation of sulfuric acid and sulfate particles.

Nitrogen Oxides

As in the case of sulfur oxides, the oxides of nitrogen are not carcinogenic but may produce carcinogenic materials as a result of chemical reactions such as those involved in photochemical smog formation. By contrast with sulfur oxides, which are derived from sulfur present in the fuel, nitrogen oxides are derived primarily from fixation (oxidation) of atmospheric nitrogen present in the combustion feed air. Consequently, nitrogen oxides cannot be effectively controlled by selection or pretreatment of the fuel.

Representative emission factors for nitric oxide (NO) and nitrogen dioxide (NO_2) combined are given in Table 2, although it should be recognized that NO_x emissions are not directly related to the amount of fuel consumed. Rather, they depend on the feed rate of air supporting combustion, the temperature, and the fuel-air mixing characteristics. Actual concentrations of NO_x are normally in the range 300–1300 ppm in stack emissions. Significantly higher concentrations are produced during natural gas combustion than during combustion of coal or oil (Table 2).

The amount of NO_2 formed during combustion is generally much less than that of NO; however, conversion of NO to NO_2 occurs fairly rapidly in a power plant plume following emission. From the standpoint of human health, therefore, it is reasonable to presume that the primary direct exposure will be to NO_2.

Organic Gases

The amounts of organic material emitted as gases or vapors from fossil-fueled power plants are quite small (2.5%) when compared with those from other anthropogenic sources. For example, transportation accounts for some 53% of the gaseous organics emitted in the United States. Consequently, rather little work has been done to determine the identities and amounts of individual organic gases emitted from power plants. Primary emissions consist of hydrocarbons, aldehydes, and organic acids for which representative emission factors are given in Table 3. Of these materials only certain aldehydes (e.g. formaldehyde and acrolein) are suspected carcinogens. Hydrocarbons and organic acids are, however, quite reactive (hydrocarbons in photochemical smog production) and are thus worthy of consideration in the present context (*3*).

Table 3. Typical emission of several classes of compounds from stationary combustion sources.[a]

	Emission, lb/ton of fuel		
Compounds	Coal	Oil	Gas
Hydrocarbons	0.3	1.0	1.0
Aldehydes	Unknown	0.5	0.5
Formaldehyde	0.0003	0.006	0.008
Organic acids	10	5	?

[a]Data from National Academy of Sciences (*3*).

Other Gaseous Emissions

With the exception of elemental mercury vapor, very little is known about gaseous emissions other than those already discussed. Mercury is, however, a suspected carcinogen.

Mercury levels in coal and fuel oil average about 1 μg/g and 0.1 μg/g, respectively. When the coal is burned, about 90–95% of the mercury present is emitted to the atmosphere as elemental vapor. The remainder is associated with fly ash. There is no apparent tendency for mercury vapor to become adsorbed or otherwise associated with fly ash or atmospheric aerosols. Consequently, mercury is transported long distances from a coal fired power plant. This behavior is exactly opposite to that of other, particulate associated, metals.

The actual concentrations of mercury vapor emitted from a given power plant will depend on the type and origin of the fuel burned; however, because of the almost quantitative release of mercury to the atmosphere, stack concentrations can be readily calculated where stack gas flow rates are known. Typical stack exit concentrations are around 1 $\mu g/m^3$ for a coal fired power plant. Plume concentrations depend, of course, on atmospheric conditions but concentrations around 80 ng/m^3 have been measured (*17*) at ground level on the plume center line 1.2 miles downwind of a coal fired power plant. Representative concentrations in urban atmospheres lie in the range 2–100 ng/m^3, most of which is present as mercury vapor (*18*).

Fossil fuel combustion also results in the release to the atmosphere of several radioactive species including the gas radon (^{222}Rn), which, with its daughter products, is a known carcinogen. The few available measurements indicate that natural gas contains 10–20 pCi/l of ^{222}Rn and that coal contains 0.1–0.4 pCi/g. While quantitative release of radon to the atmosphere will occur, present estimates suggest that fossil fuel combustion does not contribute significantly to the natural ^{222}Rn background even in the vicinity of power plants (*9*).

Particulate Emissions

Fossil-fueled power plants contribute approximately 25% of the anthropogenic particulate matter emitted to the atmosphere in the United States. In many countries the proportion is even higher. As indicated by the data in Table 2, particulate emissions from coal-fired power plants are much greater than those derived from oil or natural gas combustion. Some idea of particle mass emission factors can be obtained by noting that modern electrostatic precipitation equipment usually operates with mass removal efficiencies in excess of 98%.

Assessment of the carcinogenic hazard associated with airborne particulate material such as fly ash is very much more difficult than is the case for a gaseous pollutant. This is because particles contain a large number of potentially carcinogenic chemical species including both organic and inorganic compounds. The relative amounts of these species, and thus their net carcinogenicity, can vary significantly with the type and origin of the fuel burned and even with the operating characteristics of individual power plants. Furthermore, the way in which a given chemical species is distributed among different particles and even within a single particle can strongly influence its potential health impact. Finally, it must be recognized that, although many potentially carcinogenic compounds may be associated with solid fly ash particles these compounds are unlikely to constitute a hazard to health unless they can be mobilized into solution, e.g., body fluids.

The extent to which information is available about each of the above factors is discussed in the following sections. For convenience, different classes of chemical compounds are considered separately even though all may be present together. In this regard it is useful to note that a single particle effectively concentrates many chemical species in a localized microregion so that its influence is likely to be exerted over a very localized area of lung tissue when inhaled. This is in contrast to the more generalized influence of inhaled gases.

Particle Morphology, Size Distribution, and Matrix Composition

Particles emitted to the atmosphere from fossil fueled power plants are more or less spherical. In the case of coal combustion both solid and hollow spheres occur and some of the latter have small respirable spheres encapsulated inside them (*15, 19*). Particles derived from oil and natural gas combustion have a highly porous structure rather like that of a sponge (*20*).

The aerodynamic size of a particle is a major factor in determining the efficiency with which it can be collected by control equipment, its atmospheric transport characteristics and lifetime, and its deposition and clearance behavior when inhaled (*1*). In addition, the size of a particle determines the specific surface area which can come into intimate contact with body fluids and tissues. The size distributions of particles produced by different power plants exhibit considerable variation; however, a typical size distribution of fly ash emitted from a coal fired power plant equipped with an electrostatic precipitator is presented in Figure 1 (*21*). It is apparent from this figure that much of the emitted fly ash falls in the respirable size range.

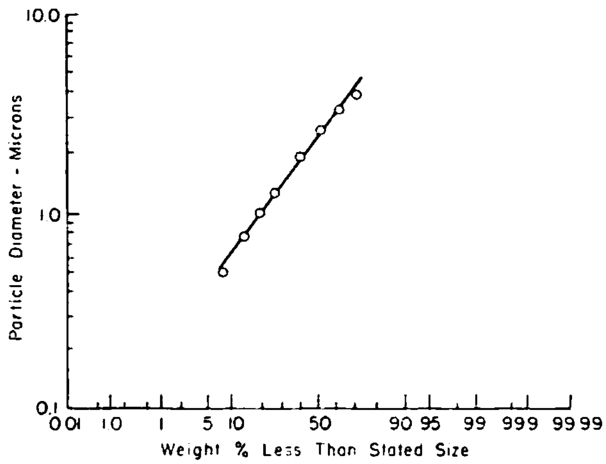

FIGURE 1. Representative aerodynamic particle size distribution of fly ash emitted from a coal fired power plant equipped with an electrostatic precipitator (*21*).

Relatively few measurements have been made of particle size distributions in power plant plumes. As a rough indication, however, particulate material collected at a distance of 5 miles downwind from a coal-fired power plant plume under stable plume conditions has an aerodynamic mass median diameter in the range 0.08–0.25 μm. Such samples usually exhibit a bimodal distribution, with the two modes being centered around 0.04 μm and 0.3 μm. The smaller modal particles are thought to represent a secondary aerosol consisting primarily of sulfate particles. Comparable information is not, to our knowledge, available for oil or natural gas-fired power plants, although similar general behavior would be expected.

The major matrix elements present in coal fly ash are Al, Si, and Fe, with minor amounts of Ca, Mg, K, Na, Ti, and S. Some typical composition ranges, expressed as weight percent as the oxides, are presented in Table 4 (*22*). The matrix elements in oil fly ash are C, Ca, Fe, S, Si, Ti, and V (*23*), whose relative proportions vary considerably in individual particles. Coal fly ash consists primarily of a semitransparent aluminosilicate glass with small amounts of microcrystalline hematite (Fe_2O_3) magnetite (Fe_3O_4). α-quartz (SiO_2). mullite ($3Al_2O_3 \cdot 2SiO_2$). anhydrite ($CaSO_4$), and lime (CaO). In addition some elemental carbon (soot) particles are present. All these compounds have low solubility in water which accounts for the low bulk solubility of fly ash. The compounds present in fly ashes derived from oil and natural gas combustion have not been established although it is known that such particles are highly carbonaceous in nature.

Table 4. Typical matrix element composition ranges of some U. S. coal fly ashes expressed as weight percentages of the oxides.

	Matrix element composition, wt-% of oxide
Major constituent	
Al_2O_3	14–30
SiO_2	22–60
Fe_2O_3	3–21
K_2O	0.2–3.5
CaO	0.5–31.0
Minor constituents	
Li_2O	0.01–0.07
Na_2O	0.2–2.3
MgO	0.7–12.7
TiO_2	0.6–2.6
P_2O_5	0.1–1.1
SO_4[b]	0.1–2.2

[a]Data of Natusch (*15*).
[b]Soluble sulfate.

Trace Elements

As a result of their geological origins coal and petroleum oil contain essentially all known stable elements in minor or trace amounts. Of these, the elements As, Be, Cd, Co, Cr, Cu, Fe, Hg, Ni, Pb, Se, and V are regarded as either known or suspected carcinogens. It must be strongly emphasized, however, that the chemical and toxicological properties of any element depend upon the nature of the chemical compound in which that element is present. Unfortunately very little is known about the identities of metal compounds emitted in particulate form from fossil fueled power plants. Consequently it is accepted, though strictly incorrect, practice to refer to the metallic elements themselves.

The specific concentrations ($\mu g/g$) of individual trace elements found in coal and oil fly ashes depend primarily on the trace element content of the original fuel. However, the relative concentrations of elements differ significantly between fly ash and fuel due to the different partitioning characteristics of individual elements between bottom ash and fly ash. Thus, in the case of coal fly ash, it is not reasonable to assume that because a given fraction of one element ends up in emitted fly ash that the same fraction of other elements will do likewise. This assumption is, however, reasonable in the case of an oil fired power plant which produces very little combustion residue.

Some representative specific ($\mu g/g$) and volume ($\mu g/m^3$) concentrations of trace elements emitted from coal and oil fired power plants are presented in Table 5. It should be noted that volume concentrations will be highly dependent on individual plant operating conditions. It should also be noted that vanadium, V, is emitted in substantial amounts from the combustion of fuel oil. This is because the element is concentrated in the form of several vanadium porphyrins in the original fuel (*24*).

At this point it is appropriate to comment on the partitioning of different elements in coal-fired (and probably also oil-fired) power plants. The most important aspect in this regard is that several potentially carcinogenic elements or their compounds are apparently volatilized at the combustion temperatures (1400–1600°C) encountered. These elements then condense or absorb onto the surface of coentrained fly ash particles as both particles and vapors leave the combustion region. Since small particles have a greater specific surface area than do large particles this phenomenon results in the volatile elements becoming preferentially associated with small particles (*14*). Table 6 presents data showing how the specific concentrations of several potentially carcinogenic elements depend on aerodynamic particle size in fly ash both emitted and retained by a representative coal-fired power plant.

This dependence of trace element concentration on particle size has the net effect of decreasing the aerodynamic equivalent mass median diameters of volatilizable trace elements with respect to that of the bulk fly ash with the following important results: (1) many potentially carcinogenic trace elements are most concentrated in the small, pulmonary depositing, fly ash particles which are least effectively collected by existing particle control devices; (2) the concentrations of volatilizable trace elements determined by analyzing fly ash collected by control devices are very much lower than the concentrations of those elements actually emitted. Trace element emission factors cannot, therefore, be obtained by multiplying the specific concentration of an element measured in retained fly ash by the bulk particle emission factor.

It should be pointed out that, although the specific concentrations of volatilizable elements increase more or less linearly with inverse particle diameter (*14, 25*), the same is not true when volume

Table 5. Specific concentrations and volume concentrations of elements in coal and oil fly ashes.

Element	Coal fly ash: Specific concn, μg/g	Coal fly ash: Volume concn, μg/m³	Oil fly ash: Specific concn, μg/g	Oil fly ash: Volume concn, μg/m³
Al	70,000–140,000	5000–10,000	100–5000	130–300
As	2–500	60–90	30	4–7
Au	0.004–0.1	—	—	—
B	10–600	—	—	—
Ba	500–7000	30–110	500–10,000	1600
Be	1–10	—	—	—
Br	0.3–20	1–5	—	—
Ca	6000–180,000	300–1000	10–1000	500–700
Cd	0.1–50	—	—	—
Ce	100–300	—	—	1–2
Cl	10–500	—	—	—
Co	5–100	1–5	90	16
Cr	50–300	8–20	66	12
Cs	1–20	—	—	0.1
Cu	50–650	—	50–2000	—
Fe	25,000–300,000	4000–10,000	10,000–100,000	700–1000
Ga	10–250	2–10	—	—
Hf	5–10	—	—	—
Hg	0.02–0.4	—	—	—
I	0.5–7	15–40	—	—
In	0.1–0.3	—	—	—
K	1500–35,000	—	1000	—
La	35–100	2–10	—	2.5
Lu	0.5–2	—	—	—
Mg	11,000–60,000	300–1000	500–5000	—
Mn	50–500	—	1–100	8
Mo	5–40	70–200	—	—
Na	1200–18,000	—	2000–50,000	4000–7000
Ni	5–100	10–25	—	—
Pb	5–1000	10–20	200–2000	—
Rb	40–300	—	—	—
Sb	1–15	0.5–3.0	5	1
Sc	10–40	2–4	—	0.03
Se	1–20	5–15	5	0.6
Sm	10–20	—	—	0.15
Sn	30–30	—	—	—
Sr	50–4000	—	—	—
Ta	0.5–1.5	—	—	—
Th	15–70	0.5–3.0	—	0.13
Ti	3500–8500	300–700	—	—
Tl	2–30	—	—	—
U	5–20	—	—	—
V	100–500	10–60	100–200,000	1000–1200
W	3–10	—	—	—
Yb	3–7	—	—	—
Zn	50–5000	20–70	200–3500	680

concentrations are employed. This is because volume concentrations depend upon the way in which the bulk particulate mass is distributed with respect to aerodynamic particle size. Some typical elemental size distributions determined in the stack gas of a coal fired power plant are presented in terms of volume concentration (μg/m³) in Figure 2 (*23*).

As mentioned previously, coal combustion results in the emission of several carcinogenic radionuclides in particulate form. Specific concentrations of ^{210}Pb, ^{226}Ra, ^{228}Ra, ^{228}Th, ^{238}Th, and ^{238}U have been measured in coal fly ash (*25–28*); however, only ^{210}Pb and ^{238}U are enriched with respect to the levels found in soil. Measurements of ^{226}Ra, ^{232}Th, and ^{238}U in the plume 6 km downwind from a coal fired power plant show that these elements are enriched over normal background levels by factors of 9, 4, and 28, respectively (*29*). These authors have assessed the lung doses from a 1000 MW coal fired power plant to be approximately 10 man-rad per year.

Table 6. Specific concentrations of several potentially carcinogenic elements in coal fly ash as a function of particle size.[a]

	Particle diameter, μm	Specific concentration, μg/g					
		Pb	Cd	Se	As	Ni	Cr
Fly ash retained in plant							
Sieved fractions							
	< 74	140	< 10	< 12	180	100	100
	44–74	160	< 10	< 20	500	140	90
Aerodynamically sized fractions							
	< 40	90	< 10	< 15	120	300	70
	30–40	300	< 10	< 15	160	130	140
	20–30	430	< 10	< 15	200	160	150
	15–20	520	< 10	< 30	300	200	170
	10–15	430	< 10	< 30	400	210	170
	5–10	820	< 10	< 50	800	230	160
	< 5	980	< 10	< 50	370	260	130
Airborne fly ash							
	> 11.3	1100	13	13	680	460	740
	7.3–11.3	1200	15	11	800	400	290
	4.7–7.3	1500	18	16	1000	440	460
	3.3–4.7	1550	22	16	900	540	470
	2.1–3.3	1500	26	19	1200	900	1500
	1.1–2.1	1600	35	59	1700	1600	3300

[a] Data of Davison (*14*).

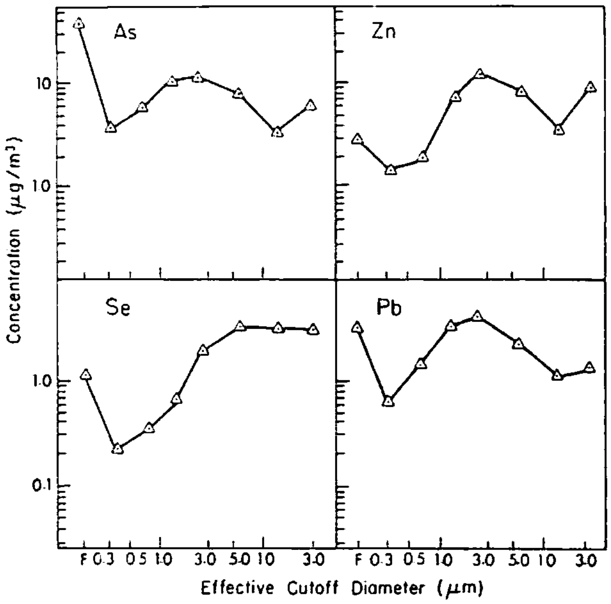

FIGURE 2. Representative aerodynamic particle size dependences of the elements As, Pb, Se, and Zn in fly ash emitted from a coal fired power plant. F refers to the final filter employed with the cascade impactor used in sampling (*23*).

Surface Association of Trace Elements

Recent results (*30*) have established that a number of trace elements, including several potential carcinogens are more highly concentrated on the surfaces of coal fly ash particles than in their interior. This phenomenon is probably due to particle surface deposition of elements volatilized during combustion and is found to occur for particles derived from a variety of high temperature combustion or smelting operations, e.g., automobile exhaust particulates and blast furnace dusts (*31*).

It is difficult to make quantitative measurements of surface concentrations. However, some semiquantitative estimates of specific concentrations of several potentially carcinogenic elements present in a shell 300 Å thick at the surface of coal fly ash particles are compared to bulk concentrations in Table 7 (*31*). It should be stressed that these data are presented primarily for the purposes of illustration and should not be regarded as definitive. This surface association is considered to be of considerable importance in determining the toxicity of trace elements in coal fly ash. The following reasons are cited. (1) Since it is the surface of a particle which comes into immediate contact with the external environment (e.g. body fluids and tissues), the surface predominance of toxic trace elements ensures their

Table 7. Estimated surface concentrations of elements in coal fly ash.

Element	Bulk concentration, μg/g	Estimated surface concentrated in 300 Å layer, μg/g
As	600	1,500
Cd	24	700
Co	65	440
Cr	400	1,400
Pb	620	2,700
S	7,100	252,000
V	380	760

ready availability. (2) Conventional bulk analyses of particulates provide a poor measure of the actual concentrations of toxic trace elements to which the external environment is exposed. This fact must be considered in designing toxicity studies using synthetic particulates. (3) Since the surface layer contains an increasing fraction of the total particle mass with decreasing size, small, lung depositing particles will have a greater proportion of their associated toxic species in immediate contact with lung tissues than will large particles, i.e., as indicated earlier, lung-depositing particles definitely constitute the most potentially carcinogenic fraction of all fly ash particles.

Solubility

Probably one of the most important properties of particulate matter emitted by fossil fueled power plants is its solubility. Indeed, unless the associated toxic chemical species can be extracted by lung fluids their ability to act as chemical carcinogens is probably negligible. Surprisingly, this point is frequently overlooked.

It is now well established that only about 2–3% of the mass of both coal and oil fly ash is soluble in water. Very little more is soluble in most dilute acids or bases. However, while the fly ash matrix is effectively insoluble, the so-called surface layer, in which many potentially carcinogenic elements are highly concentrated, is quite soluble. This is illustrated for the case of Pb in Figure 3, which shows the dependence of concentration on radial depth into coal fly ash particles before and after leaching with water (*16*).

The factors controlling the rate and extent of solubility of individual elements associated with fly ash are complex (*32*); however, it is apparent that a substantial fraction (probably ~50%) of most potentially carcinogenic elements is extractable from respirable particles.

It is appropriate here to draw attention to the distinction between the concentration and amount of a species extracted from a particle. Thus, the total amount of a given species may be quite small and unlikely to constitute a hazard. On the other hand, the localized concentration of that species may be very high (due to its surface predominance) and quite capable of causing damage in a microregion surrounding each particle. The question is whether or not such local effects are important. If not, then the surface predominance of carcinogenic trace elements may be of little consequence.

Particulate Organic Compounds

Particulate associated organic material emitted from fossil fueled power plants is known to contain both aliphatic and aromatic compounds. To date essentially all studies have been directed towards the latter class of compounds with special emphasis being given to polycyclic aromatic species which include many well established carcinogens (*2*). Even within this group, primary emphasis has been

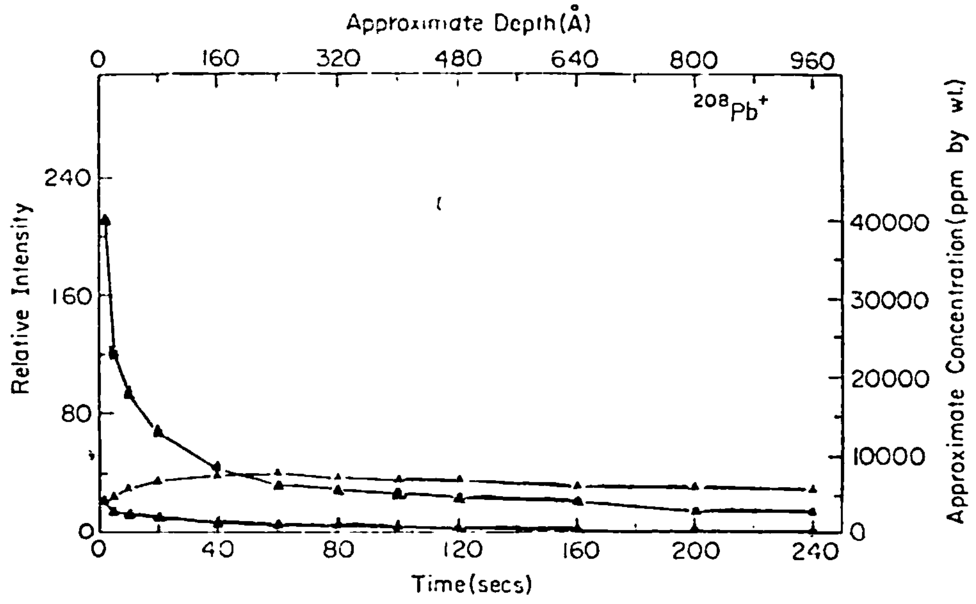

FIGURE 3. Depth profiles of Pb associated with coal fly ash recorded (*a*) before, and (*b*) after leaching the fly ash with water and dimethyl sulfoxide (*16*).

placed on hydrocarbons and little attention has been paid to heterocyclic compounds containing oxygen, nitrogen, or sulfur. Similarly, derivatives containing substituents such as carboxylic, nitro, sulfonic acid, or phenolic groups (if, indeed, they occur) have received little attention. At this time, therefore, the only polycyclic organic compounds which have been uniquely identified as being associated with fly ash emitted by fossil fuel power plants are listed in Table 8 (*15, 16, 33*). It should be noted that many more compounds have been tentatively identified but have not yet received full confirmation.

Table 8. Polycyclic organic compounds identified in stack and plume particulates from coal-fired power plants.[a]

Compound	Polycyclic organic compounds: In stack, ng/m³	In plume, ng/m³: 0–5 miles	In plume, ng/m³: 5–10 miles
Fluoranthene	2.7	5.0	4.4
Pyrene	16.4	60	9.0
Benzo[a]anthracene	69	232	14.4
Chrysene	48	68	10.8
Perylene	< 2	7.0	8.6
Benzo[e]pyrene	9.8	15.8	13.2
Benzo[a]pyrene	12.9	16.2	8.2
Benzoperylene	12	13	—
1,2,4,5-Dibenzopyrene			
3,4,7,10-Dibenzopyrene			
Phenanthrene			
Dimethylbenzanthracene			
Anthracene			
Benzo[k]fluoranthene			
9,10 dimethyl anthracene			
Benzo[b]phenanthrene			
Fluorene			
Triphenylene			

[a]Data of Stahley (*33*) and Korfmacher et al. (*34*).

A number of studies of particulate polycyclic organic matter (POM) emitted by fossil fueled power plants have concluded that total emissions are negligibly small compared with those from other sources (*2*). A summary of reported emission factors for several coal combustion operations is presented in Table 9. These figures translate to a total emission of 1 ton of benzo[a]pyrene from all coal-fired power plants in the United States. The much higher emission factors associated with hand stoked furnaces are attributed to inefficient combustion.

Table 9. POM emission factors for coal-fired furnances.[a]

Species	POM emission factors, lb/ton coal × 10⁴: Pulverized firing	Chain grate stoker	Hand fired
Benzo[a]pyrene	0.2–0.52	0.3	3520
Pyrene	0.8–1.6	3.5	5260
Benzo[e]pyrene	0–2.3	1.1	880
Perylene	0–0.6	—	526
Fluoranthene	—	6.0	8800

[a]National Academy of Sciences data (*2*).

There is now substantial evidence indicating that most, if not all, organic material remains in the vapor phase so long as the stack gases are within a power plant stack system (*15, 32, 33*). With the temperature decrease which occurs following emission to the atmosphere, however, rapid adsorption of organics onto the surfaces of co-entrained fly ash particles takes place. What this means is that fly ash retained by control equipment or collected within a power plant stack contains only a small fraction of the total organic material emitted. Conversely, emitted fly ash contains much higher specific concentrations (μg/g) of organics than the same fly ash prior to emission. In establishing POM emission factors, therefore, it is vitally important to ensure that material present in both vapor and particulate form be included when samples are collected from within a plant.

In view of the high carcinogenic potential of POM (*2*), this vapor-to-particle conversion process is of more than academic interest since it has the following ramifications.

Since polycyclic organic compounds appear to associate with fly ash by adsorption they will be present primarily on particle surfaces which can make intimate contact with lung tissues and fluids. Furthermore, preliminary indications are that extraction into solution is quite facile (*31*).

Since adsorption depends upon the available surface area of particulate adsorbent the highest specific concentrations of POM will be found associated with small particles in the respirable range. In fact size distribution studies indicate that the aerodynamic mass median diameter of benzo[a]pyrene in fly ash emitted from a coal fired power plant is around 0.1 μm (*1, 33*). In short, it is reasonable to assume that essentially all POM derived from fossil fueled power plants is capable of pulmonary deposition.

Since particulate association of POM apparently occurs primarily following emission, analysis of particulate material collected inside a power plant stack may provide a gross underestimate of POM emissions (*16*). This point is illustrated by the data in Table 8, which show that when account is taken of dilution, significantly (possibly several orders of magnitude) higher concentrations of POM are found in emitted fly ash than in that collected in a power plant stack (*33*). While there is no reason, at this time, to disbelieve the mission estimates presented in Table 9, it is of considerable importance that they be fully substantiated by additional measurements relating to modern fossil fueled power plants.

Chemical Conversion of POM

A number of studies have shown that particulate polycyclic organic species can be modified in the atmosphere as a result of photochemical decomposition or reaction with sulfur or nitrogen oxides (*2*). This is of considerable importance, since such reactions may significantly alter the carcinogenic potential of POM. Indeed, the chemical compounds actually inhaled may be quite different from those originally emitted to the atmosphere.

Recent studies (*34*) of the photochemical decomposition of several polycyclic aromatic compounds adsorbed onto the surface of coal fly ash indicate that some compounds, e.g., phenanthrene and pyrene, do not decompose appreciably under the influence of solar radiation. A second group, e.g., anthracene and benzo[a]pyrene, decompose with half lives of several hours, giving the corresponding quinone as the major product. Interesting behavior is observed in the case of fluorene, which decomposes to fluorenone in the absence of light.

Data such as these illustrate the point that estimates of the carcinogenic potential of POM emitted from fossil fueled power plants must necessarily be based on analyses of particulate material collected from the plant plume at some distance from its origin. Until the results of such analyses are available, very little can be inferred about the nature and amounts of potentially carcinogenic organic species likely to be present.

Conclusions

It is apparent from the foregoing remarks that the identities and amounts of most air pollutants emitted by fossil fueled power plants are reasonably well established. The major gap in knowledge of this type concerns the emission of particulate polycyclic organic matter (POM) which probably includes the most potentially carcinogenic species.

It is also apparent that simple knowledge of the identity of a toxic substance is scarcely adequate to enable assessment of its significance as a health hazard. This is of primary importance in the case of particulate matter for which such factors as aerodynamic size distribution and surface predominance may play a major role in determining toxicity. In this regard, the information which would be of most value is a quantitative measure of the availability of carcinogenic species associated with particles.

While there is considerable information about potentially carcinogenic species which are actually emitted from fossil fueled power plants only rudimentary knowledge is available about the changes that these species undergo prior to inhalation. Consequently, contemporary estimates of human hazards must, of necessity, be based on what is known about emitted species plus what can be inferred or guessed about the ways in which their carcinogenicity may be modified prior to inhalation.

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REFERENCES

1. Natusch, D. F. S., and Wallace, J. R. Urban aerosol toxicity: the influence of particle size. Science 186: 695 (1974).
2. National Academy of Sciences (U.S.). Particulate Polycyclic Organic Matter. Committee on Biological Effects of Atmospheric Pollutants, Division of Medical Sciences, National Research Council, National Academy of Sciences, Washington, D. C., 1972.
3. National Academy of Sciences (U. S.). Vapor Phase Organic Pollutants. Committee on Biological Effects of Atmospheric Pollutants, Division of Medical Sciences, National Research Council, National Academy of Sciences, Washington, D. C., 1976.
4. American Chemical Society. Cleaning our Environment: The Chemical Basis for Action. American Chemical Society, Washington, D. C., 1969.
5. Rhan, K. A. The chemical composition of the atmospheric aerosol. Technical report, Graduate School of Oceanography, University of Rhode Island, Kingston, R. I., 1976.
6. Schroeder, H. A. Trace metals in the air. Environment 13: 18 (1971).
7. Sax, N. I. Toxicological effects of non-nuclear pollutants. In: Atmospheric Science and Power Production. D. Randerson, Ed., US-ERDA, Washington, D. C., in press.
8. Lee, R. E., Jr., et al. National air surveillance cascade impactor network II. Size distribution measurements of trace metal components. Environ. Sci. Technol. 6: 1025 (1972).
9. National Council on Radiation Protection and Measurements. Natural Background Radiation in the United States. NCRP.
10. Shapley, D. Nitrosamines: Scientists on the trail of prime suspect in urban cancer. Science 191: 268 (1976).
11. Kertész-Sáringer, M., and Morlin, Z. On the occurrence of polycyclic aromatic hydrocarbons in the urban area of Budapest. Atmos. Environ. 9:831 (1975).
12. Lao, R. C., et al. Application of gas chromatography–mass spectrometry–data processor combination to the analysis of the polycyclic aromatic hydrocarbon content of airborne pollutants. Anal. Chem. 45: 908 (1973).
13. Goldstein, R. F., and Waddams, A. L. The Petroleum Chemicals Industry, 3rd ed. E. and F. Spon Ltd., London, 1967.
14. Davison, R. L., et al. Trace elements in fly ash: dependence of concentration on particle size. Environ. Sci. Technol. 8: 1107 (1974).
15. Natusch, D. F. S. Characterization of atmospheric pollutants from power plants. In: Proceedings of the Second Federal Conference on the Great Lakes. Great Lakes Basin Commission, 1976.
16. Linton, R. W., et al. Determination of the surface predomi-

nance of toxic elements in airborne particles by ion microprobe mass spectrometry and auger electron spectrometry. Anal. Chem., 49: 1514 (1977).
17. Skogerboe, R. K. Department of Chemistry, Colorado State University, Fort Collins, Colorado, personal communication, 1976.
18. Johnson, D. L., and Braman, R. S. Distribution of atmospheric mercury species near ground. Environ. Sci. Technol. 8: 1003 (1974).
19. Natusch, D. F. S., et al. Characterization of trace elements in fly ash. Proceedings, International Conference on Trace Metals in the Environment. Toronto, Canada, Oct. 1975. Vol. II, Part 2, p. 535.
20. McCrone, W. C., and Delly, J. G. The Particle Atlas. Ann Arbor Science Publishers, Ann Arbor, Mich., 1973.
21. Jones, H. R. Fine dust and particulates removal. Pollution Control Rev. No. 11, Noyes Data Corp., Park Ridge, N. J., 1972.
22. Bickelhaupt, R. E. Surface resistivity and the chemical composition of fly ash. J. Air Pollut. Control Assoc. 25: 148 (1975).
23. Gordon, G. E. Study of the Emissions from Major Pollution Sources and their Interaction. Progress Report Nov. 1972 to October 1974, Univ. Maryland, College Park, Md., 1977.
24. Gordon, G. E., et al. The sources and distribution of vanadium in the atmosphere. In: Trace Elements in the Environment. (Adv. Chem. Ser. No. 123) E. L. Kothny, Ed., American Chemical Society, Washington, D. C. 1973, p. 31.
25. Kaarkinen, J. W., et al. Trace element behavior in a coal fired power plant. Environ. Sci. Technol. 9: 862 (1975).
26. Bayliss, R. J., and Whaite, H. M. A study of the radium alpha-activity of coal, ash and particulate emission at a Sydney power station. Air Water Pollut. Int. J. 10: 813 (1966).
27. Pensko, J., and Stpiczynska, Z. Internal report 0-310/XIX/75, Swierk, Poland, 1975.
28. Klein, D. H., et al. Pathways of thirty-seven trace elements through a coal fired power plant. Environ. Sci. Technol. 9: 973 (1975).
29. Martin, J. E., Harvard, E. D., and Oakley, X. International Atomic Energy Association Publication STI/PUB/261, Vienna, 1971.
30. Linton, R. W., et al. Surface predominance of trace elements in airborne particles. Science 191: 852 (1976).
31. Natusch, D. F. S. Unpublished results, 1977.
32. Natusch, D. F. S. Characteristics of pollutants from coal combustion and from coal and oil shale conversion processes. In: Toxic Effects on the Aquatic Biota from Coal and Oil Shale Development, Natural Resources Ecology Laboratory, Colorado State University, Fort Collins, Colo., 1976.
33. Stahley, S. (Department of Chemistry, University of Maryland, College Park, Md.), personal communication, 1976.
34. Korfmacher, W. A., Natusch, D. F. S., and Wehry, E. Unpublished results, 1977.

Halogens, dioxins/furans

- **Halogen compounds in fuels and fuel/flue gases**
- **Chlorine-related corrosion**
- **HCl control in flue gases and fuel gases**
- **Dioxins/furans formation and control**
- **Other compounds: HF, HBr, brominated organo-halogens**

see: www.hut.fi/~rzevenho/gasbook

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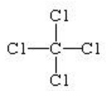
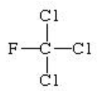
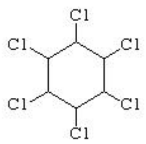
Organo-halogen compounds



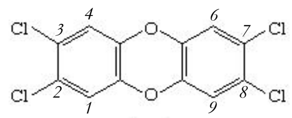
carbon tetrachloride



trichlorofluoromethane

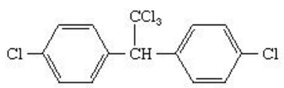


γ-benzene hexachloride (lindane)

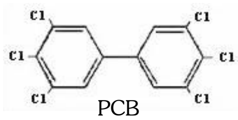


dioxin

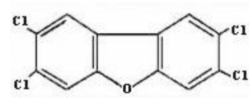
2,3,7,8 tetrachloro dibenzo - p- dioxin



DDT



PCB



furan

2,3,7,8 tetrachlorodibenzo furan

PCBs polychlorinated biphenyls

PCDDs polychlorinated dibenzodioxins

PCDFs polychlorinated dibenzofurans

with bromine: PBBs, PBDDs etc.

Halogens in fossil fuels (mg/kg)

(listed as F, **Cl**, Br)

Coal*, lignite	20 -500 / **50-2000**/0.5 -90	Light fuel oil	-
Peat	**~ 500**	Heavy fuel oil	- / **< 20**
Estonian oil shale	**~2000**	Orimulsion™	**~700**
Petroleum coke, "petcoke"	**~ 300**	Natural gas	-

* Iodine 0.5 - 1.5 mg/kg

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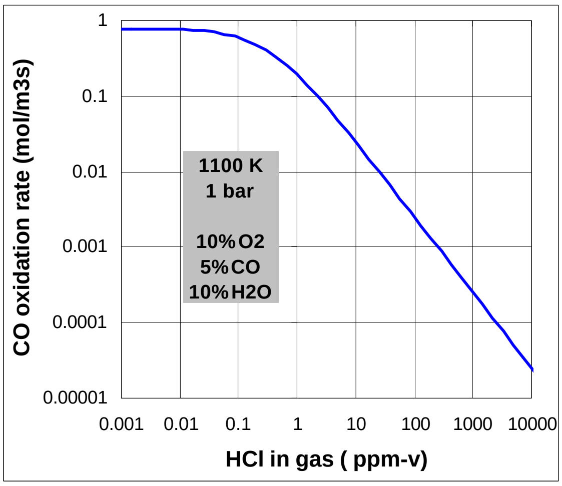
Halogens in biomass and waste streams (mg/kg)

(listed as F, **Cl**, Br)

Wood (firewood)	**0.08 - 0.13**	Munical solid waste (MSW)	0.005 - 0.025 / **0.05 - 0.25**
Bark	**0.02 - 0.4**	Refuse derived fuel (RDF)	0.001 - 0.07 / **0.3 - 0.8**
Straw	**0.1 - 1.5**	Packaging derived fuel (PDF)	0.001 - 0.012 / **1 - 4**
Landfill gas	**~50 ppmw CCl_4**	Car tyre scrap	**500 - 700**
		Auto shredder residue (ASR)	**0.5 - 2**
Textile	**~ 0.25**		
Newsprint paper	**~ 0.11**	Computer circuit boards (epoxy or phenolic resins)	**0.1 - 0.5** /2 - 6
Leather waste	**0.7 - 3**	Computer monitor housings	**~ 0.1** / ~ 2
		Electric & electronic equipment (E&E) waste plastics *	~ **3.5** / ~ 0.9
Sewage sludge	**0.03 - 1**		
		Mixed medical waste	**1 - 4**
Polyurethane foam (containing CFC11)	~ 0.7 / ~ **8**/~ 3		
PVC	**~ 50**	Black liquor solids	**0.05 - 0.2**

* Polymer market mix 1998

Oxidation rate of CO in FBC in presence of HCl



Emission standards for halogen compounds

@ 11 % O_2, dry	Power plant Finland (1990+)	MSW incinerator Finland (1994)	MSW incinerator EU (2000)	Power plant Germany (1999)	MSW incinerator Germany (1999)	Waste incinerator USA (1995)
HCl *mg/m^3_{STP}*	no standard	10	10	50	10	29.1 or 99.5% red.
HF *mg/m^3_{STP}*	no standard	1	1	2	1	no standard
PCDD/F *ng/m^3_{STP} TEQ*	no standard	1	0.1	no standard	0.1	9.63

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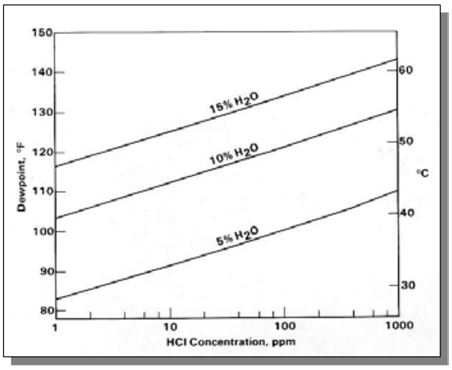
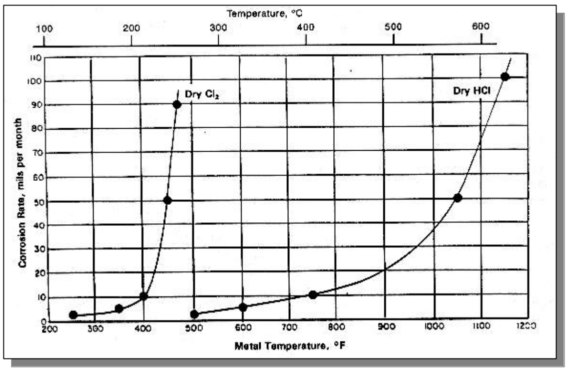
Chlorine-related corrosion #1





Dewpoint of hydrochloric acid

Corrosion rate by HCl and Cl_2

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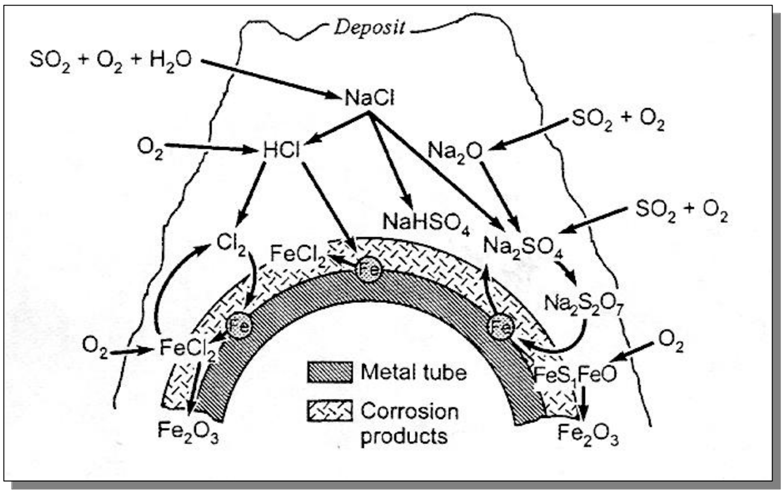
Chlorine-related corrosion #2



Important for chlorine-related corrosion:

HCl, Cl_2
NaCl, KCl,
O_2, SO_2, H_2O

Tube metals

Temperature

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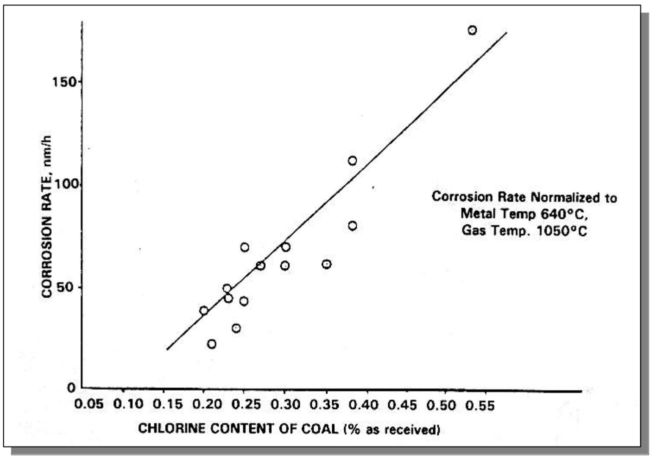
Chlorine-related corrosion #3



Corrosion rate *versus* chlorine in coal

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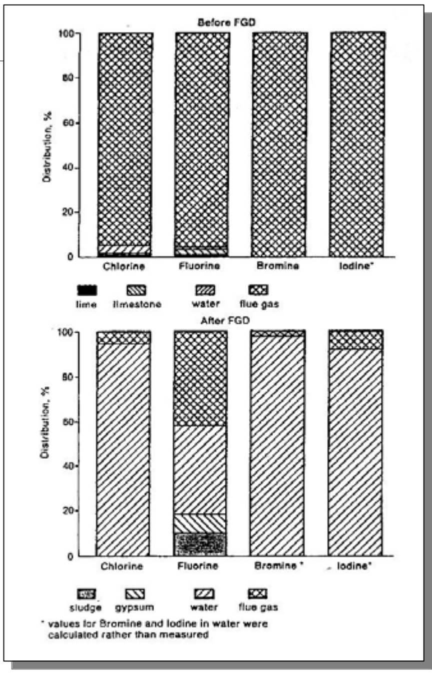
Halogen removal in FGD

(with forced oxidation)

Halogen	Conc. in coal combusted, mg/kg	Volatilisation, %	Conc. before FGD, μg/m³	Conc. after FGD, μg/m³	Removal in FGD, %
Cl	900	99	91,500	9,150	90
F	80	90	7,400	2,200	70
Br	6	60	370	20	95
I	2	90	190	40	80



Removal of HCl (& HF, HBr) from flue gases

- *Conventional, at low concentrations:*
  in wet scrubber for FGD, gives ~70% removal of HCl, HF.
  Disadvantages:
  - dissolution of SO_2 and lime/limestone are inhibited
  - HF and fly ash give AlF_x complexes in FGD (Inkoo, Finland)
  - Corrosion, deposits formation upstream

- *More suitable methods:*
  - (cold) inject alkali and collect salt particles in filter
  - (hot) injection of calcium-based sorbent in upper furnace

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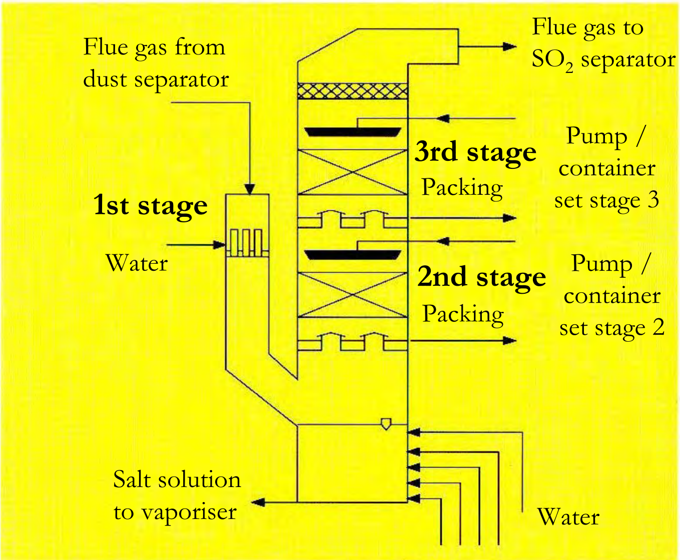


3-stage HCl scrubber, producing hydrochloric acid

gives 14-18 % HCl, which is further processed to 30-31%

Sorbents for HCl, HF, HBr (*i.e.* HX) #1

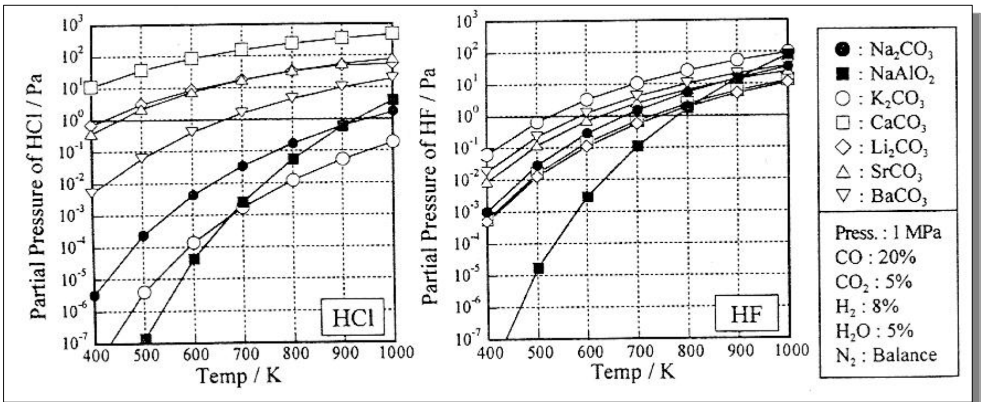
Limestone $CaCO_3$ Lime CaO Hydrated lime $Ca(OH)_2$

Nahcolite $NaHCO_3$ Soda/trona $NaHCO_3 \cdot Na_2CO_3$

Melting points of halogen salts

NaF:	988 °C ;	NaCl:	801 °C ;	NaBr:	755 °C
CaF_2:	1360 °C ;	$CaCl_2$:	772 °C ;	$CaBr_2$:	730 °C
KF:	858 °C ;	KCl:	770 °C ;	KBr:	734 °C

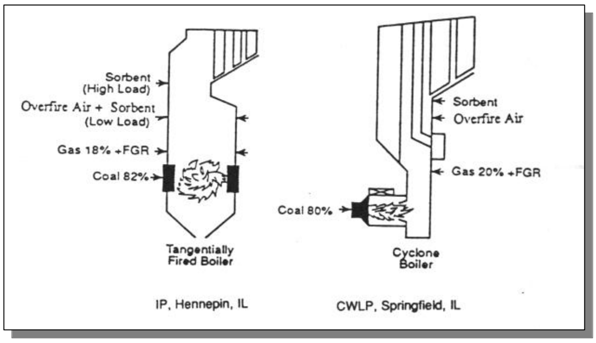
Sorbents for HCl, HF, HBr (*i.e.* HX) #2



Potassium salts : high vapour pressures for KF, KCl, KBr

Removal of HCl and HF from pulverised coal combustion flue gas (Illinois, US, 1993)

Hydrated lime injected into a coal-fired boiler at Ca/S=1.66, 3%-wt sulphur in fuel
Injected into upper furnace at ~1250°C



Chemistry :

$Ca(OH_2)$ ® $CaO + H_2O$

$CaO + 2\ HCl$ ® $CaCl_2 + H_2O$

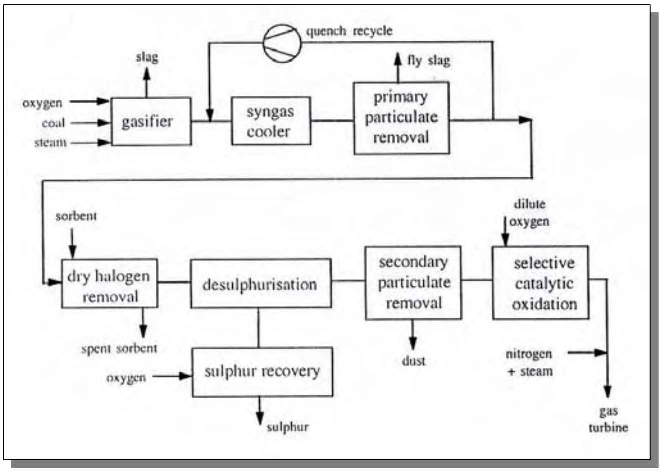
$CaO + 2\ HF$ ® $CaF_2 + H_2O$

Results :

HCl 63-86% removal, from 660 ppmw

HF 94-99% removal from 49 ppmw

Halide removal (HCl, HF) from IGCC raw fuel gas at ~400°C

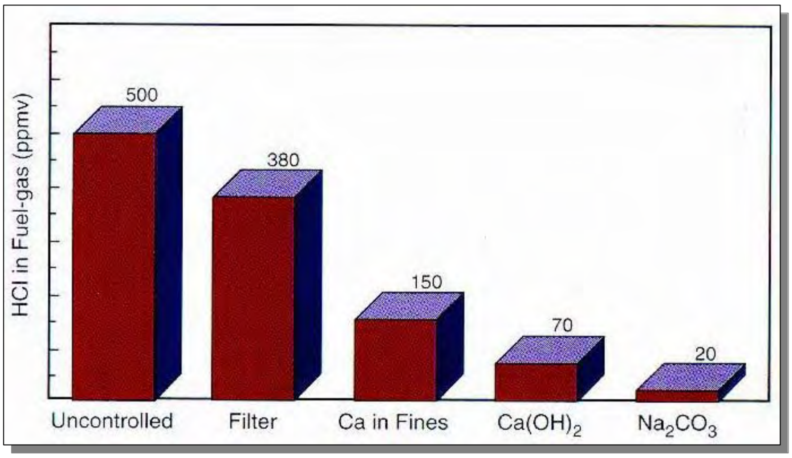


Buggenum IGCC
HCl ~ 600 ppm
HF ~ 220 ppm

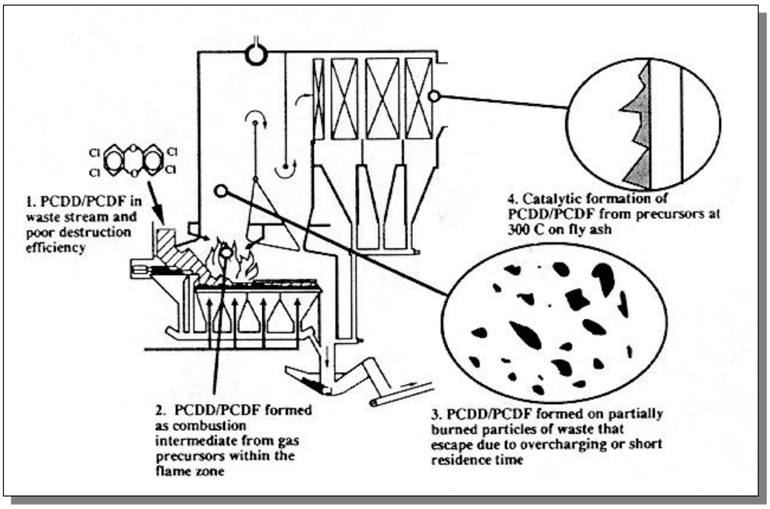
Texaco IGCC
HCl ~ 500 ppm
HF ~190 ppm

for coal,
0.2 % Cl, 0.04 % F

Removal of HCl from flue gas with various sorbents



Formation of dioxins / furans #1



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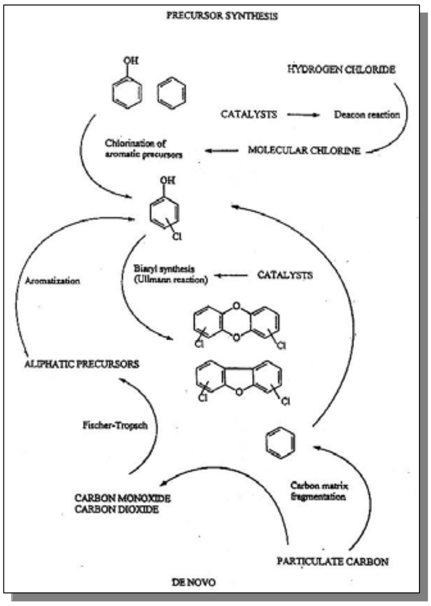

Formation of dioxins / furans #2

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"De Novo" dioxins / furans formation

Depends on 5 major factors :

1. The cooling rate of the flue gas, especially around 300°C
2. The amount of fly ash
3. The presence of trace elements, especially Cu and Pb
4. The carbon and chlorine content of the fly ash
5. The presence of free oxygen

Radical reactions are competing with $Cl + OH$ ® $HCl + O$, $OH + H$ ® H_2O; $CO + OH$ ® $CO_2 + H$

giving apparently lower stoichiometry, giving more soot and C_xH_y

Deacon reaction : $2HCl + ½ O_2 <=> Cl_2 + H_2O$

catalysed by Cu, Pb, Sn, ... ; reaction equilibrium to Cl_2 below ~500°C

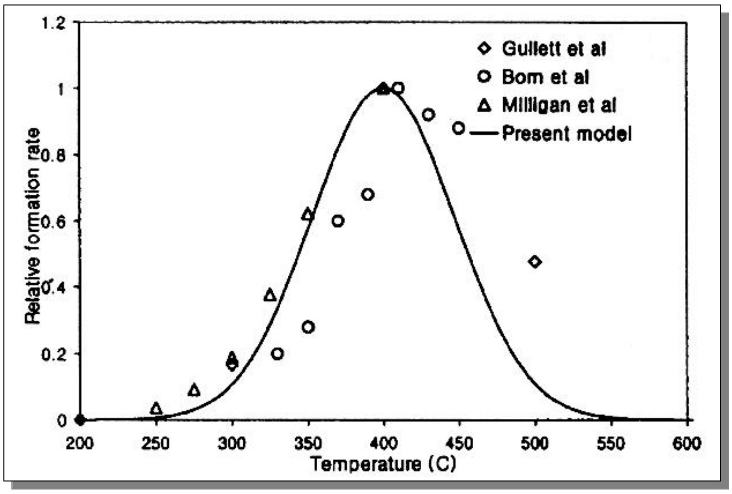
$Cl_2 + O_2 + C_xH_y$ + time @ 250-350°C ® PCDDs/Fs

Equivalence schemes for PCDD/Fs

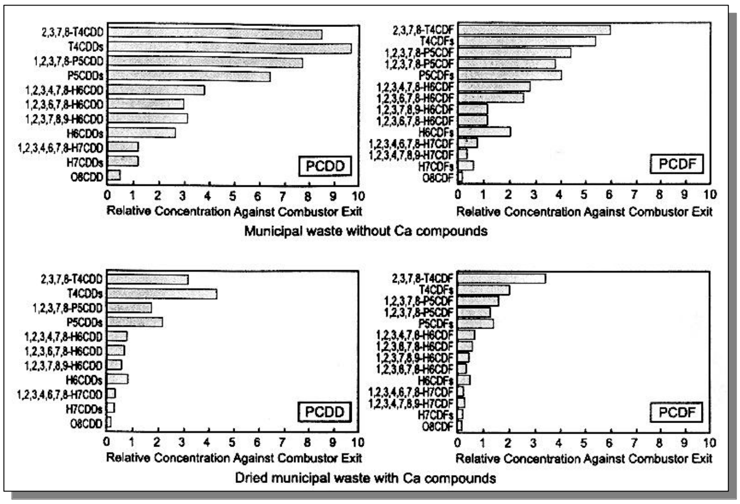
Dioxin	I- TEF	Furan	I - TEF
2,3,7,8-TCDD	1	2,3,7,8-TCDF	0.1
1,2,3,7,8-PCDD	0.5	1,2,3,7,8-PCDF	0.05
1,2,3,4,7,8-HxCDD	0.1	2,3,4,7,8-PCDF	0.5
1,2,3,6,7,8-HxCDD	0.1	1,2,3,4,7,8-HxCDF	0.1
1,2,3,7,8,9-HxCDD	0.1	1,2,3,6,7,8-HxCDF	0.1
1,2,3,4,7,8,9-HpCDD	0.01	2,3,4,6,7,8-HxCDF	0.1
1,2,3,4,6,7,8,9-OCDD	0.001	1,2,3,7,8,9-HxCDF	0.1
		1,2,3,4,6,7,8-HpCDF	0.01
		1,2,3,4,7,8,9-HpCDF	0.01
		1,2,3,4,6,7,8,9-OCDF	0.001

International Toxic Equivalence Factors (I-TEF) (NATO, 1988) standardize the toxicity of the dioxins and furans, to derive a toxic equivalence as 2,3,7,8-TCDD. The I-TEF for the dioxins and furans without chlorine atoms at the 2, 3, 7, and 8 positions is zero.

Rate of *de novo* PCDD/F formation



Effect of calcium-based sorbents on PCDD/F release from an FB waste combustor



Emission control for PCDD/Fs

- Carbon injection*
- Fixed bed carbon absorption + SNCR
- SNCR + carbon injection*
- Lime / char adsorption
- SCR catalytic oxidation
- SCR catalytic oxidation + carbon injection*

* collected downstream in (a separate) dust control system

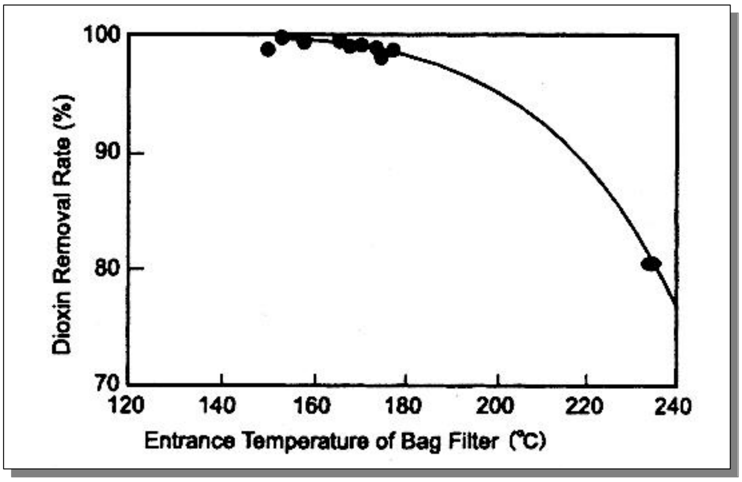
also for PCBs, brominated compounds (PBBs, PBDD/Fs)

Dioxins/furans control for waste incinerators

(MSW = municipal solid waste)

process	PCDD/Fs from furnace ng/m^3_{STP}	gas clean-up system	PCDD/Fs removal efficiency %
5 incinerators for RDF or MSW	43 - 2157	wet scrubber + fabric filter	> 95.7
3 incinerators for MSW	28 - 783	SCR + wet scrubber + fabric filter	87.7 - 99.6
pilot incinerator for MSW	87 - 2277	sorbent injection + fabric filter	> 99.55
MSW incinerator	170	wet scrubber + ESP	64.3

PCDD/F removal by a bag filter : effect of entrance temperature

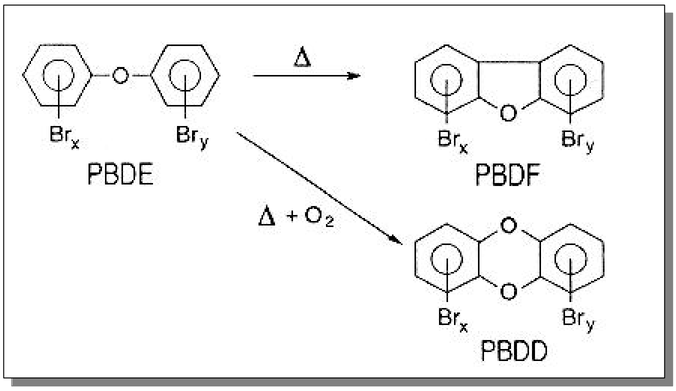


Other halogens #1: control of HF + HCl

Process*	Temperature at outlet EC	HF removal %	HCl removal %
dry sorbent injection + fabric filter	160 - 180	98	80
spray dryer absorber + ESP	140 - 160	99	> 95
spray dryer absorber + fabric filter	140 - 160	99	> 95
spray dryer absorber + dry sorbent injection + ESP or fabric filter	~ 200	99	> 95
ESP + wet scrubber	104 - 122	99	> 95
spray dryer + west scrubber + ESP or fabric filter	104 - 122	99	> 95

* sorbent = sodium- or calcium- based sorbent

Other halogens #2: formation of brominated dioxins/furans (PBDD/Fs) from PBDE flame retardants



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COMBUSTION and GASIFICATION in FLUIDIZED BEDS

Prabir Basu

CRC Taylor & Francis
Taylor & Francis Group
Boca Raton London New York

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5.3 NITROGEN OXIDE EMISSION

Nitrogen oxides are some of the major air pollutants emitted by coal-fired boilers. Uncontrolled NO_x emissions from conventional PC-fired boiler are in the range of 0.8 to 1.6 mg/MJ. Strict legislation (Table 5.4) is being considered or has been implemented by many countries that restrict the emission of nitrogen oxides. The designer of a fluidized bed boiler is required to ensure that the emission level is below the regulatory guidelines. If the operator uses innovations like a low NO_x burner, over-fire air or reburn, the NO_x might be reduced by 20 to 79%. If ammonia is injected as in selective noncatalytic reactors (SNCR), the NO_x emissions may reduce by 20 to 50%. The greatest reduction is obtained by the use of a selective catalytic reducer (SCR) downstream of the boiler, where ammonia is injected just prior to passing the flue gas over a stack of catalyst. The SCR can reduce the emission by 80 to 95%, but it is a relatively expensive retrofit and needs replacement of expensive catalysts. The following section describes the mechanism of formation (or destruction) and the effect of operating parameters on nitrogen oxide emission from BFB or CFB boilers. Section 5.4 discusses emission of the other oxide of nitrogen, N_2O.

5.3.1 Sources of NO_x

The symbol NO_x represents nitric oxide (NO) and nitrogen dioxide (NO_2). Amongst these, nitric oxide is the major product of coal combustion, and therefore most of the discussion will center on this compound.

Nitric oxide is formed through oxidation of the following:

- Atmospheric nitrogen (giving thermal NO_x)
- Fuel-bound nitrogen (giving fuel NO_x)

During combustion, the nitrogen of the combustion air is oxidized to thermal NO_x, but it is significant only above 1540°C (Morrison, 1980). Thus, it is a minor contributor (< 10%) to the NO_x generated in fluidized bed boilers, where the combustion temperature rarely exceeds 900°C.

The nitrogen content of coal is typically 1 to 2% on a dry, mineral-free basis and it comes from the volatiles and the char of the coal. The possible reaction path towards the formation of NO from the coal is shown in Figure 5.12. It assumes that the fuel nitrogen is equally (50%) distributed between the char and volatiles.

The char nitrogen is oxidized to NO through a series of reactions. The volatile nitrogen appears as NH_3 or HCN. Ammonia (NH_3) may decompose into NO being catalyzed by CaO or char, while the HCN is primarily converted into N_2O (Moritomi and Suzuki, 1992). Approximately 77% of the fuel nitrogen is oxidized to NO by the above reactions (Johnsson, 1989), and the rest appears as NH_3, which in turn is partly converted to nitrogen (Figure 5.12). Thus with a series of parallel-consecutive reactions, NO is formed by the oxidation of volatile nitrogen (Sarofim and Beer, 1979). Part of the NO formed above is also reduced back to nitrogen.

A large number of complex chemical reactions are involved in the formation and destruction of nitric oxide from either char or volatiles. Some of these reactions are catalyzed by calcined limestone (CaO), spent limestone ($CaSO_4$), and char. A list of the probable reactions and their rate constants is given by Johnsson (1989). The contributions of each reaction to the formation of NO or its subsequent destruction are not equal.

5.3.2 Methods of Reduction of NO_x Emissions

The generation of NO_x in a combustion system can be reduced somewhat through suitable modifications of the system. These modifications are discussed below.

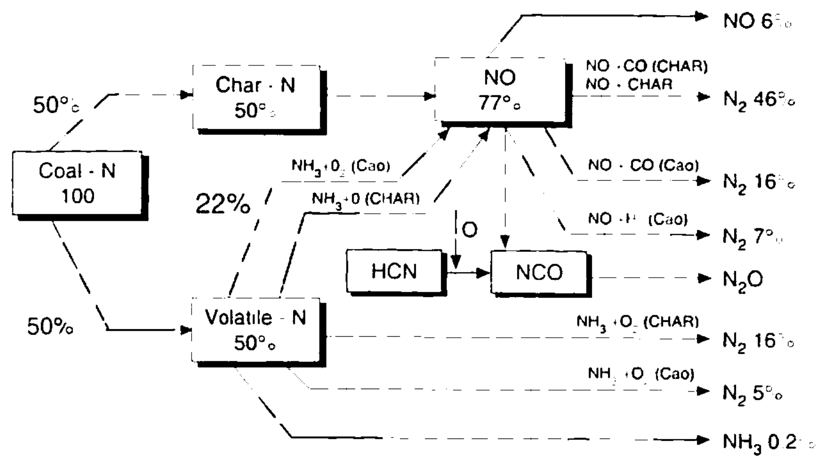


FIGURE 5.12 Relative importance (percentages of total fuel nitrogen involved) of different reaction paths in the formation and reduction of nitric oxide are indicated through numerical figures. Char and calcium oxide catalyzes some reactions as indicated within brackets

5.3.2.1 Lowering of Combustion Temperature

Low combustion temperature inhibits the oxidation of the nitrogen in the combustion air to thermal NO_x. Thus, the generation of thermal NO_x is negligible in the temperature range of 750 to 900°C. The amount of NO_x generated from fuel nitrogen is also found to decrease with temperature (Figure 5.13 and Figure 5.14).

5.3.2.2 Staging Air

Instead of feeding all the combustion air through the bottom of the furnace, part of it can be added at a section further downstream in the furnace. Such staging of combustion air has a significant beneficial influence on the reduction of NO_x emissions, especially for highly volatile coals.

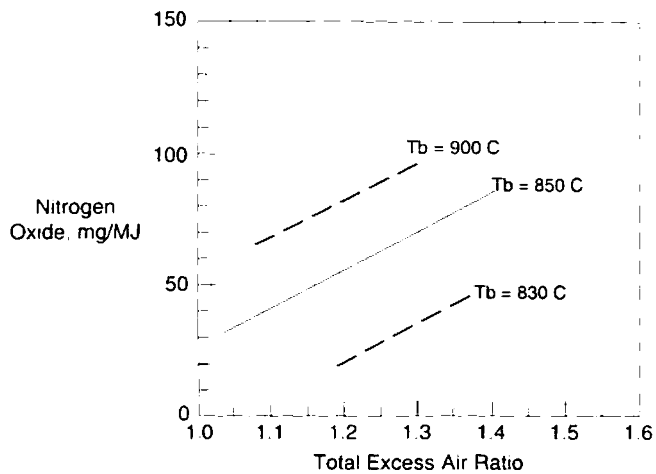


FIGURE 5.13 NO_x emission increases with excess air ratio as well as with combustion temperature.

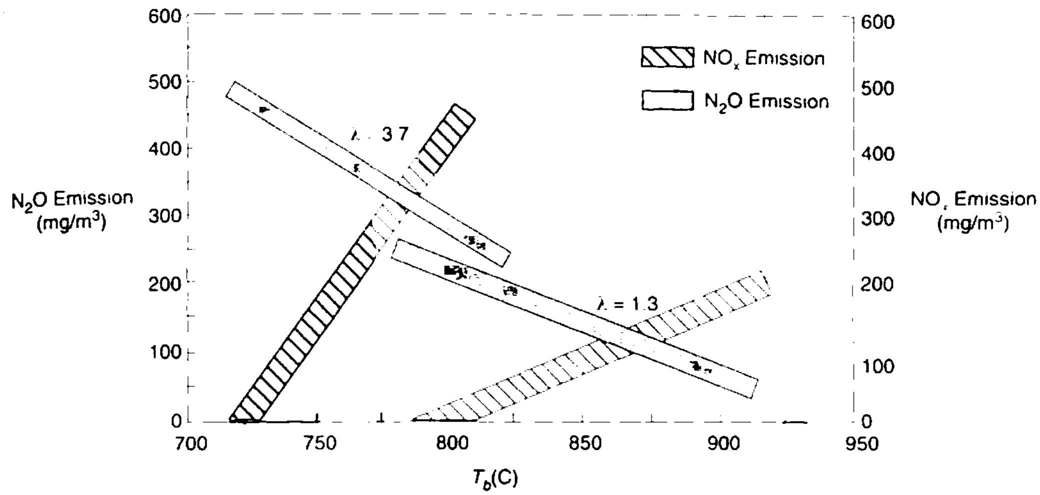


FIGURE 5.14 Dependence on the emissions of N_2O and NO_x of the combustion temperature of a fluidized bed burning low-volatile bituminous coal. Results are shown for two excess air λ = 1.3 and λ = 3.7. Thickness of the line shows the scatter of the data points. (Adapted from Braun, 1987.)

Insufficient combustion air passing through the bottom of the furnace helps the nitric oxide to be reduced by char and CO in the lower zone. A low NO_x burner in a PC boiler, working on this principle, can reduce NO_x by 40 to 50%.

5.3.2.3 Injecting Ammonia

Injections of ammonia (NH_3) into the upper section of the furnace or the cyclone of a CFB boiler have proven successful in further reduction of NO_x emissions. However, there is some danger of NH_3 escaping into the solid waste or flue gas creating additional hazards. Combustion of chlorine-bearing coal may emit ammonium chloride through the stack. Therefore, the NH_3 injection should be carefully monitored.

5.3.2.4 Lowering Excess Air

The effect of excess air on the NO_x emission from a commercial CFB boiler is shown in Figure 5.13. The NO emissions are reduced significantly when the excess air is reduced. For example, Hirama et al. (1987) noted that the NO emission from a CFB boiler reduced from 150 to 80 ppm when the excess air was reduced from 30 to 10%.

5.3.3 NO_x Emission from CFB

The mechanism of NO_x emission from CFB boilers is different from that of BFB boilers, and this difference is responsible for a lower level of emission (Hirama et al., 1987) from the former. Even without the staging of air, the NO is found to be progressively reduced to N_2 by the unburnt carbon in the furnace of a CFB boiler. Table 5.6 compares the capture efficiency of NO_x and SO_2 from CFB and BFB boilers. The nitric oxide emission from the BFB boiler is about twice that from the CFB boiler.

Very little ammonia or CO is available in the furnace to assist the reduction of NO. It is interesting to note that if the bed material contains calcined limestone, the trend is reversed.

Calcium oxide catalyzes the oxidation of NH_3 in coal volatiles to NO. Thus, NO increases with bed inventory in the presence of calcined limestone. However, the catalytic activity ceases when the calcium sulfate concentration exceeds 10%. In that case, NO does not increase with the bed inventory.

5.4 NITROUS OXIDE EMISSION

Nitrous oxide, N_2O does not have much direct adverse effect on our immediate environment, but it affects the ozone layer in the stratosphere and traps heat causing global warming. The information available now to elucidate its mechanism of formation and the exact magnitude of its effect is far from complete. The present section will, however, present a brief discussion based on information available to date.

5.4.1 Mechanism of Formation of N_2O in CFB

The mechanism of formation of N_2O in a coal-burning fluidized bed is not understood as well as it is for a gaseous flame. In gaseous flames, the intermediate combustion compound HCN is an important source of N_2O.

$$HCN + O \rightarrow NCO + H$$

$$NCO + NO \rightarrow N_2O + CO \tag{5.35}$$

However, the nitrous oxide formed is immediately destroyed by its reaction with hydrogen radicals (Amand and Andersson, 1989).

$$N_2O + H \rightarrow N_2 + OH \tag{5.36}$$

The extent of destruction of N_2O increases with the reaction temperature.

Nitrous oxide may also be produced through:

1. Reduction of nitric oxide by carbon in char:

$$Char + 2NO \rightarrow N_2O + CO$$

2. Direct oxidation of char nitrogen during combustion:

$$Char\ N + O_2 \rightarrow N_2O \tag{5.37}$$

In the range of 800 to 900°C, the rate of formation of nitrous oxide from char nitrogen is proportional to the combustion rate of char (deSoete, 1989). However, experiments at higher temperatures (>900°C) in pulverized coal flames found negligible contribution of char nitrogen oxidation or NO reduction by char carbon to the total nitrous oxide emission (Kramlich et al., 1988).

5.4.1.1 Level of Emission

The nitrous oxide emission from CFB boilers is in the range of 50 to 200 ppm (Moritomi et al., 1990). In a typical pulverized coal-fired boiler, N_2O emission is in the range of 1 to 20 ppm because of the higher combustion temperature of the PC boiler.

Harada (1992) observed that the emission of N_2O in a bubbling fluidized bed firing low-volatile coal decreased from 250 to 75 mg/m^3 when the combustion temperature increased from 800 to

900°C, but the NO_x emission increased from near 0 to 200 mg/m^3. Interestingly, the sum of NO_x and N_2O decreases only slightly with increasing temperature.

5.4.2 Effects of Operating Parameters on N_2O

5.4.2.1 Combustion Temperature

Combustion temperature has the dominant effect on the emission of NO_x and N_2O. High temperature is favorable to the thermal decomposition of N_2O, so at high temperature (800 to 900°C) one finds a rise in NO_x and a fall in N_2O emission. At higher temperatures, the char concentration is lower due to its higher burning rates. Thus, there is less reduction of NO_x to molecular nitrogen. Figure 5.14 shows that while the NO_x emission from a bubbling fluidized bed increases with temperature, the N_2O decreases continuously.

An important observation made in a CFB furnace (Amand and Andersson, 1989) was that the concentration of N_2O increased along the height of the CFB combustor, while the concentration of NO decreased continuously along the height of the combustor. Unlike the emission of NO, that of N_2O is greater at lower combustion temperatures.

5.4.2.2 Effect of Volatiles

Higher volatile content of the fuel decreases the N_2O formation, but increases the NO_x formation. Harada (1992) observed that in a bubbling fluidized bed, the sum of N_2O and NO_x remains nearly constant in the range of 800 to 900°C. Low-volatile coal gives higher carbon content in beds, creating a more favorable condition for the reduction of NO_x into molecular nitrogen, which is a precursor for N_2O.

Biomass fuel was found to have exceptionally low emissions of nitrous oxide in both CFB and BFB boilers (Leckner et al., 1992). Co-firing of coal, however, produced high N_2O emission.

5.4.2.3 Effect of Excess Air

For a given excess air, splitting the air into primary and secondary parts generally results in a decrease in emissions of both NO_x and N_2O because the oxygen deficient, substoichiometric condition helps reduce nitrogen oxides into molecular nitrogen. The NO_x emission also shows significant dependence on the total amount of excess air as shown in Figure 5.14. Additionally, this figure shows that although N_2O emission also increases with excess air, the increase is not significant between excess air coefficients of 1.3 and 3.7 at the same operating temperature.

5.4.2.4 Effect of Limestone

The presence of CaO helps reduce the NO_x in a CFB furnace, but it is not very effective in the case of a BFB furnace (Leckner and Amand, 1987). It is apparently due to the presence of a substoichiometric zone in CFB boilers and its absence in BFB boilers.

The higher catalytic effect of CaO on the destruction of N_2O at higher temperatures is another reason for lower N_2O at higher temperatures.

5.4.2.5 Effect of NH_3 Injection

Ammonia injection helps reduce NO_x emission when used in a narrow temperature range around 870°C (McInnes and Van Wormer, 1990) and is therefore used when very low NO_x emission is required. However, it increases N_2O formation. The injection of ammonia on catalysts brings about significant reduction in NO_x emissions. It is in fact the basis of operation for selective catalytic reducers (SCR)s.

5.4.3 Reduction of N_2O

Afterburning in the cyclone of a CFB boiler is a good technique for reduction in N_2O emission. Gustavsson and Leckner (1995) burned gas in the cyclone to raise the cyclone flue gas temperature and it reduced the N_2O emission from 150 to 30 ppm.

Only a small part (5%) of the nitrogen in char is converted to nitrous oxide, but its reduction on the char surface is faster than that of NO reduction (deSoete, 1989). Unlike NO reduction, N_2O reduction is independent of CO concentration. The conversion of the coal nitrogen into N_2O depends on the devolatilization process. It has been observed (Freihaut and Seery, 1981) that when coal is heated at a moderate rate up to 900°C, only a small part of the coal nitrogen appears as HCN, which is the major source of N_2O. Thus, control of the coal devolatilization rate may provide some clue to the reduction of nitrous oxide in CFB boilers. Feeding the coal in areas of the CFB loop having a lower heat-transfer rate may delay the devolatilization process.

5.5 MERCURY EMISSION

The emission of mercury has received much attention. Some countries are contemplating enforcing 90% capture from coal-fired power plants within a specified period of time.

Several options for mercury capture are used. The options can be classified under three groups (ICAC, 2005): sorbent injection, electro-catalytic oxidation, and precombustion technique.

5.5.1 Sorbent Injection

This is the most popular method. Sorbents are injected into the combustion gas to absorb gaseous mercury. These sorbents capture the gaseous mercury to retain it in solid form, and are then captured downstream in a particulate capture device like a bag-house or ESP. The sorbents could be:

1. activated carbon
2. bromine
3. polysulfide

In some cases, SCRs (used for NO_x control) or wet scrubbers (used for SO_x control) are also found to capture significant amounts of mercury.

Another approach involves the addition of some chemicals that will oxidize elemental gaseous mercury into solid compounds and make it easier to capture. Such mineral-based reagents would be cheaper than the activated carbon traditionally used for capturing mercury.

5.5.2 Electro-Catalytic Oxidation

This technique is a multicontrol technology. It can reduce the emissions of NO_x, SO_2, particulate matter, and mercury simultaneously. It consists of a discharge reactor, ammonia-based wet scrubber, and a wet electrostatic precipitator. The whole unit is located downstream of the existing ESP or fabric filter of the plant. The barrier discharge reactor oxidizes NO_x, SO_2, and H, while the ammonia-based wet scrubber removes NO_x, SO_2 and oxidized mercury creating an ammonium sulfate/nitrate solution. The wet ESP captures acid aerosols, fine particulates, and the oxidized mercury. The solution is sent to a filtration system to separate spent mercury and spent activated carbon for disposal as hazardous waste. The other part of the solution can be used in fertilizer.

5.5.3 Precombustion Technologies

Some proprietary processes are available (K-fuel) which can wash the coal of its pollutants, but the mercury removal is in the range of 70% instead of 90% as in other methods.

There is another consideration for the mercury in solid residues. Its concentration is highest in fly-ash with about 0.33 ppm, followed by FGD waste with about 0.22 ppm. Thus the disposal of these solid residues from a power plant using mercury control technology needs careful planning to prevent reemission of the mercury into the atmosphere.

5.6 CARBON MONOXIDE EMISSION

When carbon monoxide is inhaled, it displaces oxygen in the blood. Oxygen deprivation can be especially dangerous for the heart and brain tissues. CO, particularly in urban areas, comes primarily from automobiles. The emission of carbon monoxide from fluidized bed boiler plants is not generally perceived to be a major problem, and is normally below the statutory limit. The emission depends on the fuel composition and the combustion temperature. The CO level in the flue gas increases with decreasing combustion temperature, particularly below 800°C. Typical levels of emission are in the range of 40 to 300 ppm (Brereton, 1997), as compared to 200 to 400 ppm in stoker-fired boilers.

5.7 CARBON DIOXIDE EMISSION

Carbon dioxide, being the most important greenhouse gas, has received the greatest attention in terms of emission control. Release of carbon dioxide per unit power produced is an important index of a plant's performance. Table 1.3 compares the CO_2 emissions of plants using different technological options.

Carbon intensity, which is the amount of carbon released during combustion, is highest for coal, followed by oil and gas. For efficient combustion, all the carbon is oxidized into carbon dioxide. Sulfur capture requires the use of limestone in a fossil fuel-fired boiler, which produces additional amounts of carbon dioxide from the calcination reaction of limestone (Equation 5.6). The operation of a BFB boiler involves calcination of 3 to 4 times the limestone actually consumed in capturing the sulfur, while emitting an equivalent amount of extra carbon dioxide into the atmosphere. A CFB, on the other hand, needs about twice the stoichiometric amount. This aspect, as well as higher nitrous oxide emissions, makes fluidized bed boilers less attractive from a climate change point of view especially if they use limestone for sulfur capture. The problem is not as severe for fluidized bed boilers firing low-sulfur fuels which do not use limestone. If one takes a total picture of the powerplant, the comparison with a pulverized coal-fired boiler with FGD, SCR, etc., may not be as pessimistic. Higher auxiliary power consumption by mills and FGD also require additional CO_2 emission for the same net power output (Miller, 2003).

Less use of limestone means less production of CO_2 as every mole of limestone produces one mole of CO_2. Considerable effort has been made to reduce the calcium-to-sulfur ratio by using techniques like rehydration of sorbents, injection of water or steam into flue gas leaving the boiler with fly ash, and the use of synthetic sorbents. There is also the potential of using a carbonate cycle where the reverse of Equation 5.6 could be forced at a lower temperature (<750°C) to absorb CO_2 at $CaCO_3$.

$$CaO + CO_2 = CaCO_3 + \text{heat} \tag{5.38}$$

The chemical looping cycle, though still in the stage of laboratory-scale research, holds high promise of reduction of CO_2 emission from conventional fluidized bed plants. The best and the least expensive approach for reduction would be the use of higher efficiency combined- or hybrid-cycle discussed in Chapter 1.

5.8 EMISSION OF TRACE ORGANICS

Fluidized beds are also used for incinerating waste products, which are sometimes hazardous. Dichlorinated benzene and PCBs are some of the items that can be destroyed in fluidized bed incinerators. In order to provide the necessary high-temperature residence time, the incinerators are operated at high temperatures.

Desai et al. (1995) found the dioxin concentration in the flue gas from a PCB incinerator to be in the range of 3 to 42 ng/m^3. This level, being above the statutory limit of 0.1 to 1 ng/m^3 a dry scrubber is needed, which allows removal of the dioxin and furan by 99.9% (Brereton, 1997). Scrubbers are also required for removal of HCl, which can be captured by the CaO in the cooler (< 650°C) section of the incinerator.

Co-combustion of coal and waste products could help reduce the emission of dioxin below the statutory limit especially in presence of sulfur in the fuel.

5.9 PARTICULATE EMISSION

In any boiler, ash of a fuel is split into two streams. The coarser fraction is drained from the bed as bottom ash, and the finer fraction leaves the furnace as fly ash to be collected by downstream particulate collection equipment like a fabric filter or electrostatic precipitator. The amount of fuel ash that appears as fly ash in a fluidized bed boiler is generally lower than that in a pulverized coal-fired boiler because a sizeable part of the ash in the former appears as bed drain. In a typical PC boiler, more than 80% of the fuel ash appears as fly ash, while only a small to negligible fraction appears as bottom ash. The fly ash from fluidized bed boilers without limestone addition is in the range of 40 to 80%. The split of ash between bed ash and fly ash depends on:

- feed-size distribution
- dispersion of ash in the coal (intrinsic or extraneous)

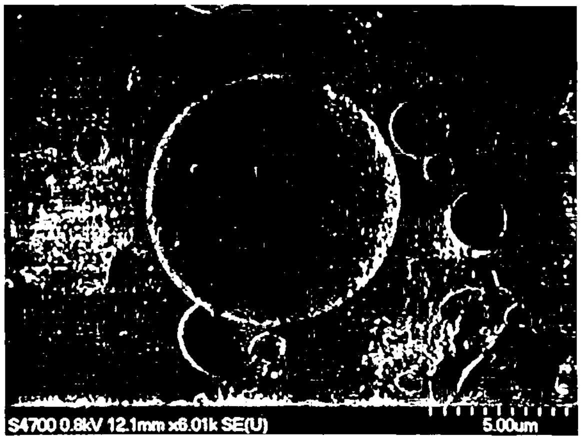
The ash in a fluidized bed is generated at 800 to 900°C. Therefore, it does not melt but remains rough edged, maintaining the original shape of the mineral matter in the ash. The ash in a PC-fired boiler, on the other hand, is produced at 1000 to 1500°C. PC ash therefore melts and, owing to its surface tension, assumes spherical shape. Figure 5.15 shows scanning electron microscope photographs of fly-ash samples from both CFB and PC boilers. The spherical shapes of the PC ash and irregular shapes of the CFB ash are clearly visible from this picture.

5.9.1 ASH CHARACTERISTICS

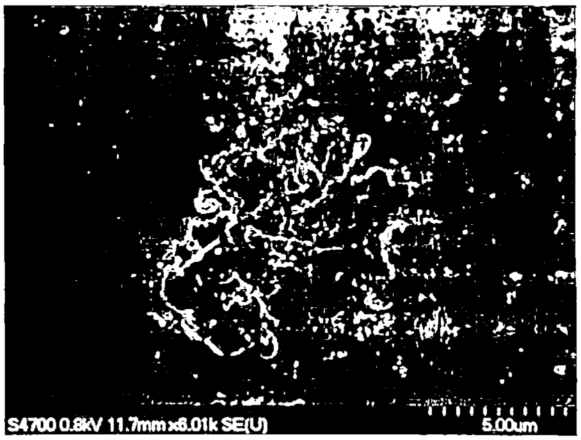
Oka (2004) reasoned that since the ash generated in a BFB boiler is entrained at a lower velocity than that for PC boiler only the finest particles appear as fly ash in a BFB boiler. The mean diameter of fly ash particles in a BFB boiler is in the range of 3.0 to 5.0 μm, while that in a PC boiler is in the range of 5.0 to 8.5 μm. Table 5.8 presents a comparison of physical characteristics of fly ash from PC and BFB boilers as outlined below:

Higher specific surface area and higher porosity favor the use of fluidized bed fly ash for concrete and cement applications. Finer size also helps its application in cement.

Oka (2004) suggests that the rough edges of the fluidized bed boiler ash increase the hydrodynamic resistance of the cakes formed on bag filters. Thus a fluidized bed boiler may need lower filtration velocity in the bag than would a PC boiler with smooth ash particles. Table 5.8 shows the filtration velocities recommended by Oka (2004) for BFB and PC boilers. The filtration velocity for BFB fly ash is less than half of that for PC fly ash, so a BFB boiler might need a larger bag-house than a PC boiler.



Fly ash from Pulverized coal fired boiler



Fly ash from Circulating fluidized bed boiler

FIGURE 5.15 Scanning electron microscope photographs of samples of fly ash from both CFB boiler and a PC boiler.

Fluidized bed boilers with limestone injection are likely to have less sulfur in the ash. Thus, in the design of electrostatic precipitators, one needs to take note of the higher resistivity of fluidized bed boilers with sulfur-capture systems. This would require large plate area.

TABLE 5.8
Comparison of Design Parameters for Particulate Control Devices for Fluidized Bed with Limestone Injection and Pulverized Coal Fired Boiler

Properties	BBF boiler	PF boiler
Specific surface area, m^2/gm	5–20	1.0–4.0
Bulk porosity ε	82–84%	58–75%
Filtration velocity, m^3/min/m^2	0.15–0.4	0.5–0.8
Specific dust loading, Kg/m^2	1.5–2	2.5–5
Ash resistivity, Ohm. cm	1011–1013	1010

Source: Data collected from Oka, 2004.

MidAmerican
ENERGY
OBSESSIVELY, RELENTLESSLY *AT YOUR SERVICE.*

MidAmerican Energy
666 Grand Avenue
P.O. Box 657
Des Moines, Iowa 50303-0657

September 25, 2005

Dave Phelps
Construction Permits
IDNR, Bureau of Air
7900 Hickman Road, Suite 1
Urbandale, IA 50322

Subject: Prevention of Significant Deterioration (PSD) Permit Application for the Council Bluffs Energy Center Unit 4

Dear Dave:

As you are aware, MidAmerican Energy Company is proposing to construct and operate a coal-fired electric generation facility referred to as the Council Bluffs Energy Center Unit 4. The facility will be located at MidAmerican's Council Bluffs Energy Center in Council Bluffs, Iowa. Construction of the proposed 750 MW coal-fired facility is proposed to start in June 2003, with commercial operation proposed for June 2007.

MidAmerican Energy Company is submitting the attached Prevention of Significant Deterioration (PSD) Permit Application for the Council Bluffs Energy Center Unit 4. The submittal includes two copies of the PSD application for DNR, and three copies have been included for distribution to Nebraska DEQ, Omaha Public Works, and Region VII EPA. Additionally, the PSD application includes a CD with the modeling results for the proposed facility.

Please contact me at (515) 281-2692 with any questions or comments regarding the PSD submittal.

Sincerely,

Steve Guyer
Director Environmental Services

Cc: Cathy Woollums

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SECTION 1.0

Introduction

MidAmerican Energy currently operates the Council Bluffs Energy Center (CBEC) site located south of Council Bluffs in Pottawattamie County, Iowa. The plant currently consists of three coal-fired electric generating units designated as Units 1, 2, and 3, with a combined net generation capacity of 821 Megawatts (MW). The CBEC facility is a major stationary source of air emissions. MidAmerican is proposing to expand the CBEC facility by adding one additional nominal 750 net MW unit designated as Unit 4. This document is intended to serve as an application for an Air Quality Construction Permit in accordance with Iowa Administrative Code 567 IAC 22.1 and a request to amend the existing permits for CBEC including PSD and Title V.

This application contains a process description for the proposed addition of Unit 4, the emissions information, a request for permit limits, regulatory review, a Best Available Control Technology (BACT) analysis, a Maximum Achievable Control Technology (MACT) analysis for applicable HAP pollutants, results of Class I and Class II modeling, monitoring information, and a compliance plan. The required construction permit application forms are provided in Appendix A of the application.

1.1 Unit 4 Impact on Emission Levels

The addition of Unit 4 is subject to Prevention of Significant Deterioration (PSD) regulations for Carbon Monoxide (CO), Total Particulate Matter (PM), Particulate Matter less than 10 Microns (PM_{10}), Volatile Organic Compounds (VOC), Sulfur Dioxide (SO_2), Nitrogen Oxide (NO_X), Lead (Pb), Sulfuric Acid Mist (H_2SO_4), Fluorides (as HF), Total Reduced Sulfur and Reduced Sulfur Compounds.

CBEC Units 1, 2 and 3 were previously permitted (92-TV-001-M004) as major stationary sources under State and Federal PSD air quality regulations. The addition of Unit 4 is subject to separate additional PSD permitting because there is a significant increase in emissions of PSD-regulated pollutants associated with the proposed addition of Unit 4. Annual emissions from Unit 4 are estimated to be 4,034 tons of SO_2, 2,689 tons of NO_x, 5,166 tons of CO, 672 tons of PM, 854 tons of PM_{10} (filterable and condensible), 126 tons of VOCs, 0.88 tons of Lead, 142 tons of H_2SO_4, 22 tons of HF, 30 tons of Total Reduced Sulfur, 30 tons of Reduced Sulfur Compounds and 109 tons of Hazardous Air Pollutants (HAPs). MidAmerican is not required to offset the increase in emissions of criteria pollutants, and therefore PSD New Source Review (NSR) requirements will apply to these pollutants for the addition of Unit 4.

The CBEC is located in an attainment area for all criteria pollutants. The CBEC will meet all National Ambient Air Quality Standards (NAAQS) and the Class I and Class II PSD increments in the vicinity of the plant. Unit 4 will also be required to meet the applicable New Source Performance Standards (NSPS) defined in federal regulations 40 CFR Subpart D(a).

1.2 Overview

The addition of Unit 4 at the CBEC facility will result in additional power generating capacity to sustain current and future power demands in the MidAmerican Energy service area. This project will result in economic benefit through the creation of jobs during facility construction, permanent jobs during startup and operation, and employment opportunities associated with facility support, fuel mining and transport functions.

The CBEC facility is located in an area of relatively low population density. The Council Bluffs facility is situated in a broad valley that is favorable to plume dispersion and the nearest Class I area is more than 500 km away. State-of-the-art pollution controls are proposed for Unit 4 that will make the new unit one of the cleanest coal-fired power plants in the nation. Pollution controls include low NO_X burners, overfire air and selective catalytic reduction to control NO_X to an outlet concentration of 0.08 lb/mmbtu; lime spray dryer flue gas desulfurization to control SO_2 to an outlet concentration of 0.12 lb/mmbtu; and a pulse-jet fabric filter baghouse to control filterable PM_{10} to an outlet concentration of 0.018 lb/mmbtu.

An air quality modeling analysis was performed to demonstrate compliance with state and federal air quality regulations that are applicable to the proposed project. Dispersion modeling was conducted for each criteria pollutant for which the annual emission rate was equal to or greater than the significant emission rates for PSD analysis. The air quality impact analysis also included a growth analysis, soils and vegetation analysis, Class I and Class II visibility impairment analyses and a cooling tower impact analysis.

1.3 Permit Application Organization

This application is organized into nine sections and six appendices. A CD-ROM of modeling files is also enclosed.

- **Section 1.0 – Introduction.** This section provides an overview of the project and describes the report organization.
- **Section 2.0 – Process Description.** This section includes a process description for the proposed Unit 4 including the boiler, emission control equipment and material handling systems.
- **Section 3.0 – Emissions Summary.** This section provides a summary of emissions related information, including stack and auxiliary equipment emissions and material handling emission estimates.
- **Section 4.0 – Requested Permit Limits.** This section presents a discussion of requested permit limits to reflect consistency with assumptions made in the analysis of project related emissions.
- **Section 5.0 – Regulatory Applicability Review and Requirements.** This section contains a detailed regulatory review of all state and federal air regulations that may impact the permitting, construction, or operation of the proposed Unit 4.

- **Section 6.0 – Control Technology Analysis.** This section includes a control technology analysis for criteria pollutants (BACT Analysis) and for Hazardous Air Pollutants, (MACT Analysis).
- **Section 7.0 – Air Quality Impact Analysis.** This section includes the Class I and Class II air quality modeling analyses including a review of growth impacts, soils and vegetation, visibility impairment and cooling tower impacts.
- **Section 8.0 – Monitoring Information.** This section presents monitoring related information.
- **Section 9.0 – Compliance Plan and Certification.** This section presents the Title V Compliance Plan and Certification including a Compliance Assurance Monitoring Plan.
- **Appendix A – Permit Application Forms.** This appendix includes the required IDNR construction permit application forms.
- **Appendix B – Regulatory Review Requirements.** This appendix includes regulatory review tables for both Iowa and Federal air quality requirements.
- **Appendix C – Modeling Files and Information.** This appendix includes a list of the modeling files on the CD-ROM and representative input and output files.
- **Appendix D – RACT/BACT/LAER Clearinghouse.** This appendix includes the RBLC database tables used for the Section 6.2 BACT analysis.
- **Appendix E – BACT Cost Analysis.** This appendix includes the cost analyses for various control technology alternatives reviewed in the Section 6.2 BACT analysis.
- **Appendix F – Emissions Calculations.** This appendix provides the calculations that were used to determine the criteria and HAP emissions for this permit application.

SECTION 2.0

Process Description

2.1 Facility Description

The Council Bluffs Energy Center (CBEC) is located in Pottawattamie County, Iowa just south of the City of Council Bluffs. The Missouri River forms the west boundary of the plant site and Interstate highway I 29 forms the east boundary (Figure 2-1). The plant currently consists of three coal-fired electric generating units designated as Units 1, 2, and 3. Their generating capacities are 43 MW, 88 MW, and 690 MW net. MidAmerican is planning the addition of a fourth unit, designated as Unit 4, that has a nominal rating of 750 MW net.

2.1.1 General Process Description

CBEC generates electric power for sale to the customers of MidAmerican Energy, the operator of the Council Bluffs Energy Center. Figure 2-2 is a general process flow diagram for Council Bluffs Unit 4. The generating plant produces electricity by combusting coal to produce heat to convert water to steam. The steam powers turbines attached to electric generators. Generators convert mechanical energy supplied by a turbine into electrical energy. Each boiler turbine generator combination is referred to as a "unit."

Fossil fuel generating plants, generally consist of the following components:

1. Boiler
2. Turbine
3. Generator
4. Various Configurations of Auxiliary Equipment
5. Fuel Handling
6. Emissions Control Equipment
7. Material Handling

In a typical fossil fuel boiler, tubes that contain water, line the inside of the furnace walls. The fuel that enters the furnace is ignited and burned. The burning fuel releases thermal energy, which is absorbed by the water in the tubes. As the temperature of the water rises, the water begins to boil, and steam is produced. The steam is piped from the boiler to the steam turbine.

The steam turbine is comprised of blades attached to a rotating shaft. Steam turbines have both stationary and rotating blades. As the high-pressure steam passes through the turbine blades, the pressure and thermal energy of the steam is converted to mechanical energy, causing the rotating set of blades to move, thus rotating the shaft of the turbine. The steam turbine shaft is coupled to the shaft of the electrical generator. The generator converts mechanical energy into electric energy.

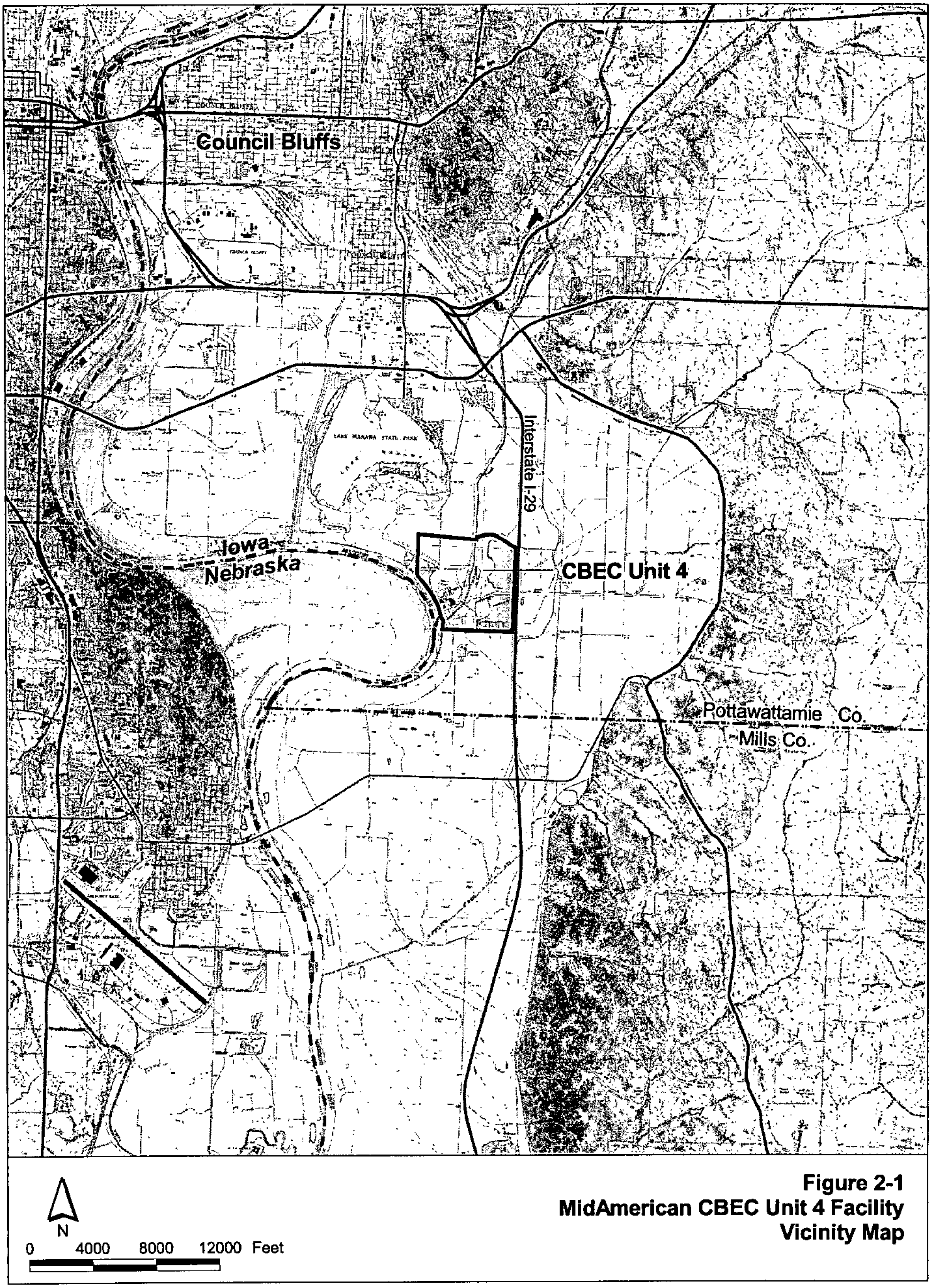


Figure 2-1
MidAmerican CBEC Unit 4 Facility
Vicinity Map

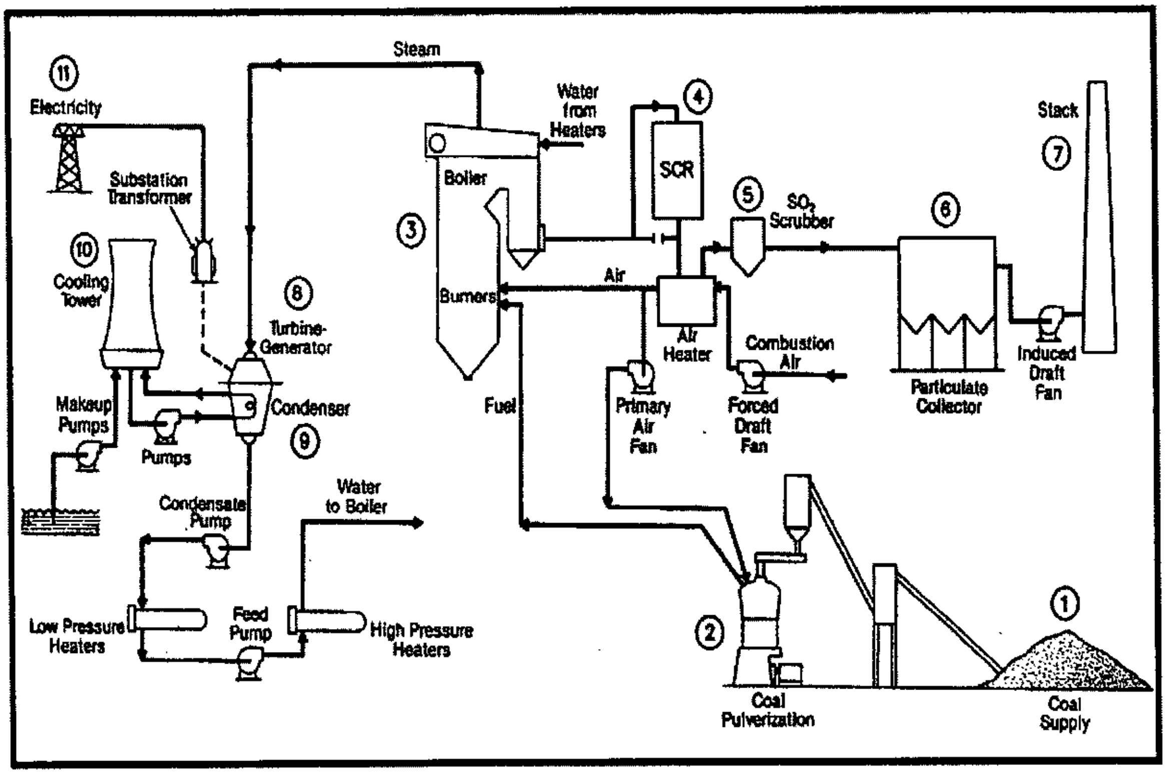


FIGURE 2-2
General Process Flow Diagram for CBEC Unit 4

After the steam passes through the turbine, it flows into the condenser. In the condenser, the steam is cooled and condensed back into water. The water is then pumped back to the boiler through a series of low-pressure condensate heaters, a deaerator, and several high-pressure feedwater heaters, and the cycle begins again. The heaters increase the efficiency of the overall cycle.

The complete loop from the boiler, through the turbine, into the condenser, through the condensate and feedwater systems, and back to the boiler is called the condensate-feedwater-steam cycle. All of the components and systems involved in the condensate-feedwater-steam cycle are generally referred to as one generating unit. Each generating unit is comprised of several component systems that are either for that one generating unit or are shared across all units. The major component systems of the existing and proposed addition to the Council Bluffs Energy Center are as follows:

1. Fuel Handling
2. Generating Units
3. Emissions Control Equipment
4. Material Handling

These systems consist of the following sub-systems. The numbers in brackets refer to the respective components shown in Figure 2-2:

Fuel Handling

a. Coal Handling [1,2]
b. Fuel Oil System
c. Natural Gas System

Generating Units

a. Boiler [3]
b. Steam Turbine [8]
c. Boiler Feedwater System [9]
d. Process Cooling Water System [10]

Emissions Control Equipment

a. Low- NO_X Burners [3]
b. Selective Catalytic Reduction System (Unit 4) [4]
c. Electrostatic Precipitator (Units 1, 2 and 3) [6]
d. Fabric Filter (Unit 4) [6]
e. Flue Gas Desulfurization System (Unit 4) [5]

Material Handling

a. Fly Ash Collection, Transport and Disposal
b. Bottom Ash Collection, Transport and Disposal
c. Lime Unloading, Storage and Transport (Unit 4)
d. Urea Unloading, Storage and Transport (Unit 4)
e. FGD Waste Collection, Transport and Disposal (Unit 4)

The summary description for Unit 4 provided below includes a description of those systems which contain or affect this facility's air emissions. Other systems, not containing or impacting air emissions, or those systems with air emissions deemed insignificant by the IDNR, are not included in this process description.

2.1.1.1 Proposed Unit 4 Process Description

The proposed primary fuel will be a sub-bituminous coal. Coal will be delivered to the plant by rail and in trucks. The Unit 4 coal heat input at full load is estimated at 67.23 x 106 MMBTU/yr. Number 2 fuel oil will be used for light off, startup, and flame stabilization. Fuel oil is stored in the existing aboveground tank, which is located on the plant site and currently serves Unit 3. No additional oil storage is planned for Unit 4. The total amount of oil burned per year will be approximately 800,000 gallons/year for both units. Coal and oil burner configurations and combustion control systems will be designed to provide high combustion efficiency and to control the production of NO_X in the flue gas.

The SO_2 emissions will be controlled with a lime spray dryer flue gas desulfurization (FGD) system. Nitrogen oxide emissions will be controlled with low NO_X burners (LNBs), overfire air (OFA) and Selective Catalytic Reduction (SCR). PM_{10} emissions will be controlled by a pulse jet fabric filter.

The clean flue gas will go from the fabric filter exit through the induced-draft fans and will be exhausted through an exhaust stack to the atmosphere. The stack will be 550 feet tall and will consist of an outer concrete wind shell and an inner flue. A continuous emission monitoring system (Part 75 CEMS) will be provided to monitor emissions.

Boiler

The proposed Unit 4 boiler will be an indoor-type supercritical pulverized coal fired boiler designed for "base load" operation. The unit will have a maximum gross heat input of approximately 7,675 MMBtu/hr and a nominal net plant electrical output of approximately 750 MW. Unit 4 will generate a main steam pressure of 3,500 to 3,700 psig and will generate steam at 1,050 to 1,100 °F. The primary fuel for Unit 4 will be Powder River Basin sub-bituminous coal. Fuel oil (No. 2) will be used as the start-up fuel. The typical fuel characteristics for Powder River Basin sub-bituminous coal are shown in Table 2-1.

It is anticipated that the Unit 4 boiler will be a dry-bottom, tangentially-fired or wall-fired (front and rear) boiler with low NO_X burners and overfire air ports. Specifications for the proposed boiler are included in Table 2-2. Flue gas from Unit 4 will pass through a series of post-combustion emission control devices, described in Section 2.2 of this permit application, and discharge through one 550-foot stack.

The boiler area will be a totally enclosed design. Burners will be located at various levels either in the four corners or in the front and back furnace walls. The coal silos will be located along the boiler front, with an enclosed coal tripper gallery. The principal components of the boiler will be:

- membrane wall furnace
- superheater
- reheater
- economizer
- convection pass
- coal feeders
- coal pulverizers
- low NO_X burners (LNBs), overfire air ports, fans, and air heater
- induced draft, forced draft and primary air fans
- air preheaters
- boiler wall cleaning/sootblowing system
- flues and ducts
- piping and valves

TABLE 2-1
Coal Characteristics

Parameter	Unit	Proposed Coal
Gross (Higher) Heating Value	Btu/lb	8,000
Moisture	wt %	28.8
Volatile Matter	wt %	30.4
Sulfur Content	wt %	0.50
Ash Content	wt %	7.00
Maximum Uncontrolled SO_2 Emission Rate	lb/mmBtu	1.25

TABLE 2-2
Boiler Parameters

Plant Parameter	Unit	Estimated Value
Nominal Net Plant Output	Net-kW	750,000
Steam Temperature	°F	1,050 to 1,100
Main Steam Pressure	psig	3,500 to 3,700
Full Load Heat Input to Boiler	MMBtu/hr	7,675
Coal Feed Rate	lb/hr	959,406

2.2 Emissions Control Equipment

2.2.1 Flue Gas Desulfurization System

The Unit 4 boiler unit will be equipped with a lime spray dryer flue gas desulfurization (FGD) system. The FGD system, located upstream from the fabric filter, removes sulfur dioxide (SO_2) from the flue gas stream by use of a lime slurry absorption process. Additional details on the lime spray dryer FGD process are provided in the BACT analysis section of this application in Section 6.

The FGD system will be designed to consistently achieve a controlled SO_2 emission rate of 0.12 lb/mmBtu. Assuming a maximum uncontrolled SO_2 emission rate of 1.25 lb/mmBtu, this represents an overall removal efficiency of approximately 90%.

Anticipated design and operating parameters for the FGD system are summarized in Table 2-3.

2.2.2 Selective Catalytic Reduction

Unit 4 will be equipped with a selective catalytic reactor (SCR) to reduce NO_X emissions from the boiler. SCR is the state-of-the-art technology for the reduction of NO_X from flue gas streams. The proposed SCR will be designed for high dust loading applications, and will be located external from the boiler. Additional details on the SCR process are provided in the BACT analysis section.

Based on technical information provided by boiler vendors, it is anticipated that NO_X emissions from the boiler (prior to the SCR) can be reduced with low NO_X burners and overfire air to 0.20 lb/mmBtu (approximately 143 ppmvd @ 3% O_2) while maintaining acceptable levels of CO and VOC. Assuming a NO_X inlet concentration of 143 ppmvd @ 3% O_2, the SCR will be designed to reduce the NO_X concentration to approximately 57 ppmvd @ 3% O_2, or 0.08 lb/mmBtu. This represents an overall removal efficiency of approximately 60%.

The anticipated SCR operating parameters are summarized in Table 2-4.

TABLE 2-3
Flue Gas Desulfurization Operating Parameters

Parameter	Unit	Estimated Design Value	Notes
General Description		Dry FGD	
Number of Scrubber Modules		TBD	
Flue Gas Flow Rate	acfm	2,961,658	FGD inlet
Flue Gas Temperature (inlet)	°F	275 – 300	
Pressure Drop Through Scrubber	in. H_2O	8 (typical)	
Inlet SO_2 Concentration	lb/mmBtu	1.25	Maximum
Outlet SO_2 Concentration	lb/mmBtu	0.12	Maximum
SO_2 Collection Efficiency	%	90.4	Design based on SO_2 concentrations listed
HCl Collection Efficiency	%	90+	
HF Collection Efficiency	%	90+	
Calcium to Sulfur Molar Ratio		1.20	
Sorbent Feed Rate	lb/hr	11,188	Maximum
Sorbent Analysis		$CaCO_3$ 0% $MgCO_3$ 0% CaO 90% Ash 10% Moisture 0%	Typical lime sorbent analysis
FGD Waste Generated (included in baghouse collected fly ash)	lb/hr	37,897	Maximum

TABLE 2-4
SCR Operating Parameters

Parameter	Unit	Estimated Design Value
Catalytic Reaction Temperature	°F	675 – 725
Inlet Gas Temperature	°F	700 – 715
Inlet Gas Flow Rate	acfm	2,961,658
Reducing Agent		Ammonia
Maximum Ammonia Feed Rate	lb/hr	378
NO_X Inlet Concentration	ppmvd @ 3% O_2	143 (0.20 lb/mmBtu)
NO_X Outlet Concentration	ppmvd @ 3% O_2	57 (0.08 lb/mmBtu)
NO_X Control Efficiency	%	60 (Based on NO_X concentrations listed)
Ammonia Slip	ppmvd	5 ppm
Catalyst Life	years	2 – 3

2.2.3 Fabric Filter

A fabric filter system (or "baghouse") will be provided for Unit 4 to remove particulate matter from the boiler flue gas stream. The fabric filter system will consist of a number of compartments containing fabric filter bags fitted over a wire cage and suspended from a horizontal tube sheet in the compartment. Additional details on the baghouse particulate removal process are provided in the BACT analysis section.

The fabric filter system will be designed to achieve a maximum filterable PM emission rate of 0.020 lb/mmBtu with a design collection efficiency of 99.7%. The maximum filterable PM_{10} emission rate will be 0.018 lb/mmBtu. Anticipated fabric filter system parameters are summarized in Table 2-5.

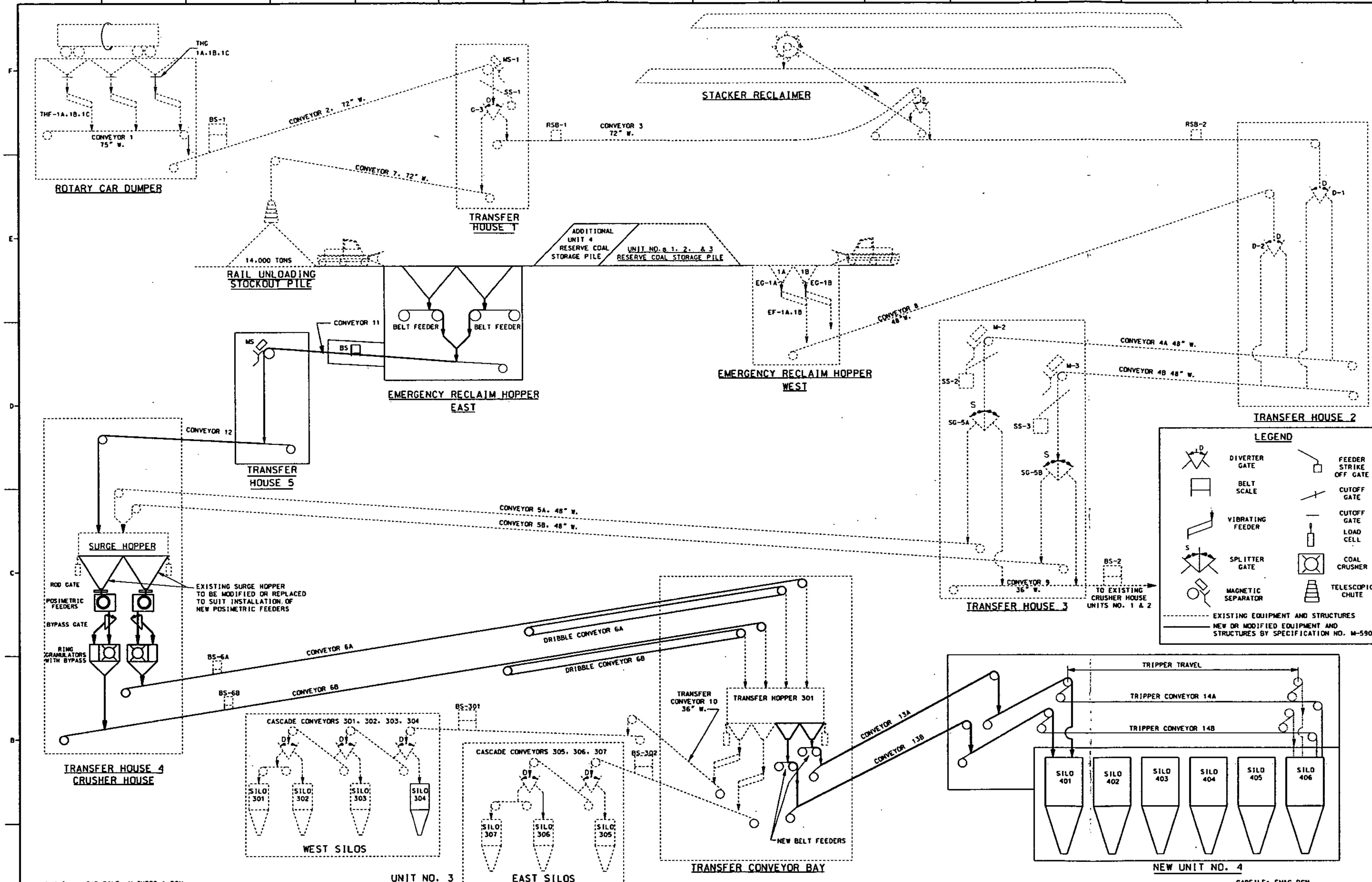
TABLE 2-5
Anticipated Fabric Filter Design Parameters

Parameter	Units	Estimated Design Value
Flue Gas Flow Rate to Fabric Filter	acfm	2,660,982
Inlet Gas Temperature	°F	165
Inlet Total Particulate Loading	lb/hr	53,727
Outlet Total Particulate Loading	lb/mmBtu	0.020
Outlet Total Particulate Loading	lb/hr	153
Collection Efficiency	%	99.7
Outlet PM_{10} Loading	lb/mmBtu	0.018
Bag Material		TBD
Bag Diameter, Length, Number of Bags		TBD
Number of modules and compartments per module		TBD
Air to Cloth Ratio		TBD
Pressure Drop Across Bags	in. H_2O	5 - 6 (typical)
Cleaning Mechanism and Cycle		Pulse-jet

2.3 Coal Handling System

Figure 2-3 presents a schematic flow diagram of the existing and modified Coal Handling System for CBEC Units 3 and 4.

In order to accommodate the increased coal burn rate due to the new steam generator for Unit 4, the existing coal handling systems will require upgrading with additions and modifications.



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CADFILE: EM1C.DGN

DRAWING RELEASE RECORD

REV.	DATE REL'D.	PREPARED	REVIEWED	APPROVED	PURPOSE	FILM
0	9-16-2002	C. WIATRAK	B. SHAH	———	ISSUED TO CLIENT FOR AIR PERMITTING	

SCALE: NONE
PROJECT NUMBER: 11175-007

COAL HANDLING FACILITIES
FLOW DIAGRAM
UNITS NO.s 1 THRU 4

MIDAMERICAN ENERGY
COUNCIL BLUFFS STATION

Sargent & Lundy

DRAWING NO.: EM1C REV.: 0
SHEET OF

WAS - CADFILE: M-CHFFD-1.DGN

2.3.1 Existing Coal Handling System

Coal is received at the station by railcars operated as unit trains and is unloaded into receiving hoppers at the Rotary Car Dumper. Coal is removed from the receiving hopper at a rate of 3,500 tons per hour (T/hr) and is discharged onto a 72" wide belt Conveyor C-1. The coal is conveyed to Transfer House 1 via Conveyors C-1 and C-2. In Transfer House 1, coal from Conveyor C-2 is transferred to a 72" wide, 3,500 T/hr Stacker/Reclaimer Conveyor C-3. The Stacker creates two active coal piles, one on each side of the Stacker's conveyor, each pile capable of storing 44,000 tons. Coal can also be conveyed to a rail unloading stock out pile by diverting it to a 72" wide, 3,500 T/hr Conveyor C-7. Mobile equipment is used to push the coal from the rail unloading stock out pile to the inactive coal storage pile.

The existing reclaim system incorporates a redundant parallel conveyor system from the coal yard to the Unit 3 in-plant transfer conveyor bay. Reclaiming coal from the active storage pile is by means of the Bucket Wheel Reclaimer, which has a reclaim rate of 1,600 T/hr. The Bucket Wheel Reclaim Conveyor C-3 conveys the coal to Transfer House 2 where the coal is transferred to one of two Conveyors C-4A/B which are 1,600 T/hr, 48" wide conveyors. Conveyors C-4A/B convey the coal to Transfer House 3, whereby it is then transferred to Conveyors C-5A/B and on to the Transfer House 4 (Crusher House). The Crusher House incorporates a surge bin with two vibratory feeders each discharging to a crusher. The coal is then loaded onto one of two Conveyors (C-6A/B), which are 900 T/hr, 48" wide conveyors. Conveyors C-6A/B convey the coal to the plant's transfer conveyor bay and discharges into a transfer hopper. The coal is discharged from the transfer hopper by means of vibratory feeders onto 450 T/hr Cascade Conveyors C-305/306/307 and 450 T/hr Transfer Conveyor C-10. Transfer Conveyor C-10 in turn feeds 450 T/hr Cascade Conveyors C-301/302/303/304. The cascade conveyors feed the seven in-plant coal silos for Unit 3.

Coal can also be reclaimed via an emergency reclaim hopper located near the west end of the Stacker/Reclaimer Conveyor C-3. Coal is moved to this emergency reclaim hopper by mobile equipment. The coal is reclaimed at a rate of up to 1,200 T/hr and conveyed to Transfer House 2 by means of 1200 T/hr, 48" wide Conveyor C-8. Emissions from all enclosed transfer points in the coal handling system are controlled through bag house fabric filters.

2.3.2 Modifications and Additions to Existing Coal Handling System (Unit 4 addition)

The coal handling modifications and additions associated with the CBEC Unit 4 project will require upgrading existing conveyors and equipment, modifying existing buildings, and installing a new emergency reclaim system.

System Description

Figure 2-3 presents a schematic flow diagram of the Coal Handling System. The stock out system will be utilized without change as will the existing rotary rail car dumper, its receiving Conveyors C-1 and C-2, which convey the coal from underground to the above ground Transfer House 1. At Transfer House 1 the coal can be diverted either to the existing stacker reclaimer Conveyor C-3 or to Conveyor C-7 for stocking out. During normal operation the coal will be deposited in an active storage pile outside via Stacker Reclaimer

Conveyor C-3 and the Stacker Boom Conveyor. In an emergency, coal will be transferred to the existing 14,000 tons (approximately 1 unit train) capacity rail unloading stock out pile by means of Conveyor C-7.

The existing active coal storage pile will be the primary active coal source for Unit 4. The existing Stacker Reclaimer will remain as the primary coal stack out and reclaim system.

The inactive coal storage capacity will be 999,000 tons to provide a 45-day storage capacity. The inactive storage pile will incorporate approximately 23-acres of land at a 40 foot height and will be located to the North of the plant inside the perimeter railroad track.

To reclaim coal from the inactive coal storage pile or the rail unloading stackout pile a new reclaim hopper will be built on the east end of the coal yard. The existing emergency reclaim hopper will remain on the west end of the coal yard for reclaiming coal from that area. During an emergency, such as an interruption in coal deliveries to the plant, coal from the inactive pile will be bulldozed to either the east or west reclaim hopper for loading into the unit silos. A new Conveyor C-11 will convey the coal from the east underground reclaim hopper to a new above ground Transfer House 5. Conveyor C-11 will discharge onto a new Conveyor C-12 which will transfer the coal to the existing surge hopper in Transfer House 4. Conveyor C-8 will convey coal reclaimed from the west underground reclaim hopper to Transfer House 2. Conveyors C-4A/B will convey the coal from Transfer House 2 to Transfer House 3 where it will be discharged onto existing conveyors C-5A/B. Conveyors C-5A/B will discharge the coal into the surge hopper in Transfer House 4.

The Transfer House 4 (Crusher House) 900 T/hr vibratory feeders and 900 T/hr ring granulators (crushers) will be replaced with 1600 T/hr equipment to accommodate Unit 4. The new crushers will discharge onto the modified 1600 T/hr Conveyors C-6A/B (currently 900 T/hr), which will convey the coal to the surge hopper located at the transfer conveyor bay area. Conveyors C-6A/B will be modified to increase capacity from 900 T/hr to 1,600 T/hr. The transfer conveyor bay surge hopper will continue to discharge onto the unchanged existing Unit 3 cascade and transfer conveyors. The surge hopper will be modified to allow coal to be fed onto new variable speed belt feeders to supply flow onto new 900 T/hr Transfer Conveyors C-13A/B. Transfer Conveyors C-13A/B will transfer coal to new 900 T/hr Tripper Conveyors C-14A/B which will feed new coal silos for Unit 4. Coal will be distributed to each of the coal silos using traveling trippers.

Dust Control

The coal handling system employs a number of effective mechanisms for minimizing fugitive dust emissions.

- All coal transfer buildings are enclosed.
- Chemical binding will be used to suppress fugitive dust from the inactive coal storage piles.
- Bag house type dust collection systems are provided for each of the enclosed conveyor transfers. Dust generated inside new Transfer House 5 will be piped to Transfer House 4 for collection in the existing Transfer House 4 bag house.

- A dust control agent is applied to the coal as it is unloaded from the rail cars at the rotary car unloader. This dust control agent remains effective for approximately ten days and thus controls dust emissions as the coal is moved to and from the active storage pile and to the unit coal silos.
- The coal stock out pile conveyors incorporate a telescopic chute to control the fugitive emissions during stock out operation.
- The stacker incorporates level probes on the stacker chute to maintain a set distance from the stock out pile and control fugitive emissions during stock out operation.

2.4 Material Handling

2.4.1 Scrubber Additive (Lime) Handling System

The spray dryer FGD system utilizes lime to remove SO_2 from the flue gas and therefore requires a lime handling system, which receives, stores and processes crushed lime.

A combination filter/separator will pneumatically remove lime from a totally enclosed, 100-ton railcar by means of a negative pressure system. The combination filter/separator will separate lime from the conveying air, performing the function of a cyclone separator and baghouse in one vessel.

The lime will then be discharged from the filter/separator into a transfer hopper and then into a positive pressure conveyance pipe to be transferred to the lime storage silo.

A day bin with a 24-hour capacity will be located in the lime processing building to supply lime to the conditioning equipment. The day bin level will be maintained by pneumatically transferring the lime from the storage silo to a transfer hopper, which then discharges into a conveyance pipe and conveys the lime using positive pressure to the day bin.

In addition to rail delivery, lime can also be provided by truck and trailer. The trailers are totally enclosed, over the road, 20-ton capacity trailers. The truck will park next to the lime preparation building, and connect a rubber conveyance hose to the truck and to a fixed conveyance pipe for the day bin. The truck will use its own compressor system to pneumatically offload the lime to the day bin. While filling the day bin an exhaust filter on top of the day bin filters the displaced air.

To control emissions generated from the lime, the system is equipped with a dust collection system at the railcar unloading area as well as the utilization of bin vent filters on the storage silo, and day bin.

2.4.2 Urea Unloading/Storage System

Ammonia that is needed for the Selective Catalytic Reduction System (SCR) will be generated from dry urea at Council Bluffs Unit 4. Dry urea is a stable, non-volatile, environmentally benign material. It is solid under ambient temperatures and pressures and is typically used as a fertilizer. Urea can be safely transported in bulk and stored for long periods of time until it is converted into ammonia. The urea used for the generation of ammonia will be delivered by truck or rail and stored in two vertical dry urea storage silos.

Each storage silo will be equipped with a bin vent filter for dust control. One pound of dry urea will produce approximately 0.56 pounds of ammonia.

The ammonia generation process using dry urea as feedstock consists of an unloading facility, storage silos, dissolving/mixer vessel, urea-water solution pumps and preheater, a hydrolyzer with process heater and sparger. The storage silos will be designed to receive urea in a pill or granular form. Dry urea is dissolved in hot water (Station-supplied condensate/demineralized water) to form an aqueous solution. To improve the solution quality and reduce dissolving time, a mixer is located in the dissolver. The urea solution is fed via pumps to a preheater and then to a hydrolyzer. To maintain the temperature and pressure at a constant level, station-supplied steam (saturated or superheated) is injected and distributed through the hydrolyzer to carry out the ammonia generation process. The process produces a gaseous mixture of ammonia gas, carbon dioxide and water. The process requires no storage of ammonia.

2.4.3 Fly Ash and FGD Waste Handling System (Unit 4)

Figure 2-4 presents a schematic flow diagram of the flyash/FGD waste handling system.

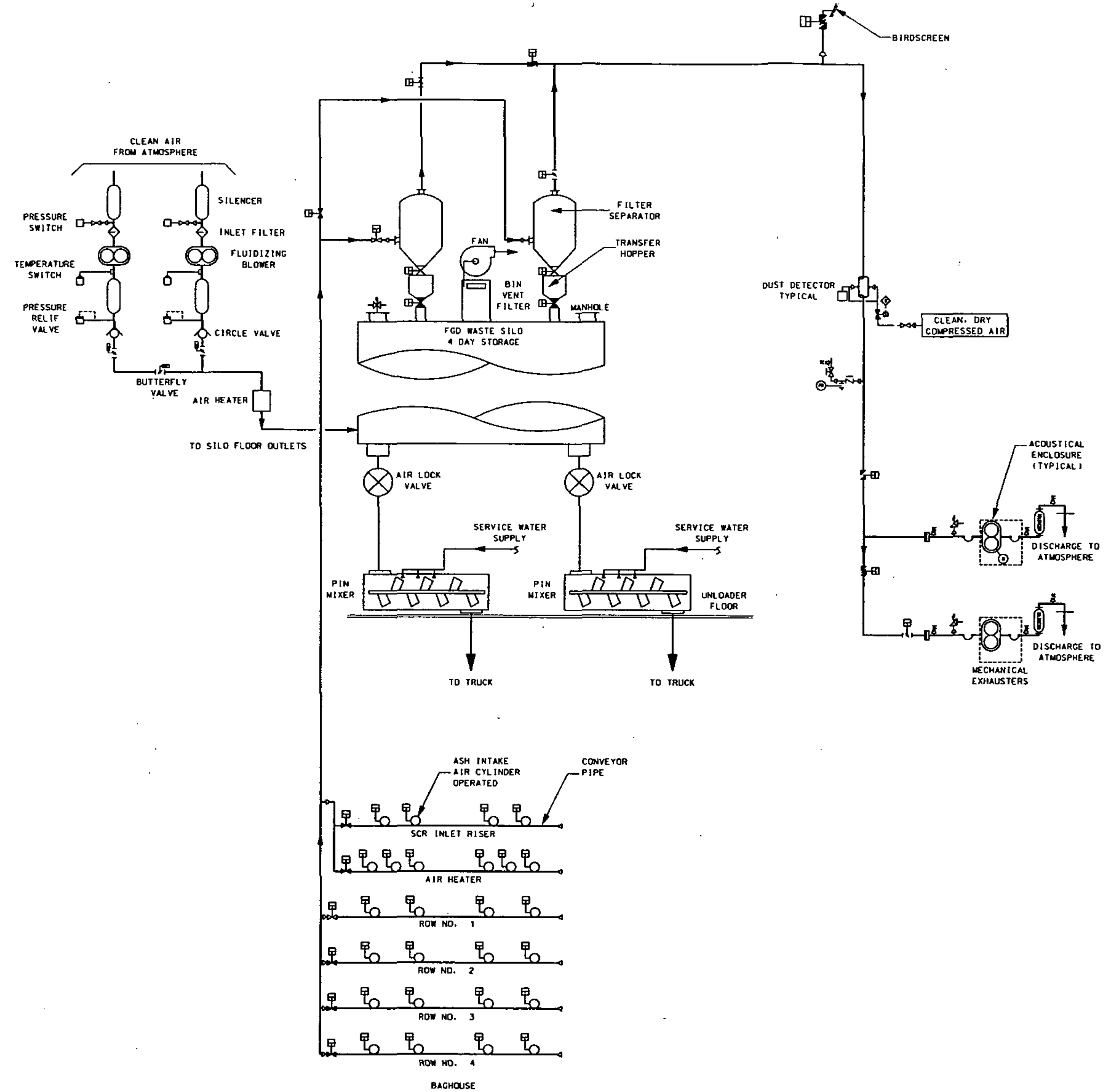
Flyash and spray dryer FGD waste entrained in the hot boiler flue gas will be removed from the flue gas using a pulse-jet baghouse. Ash will also be collected from other various locations throughout the flue gas system by means of ash hoppers located beneath the collection locations where the flue gas becomes stagnate. The flyash/FGD waste handling system will be comprised of an independent pneumatic conveyance and storage system. Economizer ash will be collected and discharged into the bottom ash water filled collection trough either by drag chain conveyor or sluice jet water conveyance.

The pulse-jet baghouse will be incorporated into the dry FGD collection system with each row of hoppers having its own conveyance header. All flyash/FGD waste will be collected and stored in a FGD waste storage silo, where it will be stored and transferred to an offsite disposal landfill.

Flyash/FGD waste will be transported through vacuum conveyance lines to the filter separators located on top of the storage silo. The filter separators will discharge the collected fly ash/FGD waste into transfer hoppers and then directly into the silo. The filter separators will be designed with sufficient bag filtering capacity to control emissions, along with a bin ventilation filter, which will be responsible for filtering the displaced silo air. Electric motor-driven vacuum exhausters will provide conveying air for the system. The discharge conditioning devices under the silo will be a water and ash mixer (pin mixer) to condition the fly ash/FGD waste prior to loading onto trucks for haulage to the disposal location.

The storage silo will have a nominal storage capacity of 4 days accumulation. The bottom of the storage silo will be equipped with a complete fluidizing air system including a porous fluidizing media, which will receive air from air blowers, an electric air heater, an inlet filter silencer, etc.

The system will employ several redundant features to ensure dependable operation. A spare filter separator and a spare conveying vacuum exhauster will be provided for the fly ash/ FGD waste handling system. The silo fluidizing system will include a spare blower.



REFERENCE FILE: EM3B-WASTE-P&ID.DGN

CAD FILE: EM3B.DGN

DRAWING RELEASE RECORD

REV.	DATE REL'D.	PREPARED	REVIEWED	APPROVED	PURPOSE	FILM

DRAWING RELEASE RECORD

REV.	DATE REL'D.	PREPARED	REVIEWED	APPROVED	PURPOSE	FILM
0	09-16-2002	C. WIATRAK			ISSUED TO CLIENT FOR AIR PERMITTING	

SCALE NONE

PROJECT NUMBER 10905-004

FGD WASTE HANDLING/STORAGE FLOW DIAGRAM

COUNCIL BLUFFS STATION
MIDAMERICA ENERGY

Sargent & Lundy

DRAWING NO. EM3B

REV. 0

SHEET OF

WAS EM3.DGN

2.4.4 Bottom Ash Handling System

Furnace ash from the steam generator furnace collects in the water filled trough of the submerged scraper conveyor (SSC) and will be removed on a continuous basis. Seal plates secured to the steam generator tubes and suspended in the SSC trough form the furnace water seal. The ash thus collected will be dragged along the conveyor and will be dewatered on its traverse up an incline before being discharged into a transfer chute.

The transfer chute equipped with a diverter gate in the chute will normally direct ash to the grizzly and accompanying crusher, transfer conveyor and to the bottom ash storage area. In an emergency, the gate will direct ash onto the boilerhouse floor. Water liberated by wet ash in each transfer conveyor and bottom ash storage area will be collected in a sump pit and pumped or gravity drained into a surge tank.

Mill rejects from the coal mill reject hoppers will be conveyed by hydro-ejectors to the SSC trough. A sluice pump will provide the water supply to the hydro-ejectors. The mill rejects will combine with the furnace ash and will be conveyed to a bottom ash storage area as described above.

The Economizer ash will also be combined with the bottom ash and will be conveyed to a bottom ash storage area as described above.

The bottom ash storage area is essentially a concrete floor with cinder block or concrete walls on three sides. Material from the bottom ash storage area will be loaded into trucks and hauled to disposal.

SECTION 3.0

Emissions Summary

The Unit 4 emission estimates include the Unit 4 boiler, auxiliary boiler, emergency diesel generator, fire pump, cooling tower and material handling sources. Unit 4 has material handling operations for coal, flyash, lime, urea, and FGD waste and ash disposal. Detailed emission estimates are provided in Appendix F.

The major air emission sources and regulated air pollutants for Unit 4 are shown in Table 3-1. IDNR Emission Source forms for Unit 4 are attached in Appendix A as is Form MI-1 which shows the locations of all of the emission points.

TABLE 3-1
Unit 4—Air Emission Sources and Regulated Air Pollutants

Source Number	Emission Point	Regulated Air Pollutants
EP-141	Main Boiler – Unit 4 Stack	SO_2, NO_x, PM, PM_{10}, CO, VOC, Lead, H_2SO_4, HF, TRS, RSC, HAPs
EP-142	Auxiliary Boiler for Unit 4	SO_2, NO_X, PM, PM_{10}, CO, VOC, and Lead
EP-143	Emergency Generator for Unit 4	SO_2, NO_X, PM, PM_{10}, CO, and VOC
EP-144	Fire Pump for Unit 4	SO_2, NO_X, PM, PM_{10}, CO, and VOC
EP-145	Unit 4 Cooling Tower	PM, PM_{10}
EP-159	Coal Handling – Transfer Conveyor Bay	PM, PM_{10}
EP-160	Coal Handling – Unit 4 East Silos	PM, PM_{10}
EP-161	Coal Handling – Unit 4 West Silos	PM, PM_{10}
EP-6*	Coal Handling – Rotary Car Dumper	PM, PM_{10}
EP-13*	Coal Handling – Transfer House 4	PM, PM_{10}
EP-167	Flyash/FGD Waste Handling – FGD Waste Silo	PM, PM_{10}
EP-168	Flyash/FGD Waste Handling – Vacuum System Exhauster #1	PM, PM_{10}
EP-169	Flyash/FGD Waste Handling – Vacuum System Exhauster #2	PM, PM_{10}
EP-170	Flyash/FGD Waste Handling – Vacuum System Exhauster #3	PM, PM_{10}
EP-162	Lime Handling – Lime Filter Separator	PM, PM_{10}
EP-163	Lime Handling – Lime Silo	PM, PM_{10}
EP-164A	Urea Handling – Urea Silo #1	PM, PM_{10}
EP-164B	Urea Handling – Urea Silo #2	PM, PM_{10}

TABLE 3-1
Unit 4—Air Emission Sources and Regulated Air Pollutants

Source Number	Emission Point	Regulated Air Pollutants
F-5A*	Coal Handling – Wind Erosion Inactive Coal Storage Pile	PM, PM_{10}
F-5B*	Coal Handling – Maintenance Inactive Coal Storage Pile	PM, PM_{10}
F-4A*	Coal Handling – Wind Erosion Active Coal Storage Pile	PM, PM_{10}
F-4B*	Coal Handling – Maintenance Active Coal Storage Pile	PM, PM_{10}
F-151B	Coal Handling – Wind Erosion Rail Unloading Coal Stockout Pile	PM, PM_{10}
F-151A	Coal Handling – Fugitives from transfer of coal from Conveyor C-11 to Rail Unloading Coal Stockout Pile	PM, PM_{10}
F-151C	Coal Handling – Fugitives from dumping of coal into the Emergency Reclaim Hopper	PM, PM_{10}
F-904	Unit 4 Paved Haul Roads – Flyash/FGD Waste to Offsite Landfill	PM, PM_{10}

*Existing Sources that will be modified with the addition of Unit 4.

3.1 Unit 4 Boiler Criteria Emissions

The estimated hourly, daily, and annual controlled emission rates of criteria pollutants from EP 141, the Unit 4 stack, are shown in Table 3-2. The emissions are based on a 100% capacity factor.

TABLE 3-2
Unit 4 Boiler Criteria Emissions

Pollutant	Hourly Emissions (lbs/hr)	Daily Emissions (lbs/day)	Annual Emissions (tpy)	PSD Significant Emission Rates (tpy)	Emission Factor Reference
Sulfur Dioxide	921.0	22,104.0	4,034	40	Engineering Estimates
Nitrogen Oxides	614.0	14,736.0	2,689	40	Engineering Estimates
Total Particulate Matter	153.5	3,684.0	672	25	Engineering Estimates
Particulate Matter PM_{10} (filterable)	138.2	3316.8	605	15	Engineering Estimates
Particulate Matter PM_{10} (filterable & condensible)	195.1	4682.4	854	15	Engineering Estimates
Carbon Monoxide	1,179.4	28,305.6	5,166	100	Engineering Estimates
VOCs	28.8	691.2	126	40	AP-42 Table 1.1-19
Lead	0.20	4.80	0.88	0.6	AP-42 Table 1.1-18

TABLE 3-2
Unit 4 Boiler Criteria Emissions

Pollutant	Hourly Emissions (lbs/hr)	Daily Emissions (lbs/day)	Annual Emissions (tpy)	PSD Significant Emission Rates (tpy)	Emission Factor Reference
Sulfuric Acid Mist	32.3	775.2	142	7	Engineering Estimates
Fluorides (as HF)	5.1	122.4	22	3	Engineering Estimates
Total Reduced Sulfur	6.8	163.2	30	10	AP-42 Table 1.1-3 (b)
Reduced Sulfur Compounds	6.8	163.2	30	10	AP-42 Table 1.1-3 (b)

3.2 Unit 4 Boiler Hazardous Air Pollutant Emissions

The estimated hourly and annual controlled emission rates of Trace Metal HAPs, Organic HAPs and Acid Gas HAPs for EP 141, the Unit 4 stack, are shown in Table 3-3, Table 3-4 and Table 3-5. Section 6.3 of the Control Technology Analysis provides additional information on emission estimates and control levels for the Section 112 Hazardous Air Pollutants.

TABLE 3-3
Unit 4 Boiler Trace Metal HAPs

Pollutant	Controlled Emissions (lb/hr)	Controlled Emissions (tons/yr)	Emission Factor Reference
Antimony	8.63E-03	0.038	AP-42 Table 1.1-18, (9/1998)
Arsenic	1.97E-01	0.861	AP-42 Table 1.1-18, (9/1998)
Beryllium	1.01E-02	0.044	AP-42 Table 1.1-18, (9/1998)
Cadmium	2.45E-02	0.107	AP-42 Table 1.1-18, (9/1998)
Chromium	1.25E-01	0.546	AP-42 Table 1.1-18, (9/1998)
Cobalt	4.80E-02	0.210	AP-42 Table 1.1-18, (9/1998)
Lead	2.01E-01	0.882	AP-42 Table 1.1-18, (9/1998)
Manganese	2.35E-01	1.030	AP-42 Table 1.1-18, (9/1998)
Mercury	3.85E-02	0.169	Engineering calculations based on CBEC coal mercury analysis and estimated control efficiency.
Nickel	1.24E-01	0.542	AP-42 Table 1.1-18, (9/1998)
Selenium	6.24E-01	2.731	AP-42 Table 1.1-18, (9/1998)
Total Trace Metal HAPs		7.161	**tpy**

TABLE 3-4
Unit 4 Boiler Organic HAPs

Pollutant	Controlled Emissions (lb/hr)	Controlled Emissions (tons/yr)	Emission Factor Reference
Acenaphthene	2.45E-04	0.001	AP-42 Table 1.1-13, (9/1998)
Acenaphthylene	1.20E-04	0.001	AP-42 Table 1.1-13, (9/1998)
Acetaldehyde	2.73E-01	1.198	AP-42 Table 1.1-14, (9/1998)
Acetophenone	7.20E-03	0.032	AP-42 Table 1.1-14, (9/1998)
Acrolein	1.39E-01	0.609	AP-42 Table 1.1-14, (9/1998)
Anthracene	1.01E-04	0.000	AP-42 Table 1.1-13, (9/1998)
Benzene	6.24E-01	2.731	AP-42 Table 1.1-14, (9/1998)
Benzo(a)anthracene	3.84E-05	0.000	AP-42 Table 1.1-13, (9/1998)
Benzo(a)pyrene	1.82E-05	0.000	AP-42 Table 1.1-13, (9/1998)
Benzo(b,j,k)fluoranthene	5.28E-05	0.000	AP-42 Table 1.1-13, (9/1998)
Benzo(g,h,i)perylene	1.30E-05	0.000	AP-42 Table 1.1-13, (9/1998)
Benzyl chloride	3.36E-01	1.471	AP-42 Table 1.1-14, (9/1998)
Biphenyl	8.15E-04	0.004	AP-42 Table 1.1-13, (9/1998)
Bis(2-ethylhexyl)phthalate (DEHP)	3.50E-02	0.153	AP-42 Table 1.1-14, (9/1998)
Bromoform	1.87E-02	0.082	AP-42 Table 1.1-14, (9/1998)
Carbon disulfide	6.24E-02	0.273	AP-42 Table 1.1-14, (9/1998)
2-Chloroacetophenone	3.36E-03	0.015	AP-42 Table 1.1-14, (9/1998)
Chlorobenzene	1.06E-02	0.046	AP-42 Table 1.1-14, (9/1998)
Chloroform	2.83E-02	0.124	AP-42 Table 1.1-14, (9/1998)
Chrysene	4.80E-05	0.000	AP-42 Table 1.1-13, (9/1998)
Cumene	2.54E-03	0.011	AP-42 Table 1.1-14, (9/1998)
Cyanide	1.20E+00	5.253	AP-42 Table 1.1-14, (9/1998)
2,4-Dinitrotoluene	1.34E-04	0.001	AP-42 Table 1.1-14, (9/1998)
Dimethyl sulfate	2.30E-02	0.101	AP-42 Table 1.1-14, (9/1998)
Ethyl benzene	4.51E-02	0.198	AP-42 Table 1.1-14, (9/1998)
Ethyl chloride	2.01E-02	0.088	AP-42 Table 1.1-14, (9/1998)
Ethylene dichloride	1.92E-02	0.084	AP-42 Table 1.1-14, (9/1998)
Ethylene dibromide	5.76E-04	0.003	AP-42 Table 1.1-14, (9/1998)
Fluoranthene	3.41E-04	0.001	AP-42 Table 1.1-13, (9/1998)
Fluorene	4.37E-04	0.002	AP-42 Table 1.1-13, (9/1998)
Formaldehyde	1.15E-01	0.504	AP-42 Table 1.1-14, (9/1998)

TABLE 3-4
Unit 4 Boiler Organic HAPs

Pollutant	Controlled Emissions (lb/hr)	Controlled Emissions (tons/yr)	Emission Factor Reference
Hexane	3.21E-02	0.141	AP-42 Table 1.1-14, (9/1998)
Indeno(1,2,3-cd)pyrene	2.93E-05	0.000	AP-42 Table 1.1-13, (9/1998)
Isophorone	2.78E-01	1.219	AP-42 Table 1.1-14, (9/1998)
Methyl bromide	7.68E-02	0.336	AP-42 Table 1.1-14, (9/1998)
Methyl chloride	2.42E-01	1.114	AP-42 Table 1.1-14, (9/1998)
5-Methyl chrysene	1.06E-05	0.000	AP-42 Table 1.1-13, (9/1998)
Methyl ethyl ketone	1.87E-01	0.819	AP-42 Table 1.1-14, (9/1998)
Methyl hydrazine	8.15E-02	0.357	AP-42 Table 1.1-14, (9/1998)
Methyl methacrylate	9.59E-03	0.042	AP-42 Table 1.1-14, (9/1998)
Methyl tert butyl ether	1.68E-02	0.074	AP-42 Table 1.1-14, (9/1998)
Methylene chloride	1.39E-01	0.609	AP-42 Table 1.1-14, (9/1998)
Naphthalene	6.24E-03	0.027	AP-42 Table 1.1-13, (9/1998)
Phenanthrene	1.30E-03	0.006	AP-42 Table 1.1-13, (9/1998)
Phenol	7.68E-03	0.034	AP-42 Table 1.1-14, (9/1998)
Propionaldehyde	1.82E-01	0.798	AP-42 Table 1.1-14, (9/1998)
Pyrene	1.58E-04	0.001	AP-42 Table 1.1-13, (9/1998)
Tetrachloroethylene	2.06E-02	0.090	AP-42 Table 1.1-14, (9/1998)
Toluene	1.15E-01	0.504	AP-42 Table 1.1-14, (9/1998)
1,1,1-Trichloroethane	9.59E-03	0.042	AP-42 Table 1.1-14, (9/1998)
Styrene	1.20E-02	0.053	AP-42 Table 1.1-14, (9/1998)
Xylenes	1.77E-02	0.078	AP-42 Table 1.1-14, (9/1998)
Vinyl acetate	3.65E-03	0.016	AP-42 Table 1.1-14, (9/1998)
Total PCDD/PCDF	1.17E-04	0.001	AP-42 Table 1.1-12, (9/1998)
Total Organic HAPs		**19.346**	**tpy**

TABLE 3-5
Unit 4 Boiler Acid Gas HAPs

Pollutant	Controlled Emissions (lb/hr)	Controlled Emissions (tons/yr)	Emission Factor Reference
Hydrogen Chloride	13.67	59.87	Engineering estimates
Hydrogen Fluoride	5.06	22.15	Engineering estimates
Total Acid Gas HAPs		**82.03**	**tpy**

3.3 Unit 4 Cooling Tower

The estimated hourly, daily, and annual controlled particulate emission rates from EP 145, the Unit 4 Cooling Tower, are shown in Table 3-6. Emissions are based on a 100% capacity factor.

TABLE 3-6
Unit 4 Cooling Tower Particulate Emissions

Pollutant	Hourly Emissions (lbs/hr)	Daily Emissions (lbs/day)	Annual Emissions (tpy)	Emission Factor Reference
Total Particulate Matter	6.4	154.2	28.1	Engineering Estimates
Particulate Matter PM_{10}	1.3	30.8	5.6	Engineering Estimates

3.4 Unit 4 Auxiliary Boiler

The estimated hourly, daily, and annual controlled emission rates of criteria pollutants from EP 142, the Unit 4 Auxiliary Boiler, are shown in Table 3-7. The emissions are based on 2,500 hours of operation per year on Fuel Oil No. 2.

TABLE 3-7
Unit 4 Auxiliary Boiler Emissions

Pollutant	Hourly Emissions (lbs/hr)	Daily Emissions (lbs/day)	Annual Emissions (tpy)	Emission Factor Reference
Sulfur Dioxide	7.12	170.88	8.65	AP-42 Tables 1.3-1 – 1.3-7
Nitrogen Oxides	20.06	481.44	24.36	AP-42 Tables 1.3-1 – 1.3-7
Particulate Matter PM_{10}	2.01	48.24	2.44	AP-42 Tables 1.3-1 – 1.3-7
Carbon Monoxide	5.01	120.24	6.09	AP-42 Tables 1.3-1 – 1.3-7
VOCs	0.34	8.16	0.41	AP-42 Tables 1.3-1 – 1.3-7
Lead	8.32E-03	0.20	1.01E-02	AP-42 Tables 1.3-1 – 1.3-7

3.5 Unit 4 Emergency Generator

The estimated hourly, daily, and annual controlled emission rates of criteria pollutants from EP 143, the Unit 4 Emergency Generator, are shown in Table 3-8. The emissions are based on 500 hours of operation per year on diesel fuel.

TABLE 3-8
Unit 4 Emergency Generator Emissions

Pollutant	Hourly Emissions (lbs/hr)	Daily Emissions (lbs/day)	Annual Emissions (tpy)	Emission Factor Reference
Sulfur Dioxide	0.54	13.01	0.14	AP-42 Section 3.4
Nitrogen Oxides	32.18	772.42	8.05	AP-42 Section 3.4
Particulate Matter PM_{10}	0.94	22.54	0.24	AP-42 Section 3.4
Carbon Monoxide	7.38	177.02	1.84	AP-42 Section 3.4
VOCs	0.86	20.64	0.22	AP-42 Section 3.4

3.6 Unit 4 Fire Pump

The estimated hourly, daily, and annual controlled emission rates of criteria pollutants from EP 144, the Unit 4 Fire Pump, are shown in Table 3-9. The emissions are based on 500 hours of operation per year on diesel fuel.

TABLE 3-9
Unit 4 Fire Pump Emissions

Pollutant	Hourly Emissions (lbs/hr)	Daily Emissions (lbs/day)	Annual Emissions (tpy)	Emission Factor Reference
Sulfur Dioxide	0.53	12.60	0.13	AP-42 Section 3.3
Nitrogen Oxides	7.75	186.00	1.94	AP-42 Section 3.3
Particulate Matter PM_{10}	0.55	13.20	0.14	AP-42 Section 3.3
Carbon Monoxide	1.68	40.20	0.42	AP-42 Section 3.3
VOCs	0.63	15.00	0.16	AP-42 Section 3.3

3.7 Unit 4 Coal Handling

The estimated hourly, daily, and annual controlled particulate emission rates from the Unit 4 Coal Handling System are shown in Table 3-10, Table 3-11, Table 3-12 and Table 3-13. The tables summarize particulate emissions; details on each emission point can be found in Appendix F – Emission Calculations. The emission sources include fugitives from the coal pile and coal handling system, and coal handling bag filter emissions from both new and modified equipment.

TABLE 3-10
Unit 4 Coal Pile – Fugitives

Pollutant	Maximum Hourly Emissions (lbs/hr)	Maximum Daily Emissions (lbs/day)	Annual Emissions (tpy)	Emission Factor Reference
Total Particulate Matter	5.11	122.64	22.39	AP-42 and Engineering Estimates
Particulate Matter PM_{10}	1.10	26.40	4.81	AP-42 and Engineering Estimates

Total wind erosion and maintenance fugitives from Unit 4 portion of active and inactive coal piles.
Includes emission points F-5A, F-5B, F-4A, F-4B and F-151B.

TABLE 3-11
Unit 4 Coal Handling – Fugitives

Pollutant	Maximum Hourly Emissions (lbs/hr)	Maximum Daily Emissions (lbs/day)	Annual Emissions (tpy)	Emission Factor Reference
Total Particulate Matter	2.35	56.30	10.27	AP-42 and Engineering Estimates
Particulate Matter PM_{10}	1.11	26.62	4.86	AP-42 and Engineering Estimates

Includes emission points F-151A (Conveyor C-11 to Stockout Pile) and F-151C (Dumping coal to Emergency Reclaim Hopper).

TABLE 3-12
Unit 4 Coal Handling System – New Sources

Pollutant	Maximum Hourly Emissions (lbs/hr)	Maximum Daily Emissions (lbs/day)	Annual Emissions (tpy)	Emission Factor Reference
Total Particulate Matter	6.90	165.60	30.25	Bag Filter Grain Loading Method
Particulate Matter PM_{10}	6.22	149.28	27.22	Bag Filter Grain Loading Method

Includes emission points EP-159 (Transfer Conveyor Bay), EP-160 (Unit 4 East Silos) and EP-161 (Unit 4 West Silos).

TABLE 3-13
Unit 4 Coal Handling System – Modified Sources

Pollutant	Maximum Hourly Emissions (lbs/hr)	Maximum Daily Emissions (lbs/day)	Annual Emissions (tpy)	Emission Factor Reference
Total Particulate Matter	15.19	364.56	66.55	Bag Filter Grain Loading Method
Particulate Matter PM_{10}	13.68	328.32	59.90	Bag Filter Grain Loading Method

Includes modified existing emission points EP-6A/7A (Rotary Car Dumper) and EP-13 (Transfer House 4).

3.8 Unit 4 Flyash/FGD Waste Handling and Hauling

The estimated hourly, daily, and annual controlled particulate emission rates from the Unit 4 Flyash/FGD Waste Handling System are shown in Table 3-14. The estimated hourly, daily, and annual controlled fugitive particulate emission rates from hauling flyash and FGD waste to the offsite landfill is shown in Table 3-15. Flyash and FGD waste are a combined product that is collected in the fabric filter hoppers following the Lime Spray Dryer FGD System.

TABLE 3-14
Unit 4 Flyash/FGD Waste Handling System

Pollutant	Maximum Hourly Emissions (lbs/hr)	Maximum Daily Emissions (lbs/day)	Annual Emissions (tpy)	Emission Factor Reference
Total Particulate Matter	1.15	27.60	5.08	Bag Filter and Filter Separator Grain Loading Method
Particulate Matter PM_{10}	1.03	24.72	4.58	Bag Filter and Filter Separator Grain Loading Method

Includes emission points EP-167 (Unit 4 Flyash/FGD Waste Silo), EP-168, EP-169 and EP-170 (Unit 4 Flyash/FGD Waste Vacuum System Exhauster #1, #2 and #3).

TABLE 3-15
Unit 4 Flyash/FGD Waste Haul Road

Pollutant	Maximum Hourly Emissions (lbs/hr)	Maximum Daily Emissions (lbs/day)	Annual Emissions (tpy)	Emission Factor Reference
Total Particulate Matter	8.78	87.80	22.43	AP-42 and Engineering Estimates
Particulate Matter PM_{10}	1.71	17.10	4.38	AP-42 and Engineering Estimates

Estimated fugitive emissions (F-904) for hauling Unit 4 flyash/FGD waste to offsite landfill on paved road.
Daily emissions based on 10 hours of hauling per day.

3.9 Unit 4 Lime Handling

The estimated hourly, daily, and annual controlled particulate emission rates from the Unit 4 Lime Handling System are shown in Table 3-16. The lime is used as a reagent in the Lime Spray Dryer FGD System.

TABLE 3-16
Unit 4 Lime Handling System

Pollutant	Maximum Hourly Emissions (lbs/hr)	Maximum Daily Emissions (lbs/day)	Annual Emissions (tpy)	Emission Factor Reference
Total Particulate Matter	0.43	10.32	1.88	Bag Filter and Filter Separator Grain Loading Method
Particulate Matter PM_{10}	0.38	9.12	1.70	Bag Filter and Filter Separator Grain Loading Method

Includes emission points EP-162 (Lime Filter Separator) and EP-163 (Lime Silo)

3.10 Unit 4 Urea Handling System

The estimated hourly, daily, and annual controlled particulate emission rates from the Unit 4 Urea Handling System are shown in Table 3-17. Urea is used to generate ammonia for the SCR System.

TABLE 3-17
Unit 4 Urea Handling System

Pollutant	Maximum Hourly Emissions (lbs/hr)	Maximum Daily Emissions (lbs/day)	Annual Emissions (tpy)	Emission Factor Reference
Total Particulate Matter	0.18	4.32	0.76	Bag Filter Grain Loading Method
Particulate Matter PM_{10}	0.16	3.84	0.68	Bag Filter Grain Loading Method

Includes emission points EP164A and EP164B (Urea Silos #1 and #2).

SECTION 4.0

Requested Permit Limits

This section presents the permit limits requested in this permit application.

4.1 Potential to Emit for Unit 4

The emission increases for the Unit 4 project are based on the potential to emit of new Unit 4, its ancillary equipment (mainly the auxiliary boiler and ash handling systems), and the new and modified coal handling sources. This section describes the procedure used to determine the potential to emit (PTE) for the proposed Unit 4 project.

4.1.1 Rationale for Determining Unit 4 Potential to Emit

The PTE values for Unit 4 use assumptions on what a newly constructed Unit 4 could achieve through the application of applicable NSPS and BACT for each pollutant under consideration. This includes the following assumptions:

- **Fuel and Unit Size**
  - A maximum boiler heat input of 7,675 mmBtu/hr.
  - A unit annual capacity factor of 100 percent.
  - A coal sulfur content of 0.5 percent.
  - A coal heating value of 8,000 Btu/lb.
- **SO_2**
  - The use of a lime spray dryer flue gas desulfurization system with an emission rate of 0.12 lb/MMBtu.
- NO_X
  - The addition of LNBs, OFA and SCR control.
  - A design SCR control efficiency of 60 percent.
- **Total PM and PM_{10}**
  - The use of a fabric filter baghouse with a design PM control efficiency of 99.7 percent.
- CO
  - The use of good combustion controls to limit CO emissions.
- VOC
  - The use of good combustion controls to limit VOC emissions.

- **Lead**

- The use of a fabric filter baghouse with a design PM control efficiency of 99.7 percent.

- **Sulfuric Acid Mist, Hydrogen Fluoride, Total Reduced Sulfur, and Reduced Sulfur Compounds**

- The use of a lime spray dryer FGD system.

4.1.2 Summary of Unit 4 Potential to Emit

A summary of the post-project potential to emit for Unit 4 is shown in Table 4-4. These emission rates are the maximum expected emission rates based on continuous operation of the new unit. These maximum hourly emission rates were the basis for Unit 4 modeling and analysis of air quality-related values (AQRVs). Additional information on CBEC plant emissions is contained in Appendix F.

4.2 PSD Permitting Applicability

The addition of the proposed Unit 4 is a major modification to an existing major stationary source. The pollutants subject to the PSD program and their significance levels are listed in Table 4-4. As shown in Table 4-4, the PTE for all criteria pollutants exceed the applicable significance levels for the proposed Unit 4 addition. Thus, PSD review is applicable to all criteria pollutants. Section 5 provides detailed information on applicable regulations.

The basic PSD permitting requirements that must be met for a major modification include:

- Application of BACT
- Performance of an ambient air quality impacts analysis (dispersion modeling)
- Analysis of impacts to soils, vegetation, and visibility
- Analysis of Class I area impacts

Section 6 of this application contains the BACT and MACT analysis. Section 7 contains the visibility and other impacts analysis.

4.3 Requested Emission Rate Limits

4.3.1 Unit 4 Emission Rates

Based on the results of the BACT analysis and Class II dispersion modeling, MEC requests the following emission rate limits for the proposed Unit 4.

SO_2: 0.12 lb/mmBtu heat input based on a 30-day rolling average as determined by the arithmetic average of all hourly emission rates for the 30 successive boiler operating days, except during period of startup, shutdown, maintenance/planned outage, or malfunction.

NO_X: 0.08 lb/mmBtu heat input based on a 30-day rolling average as determined by the arithmetic average of all hourly emission rates for the 30 successive boiler operating days, except during period of startup, shutdown, maintenance/planned outage, or malfunction.

Total PM: 0.020 lb/mmBtu heat input based on a 3-hour rolling average, except during periods of startup, shutdown, maintenance/planned outage, or malfunction.

PM_{10} (filterable): 0.018 lb/mmBtu heat input based on a 3-hour rolling average, except during periods of startup, shutdown, maintenance/planned outage, or malfunction.

CO: 0.16 lb/mmBtu heat input, except during periods of startup, shutdown, maintenance/planned outage, or malfunction.

VOC: 0.0036 lb/mmBtu heat input, except during periods of startup, shutdown, maintenance/planned outage, or malfunction.

4.3.2 Controlled Coal Handling Sources Emission Rate

MEC requests the following limits for new or modified coal handling equipment that is part of the Unit 4 project.

Emissions from the coal handling sources listed in Table 4-1 below shall be vented to a baghouse. Emissions from the baghouses shall be limited to 0.01 gr/dscf, and visible emissions from the baghouse vents shall not exceed 10% opacity.

TABLE 4-1
Coal Handling Sources

Emission Point	Description
159 (new)	Transfer Conveyor Bay
160 (new)	Unit 4 East Coal Silos
161 (new)	Unit 4 West Coal Silos
6/7 (modified)	Rotary Car Dumper
13 (modified)	Transfer House 4

4.3.3 Controlled Material Handling Sources Emission Rate

MEC requests the following limits for new material handling equipment that is part of the Unit 4 project.

Emissions from the material handling sources listed in Table 4-2 below shall be vented to a baghouse. Emissions from the baghouses shall be limited to 0.01 or 0.02 gr/dscf (see Table), and visible emissions from the baghouse vents shall not exceed 10% opacity.

TABLE 4-2
Material Handling Sources

Emission Point	Description	Emission Rate (gr/dscf)
162	Lime Filter Separator	0.01
163	Lime Silo	0.02
164A	Urea Silo #1	0.02
164B	Urea Silo #2	0.02
167	Flyash/FGD Waste Silo	0.02
168	Flyash/FGD Waste Vacuum Exhauster #1	0.01
169	Flyash/FGD Waste Vacuum Exhauster #2	0.01
170	Flyash/FGD Waste Vacuum Exhauster #3	0.01

4.3.4 Fugitive Dust Sources

MEC requests the following requirements for new or modified fugitive dust sources that are part of the Unit 4 project.

Plant roads used for hauling ash and sludge shall be controlled by the periodic use of a street sweeper. Visible emissions from roads shall not exceed 20% opacity as a 3 minute average. In addition, the ash and sludge trucks shall either be covered with a tarp or enclosed.

Fugitive emissions from the coal handling sources and coal storage piles shall be reduced by application of a chemical dust suppressant. Visible fugitive emissions from these sources shall not exceed 20% opacity as a 6-minute average.

4.3.5 Operating Hour Restrictions

MEC requests the following operating hour limits for the auxiliary fuel burning equipment listed in Table 4-3 that is part of the Unit 4 project.

TABLE 4-3
Operating Hour Restrictions

Emission Point	Description	Annual Operating Hours
142	Auxiliary Boiler	2500
143	Emergency Diesel Generator	500
144	Fire Pump	500

TABLE 4-4
Unit 4 Boiler Potential to Emit

Pollutant	Hourly Emissions[a] (lbs/hr)	Annual Emissions[a] (tpy)	PSD Significant Emission Rate (tpy)	Emission Factor Reference
Carbon Monoxide	1,179	5,166	100	Engineering Estimates
Fluorides (as HF)	5.1	22	3	Engineering Estimates
Lead	0.20	0.88	0.6	AP-42 Table 1.1-18
Nitrogen Oxides	614	2,689	40	Engineering Estimates
Particulate Matter PM_{10} (filterable & condensable)	195	854	15	Engineering Estimates
Particulate Matter PM_{10} (filterable)	138	605	15	Engineering Estimates
Reduced Sulfur Compounds	6.8	30	10	AP-42 Table 1.1-3 (b)
Sulfur Dioxide	921	4,034	40	Engineering Estimates
Sulfuric Acid Mist	32.3	142	7	Engineering Estimates
Total Particulate Matter (filterable)	154	672	25	Engineering Estimates
Total Reduced Sulfur	6.8	30	10	AP-42 Table 1.1-3 (b)
VOCs	28.8	126	40	AP-42 Table 1.1-19

5.1.1.2.1 New Source Review Significant Emission Increase Definition

By themselves, coal-fired utility boilers of the size and capacity of the proposed unit at CBEC typically are categorical sources whose emissions of sulfur dioxide (SO_2), nitrogen oxides (NO_X), carbon monoxide (CO), particulate matter (PM_{10}) and volatile organic compounds (VOCs) traditionally exceed the major source threshold established within the federal rules under 40 CFR 51. Iowa has been delegated full authority from EPA for administering the federal NSR rules. Since the CBEC is an existing major source, the construction of an additional generating unit is considered to be a modification, for which even lower "significant" emission thresholds trigger the NSR process. Under the Clean Air Act significant is defined as: "A net emissions increase or the potential of a source to emit....equal to or greater than.... carbon monoxide 100 tpy; nitrogen oxides 40 tpy; sulfur dioxide 40 tpy; PM_{10} 15 tpy; particulate matter 25 tpy; ozone 40 tpy of VOCs; lead 0.6 tpy; sulfuric acid (H_2SO_4) mist 7 tpy; hydrogen sulfide, 10 tpy; total reduced sulfur compounds (TRS) (including H_2S), 10 tpy...." The net emissions increase for SO_2, NO_X, CO, PM_{10}, VOCs, H_2SO_4 and TRS from the addition of Unit 4 are above the limits specified for significant net emissions increase. In addition, Unit 4 is considered a major stationary source. Therefore, the addition of Unit 4 is considered a major modification of an existing stationary source and is subject to requirements for SO_2, NO_X, CO, PM_{10}, VOCs, H_2SO_4 and TRS.

5.1.1.2.2 Prevention of Significant Deterioration

Since Unit 4 will be located in an area classified as attainment for criteria pollutants, the requirements of the federal PSD program will apply to the construction of Unit 4. The IDNR has been delegated full authority from the EPA for administering the federal PSD rules; consequently, these requirements are codified within the state permitting rules at IAC 22.4.

The PSD program defines a major stationary source as:

1. Any source type belonging to one of 28 source categories that has PTE of 100 tpy or more of any conventional (or "criteria") pollutant regulated under the CAA or,

2. Any other source type with a PTE of 250 tpy of any pollutant regulated under the CAA.

The facility belongs to one of the 28 listed source categories (fossil-fuel boilers, combinations thereof, totaling more than 250 MMBtu's per hour heat input) and is considered an existing major stationary source because the PTE for SO_2, NO_X, CO, PM_{10}, VOCs, lead, H_2SO_4 , HF, Reduced Sulfur Compounds and TRS all exceed the limits listed in this section.

Modifications to an existing major stationary source are considered major and subject to PSD review if a net emissions increase is equal to or greater than the corresponding significant emissions increase threshold for each respective pollutant. A net emissions increase includes both of the following:

- The potential increase in emissions due to the modification itself; and
- Contemporaneous net emissions increases and decreases of regulated air pollutants, under the PSD program.

An emissions increase is considered significant if emissions meet or exceed any of the following rates:

- Carbon monoxide, 100 ton per year (tpy);

- Carbon monoxide, 100 ton per year (tpy);
- Nitrogen oxides, 40 tpy;
- Sulfur dioxide, 40 tpy;
- PM_{10} Particulate matter, 15 tpy;
- Particulate matter, 25 tpy;
- Ozone, 40 tpy of volatile organic compounds;
- Lead, 0.6 tpy;
- Asbestos, 0.007 tpy;
- Beryllium, 0.0004 tpy;
- Mercury, 0.1 tpy;
- Vinyl Chloride, 1 tpy;
- Fluorides, 3 tpy;
- Sulfuric acid mist, 7 tpy;
- Hydrogen Sulfide, 10 tpy;
- Total reduced sulfur (including H2S), 10 tpy;
- Reduced sulfur compounds (including H2S), 10 tpy.

The basic PSD permitting requirements that must be met for a major modification include:

- BACT (presented in Section 6);
- Performance of an ambient air quality impacts analysis (dispersion modeling) (presented in Section 7);
- Analysis of impacts to soils, vegetation, and visibility (air quality related values) (presented in Section 7); and
- Analysis of Class I area impacts (presented in Section 7).

These requirements apply to attainment pollutants for which the modification is significant. As stated above, net emission increases of SO_2, NO_X, CO, PM_{10}, VOCs, lead, H_2SO_4 , HF, Reduced Sulfur Compounds and TRS associated with the proposed Unit 4 exceed significant emission rate thresholds. Based on the emissions the proposed addition of Unit 4 will be a major modification (subject to the federal and state PSD program requirements) for SO_2, NO_X, CO, PM_{10}, VOCs, lead, H_2SO_4, HF, Reduced Sulfur Compounds and TRS.

CBEC is located in a PSD area and is subject to the provisions in 567 IAC 22.4. Pursuant to this section, Unit 4 must meet all applicable emissions requirements of these provisions and modifications must be reviewed by the IDNR to determine the air quality impact of Unit 4. In addition, CBEC is required to include the following information with the air quality construction permit application:

- An analysis of the air quality impact and a demonstration that increases will not contribute to a violation of an ambient air quality standard or PSD increment.
- An analysis of ambient air quality in the affected area for each pollutant that a new source would have the potential to emit in a significant amount,
- An analysis of the air quality related impact including an analysis of the impairment to visibility, soils, and vegetation and the projected air quality impact from general

commercial, residential, industrial, and other growth associated with the source or modification, and

- Other information as requested by the IDNR.

5.1.1.3 Title V Regulations (567 IAC 22.100 through 22.116)

The federal operating permits program (Title V) is implemented by regulations codified at 40 CFR Part 70 and 71. The State of Iowa has been granted authority to implement and enforce the federal Title V program through state regulations outlined under 567 IAC Chapter 22 Sections 100 through 116. CBEC currently has an IDNR issued Title V Operating Permit (Permit No. 97-TV-001-M004). Pursuant to 567 IAC 22.113, the addition of Unit 4 will constitute a significant modification to the existing facility and will require a modification of the existing Title V permit. An application for a Title V permit revision is required within one year of commencing operation of the Unit 4, as specified in 567 IAC 22.105(1)(a)(5).

5.1.1.4 Acid Rain Sources (567 IAC 22.120 through 22.148)

As outlined in 567 IAC Chapters 22.120 through 22.148, for purposes of implementing an acid rain program that meets the requirements of Title IV of the Clean Air Act, the provisions of 40 CFR Part 72 are incorporated into Parts 73, 75, 76 and 77 by reference. The State of Iowa administers the Acid Rain Program through adoption of 40 CFR 72 of the federal code. These requirements are discussed in section 5.1.2.3.

5.1.2 Federal Air Permit Requirements

Described below are the three basic types of federal permits that Unit 4 and CBEC are subject to:

5.1.2.1 Major Source NSR/PSD (40 CFR 51)

The IDNR has been delegated full authority from EPA for administering the federal PSD and NSR rules. These rules are summarized in section 5.1.1.1 and 5.1.1.2 of this application.

5.1.2.2 Operating Permit Program (40 CFR Parts 70 and 71)

The IDNR has been delegated full authority from EPA for administering the federal Title V operating permit program rules. These rules are summarized in section 5.1.1.3 of this application.

5.1.2.3 Acid Rain Program (40 CFR Parts 72, 73, 75, 76, and 77)

As a coal-fired electric utility boiler, Unit 4 will be subject to the SO_2 allowance allocation, NO_X emission limitations, and monitoring provisions of the federal acid rain program. The existing acid rain permit for CBEC will be modified to incorporate the new unit. A Continuous Emissions Monitoring System (CEMS) will be designed, fabricated, installed, and certified on the new unit, in accordance with the requirements of Part 75.

5.2 Other State and Federal Air Quality Requirements

5.2.1 Overview of State Air Quality Regulations

The following comments all pertain to Articles within 567 IAC Chapters 20 through 31. Refer to Table B-1 for further details on the applicability of specific regulatory sections.

1. The provisions of 567 IAC Chapter 20 are general in nature, do not provide specific standards, limitations, or other requirements applicable to Unit 4, but do govern other provisions in other Chapters that pertain specifically to Unit 4 upon commencement of construction and during future operations.
2. The provisions of 567 IAC Chapter 21 pertain to compliance and do not provide specific standards, limitations, or other requirements applicable to Unit 4 at this time, but do govern other provisions in other Chapters that pertain specifically to Unit 4 upon commencement of construction and during future operations.
3. The provisions of 567 IAC Chapter 22 concern controlling pollution; in general, these provisions apply to this facility, including the sections on construction permits, Title V and Acid Rain.
4. The provisions of 567 IAC Chapter 23 pertain to emission standards for contaminants. Specific sections that apply to Unit 4 are outlined in Section 5.2.2.1.
5. The provisions of 567 IAC Chapter 24 pertains to excess emissions. This applies to CBEC and Unit 4 at all times. Refer to Section 5.2.2.2.
6. The provisions of 567 IAC Chapter 25 pertain to measurement of emissions. This section requires CEMs on Unit 4 and the associated monitoring and recordkeeping.
7. The provisions of 567 IAC Chapter 26 pertain to prevention of emergency episodes. This section applies to CBEC.
8. The provisions of 567 IAC Chapter 27 pertain to certificate of acceptance for public entities interested in adopting their own air regulations. This chapter is not applicable to CBEC.
9. The provisions of 567 IAC Chapter 28 pertain to ambient air quality standards. These are the NAAQS and are applicable to CBEC and Unit 4.
10. The provisions of 567 IAC Chapter 29 pertain to qualification of visual determination of the opacity of emissions. This section is applicable to CBEC and Unit 4.
11. The provisions of 567 IAC Chapter 30 are reserved for future use.
12. The provisions of 567 IAC Chapter 31 pertain to nonattainment areas. This chapter is not applicable to CBEC since it is located in an attainment area.

5.2.2 Specific Applicable State Regulations

Listed below are specific applicable state air regulations that apply to Unit 4.

5.2.2.1 Emission Standards (567 IAC 23.1)

The IAC adopts the applicable federal new source performance standards (NSPS) and the national emission standards for hazardous air pollutants (NESHAPs) under 567 IAC Chapter 23 Section 1. Applicable regulations are listed under following Sections:

- 567 IAC 23.1(2) v – Coal Preparation Plants (40 CFR 60 Subpart Y),
- 567 IAC 23.1(2) z – Electric Utility Steam Generating Units (40 CFR 60 Subpart Da).
- 567 IAC 23.1(3) a – NESHAP - Asbestos (40 CFR 61 Subpart M)
- 567 IAC 23.1(4)(b)(1) and (2) – Requirements for control technology determinations for major sources in accordance with Clear Air Act Sections 112(g) and 112 (j).
- 567 IAC 567 – 23.1(6) Emission Standards – Calculation of Emission Limitations based on Stack Height
- 567 IAC 23.2(1) – Open burning of combustible materials is prohibited, except as provided in 23.2(2) and 23.2(3)

5.2.2.2 Excess Emissions (567 IAC 24)

If excess emissions occur as a result of equipment malfunction other than startup, shutdown or cleaning of control equipment oral and written reporting to the IDNR is required under 567 IAC 24.1. There are specific guidelines that apply to electric utilities to ensure that consumer demand is met.

The IAC also requires that equipment and control equipment is maintained to minimize emissions under 567 IAC 24.2.

5.2.2.3 Measurement of Emissions (567 IAC 25)

Continuous emissions monitoring (CEMs) equipment is required under 567 IAC 25.1(1) for coal-fired steam generating units with a rated capacity greater than 250 MMBTUs/hr. This section also outlines the maintenance and reporting requirements.

5.2.2.4 Prevention of Emergency Episodes (567 IAC 26)

CBEC is a power generating facility and is required under 567 IAC 26 to prepare a preplanned abatement strategy to prevent the buildup up of air pollution contaminants during an air pollution episode.

5.2.2.5 Ambient Air Quality Standards (567 IAC 28)

Iowa has adopted the National Ambient Air Quality Standards under 567 IAC 28. These are applicable to CBEC and Unit 4.

5.2.2.6 Monitoring and reporting

After the construction permit and subsequently the Title V Permit are received, CBEC will be required to conduct monitoring, submit emission reports, insure that equipment meets certain specification, and other activities as IDNR requests. Some of these requirements are enumerated, below:

- Meet the reporting requirements specified in 567 IAC 24,
- Submit and retain an annual hazardous air pollutant inventory and an annual air emission inventory (567 IAC 22.100 through 22.116),
- Conduct emissions testing in accordance with (IAC 25.1(7)),
- Install CEMS and submit related reports to IDNR (567 IAC 25),
- Conduct opacity observations in accordance with EPA Method 9 (567 IAC 29),
- Ensure that stacks are consistent with good engineering practices (GEP) (567 IAC 23.1(6)).

5.2.3 Other Federal Air Quality Regulations

5.2.3.1 National Emission Standards for Hazardous Air Pollutants (HAPs) (40 CFR Part 61 and 63)

40 CFR 61.01 through 61.08 provides requirements to receive authorization from the EPA (or designated states) before construction or modification of a source. This application is being submitted pursuant to these paragraphs. 40 CFR 61.09 through 61.15 provide the reporting and monitoring requirements applicable to Unit 4.

Certain sections of NESHAP Subpart M, "National Emission Standard for Asbestos" are likely to be applicable to the existing CBEC facility, since the installation of asbestos-containing building materials (ACBM) and thermal system insulation (TSI) was commonplace prior to the late 1970s. MidAmerican Energy will be required to determine the presence of ACBM and TSI throughout the plant and assess the potential for existing ACBM or TSI to become disturbed or damaged during construction of Unit 4. The following sections of Subpart M apply to the CBEC:

§61.140	Applicability
§61.141	Definitions
§61.145	Standard for demolition and renovation
§61.148	Standard for insulating materials
§61.150	Standard for waste disposal for....demolition, renovation ...operations.

The remaining sections of 40 CFR 61 provide guidelines and requirements for specific sources that CBEC does not operate; therefore, these sections do not apply to Unit 4 or CBEC in general.

The National Emission Standards for Hazardous Air Pollutants for Source Categories are codified in 40 CFR Part 63. The emission limitations within Part 63 are referred to as Maximum Achievable Control Technology (MACT) standards. At present, the EPA has not promulgated a final MACT standard for coal-fired power plants under Part 63, although these facilities have been listed pursuant to §112(g) of the federal Clean Air Act since December, 2000. Consequently, MidAmerican Energy was required to have submitted a Part 1 application to the EPA or the IDNR, relative to requesting a case-by-case MACT determination for the CBEC. Since the addition of Unit 4 will eventually lead to the reopening of the existing Title V permit issued by IDNR for the plant, this application includes a proposed case-by-case MACT determination for that new generating unit; (see Section 6.3 of this application).

5.2.3.2 Compliance Assurance Monitoring Program (40 CFR Part 64)

Since the existing facility and the proposed Unit 4 will be an "affected unit" subject to the federal acid rain program monitoring provisions, codified at 40 CFR Part 75, the CBEC is exempt from the federal Compliance Assurance Monitoring (CAM) program requirements, codified at 40 CFR Part 64, for SO_2 and NO_X, pursuant to 40 CFR 64.2(b)(1)(iii). However, the unit will be subject to CAM requirements for SO_2 and NO_X with respect to Part 60 and IDNR permit limitations. The facility will also be subject to CAM requirements for particulates with respect to Part 60, Subparts Da and Y and IDNR permit limitations.. The CAM Plan for Unit 4 is contained in Section 9 of this application.

5.2.3.3 New Source Performance Standards (40 CFR Part 60)

These rules establish emission limitations for sulfur dioxide, nitrogen oxides, and particulate matter and provide a variety of requirements for monitoring, record keeping, and reporting of emissions and other information. Any emissions unit subject to an NSPS subpart is also subject to the general provisions under Subpart A (codified at 40 CFR 60.1 through 60.19). CBEC Unit 4 will also be subject to the provisions in Appendices B and F which outline requirements and specifications for continuous opacity monitoring systems (COMS), CEMS and the Quality Assurance and Quality Control Plans required for these monitoring systems. Guidance regarding State Plans is provided in sections 40 CFR 60.20 through 60.29 (Subpart B); these sections do not apply to CBEC.

Sections 40 CFR 60.30 through 60.39 (Subpart C) are specific to waste combustion units, incinerators, solid waste landfills and sulfuric acid production plants. CBEC does not conduct any of these processes; therefore the requirements in this section do not apply to the CBEC facility.

The provisions of 40 CFR 60.40 through 60.49 (Subpart D) apply to fossil fuel-fired steam boilers having a heat input of 250 MMBtu per hour or more, and constructed since August 17, 1971. The CBEC Unit 3 fits this definition, and is subject to the provisions of NSPS Subpart D. However, similar electric utility units constructed after September 18, 1978 are subject to the requirements of NSPS Subpart Da (see next paragraph) which, for such units, supercedes Subpart D. Units 1 and 2, while having a heat input greater than 250 MMBtu per hour, were constructed during the 1950s and are considered "pre-NSPS". The provisions of 40 CFR Part 60 do not apply to Units 1 and 2 at the CBEC.

The provisions of 40 CFR 60.40a through 60.49a (Subpart Da) apply to electric utility steam generating units having a heat input of 250 MMBtu per hour or more and constructed on or after September 18, 1978. The proposed Unit 4 will be a nominal net 750 MW coal-fired electric utility steam boiler rated at 7,675 MMBtu per hour heat input and is therefore subject to the requirements of 40 CFR Subpart Da. According to this subpart, all monitoring activities and reports of emissions should be documented and retained on file, and the following may not be exceeded:

- Particulate Matter 0.03 lb/MMBtu (§ 60.42a),
- Opacity of 20 percent, except for one 6-minute period per hour (§ 60.42a),

- SO_2 1.2 lb/MMBtu (§ 60.43a),
- 90 percent SO_2 reduction (or 70 percent reduction if emissions are less than 0.60 lb/MMBtu) (§ 60.43a), and
- NO_X 0.6 lb/MMBtu (§ 60.44a)
- NO_X 1.6 lb/Megawatt hour gross energy output (§ 60.44a)

COMS and CEMS must be installed, calibrated, maintained, operated, and recorded in accordance with the requirements in 40 CFR 60.47a through 60.49a. Documentation is required to be maintained regarding performance tests and calibration and maintenance of equipment. These monitoring systems shall be certified in accordance with the Performance Specifications provided in Appendix B to Part 60, and maintained in accordance with the Quality Assurance requirements provided in Appendix F to Part 60. Note that some of the criteria and certification test requirements within these NSPS appendices are, (for acid rain sources), superceded by certain provisions within 40 CFR Part 75, which was promulgated later.

The 137.4 MMBtu/hr diesel-fired auxiliary boiler planned for Unit 4 will be subject to the provisions of 40 CFR Part 60 Subpart Db.

The CBEC is also subject to the provisions of NSPS Subpart Y, "Standards of Performance for Coal Preparation Plants", codified at §60.250 through 60.254. These rules establish particulate emission limitations and opacity standards for thermal dryers, pneumatic coal-cleaning systems, coal handling, conveying and enclosed storage equipment. The CBEC does not have any thermal dryers or pneumatic coal-cleaning equipment; therefore the provisions of Subpart Y only apply to the coal handling, conveyance and storage facilities. 40 CFR 60.250 provides rule applicability information and 40 CFR 60.251 provides several definitions. 40 CFR 60.252, "Standards for Particulate Matter" establishes a 20% opacity limitation for these equipment items. 40 CFR 60.253 provides monitoring requirements, which are only applicable to thermal dryers; (and thus do not apply to CBEC). Finally, 40 CFR 60.254 requires that Reference Methods 5 (particulate mass emission rate) and 9 (opacity) be employed for performance tests required under §60.8.

5.2.3.3.1 Nitrogen Oxides and Excess Emissions (40 CFR Parts 76 and 77)

Under 40 CFR 76, CBEC Unit 4 is considered a Group I, Phase II boiler and shall either discharge emissions of NO_X in amounts less than 0.40 lb/MMBtu on an annual average basis for tangentially-fired boilers or 0.46 lb/MMBtu on an annual average basis for dry bottom wall-fired boilers.

5.2.4 Regulatory Applicability Summary Matrix

Appendix B contains Tables B-1 and B-2 that summarize Iowa and Federal Requirements, respectively. The table identifies these requirements, denotes applicability, provides an explanation and, if necessary, defines the methods to be used to demonstrate compliance.

SECTION 6.0

Control Technology Analysis

This section describes the air pollution control equipment that will be utilized on the proposed MidAmerican Council Bluffs Energy Center (CBEC) Unit 4 and the Best Available Control Technology analysis for applicable pollutants.

6.1 Pollution Controls

The proposed CBEC Unit 4 will be equipped with pollution controls to limit the emissions of sulfur dioxide (SO_2), sulfuric acid mist, total reduced sulfur (TRS), reduced sulfur compounds, hydrochloric acid (HCl), fluorides as hydrogen fluoride (HF), nitrogen oxides (NO_X), particulate matter (PM), particulate matter less than 10 micrometers in diameter (PM_{10}) and lead.

6.1.1 Sulfur Dioxide and Related Compounds

Emissions of sulfur dioxide and other sulfur compounds will be controlled on CBEC Unit 4 with the use of a lime spray dryer flue gas desulfurization (FGD) system. The FGD system will have a design SO_2 emission rate of 0.12 lb/MMBtu, which corresponds to a SO_2 removal efficiency of 90.4 percent at the maximum coal sulfur content of 0.50%.

The lime spray dryer FGD system will also have a similar removal efficiency for the control of sulfuric acid mist, total reduced sulfur (TRS) and reduced sulfur compounds.

In a dry FGD system lime (calcium oxide) reagent is slaked to form calcium hydroxide slurry. The slurry contacts the flue gas when it is sprayed as finely atomized droplets through a rapidly spinning atomizing wheel into a spray dryer vessel. The spray dryer vessel will be installed in the flue gas ductwork upstream of a baghouse. The flue gas temperature leaving the spray dryer vessel is maintained about 25°F above the adiabatic approach to the saturation point. This allows carbon steel construction of the spray dryer vessel and steel-lined stacks. The spray dryer vessel has sufficient residence time (about 10 seconds) to allow the SO_2 in the flue gas to react with the reagent as the water in the slurry droplets evaporates, forming a dry calcium sulfite and calcium sulfate byproduct. This dry byproduct, along with remaining flyash, is collected in the bottom of the spray dryer vessel and in the downstream baghouse. A portion of the collected dry solids will be re-slurried and re-injected into the spray dryer to improve reagent utilization. The collected dry solids will be pneumatically conveyed to a storage silo and trucked to a landfill disposal site. The dry lime FGD system for CBEC Unit 4 will be designed to meet the SO_2 emission levels described in Section 4.

There is additional removal of SO_2, H_2SO_4, TRS and Reduced Sulfur Compounds due to absorption and collection of the dry fly ash/reaction product mixture that takes place in the fabric filter.

6.1.2 Hydrochloric Acid and Hydrogen Fluoride

The use of the lime spray dryer flue gas desulfurization system on CBEC Unit 4 will also reduce hydrochloric acid (HCl) and hydrogen fluoride (HF) potential emissions by 90 percent. Based on operating data at other coal fired utilities and municipal waste combustors (MWC) that utilize combination lime spray dryer and fabric filter control systems, very high acid gas removal efficiencies have been demonstrated. Removal efficiencies up to 99% for HCl and 95% for HF have been reported. The level of control is also dependent on the coal properties. Some of the HCl and HF removal occurs in the spray dryer vessel itself due to the reaction with the lime slurry. Removal also takes place as a result of the flue gas humidification and the collection of the reagent and flyash product on the fabric filter bags.

6.1.3 Nitrogen Oxides

NO_X is formed in the boiler in the combustion process, particularly when the peak combustion temperatures in the flame exceed 2500° F. The emissions of NO_X from CBEC Unit 4 will be limited through the use of low NO_X burners (LNB) and selective catalytic reduction (SCR). Low NO_X burners control the formation of NO_X by staging the combustion of the coal to keep the peak flame temperature below the threshold for NO_X formation. The burner initially introduces the coal into the boiler with less air than is needed for complete combustion. The flame is then directed toward an area where additional combustion air is introduced from over fire air ports allowing final combustion of the fuel. A selective catalytic reduction unit will also be installed on CBEC Unit 4 to further reduce the NO_x emissions. The proposed SCR is designed for high dust loading applications, and will be located external from the boiler. The SCR system uses a catalyst and a reductant (ammonia gas, NH_3) to dissociate NOx into nitrogen gas and water vapor. The catalytic process reactions for this NOx removal are as follows:

$$4NO + 4NH_3 + O_2 \rightarrow 4N_2 + 6H_2O \text{ and,}$$

$$2NO_2 + 4NH_3 + O_2 \rightarrow 3N_2 + 6H_2O.$$

The optimum temperature window for this catalytic reaction is between approximately 575 to 750°F. Therefore, the SCR reaction chamber will be located between the boiler economizer outlet and air heater flue-gas inlet. The system will be designed to use anhydrous ammonia as the reducing agent. Ammonia injection pipes, nozzles and a mixing grid will be located upstream of the reaction chamber. A diluted mixture of ammonia gas in air will be dispersed through injection nozzles into the flue-gas stream. The ammonia/flue-gas mixture then enters the reactor where the catalytic reaction occurs. Ammonia for the SCR will be generated from dry urea at CBEC Unit 4.

Based on technical information provided by boiler vendors, it is anticipated that NO_X emissions from the boiler economizer (prior to the SCR) can be controlled with low NO_X burners and overfire air to 0.20 lb/mmBtu (approximately 143 ppmvd @ 3% O_2) while maintaining acceptable levels of CO and VOC. Assuming a NO_X inlet concentration of 143 ppmvd @ 3% O_2, the SCR will be designed to reduce the NO_X concentration to approximately 57 ppmvd @ 3% O_2, or 0.08 lb/mmBtu. This represents a SCR removal efficiency of 60% above the control of low-NO_X burners alone.

The LNB and SCR system for CBEC Unit 4 will be designed to meet the NO_x emission levels described in Section 4.

6.1.4 Particulate Matter and Particulate Matter less than 10 Micrometers in Diameter (PM_{10})

Particulate matter and particulate matter less than 10 micrometers in diameter (PM_{10}) will be controlled at CBEC Unit 4 by a pulse-jet fabric filter.

The pulse jet fabric filter will process the exhaust flue gas from the spray dryer(s) outlet. The pulse jet baghouse will consist of a number of compartments containing fabric filter bags fitted over a wire cage and suspended from a horizontal tube sheet in the compartment. The flue gas flows from the outside of the bags to the inside. The wire cage is required to keep the bags from collapsing. From the inside of the bag clean flue gas exits to a clean air plenum and is discharged via ductwork to the stack. Particulate matter that collects on the outside of the bags is removed by an intermittent reverse pulse of high pressure compressed air applied on-line during timed cleaning cycles. The particulate matter collects in hoppers below the compartments and is removed via airlock valves by a pneumatic conveying system to a storage silo. The fabric filter will have a design total particulate removal efficiency of 99.7%.

6.1.5 Lead

The use of a fabric filter and dry lime FGD system on CBEC Unit 4 will reduce potential lead emissions by 99 percent. Lead is emitted as a trace metal in the flyash leaving the boiler. The removal of lead correlates with the collection efficiency of the particulate removal device. Since the fabric filter will remove 99%+ of the total particulate matter, the removal efficiency of lead will be similar.

6.1.6 Carbon Monoxide and Volatile Organic Compounds

Carbon monoxide (CO) and non-methane volatile organic compounds (VOC) are formed from the incomplete combustion of the coal in the boiler. The formation of CO and VOC's is limited by controlling the combustion of the fuel and providing adequate oxygen for complete combustion. Thus, good combustion control is the technique to be used to limit CO and VOC emissions.

6.2 BACT Determination

This section presents the required Best Available Control Technology (BACT) analyses.

6.2.1 Applicability

The requirement to conduct a BACT analysis and determination is set forth in section 164(a)(4) of the Clean Air Act and in federal regulations 40 CFR 52.21(j).

6.2.2 Top-Down BACT Process

EPA has developed a process for conducting BACT analyses. This method is referred to as the "top-down" method. The steps to conducting a "top-down" analysis are listed in EPA's "New Source Review Workshop Manual," Draft, October 1990. The steps are:

- Step 1 – Identify All Control Technologies;
- Step 2 – Eliminate Technically Infeasible Options;
- Step 3 – Rank Remaining Control Technologies by Control Effectiveness;
- Step 4 – Evaluate Most Effective Controls and Document Results; and
- Step 5 – Select BACT.

Each of these steps has been conducted for SO_2, NO_x, CO, VOC , PM, PM_{10}, lead and fluoride and is described below.

6.2.3 SO_2 Analysis

The BACT analysis for Sulfur Dioxide is presented below. The analysis is also applicable to the related compounds; Sulfuric Acid Mist, Total Reduced Sulfur and Reduced Sulfur Compounds.

6.2.3.1 Step 1 – Identify All Control Technologies

Sulfur dioxide (SO_2) will be emitted from the proposed CBEC Unit 4 as a result of the combustion of coal that contains sulfur. The first step is to evaluate SO_2 controls determined to be BACT by permitting agencies across the United States. This information is available from the EPA RACT/BACT/LAER Clearinghouse (RBLC) database accessible on the Internet. The printout from the database for SO_2 is shown in Appendix D, Table E-8.

The potential SO_2 emission reduction options found in the RBLC are:

- Wet lime scrubbing;
- Wet limestone scrubbing;
- Lime spray dryer;
- Circulating dry scrubber.

The control efficiencies range from 73% to 95%. However, with the exception of two projects in Wyoming using a circulating dry scrubber and one project in Wyoming using a lime spray dryer, the reported removal rates are 90% to 95%.

6.2.3.2 Step 2 – Eliminate Technically Infeasible Options

The first three of these options are technically feasible for use in reducing SO_2 emissions from CBEC Unit 4. However, the use of a circulating dry scrubber requires the use of high calcium fly ash to provide the alkalinity needed to react with SO_2. The potential coals for CBEC Unit 4 are not particularly high in calcium. In addition, control efficiencies for circulating dry scrubbers have not been demonstrated above 80% in the RBLC database. For these two reasons this technology was eliminated from further consideration.

6.2.3.3 Step 3 – Rank Remaining Control Technologies by Control Effectiveness

Emission rates for each of the remaining SO_2 removal technologies are ranked in order of their control effectiveness. These effectiveness values are provided in Table 6-1.

TABLE 6-1
SO_2 Control Technology Emission Rate Ranking

Control Technology	SO_2 % Reduction [a]
Wet Lime Scrubbing	95 – 98
Wet Limestone Scrubbing	95 – 98
Lime Spray Dryer	90 - 95
NSPS Limit	70 [b]

[a] Estimate of maximum continuous SO_2 emission control efficiency. FGD control efficiencies will be in the lower end of the range when used with low sulfur coal.

b Applicable when SO_2 emissions are less than 0.60 pounds per million BTU.

The PSD NSR regulations require that BACT, at a minimum, meet the applicable NSPS limit, 40 CFR 60 Subpart Da. Because there is an NSPS that applies to the boiler, the NSPS emission limit is also included in the ranking.

6.2.3.4 Step 4 – Evaluate Most Effective Controls and Document Results

This step involves the consideration of energy, environmental, and economic impacts associated with each control technology. The top-down process requires that the evaluation begin with the most effective technology.

Wet Limestone/Lime FGD

Wet SO_2 scrubbers operate by flowing the flue gas upward through a large reactor vessel that has an alkaline reagent (i.e., lime or limestone slurry) flowing down from the top. The scrubber mixes the flue gas and alkaline reagent using a series of spray nozzles to distribute the reagent across the scrubber vessel. The calcium in the reagent reacts with the SO_2 in the flue gas to form calcium sulfite and/or calcium sulfate that is removed from the scrubber with the sludge and is disposed. Most wet FGD systems utilize forced oxidation to assure that only a calcium sulfate sludge is produced.

The creation of sludge from the scrubber does create a solid waste handling and disposal problem. This sludge needs to be handled in a manner to not result in ground water contamination. Also, the sludge disposal area needs to be permanently set aside from future surface uses since the disposed sludge can not bear any weight from such uses as buildings or cultivated agriculture.

Other disadvantages associated with wet limestone or lime FGD includes the creation of a visible wet stack plume, generation of primary particulate matter by the scrubbing process, increased acid gas emissions, high energy costs, incompatibility with mercury removal options and water/wastewater issues. Wet FGD generates more primary particulate emissions leaving the stack than dry FGD systems because the particulate removal device

(ESP or Fabric Filter) is upstream of the scrubber instead of downstream as in this case. Sulfuric acid removal for a wet FGD system is in the range of 40 to 60% compared to 90% for a lime spray dryer/fabric filter combination. The potential future use of activated carbon or sorbent injection for mercury removal is also limited with a wet FGD application since the fabric filter is upstream of the scrubber and the flue gas temperature is higher than the optimum mercury capture range.

Spray Dryer Followed by Fabric Filter

Spray dryers operate by flowing the flue gas through a large vessel. In the top of the vessel is a rapidly rotating atomizer wheel through which lime slurry is flowing. The rapid speed of the atomizer wheel causes the lime slurry to separate into very fine droplets that intermix with the flue gas where the SO_2 in the flue gas react with the calcium in the lime slurry to form particulate calcium sulfate. This dry material is captured in the fabric filter along with the fly ash.

Fabric filtration has been widely applied to coal combustion sources since the early 1970s and consists of a number of filtering elements (bags) along with a bag cleaning system contained in a main shell structure incorporating dust hoppers. Fabric filters use fiberglass fabric bags as filters to collect particulate matter. The particle-laden gas enters a fabric filter compartment and passes through the bags and through a layer of accumulated particulate matter collected on the fabric of the filter bags. The collected particulate matter forms a filter cake layer on the bag that enhances the bag's filtering efficiency. However, excessive caking will increase the pressure drop across the fabric filter. When this occurs, the fabric filter is placed into a cleaning cycle and the excess particulate matter is removed by the ash handling system.

On this project, MidAmerican Energy is proposing the installation of a lime spray dryer flue gas desulfurization system that produces a dry waste product suitable for landfill disposal.

Since dry lime scrubbing is being proposed for this project, the environmental, energy and economic impacts must be examined. A cost estimate for dry lime FGD installation and operation has been prepared for this project and is provided in Appendix E. The effective cost of a dry lime scrubber has been estimated at $605 per ton of SO_2 controlled. An incremental cost analysis has also been prepared based on the use of wet limestone FGD with a control efficiency of 95%. The detailed cost estimate is provided in Appendix E. The incremental cost difference between dry lime FGD and wet limestone FGD is $5,452 per additional ton of SO_2 removed and is $6,132 per additional ton of SO_2 removed when the higher fabric filter costs are factored in. With a wet FGD design, the fabric filter would be prior to the FGD system, and the resultant capital and operating costs are higher than a similar fabric filter that follows a dry lime FGD system. A comparison of the costs and SO_2 removed is summarized in Table 6-2. The annualized cost estimate for a wet lime system would be similar to the one prepared for wet limestone with the primary difference being the higher cost of lime reagent. Because wet limestone FGD has a similar removal efficiency to wet lime FGD and the operating costs are lower, it was decided that wet limestone FGD was the appropriate cost comparison alternative to the lime spray dryer.

MidAmerican believes that the high incremental cost of wet limestone/lime scrubbing is not warranted for this project based on the use of low sulfur coal and the limited additional tons of SO_2 removed. Wet FGD also has the disadvantages of waste disposal of a wet FGD sludge, possible future complications with mercury removal (see section 6.3.3.4.2 below), higher particulate and sulfuric acid mist emissions, and higher energy usage. Dry lime scrubbing can meet an SO_2 emission limit that is comparable to the best in the RBLC database.

TABLE 6-2
CBEC Unit 4 SO_2 Control Cost Comparison

Factor	Dry Lime FGD	Wet Limestone FGD
Total Installed Capital Costs	$ 67,775,760	$ 137,958,260
Total Fixed & Variable O&M Costs	$ 11,331,111	$ 10,576,667
Total Annualized Cost	$ 22,983,556	$ 33,522,072
FGD Design Control Efficiency	90.4%	95.0%
Tons SO_2 Removed per Year	37,987	39,920
Cost Effectiveness per Ton of SO_2 Removed	$ 605	$ 840
Incremental Annualized Cost Difference between Wet FGD and Dry FGD	-	$ 10,538,517
Incremental Annualized Cost Difference for Fabric Filter	-	$ 1,313,912
Incremental Tons SO_2 Removed between Wet FGD and Dry FGD	-	1,933
Incremental Cost Effectiveness per Ton of Additional SO_2 Removed by Wet FGD	-	$ 6,132

6.2.3.5 Step 5 – Select BACT

The final step in the top-down BACT analysis process is to select BACT. EPA's RACT/BACT/LAER Clearinghouse (RBLC), a database of past technology decisions, was again consulted to assist in selecting BACT for this project.

Both wet lime scrubbing and wet limestone scrubbing have been demonstrated at removal efficiencies greater that 90%. The installation of a lime spray dryer FGD on CBEC Unit 4 will result in a SO_2 removal efficiency of 90.4% for the worst case coal, which has a sulfur content of 0.50%. The highest collection efficiency shown in the RBLC is 95% on Santee Cooper Cross Unit No. 1. This unit burns high sulfur coal. The design SO_2 emission rate on CBEC Unit 4 is 0.12 lb/MMBtu which is consistent with the low end of the range of emissions for units in the RBLC. The recent addition at the Kansas City Power and Light Hawthorn Station was permitted at 0.12 lb/MMBtu based on the use of low sulfur coal and a lime spray dryer FGD. Therefore lime spray dryer FGD is selected as BACT for this project with an SO_2 emission limit of 0.12 lb/MMBtu based on a 30-day rolling average. Lime spray dryer FGD is also selected as BACT for the control of Sulfuric Acid Mist, Total Reduced Sulfur and Reduced Sulfur Compounds.

6.2.4 NO_x Analysis

The BACT analysis for Nitrogen Oxides is presented below.

6.2.4.1 Step 1 – Identify All Control Technologies

NO_x will be emitted by combustion of coal in the boiler. NO_x formed in the combustion process consists of fuel NO_x (NO_x derived from nitrogen in the fuel) and thermal NO_x (which is produced from nitrogen in the flue gas) when the peak flame temperature reaches a sufficiently high temperature (approximately 2500°F).

The first step is to evaluate NO_x controls determined to be BACT by permitting agencies across the United States. This information is available from the EPA RACT/BACT/LAER Clearinghouse (RBLC) database assessable on the Internet. The printout from the database for NO_x is shown in Appendix D, Table E-9.

Potential NO_x control technology options are:

- Selective catalytic reduction (SCR);
- Selective noncatalytic reduction (SNCR);
- Low NO_x burners with overfire air;
- Low NO_x Burners;
- Flue Gas Recirculation (FGR); and
- Good combustion control.

6.2.4.2 Step 2 – Eliminate Technically Infeasible Options

All of these technologies except Flue Gas Recirculation are listed in the RBLC for coal-fired utility boilers. All of the technologies are technically feasible.

6.2.4.3 Step 3 – Rank Remaining Control Technologies by Control Effectiveness

Emission rates for each of the remaining technology combinations are required to rank them in order of effectiveness. These emission rates are provided in Table 6-3. The control efficiencies are those shown in the RBLC database (Appendix D, Table E-9). The emission rate range for Flue Gas Recirculation is highly variable based on boiler design but it was estimated to be similar to Low NO_x burners.

The PSD NSR regulations require that BACT, at a minimum, meet the applicable NSPS limit. Because there is an NSPS that applies to the boiler, the NSPS emission limit is also included in the ranking.

6.2.4.4 Step 4 – Evaluate Most Effective Controls and Document Results

SCR is being examined for this project, so its environmental, energy, and economic impacts must be examined. SCR is a control technique that reacts ammonia with the NO_x in the flue gas at the appropriate temperature in the presence of a catalyst to form water and nitrogen.

TABLE 6-3
NO_x Control Technology Emission Rate Ranking

Control Technology	NO_x Emission Rate [a]
SCR	0.08 – 0.15
SNCR	0.09 - 0.17
Low NO_x Burners with Overfire Air	0.15 – 0.33
Low NO_x Burners	0.32 – 0.39
Flue Gas Recirculation	0.32 – 0.39
Combustion Controls	0.23 – 0.55
NSPS Limit	0.16 [b]

[a] Pounds per million BTU as found in the RBLC database.
[b] Converted from NSPS limit of 1.6 pounds per megawatt hour assuming a heat rate of 10000 BTU per kwh.

Nomenclature:
SCR = Selective catalytic reduction
SNCR = Selective noncatalytic reduction
NO_x = Oxides of nitrogen
NSPS = New Source Performance Standards

SCR has two well-documented environmental impacts associated with it, ammonia emissions and disposal of spent catalyst. Some ammonia emissions from an SCR system are unavoidable because of imperfect distribution of the reacting gases and ammonia injection control limitations. Also, the NO_x removal efficiency depends on the ratio of ammonia to NO_x. Increasing the amount of ammonia injected increases the control efficiency but also increases the amount of unreacted ammonia that is emitted to the atmosphere (referred to as ammonia slip). Ammonia emissions from a well-controlled SCR system can likely be limited to 10 ppmv or less. Ammonia emissions are of concern, because ammonia is a significant contributor to regional secondary particulate formation and visibility degradation. In this case reduced NO_x emissions as an environmental benefit would be traded for increased ammonia emissions as an environmental cost.

The other environmental impact associated with SCR is disposal of the spent catalyst. Some of the catalyst used in SCR systems must be replaced every two to three years. These catalysts contain heavy metals including vanadium pentoxide. Vanadium pentoxide is an acute hazardous waste under the Resource Conservation and Recovery Act (RCRA), Part 261, Subpart D – Lists of Hazardous Materials. This must be addressed when handling and disposing of the spent catalyst.

There are also significant cost impacts associated with SCR. A cost estimate for SCR installation and operation has been prepared for this project and is provided in Appendix E. The estimated capital cost of a SCR for CBEC Unit 4 is $65,476,300. The estimated annual fixed and variable O&M costs are $2,942,222. The total annualized cost is $12,839,934 and the cost effectiveness per ton of NO_x removed is $3,183. This cost does not include the additional cost of low NO_x burners and the associated NO_x removal in the boiler.

The next control technology in the hierarchy is SNCR. The range of control efficiencies for SNCR ranges above the NSPS so it was not evaluated further. The other technologies listed in Table 6-2 were also not determined to achieve a level of control sufficient to meet NSPS and were not considered further. As such, further evaluation of energy, environmental, and cost data is not required.

6.2.4.5 Step 5 – Select BACT

The final step in the top-down BACT analysis process is to select BACT. EPA's RACT/BACT/LAER Clearinghouse (RBLC), a database of past technology decisions, was again consulted to assist in selecting BACT for this project.

Of the projects found, only SCR is shown to meet NSPS. The installation of SCR on CBEC Unit 4 will result in a NO_x removal efficiency of 60% or greater with an emission rate of 0.08 lb/MMBtu. The recent addition at the Kansas City Power and Light Hawthorn Station was initially permitted at 0.12 lb/MMBtu based on the use of low-NO_x burners and SCR. Based on operation and performance test results, the final emission limit for Hawthorne may be as low as 0.08 lb/MMBtu. Therefore SCR is selected as BACT for this project with an emission limit of 0.08 lb/MMBtu based on a 30-day rolling average.

6.2.5 CO and VOC Analysis

The BACT analysis for Carbon Monoxide and Volatile Organic Compounds is presented below.

6.2.5.1 Step 1 – Identify All Control Technologies

Only two control technologies have been identified for control of CO and VOC:

- Catalytic Oxidation; and
- Combustion controls.

Catalytic oxidation is a post-combustion control device that would be applied to the combustion system exhaust, while combustion controls are part of the combustion system design.

6.2.5.2 Step 2 – Eliminate Technically Infeasible Options

Catalytic oxidation has been the control alternative used to obtain the most stringent control level for CO and VOCs emitting from primarily combustion turbines firing natural gas. This alternative, however, has never been applied to a coal-fired unit, and thus has not been demonstrated in practice in this application.

For sulfur containing fuels, such as coal, an oxidation catalyst will convert SO_2 to SO_3 and therefore this conversion would result in unacceptable levels of corrosion to the flue gas system. Generally, oxidation catalysts are designed for a maximum particulate loading of 50 mg/M^3. The proposed Council Bluffs Unit 4 boiler will have a particulate loading upstream of the fabric filter in excess of 5,393 mg/M^3. In addition, trace elements present in coal, in particular chlorine, are poisonous to oxidation catalysts. There are no oxidation catalysts developed that have or can be applied to coal or oil fired boilers due to the high levels of particulate matter and trace elements present in the flue gas.

Although the catalyst could be installed downstream of the fabric filter to reduce the particulate loading, the flue gas temperature at that point will be approximately 165°F, which is well below the minimum temperature required (600°F) for operation of oxidation catalyst. The flue gas would have to be reheated, resulting in significant unfavorable energy and economic impacts.

For these reasons, as well as the generally low level of CO and VOC in coal-fired units, no PC boilers have been equipped with oxidation catalysts. Use of an oxidation catalyst system in the proposed CBEC Unit 4 PC boiler is thus considered technically infeasible. Thus, this alternative cannot be considered to represent BACT for control of CO and VOCs.

6.2.5.3 Step 3 – Rank Remaining Control Technologies by Control Effectiveness

Based on the Step 2 analysis, combustion control is the only remaining technology for this application.

6.2.5.4 Step 4 – Evaluate Most Effective Controls and Document Results

There are no environmental or energy costs associated with combustion control.

6.2.5.5 Step 5 – Select BACT

The EPA NSR RBLC clearinghouse database for comparable sources related to CO and VOC's are shown in Tables E-1 and E-2 in Appendix D. The final step in the top-down BACT analysis process is to select BACT. The recent addition at the Kansas City Power and Light Hawthorn Station was permitted at 0.16 lb/MMBtu for CO and 0.0036 lb/MMBtu for VOCs based on the combustion control. Based on the above analysis, combustion control for CO and VOCs is chosen as BACT for this project with an emission limit of 0.16 lb/MMBtu for CO and 0.0036 lb/MMBtu for VOCs.

6.2.6 PM/PM_{10} Analysis

PM and PM_{10} emissions will be emitted from the boilers, cooling tower and the coal, ash, lime and urea handling systems. An analysis for the emissions from the boilers is presented, followed by an analysis for the cooling tower and the material handling systems.

Unit 4 Boiler

6.2.6.1 Step 1 – Boilers: Identify All Control Technologies

Two control technologies for the boilers have been identified for PM/PM_{10} control:

- Electrostatic precipitators (ESPs);
- Fabric filters

6.2.6.2 Step 2 – Boilers: Eliminate Technically Infeasible Options

Electrostatic Precipitators

Electrostatic precipitation (ESP) technology is applicable to a variety of coal combustion sources. ESPs remove particulate matter from the flue gas stream by charging fly ash particles with a very high dc voltage and attracting these particles to grounded collection plates. A layer of collected particulate forms on the collecting plates and is removed by rapping the plates. The collected ash particles drop into hoppers below the precipitator and are periodically removed by the fly ash handling system.

Fabric Filters

Fabric filtration has been widely applied to coal combustion sources since the early 1970s and consists of a number of filtering elements (bags) along with a bag cleaning system contained in a main shell structure incorporating dust hoppers. Fabric filters use fiber glass fabric bags as filters to collect particulate matter. The particulate-laden gas enters a fabric filter compartment and passes through the bags and through a layer of accumulated particulate matter collected on the fabric of the filter bags. The collected particulate matter forms a filter cake layer on the bag that enhances the bag's filtering efficiency. However, excessive caking will increase the pressure drop across the fabric filter. When this occurs, the fabric filter is placed into a cleaning cycle and the excess particulate matter is removed by the ash handling system.

Fabric filters are effective in meeting NSPS emission requirements on coal-fired boilers. Fabric filters have been used as a control technology of choice on projects where LAER review is required. Unlike precipitators, fabric filter design is not based on any physical properties of the fly ash.

6.2.6.3 Step 3 – Boilers: Rank Remaining Control Technologies by Control Effectiveness

The fabric filter is more effective at capturing fine particulate than an ESP because ESP's tend to selectively collect larger particles. Large particles have a high mass to surface area ratio, which allows a charged particle to be efficiently dragged through the flue gas stream for collection on a grounded plate. Ultra fine particles have a low terminal velocity and cannot carry a strong enough electrical charge to result in complete collection.

The fabric filter is also more effective at collecting fly ash generated from western low sulfur coals such as those combusted at the Council Bluffs Energy Center. ESP's operate by first electrostatically charging for collection and then discharging the fly ash particles for removal in the ash handling system. Western low sulfur coal fly ash has a very high electrical resistivity that makes it difficult for the ESP to charge and discharge the particles. One solution that has been attempted on western power plants is the use of a hotside precipitator that operates at approximately 800°F as opposed to approximately 250°F operating temperature used on most ESP's. However even with this change in operating temperature, the ESP is still less effective at collecting fly ash in western power plants than is the fabric filter. The use of a fabric filter is also the preferred particulate control device for following a dry lime scrubber.

6.2.6.4 Step 4 – Boilers: Evaluate Most Effective Controls and Document Results

No negative environmental impacts have been identified for use of a fabric filter to control particulate emissions from pulverized coal boilers. There is, however, a high energy demand for this system. Energy is required to overcome the complete system's (fabric filter and associated ductwork) 8-12 inches water gauge pressure drop, and miscellaneous loads such as electric hopper heating. As baghouse filters are thought to represent the most effective PM/PM_{10} control technique that can be applied to PC boilers, no economic evaluation is required. However, for information purposes, a cost analysis has been prepared and is included in Appendix E. The estimated capital cost of a pulse-jet fabric filter for CBEC Unit 4 is $41,479,200. The estimated annual fixed and variable O&M costs are $1,977,778. The total annualized cost is $8,371,139 and the cost effectiveness per ton of PM_{10} removed is $252.

6.2.6.5 Step 5 – Boilers: Select BACT

The recent addition at the Kansas City Power and Light Hawthorn Station was permitted with a PM_{10} filterable emission rate of 0.018 lb/MMBtu based on the use of a fabric filter. Based on the above analysis and the EPA NSR RBLC clearinghouse data base available for recent years (refer to Tables E-3 and E-4 in Appendix D), a fabric filter with a filterable PM emission rate of 0.020 lb/mmBtu based on a 3-hour rolling average and a filterable PM_{10} emission rate of 0.018 lb/mmBtu based on a 3-hour rolling average, is selected as BACT for this project.

Unit 4 Cooling Tower

6.2.6.6 Step 1 – Cooling Tower: Identify All Control Technologies

The only control method for reducing PM/PM_{10} emissions from cooling towers is the use of drift eliminators.

6.2.6.7 Step 2 – Cooling Tower: Eliminate Technically Infeasible Options

Drift eliminators are technically feasible for this project and will be used.

6.2.6.8 Step 3 – Cooling Tower: Rank Remaining Control Technologies by Control Effectiveness

Drift eliminators are the only control method.

6.2.6.9 Step 4 – Cooling Tower: Evaluate Most Effective Controls and Document Results

Drift eliminators are the only control method. The industry state of the art drift eliminators for mechanical cooling towers have a control efficiency of 0.0005% (gallons of drift per gallon of cooling water flow).

6.2.6.10 Step 5 – Cooling Tower: Select BACT

Drift eliminators are the only control method identified for control of PM/PM_{10} emissions from cooling towers. Based on the above analysis and the EPA NSR RBLC clearinghouse data base available since 1990 (refer to Table E-5 in Appendix D), drift eliminators with a control efficiency of 0.0005% is chosen as BACT for this project.

Unit 4 Coal, Ash, Lime and Urea Handling Systems

6.2.6.11 Step 1 – Coal, Ash, Lime and Urea Handling Systems: Identify All Control Technologies

PM and PM_{10} will be emitted from the handling of the coal for the power plant, the ash that results from the combustion process, lime that is used as a reagent for the lime spray dryer, and urea that is used to generate ammonia for the SCR. These emissions are fugitive dust that comes from the various transfer points in the handling systems for these materials.

The potential technologies that can be used to control the fugitive dust emissions are as follows for the various operations:

Coal Pile: Potential control technologies for the active coal storage pile include the use of an enclosed storage barn or the use of water sprays and dust suppression chemicals on an outside pile. Water sprays and dust suppression chemicals are potential control technologies for inactive (long-term storage) coal piles.

Coal Handling: Potential control technologies for coal transfer and handling operations include the use of enclosures vented to fabric filters. Telescopic chutes can be utilized for coal unloading onto storage piles.

Coal, Flyash/FGD Waste, Lime and Urea Storage: Storage silos and associated transfer operations can be vented to fabric filters for control.

Flyash/FGD Waste Haul Roads: Potential technologies for control of fugitive emissions on haul roads are the use of paved roads, the use of covered haul trucks, the use of water sprays, the use of dust suppression chemicals, or the use of street sweepers.

6.2.6.12 Step 2 – Coal, Ash, Lime and Urea Handling Systems: Eliminate Technically Infeasible Options

All of the potential control technologies listed in Step 1 are technically feasible.

6.2.6.13 Step 3 – Coal, Ash, Lime and Urea Handling Systems: Rank Remaining Control Technologies by Control Effectiveness

Generally the use of fabric filters where possible is the most effective control option. In locations where fabric filters can not be used, the use of water sprays and dust suppression chemicals are the most effective control methods.

6.2.6.14 Step 4 – Coal, Ash, Lime and Urea Handling Systems: Evaluate Most Effective Controls and Document Results

Fabric filters are the control method of choice where the dust source can be completely enclosed in a building. For dust sources that can not be completely enclosed, the use of water sprays and dust suppression chemicals are the control methods of choice.

The preliminary design for CBEC Unit 4 was to include an enclosed active coal storage barn. However, the capital cost estimate for the enclosure is $51,000,000. MidAmerican believes that this cost cannot be justified for the incremental improvement in fugitive emissions control versus the use of best operating practices and water sprays on an open pile. The air quality modeling was conducted based on open storage of the active pile.

Chemical binding (dust suppression chemicals) will be used on the inactive coal pile

New and modified coal handling operations (EP-159, Transfer Conveyor Bay; EP-160, Unit 4 East Coal Silos; EP-161, Unit 4 West Coal Silos; EP-6, Modified Rotary Car Dumper; and EP-13, Modified Transfer House 4) will have enclosures with fabric filters for dust control. The fabric filters have a maximum outlet grain loading of 0.010 gr/dscf.

The Flyash/FGD Waste vacuum system exhausters (EP-168, EP-169, EP-170) and the Lime Handling (EP-162) will use filter separators with a maximum outlet grain loading of 0.010 gr/dscf.

The Flyash/FGD Waste Silo (EP-167) and the Urea Silos (EP-164A, EP164-B) will have vent fabric filters with a maximum outlet grain loading of 0.020 gr/dscf.

MidAmerican will use a paved road, covered trucks and street sweepers for dust control on the Flyash/FGD Waste haul road.

6.2.6.15 Step 5 – Coal, Ash, Lime and Urea Handling Systems: Select BACT

Fabric filters are BACT for the transfer points, silos and crusher houses on the coal handling system. For the rail unloading stockout pile and the active coal storage pile, dust suppression is BACT. The inactive coal storage pile will be controlled by the application of a chemical binder. The coal will also be treated with a dust suppression chemical as it is transferred from the rail unloading facility to the storage pile. Fabric filters are also BACT for the transfer points and silos on the ash, lime and urea handling systems.

6.2.7 Lead Analysis

Lead emissions will be emitted from the boiler. Lead will accumulate as a component of the fly ash and control technologies that are effective in controlling particulate matter emissions will also control lead emissions.

6.2.7.1 Step 1 – Identify All Control Technologies

Two control technologies for the boilers have been identified for lead control:

- Electrostatic precipitators (ESPs);
- Fabric filters

6.2.7.2 Step 2 – Eliminate Technically Infeasible Options

Electrostatic Precipitators

Electrostatic precipitation technology is applicable to a variety of coal combustion sources. ESPs remove particulate matter from the flue gas stream by charging fly ash particles with a very high dc voltage and attracting these particles to oppositely charged collection plates. A layer of collected particles forms on the collecting plates (electrodes) and is removed by rapping the electrodes. The collected ash particles drop into hoppers below the precipitator and are periodically removed by the fly ash handling system.

Fabric Filters

Fabric filtration has been widely applied to coal combustion sources since the early 1970s and consists of a number of filtering elements (bags) along with a bag cleaning system contained in a main shell structure incorporating dust hoppers. Fabric filters use fiber glass fabric bags as filters to collect particulate matter. The particulate-laden gas enters a fabric filter compartment and passes through the bags and through a layer of accumulated particulate matter collected on the fabric of the filter bags. The collected particulate matter forms a filter cake layer on the bag that enhances the bag's filtering efficiency. However, excessive caking will increase the pressure drop across the fabric filter. When this occurs, the fabric filter is placed into a cleaning cycle and the excess particulate matter is removed by the ash handling system.

Fabric filters are effective in meeting NSPS emission requirements on coal-fired boilers. Fabric filters have been used as a control technology of choice on projects where LAER review is required. Unlike precipitators, fabric filter design is not based on any physical properties of the fly ash.

6.2.7.3 Step 3 – Rank Remaining Control Technologies by Control Effectiveness

The fabric filter is more effective at capturing fine particulate than an ESP because ESP's tend to selectively collect larger particles. Large particles have a high mass to surface area ratio, which allows a charged particle to be efficiently dragged through the flue gas stream for collection on a charged plate. Ultra fine particles have a low terminal velocity and cannot carry a strong enough electrical charge to result in complete collection.

The fabric filter is also more effective at collecting fly ash generated from western low sulfur coals such as those combusted at Council Bluffs Energy Center. ESP's operate by first electrostatically charging for collection and then discharging the fly ash particles for removal in the ash handling system. Western low sulfur coal fly ash has a very high electrical resistivity that makes it difficult for the ESP to charge and discharge the particles. One solution that has been attempted on western power plants is the use of a hotside precipitator that operates at approximately 800°F as opposed to approximately 250°F operating temperature used on most ESP's. However even with this change in operating temperature, the ESP is still less effective at collecting fly ash in western power plants than is the fabric filter.

6.2.7.4 Step 4 – Evaluate Most Effective Controls and Document Results

No negative environmental impacts have been identified for use of a fabric filter to control particulate emissions from pulverized coal boilers. There is, however, a high energy demand for this system. Energy is required to overcome the complete system's (fabric filter and associated ductwork) 8-12 inches water gauge pressure drop, and miscellaneous loads such as electric hopper heating. As baghouse filters are thought to represent the most effective PM/PM_{10} control technique that can be applied to PC boilers, no economic evaluation is warranted.

6.2.7.5 Step 5 – Select BACT

The EPA NSR RBLC clearinghouse database shows four comparable sources related to lead. They are shown in Table E-6 in Appendix D. Based on the above analysis and the clearinghouse data, a fabric filter preceded by a dry lime FGD system are selected as BACT for the control of lead emissions for this project.

6.2.8 Fluoride Analysis

Fluoride compounds will be emitted from the boilers from the combustion of coal. The fluoride compounds will be mainly in the gaseous form of hydrogen fluoride in the flue gas exiting the boiler.

6.2.8.1 Step 1 – Identify All Control Technologies

Two control technologies for fluoride control of flue gas from the boilers have been identified:

- Wet Limestone/Lime FGD
- Spray dryers followed by fabric filters

6.2.8.2 Step 2 – Eliminate Technically Infeasible Options

Wet Limestone/Lime FGD

Wet SO_2 scrubbers operate by flowing the flue gas upward through a large reactor vessel that has an alkaline reagent (i.e. lime or limestone slurry) flowing down from the top. The scrubber mixes the flue gas and alkaline reagent using a series of spray nozzles to distribute the reagent across the scrubber vessel. The calcium in the reagent reacts with the fluoride in the flue gas to form calcium fluoride that is removed from the scrubber with the sludge and is disposed.

The creation of sludge from the scrubber does create a solid waste handling and disposal problem. This sludge needs to be handled in a manner to not result in ground water contamination. Also, the sludge disposal area needs to be permanently set aside from future surface uses since the disposed sludge can not bear any weight from such uses as buildings or cultivated agriculture.

Spray Dryer Followed by Fabric Filter

Spray dryers operate by flowing the flue gas through a large vessel. In the top of the vessel is a rapidly rotating atomizer wheel through which lime slurry is flowing. The rapid speed of the atomizer wheel causes the lime slurry to separate into very fine droplets that intermix with the flue gas where the fluorides in the flue gas react with the calcium in the lime slurry to form particulate calcium fluoride. This dry material is captured in the fabric filter along with the fly ash and calcium sulfate from the sulfur removal process.

Fabric filtration has been widely applied to coal combustion sources since the early 1970s and consists of a number of filtering elements (bags) along with a bag cleaning system contained in a main shell structure incorporating dust hoppers. Fabric filters use fiberglass fabric bags as filters to collect particulate matter. The particulate-laden gas enters a fabric filter compartment and passes through the bags and through a layer of accumulated particulate matter collected on the fabric of the filter bags. The collected particulate matter forms a filter cake layer on the bag that enhances the bag's filtering efficiency. However, excessive caking will increase the pressure drop across the fabric filter. When this occurs, the fabric filter is placed into a cleaning cycle and the excess particulate matter is removed by the ash handling system.

6.2.8.3 Step 3 – Rank Remaining Control Technologies by Control Effectiveness

Either control technology will achieve 90% or greater control of fluorides.

6.2.8.4 Step 4 – Evaluate Most Effective Controls and Document Results

Either approach can achieve 90% or greater control of fluorides. No negative environmental impacts have been identified for use of a spray dryer absorber followed by a fabric filter to control fluoride emissions from pulverized coal boilers. The use of a wet scrubber has the negative environmental impact of wet sludge disposal.

6.2.8.5 Step 5 –Select BACT

The EPA NSR RBLC clearinghouse database shows six comparable sources related to fluoride. They are shown in Table E-7 in Appendix D. Five of the sources determined that the use of a dry lime scrubber followed by a fabric filter was BACT. The other source selected an electrostatic precipitator followed by a wet limestone FGD system as BACT for fluoride.

Based on the technology and clearinghouse database discussion above, a spray dryer FGD system followed by a fabric filter are selected as BACT for the control of fluoride emissions for this project.

6.3 Case-by-Case MACT Demonstration for Hazardous Air Pollutants

6.3.1 Background

MidAmerican Energy Company (MidAmerican) is proposing the addition of a nominal 750 Megawatt (MW) net pulverized coal-fired boiler at its existing facility located in Council Bluffs, Iowa. The new Council Bluffs Energy Center (CBEC) Unit 4 coal-fired boiler will burn Powder River Basin (PRB) subbituminous coal, and will be equipped with a lime spray dryer flue gas desulfurization system for acid gas control, fabric filters for fine particulate control and SCR for Nitrogen Oxides control. Combustion controls will be used to minimize products of incomplete combustion (PIC's) such as carbon monoxide (CO) and volatile organic compounds (VOC). This combination of control technologies will also provide substantial control of the other Hazardous Air Pollutants (HAPs) emitted from the proposed coal-fired boiler.

The EPA's regulations for case-by-case MACT, which were promulgated in 1996, are set out in 40 CFR Part 63, Subpart B. Those regulations require case-by-case determinations of MACT by the Title V permitting authority for each major source of HAP which is constructed or reconstructed after the effective date of the 112(g) program. For electric utility steam generating units, the case-by-case provisions contain an exemption from applicability "unless and until such time as these units are added to the source category list." On December 14, 2000, the EPA announced that it was adding coal- and oil-fired power plants to the section 112(c) list of sources (65 FR 79825; December 20, 2000). Therefore, each coal or oil-fired electric utility steam generating unit which is constructed or reconstructed is now subject to the case-by-case provisions of the Act until the EPA promulgates a nationally applicable MACT standard to address hazardous air pollutants for this source category. The EPA expects to promulgate a final standard in December 2004.

Pursuant to 40 CFR Part 63, Subpart B, case-by-case MACT determination must be made by the permit applicant for each new unit that has emissions above the major source threshold for HAPs. This document represents the case-by-case MACT determination for the CBEC Unit 4, as required for a new major source of HAPs.

6.3.2 Applicability of 112(g) Requirements

Table 6-4 presents a summary of projected potential emissions of hazardous air pollutants emitted from CBEC Unit 4. These emission estimates have been derived from HAP constituent analyses of PRB coal, EPA's AP-42 emission factor database and estimates of levels of control expected based on the configuration of the proposed boilers. We note that AP-42 factors represent the average of many field tests, and that HAP constituents of coal ash are highly variable. For these reasons, these values should not be construed to represent short-term compliance limits based on a one-time stack test.

TABLE 6-4
Annual Emission Estimate of Hazardous Air Pollutants

Hazardous Air Pollutant	Emissions (TPY)
Total PCDD/PCDF[1]	0.00051
PAH[2]	0.044
Other Organic Compounds[3]	19.301
HCl[4]	59.873
HF[4]	22.153
Antimony[6]	0.038
Arsenic[6]	0.861
Beryllium[6]	0.044
Cadmium[6]	0.107
Chromium[6]	0.546
Cobalt[6]	0.210
Lead[6]	0.882
Manganese[6]	1.030
Mercury[5]	0.169
Nickel[6]	0.542
Selenium[6]	2.731
Total	**108.537**

1. AP-42, Section 1.1, Table 1.1-12 (EPA September 1998).

2. AP-42, Section 1.1, Table 1.1-13 (EPA September 1998).

3. AP-42, Section 1.1, Table 1.1-14 (September 1998).

4. AP-42, Section 1.1, Table 1.1-15 (September 1998).

5. Estimated Mercury emissions provided by Sargent & Lundy. 20% control efficiency based on fabric filter/dry lime FGD combination.

6. AP-42, Section 1.1, Table 1.1-18 (September 1998).

It can be seen from Table 6-4 that based on these emission estimates, two HAPs (Hydrogen Chloride and Hydrogen Fluoride) will potentially exceed annual emissions of 10 tons per year (tpy) and total HAPs will exceed 25 tpy. For purposes of new source permitting, CBEC Unit 4 is being treated as major source for HAPs, and will employ case-by-case MACT for these pollutants.

6.3.3 Case-by-Case MACT Analysis

6.3.3.1 Case-by-Case MACT for Non-Mercury HAP Metals

The particulate matter emitted from CBEC Unit 4 will include entrained metals that are contained in coal. These metals will include arsenic, beryllium, cadmium, chromium, lead, manganese, nickel, and vanadium.

As noted in the BACT analysis for PM presented in Section 6.2 herein, the top control option is a fabric filter baghouse. The control options for non-mercury HAP metals are those identified in the BACT analysis for PM, and the control efficiencies for non-mercury HAP metals correspond to the control efficiencies for PM. Thus, it is concluded that a fabric filter baghouse represents case-by-case MACT for non-mercury HAP metals.

As was also noted in the BACT analysis, the proposed BACT emission limit of 0.020 lb PM per MMBtu heat input (0.018 lb/MMBtu for PM_{10}) is the most stringent limit identified for any coal-fired boiler of any type. Based on precedent established by U.S. EPA in establishing MACT standards for several categories of sources emitting non-mercury HAP metals, a PM emission limit is an effective surrogate for individual HAP metals emission limits and is an acceptable format for expressing the MACT standard. For example, U.S. EPA described its rationale for setting PM emission limits in the proposed iron & steel MACT standard:

"For the proposed rule, we decided that it is not practical to establish individual standards for each specific type of metallic HAP that could be present in the various processes (e.g., separate standards for manganese emissions, separate standards for lead emissions, and so forth for each of the metals listed as HAP and potentially could be present). When released, each of the metallic HAP compounds behaves as PM. As a result, strong correlation exists between air emissions of PM and emissions of the individual metallic HAP compounds. The control technologies used for the control of PM emissions achieve comparable levels of performance on metallic HAP emissions. Therefore, standards requiring good control of PM will also achieve good control of metallic HAP emissions. Therefore, we decided to establish standards for total PM as a surrogate pollutant for the individual types of metallic HAP. In addition, establishing separate standards for each individual type of metallic HAP would impose costly and significantly more complex compliance and monitoring requirements and achieve little, if any, HAP emissions reductions beyond what would be achieved using the surrogate pollutant approach based on total PM."

For the above reasons, and in light of the precedent established by U.S. EPA in setting MACT standards using a surrogate pollutant, it is determined that the BACT emission limit for PM will suffice as MACT standards for non-mercury HAP metals for CBEC Unit 4.

6.3.3.2 Case-by-Case MACT for Acid Gas HAPs

Fluoride emissions from coal-fired boilers result from trace concentrations of fluoride-containing compounds in the fuel. These emissions occur primarily in the form of hydrogen fluoride. In addition, hydrogen chloride emissions will occur as a result of chloride-containing compounds present in the fuel. Both hydrogen fluoride and hydrogen chloride are HAP's subject to the case-by-case MACT requirement.

The control options and relative control effectiveness hierarchy is the same for hydrogen chloride and hydrogen fluoride. The top control option for these acid gases is same as that for SO_2. A lime spray dryer is considered the top control technology for these acid gases. Thus, it is concluded that this control equipment configuration at 90% acid gas control represents case-by-case MACT for hydrogen fluoride and hydrogen chloride.

6.3.3.3 Case-by-Case MACT for Organic HAPs including Dioxin/Furans

The emissions of the organic compounds depend on the combustion efficiency of the boiler. Therefore, combustion modifications that change combustion residence time, temperature, or turbulence may increase or decrease concentrations of organic compounds in the flue gas. Organic emissions include volatile, semivolatile, and condensable organic compounds either present in the coal or formed as a product of incomplete combustion (PIC). Organic emissions are primarily characterized by the criteria pollutant class of unburned vapor-phase hydrocarbons. These emissions include alkanes, alkenes, aldehydes, alcohols, and substituted benzenes (e.g., benzene, toluene, xylene, and ethyl benzene). The remaining organic emissions are composed largely of compounds emitted from combustion sources in a condensed phase. These compounds can almost exclusively be classed into a group known as polycyclic organic matter (POM), and a subset of compounds called polynuclear aromatic hydrocarbons (PAH). Polycyclic organic matter is more prevalent in the emissions from coal combustion because of the more complex structure of coal.

While trace quantities of organic PIC HAPs will be emitted, these are well controlled by implementation of BACT for CO/VOC and PM_{10}, which also represents case-by-case MACT for these HAP species.

Emissions of polychlorinated dibenzo-p-dioxins and polychlorinated dibenzofurans (PCDD/PCDF) also result from the combustion of coal. Of primary interest environmentally are tetrachloro- through octachloro- dioxins and furans. Dioxin and furan emissions are influenced by the extent of destruction of organics during combustion and through reactions in the air pollution control equipment. The formation of PCDD/PCDF in air pollution control equipment is primarily dependent on flue gas temperature, with maximum potential for formation occurring at flue gas temperatures of 450 degrees to 650 degrees Fahrenheit.

The formation of dioxin in a combustion source is dependent on the presence of chlorine and complex unburned hydrocarbon chains which may recombine within a certain temperature window of the process as the gases cool. For example, PCB incinerators have been identified with high dioxin emission levels due to the extreme resistance to complete thermal destruction of this "engineered" complex hydrocarbon molecule and the presence of substantial chlorine. Coal combustion, on the other hand, is a process designed to completely burn organic hydrocarbons at high temperature and ample excess oxygen in the presence of only trace amounts of chlorine. Note that the PRB coal to be burned in CBEC Unit 4 contain very low levels of chlorine, which will limit formation of any chlorine compounds to a fraction of EPA's published generic AP 42 factors for coal combustion. Further, what chlorine is emitted will be effectively captured by the proposed dry lime scrubber acid gas control system, and any dioxin that does form will be captured within unburned carbon (LOI) and other adsorbents deposited on the filter cake of the baghouse.

Activated carbon injection (ACI) has been shown to be effective at controlling high dioxin emissions from incinerators. In this case, the dioxin emission level is simply too low to be effectively captured by the inherent adsorbents in the baghouse filters. The trace levels of chlorine in the CBEC Unit 4 coal and flue gas, combined with the unburned carbon (LOI) associated with combustion of subbituminous PRB coal, yields an effective carbon adsorption mechanism for the trace levels of dioxin which might be emitted from CBEC Unit 4. There is no evidence that any additional or measurable dioxin control could actually be achieved by the injection of additional carbon in the proposed unit.

The premise that ACI would result in measurable dioxin control beyond levels achieved by the best controlled similar source is entirely speculative. Good combustion controls and adsorption onto western coal ash and LOI in a fabric filter, therefore, represents case-by-case MACT for control of dioxin and organics from the proposed CBEC Unit 4.

6.3.3.4 Case-by-Case MACT for Mercury

EPA has specifically targeted Mercury (Hg) for new MACT standards to be developed by 2003, and has determined that mercury is the HAP of primary concern from coal-fired utility boilers. The control level approved as case-by-case MACT in this application may be revised in the future based on EPA's promulgation of a MACT rule. The starting point of this case-by-case MACT demonstration, therefore, is to establish the lowest mercury emission rate that has been achieved in operating pulverized coal-fired boilers on PRB subbituminous coal, and then adjusting that value to the coal-specific mercury content of the coal burned at CBEC Unit 4. This represents the minimum level of mercury control that would qualify as case-by-case MACT, "the emission limitation which is not less stringent than the emission limitation achieved in practice by the best controlled similar source".

The analysis also requires consideration of alternative levels of control which go beyond that of the best controlled similar source, i.e. "which reflects the maximum degree of reduction in emissions that the permitting authority, taking into account the cost of achieving such emission reduction, and any non-air quality health and environmental impacts and energy requirements, determines is achievable by the [proposed] source." These MACT emission levels are considered in the following sections.

6.3.3.4.1 Mercury Emissions

Mercury (Hg) is a naturally occurring constituent of soil and mineral deposits, including deposits of coal. When coal is burned, any trace quantities of mercury present is vaporized at the high temperatures within the furnace section of the boiler. In the presence of chlorine, a portion of the gaseous mercury may react to form mercuric chloride ($HgCl_2$), with most of the remaining mercury emitted as a gas in elemental form. The speciation of the emitted mercury depends on the coal composition (primarily the ash and chlorine content), the combustion system, and the time and temperature history of the flue gas.

The other primary variable affecting mercury emissions is the quantity of mercury contained in the particular coal being burned. Western coals exhibit generally lower mercury content than eastern coals. Testing conducted at CBEC on PRB subbituminous coal for the EPA Mercury ICR showed an uncontrolled coal mercury concentration of 1.0030×10^{-4} lb/ton.

6.3.3.4.2 Mercury Control Levels and Alternatives

The case-by-case MACT determination for CBEC Unit 4 contained in this application focuses on the application of the best level of mercury control being achieved in practice by similar utility scale pulverized coal-fired boilers burning PRB subbituminous coals, and then evaluating the practical potential for achieving even greater levels of control using available technology.

The application for MACT must demonstrate how the project will obtain a degree of emission reduction that is at least as stringent as the emissions reduction that would have been obtained had EPA promulgated MACT standards for mercury control for this source category. EPA has indicated that it does plan to promulgate a MACT standard for the source category of coal-fired steam electric generating units by 2003.

Very limited mercury emission rate data is available for pulverized coal-fired boilers in general. EPA has gathered test data from a number of various coal-fired utility boilers for mercury, particularly within the last few years. This "snapshot" sampling was conducted on coal-fired utility boilers ranging from smaller to larger, new to archaic, wall and tangential fired, with various coal types and properties, and various combinations of air pollutant control equipment. Even within apparently similar units, the data are highly variable, and this variability is not yet fully understood. Because of the many variables that make each tested unit somewhat unique, and unexplained variability within the data itself, it is difficult at this time to determine a precise emission factor and degree of control that would apply to the proposed units. For example, for boilers burning western coals, available data did not identify a clear advantage one way or the other for units that employed wet scrubbers and electrostatic precipitators versus units that employed spray dryers and fabric filters.

Although many pilot-scale tests have been performed and a few demonstration projects are scheduled for alternative approaches to mercury control, existing coal plants use either spray dryer/fabric filter, electrostatic precipitator, or electrostatic precipitator/wet FGD systems. Flue Gas Desulfurization (FGD) systems may control $HgCl_2$ to 85 to 95% but are not effective in treating elemental mercury. Conversely, elemental mercury can be adsorbed onto activated carbon and ash particles, particularly on units that employ fabric filters, a technique that has been employed for mercury control in certain incineration processes. Since mercury is emitted from the combustion of PRB subbituminous coals primarily in the form of elemental mercury (due to its lower chlorine content), adsorption with fabric filters should provide the maximum level of control for these particular units.

The USEPA has generated the ICR database for PRB coal firing with various control equipment combinations. The average mercury content in the PRB coal was approximately 9.1 lb/trillion Btu. On average, the ICR data showed the flue gas to have mercury speciated as approximately 10% particulate mercury, 15% to 20% ionic mercury, and 55% to 90% elemental mercury. Some units had as low as 1% particulate mercury, as low as 5% ionic mercury, and as high as 90% elemental mercury. Due to such a broad range in the speciation of the mercury, definitive predictions of the overall mercury removal efficiency will be very difficult. From the ICR database, almost 90% to 99% particulate mercury is collected in the baghouse, and approximately 10% of the elemental mercury is collected in the baghouse due to adsorption on ash. However, a close scrutiny of these data reveals that these units had a high level of mercury as particulate mercury (25%) and a low level as elemental mercury (35%). The combination of spray dryer FGD/baghouse at Craig Unit 3, Rawhide, and Sherburne County Station shows an average mercury removal of 25% with a range of 0% to 47%. Based on the chloride level in the CBEC Unit 4 fuel, it is estimated that approximately 20% to 25% of the mercury will be removed in the spray dryer FGD/baghouse system.

The possibility of oxidizing mercury in the SCR catalyst is very remote, but very limited experience and no significant data are available. Due to the high alkalinity in the PRB coal, it would be very difficult to oxidize elemental mercury to ionic mercury as most of the available chlorine would be reacted with alkali to form stable chloride compounds. Therefore, unless proven otherwise, it would not be prudent to take credit for elemental mercury oxidation due to the SCR catalyst while burning PRB coal.

A fabric filter combined with the use of the lime spray dryer flue gas desulfurization system has in the past been determined to represent the best technology for control of mercury from the combustion of subbituminous western coal from new utility scale PC boilers. Therefore, the lime spray dryer FGD/baghouse is the mercury control technology proposed for CBEC Unit 4.

6.3.3.4.3 Identification of Best Controlled Similar Source

Tucson Electric Power Company was issued a revision to the Title V permit for construction and operation of their Springerville Generating Station Unit 3 and 4 on April 29, 2002. Both of these units are pulverized coal fired units that will use a lime spray dryer and baghouse. The case by case emission limit for mercury for each of these units was established as 6.9 lbs/trillion Btu. The predicted mercury emissions from CBEC Unit 4 are 5.01 lb/trillion Btu.

Based on the coal and manufacturers data , we conclude that the mercury emission rate for CBEC Unit 4 burning PRB coal would be lower than this permitted Springerville Generating Station. However since the emission rate of mercury is depended on concentration of mercury in the coal and is highly variable, we suggest that efficient operation of the lime spray dryer and baghouse be used as surrogate for establishing compliance for mercury emissions. The efficient operation of the baghouse and lime spray dyer is established by demonstration of compliance with the BACT emission limits for PM and SO_2.

6.3.4 Data Required by 40 CFR 63.43

The content of an application for a case-by-case MACT determination is described in 40 CFR 63.43. The following sections correspond to the case-by-case MACT application content prescribed in 40 CFR 63.53 (e).

i. The name and address (physical location) of the major source to be constructed or reconstructed

Council Bluffs Energy Center Unit 4 is proposed to be located on the existing MidAmerican Plant site at 2115 Navajo Street, Council Bluffs, Iowa. The facility is a major source of hazardous air pollutants (i.e. greater than 10 tpy of HCl and HF and greater than 25 tpy of total HAPs), as shown in Table 6-4.

ii. A brief description of the major source to be constructed or reconstructed and identification of any listed source category or categories in which it is included.

The Council Bluffs Energy Center Unit 4 Project consists of one nominal 750 MW (net) pulverized coal-fired utility steam-electric generating unit. The applicable source category is "utility steam-electric generating units". The coal fired boiler is the source requiring new source MACT. The boiler is to be equipped with a lime spray dryer for acid gas control and fabric filter for PM and PM_{10} control.

iii. The Expected date of Commencement of Construction

Construction of the Council Bluffs Energy Center Unit 4 is expected to commence by June 2003 (site preparation).

iv. The Expected Date of Completion of Construction

Construction is expected to be completed in October 2006.

v. The Anticipated Date of startup of operation

Start up of the Unit 4 is anticipated in October 2006.

vi. The HAP emitted by the constructed major source, and the estimated emission rate for each such HAP

The hazardous air pollutants projected to be emitted annually from the coal-fired boiler are summarized in Table 6-4. These values are estimates based on EPA AP-42 emission factors and vendor data, properties of proposed coal to be fired and maximum rated heat input. Additional details on emissions is provided in Table 6-6 for Polynuclear Aromatic Hydrocarbons, Table 6-7 for other Organic Chemical, Table 6-8 for acid gases and Table 6-9 for trace metals.

vii. Any federally enforceable emission limitations applicable to the constructed or reconstructed major source

Federally enforceable emission limits will be established in the PSD permit as Best Available Control Technology requirements. In addition, 40 CFR 60 Subpart Da and 40 CFR 72-75 are also applicable federal requirements for this proposed Council Bluffs Energy Center Unit 4.

viii. The maximum and expected utilization of capacity of the constructed or reconstructed major source, and the associated uncontrolled emission rates for that source

The Unit 4 boiler, in theory, may operate for the full 8,760 hours of any given year. The annual HAP emission rates provided in Table 6-4, Table 6-6, Table 6-7 , Table 6-8 and Table 6-9 are based on a capacity factor of 100%. The uncontrolled emissions are calculated after excluding all add on controls. However, combustion controls that are inherent to the boiler have been taken into account in calculating uncontrolled emissions. No calculations have been provided for the uncontrolled PAHs and other organic compounds as the combustion controls are mainly utilized for controlling emissions of these chemicals.

ix. The controlled emissions for the constructed or reconstructed major source in tons per year at expected and maximum utilization capacity

The controlled emissions of HAPs are provided in Table 6-4, Table 6-6, Table 6-7, Table 6-8 and Table 6-9. These annual emissions are also calculated based on a 100% capacity factor but taking into account all proposed air pollution control devices. Hourly emissions are calculated at the rated capacity of the boiler.

x. A recommended emission limitation for the constructed or reconstructed major source consistent with the principles set forth in paragraph (d) of this section

Table 6-5 provides recommended emission limits, averaging time and test method for each HAP or category of HAP.

TABLE 6-5
Proposed Emission Limits

HAP Category	Surrogate Pollutant	Emission Limit	Averaging Time	Test Method
Organics	CO	0.16 lb/MMBtu	N/A	Reference Method 10
Acid Gases	SO_2	0.12 lb/MMBtu	30 day rolling	CEM for SO_2
Trace Metals	PM	0.020 lb/MMBtu	3 hour rolling	Reference method 5
Mercury	SO_2, PM	Same as above	Same as above	Same as above

xi. The selected control technology to meet the recommended MACT emission limitation, including technical information on the design, etc.

As stated previously, MACT for HAPs from CBEC Unit 4 burning PRB subbituminous coal is concluded to be control technology capable of demonstrating BACT for CO, VOC, PM_{10} and SO_2. Technical information on the design of the proposed control technology is provided in the PSD application in Sections 6.1 and 6.2.

xii. Supporting documentation including identification of alternative control technologies considered, and analysis of cost of non-air quality health environmental impacts or energy requirements for the selected control technology

The project is required to meet Best Available Control technology for the CO and VOC as well as PM_{10}. This combination of technology also represents the most stringent control that has been demonstrated in practice for HAPs control from similar PC utility boilers burning PRB subbituminous coal; less effective control technologies would not satisfy BACT requirements, and hence no alternatives analysis is required.

xiii. Any other relevant information required pursuant to subpart A

No other relevant information has been identified.

TABLE 6-6
Polynuclear Aromatic Hydrocarbons

Compounds[2]	Controlled[1] Emissions lb/hr	Controlled Emissions ton/yr
Biphenyl	8.15E-04	3.57E-03
Acenaphthene	2.45E-04	1.07E-03
Acenaphthylene	1.20E-04	5.26E-04
Anthracene	1.01E-04	4.42E-04
Benzo(a)anthracene	3.84E-05	1.68E-04
Benzo(a)pyrene	1.82E-05	7.97E-05
Benzo(b,j,k)fluoranthene	5.28E-05	2.31E-04
Benzo(g,h,l)perylene	1.30E-05	5.69E-05
Chrysene	4.80E-05	2.10E-04
Fluoranthene	3.41E-04	1.49E-03
Fluorene	4.37E-04	1.91E-03
Indeno(1,2,3-cd)pyrene	2.93E-05	1.28E-04
Naphthalene	6.24E-03	2.73E-02
Phenanthrene	1.30E-03	5.69E-03
Pyrene	1.58E-04	6.92E-04
5-Methyl chrysene	1.06E-05	4.64E-05

[1] AP-42 Section 1.1, Table 1.1-13 (9/1998)

[2] USEPA – TTN, Unified Air Toxics website, Section 112 Hazardous Air Pollutants, (8/21/2000)

TABLE 6-7
Other Organic Compounds including dioxin and furans

Compounds[2]	Controlled[1] Emissions lb/hr	Controlled Emissions ton/yr
Acetaldehyde	2.73E-01	1.20E+00
Acetophenone	7.20E-03	3.15E-02
Acrolein	1.39E-01	6.09E-01
Benzene	6.24E-01	2.73E+00
Benzyl chloride	3.36E-01	1.47E+00
Bis(2-ethylhexyl)phthalate (DEHP)	3.50E-02	1.53E-01
Bromoform	1.87E-02	8.19E-02
Carbon disulfide	6.24E-02	2.73E-01
2-Chloroacetophenone	3.36E-03	1.47E-02
Chlorobenzene	1.06E-02	4.64E-02
Chloroform	2.83E-02	1.24E-01
Cumene	2.54E-03	1.11E-02
Cyanide	1.20E+00	5.26E+00
2,4-Dinitrotoluene	1.34E-04	5.87E-04
Dimethyl sulfate	2.30E-02	1.01E-01
Ethyl benzene	4.51E-02	1.98E-01
Ethyl chloride	2.01E-02	8.80E-02
Ethylene dichloride	1.92E-02	8.41E-02
Ethylene dibromide	5.76E-04	2.52E-03
Formaldehyde	1.15E-01	5.04E-01
Hexane	3.21E-02	1.41E-01
Isophorone	2.78E-01	1.22E+00
Methyl bromide	7.68E-02	3.36E-01
Methyl chloride	2.54E-01	1.11E+00
Methyl ethyl ketone	1.87E-01	8.19E-01
Methyl hydrazine	8.15E-02	3.57E-01
Methyl methacrylate	9.59E-03	4.20E-02
Methyl tert butyl ether	1.68E-02	7.36E-02
Methylene chloride	1.39E-01	6.09E-01
Phenol	7.68E-03	3.36E-02
Propionaldehyde	1.82E-01	7.97E-01

TABLE 6-7
Other Organic Compounds including dioxin and furans

Compounds[2]	Controlled[1] Emissions lb/hr	Controlled Emissions ton/yr
Tetrachloroethylene	2.06E-02	9.02E-02
Toluene	1.15E-01	5.04E-01
1,1,1-Trichloroethane	9.59E-03	4.20E-02
Styrene	1.20E-02	5.26E-02
Xylenes	1.77E-02	7.75E-02
Vinyl acetate	3.65E-03	1.60E-02
Total PCDD/PCDF	1.17E-04	5.12E-04

[1] AP-42 Section 1.1, Table 1.1-14 (9/1998)

[2] USEPA – TTN, Unified Air Toxics website, Section 112 Hazardous Air Pollutants, (8/21/2000)

[3]Uncontrolled emissions were calculated based on a control efficiency of 90%.

TABLE 6-8
Acid Gas Emissions

Compounds[2]	Uncontrolled Emissions[3] lb/hr	Uncontrolled Emissions tons/yr	Controlled Emissions[1] lb/hr	Controlled Emissions tons/yr
HCl	136.70	598.73	13.67	59.87
HF	50.58	221.53	5.06	22.15

[1] AP-42 Section 1.1, Table 1.1-15 (9/1998)

[2] USEPA – TTN, Unified Air Toxics website, Section 112 Hazardous Air Pollutants, (8/21/2000)

[3]Uncontrolled emissions were calculated based on a control efficiency of 90%.

TABLE 6-9
Trace Metal HAPS Emissions from CBEC Unit 4

Compounds[2]	Uncontrolled[4] Emissions lb/hr	Uncontrolled[4] Emissions ton/yr	Controlled[1] Emissions lb/hr	Controlled[1] Emissions ton/yr
Antimony	2.88E+00	1.26E+01	8.63E-03	3.80E-02
Arsenic	6.56E+01	2.87E+02	1.97E-01	8.61E-01
Beryllium	3.36E+00	1.47E+01	1.01E-02	4.41E-02
Cadmium	8.15E+00	3.57E+01	2.45E-02	1.07E-01
Chromium	4.16E+01	1.82E+02	1.25E-01	5.46E-01
Cobalt	1.60E+01	7.00E+01	4.80E-02	2.10E-01
Lead	6.72E+01	2.94E+02	2.01E-01	8.82E-01
Manganese	7.84E+01	3.43E+02	2.35E-01	1.03E+00
Mercury[3]	4.81E-02	2.11E-01	3.85E-02	1.69E-01
Nickel	4.13E+01	1.81E+02	1.67E-01	5.42E-01
Selenium	2.08E+02	9.10E+02	6.24E-01	2.73E+00

[1] AP-42 Section 1.1, Table 1.1-18, (9/1998)

[2] USEPA - TTN, Unified Air Toxics website, Section 112 Hazardous Air Pollutants, (8/21/2000)

[3] Estimated Mercury emissions provided by Sargent & Lundy. Uncontrolled mercury emissions estimated to be 0.0481 lb/hr at maximum load, 20% control efficiency based on fabric filter/dry lime FGD combination, controlled mercury emissions of 0.0385 lb/hr at maximum load.

[4] Uncontrolled emissions of trace metals except mercury were calculated based on the control efficiency of the fabric filter (99.7%). Uncontrolled emissions for mercury were calculated using a control efficiency of 20%.

6.3.5 MACT Compliance

Since the combustion controls, spray dryer and fabric filter have been determined to be MACT for the combustion of PRB coal, for CBEC Unit 4, compliance will be by demonstrating proper operation of the these control technologies to meet suggested emission limits. A detailed Compliance Assurance Monitoring (CAM) Plan has been proposed for ensuring continuous compliance with PM_{10}, NO_x and SO_2 emission limits (see Section 8). Adherence to this CAM plan will similarly ensure that the control technology is performing at design efficiency for control of HAPs.

6.3.6 References

USEPA, 1998 *Study of Hazardous Air Pollutant Emissions from Electric Utility Steam Generating Units – Final Report to Congress.*

USEPA, 1998 AP-42, Fifth Edition, Section 1.1, "Bituminous and Subbituminous Coal Combustion" (9/1998).

SECTION 7.0

Air Quality Impact Analysis

This section presents a detailed description of the air quality impact analysis for the Council Bluffs Energy Center (CBEC) Unit 4 Project (CBEC4).

7.1 Project Overview

MidAmerican Energy Company (MidAmerican) is proposing to add a fourth unit to its CBEC facility located near Council Bluffs, Iowa. The proposed coal-fired Unit 4 is planned for a nominal net 750 megawatts (MW). Currently, the CBEC facility consists of three coal-fired units: Unit 1 (43 MW_{net}), Unit 2 (88 MW_{net}), and Unit 3 (690 MW_{net}). The Unit 4 Project will be supported by additional equipment that includes an auxiliary boiler, an emergency generator, a diesel engine/fire pump, a cooling tower, and equipment associated with the handling of coal and other material.

At the request of MidAmerican, CH2M HILL has conducted an air quality impact analysis as part of the Prevention of Significant Deterioration (PSD) permit application for the project. Representatives of MidAmerican and CH2M HILL met with DNR personnel on June 19, 2002 for a discussion of the air quality modeling and permitting requirements for the project. CH2M HILL presented a modeling protocol to the DNR on June 27, 2002, and DNR sent (via e-mail) a letter to CH2M HILL dated July 3, 2002 that provided approval of the protocol. The modeling analysis described in this section was performed in conformance with the approved protocol.

7.2 Project Description

MidAmerican proposes to expand the CBEC with a coal-fired Unit 4. Although currently operating with three units, the CBEC was designed for possible expansion, and some of the infrastructure is already in place to handle an additional generating unit.

The CBEC is located approximately 4 kilometers (km) southeast of Council Bluffs, Iowa on the eastern bank of the Missouri River at an approximate base elevation of 970 feet above mean sea level (msl). Figure 2-1 from Section 2 of this document presents a vicinity map for the CBEC. Terrain near the facility rises gradually from the river basin to an elevation of approximately 1,300 feet msl within approximately 6 km to the southeast of the facility boundary. Within 30 km of the facility, terrain does not exceed 1,350 feet. Figure 7-1 shows the terrain near the CBEC.

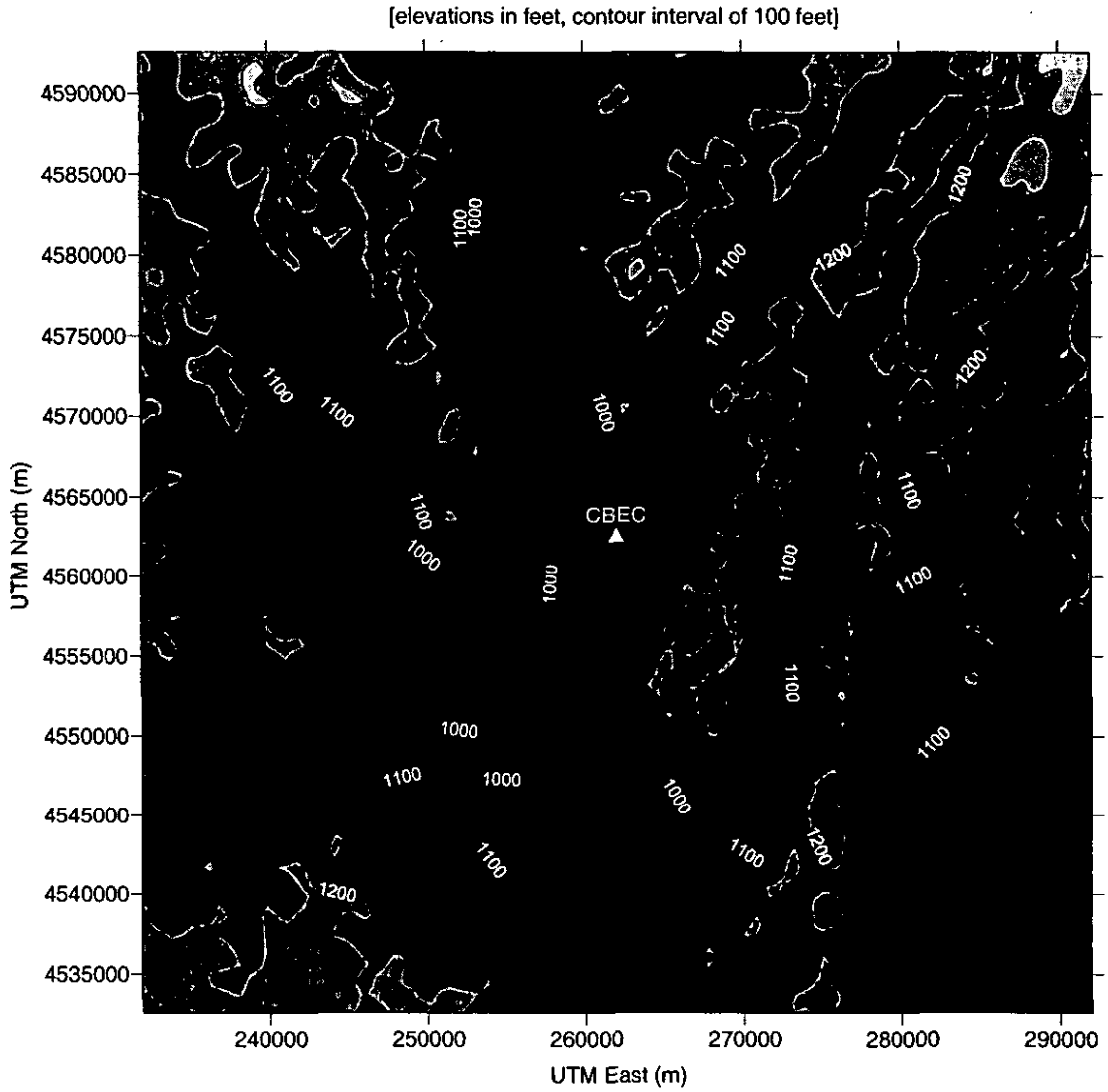


FIGURE 7-1
Terrain Features Near the CBEC

7.3 Source Designation

The proposed project will constitute a major modification to a major stationary source with respect to the PSD rules established under the Federal New Source Review program. The existing CBEC belongs to one of the 28 categorical sources listed under PSD regulations that are assigned a major source threshold of 100 tons per year of any regulated pollutant (fossil-fuel boilers, combinations thereof, totaling more than 250 million British thermal units per hour heat input). The goals of the air quality modeling analysis were to demonstrate compliance with state and federal air quality regulations that are applicable to the proposed project. CH2M HILL performed a dispersion modeling analysis for each criteria pollutant for which the annual emission rate was equal to or greater than the significant emission rates for PSD analysis (Table 7-1). Table 7-2 summarizes the modeling significance levels, PSD increments, and air quality standards that apply to criteria pollutant emissions from the project.

TABLE 7-1
Emissions Levels That Trigger Requirements for Dispersion Modeling

Pollutant	Prevention of Significant Deterioration Significant Emission Rates (tons/year)
CO	100
NO_X	40
SO_2	40
PM/PM_{10}	25/15
Lead	0.6

Notes:

CO = Carbon monoxide
NO_X = Nitrogen oxides
PM = Particulate matter
PM_{10} = Particulate matter less than 10 microns

TABLE 7-2
Air Quality Standards Applicable to the Project

Averaging Period/ Pollutant	Class II Modeling Significance Level ($\mu g/m^3$)	Class II PSD Increment ($\mu g/m^3$)	Class I PSD Increment ($\mu g/m^3$)	Significant Monitoring Concentrations ($\mu g/m^3$)	National Ambient Air Quality Standard ($\mu g/m^3$)
Annual NO_2	1 (NO_X)	25	2.5	14	100
3-hour SO_2	25	512[a]	25[a]	NS	1,300[a]
24-hour SO_2	5	91[a]	5[a]	13	365[a]
Annual SO_2	.1	20	2	NS	80
24-hour PM_{10}	5	30[a]	8[a]	10	150[a]
Annual PM_{10}	1	17	4	NS	50
Lead (Pb)	NS	NS	NS	0.1 (quarterly)	1.5 (quarterly)
1-hour CO	2,000	NS	NS	NS	40,000[a]
8-hour CO	500	NS	NS	575	10,000[a]

[a] Not to be exceeded more than once per year.

Notes:

$\mu g/m^3$ = micrograms per cubic meter
CO = Carbon monoxide
NO_2 = Nitrogen dioxide
NO_x = Nitrogen oxides
NS = No standard
PM_{10} = Particulate matter less than 10 microns
PSD = Prevention of Significant Deterioration
SO_2 = Sulfur dioxide

7.4 Area Classifications

The CBEC is located in Pottawattamie County, Iowa. The proposed project is situated in an area that is designated as attainment for all criteria pollutants, while the surrounding areas are designated as Class II areas for PSD permitting.

7.5 Model Selection

Air quality impacts from the CBEC Unit 4 Project were determined with the latest version of the EPA Industrial Source Complex Short-Term (ISCST3) model that incorporates enhanced building downwash algorithms. The enhanced downwash algorithms are referred to as Plume RIse Model Enhancements (PRIME), and the model, ISC-PRIME, is being evaluated by EPA as the next generation building downwash model. Although ISC-PRIME has been recommended by the EPA to be added to the list of EPA-preferred models, it is currently considered an "alternative" model. While the enhanced algorithms in ISC-PRIME will provide better performance for estimates of building downwash effects, the model is based on the EPA ISCST3 model, which is the latest generation of the EPA's ISC short-term model. The ISCST3 model is recommended for predicting impacts from industrial point sources, as well as area and volume sources. The model combines simple terrain and complex terrain algorithms, and therefore accounts for the effects of elevated terrain on all modeled plumes.

Because the determination of the acceptability of the use of ISC-PRIME as an alternative model is an EPA Regional Office responsibility, DNR obtained approval from EPA Region VII for CH2M HILL to use ISC-PRIME for this project.

7.6 Model Input Defaults/Options

The ISC-PRIME model was used with regulatory default options as recommended in the EPA Guideline on Air Quality Models (Appendix W of 40 CFR Part 51; EPA, 2000) as listed below:

- Use stack-tip downwash (except for Schulman-Scire downwash)
- Use buoyancy-induced dispersion (except for Schulman-Scire downwash)
- Do not use gradual plume rise (except for building downwash)
- Use the calms processing routines
- Use upper-bound concentration estimates for sources influenced by building downwash from super-squat buildings
- Use default wind profile exponents
- Use default vertical potential temperature gradients

The land surrounding CBEC in all directions is open country with no significant development. Therefore, rural dispersion coefficients were utilized within the ISC-PRIME model. Point sources were modeled with stack heights that did not exceed good engineering practice (GEP) stack height. Building downwash parameters for the point sources at the CBEC facility (including the cooling tower cells) were determined with the latest version of the EPA Building Profile Input Program (BPIP) designed for the ISC-PRIME model (BPIP, version 95086).

7.7 Modeling Receptors

7.7.1 Receptor Configuration

The base receptor grid for ISC-PRIME modeling consisted of receptors that were placed at the CBEC ambient air boundary, and Cartesian-grid receptors that were placed beyond the boundary at spacing that increased with distance from the origin. The base grid originated at the approximate proposed location of the Unit 4 boiler stack. Ambient boundary receptors were placed at 50-meter (m) intervals along a line that represents the physical barrier (fence) that restricts public access to the facility. Beyond the ambient boundary, receptor spacing was as follows:

- 100-m spacing from the boundary to 1 km beyond the ambient boundary in all directions
- 250-m spacing from beyond the 100-m receptors to 5 km from the origin
- 500-m spacing from beyond 5 km to 10 km from the origin
- 1,000-m spacing from beyond 10 km to 30 km from the origin

CH2M HILL supplemented the base receptor grid with receptors at closer (tighter) receptor spacing, where appropriate, to ensure that the maximum points of impact were identified.

7.7.2 Receptor Elevations

Terrain in the vicinity of CBEC was accounted for by assigning elevations to each modeling receptor. CH2M HILL used Digital Elevation Model (DEM) data from the U.S. Geological Survey (USGS) to determine receptor elevations. We obtained DEM data from the USGS National Elevation Dataset (NED). The NED has been developed by merging the highest-resolution, best-quality elevation data available across the United States, and is the result of the maturation of the USGS effort to provide 1:24,000-scale (7.5-minute) DEM data for the entire continental United States. Figure 7-1 shows the terrain features near the CBEC, as derived from the NED data.

7.8 Meteorological Input Data

Meteorological input to the ISC-PRIME model included five years (1987-1991) of data from Omaha, Nebraska. Sequential hourly surface data and concurrent upper-air data (mixing heights) have been combined into model-ready format for previous modeling of the CBEC. The surface data were collected at Eppley Airfield in Omaha, while the upper-air data were collected at the Omaha National Weather Service Station. Figure 7-2 presents a wind rose for the 1991 data.

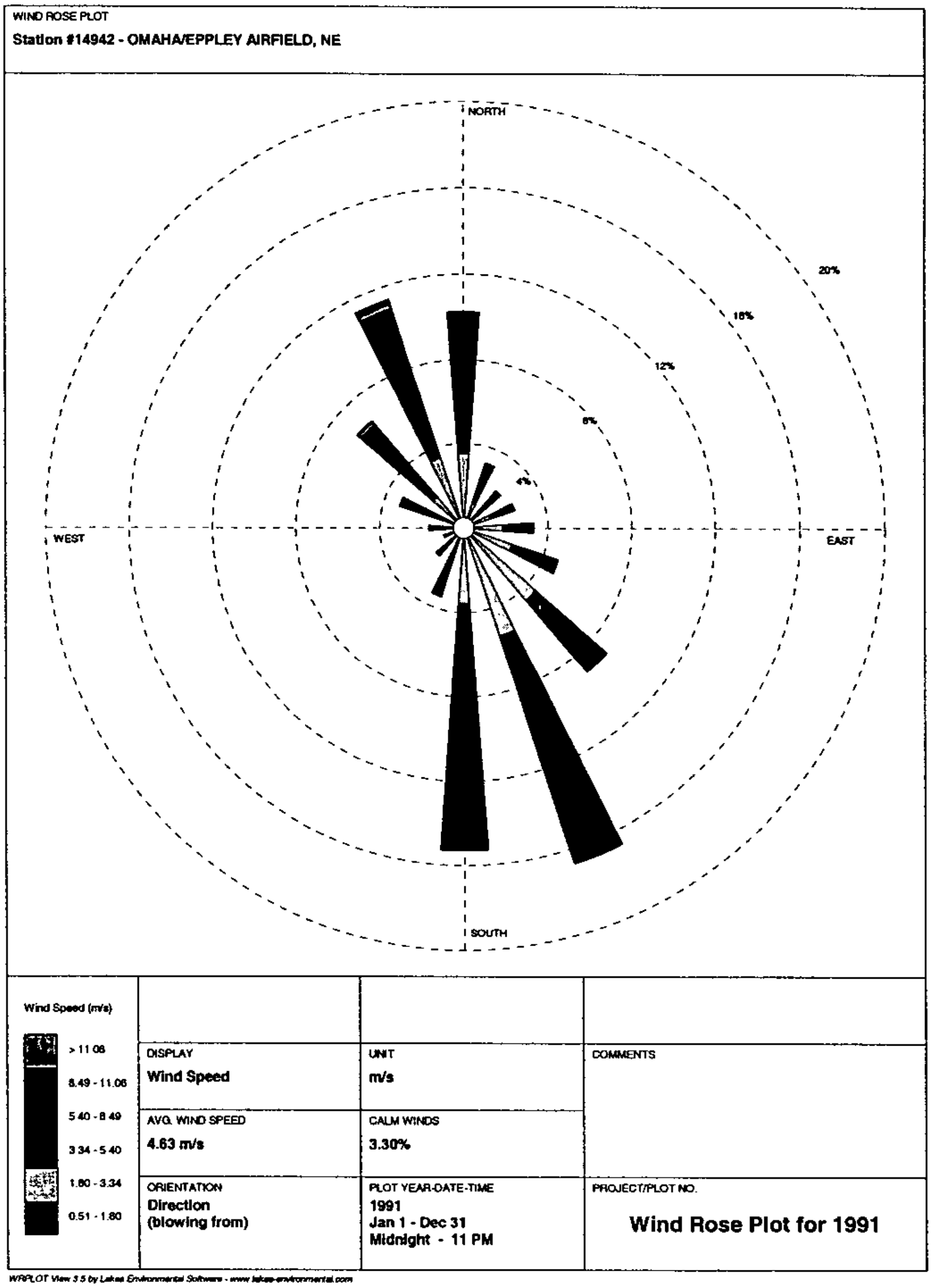


FIGURE 7-2
Omaha Wind Rose for 1991

7.9 Emission Source Characterization

CH2M HILL modeled the various emission sources at the CBEC as point, area, and volume sources, depending on the nature of the particular source. Sources that emit from a stack, including PM_{10} sources from the cooling towers cells and material handling dust collectors, were modeled as point sources.

Fugitive emissions from storage piles were modeled as area sources within ISC-PRIME. Area source length and width approximated the actual dimensions of the piles. The area sources were elevated at heights that represented 2/3 of the average maximum heights of the piles.

Fugitive emissions from traffic over haul roads were modeled as a series of volume sources. Volume source parameters for the haul roads were taken in part from the EPA document *Modeling Fugitive Dust Impacts from Surface Coal Mining Operations – Phase II Model Evaluation Protocol* (EPA, 1994). The source height of the haul road volume sources was 2 meters, as based on the statement from the EPA document that the maximum mass flux from haul road dust plumes occurs at that height. Initial vertical dispersion terms (3 m) for the haul road volumes were also be taken from the EPA document. The separation distance of the volume sources was set at 100 feet (two road widths), in accordance with recommendations in the *User's Guide For The Industrial Source Complex (ISC3) Dispersion Models, Volume I – User Instructions* (EPA, 1995). Initial horizontal dimensions for the volume sources were determined from the separation distance and Table 3-1 in the ISC3 User's Guide using the factor for a "line source represented by separated volume sources":

Center to center distance (30.48 m) divided by 2.15 = 14.2 m

Material transfer emission points that are not controlled by dust collectors or other control equipment were also modeled as volume sources. These volume sources were elevated at an appropriate height representative of the actual release height of the source, and with initial dimensions that approximate the actual lateral and vertical extent of the source.

The point, area, and volume sources were placed where actual operations for the CBEC occur. Form MI-1 (in map pocket of Appendix A) shows the general layout of the CBEC area, and the location of the various modeled sources.

Detailed emissions calculations for each modeled source are presented in Appendix F, and listings of other source input parameters (source heights, stack diameters, exhaust temperatures, etc.) are presented in Appendix C.

7.10 Preliminary Analysis Overview

For a preliminary analysis of the impacts from the CBEC Unit 4 Project, CH2M HILL compared the maximum model-predicted impacts from the sources associated with the project to the modeling significance levels for Class II areas. The ISC-PRIME model was run with the full five-year record (1987-1991) of meteorological input for each pollutant and averaging period. If the predicted impacts were greater than or equal to the modeling significance levels for any pollutant, CH2M HILL conducted a full impact analysis for compliance with the National Ambient Air Quality Standards (NAAQS) and PSD increments. The determination of preliminary impacts for the proposed project sources was made using the highest modeled impact for each pollutant and averaging period.

Previous modeling of the existing emission units at the CBEC by the Iowa Department of Natural Resources (DNR) has indicated predicted exceedances of the PM_{10} NAAQS with actual and potential emissions and predicted exceedances of the SO_2 NAAQS with potential emissions. A compliance plan that will be made federally enforceable to mitigate these predicted exceedances was submitted by MidAmerican to the DNR in July of 2002. Because of this history, a NAAQS modeling analysis for PM_{10} and SO_2 for all CBEC sources (including Unit 4 Project sources) is automatically part of this air quality analysis (regardless of the results of the preliminary analysis), and is described in detail in a later section of this document.

7.10.1 Screening Analysis for Unit 4

CH2M HILL began the Unit 4 Project preliminary analysis by performing a screening analysis of the Unit 4 boiler at various operating conditions. Operation at full load and at selected reduced loads (75 percent and 50 percent) were evaluated to determine which operating condition produces the worse-case predicted impacts for short-term averaging periods. This screening analysis was performed in accordance with guidance found in Section 9.1 of Appendix W of 40 CFR Part 51 (EPA, 2000). The load condition that yielded the highest impacts for a particular pollutant/averaging period was used to represent Unit 4 in subsequent modeling analyses. Table 7-3 presents the exhaust characteristics for the Unit 4 screening analysis. Table 7-4 presents the results of the analysis. The highest impact found for each pollutant and averaging period over the full five-year record of meteorological input data is reported in Table 7-4. Operation at full (100 percent) load yielded the highest impacts for all pollutants and all short-term averaging periods, and therefore full load was used to represent Unit 4 in all subsequent modeling analyses.

TABLE 7-3
Input Parameters for Unit 4 Load Screening

Parameter	100% Load	75% Load	50% Load
Exit Velocity (m/s)	28.3	20.2	15.0
Exhaust Temperature (K)	347	347	347
SO_2 Emissions (g/s)	116.0	82.9	57.5
PM_{10} Emissions (g/s)	24.6	17.6	12.2
CO Emissions (g/s)	148.6	106.1	73.6

Notes:
CO = Carbon monoxide
g/s = Grams per second
K = Kelvin
m/s = Meters per second
PM_{10} = Particulate matter less than 10 microns
SO_2 = Sulfur dioxide

TABLE 7-4
Results of Unit 4 Load Screening

Parameter	Maximum Predicted Impact for 100% Load ($\mu g/m^3$)	Maximum Predicted Impact for 75% Load ($\mu g/m^3$)	Maximum Predicted Impact for 50% Load ($\mu g/m^3$)
3-Hour SO_2	39.0	32.4	27.9
24-Hour SO_2	9.4	8.3	6.6
1-Hour CO	97.2	71.8	59.9
8-Hour CO	23.4	21.6	18.6
24-Hour PM_{10}	2.0	1.8	1.4

Notes:
CO = Carbon monoxide
PM_{10} = Particulate matter less than 10 microns
SO_2 = Sulfur dioxide
$\mu g/m^3$ = micrograms per cubic meter

7.10.2 Preliminary Analysis for Carbon Monoxide (CO)

Two sources of CO emissions were modeled for the Unit 4 Project preliminary analysis, the Unit 4 boiler and the Unit 4 auxiliary boiler. Because these two sources will not operate simultaneously, they were evaluated separately. The Unit 4 boiler was modeled with exhaust parameters and emissions reflective of the load condition (100%) that was found to produce the highest short-term impacts, as described in Section 7.10.1.

The highest 1-hour CO impact for the Unit 4 boiler was 97.2 $\mu g/m^3$. This predicted impact occurred 1.2 km southeast of the Unit 4 boiler stack at the ambient boundary for the CBEC. Impacts for the auxiliary boiler were much lower, with a maximum 1-hr impact of only 6.1 $\mu g/m^3$. These predicted impacts were both well below the Class II modeling significance level of 2,000 $\mu g/m^3$ for 1-hour CO.

For 8-hour CO, the highest impact for the Unit 4 boiler was 23.4 $\mu g/m^3$. This predicted impact occurred 1.1 km south-southeast of the Unit 4 boiler stack, less then 400 meters south of the CBEC ambient boundary, in an area of 100-m receptor spacing. As with the predicted 1-hour impacts, predicted impacts for the auxiliary boiler were much lower, with a maximum 8-hr impact of only 2.9 $\mu g/m^3$. These predicted impacts were both well below the Class II modeling significance level of 500 $\mu g/m^3$ for 8-hour CO.

Because the preliminary analysis demonstrated that the Unit 4 Project will not produce a significant impact of CO, no further analysis of the project's CO impacts was conducted. Table 7-5 present the results of the preliminary analysis for CO impacts.

TABLE 7-5
Results of Preliminary Analysis for CO

Averaging Period	Maximum Predicted Impact for Unit 4 Boiler ($\mu g/m^3$)	Maximum Predicted Impact for Unit 4 Auxiliary Boiler ($\mu g/m^3$)	Class II Modeling Significance Level ($\mu g/m^3$)
1-Hour CO	97.2	6.1	2000
8-Hour CO	23.4	2.9	500

Notes:
CO = Carbon monoxide
$\mu g/m^3$ = micrograms per cubic meter

7.10.3 Preliminary Analysis for Nitrogen Oxides (NO_X)

For the preliminary analysis of the impacts of NO_X emissions for the Unit 4 Project, the Unit 4 boiler and the Unit 4 auxiliary boiler were modeled together, with NO_X emission rates that reflect the potential annual operating conditions for each source. The Unit 4 boiler was modeled with exhaust parameters and emissions reflective of the load condition (100%) that would persist for an annual period of operation. For the Unit 4 auxiliary boiler, an annual average emission rate for NO_X was calculated from the potential annual hours of operation (2,500) for the source.

The highest predicted annual impact of NO_X with the base ISC-PRIME receptor grid was 0.39 $\mu g/m^3$. This predicted impact occurred approximately 18 km to the north of the Unit 4 boiler stack, and is well below the Class II modeling significance level of 1.0 $\mu g/m^3$ for annual NO_X. To further refine this estimated impact, a fine-spaced receptor grid with 100-meter spacing was built around the maximum course-grid receptor. With this fine-spaced grid, the maximum estimated annual impact was 0.46 $\mu g/m^3$. The preliminary analysis demonstrated that the Unit 4 Project will not produce a significant impact of annual NO_X.

7.10.4 Preliminary Analysis for Sulfur Dioxide (SO_2)

For a preliminary analysis of the SO_2 impacts for the Unit 4 Project, the Unit 4 boiler and the Unit 4 auxiliary boiler were modeled separately for short-term (3-hour and 24-hour) impacts. The Unit 4 boiler was modeled with exhaust parameters and emissions reflective of the load condition (100%) that was found to produce the highest short-term impacts, as described in Section 7.10.1. Short-term impacts for the auxiliary boiler were modeled with the maximum hourly SO_2 emission rate expected from that source. For annual impacts, the two sources were modeled together. The emission rate for the auxiliary boiler was an annual average emission rate that was calculated from the potential annual hours of operation (2,500) for that source.

The highest predicted 3-hour SO_2 impact for the Unit 4 boiler alone was 39.0 $\mu g/m^3$. This impact exceeded the Class II modeling significance level of 25.0 $\mu g/m^3$ for 3-hour SO_2. Predicted 24-hour impacts for the Unit 4 boiler also exceeded the Class II modeling significance level of 5.0 $\mu g/m^3$, with a maximum modeled impact of 9.4 $\mu g/m^3$. Short-term impacts from the Unit 4 auxiliary boiler by itself were well below Class II modeling significance levels. Annual impacts for the Unit 4 boiler and the Unit 4 auxiliary boiler together were below the modeling significance level of 1.0 $\mu g/m^3$, with a maximum modeled impact of 0.58 $\mu g/m^3$.

With predicted 3-hour and 24-hour impacts for the Unit 4 boiler exceeding the Class II modeling significance levels, we next determined the impact area for SO_2. The impact area for a particular pollutant, as described in the draft EPA *New Source Review Workshop Manual* (EPA 1990), is "a circular area extending from the source to the most distant point where approved dispersion modeling predicts a significant impact will occur". The impact area will define the area over which the analyses for NAAQS compliance and PSD increment consumption will be performed. For a given pollutant, the impact area is determined for each averaging period, and the area used for a given pollutant is the largest of the impact areas. For the Unit 4 Project, the largest impact area has a radius of 18.1 kilometers. Table 7-6 presents the results of the preliminary analysis for SO_2.

TABLE 7-6
Results of Preliminary Analysis for SO_2

Averaging Period	Maximum Predicted Impact for Unit 4 Boiler ($\mu g/m^3$)	Maximum Predicted Impact for Unit 4 Auxiliary Boiler ($\mu g/m^3$)	Class II Modeling Significance Level ($\mu g/m^3$)
3-Hour SO_2	39.0	5.7	25
24-Hour SO_2	9.4	3.4	5
Annual SO_2*	0.58	0.58	1

* Annual impacts were determined by modeling the proposed Unit 4 and the Unit 4 auxiliary boiler

Notes:

SO_2 = Sulfur dioxide
$\mu g/m^3$ = micrograms per cubic meter

7.10.5 Preliminary Analysis for Fine Particulate Matter (PM_{10})

The preliminary analysis for PM_{10} included the Unit 4 boiler, the Unit 4 cooling tower, and sources associated with material handling for the new unit. Dust collectors will serve as emissions controls and emission points for several new systems that will transfer and process coal for use with the new unit. Additionally, several coal-handling systems will be modified for the Unit 4 Project, including dust collectors associated with the following:

- Rotary Car Dumper
- Transfer House 4

Other types of material that will be handled for Unit 4 operation include fly ash, lime, urea, and FGD waste. Emissions from the systems that handle these materials will be controlled by vent bag filters or filter separators. These sources were modeled as point sources within the ISC-PRIME model, as were dust collectors and the Unit 4 cooling tower cells.

Fugitive emission sources associated with the Unit 4 Project include the transfer of coal to coal storage piles, wind erosion/maintenance of the storage piles, and emissions arising from traffic over paved haul roads. All of the fugitive sources were modeled as volume sources within ISC-PRIME, with the exception of wind erosion/maintenance of storage piles, which were modeled as area sources. Model inputs for the haul road volume sources and the storage pile area sources were described earlier in Section 7-9.

Model results indicated that the modeling significance levels would be exceeded for 24-hour and annual PM_{10}. The radius of significant impact for 24-hour PM_{10} was 7.4 km, and for annual PM_{10}, 3.8 km. The larger of the two impact areas was chosen as the area within which to conduct the full-impact analysis. Table 7-7 presents the results of the preliminary analysis for PM_{10}.

TABLE 7-7
Results of Preliminary Analysis for PM_{10}

Averaging Period	Maximum Predicted Impact (μg/m³)	Class II Modeling Significance Level (μg/m³)
24-Hour PM_{10}	26.9	5
Annual PM_{10}	4.5	1

Notes:

PM_{10} = Particulate matter less than 10 microns
μg/m³ = micrograms per cubic meter

7.10.6 Preliminary Analysis for Lead

Estimated lead emissions from the proposed CBEC Unit 4 Project exceed the PSD significant emission rate of 0.6 tons per year. Because no modeling significance level has been established for lead impacts, CH2M HILL conservatively modeled total lead impacts by including emissions from Units 1 through 4 and the auxiliary boilers at the CBEC. The modeled lead impacts were compared to the NAAQS for lead of 1.5 μg/m³. Because the NAAQS for lead is set for an averaging period of a calendar quarter, the ISC-PRIME model was run for quarterly periods representing January through March, April through June, July through September, and October through December for each of the five years of meteorological input data.

The highest modeled lead impact for a calendar quarter of 0.0015 μg/m³ was estimated for the fourth quarter of 1989. This estimated impact occurred at the south CBEC fenceline. Because the estimated maximum impact is three orders of magnitude lower than the NAAQS for lead, and because background levels of lead in the vicinity of the CBEC are assumed to be negligible, the modeling analysis demonstrates that the NAAQS for lead will not be threatened by the proposed Unit 4 Project or the existing facility together with the Unit 4 Project.

7.11 Full Impact Analysis

As described above, the Class II modeling significance levels were exceeded for 3-hour and 24-hour SO_2 and 24-hour and annual PM_{10}. Full-impact analyses were conducted for these pollutants and averaging periods to demonstrate compliance with the NAAQS and PSD increments. For the full-impact analyses, CH2M HILL modeled sources at CBEC and outside sources as provided the DNR, the City of Omaha, and the Nebraska Department of Environmental Quality (DEQ).

7.11.1 Background Concentrations and Air Quality Monitoring

Background concentrations represent all air pollution sources other than those that are explicitly modeled. Commonly, the impacts of distant background sources are accounted for by using appropriate, monitored air quality data (i.e., a background concentration). For full-impact analyses pertaining to NAAQS compliance, background concentrations were added to the model-predicted impacts for comparison to the NAAQS. As directed by DNR, CH2M HILL used the background concentrations that were used by DNR for recent modeling of the existing sources at CBEC:

Annual NO_2: 14 $\mu g/m^3$

3-hour, 24-hour, and annual SO_2: 20 $\mu g/m^3$

24-hour PM_{10}: 52 $\mu g/m^3$

Annual PM_{10}: 26 $\mu g/m^3$

Post-construction monitoring is required if estimated air quality impacts exceed the PSD significant monitoring concentrations listed in Table 7-2. This requirement is discussed in more detail later in this document.

7.11.2 PSD Increment Analysis for Fine Particulate Matter (PM_{10})

To determine compliance with the allowable PSD increments for PM_{10}, CH2M HILL modeled increment-consuming sources and compared the predicted highest 2nd-high 24-hour impacts to the allowable Class II 24-hour increment of 30 $\mu g/m^3$, and the highest annual impact to the allowable Class II annual increment of 17 $\mu g/m^3$. Sources associated with Units 1 and 2 at CBEC were not included because Units 1 and 2 are not increment consuming sources. Several material handling sources process material for each of the main units at CBEC, but rather than attempt to subtract emissions associated with Units 1 and 2 only, these sources were conservatively modeled as if all processed material was associated with the increment-consuming Units 3 and 4.

Actual emission rates were used for several sources, including the Unit 3 boiler stack and the dust collectors associated with Transfer Towers 1, 2, and 3, and the coal silos for Unit 3. The actual emissions for dust collectors were taken from stack test results. Source parameters used for the increment analysis are summarized in Appendix C. Short-term, maximum hourly emission rates were used to model 24-hour impacts for each source, and also to conservatively model annual impacts for each source. Outside sources from DNR, the City of Omaha, and the Nebraska DEQ were also included. Specific emission rates for use in increment modeling were provided by the DNR for the Bunge facility located approximately 3 km to the south east, but all other outside sources were conservatively modeled at PTE emission rates. Building profile parameters for the Bunge facility were also provided by the DNR, and these parameters were included in the full-impact model runs that included Bunge sources. Input parameters for the outside sources are listed in Appendix C.

For each of the five years of meteorological input, there were several receptors for which the highest 2nd-high 24-hour impacts exceeded the allowable increment level of 30 $\mu g/m^3$. Also for each of the five years of meteorological input, there was a single receptor that yielded an annual impact that exceeded the allowable annual increment level of 17 $\mu g/m^3$. Each of these high receptors were clustered near sources outside of the CBEC facility. Specifically, the high receptors were located near 1) sources associated with the Bunge facility 3 km to the southeast of CBEC, 2) sources associated with the IBP 7 km northwest of CBEC and Griffin Pipe facilities 8 km to the northwest of CBEC, and 3) sources associated with the Peoples Natural Gas facility 2 km to the northeast of CBEC. Figure 7-3 shows the relative locations of CBEC, these other nearby sources and the high receptors.

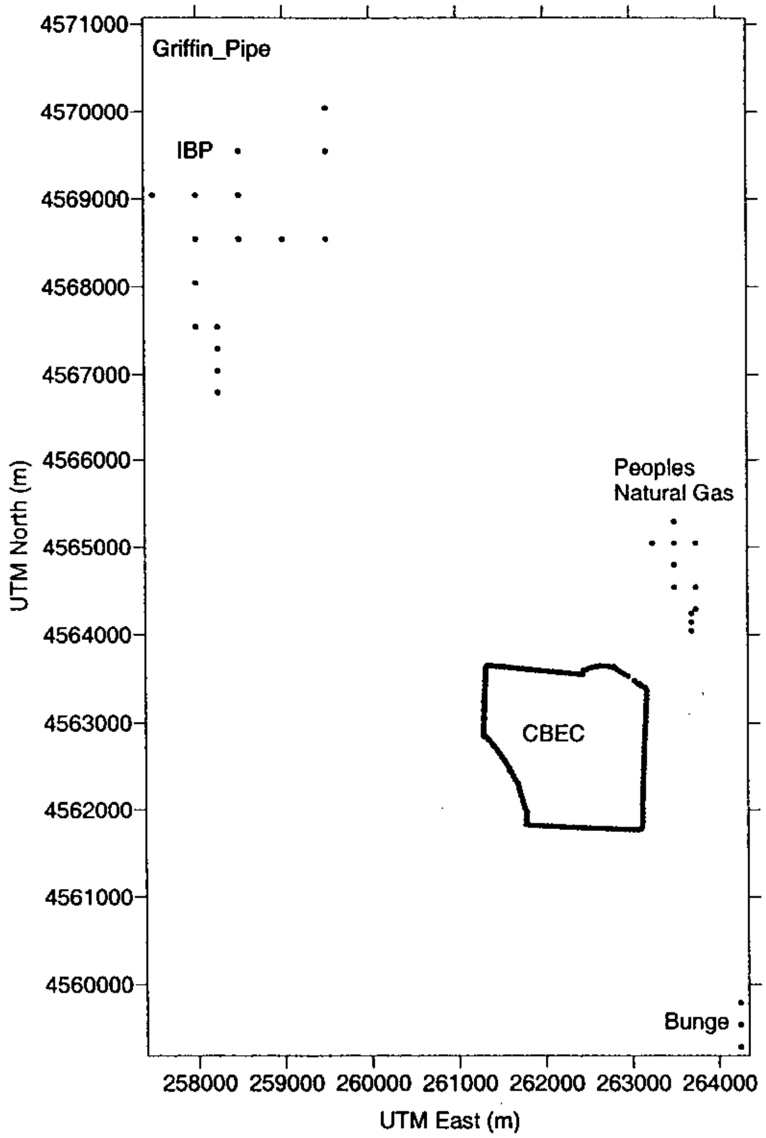


FIGURE 7-3
Nearby Sources and High Receptors for PM_{10} Increment Modeling

TABLE 7-8
CBEC4 Contribution to Modeled Exceedances of PSD Increment for PM_{10}

Averaging Period	Maximum Predicted Impact ($\mu g/m^3$)	Class II Modeling Significance Level ($\mu g/m^3$)
24-Hour PM_{10}	3.3	5
Annual PM_{10}	0.36	1

Notes:

PM_{10} = Particulate matter less than 10 microns
$\mu g/m^3$ = micrograms per cubic meter

The next step in the analysis was to determine if CBEC4 sources contributed significantly to these modeled violations of the PSD increment. CH2M HILL created a receptor grid that consisted only of the receptors that yielded violations of the PSD increments and used that receptor grid to re-model the CBEC4 preliminary analysis for PM_{10}. Results of this analysis showed that the contribution from CBEC4 sources was below the Class II modeling significance levels for each year of meteorological input, as shown in Table 7-8. Therefore, the CBEC4 Project does not significantly contribute to any modeled exceedances of the PSD increment for PM_{10}.

7.11.3 NAAQS Analysis for Fine Particulate Matter (PM_{10})

The full-impact NAAQS analysis for PM_{10} made use of the Pre-1997 Method for determining compliance. The Pre-1997 Method consists of calculating the highest 6th-high 24-hour average concentration for a five-year period and calculating the highest five-year average for the "annual" value ("highest" means the receptor with the highest value, e.g. highest 6th-high or highest 5-year average). The 24-hour and annual impacts determined in this way were compared to the 24-hour NAAQS for PM_{10} (150 $\mu g/m^3$) and the annual NAAQS for PM_{10} (50 $\mu g/m^3$).

With the exception of auxiliary equipment (fire pumps and emergency generators) that were modeled in a separate analysis, all PM_{10} sources at CBEC and those associated with the CBEC4 Project were included in the NAAQS analysis, with emission rates at potential-to-emit (PTE). Outside sources from DNR, the City of Omaha, and the Nebraska DEQ were also included. Source parameters for the outside sources are listed in Appendix C.

The highest 6th-high 24-hour average concentration for the five-year period was 98.1 $\mu g/m^3$. With the addition of the 24-hour PM_{10} background provided by DNR (52 $\mu g/m^3$), this modeled impact would exceed the 24-hour NAAQS. However, this modeled impact occurs at a receptor that is located in the center of the sources that represent the Bunge facility. This high receptor was one that was evaluated for significant impact from CBEC4 sources (as described in the previous section), and was found to yield a contribution from CBEC4 sources below the modeling significance levels. The highest annual impact over the five-year period was also predicted to occur at the same receptor within the Bunge facility. The magnitude of the highest annual impact was 29.1 $\mu g/m^3$. With the addition of the annual

PM_{10} background provided by DNR (26 µg/m³), this modeled impact would also exceed the annual NAAQS. However, as with the highest 24-hour impact, CBEC4 sources do not contribute significantly to this total. If the highest Bunge receptor is removed from the analysis, all other receptors yield estimated impacts that, when added to the appropriate DNR background, are below the 24-hour and annual NAAQS. The next highest 6th-high 24-hour average (90.8 µg/m³) occurs near the IBP facility, and the next highest annual impact (15.2 µg/m³) occurs near the Bunge facility, both at receptors for which CBEC4 again does not contribute a significant impact.

7.11.4 PSD Increment Analysis and NAAQS Analysis for Sulfur Dioxide (SO_2)

To determine compliance with the allowable PSD increments for SO_2, CH2M HILL modeled increment-consuming sources and compared the highest predicted 2nd-high 3-hour and 24-hour impacts to the allowable Class II 3-hour increment of 512 µg/m³, and the 24-hour increment of 91 µg/m³.

To determine compliance with the allowable NAAQS for SO_2, CH2M HILL modeled all CBEC and all outside sources of SO_2 and added the appropriate background as provided by the DNR. The highest predicted 2nd-high 3-hour and 24-hour total impacts were compared to the 3-hour NAAQS of 1,300 µg/m³ and the 24-hour NAAQS of 365 µg/m³.

Sources associated with Units 1 and 2 at CBEC were not included in the increment modeling because Units 1 and 2 are not increment consuming sources. Actual emission rates were used for the Unit 3 boiler stack. Modeling results showed several receptors for which the highest 2nd-high 3-hour and 24-hour impacts exceeded the allowable increment levels, and the 3-hour and 24-hour NAAQS (with the addition of the DNR background of 20 µg/m³ for both averaging periods). These high receptors were clustered near the sources associated with the Griffin Pipe facility to the northwest of CBEC.

To determine if CBEC4 contributed a significant amount to the modeled exceedances, the increment and NAAQS analyses were repeated with a reduced receptor grid that included only those receptors that yielded a significant impact of 3-hour and 24-hour SO_2 from CBEC4 sources. Table 7-9 shows the results of the analysis with the reduced receptor grid. Predicted impacts for NAAQS compliance and PSD increment consumption were well below allowable levels, thus indicating that the CBEC4 Project sources do not contribute to any modeled violations for SO_2.

TABLE 7-9
Summary of Full-Impact SO_2 Modeling for Reduced Receptor Grid

Averaging Period/ Pollutant	Modeled Increment Impact (µg/m³)	Class II PSD Increment (µg/m³)	Modeled NAAQS Impact (µg/m³)	Background Concentration (µg/m³)	Total NAAQS Impact (µg/m³)	National Ambient Air Quality Standard (µg/m³)
3-hour SO_2	143.8	512	901.3	20	921.3	1300
24-hour SO_2	39.0	91	201.0	20	221.0	365

7.11.5 NAAQS Analysis for Auxiliary Equipment

Short-term impacts of PM_{10} and SO_2 from the Unit 4 Project sources that operate sporadically or only in emergencies (emergency generator and the diesel engine/fire pump) were modeled separately to ensure that impacts from these sources do not by themselves exceed the short-term NAAQS for PM_{10} and SO_2. Table 7-10 presents the results of the analysis. Maximum modeled impacts were added to DNR background to arrive at total impacts for these sources. All short-term impacts were well below the NAAQS.

TABLE 7-10
Summary of NAAQS Modeling for Auxiliary Equipment

Averaging Period/ Pollutant	Maximum Modeled Impact ($\mu g/m^3$)	Background Concentration ($\mu g/m^3$)	Total NAAQS Impact ($\mu g/m^3$)	National Ambient Air Quality Standard ($\mu g/m^3$)
24-hour PM_{10}	5.3	52	57.3	150
3-hour SO_2	18.0	20	38.0	1300
24-hour SO_2	4.6	20	24.6	365

7.12 Growth Analysis

7.12.1 Work Force

CH2M HILL consulted with Council Bluffs Energy Center (CBEC) personnel to obtain information on labor requirements and labor availability for the project, and made the following determinations. Most of the approximately 1000 construction jobs (peak) needed for the project will be filled by workers commuting to the site, many from the greater Omaha/Council Bluffs metropolitan area. Of the permanent positions needed for the project (up to 77), it is assumed that the majority will be filled by local workers with the remainder filled by people who will relocate to the area. Even if all 77 positions were filled through relocations, this represents less than 0.02 % of the population of the Omaha/ Council Bluffs area.

7.12.2 Housing/Industry

Due to the need for temporary and permanent positions for the project, there will be some emissions associated with the construction of housing in the Council Bluffs area. However, these emissions will be temporary and, because of the limited numbers of new homes expected, are considered to be insignificant.

The small number of people that would be brought into the Council Bluffs area to support the project is not expected to generate commercial growth. The expansion of CBEC is not expected to generate industrial growth because operational and maintenance systems are already in place for existing plant operations. Because there will be no associated commercial or industrial growth expected, there will be no growth-related air quality impacts.

7.13 Soils and Vegetation Analysis

CH2M HILL conducted a search for information regarding sensitive soils, sensitive vegetation, and vegetation with commercial or recreational value in the vicinity of CBEC. A literature search was conducted to determine the ambient air pollution levels that may cause damage to sensitive species or vegetation with commercial or recreational value. CH2M HILL then compared the maximum impacts predicted with the ISC-PRIME model to the levels of criteria pollutants that are known to produce damage to soil and vegetation, as described later.

Pottawattamie County has a significant amount of land under cultivation. In 2001, 545,500 acres were used for agricultural purposes. Pottawattamie County agriculture consists mostly of corn, soybeans, hay/alfalfa, corn silage, and oats. According to the USDA, National Agricultural Statistics Service, 215,100 acres were farmed for corn production, 230,700 acres were devoted to soybeans, and 35,000 acres were used for hay/alfalfa in 2001, which is the most recent year that harvesting data were available.

The Gifford State Forest is a 40 acre stand located in Pottawattamie County. Cottonwood is the primary tree species found in the area. American Elm, green ash, silver maple, boxelder, mulberry, European black alder, and honey locust also grow in the forest (DNR, 2002).

Of the species identified in the Council Bluffs vicinity, alfalfa, oats and soybeans have been identified as crops sensitive to pollutant effects. The exact tolerance of a given crop is dependent on the particular horticultural varieties. Table 7-11 indicates levels of NO_X which have been found to result in plant damage for different species. Photosynthesis is found to be inhibited in alfalfa at 2-hour NO_2 exposures of 4,105 $\mu g/m^3$ (Hill and Bennett, 1974). In addition, a mixture of approximately 191 ug/m3 NO_X and 265 ug/m3 of SO_x administered for 4 hours has been discovered to cause foliar injury to soybeans and oat.

CH2M HILL used the ISC-PRIME model to determine the maximum NO_X and SO_x impacts that would result from the project. The worst case 3-hour SO_x impact from the proposed unit is 39 ug/m^3 while the worst case 3-hour NO_x impact is 26 ug/m^3. As a result, the worst-case combined NO_x and SO_x 3-hour impact is 65 ug/m^3. All predicted concentrations are well below those that would be expected to impact vegetation.

TABLE 7-11
Pollutant Effects on Species in the Council Bluffs Area

Species	Category of Plant	4-hour NOx Concentrations which Result in 5% Foliar Injury	Unit 4 Worst Case 3-hour NOx Concentration
Alfalfa, Oats	Sensitive	3.76-11.28 mg/m^3	
Corn, Wheat	Intermediate	9.4-18.8 mg/m^3	0.026 mg/m^3
Elder, Ash	Tolerant	> 16.92 mg/m^3	

Based on "Air Quality Criteria for Oxides of Nitrogen", EPA/600/8-91/049bF, Vol. II, August, 1993.

The DeSoto and Boyer Chute National Wildlife Refuges (NWR) are located approximately 53 and 43 kilometers, respectively, north of the CBEC facility. Based on modeling results, the addition of Unit 4 is not expected to have a significant impact beyond 18 kilometers. Therefore, Unit 4 is not projected to have any impact at these two NWRs areas.

7.14 Visibility Impairment Analysis

CH2M HILL used the EPA VISCREEN model to estimate the Class II area visibility impacts near the CBEC from the proposed project and the impact at the nearest Class I area, the Mingo National Wildlife Refuge (Mingo NWR) in southeastern Missouri.

Additional air quality analyses were performed to assess the proposed facilities impact on highway I-29 from fog and icing and visual range impacts in recreational areas. The methods, input information, and results are discussed below.

Cooling Tower Impacts on I-29

Cooling towers are used to dissipate heat generated in the electrical power production. Mechanical-draft "wet" cooling towers are proposed to cool the water from the condenser. In a mechanical-draft cooling tower, fans force air into the cooling tower and through a fine spray of heated water where evaporation cools the water stream and transfers heat to the air. The warm moist air exhausts through the top of the cooling tower and comes in contact with cooler ambient atmosphere where the water vapor condenses into fine water drops creating a visible "steam" plume. As the plume mixes with more ambient air, the drops eventually re-evaporate and the visible plume dissipates.

Fogging is assumed to occur when the visible plume reaches the ground, posing a potential hazard to nearby traffic. Icing occurs when the visible plume reaches the ground under freezing conditions. Highway I-29 runs North/South along the plant's eastern property boundary. This analysis examines the potential for fogging or icing conditions to occur along I-29.

The Seasonal/Annual Cooling Tower Impact (SACTI) model was used to predict the potential for fogging and icing conditions. This models was developed by Argonne National Laboratories for the Electrical Power Research Institute (EPRI) in the mid 1980's in order to better evaluate impacts associated with water vapor plumes emitted from cooling towers. The model comes with several modules: a meteorological data preprocessor, a plume drift preprocessor, and several post-processors. Table 7-12 shows the general site parameters used in this SACTI modeling. MidAmerican provided the cooling tower design and operational characteristics.

The model requires monthly clearness index values and total average daily solar insolation values. For this analysis, values from the Omaha, NE airport as reported in Appendix B of the SACTI Users Guide were used.

The SACTI model was designed to evaluate a single group of cooling towers that have similar characteristics (e.g., type shape and exhaust characteristics). The MidAmerican cooling towers for the CBEC Unit 4 facility contains a single tower housing with 18 cells. Design parameters are summarized in Table 7-13.

TABLE 7-12
General Input Parameters for the SACTI Modeling Analysis

Input Parameter Name	Input Value	Units/Comments
Site Latitude	41.1567	Decimal degrees
Site Longitude	91.8371	Decimal degrees
Zone	6	Central time zone
Rural/Urban Switch	1	Rural mode
Surface Roughness	10	Centimeters
Mixing Height Type	2	Twice daily values
Year of Meteorological Data	1990	
Surface Meteorology Station and Mixing Height Station	Omaha WSFO #94918 Omaha, NE	Weather Service Field Office
No. of Representative Wind Directions	3	
Wind Directions	236, 281, 326	Degrees east of north
Reference Height	10	Meters
Evaluation Period	Annual	Full year evaluated
Maximum Downwind Distance	1600	Meters

TABLE 7-13
Cooling Tower Design Parameters Used in the SACTI Modeling Analysis

Input Parameter Name	Cooling Tower Input Value	Units/Description
Number of Tower Housings	1	
Tower Height	14.6	Meters
Tower Housing Length	131.7	Meters
Tower Housing Width	32.92	Meters
Number of Cells per Tower	18	Cells
Single Cell Diameter	10.4	Meters
Tower Effective Diameter	44.1	Meters
Total Heat Dissipation	977	Megawatts
Exhaust Air Flow Rate per cell	1,401,485	Actual cubic feet per min. at 103°F
Input Air Flow Rate	12,447	Kilograms per second

The SACTI model was run for a full year of meteorological data (1990) from the Weather Service Field Office in Omaha, Nebraska. The meteorological data consisted of hourly surface meteorological data observations and twice-daily mixing height data. Plume characteristics were calculated for all 16 wind direction sectors. The maximum plume dimensions for the critical (worst case) wind directions are summarized in Table 7-14. The critical wind directions are selected based on the geometry of the cooling tower. For a straight line of cells, representative wind directions would be parallel to the long axis, perpendicular to the long axis and at 45 degrees (mid-way) to the long axis and are generally directed toward I-29.

TABLE 7-14
Maximum Cooling Tower Plume Characteristics along the Critical Radials
MidAmerican CBEC Unit 4 Facility

Critical Wind Direction (direction from)	Maximum Plume Length (m)	Maximum Plume Height (m)	Maximum Plume Radius (m)
236 degrees east of north (perpendicular to long axis)	1035.5	128.7	30.50
281 degrees east of north (45 degrees to long axis)	1552.3+	365.7+	92.40+
326 degrees east of north (parallel to long axis)	1552.5+	370.2+	88.20+

+ indicates that the visible plume did not end within a centerline distance of 1600 meters

The highway I-29 is about 1,000 meters east of the cooling tower. Under most conditions the plume dissipates before reaching the highway. The plume length is 1,000 meters or greater only 19.97 percent of the time for all wind directions. The cooling tower plume travels over the I-29 highway only 3.33 percent of the time, but during these times the plume is elevated above the highway.

The SACTI model also calculates fogging and icing conditions. Fogging occurs only when the visible plume strikes the ground; icing occurs when the visible plume reaches the ground under freezing conditions. For the period evaluated, no fogging or icing conditions along the I-29 highway were predicted.

Visual Range Impacts in Class II Recreational Areas

The nearest Class I area is the Mingo National Wildlife Refuge (NWR) in southeastern Missouri. It is over 500 kilometers to the southeast of the plant site The plume impact from CBEC Unit 4 has been calculated for this Class I area and compared to acceptable visibility impacts for Class I areas. A plume from CBEC Unit 4 should not be visible in the Mingo Class I area in Missouri.

There are several Class II parks and recreational areas within 15 kilometers (9.3 miles) of the proposed facility. The plume from the CBEC4 stack may be visible in many of these areas. There are no standards that define allowable reductions in visual range for parks and recreational areas located in Class II areas, however, plume visibility parameters have been calculated for public information. Table 7-15 list the Class I and Class II parks and recreational areas included in the visual plume analysis, and Figures 7-4 and 7-5 show the locations of the Class II and Class I areas, respectively.

TABLE 7-15
Class I and Class II Recreational Areas Used in Visibility Analysis
MidAmerican CEBC Unit 4 Facility

Park or Recreational Area	Location Easting (m)	Location Northing (m)	Downwind Distance (km)	Background Visual Range* (km)
Class I Site Mingo National Wildlife Refuge, Missouri	751596	4102646	671.7	25.0
Class I Sites				
Lake Manawa State Park	261100	4564900	2.50	40.0
Wabash Trace Nature Trail at Mineola	273500	4558100	12.4	40.0
Council Bluff Municipal Airport	268800	4571000	10.9	40.0
Lewis and Clark Monument	260800	4576200	13.7	40.0
CBEC Unit 4 Stack	261980	4562557		

*Taken from EPA users guide for VISCREEN Model (EPA, 1992)

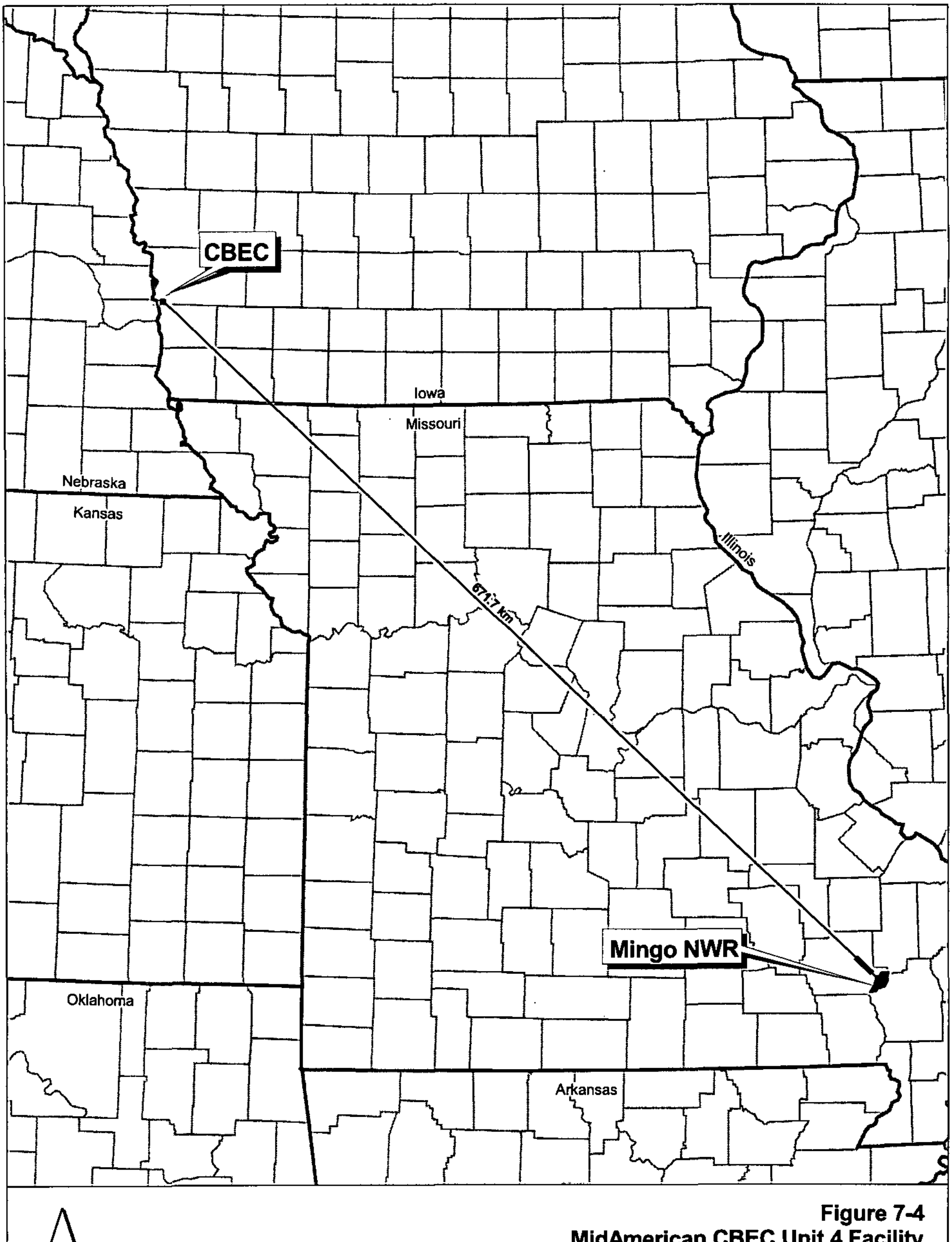


Figure 7-4
MidAmerican CBEC Unit 4 Facility
Distance to Class I Recreation Areas

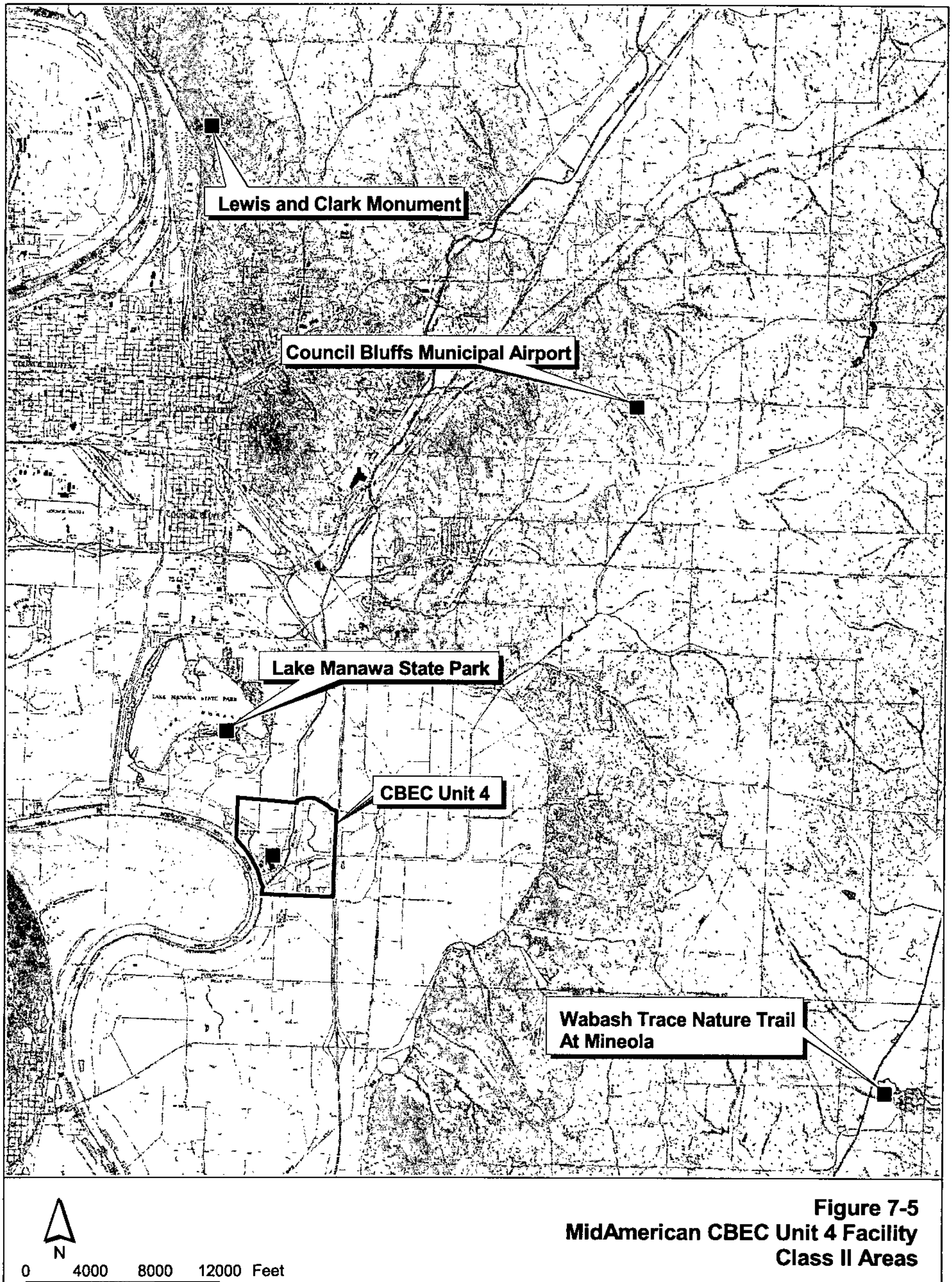


Figure 7-5
MidAmerican CBEC Unit 4 Facility
Class II Areas

The VISCREEN model calculates visibility impact by computing the color and intensity of the plume and compares it to its background sky or hillside. Contrasts at all wavelengths in the visible spectrum characterize the brightness and color of a viewed object relative to its viewing background. In the plume visual impact screening model VISCREEN, contrasts at three wavelengths (0.45, 0.55 and 0.65 μm) are used to characterize blue, green and red regions of the visible spectrum. If the plume contrast is positive, the plume is brighter than its viewing background; if negative, the plume is darker. If contrasts are difference at different wavelengths, the plume is discolored. If contrasts are all zero, the plume is indistinguishable from its background (i.e., imperceptible).

The perceptibility of a plume depends on the plume contrasts at all visible wavelengths. With a range of wavelengths, a measure of contrast must recognize both "overall" brightness and color. To address the added dimension of color as well as brightness, the color contrast parameter, ΔE, was chosen for use as the primary basis for determining the perceptibility of plume visual impacts in screening analyses.

Four lines of sight were selected by VISCREEN. The lines of sight are described by a view number. The plume is viewed in 5-degree increments of azimuth starting from the emission source. The other three views or lines of sight are for plume parcels 1 kilometer downwind from the source and the nearest and most distant park boundary. Results are provided for two assumed worst-case sun angles, forward scatter (looking toward the sun) and backward scatter (looking away from the sun).

The results of the Level-1 screening analysis using the VISCREEN model for the Class I Mingo National Wildlife Refuge in Missouri are presented in Table 7-16. This table shows that for all contrast parameters, the plume is imperceptible from the background and no adverse impact is predicted within the Class I area. Results are not presented for areas outside of the Class I area, since no integral vista has been identified for Mingo NWR.

TABLE 7-16
Visual Plume Impacts in Class I Mingo National Wildlife Refuge

					Delta E		Contrast	
Background	**Theta**	**Azimuth**	**Distance**	**Alpha**	**Criteria**	**Plume**	**Criteria**	**Plume**
Maximum Visual Impacts Inside Class I Area								
Sky	10.	84.	671.7	84.	2.00	0.00	0.05	0.00
Sky	140.	84.	671.7	84.	2.00	0.00	0.05	0.00
Terrain	10.	84.	671.7	84.	2.00	0.00	0.05	0.00
Terrain	140.	84.	671.7	84.	2.00	0.00	0.05	0.00

Tables 7-17 through 7-20 present plume contrast parameters for the Iowa parks, recreational areas and airports located in Class II air quality area. There are no established criteria for determining how visible a plume may be in a Class II air quality area. The values presented are the worst case impact Level-1 VISCREEN screening results within each Class II area. Actual plume contrast parameters would be much lower under most conditions.

TABLE 7-17
Visual Plume Impacts in Class II Lake Manawa State Park
MidAmerican CBEC Unit 4 Facility

					Delta E		Contrast	
Background	Theta	Azimuth	Distance	Alpha	Criteria	Plume	Criteria	Plume
Maximum Visual Impacts Inside Class II Area								
Sky	10.	84.	2.5	84.	--	13.433	--	0.230
Sky	140.	84.	2.5	84.	--	7.638	--	-0.214
Terrain	10.	84.	2.5	84.	--	75.411	--	0.538
Terrain	140.	84.	2.5	84.	--	17.846	--	0.329
Maximum Visual Impacts Outside Class II Area								
Sky	10.	7.	1.0	161.	--	23.051	--	0.422
Sky	140.	7.	1.0	161.	--	10.761	--	-0.371
Terrain	10.	20.	1.6	149.	--	85.165	--	0.783
Terrain	140.	20.	1.6	149.	--	25.310	--	0.697

Plume contrast criteria have not been established for Iowa Class II areas.

TABLE 7-18
Visual Plume Impacts in Class II Wabash Trace Nature Trail
MidAmerican CBEC Unit 4 Facility

					Delta E		Contrast	
Background	Theta	Azimuth	Distance	Alpha	Criteria	Plume	Criteria	Plume
Maximum Visual Impacts Inside Class II Area								
Sky	10.	84.	12.4	84.	--	9.532	--	0.072
Sky	140.	84.	12.4	84.	--	6.194	--	-0.128
Terrain	10.	84.	12.4	84.	--	22.206	--	0.220
Terrain	140.	84.	12.4	84.	--	4.542	--	0.130
Maximum Visual Impacts Outside Class II Area								
Sky	10.	135.	15.8	34.	--	14.628	--	0.067
Sky	140.	135.	15.8	34.	--	7.045	--	-0.177
Terrain	10.	35.	9.8	134.	--	26.206	--	0.320
Terrain	140.	35.	9.8	134.	--	7.122	--	0.278

Plume contrast criteria have not been established for Iowa Class II areas.

TABLE 7-19
Visual Plume Impacts in Class II Council Bluffs Municipal Airport
MidAmerican CBEC Unit 4 Facility

					Delta E		Contrast	
Background	**Theta**	**Azimuth**	**Distance**	**Alpha**	**Criteria**	**Plume**	**Criteria**	**Plume**
Maximum Visual Impacts Inside Class II Area								
Sky	10.	84.	10.9	84.	--	8.919	--	0.083
Sky	140.	84.	10.9	84.	--	6.168	--	-0.132
Terrain	10.	84.	10.9	84.	--	25.416	--	0.243
Terrain	140.	84.	10.9	84.	--	5.136	--	0.141
Maximum Visual Impacts Outside Class II Area								
Sky	10.	140.	14.6	29.	--	15.141	--	0.080
Sky	140.	140.	14.6	29.	--	7.089	--	-0.192
Terrain	10.	30.	8.3	139.	--	30.592	--	0.364
Terrain	140.	30.	8.3	139.	--	8.291	--	0.316

Plume contrast criteria have not been established for Iowa Class II areas.

TABLE 7-20
Visual Plume Impacts in Class II Lewis and Clark Monument
MidAmerican CBEC Unit 4 Facility

					Delta E		Contrast	
Background	**Theta**	**Azimuth**	**Distance**	**Alpha**	**Criteria**	**Plume**	**Criteria**	**Plume**
Maximum Visual Impacts Inside Class II Area								
Sky	10.	84.	13.7	84.	--	20.709	--	0.013
Sky	140.	84.	13.7	84.	--	10.120	--	-0.168
Terrain	10.	84.	13.7	84.	--	20.897	--	0.215
Terrain	140.	84.	13.7	84.	--	5.181	--	0.134
Maximum Visual Impacts Outside Class II Area								
Sky	10.	125.	16.2	44.	--	22.540	--	0.004
Sky	140.	125.	16.2	44.	--	10.161	--	-0.198
Terrain	10.	40.	11.3	129.	--	24.088	--	0.294
Terrain	140.	40.	11.3	129.	--	6.543	--	0.236

Plume contrast criteria have not been established for Iowa Class II areas.

7.15 Determination of Post-Construction Monitoring Requirements

Table 7-21 presents a comparison of the maximum estimated impacts for the CBEC4 Project and the significant monitoring concentrations. Post-construction monitoring of PM_{10} may be required.

TABLE 7-21
Maximum Impacts and Significant Monitoring Concentrations

Parameter	Estimated Impact ($\mu g/m^3$)	Significant Monitoring Concentration ($\mu g/m^3$)
Annual NO_2	0.45	14
24-hour SO_2	9.4	13
Lead	0.0015	0.1
8-hour CO	23.4	575
24-hour PM_{10}	26.9	10

Notes:
$\mu g/m^3$ = micrograms per cubic meter
CO = carbon monoxide
NO_2 = nitrogen dioxide
PM_{10} = fine particulate matter

7.16 References

DNR, 2002. *Soils and Vegetation Impacts Analysis under the PSD Program*. Presentation made to Iowa DNR by Jon Knodel of EPA Region 7 on May 13, 2002.

EPA, 2000. Appendix W of 40 CFR Part 51 - *Guideline On Air Quality Models (Revised)*, Office of Air Quality Planning and Standards, Research Triangle Park, North Carolina, April 2000.

EPA, 1995. User's Guide for the Industrial Source Complex (ISC3) Dispersion Model, Volume I – User Instructions (EPA-454/B-95-003a), Office of Air Quality Planning and Standards, Research Triangle Park, North Carolina, September, 1995.

EPA, 1994. *Modeling Fugitive Dust Impacts from Surface Coal Mining Operations – Phase II Model Evaluation Protocol*, Office of Air Quality Planning and Standards, Research Triangle Park, North Carolina, October 25, 1994.

EPA, 1992. *Workbook for Plume Visual Impact Screening and Analysis (Revised)*, (EPA-454/R-92-023. Office of Air Quality Planning and Standards, Research Triangle Park, North Carolina, October 1992.

White, K., Hill, A., and Bennett, J., 1974. *Synergistic Inhibition of Apparent Photosynthesis Rate of Alfalfa by Combinations of Sulfur Dioxide and Nitrogen Dioxide*, Environmental Science & Technology, Volume 8, Number 6, June 1974.

SECTION 8.0

Monitoring Information

This section describes the compliance monitoring devices and activities. The applicable test methods used for determining compliance are also described.

8.1 Compliance Monitoring Devices and Activities

Unit 4 will be equipped with 40 CFR Part 75 CEMS for the measurement of SO_2 and NO_X. Visible emissions (opacity) will be measured with a Continuous Opacity Monitoring System (COMS) installed at the outlet of the baghouse.

8.2 Applicable Test Methods

Listed below are the EPA test methods from 40 CFR 60 Appendix A that are applicable to this project, that will be used to demonstrate compliance with permit limits.

Method 1—Sample and Velocity Traverses for Stationary Sources
This method is designed to aid in the representative measurement of pollutant emissions and/or total volumetric flow rate from a stationary source. A measurement site where the effluent stream is flowing in a known direction is selected, and the cross-section of the stack is divided into a number of equal areas. Traverse points are then located within each of these equal areas.

Method 2—Determination of Stack Gas Velocity and Volumetric Flow Rate (Type S Pitot Tube)
This method is applicable for the determination of the average velocity and the volumetric flow rate of a gas stream.

Method 3A—Determination of Oxygen and Carbon Dioxide Concentrations in Emissions from Stationary Sources (Instrumental Analyzer Procedure)
This method is applicable to the determination of O_2 and CO_2 concentrations in emissions from stationary sources only when specified within the regulations.

Method 5 and/ or Method 17—Determination of Particulate Matter Emissions from Stationary Sources
Particulate matter is withdrawn isokinetically from the source and collected on a glass fiber filter maintained at a temperature of 120 ± 14°C (248 ± 25°F) or such other temperature as specified by an applicable subpart of the standards or approved by the Administrator for a particular application. The PM mass, which includes any material that condenses at or above the filtration temperature, is determined gravimetrically after the removal of uncombined water.

Method 6C—Determination of Sulfur Dioxide Emissions from Stationary Sources (Instrumental Analyzer Procedure)
This method is applicable to the determination of SO_2 concentrations in controlled and uncontrolled emissions from stationary sources. A gas sample is continuously extracted

from a stack, and a portion of the sample is conveyed to an instrumental analyzer for determination of SO_2 gas concentration using an UV, nondispersive infrared (NDIR), or fluorescence analyzer.

Method 7E—Determination of Nitrogen Oxide Emissions from Stationary Sources (instrumental Analyzer Procedure)
This method is applicable to the determination of NO_X concentrations in emissions from stationary sources. A gas sample is continuously extracted from a stack, and a portion of the sample is conveyed to an instrumental chemiluminescent analyzer for determination of NO_X concentration.

Method 9—Visual Determination of the Opacity of Emissions from Stationary Sources
This method is applicable for the determination of the opacity of emissions from stationary sources pursuant to § 60.11(b) and for qualifying observers for visually determining opacity of emissions. The opacity of emissions from stationary sources is determined visually by a qualified observer.

Method 10—Determination of Carbon Monoxide Emissions from Stationary Sources
This method is applicable for the determination of carbon monoxide emissions from stationary sources only when specified by the test procedures for determining compliance with new source performance standards. The test procedure will indicate whether a continuous or integrated sample is to be used. The integrated or continuous gas sample is extracted from a sampling point and analyzed for carbon monoxide (CO) content using a Luft-type nondispersive infrared analyzer (NDIR) or equivalent.

Method 19—Determination of Sulfur Dioxide Removal Efficiency and Particulate Matter, Sulfur Dioxide, and Nitrogen Oxides Emission Rates

1.0 Emission Rates. O_2 or CO_2 concentrations and appropriate F factors (ratios of combustion gas volumes to heat inputs) are used to calculate pollutant emission rates from pollutant concentrations.

2.0 Sulfur Reduction Efficiency and SO_2 Removal Efficiency. An overall SO_2 emission reduction efficiency is computed from the efficiency of fuel pretreatment systems, where applicable, and the efficiency of SO_2 control devices.

  2.1 The sulfur removal efficiency of a fuel pretreatment system is determined by fuel sampling and analysis of the sulfur and heat contents of the fuel before and after the pretreatment system.

  2.2 The SO_2 removal efficiency of a control device is determined by measuring the SO_2 rates before and after the control device.

  2.3 The inlet rates to SO_2 control systems (or, when SO_2 control systems are not used, SO_2 emission rates to the atmosphere) are determined by fuel sampling and analysis.

Methods 201 & 201A — Determination of Filterable PM_{10} Emissions
Methods 201 and 201A are used to determine filterable PM_{10} emissions from stationary sources. Method 201, known as the Exhaust Gas Recycle Procedure, extracts a gas sample isokinetically from the source. An in-stack cyclone is used to separate PM greater than PM_{10}, and an in-stack glass fiber filter is used to collect PM_{10}. To maintain isokinetic flow rate

conditions at the tip of the probe and a constant flow rate through the cyclone, a clean, dried portion of the sample gas at stack temperature is recycled into the nozzle. The particulate mass is determined gravimetrically after removal of uncombined water. An alternate procedure, Method 201A, known as the Constant Sampling Rate Procedure, extracts a gas sample at a constant flow rate through an in-stack sizing device, which separates PM greater than PM_{10}. The particulate mass is determined gravimetrically after removal of uncombined water.

Method 202 — Determination of Condensible Particulate Emissions From Stationary Sources

This method applies to the determination of condensible particulate matter (CPM) emissions from stationary sources. For this project, it will be applicable to the combustion sources only. The method may be used in conjunction with Method 201 or 201A if the probe is glass-lined. The CPM is collected in the impinger portion of a Method 17 type sampling train. The impinger contents are immediately purged after the run with nitrogen to remove dissolved sulfur dioxide gases from the impinger contents. The impinger solution is then extracted with methylene chloride. The organic and aqueous fractions are then taken to dryness and the residues weighed. The total of both fractions represents the condensible particulate matter.

SECTION 9.0

Compliance Plan and Certification

9.1 Evidence of Compliance with Standards

The present Title V permit requires submittal of annual compliance certification documents, demonstrating compliance with the standards. These compliance certificates have been submitted to IDNR and are in their file.

9.2 Compliance Status

CBEC is in compliance with applicable environmental laws and regulations. There are no enforcement actions or compliance plans in progress for CBEC.

9.3 Compliance Plan

Since CBEC is in compliance with applicable requirements, there are no Compliance Plans.

9.3.1 Compliance Schedule

CBEC is in compliance with applicable requirements; therefore, there is no compliance schedule provided.

9.3.2 Other Requirements

CBEC will meet other applicable requirements that become effective during the term of the permit as required by the IDNR.

9.4 Compliance Certification

A compliance certification signed by a responsible official of CBEC is provided at the end of this section.

9.5 Compliance Assurance Monitoring Plan

9.5.1 Applicability

The Compliance Assurance Monitoring (CAM) rule requirements established by 40 CFR Part 64 apply to pollutant specific emission units at a major source that are required to obtain a Title V permit and that use a control device to comply with an emission limitation.

Unit 4 will be subject to CAM requirements for PM_{10}, SO_2, and NO_X. CAM applicability for SO_2 and NO_X only applies to the Part 60 and IDNR permit emission limitations. Limitations imposed under the Acid Rain Program are exempt from the 40 CFR Part 64 CAM requirements. The CAM plans are provided below.

9.5.2 Compliance Assurance Monitoring Plan – PM_{10}

The Compliance Plan—Control of PM_{10} for CBEC Unit 4 consists of a fabric filter for PM_{10} control on the generating unit. The suggested CAM plan format from the EPA Technical Guidance Document will be used.

9.5.2.1 Background

A. Emission Unit

Facility:	Council Bluffs Energy Center, Council Bluffs, IA
Description:	Unit 4 Coal-Fired Utility Boiler
Identification:	Unit 4 Boiler

B. Applicable Regulations, Emission Limits, and Monitoring Requirements

Applicable Regulations:	40 CFR Part 60.42a
Regulated Pollutant:	PM_{10}
Emission Limits:	Unit 4: 0.018 lb/MMBTU (BACT, filterable fraction only)
Monitoring Requirements:	Visible Emissions (opacity), Periodic Monitoring for PM_{10}

C. Control Technology — Fabric Filter Dust Collector

9.5.2.2 Monitoring Approach

The key elements of the monitoring approach are presented below:

A.	**Indicator**	Visible emissions (opacity) will be used as an indicator. Pressure drop across the fabric filter will also be used as an indicator.
B.	**Measurement Approach**	Visible emissions (opacity) will be measured continuously with a Continuous Opacity Monitoring System (COMS) installed on the outlet of the unit's fabric filter. Pressure drop will be measured continuously with a pressure gauge.
C.	**Indicator Range**	Visible Emissions greater than 10 percent opacity based on a 24-hour rolling average. Pressure drop outside of the range to be established during the initial operating period.
D.	**Corrective Action Threshold**	If the 24-hour rolling average opacity exceeds 10 percent, or if the pressure drop stays outside of the established range for more than 1 hour, CBEC personnel will initiate an investigation of the

control equipment within 24 hours for possible corrective action. If corrective action is required, CBEC will proceed to implement such corrective action as soon as practicable in order to minimize possible exceedances of the PM_{10} standard established in the permit.

CBEC will also perform a performance test on the generating unit to determine compliance with the PM_{10} emission limit per EPA Reference Methods 201/201A and 202 once per permit term.

E. Performance Criteria

Data Representativeness: Visible emissions (opacity) are measured at the emission point (between the fabric filter outlet and the stack emission discharge). Pressure drop is measured between the inlet and outlet of the fabric filter compartment.

QA/QC Practices and Criteria: The COMS on the unit will comply with 40 CFR Part 60, Appendix B, Performance Specification 1, "Specification and Test Procedures for Opacity Continuous Emission Monitoring Systems in Stationary Sources."

The COMS will have a zero and span calibration drift check at least once daily in accordance with a written procedure.

The zero and span shall, as a minimum, be adjusted whenever the 24-hour zero drift or 24-hour span drift exceeds 4 percent opacity.

The system shall allow for the amount of excess zero and span drift measured at the 24-hour interval checks to be recorded and quantified.

If a system with automatic zero adjustments is used, the optical surfaces shall be cleaned when the cumulative automatic zero compensation exceeds 4 percent opacity.

A method will be used by CBEC for producing a simulated zero opacity condition and an upscale (span) opacity condition using a certified neutral density filter or other related technique to produce a known obscuration of the light beam to provide a system check of the analyzer internal optical surfaces and all electronic circuitry including the lamp and photo detector assembly.

Except during periods of system breakdowns, repairs, calibration checks, and zero and span adjustments, the COMS will be in continuous operation and will complete a minimum of one cycle of sampling and analyzing for each successive 10-second period and one cycle of data recording for each successive 6-minute period.

CBEC will reduce all data from the COMS to 6-minute averages. Six-minute opacity averages shall be calculated from 36 or more data points equally spaced over each 6-minute period.

Data recorded during periods of system breakdowns, repairs, calibration checks, and zero and span adjustments will not be included in the data averages computed under the previous paragraph. An arithmetic or integrated average of all data may be used.

The pressure drop monitor shall be maintained in accordance with the manufacturers recommendations.

Monitoring Frequency Data	Continuous opacity monitoring with data recorded as 6-minute averages. Continuous pressure drop monitoring with data recorded as 1-hour averages.
Collection Procedure:	Continuous.

9.5.2.3 Justification

A. Background

CBEC produces electricity. The pollutant specific emission unit is a coal fired utility boiler. PM_{10} is controlled by fabric filters prior to the discharge stack. The design collection efficiency of the fabric filter is 99.7 percent.

B. Rationale for Selection of Performance Indicator

The presence of visible emissions, recorded as opacity with the COMS, and pressure drop across the fabric filter were selected as the performance indicators because they are indicative of operation of the fabric filter in a manner necessary to comply with the PM_{10} emission standard. When the fabric filter is operating properly, the pressure drop will be within normal ranges and visible emissions from the exhaust will be minimal. Pressure drop outside of the established range, or visible emissions greater than 10 percent for a 24 hour rolling average, as recorded by the COMS, indicates reduced performance of the PM_{10} control device; therefore, abnormal pressure drop readings or the presence of visible emissions (opacity) are used as the performance indicators.

C. Rationale for Selection of Indicator Level

The selected indicator range is visible emissions greater than 10 percent opacity based on a 24 hour rolling average, or pressure drop as a 1 hour average outside of the established range. Although these measures do not in themselves constitute a violation of the PM_{10} standard, they do indicate that corrective action should be initiated so that any possible exceedance of the PM_{10} standard can be prevented.

9.5.3 Compliance Assurance Monitoring Plan – Sulfur Dioxide

The Compliance Plan—SO_2 emission controls for CBEC consist of a lime spray dryer flue gas desulfurization system for SO_2 control on the generating unit and the use of a 40 CFR Part 60 and 75 continuous emissions monitoring system (CEMS).

9.5.3.1 Background

A. Emission Unit

Facility:	Council Bluffs Energy Center, Council Bluffs, IA
Description:	Unit 4 Coal-Fired Utility Boiler
Identification:	Unit 4 Boiler

B. Applicable Regulations, Emission Limit, and Monitoring Requirements

Applicable Regulations:	40 CFR 60.43a
Regulated Pollutant:	Sulfur Dioxide
Emission Limits:	Unit 4: 0.12 lb/MMBTU 30-day rolling average (BACT)
Monitoring Requirements:	40 CFR Part 60 and 75 CEMS

C. Control Technology: Lime Spray Dryer Flue Gas Desulfurization System

9.5.3.2 Monitoring Approach

CBEC will use the 40 CFR Part 60 and 75 CEMS to continuously measure SO_2 emissions from the generating unit. The data reporting system for the CEMS will calculate SO_2 emission rates in terms of lb/MMBTU based on 30-day rolling averages and compare the computed emission rate to the applicable standard. The data reporting system will also calculate monthly and annual SO_2 emissions.

9.5.3.3 Justification

The use of a CEMS that provides results in units of the standard for the pollutant of interest and meets the criteria in 40 CFR Part 64.3(d)(2) is considered presumptively acceptable CAM.

9.5.4 Compliance Assurance Monitoring Plan – NO_X

The Compliance Plan—Control of NO_X emissions from Unit 4 consists of Low- NO_X Burners, Separate Overfire Air (SOFA), and Selective Catalytic Reduction, and the use of a 40 CFR Part 60 and 75 CEMS.

9.5.4.1 Background

A. Emission Unit

Facility:	Council Bluffs Energy Center, Council Bluffs, IA
Description:	Unit 4 Coal-Fired Utility Boiler
Identification:	Unit 4 Boiler

B. Applicable Regulations, Emission Limit, and Monitoring Requirements

Applicable Regulations:	40 CFR 60.44.a
Regulated Pollutant:	Nitrogen Oxides
Emission Limits:	Unit 4: 0.08 lb NO_X /MMBTU 30-day rolling average (BACT)
Monitoring Requirements:	40 CFR Part 60 and 75 CEMS

C. Control Technology: LNB, SOFA, and SCR

9.5.4.2 Monitoring Approach

CBEC will use the 40 CFR Part 60 and 75 CEMS to continuously measure NO_X on the generating unit. The data reporting system for Unit 4 CEMS will calculate NO_X emission rates in terms of lb/MMBTU based on 30-day rolling averages and compare to the applicable standard. The data reporting system for each CEMS will also calculate the monthly and annual NO_X emissions.

9.5.4.3 Justification

The use of a CEMS that provides results in units of the standard for the pollutant of interest and meets the criteria in 40 CFR Part 64.3(d)(2) is considered presumptively acceptable CAM.

9.6 Acid Rain Compliance Plan

CBEC is in compliance with Title IV Acid Rain Program requirements. An application for amendment for their acid rain permit will be submitted separately.

9.7 Periodic Monitoring Plan

The controlled coal handling sources associated with CBEC Unit 4 will be subject to Periodic Monitoring requirements for PM_{10}.

<u>Periodic Monitoring Requirements</u>

9.7.1 Stack Testing

Pollutant – Particulate Matter

1st Stack Test to be Completed within 6 months of start-up of operations

Test Method – Iowa Method 5

9.7.2 Operation & Maintenance Plan – Baghouses

The coal handling baghouses shall be installed, operated and maintained in accordance with the manufacturer's specifications. The baghouses shall be equipped with gauges which indicate the pressure drop across the baghouse compartments.

9.7.3 Monitoring Guidelines

9.7.3.1 General

Periodic Monitoring, which to be of value requires the source to be operating, is not required during periods of time greater than one day in which the source does not operate.

9.7.3.2 Daily

CBEC shall monitor and record the operating pressure drop across the coal handling baghouses at least once for every operation day. The operating pressure drop on the coal handling baghouses shall be maintained within the design conditions specified by the manufacturer's performance warranty.

9.7.3.3 Weekly

Opacity shall be observed on a weekly basis to ensure no visible emissions during the material handling operations. If visible emissions are observed this would be an excursion, not a violation, and action will be taken as soon as possible, but no later than eight (8) hours from the observation of visible emissions. If weather conditions prevent the observer from conducting an opacity observation, the observer shall note such conditions on the data observation sheet. At least three attempts shall be made to retake opacity readings at approximately 2 hour intervals throughout the day. If all observation attempts for a week have been unsuccessful due to weather, an observation shall be made the next operating day where weather permits.

- Check the cleaning sequence of the baghouse.
- Check hopper functions and performance.

9.7.3.4 Each Major Unit Overhaul

- Thoroughly inspect bags for leaks and wear. Bag removal is not required during this inspection.
- Inspect bag cleaning components.
- Inspect hopper unloading components.
- Inspect all components that are not subject to wear or plugging, including structural components, housing, ducts, and hoods.

9.7.4 Record Keeping and Reporting

A written or electronic record will be kept of the daily, weekly, and overhaul inspections and any actions resulting from the inspections.

Maintenance and inspection records will be kept for five (5) years and available upon request.

9.7.5 Corrective Action

The facility will take timely corrective action during periods of excursion where the indicators are out of range. A corrective action may include an investigation of the reason for the excursion, evaluation of the situation and necessary follow-up action to return operation within indicator range. An excursion is determined by the averaged discrete data point over a period of time, or the presence of a monitored abnormal condition. An excursion does not necessarily indicate a violation of an applicable requirement. If the corrective action measures fail to return the indicators to the appropriate range, the facility will report the excursion to the department and conduct source testing within 90 days of the excursion to demonstrate compliance with applicable requirements. If the test demonstrates compliance with emission limits then new indicator ranges must be set for monitoring and the new ranges must be incorporated in the operating permit. If the test demonstrates noncompliance with the emission limits, then the facility, within 60 days, proposes a schedule to implement corrective action to bring the source into compliance and demonstrate compliance.

9.7.6 Quality Control

The baghouses will be operated and maintained according to the manufacturers recommendations.

A spare parts inventory is maintained by a computerized inventory management system. Parts are automatically queued for re-order when the inventory level falls below a minimum re-order point.

Council Bluffs Energy Center Compliance Certification:

I, Jack L. Alexander, as responsible official for CBEC, hereby certify that, based on information and belief formed after reasonable inquiry, the statements and information in this document are true, accurate, and complete.

Jack L. Alexander

Jack L. Alexander
Senior Vice President, Supply and Marketing

Date: 9-24-02

Pottawattamie
1000000016121
92-3600

AIR CONSTRUCTION PERMIT APPLICATION

DNR

Form FI: Facility Information

Revision: 1/2001

☞ SEE INSTRUCTIONS ON REVERSE SIDE ☞

DNR USE ONLY	
Plant ID: 78-01-026	Project Number: 02-528

COMPANY NAME

(1) MidAmerican Energy Company

(2) CERTIFICATION

I certify that based on information and belief formed after reasonable inquiry, the enclosed documents including the attachments are true, accurate, and complete. Legal entitlement to install and operate the equipment covered by and on the property identified in the permit application has been obtained.

Responsible Official: Print Name: Jack L. Alexander Title: Sr. Vice President Supply and Marketing

Signature: J. L. Alexander Date: 9-24-02

PLANT PERMIT CONTACT PERSON

(3) Name:	(4) Title:	(5) Telephone #:	(6) E-mail Address:
Chad A. Teply	Outage Project Manager	(712) 366-5316	cateply@midamerican.com

(7) Street Address:	(8) City:	(9) State:	(10) Zip:
2115 Navajo Road	Council Bluffs	Iowa	51501

EQUIPMENT LOCATION

(11) Street or Route:	(12) City:	(13) State:	(14) Zip:
same		Iowa	

(15) Is the Equipment Portable?

☒ No

☐ Yes, other location(s) is:

PERMIT PREPARER/CONSULTANT

(16) Name:	(17) Title:	(18) Iowa P.E. Number (see instructions):	(19) Signature:
Steven C. Guyer	Director, Environmental Services	NA	Steve C. Guyer

(20) Company Name:	(21) Telephone #:	(22) Fax #:
MidAmerican Energy Company	(515) 281-2692	(515) 242-3084

(23) Street Address:	(24) City:	(25) State:	(26) Zip:
666 Grand Avenue	Des Moines	Iowa	50309

BUSINESS TYPE

(27) Briefly describe the activity of your business and its principal product:

Council Bluffs Energy Center (CBEC) generates electric power for sale to the customers of MidAmerican, the operator of CBEC. Refer to Section 2 of the application package for a general process flow diagram for CBEC. The generating plant produces electricity by combusting coal to produce heat to convert water to steam. The steam powers turbines attached to electric generators. Generators convert mechanical energy supplied by a turbine into electrical energy.

(28) Provide SIC code of your plant (if known): 4911

(29) APPLICATION FORMS ATTACHED

☒ EU(Number of forms #: 18) ☒ CS(#: 19) ☒ EC(#: 18) ☒ EI(#: 1) ☒ M(#:) ☒ L(#:)

Other Forms and Attachments: Figure EU/EC-1

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(IDNR Form 542-3190-03)

AIR CONSTRUCTION PERMIT APPLICATION

Form EU: **Emission Unit Information** **Revision: 1/2001**

SEE INSTRUCTIONS ON REVERSE SIDE

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS		
(1) Emission Unit (EU) Name: *Rotary Car Dumper*	(2) EU ID Number: *006*	(3) Emission Unit Type ☐ New Source ☐ Unpermitted Existing Source ☒ Modification to a Permitted Source Previous Permit # is: *78-A-167*
(4) Manufacturer: TBD	(5) Model: TBD	
(6) Maximum Capacity: *3500 tons of coal per hour*	(7) Date of Construction: *1/1/77*	
(8) Date of Modification (if applicable): *TBD*	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: *Baghouse CE007*	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☒ Other: *0.01 gr/dscf (emissions from the baghouse)* *Refer to Section 4 of the application package*

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

Coal received at CBEC by railcar is unloaded into receiving hoppers at the rotary car dumper. Coal is removed from the hopper at a rate of 3,500 TPH and discharged onto a conveyor. Refer to Section 2.3.2 in the application package for additional details.

Refer to Figure 2-3, coal handling process diagram.

AIR CONSTRUCTION PERMIT APPLICATION

Form EU: **Emission Unit Information** — **Revision: 1/2001**

☛ **SEE INSTRUCTIONS ON REVERSE SIDE** ☛

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS

(1) Emission Unit (EU) Name: *Transfer House 4*	(2) EU ID Number: *13*	(3) Emission Unit Type ☐ New Source ☐ Unpermitted Existing Source ☒ Modification to a Permitted Source Previous Permit # is: *78-A-173*
(4) Manufacturer: *TBD*	(5) Model: *TBD*	
(6) Maximum Capacity: *3,600 tons of coal per hour*	(7) Date of Construction: *1/1/77*	
(8) Date of Modification (if applicable): *TBD*	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: *Baghouse CE014*	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☒ Other: *0.01 gr/dscf (emissions from the baghouse)* *Refer to Section 4 of the application package*

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

Coal is conveyed from Transfer House 5 and Transfer House 3 to a surge hopper in Transfer House 4. The Transfer House 4 (Crusher House) 900 T/hr vibratory feeders and 900 T/hr ring granulators (crushers) will be replaced with 1600 T/hr equipment to accommodate Unit 4. The new crushers will discharge onto conveyors), which will transport the coal to the surge hopper located at the transfer conveyor bay area. Refer to Section 2.3.2 in the application package for additional details.

Refer to Figure 2-3, coal handling process diagram.

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form EU:** **Emission Unit Information** **Revision: 1/2001**

SEE INSTRUCTIONS ON REVERSE SIDE

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS

(1) Emission Unit (EU) Name: *CBEC 4 Boiler*	(2) EU ID Number: *141*	(3) Emission Unit Type ☒ New Source ☐ Unpermitted Existing Source ☐ Modification to a Permitted Source Previous Permit # is:
(4) Manufacturer: TBD	(5) Model: *TBD*	
(6) Maximum Capacity: *7,675 mmBTU/hour*	(7) Date of Construction: *TBD*	
(8) Date of Modification (if applicable): N/A	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: *Pulse Jet Baghouse CE141a* *Selective Catalytic Reduction CE141b* *Lime Spray Dryer Flue Gas Desulfurization CE141C*	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☒ Other: *Refer to Section 4 of the application package*

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

The proposed Unit 4 boiler will be an indoor-type supercritical pulverized coal fired boiler designed for "base load" operation. The unit will have a maximum gross heat input of approximately 7,675 MMBtu/hr and a nominal net plant electrical output of approximately 750 MW. Unit 4 will generate a main steam pressure of 3,500 to 3,700 psig and will generate steam at 1,050 to 1,100 °F. The primary fuel for Unit 4 will be Powder River Basin sub-bituminous coal. Fuel oil (No.2) will be used as the start-up fuel. Refer to Section 2 of the application package for additional details.

Refer to Figure 2-2 for a detailed flow diagram of Unit 4.

AIR CONSTRUCTION PERMIT APPLICATION

Form EU: **Emission Unit Information** **Revision: 1/2001**

SEE INSTRUCTIONS ON REVERSE SIDE

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS

(1) Emission Unit (EU) Name: *Auxiliary Boiler*	(2) EU ID Number: *142*	(3) Emission Unit Type ☒ New Source ☐ Unpermitted Existing Source ☐ Modification to a Permitted Source Previous Permit # is:
(4) Manufacturer: *TBD*	(5) Model: *TBD*	
(6) Maximum Capacity: *974 gallons of fuel/hour*	(7) Date of Construction: *TBD*	
(8) Date of Modification (if applicable): N/A	(9) Is this a Controlled Emission Unit? ☒ No ☐ Yes Control equipment name/ID are:	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☒ Operation Hour Limits: *2,500 hours/ year*	☐ Production Limits:
☐ Material Usage Limits:	☐ Other:

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

The auxiliary boiler burns No. 2 fuel oil and will be used only when Unit 4 is not in operation, or as needed for start-up of Unit 4, or not more than 10 hours/ month for testing.

Refer to attached Figure EU/EC-1.

AIR CONSTRUCTION PERMIT APPLICATION

Form EU: **Emission Unit Information** **Revision: 1/2001**

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS		
(1) Emission Unit (EU) Name: *Emergency Generator*	(2) EU ID Number: *143*	(3) Emission Unit Type ☒ New Source ☐ Unpermitted Existing Source ☐ Modification to a Permitted Source Previous Permit # is:
(4) Manufacturer: TBD	(5) Model: TBD	
(6) Maximum Capacity: *73 gallons of No. 2 fuel/hour*	(7) Date of Construction: TBD	
(8) Date of Modification (if applicable): N/A	(9) Is this a Controlled Emission Unit? ☒ No ☐ Yes Control equipment name/ID are:	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☒ Operation Hour Limits: *500 hours/year*	☐ Production Limits:
☐ Material Usage Limits:	☐ Other:

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

The emergency generator burns No. 2 fuel oil and will be operated a maximum of 500 hours per year.

Refer to Figure EU/EC-1.

AIR CONSTRUCTION PERMIT APPLICATION

Form EU: **Emission Unit Information** **Revision: 1/2001**

☞ **SEE INSTRUCTIONS ON REVERSE SIDE** ☞

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS

(1) Emission Unit (EU) Name: *Cooling Tower*	(2) EU ID Number: *145*	(3) Emission Unit Type ☒ New Source ☐ Unpermitted Existing Source ☐ Modification to a Permitted Source Previous Permit # is:
(4) Manufacturer: TBD	(5) Model: TBD	
(6) Maximum Capacity: *349,400 gallons of water/minute*	(7) Date of Construction: TBD	
(8) Date of Modification (if applicable): N/A	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: *Drift Eliminator CE145*	

(10) Are you requesting any permit limits? ☒ No ☐ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☐ Other:

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

The cooling tower receives water from the condenser, cools it, and returns the water to the process. Refer to Section 2 of the application for additional details.

Refer to Figure 2-2 for a schematic of the process.

AIR CONSTRUCTION PERMIT APPLICATION

Form EU: **Emission Unit Information** **Revision: 1/2001**

☛ **SEE INSTRUCTIONS ON REVERSE SIDE** ☛

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS

(1) Emission Unit (EU) Name: *Transfer House 5*	(2) EU ID Number: *155*	(3) Emission Unit Type ☒ New Source ☐ Unpermitted Existing Source ☐ Modification to a Permitted Source Previous Permit # is:
(4) Manufacturer: *TBD*	(5) Model: *TBD*	
(6) Maximum Capacity: *1,000 tons of coal per hour*	(7) Date of Construction: *TBD*	
(8) Date of Modification (if applicable): N/A	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: *Baghouse CE014*	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☒ Other: *0.01 gr/dscf (emissions from the baghouse)* *Refer to Section 4 of the application package*

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

Transfer House 5 receives coal from the east emergency reclaim hopper and transfers it to the crusher house (transfer house 4). Note that emissions from the Transfer House 5 are captured by the baghouse for transfer house 4. Refer to Section 2.3.2 in the application package for additional details.

Refer to Figure 2-3, coal handling process diagram.

AIR CONSTRUCTION PERMIT APPLICATION

Form EU: Emission Unit Information **Revision: 1/2001**

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS

(1) Emission Unit (EU) Name: *Transfer Conveyor Bay*	(2) EU ID Number: *159*	(3) Emission Unit Type ☒ New Source ☐ Unpermitted Existing Source ☐ Modification to a Permitted Source Previous Permit # is:
(4) Manufacturer: *TBD*	(5) Model: *TBD*	
(6) Maximum Capacity: *1,800 tons of coal/ hour*	(7) Date of Construction: *TBD*	
(8) Date of Modification (if applicable): N/A	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: Baghouse	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☒ Other: *0.01 gr/dscf (emissions from the baghouse)* *Refer to Section 4 of the application package.*

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

The transfer conveyor bay consists of a hopper and associated conveyors which receive coal from Transfer House 4. The hopper and load-out conveyors transport coal to Unit 3 east/west silos or Unit 4 east/west silos. Refer to Section 2.3.2 in the application package for additional details.

Refer to Figure 2-3, coal handling process diagram.

AIR CONSTRUCTION PERMIT APPLICATION

Form EU: Emission Unit Information

Revision: 1/2001

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Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS

(1) Emission Unit (EU) Name: *Unit 4 East Silos*	(2) EU ID Number: *160*	(3) Emission Unit Type ☒ New Source ☐ Unpermitted Existing Source ☐ Modification to a Permitted Source Previous Permit # is:
(4) Manufacturer: TBD	(5) Model: TBD	
(6) Maximum Capacity: *900 tons of coal per hour load-in*	(7) Date of Construction: *TBD*	
(8) Date of Modification (if applicable): N/A	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: *Baghouse CE160*	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☒ Other: *0.01 gr/dscf (emissions from the baghouse)* *Refer to Section 4 of the application package*

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

Series of 3 coal storage silos and associated conveyors with 900 tons/hour load-in capacity. Refer to Section 2.3.2 in the application package for additional details.

Refer to Figure 2-3, coal handling process diagram.

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form EU:** **Emission Unit Information** **Revision: 1/2001**

SEE INSTRUCTIONS ON REVERSE SIDE

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS		
(1) Emission Unit (EU) Name: *Unit 4 West Silos*	(2) EU ID Number: *161*	(3) Emission Unit Type ☒ New Source ☐ Unpermitted Existing Source ☐ Modification to a Permitted Source Previous Permit # is:
(4) Manufacturer: TBD	(5) Model: TBD	
(6) Maximum Capacity: *900 tons of coal per hour*	(7) Date of Construction: *TBD*	
(8) Date of Modification (if applicable): N/A	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: *Baghouse CE161*	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☒ Other: *0.01 gr/dscf (emissions from the baghouse)* *Refer to Section 4 of the application package*

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

Series of 3 coal storage silos and associated conveyors with 900 tons/hour load-in capacity. Refer to Section 2.3.2 in the application package for additional details.

Refer to Figure 2-3, coal handling process diagram.

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form EU:** **Emission Unit Information** Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS

(1) Emission Unit (EU) Name: *Lime Filter Separator*	(2) EU ID Number: *162*	(3) Emission Unit Type ☒ New Source ☐ Unpermitted Existing Source ☐ Modification to a Permitted Source Previous Permit # is:
(4) Manufacturer: *TBD*	(5) Model: *TBD*	
(6) Maximum Capacity: *100 TPH (tons of lime per hour)*	(7) Date of Construction: *TBD*	
(8) Date of Modification (if applicable): N/A	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: *Baghouse CE162*	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☒ Other: *0.01 gr/dscf (emissions from the baghouse)* *Refer to Section 4 of the application package*

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

A combination filter / separator will pneumatically remove lime from a totally enclosed, 100-ton railcar by means of a negative pressure system. The combination filter/separator will separate lime from the conveying air, performing the function of a cyclone separator and baghouse in one vessel.

The lime will then be discharged from the filter / separator into a transfer hopper and then into a positive pressure conveyance pipe to be transferred to the lime storage silo. Refer to Section 2.4.1 of the application package for additional details.

Refer to Figure EU/EC-1.

AIR CONSTRUCTION PERMIT APPLICATION

Form EU: Emission Unit Information — Revision: 1/2001

SEE INSTRUCTIONS ON REVERSE SIDE

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS

(1) Emission Unit (EU) Name: *Lime Storage Silo*	(2) EU ID Number: *163*	(3) Emission Unit Type ☒ New Source ☐ Unpermitted Existing Source ☐ Modification to a Permitted Source Previous Permit # is:
(4) Manufacturer: *TBD*	(5) Model: *TBD*	
(6) Maximum Capacity: *2,000 ton*	(7) Date of Construction: *TBD*	
(8) Date of Modification (if applicable): N/A	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: *Vent Bag Filter CE163*	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☒ Other: *0.02 gr/dscf (emissions from the baghouse)* *Refer to Section 4 of the application package*

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

The lime is transferred to the lime storage silo by a positive pressure conveyance pipe connected to the transfer hopper.

Lime from the storage silo will be pneumatically transferred to a transfer hopper, which then discharges into a conveyance pipe and conveys the lime using positive pressure to the day bin. Refer to Section 2.4.1 of the application package for additional details.

Refer to Figure EU/EC-1.

AIR CONSTRUCTION PERMIT APPLICATION

Form EU: **Emission Unit Information** **Revision: 1/2001**

☞ **SEE INSTRUCTIONS ON REVERSE SIDE** ☞

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS

(1) Emission Unit (EU) Name: *Urea Silo #1*	(2) EU ID Number: *164A*	(3) Emission Unit Type ☒ New Source
(4) Manufacturer: *TBD*	(5) Model: *TBD*	☐ Unpermitted Existing Source ☐ Modification to a Permitted Source
(6) Maximum Capacity: *60 ton*	(7) Date of Construction: *TBD*	Previous Permit # is:
(8) Date of Modification (if applicable): N/A	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: *Vent Bag Filter CE164A*	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☒ Other: *0.02 gr/dscf (emissions from the baghouse)* *Refer to Section 4 of the application package*

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

The urea used for the generation of ammonia will be delivered by truck or rail and stored in one of two vertical dry urea storage silos. Each storage silo will be equipped with a bin vent filter for dust control. Refer to Section 2.4.2 of the application package for additional details.

Refer to Figure EU/EC-1.

AIR CONSTRUCTION PERMIT APPLICATION

Form EU: **Emission Unit Information** **Revision: 1/2001**

☛ **SEE INSTRUCTIONS ON REVERSE SIDE** ☛

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS

(1) Emission Unit (EU) Name: *Urea Silo #2*	(2) EU ID Number: *164B*	(3) Emission Unit Type ☒ New Source ☐ Unpermitted Existing Source ☐ Modification to a Permitted Source Previous Permit # is:
(4) Manufacturer: *TBD*	(5) Model: *TBD*	
(6) Maximum Capacity: *60 tons*	(7) Date of Construction: *TBD*	
(8) Date of Modification (if applicable): N/A	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: *Vent Bag Filter CE164B*	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☒ Other: *0.02 gr/dscf (emissions from the baghouse)* *Refer to Section 4 of the application package*

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

The urea used for the generation of ammonia will be delivered by truck or rail and stored in one of two vertical dry urea storage silos. Each storage silo will be equipped with a bin vent filter for dust control. Refer to Section 2.4.2 of the application package for additional details.

Refer to Figure EU/EC-1..

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form EU:** **Emission Unit Information** **Revision: 1/2001**

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS

(1) Emission Unit (EU) Name: *Flyash/FGD Waste Storage Silo*	(2) EU ID Number: *167*	(3) Emission Unit Type ☒ New Source ☐ Unpermitted Existing Source ☐ Modification to a Permitted Source Previous Permit # is:
(4) Manufacturer: TBD	(5) Model: TBD	
(6) Maximum Capacity: *2000 Tons*	(7) Date of Construction: *TBD*	
(8) Date of Modification (if applicable): N/A	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: *Vent Bag Filter CE167*	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☒ Other: *0.02 gr/dscf (emissions from the baghouse)* *Refer to Section 4 of the application package*

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

The pulse-jet baghouse will be incorporated into the dry FGD collection system with each row of hoppers having its own conveyance header. All flyash / FGD waste will be collected and stored in a FGD waste storage silo, where it will be stored and transferred to an offsite disposal landfill. Refer to Section 2.4.3 in the application package for additional details.

Refer to Figure 2-4, Flyash/ FGD Waste process diagram.

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form EU:** **Emission Unit Information** **Revision: 1/2001**

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS

(1) Emission Unit (EU) Name: Flyash/FGD Waste Vacuum System Exhauster #1	(2) EU ID Number: *168*	(3) Emission Unit Type ☒ New Source ☐ Unpermitted Existing Source ☐ Modification to a Permitted Source Previous Permit # is:
(4) Manufacturer: *TBD*	(5) Model: *TBD*	
(6) Maximum Capacity: TBD	(7) Date of Construction: *TBD*	
(8) Date of Modification (if applicable): *N/A*	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: *Baghouse CE168*	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☒ Other: *0.01 gr/dscf (emissions from the baghouse)* *Refer to Section 4 of the application package*

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

Refer to Section 2.4.3 in the application package for additional details.

Refer to Figure 2-4, Flyash/ FGD Waste process diagram.

AIR CONSTRUCTION PERMIT APPLICATION

Form EU: Emission Unit Information Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS

(1) Emission Unit (EU) Name: Flyash/FGD Waste Vacuum System Exhauster #2	(2) EU ID Number: *169*	(3) Emission Unit Type ☒ New Source
(4) Manufacturer: *TBD*	(5) Model: *TBD*	☐ Unpermitted Existing Source ☐ Modification to a Permitted Source
(6) Maximum Capacity: *TBD*	(7) Date of Construction: *TBD*	Previous Permit # is:
(8) Date of Modification (if applicable): N/A	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: *Baghouse CE169*	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☒ Other: *0.01 gr/dscf (emissions from the baghouse)* *Refer to Section 4 of the application package*

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

Refer to Section 2.4.3 in the application package for additional details.

Refer to Figure 2-4, Flyash/ FGD Waste process diagram.

AIR CONSTRUCTION PERMIT APPLICATION

Form EU: **Emission Unit Information** Revision: 1/2001

☞ SEE INSTRUCTIONS ON REVERSE SIDE ☞

Company Name: *MidAmerican Energy*

EMISSION UNIT (SOURCE OF AIR POLLUTANT(S)) DESCRIPTION AND SPECIFICATIONS

(1) Emission Unit (EU) Name: *Flyash/FGD Waste Vacuum System Exhauster #3*	(2) EU ID Number: *170*	(3) Emission Unit Type ☒ New Source ☐ Unpermitted Existing Source ☐ Modification to a Permitted Source Previous Permit # is:
(4) Manufacturer: *TBD*	(5) Model: *TBD*	
(6) Maximum Capacity: *TBD*	(7) Date of Construction: *TBD*	
(8) Date of Modification (if applicable): N/A	(9) Is this a Controlled Emission Unit? ☐ No ☒ Yes Control equipment name/ID are: *Baghouse CE170*	

(10) Are you requesting any permit limits? ☐ No ☒ Yes. If yes, check below and write down all that apply

☐ Operation Hour Limits:	☐ Production Limits:
☐ Material Usage Limits:	☒ Other: *0.01 gr/dscf (emissions from the baghouse)* *Refer to Section 4 of the application package*

Rationale for Requesting the Limit(s):

(11) Provide a description **and** a drawing to show quantitatively how **product or material** flows through this emission unit. Include product input and output, fuel throughput, and any parameters which impact air emissions. If space below is insufficient, attach a separate sheet labeled EU-11A.

Refer to Section 2.4.3 in the application package for additional details.

Refer to Figure 2-4, Flyash/ FGD Waste process diagram.

AIR CONSTRUCTION PERMIT APPLICATION

Form EU1: Industrial Engine Information — **Revision: 1/2001**

SEE INSTRUCTIONS ON REVERSE SIDE

EXEMPTION

According to 567 Iowa Administrative Code Chapter 22.1(2)r, an internal combustion engine with a brake horsepower rating of less than 400 is exempted from the provisions of construction permits.

Company Name: MidAmerican Energy — ☒ **Private Company** ☐ **Public Facility**

ENGINE (EMISSION UNIT) DESCRIPTION AND SPECIFICATIONS

☒ **New Unit** ☐ **Unpermitted Existing Unit** ☐ **Modification to An Unit with Permit #:**

(1) Use of Engine: ☐ **Normal Operation** ☒ **Emergency** ☐ **Back-up** ☐ **Other:**

(2) Engine ID Number: TBD	(3) Rated Power: ☒ 250 Brake Horsepower(bhp) ☐ Kilowatts(kW)	
(4) Construction Date: TBD	(5) Manufacturer: TBD	(6) Model: TBD
(7) Date of Modification (if applicable): NA	(8) Serial Number (if available): Not available	(9) Control Device (if any): None

FUEL DESCRIPTION AND SPECIFICATIONS

(10) Fuel Type	☒ Diesel Fuel (# 2) (gal/hr)	☐ Gasoline Fuel (gal/hr)	☐ Natural Gas (cf/hr)	☐ Other Fuels (unit:)
(11) Full Load Consumption Rate	14			
(12) Actual Consumption Rate	14			
(13) Sulfur Content wt%	0.05	N/A	N/A	

OPERATING LIMITS & SCHEDULE

(14) Imposed Operating Limits (hours/year, or gallons fuel/year, etc.):
NA

(15) Operating Schedule (hours/day, months/year, etc.):
500 hours/year

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(16) Stack/Vent ID: 144	(17) Stack Opening Size: ☒ circular, diameter (inches) is: 3
(18) Stack Height (feet) from the Ground: 15	☐ other, size (inches x inches) is: ☐ Single Stack ☐ Dual Stack
(19) Stack Height (feet) above the Building (If Applicable): NA	(20) Discharge Style: ☒ V (Vertical, without rain cap or with unobstructing rain cap) ☐ VR (Vertical, with obstructing rain cap)
(21) Distance (feet) from the Property Line: 598	☐ H (Horizontal discharge) ☐ D (Downward discharge; for example, a goose neck stack)

EXHAUST INFORMATION

(22) Rated Flow Rate (☐ acfm ☒ scfm):	(23) Moisture Content % (if known):	(24) Exit Temperature (°F)
1,030		845

APPENDIX A

CS Forms

AIR CONSTRUCTION PERMIT APPLICATION

Form CS: **Control Equipment and Stack/Vent Information** — Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Baghouse CE007*

(2) Date of Installation: *1/1/1977*

(3) Manufacturer: *TBD*

(4) Model: *TBD*

(5) Date of Modification (if any): *TBD*

(6) Is operating schedule different than emission unit(s) controlled?
☒ No ☐ Yes Specify the schedule:

(7) Capture Hood Involved?
☐ No ☒ Yes

(8) Capture Hood Efficiency (if known): *Unknown*

(9) ID(s) of EU(s) Controlled: *006*

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	*PM*	*PM_{10}*			
Control Efficiency %	*99+*	*90+*			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *006*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *82*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *90*

(15) Height (ft) from Highest Building Level: 55

(16) Distance (feet) from the Nearest Property Line: *1,453*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *150,000*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F): *Ambient*

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form CS:** **Control Equipment and Stack/Vent Information** — **Revision: 1/2001**

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

Company Name: MidAmerican Energy

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): Baghouse CE006A		(2) Date of Installation: 1/1/1977
(3) Manufacturer: TBD	(4) Model: TBD	(5) Date of Modification (if any): TBD
(6) Is operating schedule different than emission unit(s) controlled? ☒ No ☐ Yes Specify the schedule:		(9) ID(s) of EU(s) Controlled: 006
(7) Capture Hood Involved? ☒ No ☐ Yes	(8) Capture Hood Efficiency (if known): N/A	

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☐ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	PM	PM_{10}			
Control Efficiency %	99+	90+			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: 006	(13) Stack Opening Size (check one): ☒ circular, diameter (inches) is: 82
(14) Height (ft) from the Ground: 90	☐ other, size (inches x inches) is:
(15) Height (ft) from Highest Building Level: 55	(17) Discharge Style (check one): ☒ V (Vertical, without rain cap or with unobstructing rain cap)
(16) Distance (feet) from the Nearest Property Line: 443	☐ VR (Vertical, with obstructing rain cap) ☐ D (Downward discharge; for example, a goose neck stack) ☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm):	(19) Moisture Content % (if known):	(20) Exit Temperature (°F)
150,000		Ambient

AIR CONSTRUCTION PERMIT APPLICATION

Form CS: Control Equipment and Stack/Vent Information Revision: 1/2001

☞ SEE INSTRUCTIONS ON REVERSE SIDE ☞

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Baghouse CE007A*		(2) Date of Installation: *TBD*
(3) Manufacturer: *TBD*	(4) Model: *TBD*	(5) Date of Modification (if any): *N/A*
(6) Is operating schedule different than emission unit(s) controlled? ☒ No ☐ Yes Specify the schedule:		(9) ID(s) of EU(s) Controlled: *006*
(7) Capture Hood Involved? ☒ No ☐ Yes	(8) Capture Hood Efficiency (if known): *N/A*	

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☐ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	PM	PM_{10}			
Control Efficiency %	99+	90+			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *006*	(13) Stack Opening Size (check one): ☒ circular, diameter (inches) is: *82*
(14) Height (ft) from the Ground: *90*	☐ other, size (inches x inches) is:
(15) Height (ft) from Highest Building Level: *55*	(17) Discharge Style (check one): ☒ V (Vertical, without rain cap or with unobstructing rain cap)
(16) Distance (feet) from the Nearest Property Line: *443*	☐ VR (Vertical, with obstructing rain cap) ☐ D (Downward discharge; for example, a goose neck stack) ☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm):	(19) Moisture Content % (if known):	(20) Exit Temperature (°F)
150,000		*Ambient*

AIR CONSTRUCTION PERMIT APPLICATION

Form CS: Control Equipment and Stack/Vent Information — Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Baghouse CE014*

(2) Date of Installation: *1/1/77*

(3) Manufacturer: *Air-Cure*

(4) Model: *484-RF-10*

(5) Date of Modification (if any): *3-29-99*

(6) Is operating schedule different than emission unit(s) controlled?
☒ No ☐ Yes Specify the schedule:

(9) ID(s) of EU(s) Controlled: *013 & 155*

(7) Capture Hood Involved?
☐ No ☒ Yes

(8) Capture Hood Efficiency (if known): *Unknown*

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	*PM*	*PM_{10}*			
Control Efficiency %	*99+*	*90+*			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *013*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *39*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *50*

(15) Height (ft) from Highest Building Level: *NA*

(16) Distance (feet) from the Nearest Property Line: *1,043*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *26,500*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F): *Ambient*

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form CS:** Control Equipment and Stack/Vent Information — Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Baghouse CE141a*

(2) Date of Installation: *TBD*

(3) Manufacturer: *TBD*

(4) Model: *TBD*

(5) Date of Modification (if any): *N/A*

(6) Is operating schedule different than emission unit(s) controlled?
☒ No ☐ Yes Specify the schedule:

(7) Capture Hood Involved?
☒ No ☐ Yes

(8) Capture Hood Efficiency (if known): *N/A*

(9) ID(s) of EU(s) Controlled: *141*

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	*PM*	*PM_{10}*	*Lead & All Other Metals*	*Hg*	
Control Efficiency %	*99.7*	*98.2*	*99+*	*20*	

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *141*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *295.8*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *550*

(15) Height (ft) from Highest Building Level: *NA*

(16) Distance (feet) from the Nearest Property Line: *1,257*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *2,660,982*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F): *165*

AIR CONSTRUCTION PERMIT APPLICATION

Form CS: **Control Equipment and Stack/Vent Information** **Revision: 1/2001**

☞ SEE INSTRUCTIONS ON REVERSE SIDE ☞

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Selective Catalytic Reduction (SCR) CE141b*

(2) Date of Installation: *TBD*

(3) Manufacturer: *TBD*

(4) Model: *TBD*

(5) Date of Modification (if any): *N/A*

(6) Is operating schedule different than emission unit(s) controlled?
☒ No ☐ Yes Specify the schedule:

(9) ID(s) of EU(s) Controlled: *141*

(7) Capture Hood Involved?
☒ No ☐ Yes

(8) Capture Hood Efficiency (if known): *N/A*

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	*NOx*				
Control Efficiency %	*60*				

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *141*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *295.8*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *550*

(15) Height (ft) from Highest Building Level: *NA*

(16) Distance (feet) from the Nearest Property Line: *1,257*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *2,660,982*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F) *165*

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form CS:** **Control Equipment and Stack/Vent Information** **Revision: 1/2001**

SEE INSTRUCTIONS ON REVERSE SIDE

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Lime Spray Dryer Flue Gas Desulfurization CE141c*

(2) Date of Installation: *TBD*

(3) Manufacturer: *TBD*

(4) Model: *TBD*

(5) Date of Modification (if any): *N/A*

(6) Is operating schedule different than emission unit(s) controlled?
☒ No ☐ Yes Specify the schedule:

(9) ID(s) of EU(s) Controlled: *141*

(7) Capture Hood Involved?
☒ No ☐ Yes

(8) Capture Hood Efficiency (if known): *N/A*

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	*SOx*	H_2SO_4	*HF*	*HCL*	
Control Efficiency %	*90.4*	*90*	*90*	*90*	

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *141*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *295.8*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *550*

(15) Height (ft) from Highest Building Level: *NA*

(16) Distance (feet) from the Nearest Property Line: *1,257*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *2,660,982*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F) *165*

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form CS:** **Control Equipment and Stack/Vent Information** — **Revision: 1/2001**

SEE INSTRUCTIONS ON REVERSE SIDE

Company Name: MidAmerican Energy

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): None

(2) Date of Installation:

(3) Manufacturer:

(4) Model:

(5) Date of Modification (if any):

(6) Is operating schedule different than emission unit(s) controlled?
☐ No ☐ Yes Specify the schedule:

(7) Capture Hood Involved?
☐ No ☐ Yes

(8) Capture Hood Efficiency (if known):

(9) ID(s) of EU(s) Controlled:

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☐ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled					
Control Efficiency %					

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: 142

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: 38.9
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: 310

(15) Height (ft) from Highest Building Level: 10

(16) Distance (feet) from the Nearest Property Line: 1,280

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): 49,300

(19) Moisture Content % (if known):

(20) Exit Temperature (°F): 400

AIR CONSTRUCTION PERMIT APPLICATION

Form CS: **Control Equipment and Stack/Vent Information** — Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *None*

(2) Date of Installation:

(3) Manufacturer:

(4) Model:

(5) Date of Modification (if any):

(6) Is operating schedule different than emission unit(s) controlled?
☐ No ☐ Yes Specify the schedule:

(7) Capture Hood Involved?
☐ No ☐ Yes

(8) Capture Hood Efficiency (if known):

(9) ID(s) of EU(s) Controlled:

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☐ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled					
Control Efficiency %					

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *143*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *10*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *20*

(15) Height (ft) from Highest Building Level: NA

(16) Distance (feet) from the Nearest Property Line: *1,149*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *5,430*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F): *1,025*

AIR CONSTRUCTION PERMIT APPLICATION

Form CS: **Control Equipment and Stack/Vent Information** Revision: 1/2001

☞ SEE INSTRUCTIONS ON REVERSE SIDE ☞

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Drift Eliminator CE145*

(2) Date of Installation: *TBD*

(3) Manufacturer: *TBD*

(4) Model: *TBD*

(5) Date of Modification (if any): *N/A*

(6) Is operating schedule different than emission unit(s) controlled?
☒ No ☐ Yes Specify the schedule:

(9) ID(s) of EU(s) Controlled: *145*

(7) Capture Hood Involved?
☒ No ☐ Yes

(8) Capture Hood Efficiency (if known): *N/A*

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	PM	PM_{10}			
Control Efficiency %	99.9995% (1)	99.9995% (1)			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

(1) The drift eliminator controls to 0.0005% gal drift/ gal flow.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *145*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *410 per cell*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *48*

(15) Height (ft) from Highest Building Level: *N/A*

(16) Distance (feet) from the Nearest Property Line: *2,238*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *1,401,485 per cell*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F): *103*

AIR CONSTRUCTION PERMIT APPLICATION

Form CS: Control Equipment and Stack/Vent Information

Revision: 1/2001

SEE INSTRUCTIONS ON REVERSE SIDE

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Baghouse CE159*

(2) Date of Installation: *TBD*

(3) Manufacturer: *TBD*

(4) Model: *TBD*

(5) Date of Modification (if any): *N/A*

(6) Is operating schedule different than emission unit(s) controlled?
☒ No ☐ Yes Specify the schedule:

(7) Capture Hood Involved?
☐ No ☒ Yes

(8) Capture Hood Efficiency (if known): *Unknown*

(9) ID(s) of EU(s) Controlled: *159*

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	*PM*	*PM_{10}*			
Control Efficiency %	*99+*	*90+*			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *159*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *30*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *305*

(15) Height (ft) from Highest Building Level: *5*

(16) Distance (feet) from the Nearest Property Line: *1,129*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *19,500*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F): *Ambient*

AIR CONSTRUCTION PERMIT APPLICATION

Form CS: Control Equipment and Stack/Vent Information Revision: 1/2001

☞ SEE INSTRUCTIONS ON REVERSE SIDE ☞

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Baghouse CE160*

(2) Date of Installation: *TBD*

(3) Manufacturer: *TBD*

(4) Model: *TBD*

(5) Date of Modification (if any): *N/A*

(6) Is operating schedule different than emission unit(s) controlled?
☒ No ☐ Yes Specify the schedule:

(7) Capture Hood Involved?
☐ No ☒ Yes

(8) Capture Hood Efficiency (if known): *Unknown*

(9) ID(s) of EU(s) Controlled: *160*

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	PM	PM_{10}			
Control Efficiency %	99+	90+			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *160*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *40*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *305*

(15) Height (ft) from Highest Building Level: *5*

(16) Distance (feet) from the Nearest Property Line: *1,329*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *34,800*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F): *Ambient*

AIR CONSTRUCTION PERMIT APPLICATION

Form CS: Control Equipment and Stack/Vent Information Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Baghouse CE161*

(2) Date of Installation: *TBD*

(3) Manufacturer: *TBD*

(4) Model: *TBD*

(5) Date of Modification (if any): *N/A*

(6) Is operating schedule different than emission unit(s) controlled?
☒ No ☐ Yes Specify the schedule:

(7) Capture Hood Involved?
☐ No ☒ Yes

(8) Capture Hood Efficiency (if known): *Unknown*

(9) ID(s) of EU(s) Controlled: *161*

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	*PM*	*PM_{10}*			
Control Efficiency %	*99+*	*90+*			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *161*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *35*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *305*

(15) Height (ft) from Highest Building Level: *5*

(16) Distance (feet) from the Nearest Property Line: *1,112*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *26,100*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F): *Ambient*

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form CS:** Control Equipment and Stack/Vent Information — Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Baghouse CE162*

(2) Date of Installation: *TBD*

(3) Manufacturer: *TBD*

(4) Model: *TBD*

(5) Date of Modification (if any): *N/A*

(6) Is operating schedule different than emission unit(s) controlled?
☒ No ☐ Yes Specify the schedule:

(7) Capture Hood Involved?
☒ No ☐ Yes

(8) Capture Hood Efficiency (if known): *N/A*

(9) ID(s) of EU(s) Controlled: *162*

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	PM	PM_{10}			
Control Efficiency %	99+	90+			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *162*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *10*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *12*

(15) Height (ft) from Highest Building Level: *NA*

(16) Distance (feet) from the Nearest Property Line: *1,391*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *2,000*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F): *Ambient*

AIR CONSTRUCTION PERMIT APPLICATION

Form CS: Control Equipment and Stack/Vent Information — Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Vent Bag Filter CE163*

(2) Date of Installation: *TBD*

(3) Manufacturer: *TBD*

(4) Model: *TBD*

(5) Date of Modification (if any): *N/A*

(6) Is operating schedule different than emission unit(s) controlled?
☒ No ☐ Yes Specify the schedule:

(9) ID(s) of EU(s) Controlled: *163*

(7) Capture Hood Involved?
☒ No ☐ Yes

(8) Capture Hood Efficiency (if known): *N/A*

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	PM	PM_{10}			
Control Efficiency %	99+	90+			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *163*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *20*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *90*

(15) Height (ft) from Highest Building Level: *5*

(16) Distance (feet) from the Nearest Property Line: *1,391*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *1,500*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F): *Ambient*

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form CS: Control Equipment and Stack/Vent Information** **Revision: 1/2001**

☞ SEE INSTRUCTIONS ON REVERSE SIDE ☞

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Vent Bag Filter CE164A*		(2) Date of Installation: *TBD*
(3) Manufacturer: *TBD*	(4) Model: *TBD*	(5) Date of Modification (if any): *N/A*
(6) Is operating schedule different than emission unit(s) controlled? ☒ No ☐ Yes Specify the schedule:		(9) ID(s) of EU(s) Controlled: *164*
(7) Capture Hood Involved? ☒ No ☐ Yes	(8) Capture Hood Efficiency (if known): *N/A*	

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	*PM*	*PM_{10}*			
Control Efficiency %	*99+*	*90+*			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *164A*	(13) Stack Opening Size (check one): ☒ circular, diameter (inches) is: *12*
(14) Height (ft) from the Ground: *40*	☐ other, size (inches x inches) is:
(15) Height (ft) from Highest Building Level: *5*	(17) Discharge Style (check one): ☒ V (Vertical, without rain cap or with unobstructing rain cap)
(16) Distance (feet) from the Nearest Property Line: *1,440*	☐ VR (Vertical, with obstructing rain cap) ☐ D (Downward discharge; for example, a goose neck stack) ☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm):	(19) Moisture Content % (if known):	(20) Exit Temperature (°F)
500		*Ambient*

AIR CONSTRUCTION PERMIT APPLICATION

Form CS: Control Equipment and Stack/Vent Information Revision: 1/2001

☞ SEE INSTRUCTIONS ON REVERSE SIDE ☞

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Vent Bag Filter CE164B*		(2) Date of Installation: *TBD*
(3) Manufacturer: *TBD*	(4) Model: *TBD*	(5) Date of Modification (if any): *N/A*
(6) Is operating schedule different than emission unit(s) controlled? ☒ No ☐ Yes Specify the schedule:		(9) ID(s) of EU(s) Controlled: *164*
(7) Capture Hood Involved? ☒ No ☐ Yes	(8) Capture Hood Efficiency (if known): *N/A*	

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	*PM*	*PM_{10}*			
Control Efficiency %	*99+*	*90+*			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *164B*	(13) Stack Opening Size (check one): ☒ circular, diameter (inches) is: *12* ☐ other, size (inches x inches) is:
(14) Height (ft) from the Ground: *40*	
(15) Height (ft) from Highest Building Level: *5*	(17) Discharge Style (check one): ☒ V (Vertical, without rain cap or with unobstructing rain cap) ☐ VR (Vertical, with obstructing rain cap) ☐ D (Downward discharge; for example, a goose neck stack) ☐ H (Horizontal discharge)
(16) Distance (feet) from the Nearest Property Line: *1,421*	

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm):	(19) Moisture Content % (if known):	(20) Exit Temperature (°F)
500		*Ambient*

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form CS:** **Control Equipment and Stack/Vent Information** Revision: 1/2001

☞ SEE INSTRUCTIONS ON REVERSE SIDE ☞

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Vent Bag Filter CE167*

(2) Date of Installation: *TBD*

(3) Manufacturer: *TBD*

(4) Model: *TBD*

(5) Date of Modification (if any): *N/A*

(6) Is operating schedule different than emission unit(s) controlled?
☒ No ☐ Yes Specify the schedule:

(9) ID(s) of EU(s) Controlled: *167*

(7) Capture Hood Involved?
☒ No ☐ Yes

(8) Capture Hood Efficiency (if known): *N/A*

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	*PM*	*PM_{10}*			
Control Efficiency %	*99+*	*90+*			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *167*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *24*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *100*

(15) Height (ft) from Highest Building Level: *10*

(16) Distance (feet) from the Nearest Property Line: *1,618*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *3,000*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F): *Ambient*

AIR CONSTRUCTION PERMIT APPLICATION

Form CS: Control Equipment and Stack/Vent Information — **Revision: 1/2001**

SEE INSTRUCTIONS ON REVERSE SIDE

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Baghouse CE168*

(2) Date of Installation: *TBD*

(3) Manufacturer: *TBD*

(4) Model: *TBD*

(5) Date of Modification (if any): *N/A*

(6) Is operating schedule different than emission unit(s) controlled?
☒ No ☐ Yes Specify the schedule:

(9) ID(s) of EU(s) Controlled: *168*

(7) Capture Hood Involved?
☒ No ☐ Yes

(8) Capture Hood Efficiency (if known): *N/A*

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	PM	PM_{10}			
Control Efficiency %	99+	90+			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *168*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *12*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *12*

(15) Height (ft) from Highest Building Level: *NA*

(16) Distance (feet) from the Nearest Property Line: *1,663*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *2,500*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F): *Ambient*

AIR CONSTRUCTION PERMIT APPLICATION

Form CS: Control Equipment and Stack/Vent Information Revision: 1/2001

SEE INSTRUCTIONS ON REVERSE SIDE

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Baghouse CE169*

(2) Date of Installation: *TBD*

(3) Manufacturer: *TBD*

(4) Model: *TBD*

(5) Date of Modification (if any): *N/A*

(6) Is operating schedule different than emission unit(s) controlled?
☒ No ☐ Yes Specify the schedule:

(9) ID(s) of EU(s) Controlled: *169*

(7) Capture Hood Involved?
☒ No ☐ Yes

(8) Capture Hood Efficiency (if known): *N/A*

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	*PM*	*PM_{10}*			
Control Efficiency %	*99+*	*90+*			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *169*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *12*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *12*

(15) Height (ft) from Highest Building Level: *NA*

(16) Distance (feet) from the Nearest Property Line: *1,637*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *2,500*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F): *Ambient*

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form CS:** Control Equipment and Stack/Vent Information

Revision: 1/2001

SEE INSTRUCTIONS ON REVERSE SIDE

Company Name: *MidAmerican Energy*

CONTROL EQUIPMENT DESCRIPTION AND SPECIFICATIONS

(1) Control Equipment (CE) Name and ID (if none, skip to (12)): *Baghouse CE170*

(2) Date of Installation: *TBD*

(3) Manufacturer: *TBD*

(4) Model: *TBD*

(5) Date of Modification (if any): *N/A*

(6) Is operating schedule different than emission unit(s) controlled?
☒ No ☐ Yes Specify the schedule:

(9) ID(s) of EU(s) Controlled: *170*

(7) Capture Hood Involved?
☒ No ☐ Yes

(8) Capture Hood Efficiency (if known): *N/A*

(10) Control Efficiency Documents (Must check one and provide documents as attachment as CS-10A):
☒ Manufacturer's design specifications and performance data/guarantee ☐ Stack testing report

Pollutant Controlled	*PM*	*PM_{10}*			
Control Efficiency %	*99+*	*90+*			

(11) If manufacturer's data is not available, use space below or attach a separate sheet (labeled CS-11A) to provide the Control equipment design specifications and performance data to support the above-mentioned control efficiency.

Control efficiencies for all equipment based on design specifications. Request for bids have not been submitted; as a result, equipment manufacturers have not been chosen.

STACK/VENT (EMISSION POINT) SPECIFICATIONS

(12) EP (Stack/Vent) ID: *170*

(13) Stack Opening Size (check one):
☒ circular, diameter (inches) is: *12*
☐ other, size (inches x inches) is:

(14) Height (ft) from the Ground: *12*

(15) Height (ft) from Highest Building Level: *NA*

(16) Distance (feet) from the Nearest Property Line: *1,614*

(17) Discharge Style (check one):
☒ V (Vertical, without rain cap or with unobstructing rain cap)
☐ VR (Vertical, with obstructing rain cap)
☐ D (Downward discharge; for example, a goose neck stack)
☐ H (Horizontal discharge)

EXHAUST INFORMATION

(18) Rated Flow Rate (☒ acfm ☐ scfm): *2,500*

(19) Moisture Content % (if known):

(20) Exit Temperature (°F): *Ambient*

APPENDIX A

EC Forms

FIGURE EU/EC-1: SCHEMATIC EMISSION UNIT DIAGRAM - COUNCIL BLUFFS ENERGY CENTER

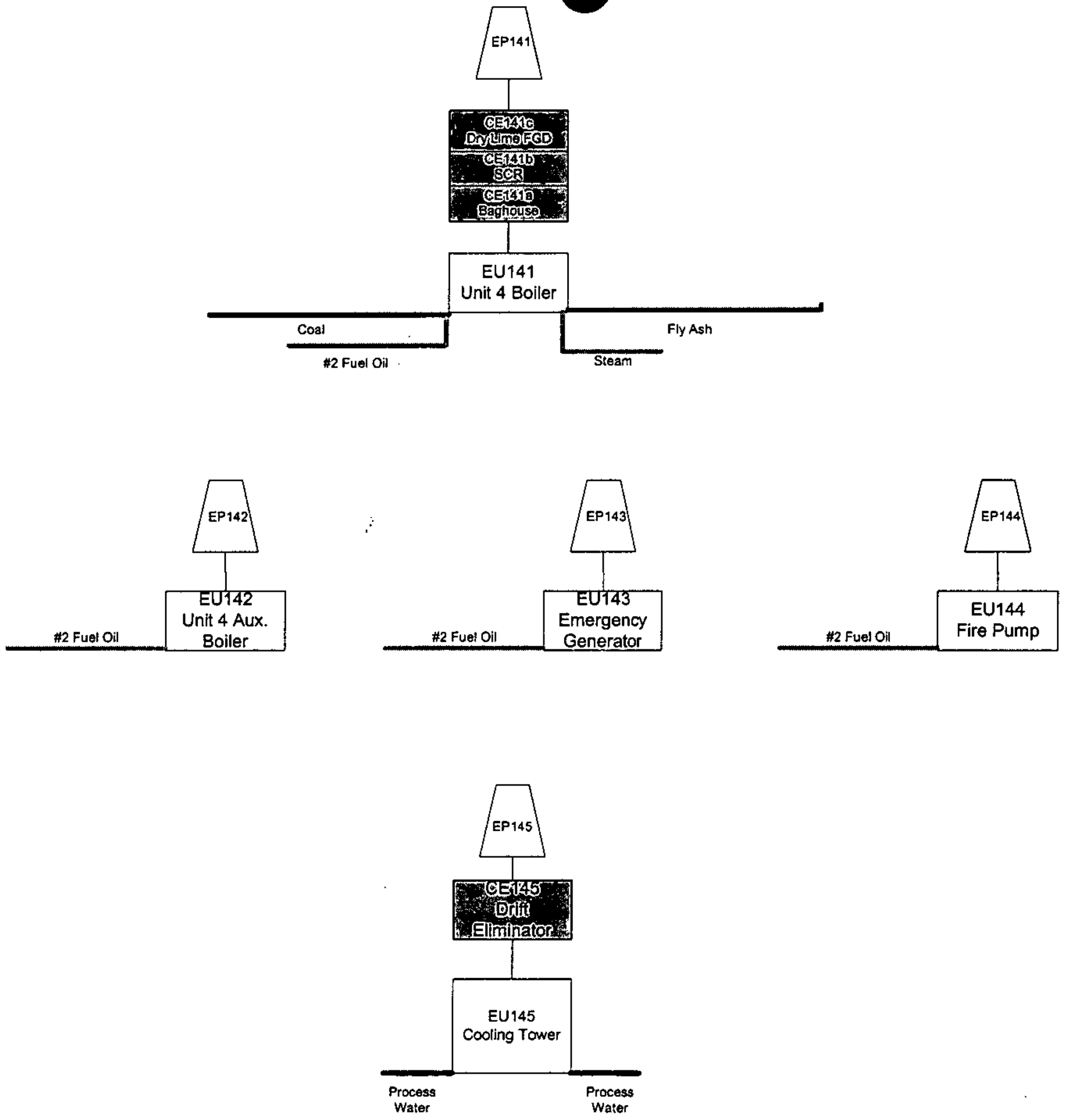
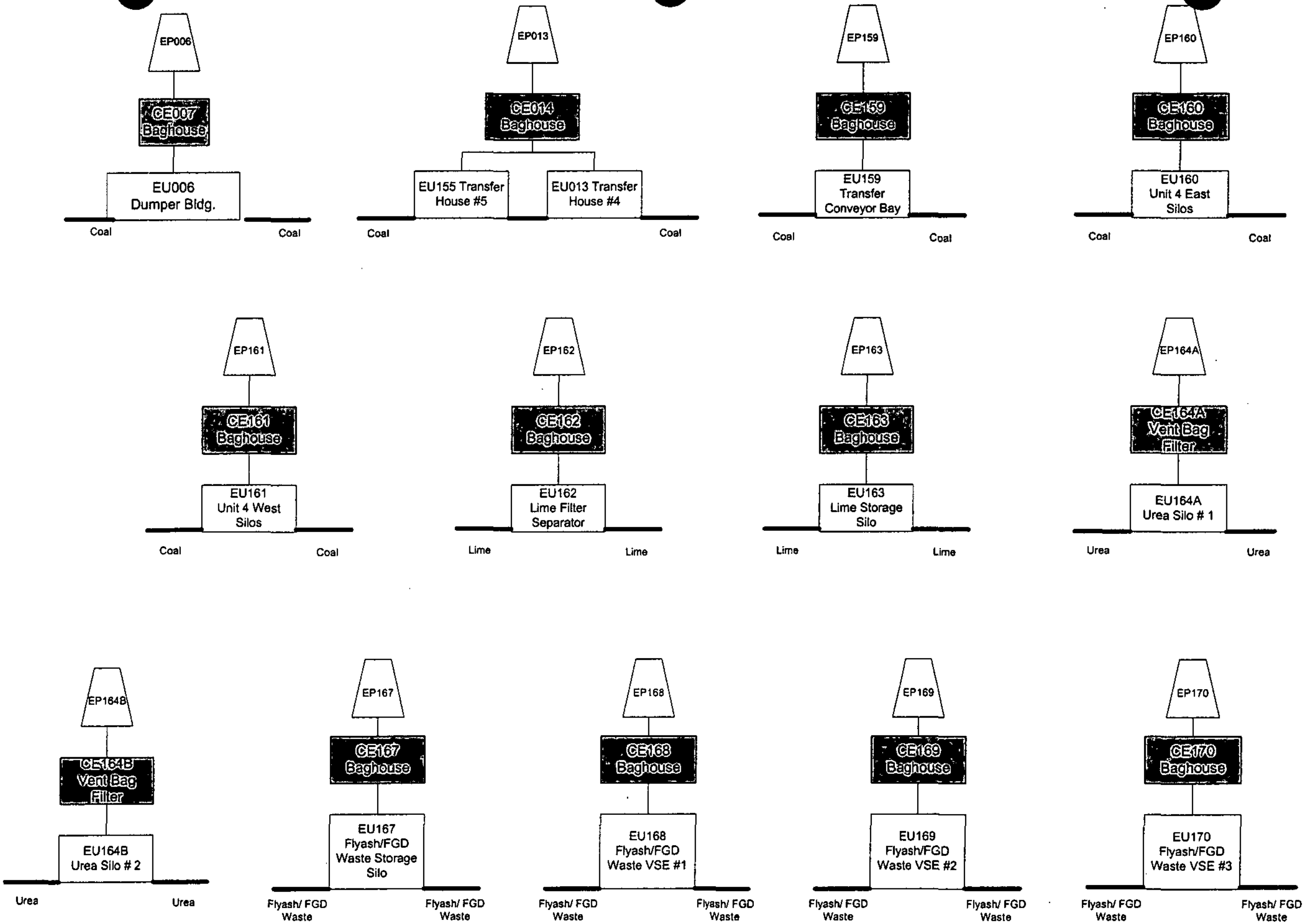


FIGURE EU/EC-1: SCHEMATIC EMISSION UNIT DIAGRAM - COUNCIL BLUFFS ENERGY CENTER



Form EC: Emission Calculations

AIR CONSTRUCTION PERMIT APPLICATION

Revision: 1/2001

SEE INSTRUCTIONS ON REVERSE SIDE

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-006

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to Figure EU/EC-1.

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
(5) Emissions (After control if applicable)	Concentration, Unit: *gr/dscf*	*0.01*	*0.009*							
	lbs/hr	*12.9*	*11.6*							
	tons/year	*56*	*51*							

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form EC:** **Emission Calculations**

Revision: 1/2001

SEE INSTRUCTIONS ON REVERSE SIDE

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-013

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to Figure EU/EC-1.

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations. Note emissions from EP-155 are included with calculations for this emission point.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

(5) Emissions (After control if applicable)	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
	Concentration, Unit: *gr/dscf*	*0.01*	*0.009*							
	lbs/hr	*2.3*	*2.1*							
	tons/year	*10.1*	*9.1*							

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form EC:** **Emission Calculations**

Revision: 1/2001

SEE INSTRUCTIONS ON REVERSE SIDE

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-141

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to Figure EU/EC-1.

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

(5) Emissions (After control if applicable)	Pollutant	PM [1]	PM_{10} [2]	SO_2	NOx	VOC	CO	Lead		
	Concentration, Unit:	0.02 lb/mmBTU	0.025 lb/mmBTU	0.12 lb/mm BTU	0.08 lb/mmBTU	0.06 lb/ton	0.154 lb/mmBTU	4.2E-4 lb/ton		
	lbs/hr	154	195	921	614	28.8	1,179	0.2		
	tons/year	672	854	4,034	2,689	126	5,166	0.88		

Notes:
(1) PM emission estimates are filterable portion only.
(2) PM_{10} emission estimates are combined filterable and condensable portions.

Form EC: Emission Calculations

AIR CONSTRUCTION PERMIT APPLICATION

Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-142

(3) Air Emissions Pathway Diagram (See Examples in the Instruction):

Refer to Figure EU/EC-1.

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
(5) Emissions (After control if applicable)	Concentration, Unit: *lbs/gal*		*0.0002*	*0.0071*	*0.02*	*0.00034*	*0.005*	*8.30 E-6*		
	lbs/hr		*2.0*	*7.1*	*20.1*	*0.34*	*5.0*	*0.008*		
	tons/year		*2.4*	*8.6*	*24*	*0.41*	*6.1*	*0.01*		

DNR **Form EC:** **Emission Calculations**

AIR CONSTRUCTION PERMIT APPLICATION

Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-143

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to Figure EU/EC-1.

(4) Emission Calculation. This calculation is based on (check all that apply):
☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:
☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

(5) Emissions (After control if applicable)	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
	Concentration, Unit: *lbs/hp-hr*		*7.0 E-4*	*4.05 E-4*	*2.4 E-02*	*6.42 E-04*	*5.5 E-03*			
	lbs/hr		*0.94*	*0.54*	*32.2*	*0.86*	*7.4*			
	tons/year		*0.24*	*0.14*	*8.0*	*0.22*	*1.8*			

Form EC: Emission Calculations

AIR CONSTRUCTION PERMIT APPLICATION

Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-144

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to Figure EU/EC-1.

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

(5) Emissions (After control if applicable)	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
	Concentration, Unit: *lbs/hp-hr*		*2.2 E-3*	*2.1 E-3*	*3.1 E-02*	*2.5 E-03*	*6.7 E-03*			
	lbs/hr		*0.55*	*0.53*	*7.8*	*0.63*	*1.7*			
	tons/year		*0.14*	*0.13*	*1.9*	*0.16*	*0.42*			

DNR **Form EC:** **Emission Calculations**

AIR CONSTRUCTION PERMIT APPLICATION

Revision: 1/2001

SEE INSTRUCTIONS ON REVERSE SIDE

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-145

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to Figure EU/EC-1.

(4) Emission Calculation. This calculation is based on (check all that apply):
☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:
☐ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

(5) Emissions (After control if applicable)	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
	Concentration, Unit:									
	lbs/hr	*6.4*	*1.3*							
	tons/year	*28*	*5.6*							

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form EC: Emission Calculations**

Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-159

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to Figure EU/EC-1.

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

(5) Emissions (After control if applicable)	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
	Concentration, Unit: *gr/dscf*	*0.01*	*0.009*							
	lbs/hr	*1.7*	*1.5*							
	tons/year	*7.3*	*6.6*							

AIR CONSTRUCTION PERMIT APPLICATION

Form EC: Emission Calculations

Revision: 1/2001

SEE INSTRUCTIONS ON REVERSE SIDE

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-160

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to Figure EU/EC-1.

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
(5) Emissions (After control if applicable)	Concentration, Unit: *gr/dscf*	*0.01*	*0.009*							
	lbs/hr	*3.0*	*2.7*							
	tons/year	*13.1*	*11.8*							

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form EC:** **Emission Calculations**

Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-161

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to Figure EU/EC-1.

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

(5) Emissions (After control if applicable)	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
	Concentration, Unit: *gr/dscf*	*0.01*	*0.009*							
	lbs/hr	*2.2*	*2.0*							
	tons/year	*9.8*	*8.8*							

(IDNR Form 542-3190-1)

Form EC: Emission Calculations

AIR CONSTRUCTION PERMIT APPLICATION

Revision: 1/2001

☞ SEE INSTRUCTIONS ON REVERSE SIDE ☞

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-162

(3) Air Emissions Pathway Diagram (See Examples in the Instruction):

Refer to Figure EU/EC-1.

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

(5) Emissions (After control if applicable)	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
	Concentration, Unit: *gr/dscf*	*0.01*	*0.009*							
	lbs/hr	*0.17*	*0.15*							
	tons/year	*0.75*	*0.68*							

(IDNR Form 542-3190-1)

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form EC:** **Emission Calculations**

Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-163

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to attached Figure EU/EC-1

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

(5) Emissions (After control if applicable)	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
	Concentration, Unit:	*0.02*	*0.018*							
	lbs/hr	*0.26*	*0.23*							
	tons/year	*1.1*	*1.0*							

AIR CONSTRUCTION PERMIT APPLICATION

Form EC: Emission Calculations

Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-164A

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to attached Figure EU/EC-1

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
(5) Emissions (After control if applicable)	Concentration, Unit: *gr/dscf*	*0.02*	*0.018*							
	lbs/hr	*0.09*	*0.08*							
	tons/year	*0.38*	*0.34*							

(IDNR Form 542-3190-1)

AIR CONSTRUCTION PERMIT APPLICATION

Form EC: Emission Calculations

Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-164B

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to attached Figure EU/EC-1

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

(5) Emissions (After control if applicable)	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
	Concentration, Unit: *gr/dscf*	*0.02*	*0.018*							
	lbs/hr	*0.09*	*0.08*							
	tons/year	*0.38*	*0.34*							

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form EC:** **Emission Calculations**

Revision: 1/2001

SEE INSTRUCTIONS ON REVERSE SIDE

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-167

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to attached Figure EU/EC-1

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

(5) Emissions (After control if applicable)	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
	Concentration, Unit: *gr/dscf*	*0.02*	*0.018*							
	lbs/hr	*0.52*	*0.46*							
	tons/year	*2.3*	*2.0*							

Form EC: Emission Calculations

AIR CONSTRUCTION PERMIT APPLICATION

Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-168

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to attached Figure EU/EC-1

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
(5) Emissions (After control if applicable)	Concentration, Unit: *gr/dscf*	*0.01*	*0.009*							
	lbs/hr	*0.21*	*0.19*							
	tons/year	*0.94*	*0.85*							

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form EC:** **Emission Calculations**

Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-169

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to attached Figure EU/EC-1

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

(5) Emissions (After control if applicable)	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
	Concentration, Unit: *gr/dscf*	*0.01*	*0.009*							
	lbs/hr	*0.21*	*0.19*							
	tons/year	*0.94*	*0.85*							

(IDNR Form 542-3190-1)

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form EC:** Emission Calculations

Revision: 1/2001

☛ SEE INSTRUCTIONS ON REVERSE SIDE ☛

(1) Company Name:
MidAmerican Energy

(2) Emission Point (Stack/Vent) Number:
EP-170

(3) Air Emissions Pathway Diagram
(See Examples in the Instruction):

Refer to attached Figure EU/EC-1

(4) Emission Calculation. This calculation is based on (check all that apply):

☒ Emission Factors ☐ Mass Balance ☐ Testing Data ☐ Other:

☒ Requested Limits (Note: A requested limit that is not based on emission factors, mass balance or stack testing data will need to be verified through initial compliance stack test.)

Refer to Appendix F of the application package for emission calculations.

SUMMARY OF EMISSIONS FROM THIS EMISSION POINT

	Pollutant	PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
(5) Emissions (After control if applicable)	Concentration, Unit: *gr/dscf*	0.01	0.009							
	lbs/hr	0.21	0.19							
	tons/year	0.94	0.85							

AIR CONSTRUCTION PERMIT APPLICATION

DNR **Form EI:** Plant Emission Inventory

Revision: 1/2001

SEE INSTRUCTIONS ON REVERSE SIDE

Company Name: *MidAmerican Energy*

PSD Classification: ☒ Major ☐ Minor ☐ Unknown

STACK/VENT EMISSIONS SUMMARY

(1) EP ID	(2) EU ID	(3) Source Description	(4) Construction Date	(5) Permit Number	(6) Potential or Permitted Emission Rate (tons/yr) PM	PM_{10}	SO_2	NOx	VOC	CO	Lead		
141	141	Unit 4 Boiler	TBD	NA	672(1)	854(2)	4,034	2,689	126	5,166	0.88		
142	142	Auxiliary Boiler	TBD	NA		2.4	8.6	24	0.41	6.1	0.01		
143	143	Emergency Diesel Generator	TBD	NA		0.24	0.14	8.0	0.22	1.8			
145	145	Cooling Tower	TBD	NA	28	5.6							
006	006	Rotary Car Dumper	1/1/1977	78-A-167	56	51							
013	013	Transfer House 4 (Crusher)	1/1/1977	78-A-173	10.1	9.1							
013	155	Transfer House 5	TBD	NA	Emissions included with EP-013. They share the same baghouse and stack.								
159	159	Transfer Conveyor Bay	TBD	NA	7.3	6.6							
160	160	Unit 4 East Silos	TBD	NA	13.1	11.8							
161	161	Unit 4 West Silos	TBD	NA	9.8	8.8							
162	162	Lime Filter Separator	TBD	NA	0.75	0.68							
163	163	Lime Silo	TBD	NA	1.1	1.0							
164A	164A	Urea Silo #1	TBD	NA	0.38	0.34							
164B	164B	Urea Silo #2	TBD	NA	0.38	0.34							
167	167	Flyash/ FGD Waste Silo	TBD	NA	2.3	2.0							
168	168	Flyash/ FGD Waste Vacuum System Exhauster # 1	TBD	NA	0.94	0.85							
169	169	Flyash/ FGD Waste Vacuum System Exhauster # 2	TBD	NA	0.94	0.85							

170	170	Flyash/ FGD Waste Vacuum System Exhauster # 3	TBD	NA	0.94	0.85							
(7) Total Stack Emissions					*804*	*956*	*4,043*	*2,721*	*127*	*5,174*	*0.89*		
FUGITIVE EMISSIONS SUMMARY													
(8) Source ID:													
F-4A/ 4B		Active Coal Storage Pile and maintenance (bulldozing)			11.6	2.6							
F-5A/ 5B		Inactive Coal Storage Pile and maintenance (bulldozing)			10.6	2.1							
F-151A		Transfer of coal from Conveyor 11 to Rail Unloading Stockout pile			7.7	3.6							
F-151B		Rail Unloading Coal Stockout pile wind erosion			0.19	0.1							
F-151C		Dumping of coal into emergency reclaim hopper			2.6	1.2							
F-904		Paved Ash Haul Road			22.4	4.4							
(9) Total Fugitive Emissions					*55*	*14*	*0*	*0*	*0*	*0*	*0*		
(10) Total Plant Emissions					*859*	*970*	*4,043*	*2,721*	*127*	*5,174*	*0.89*		

Notes:

(1) PM emission estimates are filterable portion only.

(2) PM_{10} emission estimates are combined filterable and condensable portions.

AIR CONSTRUCTION PERMIT APPLICATION

Form MI-2: Modeling Information (Emission Point Characteristics) Revision:

1/2001

☞ SEE INSTRUCTIONS ON REVERSE SIDE ☞

Company Name: *MidAmerican Energy*

TABLE 1. SUMMARY OF STACK/VENT EMISSION SOURCES

(1) Emission Point I.D. Number	(2) Stack Height (feet)	(3) Stack Size (inches)	(4) Exhaust Temperature (°F)	(5) Discharge Style	(6) Exhaust Flow Rate (acfm)	(7) Air Pollutant Emission Rate (lbs/hr) (Potential to emit or permitted emission rate)					
						PM_{10}	NOx	SO_2	CO	VOC	Lead
EP-141	550	295.8	165	V	2,660,982	195	614	921	1,179	28.8	0.2
EP-142	310	38.9	400	V	49,300	2.0	20.1	7.1	5.0	0.34	0.008
EP-143	20	10	1025	V	5,430	0.94	32.2	0.54	7.4	0.86	
EP-145	48	410/ cell	103	V	1,401,485/ cell	1.3					
EP-006	90	82	Ambient	V	150,000	11.6					
EP-013	50	39	Ambient	V	26,900	2.1					
EP-159	305	30	Ambient	V	19,500	1.5					
EP-160	305	40	Ambient	V	34,800	2.7					
EP-161	305	35	Ambient	V	26,100	2.0					
EP-162	12	10	Ambient	V	2,000	0.15					
EP-163	90	20	Ambient	V	1,500	0.23					
EP-164A	40	12	Ambient	V	500	0.08					
EP-164B	40	12	Ambient	V	500	0.08					

EP-167	*100*	*24*	*Ambient*	*V*	*3,000*	*0.46*					
EP-168	*12*	*12*	*Ambient*	*V*	*2,500*	*0.19*					
EP-169	*12*	*12*	*Ambient*	*V*	*2,500*	*0.19*					
EP-170	*12*	*12*	*Ambient*	*V*	*2,500*	*0.19*					

TABLE 2. SUMMARY OF FUGITIVE EMISSION SOURCES

(8) Source I.D. Number	(9) Source Description	(10) Dimensions (feet) (Length x Width x Height)	(11) Air Pollutant Emission Rate (lbs/hr) (Potential to emit or permitted emission rate)					
			PM_{10}	NOx	SO_2	CO	VOC	Lead
F-4A/ 4B	*Active Coal Storage Pile and maintenance*	*934 x 333 x 27*	*0.59*					
F-5A/ 5B	*Inactive Coal Storage Pile and maintenance*	*1,795 x 667 x 27*	*0.48*					
F-151A	*Transfer of coal from Conveyor 11 to Rail Unloading Stockout pile*	*39 x 39 x 75*	*0.83*					
F-151B	*Rail Unloading Coal Stockout pile wind erosion*	*168 x 168 x 50*	*0.02*					
F-151C	*Dumping of coal into emergency reclaim hopper*	*39 x 39 x 6*	*0.28*					
F-904	*Paved Ash Haul*	*5,484 x 50*	*1.7*					

AIR CONSTRUCTION PERMIT APPLICATION

Form 112(g): CASE-BY-CASE MACT **Revision: 1/2001**

☛ **SEE INSTRUCTIONS ON REVERSE SIDE** ☛

Company Name: *MidAmerican Energy*

1990 CAA Section112(g) APPLICABILITY DETERMINATION

(1) Does any emission unit in the proposed project emit a hazardous air pollutant (HAP)? (HAPs are chemical compounds as listed in the attached Table A) ☐ No (If No, stop here) ☒ Yes

(2) Do you propose a new project that was/is constructed or reconstructed **on or after June 29, 1998?**

☐ No (If No, stop here) ☒ Yes, the expected construction completion date is (mm/dd/yy): *TBD*

the anticipated start-up date is (mm/dd/yy): *TBD*

Note: **If your project does not fit the definition of "construction" or "reconstruction" in the instruction, stop here.**

(3) Is your facility one of the following? (Please call DNR at 515/281-8189 if you need help)

a. an electric utility steam generating unit ☐ No ☒ Yes

b. a research and development facility ☒ No ☐ Yes

c. a source that has been deleted from the 1990 CAA Section 112(c) ☒ No ☐ Yes

d. a source that is specifically regulated or exempted under 1990 CAA Sections 112(d), (h), (j) and incorporated in 40 CFR Part 63 ☒ No ☐ Yes

If "Yes" to one of these, stop here

HAP EMISSIONS SUMMARY

(4) EP ID	(5) EU ID	(6) Name of HAP Emitted	(7) CAS Number	(8) Potential to Emit (Tons/Year)	(9) Note
					See Appendix F for calculations and an estimate of HAP emissions.

(10) Does the **PROJECT** have the potential to emit:

a. 10 tons per year or more of any individual HAP? ☐ Yes ☐ No

b. 25 tons per year or more of any combination of HAPs? ☐ Yes ☐ No (If "No" to **both** a and b, stop here)

Note: **If your answer is "Yes" to one of the above, your project is subject to case-by-case MACT determination.**

IMPLEMENTATION OF SECTION 112(g) OF THE CLEAN AIR ACT

(11) Provide the proposed Maximum Achievable Control Technology (MACT) for the source:

a. Recommended emission limitation:

b. Selected control technology to meet the emission limitation:

Note: Support documentation for the proposed MACT must be submitted with the application. The documentation must include all alternative technologies considered to meet the emission limit and analyses of the cost of control, any non-air quality health and environmental impacts, and energy requirements associated with the expected emission reductions. The analyses must be emission unit specific. Technical information regarding the selected control must include information on the design, operation, and estimated control efficiency.

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4?		Explanation/ Comments	Methods Used to Demonstrate Compliance
			Yes	No		
567 – 20.1 through 20.3	Scope of Title, Definitions, Forms, Rules of Practice	20.1 – Scope of Title II – Air Quality. 20.2 – Definitions regarding Iowa Administrative Code (IAC) Chapters 20, 21, 22, 23, 24, 25, 26, 27, 28, and 29. 20.3 – Air quality forms generally and rules of practice for Iowa Code section 17A.3 and chapter 455B, division II.	✓		This is not an applicable standard or limitation; however, these definitions do apply when evaluating other applicable requirements within Title II – Air Quality.	Not applicable.
567 – 21.1 through 21.5	Compliance	21.1 – Compliance schedule: References 567 IAC Chapter 23. Also outlines the public availability of data and maintenance of records. 21.2 – Variances: How to apply, information required, processing and decisions. 21.3 – Emissions reduction program: Content, action and reports. 21.4 – Circumvention of Rules: "Can not reduce or conceal an emission which would otherwise constitute a violation of these rules." 21.5 – Evidence used in establishing that a violation has or is occurring: Outlines the credible evidence and methods used to establish if a violation has or is occurring.	✓		Establishes jurisdiction compliance obligation, emission reductions, circumvention and credible evidence requirements.	Not applicable.

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4?		Explanation/ Comments	Methods Used to Demonstrate Compliance
			Yes	No		
567 – 22.1	Permits required for new or existing stationary sources	22.1(1) – "Unless exempted in subrule 22.1(2) or to meet the parameters established in paragraph "c" of this subrule, no person shall construct, install or reconstruct or alter any equipment, control equipment or anaerobic lagoon without first obtaining a construction permit, or conditional permit, or permit pursuant to 22.8(455B), or permits required pursuant to 22.4(455B) and 22.5(455B) as required in this subrule. A permit shall be obtained prior to the initiation of construction, installation or alteration of any portion of the stationary source or anaerobic lagoon." 22.1(2) – Section 22.1 also contains criteria for exempting equipment from an air quality construction permit 22.1(3) – Information required to obtain a construction permit () (including MACT).	✓		An air quality construction permit must be obtained from the Iowa Department of Natural Resources (IDNR) prior to the initiation of construction of Unit 4. CBEC is not eligible to commence construction of Unit 4 prior to issuance of a PSD permit. CBEC is not eligible for any exemptions listed.	CBEC and IDNR records.
567 – 22.2(1) – 22.2(3)	Processing Permit Applications	Procedures are outlined for the IDNR review and action on construction permit applications, including incomplete applications and public notice and participation and final notice.	✓		Public notice must be published by IDNR in a local newspaper 30 days prior to issuing a permit.	None. IDNR Responsibility.
567 – 22.3(1)	Issuing Permits – Stationary Sources Other than Anaerobic Lagoons	Describes the criteria for issuing construction permits for stationary sources other than lagoons.	✓		Regulations pertain to the criteria and protocol used by the IDNR for taking various actions with regard to application and issued permits.	Agency Files.

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4? Yes	No	Explanation/ Comments	Methods Used to Demonstrate Compliance
567 – 22.3(2)	Issuing Permits – Anaerobic Lagoons	Describes the criteria for issuing construction permits for anaerobic lagoons.		✓	CBEC will not be installing an anaerobic lagoon.	Agency Files.
567 – 22.3(3)	Issuing Permits – Conditions of Approval	"A permit may be issued subject to conditions which shall be specified in writing. Such conditions may include but are not limited to emission limits, operating conditions, fuel specifications compliance testing, continuous monitoring, and excess emission reporting."	✓		Regulations pertain to the criteria and protocol used by the IDNR for taking various actions with regard to application and issued permits.	Agency Files.
567 – 22.3(4)	Issuing Permits – Denial of a Permit	If a permit is denied, the applicant will be issued a written notice listing the reasons for denial. IDNR can deny an application based upon the applicant's failure to provide a signed statement of the applicant's legal entitlement to install and operate equipment.	✓		Regulations pertain to the criteria and protocol used by the IDNR for taking various actions with regard to application and issued permits.	Agency Files.
567 – 22.3(5)	Issuing Permits – Modification of a Permit	"The director may, after public notice of such decision, modify a condition of approval of an existing permit for a major stationary source or an emission limit contained in an existing permit for a major stationary source if necessary to attain or maintain an ambient air quality standard."	✓		Regulations pertain to the criteria and protocol used by the IDNR for taking various actions with regard to application and issued permits.	Agency Files.
567 – 22.3(6)	Issuing Permits – Limits on Hazardous Air Pollutants	DNR may limit a source's Hazardous Air Pollutant (HAP) Potential to Emit (PTE) to establish federally enforceable emission limits on the source.	✓		Regulations pertain to the criteria and protocol used by the IDNR for taking various actions with regard to application and issued permits.	Agency Files.

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4?		Explanation/ Comments	Methods Used to Demonstrate Compliance
			Yes	No		
567 – 22.3(7)	Issuing Permits – Revocation of a permit	IDNR can revoke a permit if owner has lost legal entitlement to the equipment or if the owner requests a revocation for future operations.	✓		Regulations pertain to the criteria and protocol used by the IDNR for taking various actions with regard to application and issued permits.	Agency Files.
567 – 22.3(8)	Issuing Permits – Ownership change of permitted equipment	If a change in ownership occurs, the IDNR shall be notified within 30 days, specifying the information requested in this section.	✓		Regulations pertain to the criteria and protocol used by the IDNR for taking various actions with regard to application and issued permits.	Agency Files.
567 – 22.4	Special requirements for major stationary sources located in areas designated attainment or unclassified (PSD)	22.4(1) – This section adopts the Federal PSD regulations (40 CFR Subsection 52.21), with the exception of 40 CFR 52.21 (a), 52.21(q), 52.21(s) and 52.21(u). 22.4(2) – Clarifies definitions in specific sections of 40 CFR 52.21. 22.4(3) – Clarifies definitions in specific sections of 40 CFR 52.116(q). 22.4(4) – Establishes the ambient air impact significance levels for SO2, PM10, NO2 and CO.	✓		CBEC is located in an area designated as attainment with all NAAQS; therefore this rule does apply.	Obtain a PSD permit for Unit 4.

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4?		Explanation/ Comments	Methods Used to Demonstrate Compliance
			Yes	No		
567 – 22.5	Special requirements for non-attainment areas	22.5 (1) – Outlines the requirements for nonattainment areas including definitions. 22.5(2) – Applicability. 22.5(3) – Emission offsets. 22.5(4) – Acceptable emission offsets. 22.5(5) – Banking of offsets in nonattainment areas. 22.5(6) – Control technology review. 22.5(7) – Compliance of existing sources. 22.5(8) – Alternate site analysis. 22.5(9) – Additional conditions for permit approval 22.5(10) – Public availability of information.		✓	CBEC is located in an area designated as attainment with all NAAQS; therefore this rule does not apply.	
567 – 22.6	Nonattainment area designations	States that Iowa's nonattainment areas are listed under 40 CFR Part 81.316.		✓	CBEC is located in an area designated as attainment with all NAAQS; therefore this rule does not apply.	
567 – 22.7	Alternative Emission Control Program	Only applicable to sources "located in an area with attainment or unclassified status (as published at 40 CFR 81.316, amended 3/19/98) or located in an area with an approved State Implementation Plan (SIP) demonstrating attainment by the statutory deadline may apply for an alternative set of emission limits..."	✓		This alternative program is available to CBEC.	

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4?		Explanation/ Comments	Methods Used to Demonstrate Compliance
			Yes	No		
567 – 22.8	Permit by rule	Applicable to spray booths that spray less than 3 gallons of sprayed material per day.		✓	If CBEC has a paint booth during construction of unit 4, emissions are likely to be greater than 3 gallons per day, but will likely be exempt because painting would occur during construction.	
567 – 22.9 through 22.99	Reserved			✓	Reserved for later use by IDNR.	

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4? Yes	Applicable to Unit 4? No	Explanation/ Comments	Methods Used to Demonstrate Compliance
567 – 22.100 through 22.116	Title V Operating Permits	22.100 – Definitions For Title V Operating Permits 22.101 – Applicability Of Title V Operating Permit 22.102 – Source Categories Exempt from Obtaining Title V Operating Permit 22.103 – Insignificant Activities 22.104 – Requirement to Have A Title V Permit 22.105 – Title V Permit Applications 22.106 – Title V Permit Fees 22.107 – Title V Permit Processing Procedures 22.108 – Permit Content 22.109 – General Permits 22.110 – Changes Allowed without a Title V Permit Revision 22.111 – Administrative Amendments to Title V Permits 22.112 – Minor Title V Permit Modifications 22.113 – Significant Title V Permit Modifications 22.114 – Title V Permit Reopenings 22.115 – Suspension, Terminations and Revocation of Title V Permits 22.116 – Title V Permit Renewals	✓		CBEC is required to obtain a Title V Operating Permit. The source is subject to Title IV of the Clean Air Act and is considered a major source, emitting over 100 TPY of a regulated pollutant and over 10 TPY of a single HAP and 25 TPY of combined HAPs. Unit 4 will require an amendment to the existing CBEC Title V Operating permit.	CBEC has a Title V Permit for the existing facility and will apply for a permit modification within one year of beginning operation of Unit 4.
567 – 22.117 through 22.119	Reserved			✓	Reserved for later use by IDNR.	

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4? Yes	Applicable to Unit 4? No	Explanation/ Comments	Methods Used to Demonstrate Compliance
567 – 22.120 through 22.148	Acid Rain	22.120 – Acid Rain Program – Definitions 22.121 – Measurements, abbreviations, and acronyms 22.122 – Applicability 22.123 – Acid Rain Exemptions 22.124 – Reserved 22.125 – Standard requirements 22.126 – Designated representative – submissions 22.127 – Designated representative – objections 22.128 – Acid Rain applications – requirement to apply 22.129 – Information requirements for acid rain permit applications 22.130 – Acid rain permit application shield and binding effect of permit application 22.131 – Acid rain compliance plan and compliance options – general 22.132 – Reserved 22.133 – Acid rain permit contents – general 22.134 – Acid rain permit shield 22.135 – Acid rain permit issuance procedures – general 22.136 – Acid rain permit issuance procedures – completeness 22.137 – Acid rain permit issuance procedures – statement of basis 22.138 – Issuance of acid rain permits 22.139 – Acid rain permit appeal procedures 22.140 – Permit revisions – general 22.141 – Permit Modifications 22.142 – Fast Track Modifications (Not Applicable) 22.143 – Administrative Permit Amendment	✓		Pursuant to 567 – 22.122(1)(c)(1), Unit 4 is a new utility unit; therefore, these rules do apply unless otherwise indicated.	Refer to Table X-1 for Federal Regulation Requirements.

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4?		Explanation/ Comments	Methods Used to Demonstrate Compliance
			Yes	No		
567 – 22.120 through 148	Acid Rain	22.144 – Automatic Permit Amendment 22.145 – Permit Reopenings 22.146 – Compliance Certification – Annual Report 22.147 – Reserved 22.148 – Sulfur dioxide opt-ins (Not Applicable)	✓		Pursuant to 567 – 22.122(1)(c)(1), Unit 4 is a new utility unit; therefore, these rules do apply unless otherwise indicated.	Refer to Table X-1 for Federal Regulation Requirements.
567 – 22.149 through 22.199	Reserved			✓	Reserved for later use by IDNR.	
567 – 22.200 through 22.208	Voluntary Operating Permits	22.200 – Voluntary Operating Permits 22.201 – Eligibility for Voluntary Operating Permits 22.202 – Requirement to have a Title V Operating Permit 22.203 – Voluntary Operating Permit Applications 22.204 – Voluntary Operating Permit Fees 22.205 – Voluntary Operating Permit Processing Procedures 22.206 – Permit content 22.207 – Relation to Construction Permits 22.208 – Suspension, Termination, and Revocation of Voluntary Operating Permits		✓	Available only to sources with PTE and actual emissions below the 100 TPY for criteria pollutants and below 10/25 TPY for HAPs.	
567 – 22.209 to 22.299	Reserved			✓	Reserved for later use by IDNR	
567 – 22.300 (1) to (11)	Operating Permit by Rule for Small Sources	This rule applies to sources who choose to operate under a "permit by rule" operating permit by taking stringent permit limits. This regulation applies to small sources only.		✓	Not applicable to CBEC because they are subject to Title V requirements under 567 IAC 22.100 through 22.116.	

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4?		Explanation/ Comments	Methods Used to Demonstrate Compliance
			Yes	No		
567 – 23.1(1)	Emissions Standards – In general	Adoption of the federal standards into IAC.	✓		CBEC is subject to federal standards defined in Chapter 23.	No requirements mentioned in this section.
567 – 23.1(2)	Emissions Standards – New Source Performance Standards (NSPS)	23.1(2) NSPS – Only the NSPS applicable to CBEC are listed here: 23.1(2) v – Coal Preparation Plants (40 CFR 60 Subpart Y) 23.1(2) z – Electric Utility Steam Generating Units (40 CFR 60 Subpart Da)	✓		Unit 4 meets the criteria listed under 40 CFR 60 Subparts Y and Da and must meet the requirements of these subparts.	No requirements mentioned in this section, refer to referenced federal standard.
567 – 23.1(3)	Emissions Standards – Emission Standards for Hazardous Air Pollutants (NESHAP)	23.1(3) – NESHAP – Only the applicable NESHAPs are listed: 23.1(3) a – Asbestos (40 CFR 61 Subpart M)	✓		Likely to be applicable to CBEC since the installation of asbestos containing materials and thermal system installation was common place prior to the late 1970's. CBEC was in operation prior to that time.	No requirements mentioned in this section, refer to referenced federal standard.
567 – 23.1(4)	Emission Standards – Emission Standards for hazardous Air Pollutants for Source Categories	23.1(4)(b)(1) and (2) – Requirements for control technology determinations for major sources in accordance with Clear Air Act Sections 112(g) and 112 (j). 23.1(4)(b)(1) – New HAP sources must apply maximum achievable control technology. 23.1(4)(b)(2) – New HAP sources must apply for a Title V Permit or Modification	✓		Unit 4 meets these criteria, therefore control equipment design will meet applicable MACT standards and an application for modification of their Title V will be made.	

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4? Yes	Applicable to Unit 4? No	Explanation/ Comments	Methods Used to Demonstrate Compliance
567 – 23.1(4)	Emission Standards – Emission Standards for Hazardous Air Pollutants for Source Categories	23.1(4)(q) – Emission Standards for hazardous air pollutants for industrial process cooling towers. Applicable to cooling towers that use chromium-based water treatment chemicals on or after 9/8/94.		✓	Cooling towers at CBEC will not use chromium-based chemicals, and therefore this NESHAP is not applicable	
567 – 23.1(5)	Emission Standards – Emission Guidelines	23.1(5)(a) – Emission Guidelines for Municipal Solid Waste Landfills		✓		

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4?		Explanation/ Comments	Methods Used to Demonstrate Compliance
			Yes	No		
567 – 23.1(6)	Emission Standards – Calculation of Emission Limitations based on Stack Height	a. Good Engineering Practice (GEP) stack height means the greater of: 1) 65 meters measured from the base of the stack 2) GEP = Height of nearby structures + 1.5 Lesser Dimension, height or projected width of nearby structures 3) Height demonstrated by a fluid model, which ensures that excessive concentrations of emissions do not result b. The degree of emission limitation required for control of any air contaminant under this chapter shall not be affected in any manner by: 1) Consideration of the portion of the stack which exceeds GEP stack height 2) Varying the emission rate of a pollutant according to atmospheric conditions or ambient concentrations 3) Increasing final exhaust gas plume rise by manipulating source process parameters, exhaust gas parameters, stack parameters, or combined exhaust gases from several existing stack into one stack or other selective handling of exhaust gas streams so as to increase gas plume rise.	✓			

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4?		Explanation/ Comments	Methods Used to Demonstrate Compliance
			Yes	No		
567 – 23.2	Open Burning	23.2(1) – Open burning of combustible materials is prohibited, except as provided in 23.2(2) and 23.2(3). 23.2(2) – Variances from rule. Any person wishing to conduct open burning of material not exempted in 23.2(2) may make application for a variance 23.2(3) – Exemptions: Permitted unless prohibited by local ordinances: a) Disaster rubbish b) Tree and tree trimmings c) Flare Stacks d) Landscape Waste e) Recreational Fires f) Residential Waste g) Training Fires h) Paper or plastic pesticide containers and seed corn bags i) Agricultural structures	✓		CBEC may need to open burn at the site for fire training purposes or from clearing and grubbing.	
567 – 23.3	Specific Contaminants	23.3(1) – General. Discusses applicability of emission standards. 23.3(2) – Particulate Matter. 23.3(3) – Sulfur Compounds.		✓	Pursuant to 23.3(1) that standards in this section do not apply, since the processes involved are subject o standards (e.g. NSPS and NESHAPs) prescribed elsewhere in Chapter 23 (e.g. 23.1).	

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4?		Explanation/ Comments	Methods Used to Demonstrate Compliance
			Yes	No		
567 – 23.4	Specific Processes	23.4(1) – General. The provisions of this rule shall not apply to those facilities for which performance standards are specified in 23.1(2).		✓	Unit 4 is subject to the performance standards specified in 23.1(2). Also, none of the specific processes identified in this rule exist at CBEC.	
567 – 23.5	Anaerobic lagoons	Applicable to anaerobic lagoons at animal feeding operations.		✓	Not applicable.	
567 – 23.6	Alternative emission limits (the bubble concept)	Emission limits for certain individual emission points included in 23.3 and 23.4 that must meet specific criteria.		✓	Not applicable to Unit 4 due to the NSPS and PSD requirements. Also Unit 4 is not one of the emission points included in 23.3 or 24.4.	

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4? Yes	Applicable to Unit 4? No	Explanation/ Comments	Methods Used to Demonstrate Compliance
567 – 24.1	Excess Emissions – Excess Emission Reporting	24.1(1) – Excess emissions during period of startup, shut down, or cleaning of control equipment. When these criteria are met, it is not considered excess as long as the activity is completed expeditiously and in a manner consistent with good practice for minimizing emissions. Cleaning of control equipment is not considered an excess emission if it is limited to one six-minute period per one-hour period. 24.1(2) – Oral report of excess emissions. Excess emissions other than those occurring during startup, shutdown or cleaning are required to be reported to the IDNR within 8 hours or at the start of the first working day following the onset of the incident. 24.1(3) – Written report of excess emission. A written report of an incident of excess emissions shall be submitted as a follow-up to all required oral reports to the IDNR within 7 days of the onset of the upset condition. 24.1(4) – Excess emissions. Excess emissions occurring during times other than startup, shutdown or cleaning is a violation. Specific guidelines are applicable to electric utilities.	✓		Applicable when excess emissions occur, except during periods of startup, shutdown, or cleaning of control equipment.	CEMS and maintenance records. Records of oral and written reports will be kept on file at CBEC for a minimum of 3 years.

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4?		Explanation/ Comments	Methods Used to Demonstrate Compliance
			Yes	No		
567 – 24.2	Excess Emissions – Maintenance and Repair Requirements.	24.2(1) – Maintenance and repair. Owner or operator of any equipment or control equipment shall maintain the equipment or control equipment to minimize emissions, remedy excess emissions in a timely manner, minimize the amount and duration of excess emissions, implement measures contained in a contingency plan, if applicable, and schedule routine maintenance of equipment or control equipment during periods of shutdown. 24.2(2) – Maintenance plans. A maintenance plan may be required by IDNR if excess emissions are repeatedly occurring from the equipment or control equipment.	✓		CBEC is required to maintain equipment and control equipment.	Maintenance records.
567 – 25.1(1)	Measurement of Emissions – Continuous monitoring of opacity from coal-fired steam generating units	"The owner or operator of any coal-fired or coal gas fired steam generating unit with a rated capacity of greater than 250 million BTUs per hour heat input shall install, calibrate, maintain and operate continuous monitoring equipment to monitor opacity."	✓		CBEC must install on Unit 4 COMS, follow record keeping and reporting requirements.	Installation of COMS equipment, proper record keeping and reporting of opacity. All COMS installation, operation and maintenance records will be maintained at CBEC for a minimum of 3 years (per 40 CFR Part 75 requirements).
567 – 25.1(2) through (3)	Reserved			✓	Reserved for later use by IDNR.	

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4?		Explanation/ Comments	Methods Used to Demonstrate Compliance
			Yes	No		
567 – 25.1(4)	Measurement of Emissions – Continuous monitoring of sulfur dioxide from sulfuric acid plants	Not applicable, CBEC is not a sulfuric acid plant.		✓		
567 – 25.1(5)	Measurement of Emissions – Maintenance records of continuous monitors	Owner or operator must maintain for a minimum of two years a file of all information pertinent to each monitoring system present at the facility.	✓		CBEC must install on Unit 4 COMS, follow record keeping and reporting requirements.	Installation of COMS equipment, proper record keeping and reporting of opacity. All COMS installation, operation and maintenance records will be maintained at CBEC for a minimum of 3 years (per 40 CFR Part 75 requirements).
567 – 25.1(6)	Measurement of Emissions – Reporting of continuous monitoring information	Owner or operator must file quarterly reports to the director of IDNR, no later than 30 days after the end of the calendar quarter.	✓		CBEC must install on Unit 4 COMS, follow record keeping and reporting requirements.	Installation of COMS equipment, proper record keeping and reporting of opacity. All COMS installation, operation and maintenance records will be maintained at CBEC for a minimum of 3 years (per 40 CFR Part 75 requirements).

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4? Yes	Applicable to Unit 4? No	Explanation/ Comments	Methods Used to Demonstrate Compliance
567 – 25.1(7)	Measurement of Emissions – Tests by Owner	Owner shall conduct emission test to determine compliance with applicable rules in accordance with these requirements. 25.1(7) a – General. Owner must notify IDNR in writing within 30 days of a performance evaluation in order for the results to be considered valid. A pretest meeting shall be held no later than 15 days prior to the evaluation may be waived if a written protocol is submitted. IDNR is allowed to observe tests. Results must be submitted within 6 weeks of completion of the testing. 25.1(7) b – New Equipment. Unless otherwise specified by the IDNR, all new equipment must be tested. Must be completed within 60 day of achieving maximum production but no later than 180 days after startup, unless a shorter timeframe is specified in the permit. 25.1(7) c – Existing Equipment. Not applicable.	✓		CBEC will be required to perform emission testing.	Records that protocol was followed as outlined in IAC.
567 – 25.1(8)	Measurement of Emissions – Tests by Department	IDNR has the right to conduct independent emission test and continuous monitor performance tests of an installation at the expense of the state.	✓		May be used at IDNR's discretion.	None. IDNR's responsibility.
567 – 25.1(9)	Measurement of Emissions – Methods and procedures	Incorporation of the Federal methods and procedures for stack sampling and associated analytical methods.	✓		CBEC is required to emission test using specified methods.	

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4?		Explanation/ Comments	Methods Used to Demonstrate Compliance
			Yes	No		
567 – 25.1(10)	Measurement of Emissions – Exemptions from Continuous Monitoring Requirements	Exemptions include: 24.1(10) a – Affected source is subject to a NSPS promulgated in 40 CFR Part 60 as amended through 11/24/98. 24.1(10) b – An affected steam generator had an annual capacity factor for calendar year 1974, as reported to the FPC, of less than 30% or the projected use of the unit indicated the annual capacity factor will not be increased above 30% in the future. 24.1(10) c – An affected steam generator is scheduled to be retired from service within 5 years of the date these rules become effective. 24.1(10) d – Rescinded. 24.1(10) e – IDNR may provide an temporary exemption if it is during a period of equipment malfunction, and if the malfunction was unavoidable and is being repaired.	✓		Applicable if CBEC meets these criteria.	
567 – 25.1(11)	Measurement of Emissions – Extensions	Owner may request an extension of time provided for installation of the monitor by demonstrating good faith efforts had been made to install the monitor in the prescribed time.	✓		Applicable to CBEC if necessary.	

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4?		Explanation/ Comments	Methods Used to Demonstrate Compliance
			Yes	No		
567 – 25.1(12)	Measurement of Emissions – Continuous monitoring of sulfur dioxide from emission points involved in an alternative emission control program	Applicable to facilities that are applying for an alternative emission control program.		✓	CBEC is not applying for an alterative emission control program at this time.	
567- 25.2	Continuous Emission Reporting under the Acid Rain Program	The continuous emission monitoring requirements for affected units under the acid rain program as provided in 40 CFR 75 are adopted by reference.	✓		CBEC is subject to the Federal Acid Rain Program.	

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4? Yes	Applicable to Unit 4? No	Explanation/ Comments	Methods Used to Demonstrate Compliance
567- 26.1 through 26.4	Prevention of Emergency Episodes	26.1 – General. The provisions of this chapter are designed to prevent the excessive buildup of air contaminants during air pollution episodes, thereby preventing the occurrence of an emergency due to the effect of these contaminants on the health of persons. 26.2 – Episode Criteria. Discusses the conditions that would constitute an air pollution alert, warning or emergency. 26.3 – Preplanned abatement strategies. Requires that coal or oil fired electric power generating facility prepare an abatement strategy. 26.4 – Actions taken during episodes.	✓		CBEC is a coal-fired electric power generating facility and therefore is required to have an abatement strategy. Otherwise, this chapter identifies action to be taken by IDNR, not CBEC. CBEC already has an abatement strategy; it will need to be revised to include Unit 4, prior to commencement of operations.	Records maintained at CBEC.
567 – 27.1 through 27.5	Certificate of Acceptance	Applicable to political subdivisions that seek their own air pollution control program.		✓	CBEC does not qualify as a political subdivision.	
567 – 28.1	Ambient Air Quality Standards	28.1 – Statewide Standards. "The state of Iowa ambient air quality standards shall be the National Primary and Secondary Ambient Air Quality Standards as published in 40 CFR Part 50."	✓		The addition of Unit 4 is subject to the NAAQS.	Modeling associated with obtaining an approved PSD/construction permit from IDNR.

TABLE B-1
Council Bluffs Energy Center Unit 4
Iowa Administrative Code Review

Citation	Description	Requirement/Standard	Applicable to Unit 4?		Explanation/ Comments	Methods Used to Demonstrate Compliance
			Yes	No		
567 – 29.1	Qualification in Visual Determination of the Opacity of Emissions – Methodology and qualified observer	The federal method for visual determination of opacity of emissions and requirements for qualified observers as defined in Method 9, 40 CFR Part 60 Appendix A as amended through March 12, 1996 is adopted by reference. To qualify as an observer a candidate must, after meeting the requirements of 40 CFR Part 60 Appendix A have on record with IDNR a minimum of 250 readings of black at white plumes taken at approved smoke reading courses.		✓	Not required by IAC to have an employee certified at the facility.	
567 – 30	Reserved			✓	Reserved for later use by IDNR.	
567 – 31.1 through 31.2	Nonattainment Areas	Applies to sources that are located in nonattainment areas.		✓	CBEC is not located in a nonattainment area.	

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
Federal Requirements					
40 CFR 50, National Primary and Secondary Ambient Air Quality Standards					
40 CFR 50	This part sets forth national primary and secondary ambient air quality standards.		✓	These guidelines apply to the EPA; therefore, do not apply to CBEC.	
40 CFR 51, Requirements For Preparation, Adoption, and Submittal of Implementation Plans					
40 CFR 51	This part outlines requirements for SIP.		✓	These guidelines apply to States and are not requirements of CBEC; however, definitions may apply when evaluating other applicable requirements.	
40 CFR 52, Approval and Promulgation of Implementation Plans					
40 CFR 52	This part sets forth the Administrator's approval and disapproval of State plans and the Administrator's promulgation of such plans or portions thereof.		✓	This section is administrative and has no requirements pertaining to CBEC Unit 4.	
40 CFR 53, Ambient Air Monitoring Reference and Equivalent Methods					
40 CFR 53	This part guidelines monitoring reference and equivalent methods.		✓	Requirements in this section apply to States; therefore, do not apply to CBEC.	
40 CFR 54, Prior Notice of Citizen Suits					
40 CFR 54	Guidelines for citizens to file suits.		✓	Requirements apply to citizens; therefore, do not apply to CBEC.	
40 CFR 55, Outer Continental Shelf Air Regulations					
40 CFR 55	Guidelines and requirements for facilities on the outer continental shelf.		✓	CBEC is not located on the outer continental shelf; therefore, these rules do not apply.	
40 CFR 56, Regional Consistency					

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 56	This part applies to EPA employees.		✓	CBEC is not an EPA employee; therefore, these rules do not apply.	
40 CFR 57, Primary Nonferrous Smelter Orders					
40 CFR 57	Guidelines and requirements for smelters.		✓	CBEC does not operate a smelter; therefore, these rules do not apply.	
40 CFR 58, Ambient Air Quality Surveillance					
40 CFR 58	This part sets guidelines and requirements for PSD monitoring stations and air pollution control agencies.		✓	CBEC does not operate a PSD monitoring station nor is it an air pollution control agency; therefore, these rules do not apply.	
40 CFR 59, National VOC Emission Standards for Consumer and Commercial Products					
40 CFR 59	This part sets guidelines and requirements for consumer and commercial products.		✓	CBEC does not manufacture consumer or commercial products; therefore, these rules do not apply.	
40 CFR 60, Subpart A, General Provisions for Standards of Performance for New Sources					
40 CFR 60.1 – 60.4	Specifies applicability, definitions, units and abbreviations, and communication guidelines of 40 CFR 60.	✓		This is not an applicable standard or limitation; however, these definitions do apply when evaluating other applicable requirements within 40 CFR 60.	
40 CFR 60.5 – 60.6	Administrator determination of construction or modification.		✓	This section applies to the EPA; therefore, it does not apply to CBEC.	

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 60.7(a)	Notification, reporting and recordkeeping requirements for the affected units and the CEMS.	✓		Notification must be sent to the Iowa Department of Natural Resources (IDNR) of: the date construction is commenced (no more than 30 days after), the date of initial start up (no more than 15 days after), physical or operational changes that may increase emission rates (no less than 60 days before), the demonstration of the continuous monitoring system performance (no less than 30 days before), the date for conducting opacity observations (no less than 30 days before), continuous opacity monitoring system data results will be used to determine compliance with the opacity standard in lieu of Method 9 (no less than 30 days before).	Send required information to IDNR. Maintain copies on file.
40 CFR 60.7(b)	Owners or operators shall maintain records of the occurrence and duration of any startup, shutdown, or malfunction in the operation of an affected facility; any malfunction of the air pollution control equipment; or any periods during which a continuous monitoring system or monitoring device is inoperative.	✓		CBEC is subject to NSPS and; therefore, to this requirement.	Records of these occurrences and subsequent agency notifications will be maintained on file.

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4?		Comments	Methods Used to Demonstrate Compliance[1]
		Yes	No		
40 CFR 60.7(c) & (d)	Owners or operators required to install a continuous monitoring device shall submit excess emissions and monitoring systems performance report and/or summary report form semiannually.	✓		Written reports shall include magnitude of excess emissions, conversion factors used, date and time of commencement process operating time, specific identification of each period of excess emissions, nature and cause of any malfunction, corrective action, dates and times when the continuous monitoring system was inoperative, or statement of no excess emissions. Reports will be sent within 30 days of the end of the 6-month period. Also see 40 CFR Part 75.	Reports shall be completed and sent to IDNR via certified mail. Copies shall be maintained.
40 CFR 60.7(e)	Adjusts more frequent reporting requirements to the requirements above if the facility meets certain conditions.		✓	This can only be accomplished after a minimum of 12 months of monitoring; therefore this rule does not apply to CBEC Unit 4 at this time.	
40 CFR 60.7(f) – (h)	Owners or operators shall maintain a file of all measurements; continuous monitoring system performance evaluations, calibration checks, adjustments and maintenance in permanent form suitable for inspection.	✓		Files shall be retained for at least 2 years. Note: 40 CFR Part 75 requires a minimum of 3 years retention.	Files shall be retained for at least 3 years.
40 CFR 60.8	Within 60 days after achieving the maximum production rate, but not later than 180 days after initial startup and at such other times as may be required by the Administrator, the owner or operator shall conduct performance test(s) and furnish the Administrator a written report of the results of such performance test(s).	✓		Performance tests shall be conducted and data reduced in accordance with the test methods and procedures contained in each applicable subpart or as the Administrator shall specify. Notice should be sent to the Administrator at least 30 days prior. Adequate performing testing facilities will be provided. Each test will consist of 3 runs unless otherwise specified.	Copies of agency notifications and testing reports will be maintained on site.

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4?		Comments	Methods Used to Demonstrate Compliance[1]
		Yes	No		
40 CFR 60.9	Availability of information to the public regarding this source and permit.		✓	This requirement is for the Administrator; therefore, does not apply to CBEC.	
40 CFR 60.10	State Authority- States maintain their authority to impose stricter requirements than the federal regulations.		✓	This is guidance for the States and does not apply directly to CBEC.	CBEC must comply with all applicable state regulations (see IAC sections of Table B-1).
40 CFR 60.11	Performance tests shall determine compliance with standards in this part, except opacity standards which will be determined by conducting observations in accordance with Method 9, using an alternative method approved by the Administrator, or by implementing a Continuous Opacity Monitoring System (COMS). Air pollution control equipment shall be maintained in a manner consistent with good air pollution control practice.	✓		Opacity observations shall be conducted concurrently with the initial performance test, or within 60 days after achieving the maximum production rate if performance tests will not be conducted.	Required tests/observations shall be recorded and retained on file.
40 CFR 60.12	No owner or operator subject to the provisions of this part shall build, erect, install, or use any article, machine, equipment or process, the use of which conceals an emission which would otherwise constitute a violation of an applicable standard. Such concealment includes, but is not limited to, the use of gaseous dilutents to achieve compliance with an opacity standard or with a standard which is based on the concentration of a pollutant in the gases discharged to the atmosphere.	✓		CBEC shall not use any device to conceal their emissions.	Maintain all building plans and equipment specifications to document compliance.

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 60.13(a), Appendix B (COMS)	COMS installed will meet ASTM 6216-98 and have a certificate of conformance from the manufacturer. COMS will be located where measurements are representative of the total emissions from the facility. All tests and re-tests will be conducted as outlined in 40 CFR 60 Appendix B.	✓		Appendix B gives extensive requirements and specifications for COMS and should be referenced to verify compliance. Also see 40 CFR Part 75	Verify and document that COMS meet ASTM 6216-98, retain certificate of conformance on file. Document all tests, re-test, and all other requirements given in Appendix B.
40 CFR 60.13(a), Appendix B (CEMS)	Procedures for measuring CEMS relative accuracy and calibration drift are outlined. CEMS installation and measurement location specifications, equipment specifications, performance specifications, and data reduction procedures are included. Conformance of the CEMS with the Performance Specification is determined.	✓		Appendix B gives extensive requirements and specifications for CEMS and should be referenced to verify compliance. Also see 40 CFR Part 75	Verify and document that CEMS meet requirements of this appendix. Document all tests, re-test, and all other requirements given in Appendix B.

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 60.13(a), Appendix F	This procedure specifies the minimum QA requirements necessary for the control and assessment of the quality of CEMS data submitted to the Environmental Protection Agency (EPA). Source owners and operators responsible for one or more CEMS's used for compliance monitoring must meet these minimum requirements and are encouraged to develop and implement a more extensive QA program or to continue such programs where they already exist. Data collected as a result of QA and QC measures required in this procedure are to be submitted to the Agency. These data are to be used by both the Agency and the CEMS operator in assessing the effectiveness of the CEMS QC and QA procedures in the maintenance of acceptable CEMS operation and valid emission data.	✓		Each source owner or operator must develop and implement a QC program. As a minimum, each QC program must include written procedures which should describe in detail, complete, step-by-step procedures and operations for each of the following activities: 1. Calibration of CEMS. 2. CD determination and adjustment of CEMS. 3. Preventive maintenance of CEMS (including spare parts inventory). 4. Data recording, calculations, and reporting. 5. Accuracy audit procedures including sampling and analysis methods. 6. Program of corrective action for malfunctioning CEMS. These written procedures must be kept on record and available for inspection by the enforcement agency. Also see 40 CFR Part 75.	Procedures shall be written, implemented, and maintained on file. Activities outlined in procedures shall also be documented and records retained.
40 CFR 60.13(b)	CEMS will be installed and operational prior to performance tests. Manufacturer's written requirements or recommendations for installation operation and calibration shall be completed, as a minimum. If COMS data will be submitted, compliance with Performance Specification 1 (see 40 CFR 60 Appendix B) must be met before the performance test.	✓		Monitoring systems shall be operational and all necessary documentation completed before performance tests. Also see 40 CFR Part 75.	Document and retain records of installation and operational tests Maintain records of manufacturer's requirements.

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4?		Comments	Methods Used to Demonstrate Compliance[1]
		Yes	No		
40 CFR 60.13(c)	If the owner or operator of an affected facility elects to submit COMS data for compliance with the opacity, he shall conduct a performance evaluation of the COMS as specified in Performance Specification 1, Appendix B, of this part before the performance test required under § 60.8 is conducted. Otherwise, the owner or operator of an affected facility shall conduct a performance evaluation of the COMS or CEMS during any performance test required under § 60.8 or within 30 days thereafter in accordance with the applicable performance specification in Appendix B of this part. The owner or operator of an affected facility shall conduct COMS or CEMS performance evaluations at such other times as may be required by the Administrator.	✓		If COMS data will be submitted for compliance a performance evaluation will be completed before the performance test. Otherwise, performance evaluations shall be conducted during performance tests or within 30 days of performance tests. Also see 40 CFR Part 75.	Document performance evaluations and retain records.

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 60.13(d)	Owners and operators of a CEMS installed in accordance with the provisions of this part, must automatically check the zero (or low level value between 0 and 20 percent of span value) and span (50 to 100 percent of span value) calibration drifts at least once daily in accordance with a written procedure. The zero and span must, as a minimum, be adjusted whenever either the 24-hour zero drift or the 24-hour span drift exceeds two times the limit of the applicable performance specification. The system must allow the amount of the excess zero and span drift to be recorded and quantified whenever specified. Owners and operators of a COMS installed in accordance with the provisions of this part, must automatically, intrinsic to the opacity monitor, check the zero and upscale (span) calibration drifts at least once daily. For continuous monitoring systems measuring opacity of emissions not using automatic zero adjustments, the optical surfaces exposed to the effluent gases shall be cleaned prior to performing the zero and span drift adjustments. For systems using automatic zero adjustments, the optical surfaces shall be cleaned when the cumulative automatic zero compensation exceeds 4 percent opacity.	✓		Owners and operators of COMS and/or CEMS must check the zero and span calibration drifts at least once daily in accordance with a written procedure. Adjustments will be made when necessary. Also see 40 CFR Part 75.	Write and implement a procedure for this requirement. Document all checks, calibrations, adjustments and cleanings.
40 CFR 60.13(e) – (j)	Guidelines for adjustments, monitoring requirements, tests, and data requirements for CEMS and COMS are outlined in these paragraphs.	✓		These paragraphs give extensive requirements and specifications for CEMS and COMS and should be referenced to verify compliance. Also see 40 CFR Part 75.	Compliance with all required activities shall be documented and records retained.

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 60.14	Any physical or operational change to an existing facility, which results in an increase in the emission rate to the atmosphere of any pollutant to which a standard applies, shall be considered a modification. Upon modification, an existing facility shall become an affected facility for each pollutant to which a standard applies and for which there is an increase in the emission rate to the atmosphere.	✓		Installing Unit 4 qualifies as a modification and must be covered by an air permit.	MidAmerican Energy is applying for this permit modification for the addition of Unit 4. Unit 4 will not be built until all necessary permits are obtained.
40 CFR 60.15	An existing facility, upon reconstruction, becomes an affected facility, irrespective of any change in emission rate.		✓	CBEC is not planning any reconstruction at this time; therefore, this rule does not apply.	
40 CFR 60.16	Priority list for regulators.		✓	The priority list is guidance for the regulators and does not apply to CBEC.	
40 CFR 60.17	Incorporations by reference.	✓		No specific requirements are presented in this section.	
40 CFR 60.18	This section contains requirements for control devices used to comply with applicable subparts of parts 60 and 61. The requirements are placed here for administrative convenience and only apply to facilities covered by subparts referring to this section.		✓	This section does not cover the control devices used for Unit 4; therefore, this section does not apply to CBEC.	
40 CFR 60.19	General notification and reporting requirements.	✓		Refer to this section for details of all notification and reporting requirements.	All necessary reports will be submitted to IDNR in the appropriate time frame.
40 CFR 60.20 – 29	State Plan guidance.		✓	These sections give guidance for states and does not apply to CBEC.	

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 60.30 – 60.39	These sections are specific to waste combustion units, incinerators, solid waste landfills, and sulfuric acid production plants.		✓	CBEC does not conduct any of the mentioned processes; therefore, these sections do not apply.	
40 CFR 60, Subpart D, Standards of Performance for Fossil-Fuel-Fired Steam Generators for Which Construction is Commenced After August 17, 1971					
40 CFR 60.40 – 46	Each fossil-fuel-fired steam-generating unit of more than 73 megawatts heat input rate (250 MMBtu per hour) for which construction is commenced after August 17, 1971. Excludes sources that are subject to Subpart Da.		✓	Unit 4 is covered under subpart Da; therefore, subpart D does not apply. Note: Units 1 and 2 are "pre-NSPS" and Unit 3 is subject to Subpart D.	
40 CFR 60, Subpart Da, Standards of Performance for Electric Utility Steam Generating Units for Which Construction is Commenced After September 18, 1978					
40 CFR 60.40a	The affected facility to which this subpart applies is each electric utility steam-generating unit that is capable of combusting more than 73 megawatts (250 million Btu/hour) heat input of fossil fuel (either alone or in combination with any other fuel); and for which construction or modification is commenced after September 18, 1978.	✓		Unit 4 meets the criteria listed and must meet the requirements in this subpart.	No requirements mentioned in this section.
40 CFR 60.41a	Definitions for 40 CFR 60, Subpart Da.	✓		This is not an applicable standard or limitation, however, these definitions do apply when evaluating other applicable requirements from Subpart Da.	

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 60.42a	On and after the date on which the performance test required to be conducted under § 60.8 is completed, no owner or operator subject to the provisions of this subpart shall cause to be discharged into the atmosphere from any affected facility any gases which contain particulate matter in excess of: (1) 13 ng/J (0.03 lb/million Btu) heat input derived from the combustion of solid, liquid, or gaseous fuel; (2) 1 percent of the potential combustion concentration (99 percent reduction) when combusting solid fuel; and (3) 30 percent of potential combustion concentration (70 percent reduction) when combusting liquid fuel. (b) On and after the date the particulate matter performance test required to be conducted under § 60.8 is completed, no owner or operator subject to the provisions of this subpart shall cause to be discharged into the atmosphere from any affected facility any gases which exhibit greater than 20 percent opacity (6-minute average), except for one 6-minute period per hour of not more than 27 percent opacity.	✓		Unit 4 may not discharge in amounts greater than what is listed in this section.	All monitoring activities and/or reports of emissions should shall be documented and retained on file. CBEC will install, certify (Appendix B) and maintain (Appendix F) a COMS.
40 CFR 60.43a	On and after the date on which the initial performance test is completed, no owner or operator subject to the provisions of this subpart shall cause to be discharged into the atmosphere from any affected facility which combusts solid fuel or solid-derived fuel any gases which contain sulfur dioxide in excess of 520 ng/J (1.20 lb/million Btu) heat input and 10 percent of the potential combustion concentration (90 percent reduction), or 30 percent of the potential combustion concentration (70 percent reduction), when emissions are less than 260 ng/J (0.60 lb/million Btu) heat input.	✓		Unit 4 may not discharge in amounts greater than what is listed in this section. Both scrubber inlet and outlet SO2 concentrations will be continuously monitored to determine removal efficiency.	All monitoring activities and/or reports of emissions shall be documented and retained on file. CBEC will install, certify (Appendix B) and maintain (Appendix F) a CEMS for SO2 and a diluent gas.

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 60.44a	On and after the date on which the initial performance test is completed, no owner or operator subject to the provisions of this subpart shall cause to be discharged into the atmosphere from any affected facility any gases which contain nitrogen oxides (expressed as NO2) in excess of the following emission limits, based on a 30-day rolling average: Subbituminous coal – 210 (ng/J), 0.50 (lb/MMBtu) Bituminous coal – 260 (ng/J), 0.60 (lb/MMBtu) Anthracite coal - 260 (ng/J), 0.60 (lb/MMBtu) All other fuels – 260 (ng/J), 0.60 (lb/MMBtu) In addition the unit may not emit NOx in excess of 1.6 pounds per megawatt hour of electricity produced.	✓		Unit 4 may not discharge in amounts greater than what is listed in this section. Current plans call for the use Powder River Basin (PRB) subbituminous coal in Unit 4.	All monitoring activities and/or reports of emissions shall be documented and retained on file. CBEC will install, certify (Appendix B) and maintain (Appendix F) a CEMS for NOx and a diluent gas.
40 CFR 60.45a	An owner or operator of an affected facility proposing to demonstrate an emerging technology may apply to the Administrator for a commercial demonstration permit. Only the Administrator may issue commercial demonstration permits, and this authority will not be delegated.		✓	No emerging technologies are currently planned for Unit 4; therefore, this section does not apply.	

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4?		Comments	Methods Used to Demonstrate Compliance[1]
		Yes	No		
40 CFR 60.46a	Compliance with PM and NOx limits listed in 40 CFR 60.42 and 60.44 constitutes compliance for these pollutants. During emergency conditions in the principal company, an affected facility with a malfunctioning flue gas desulfurization system may be operated if sulfur dioxide emissions are minimized by operating all operable flue gas desulfurization system modules, and bringing back into operation any malfunctioned module as soon as repairs are completed, bypassing flue gases around only those flue gas desulfurization system modules that have been taken out of operation because they were incapable of any sulfur dioxide emission reduction or which would have suffered significant physical damage if they had remained in operation, and designing, constructing, and operating a spare flue gas desulfurization system module for an affected facility larger than 365 MW (1,250 million Btu/hr) heat.	✓		If compliance with 40 CFR 60.42 or 60.44 cannot be maintained, refer to this section for further guidance. If desulfurization system is malfunctioning, operate only if compliance with this section can be maintained.	Maintain documents illustrating compliance with 40 CFR 60.42 and 60.44. If compliance cannot be achieved or desulfurization system is malfunctioning, maintain documentation of activities required in this section.
40 CFR 60.47a	The owner or operator of an affected facility shall install, calibrate, maintain, and operate a continuous monitoring system, and record the output of the system, for measuring the opacity of emissions and sulfur dioxide and NOx emissions discharged to the atmosphere. If the owner or operator has installed a nitrogen oxides emission rate CEMS to meet the requirements of part 75 of this chapter and is continuing to meet the ongoing requirements of part 75 of this chapter, that CEMS may be used to meet the requirements of this section, except that the owner or operator shall also meet the requirements of § 60.49a.	✓		CBEC must have CEMS and must comply with this section.	Install CEMS and COMS and document calibration and maintenance of equipment, or comply with 40 CFR 75 and 60.49a.
40 CFR 60.48a	In conducting the performance tests required, the owner or operator shall use as reference methods and procedures in Appendix A of this part or the methods and procedures as specified in this section.	✓		CBEC must use these methods to conduct performance tests.	Document methods used to conduct tests.

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 60.49a	For sulfur dioxide, nitrogen oxides, and particulate matter emissions, the performance test data from the initial performance test and from the performance evaluation of the continuous monitors (including the transmissometer) are submitted to the Administrator.	✓		CBEC must submit these documents quarterly if electronic and semiannually if written, except when opacity limits are exceeded which must be submitted every quarter. Specific reporting requirements are listed in this section. Refer to section for specific requirements.	Submit required documents as outlined in this section.
40 CFR 60, Subpart Db, Standards of Performance for Industrial-Commercial-Institutional Steam Generating Units					
40 CFR 60.40b – end	Coal-fired affected facilities having a heat input capacity greater than 29 MW (100 MMBtu/hour) and less than 73 MW (250 MMBtu/hour) and meeting the applicability requirements under subpart D (Standards of performance for fossil-fuel-fired steam generators; § 60.40) are subject to the particulate matter and nitrogen oxides standards under this subpart and to the sulfur dioxide standards under subpart D (§ 60.43).	✓		Subpart Db applies to boilers with heat input >100 MMBtu/hour and <250 MMBtu/hour; CBEC Unit 4 is much larger (7,675 MMBtu/hr). Therefore, this subpart does not apply to Unit 4. The subpart does apply to the planned Auxiliary Boiler for Unit 4. This boiler will be diesel fired and rated at 137.4 MMBtu/hr. The NOx provisions of Subpart Db will apply.	Auxiliary Boiler for Unit 4 will need to meet NOx performance limits and reporting outlined in Subpart Db.
40 CFR Part 60, Subpart Y, Standards of Performance for Coal Preparation Plants					

TABLE B-2
Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 60.250 (a) and (b)	The provisions of this subpart apply to thermal dryers, pneumatic coal cleaning equipment (air tables), coal processing and conveying equipment (including breakers and crushers), coal storage systems, and coal transfer and loading systems at coal preparation plants which process more than 200 tons of coal per day and were constructed or modified after October 24, 1974.	✓		CBEC includes coal unloading, stacking, storage and conveying equipment; therefore this rule applies to the Unit 4 project.	See 40 CFR 60.253 and 60.254.
40 CFR 60.251	Definitions.	✓		This is not an applicable standard or limitation, however, these definitions do apply when evaluating other applicable requirements from Subpart Y.	
40 CFR 60.252	Standards for Particulate Matter: Thermal dryers: 0.070 g/dscm, 20% opacity Pneumatic coal cleaning: 0.040 g/dscm, 10% opacity Processing, storage, conveying: 20% opacity	✓		CBEC includes coal unloading, conveying and storage equipment; therefore the 20% opacity limitation in this rule applies. CBEC does not include any thermal dryers or pneumatic coal-cleaning equipment.	
40 CFR 60.253	Monitoring of Operations: Operators of thermal dryers shall install, calibrate maintain and continuously operate monitoring devises for gas stream temperature and (if the dryer is equipped with a venturi scrubber) gas stream pressure loss and water supply pressure. Devices shall be recalibrated annually.		✓	CBEC does not have a thermal dryer; therefore this rule does not apply.	

TABLE B-2
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Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 60.254	Test Methods and Procedures: This rule specifies that Reference Methods 5 and 9 are to be used for the performance tests required under §60.8	✓		Following startup of Unit 4, performance tests will be required to verify compliance with all applicable stack and coal handling source emission limitations.	Performance Test Report submitted to EPA and IDNR. Records of continuous monitoring shall be maintained on-site for a minimum of 3 years.

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 61, National Emission Standards For Hazardous Air Pollutants					
40 CFR 61.01 – 61.03	Definitions and general information regarding 40 CFR 61.	✓		This is not an applicable standard or limitation; however, these definitions do apply when evaluating other applicable requirements within 40 CFR 61.	
40 CFR 61.04	All requests, reports, applications, submittals, and other communications to the Administrator pursuant to this part shall be submitted in duplicate to the U.S. EPA Region VII office in Kansas City. A copy should also be sent to the Iowa Department of Natural Resources, Bureau of Air Quality in Des Moines.	✓		All reports required under 40 CFR 61 shall be submitted to the listed agencies.	Maintain records of all submittals on file.
40 CFR 61.05	No owner or operator shall construct or modify any stationary source without first obtaining written approval from the Administrator. No owner or operator shall operate a new stationary source in violation of standards, except under an exemption. Ninety days after the effective date of any standard, no owner or operator shall operate any existing source subject to that standard in violation of the standard, except under a waiver granted by the Administrator or under an exemption granted by the President. No owner or operator subject to the provisions of this part shall fail to report, revise reports, or report source test results as required under this part.	✓		CBEC may not operate in violation of any applicable standards without a waiver or exemption. All reports required under this part shall be completed and sent to the appropriate regulatory agency as required.	Maintain all reports demonstrating compliance with regulations. Periodically audit internal procedures and practices to insure compliance.
40 CFR 61.06	Advises facilities that they can request a determination of construction or modification from the Administrator.		✓	It has already been determined that Unit 4 is considered a modification; therefore, this section does not apply.	

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Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 61.07	The owner or operator shall submit to the Administrator an application for approval of the construction of any new source or modification of any existing source. The application shall be submitted before the construction or modification is planned to commence, or within 30 days after the effective date if the construction or modification had commenced before the effective date and initial startup has not occurred.	✓		CBEC must receive approval for the construction of Unit 4.	This application is being submitted for approval.
40 CFR 61.08	The Administrator will notify applicant of approval.		✓	This applies to the EPA and is not a requirement of CBEC.	
40 CFR 61.09	The owner or operator of each stationary source which has an initial startup after the effective date of a standard shall furnish the Administrator with written notification as follows: 1. A notification of the anticipated date of initial startup of the source not more than 60 days nor less than 30 days before that date. 2. A notification of the actual date of initial startup of the source within 15 days after that date.	✓		CBEC must send notification of anticipated and actual start up.	Maintain documentation that notification was sent on file.
40 CFR 61.10 – 61.11	Describes source reporting, waiver requests, and other requirements for existing sources.		✓	Unit 4 is not an existing source; therefore, these rules do not apply.	
40 CFR 61.12	The owner or operator of each stationary source shall maintain and operate the source, including associated equipment for air pollution control, in a manner consistent with good air pollution control practice for minimizing emissions.	✓		CBEC must minimize emissions.	Implementation of BACT along with documentation of proper maintenance and monitoring will demonstrate compliance.
40 CFR 61.13 – 61.14	Each owner or operator shall conduct emission testing and maintain and operate each monitoring system as specified in applicable subparts.	✓		CBEC must complete requirements in applicable subparts. No new requirements mentioned in this section.	Maintain documentation of compliance with subparts.

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 61.15	Upon modification, an existing source shall become a new source for each hazardous pollutant for which the rate of emission to the atmosphere increases and to which a standard applies.	✓		Unit 4 constitutes a modification and must comply with this section.	HAPs discharged should be expressed in kg/hr. Emission factors should be from AP-42 or material balances, monitoring data, or manual emission tests if AP 42 does not satisfactorily demonstrate an increase or decrease.
40 CFR 61.20 – 61.26	Guidelines and requirements for uranium mines.		✓	CBEC does not operate any uranium mines on this property; therefore, these rules do not apply.	
40 CFR 61.30 – 61.34	Guidelines and requirements for facilities that process beryllium and beryllium compounds.		✓	CBEC does not process beryllium or beryllium compounds; therefore, these rules do not apply.	
40 CFR 61.40 – 61.44	Guidelines and requirements for rocket motor test sites.		✓	CBEC does not test rocket motors; therefore, these rules do not apply.	
40 CFR 61.50 – 61.56	Guidelines and requirements for facilities that process mercury ore to recover mercury, use mercury chloralkali cells to produce chlorine gas and alkali metal hydroxide, and incinerate or dry wastewater treatment plant sludge.		✓	CBEC does not have any processes that recover mercury or use mercury chloralkali cells, or incinerate dry sludge; therefore, these rules do not apply.	
40 CFR 61.60 – 61.71	Guidelines and requirements for facilities which produce ethylene dichloride by reaction of oxygen and hydrogen chloride with ethylene, vinyl chloride by any process, and/or one or more polymers containing any fraction of polymerized vinyl chloride.		✓	CBEC does not have any of these processes; therefore, these rules do no apply.	

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 61.90 – 61.97	Guidelines and requirements for operations at any facility owned or operated by the Department of Energy (DOE) that emits any radionuclide other than radon-222 and radon-220 into the air.		✓	CBEC is not owned or operated by the DOE; therefore, these rules do not apply.	
40 CFR 61.100 – 61.108	Guidelines and requirements for facilities owned or operated by any Federal agency other than the DOE and not licensed by the Nuclear Regulatory Commission that emits radionuclides into the air.		✓	CBEC is not owned or operated by any federal agency; therefore, these rules do not apply.	
40 CFR 61.110 – 61.112	Guidelines and requirements for facilities that have possible equipment leaks of benzene.		✓	CBEC does not have benzene in its processes; therefore these rules do not apply.	
40 CFR 61.120 – 61.127	Guidelines and requirements for radionuclide emissions from elemental phosphorus plants.		✓	CBEC does not have any processes with elemental phosphorus; therefore, these rules do not apply.	
40 CFR 61.130 – 61.139	Guidelines and requirements for furnace and foundry coke by-product recovery plants.		✓	CBEC does not recover coke by-products; therefore, these rules do not apply.	
40 CFR 61.140 – 61.157	Guidelines and requirements for facilities that manufacture, use, or handle asbestos.	✓		Units 1, 2 and 3 at CBEC were built prior to the promulgation of the NESHAP, OSHA and AHERA rules pertaining to asbestos and likely contain asbestos-containing building materials (ACBM) and thermal system insulation (TSI); therefore, these rules apply to the handling of ACBM and TSI within the existing facility. MidAmerican is required under NESHAP to evaluate whether any existing asbestos will be disturbed or affected during construction of Unit 4.	Pre-construction survey report; asbestos management plan, records of asbestos handling and personnel exposure testing shall be maintained on-site for a minimum of 10 years.

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4?		Comments	Methods Used to Demonstrate Compliance[1]
		Yes	No		
40 CFR 61.160 – 61.165	Guidelines and requirements for glass manufacturing plants.		✓	CBEC does not manufacture glass; therefore, these rules do not apply.	
40 CFR 61.170 – 61.177	Guidelines and requirements for primary copper smelters.		✓	CBEC is not a copper smelter; therefore, these rules do not apply.	
40 CFR 61.180 – 61.186	Guidelines and requirements for arsenic production facilities.		✓	CBEC is not an arsenic production facility; therefore, these rules do not apply.	
40 CFR 61.190 – 61.193	Guidelines and requirements for DOE facilities.		✓	CBEC is not a DOE facility; therefore, these rules do not apply.	
40 CFR 61.200 – 61.210	Guidelines and requirements for facilities with a phosphogypsum stack, or otherwise uses any quantity of phosphogypsum which is produced as a result of wet acid phosphorus production or is removed from any existing phosphogypsum stack.		✓	CBEC does not use phosphogypsum; therefore, these rules do not apply.	
40 CFR 61.220 – 61.226	Guidelines and requirements for sites that are used for the disposal of tailings, and that managed residual radioactive material during and following the processing of uranium ores.		✓	CBEC does not manage uranium or use its property for tailing disposal; therefore, these rules do not apply.	
40 CFR 61.240 – 61.247	Guidelines and requirements for sources that are intended to operate in volatile hazardous air pollutant (VHAP) service.		✓	CBEC does not have any sources intended to operate in (VHAP) service; therefore, these rules do not apply.	
40 CFR 61.250 – 61.256	Guidelines and requirements for facilities licensed to manage uranium byproduct materials during and following the processing of uranium ores, commonly referred to as uranium mills and their associated tailings. This subpart does not apply to the disposal of tailings.		✓	CBEC does not manage any uranium materials; therefore, these rules do not apply.	

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4?		Comments	Methods Used to Demonstrate Compliance[1]
		Yes	No		
40 CFR 61.270 – 61.277	Guidelines and requirements for facilities that store benzene.		✓	CBEC does not store benzene; therefore, these rules do not apply.	
40 CFR 61.300 – 61.306	Guidelines and requirements for benzene transfer operations.		✓	CBEC does not have any benzene transfer operations; therefore, these rules do not apply.	
40 CFR 61.340 – 61.358	Guidelines and requirements for chemical manufacturing plants, coke by-product recovery plants, petroleum refineries or hazardous waste treatment, storage and disposal facilities (TSDFs) that accept wastes from the previously mentioned plants.		✓	CBEC does not apply as any of the plants listed; therefore, these rules do not apply.	
40 CFR 62, Approval and Promulgation of State Plans for Designated Facilities and Pollutants					
40 CFR 62	This part sets forth the Administrator's approval and disapproval of State plans for the control of pollutants and facilities.		✓	This is the responsibility of the States and the Administrator and does not apply to CBEC.	
40 CFR 63, National Emission Standards for Hazardous Air Pollutants for Source Categories					
40 CFR 63.1 – 63.3	Definitions and general information regarding 40 CFR 63.	✓		This is not an applicable standard or limitation; however, these definitions do apply when evaluating other applicable requirements within 40 CFR 63.	
40 CFR 63.4	No owner or operator subject to the provisions of this part may operate any affected source in violation of the requirements of this part. No owner or operator subject to the provisions of this part shall fail to keep records, notify, report, or revise reports as required under this part.	✓		CBEC will not operate in violation of this part and will maintain records as required.	Record activities showing compliance and maintain on file.

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 63.5	No person may, without obtaining written approval in advance from the Administrator do any of the following: construct a new affected source that is major-emitting and subject to such standard; reconstruct an affected source that is major-emitting and subject to such standard; or reconstruct a major source such that the source becomes an affected source that is major-emitting and subject to the standard.	✓		MidAmerican Energy must receive approval before constructing Unit 4.	This application is being submitted in compliance with this rule.
40 CFR 63.6	The owner or operator of an affected source must develop and implement a written startup, shutdown, and malfunction plan that describes, in detail, procedures for operating and maintaining the source during periods of startup, shutdown, and malfunction; a program of corrective action for malfunctioning process; and air pollution control and monitoring equipment used to comply with the relevant standard. This plan must be developed by the source's compliance date for that relevant standard.	✓		MidAmerican Energy must implement a startup, shutdown and malfunction plan as described in this rule.	Maintain a copy of this plan on file.
40 CFR 63.7	If required to do performance testing by a relevant standard, and a waiver of performance testing is not obtained, the owner or operator of the affected source must perform such tests within 180 days of the compliance date for such source.	✓		MidAmerican Energy must complete all required performance testing within 180 days of the compliance date.	Document the date all applicable tests are conducted and maintain on file.

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 63.8	The owner or operator of an affected source shall maintain and operate each CMS in a manner consistent with good air pollution control practices. All CMS must be installed such that representative measures of emissions or process parameters from the affected source are obtained. In addition, CEMS must be located according to procedures contained in the applicable performance specification(s). All CMS shall be installed, operational, and the data verified as specified in the relevant standard either prior to or in conjunction with conducting performance tests. Verification of operational status shall, at a minimum, include completion of the manufacturer's written specifications or recommendations for installation, operation, and calibration of the system. Except for system breakdowns, out-of-control periods, repairs, maintenance periods, calibration checks, and zero (low-level) and high-level calibration drift adjustments, all CMS, including COMS and CEMS, shall be in continuous operation and shall meet minimum frequency of operation requirements.		✓	Although Unit 4 will be equipped with a COMS and a CEMS, pursuant to the federal NSPS and acid rain programs, continuous monitoring is not required under NESHAP.	
470 CFR 63.9	The owner or operator of a source shall notify the Administrator designated state authority if emissions increase, if a source will be constructed or reconstructed, and other notifications regarding CMS mentioned in 40 CFR 75.	✓		This application is being submitted in accordance with this rule. MidAmerican Energy will need to notify the State if changes are made to operations that affect emissions.	This application is being submitted in accordance with this rule.

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 63.10	The owner or operator of an affected source shall submit reports to the delegated State authority. In addition, if the delegated authority is the State, the owner or operator shall send a copy of each report submitted to the State to the appropriate Regional Office of the EPA, as specified in paragraph (a)(4)(i) of this section. The Regional Office may waive this requirement for any reports at its discretion.	✓		Records shall be maintained of the occurrence and duration of each startup, shutdown, or malfunction of operation; the occurrence and duration of each malfunction of the required air pollution control and monitoring equipment; all required maintenance performed on the air pollution control and monitoring equipment; actions taken during periods of startup, shutdown, and malfunction when such actions are different from the procedures specified in the affected source's startup, shutdown, and malfunction plan; all information necessary to demonstrate conformance with the affected source's startup, shutdown, and malfunction plan when all actions taken during periods of startup, shutdown, and malfunction are consistent with the procedures specified in such plan; each period during which a CMS is malfunctioning or inoperative; and all required measurements needed to demonstrate compliance with a relevant standard.	These records will be created and maintained on file.
40 CFR 63.11	Owners or operators using flares to comply with the provisions of this part shall monitor these control devices to assure that they are operated and maintained in conformance with their designs. Applicable subparts will provide provisions stating how owners or operators using flares shall monitor these control devices.		✓	Flares will not be used as control devices; therefore, this rule does not apply.	

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4?		Comments	Methods Used to Demonstrate Compliance[1]
		Yes	No		
40 CFR 63.12 – 63.15	General information, authority delegation, and addresses pertaining to 40 CFR 63.	✓		These are not applicable standards or limitations; however, these sections do apply when evaluating other applicable requirements within 40 CFR 63.40 – 63.44.	
40 CFR 63.40	The requirements of this subpart apply to any owner or operator who constructs or reconstructs a major source of hazardous air pollutants after the effective date of section 112(g)(2)(B) and the effective date of a Title V permit program in the State or local jurisdiction in which the major source is located unless the major source in question has been specifically regulated or exempted from regulation, or the owner or operator of such major source has received all necessary air quality permits for such construction or reconstruction.	✓		Coal and oil-fired power plants have been included in the 112(c) listing of source categories since December 2000; therefore, this section does apply to Unit 4.	
40 CFR 63.41	Definitions applicable to 40 CFR 63.40 – 63.44.	✓		This is not an applicable standard or limitation; however, this section will apply when evaluating other applicable requirements within 40 CFR 63.40 – 63.44.	
40 CFR 63.42	Program requirements governing construction or reconstruction of major sources. The anticipated promulgation date for a MACT standard for coal and oil-fired power plants is December 2004; therefore, a case-by-case MACT standard must be proposed and implemented by IDNR.	✓		This rule applies to IDNR and is not an obligation of CBEC. However, CBEC must comply with standards required by IDNR.	

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4?		Comments	Methods Used to Demonstrate Compliance[1]
		Yes	No		
40 CFR 63.43	The requirements of this section apply to an owner or operator who constructs or reconstructs a major source of HAP subject to a case-by-case determination of maximum achievable control technology.	✓		MidAmerican Energy must request approval of case-by-case MACT determinations.	This application contains Section 6, its tables and/or appendices that requests a MACT determination and provides all necessary documents.
40 CFR 63.44	Requirements for constructed or reconstructed major sources subject to a subsequently promulgated MACT standard or MACT requirement.		✓	There are no promulgated MACT standards or requirements for coal-fired power plants at this time; therefore, this section does not apply.	
40 CFR 63.50 – 63.56	This section implements section 112(j) of the CAA and includes the "MACT Hammer". In general, permitting authorities must issue or reopen Title V permits when a source becomes subject to 112(j).	✓		CBEC already has a Title V permit, which does not address the section 112(j) requirements and the plant became subject to section 112(j) in December 2000. Therefore, the provisions of 40 CFR 63.52 (b) apply to Unit 4.	Request for case-by-case MACT determination included in section 6 of this application.
40 CFR 63.60 – 63.62	Deletion and redefinition of specific chemicals on the HAPs list.		✓	This is not an applicable standard or limitation.	
40 CFR 63.70 – 63.5779	MACT regulations pertaining to specific industries.		✓	Coal-fired boilers are not included in these sections; therefore, these rules do not apply to CBEC or Unit 4.	
40 CFR 64, Compliance Assurance Monitoring					

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 64	Compliance Assurance Monitoring.	✓		CBEC is subject to federal acid rain program and is thus exempt from Part 64, pursuant to 40 CFR 64.2(b)(1)(iii) for the acid rain requirements only. However, Unit 4 will be subject to the CAM requirements for PM10, SO2 and NOx with respect to 40 CFR Part 60 and IDNR permit limitations.	The CAM Plan for Unit 4 is contained in Section 9 of the application text.
40 CFR 65, Consolidated Federal Air Rule					
40 CFR 65	The provisions of this subpart apply to owners or operators expressly referenced to this part from a subpart of 40 CFR part 60, 61, or 63 for which the owner or operator has chosen to comply with the provisions of this part as an alternative to the provisions in the referencing subpart.		✓	CBEC is not seeking alternate compliance provisions in accordance with this rule; therefore, these rules do not apply.	
40 CFR 66, Assessment and Collection of Non-Compliance Penalties by EPA					
40 CFR 66	Applies to all proceedings for the assessment by EPA of noncompliance penalties.		✓	Requirements for the EPA, not an obligation of CBEC.	
40 CFR 67, EPA Approval of State Non-Compliance Program					
40 CFR 67	Standards and procedures under which EPA will approve State programs for administering the noncompliance penalty program.		✓	EPA's requirements for states to implement a noncompliance penalty program, not an obligation of CBEC.	
40 CFR 68, Chemical Accident Prevention Provisions					

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 68	This part sets forth the list of regulated substances and thresholds, gives the petition process for adding or deleting substances to the list of regulated substances, outlines who need a Risk Management Plan (RMP), and sets requirements for RMPs.	✓		MidAmerican Energy does not currently have any chemicals onsite in excess of their threshold quantity listed in 40 CFR 68.130. MidAmerican Energy will evaluate the chemical storage requirements associated with the new plant construction to determine whether the RMP program is triggered.	TBD
40 CFR 69, Special Exemptions From the Requirements of the Clean Air Act					
40 CFR 69	Lists special exemptions.		✓	CBEC is not eligible for any special exemptions for the CAA.	
40 CFR 70, State Operating Permit Program					
40 CFR 70	The regulations in this part provide for the establishment of comprehensive State air quality permitting systems consistent with the requirements of Title V of the CAA. These regulations define the minimum elements required by the CAA for State operating permit programs and the corresponding standards and procedures by which the Administrator will approve, oversee, and withdraw approval of State operating permit programs.	✓		CBEC already has a Title V permit., which will need to be reopened to add the applicable requirements for Unit 4. This application is submitted to IDNR pursuant to Iowa's construction permit requirements, only.	This application is being submitted as required by IDNR for modifications. A separate application to reopen the existing Title V permit to add Unit 4 will be prepared and submitted within the required time frame.
40 CFR 71, Federal Operating Permit Programs					
40 CFR 71.1 – 71.23	Specifies applicability, definitions, units and abbreviations, and general guidelines of 40 CFR 71.	✓		This is not an applicable standard or limitation; however, these definitions do apply when determining fees and evaluating other applicable requirements within 40 CFR 71.	

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 71.24	Identifies where a permit application should be filed and outlines the following information that a permit application should contain to be complete: Identifying information, All information required in § 63.74, A statement of the proposed alternative emission limitation for hazardous air pollutants from the early reductions source on an annual basis, reflecting the emission reductions required to qualify the early reductions source for a compliance extension, Additional emission limiting requirements which are necessary to assure proper operation of installed control equipment and compliance with the annual alternative emission limitation for the early reductions source, Information necessary to define alternative operating scenarios for the early reductions source or permit terms and conditions for trading hazardous air pollutant increases and decreases, Address compliance status with respect to all applicable air pollution control requirements, a commitment to maintain continuing compliance, and a certification of compliance.	✓		A separate application to IDNR, which reopens the existing Title V permit to add Unit 4, must comply with the requirements in this section.	
40 CFR 71.25 – 71.27	Administrative guidelines on what a permit should contain; issuance, reopenings, and revisions; and public comment periods.	✓		These rules apply to the permitting authority and are not an obligation of CBEC.	
40 CFR 72 Permits Regulation					
40 CFR 72.1 – 72.5	General Provisions of the Acid Rain Program. 40 CFR 72.9 specifies the standard permitting, monitoring, sulfur dioxide, NO_X, excess emissions, recordkeeping and reporting, and liability requirements for affected sources.	✓		These sections do not include applicable standards or limitations; however, these definitions do apply when evaluating other applicable requirements in 40 CFR 72.	Maintenance of records.

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 72.6	Defines facilities and units to which 40 CFR 72 apply.	✓		Unit 4 is a new utility unit; therefore, these rules do apply.	
40 CFR 72.7 & 72.8	Outlines exemptions from these rules.		✓	CBEC does not qualify for any exemptions.	
40 CFR 72.9	Specifies that all facilities to which these rules apply must have an Acid Rain Permit.	✓		Separate EPA forms shall be downloaded, filled out and submitted to the EPA. The first step is to get an ORIS number assigned. Then the complete package of forms, which identify the DR and the ORIS number goes to the EPA.	Copies of MidAmerican Energy's acid rain permit revision application will be submitted to EPA and IDNR; a copy will be kept on file at CBEC.
40 CFR 72.10 – 72.13	Definitions and general information regarding 40 CFR 72.	✓		These are not applicable standards or limitations; however, these definitions do apply when evaluating other applicable requirements within 40 CFR 72.	
40 CFR 72.20	Each affected source, including all affected units at the source, shall have one and only one designated representative, with regard to all matters under the Acid Rain Program concerning the source or any affected unit at the source.	✓		CBEC must have one and only one representative for issues concerning the Acid Rain Program.	CBEC will specify one representative, and maintain the certificate listing the representative on file.

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 72.21	In each submission required to by signed by the designated representative under the Acid Rain Program, the designated representative shall certify, by signature: "I am authorized to make this submission on behalf of the owners and operators of the affected source or affected units for which the submission is made." and "I certify under penalty of law that I have personally examined, and am familiar with, the statements and information submitted in this document and all its attachments. Based on my inquiry of those individuals with primary responsibility for obtaining the information, I certify that the statements and information are to the best of my knowledge and belief true, accurate, and complete. I am aware that there are significant penalties for submitting false statements and information or omitting required statements and information, including the possibility of fine or imprisonment." The representative will provide a copy of the submission or determination to the owners and operators.	✓		The designated representative must have the quoted certifications on all documents being submitted or they will not be accepted by the regulatory agency. Owners and operators shall be kept informed of submissions and other activities pertaining to these rules.	Documentation of submissions including certification shall be kept on file. Documentation of updates to owners / operators shall be kept on file (e.g., management review minutes).
40 CFR 72.22	The certificate of representation may designate one and only one alternate designated representative, who may act on behalf of the designated representative.	✓		One alternate representative may be chosen to act in place of the designated representative.	Procedures for choosing an alternate and certification of the alternate shall be maintained.
40 CFR 72.23	The designated representative, alternate designated representative, and owners or operators may be changed at any time upon receipt by the Administrator of a superseding complete certificate of representation. A superseding certificate must be received within 30 days of a change in owner or operator.	✓		When any of these individuals change, a new certificate must be received.	All representatives and owners / operators must be listed on the most current certificate and certificates retained.

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 72.24	Requirements for a complete certificate of representation.	✓		Specific and extensive requirements. See 40 CFR 72.24 for list of all applicable requirements.	Each certificate of representation issued will contain all required elements and will be retained on file.
40 CFR 72.25	Once a complete certificate of representation has been submitted in accordance with § 72.24, the Administrator will rely on the certificate of representation unless and until a superseding complete certificate is received by the Administrator.	✓		MidAmerican Energy must submit a new certification to change representatives.	MidAmerican Energy will wait to change representatives until a new certificate has been issued whenever possible.
40 CFR 72.30 – 72.33	The designated representative of any source with an affected unit shall submit a complete Acid Rain permit application by the applicable deadline in paragraphs (b) and (c) of this section, and the owners and operators of such source and any affected unit at the source shall not operate the source or unit without a permit that states its Acid Rain program requirements.	✓		MidAmerican Energy will need to update their current acid rain permit to accommodate the addition of Unit 4, which will be performed separately. This application is submitted pursuant to Iowa's construction permit process only.	Current permit for CBEC facility will be retained on file. Copies of acid rain permit application for Unit 4 will be submitted to IDNR and will be kept on file at MidAmerican Energy.
40 CFR 72.40	Outlines the requirements of a complete compliance plan.	✓		MidAmerican Energy will need to create a complete compliance plan in accordance with this section.	A copy of the compliance plan will be submitted to EPA and IDNR. MidAmerican Energy will implement and maintain compliance plan on site.

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 72.41 – 72.44	Guidelines for substitution plans, extension plans, reduced utilization plans, and repowering extensions.		✓	MidAmerican Energy is not conducting any of the activities required for these plans; therefore, these rules do not apply at this time.	
40 CFR 72.50 – 72.74	Guidelines for obtaining a Title IV permit.		✓	CBEC is not receiving a new permit, but will modify a current permit. The provisions of 40 CFR 72.50 through 72.74 are applicable to initial permits. Modifications to existing permits are provided in 40 CFR 72.80 through 72.85.	
40 CFR 72.80	A permit revision may be submitted for approval at any time. No permit revision shall affect the term of the Acid Rain permit to be revised. No permit revision shall excuse any violation of an Acid Rain Program requirement that occurred prior to the effective date of the revision.	✓		MidAmerican Energy must revise its acid rain permit to accommodate Unit 4, which will occur separately.	Copies of the acid rain permit revision application will be submitted to EPA and IDNR; kept on file at MidAmerican Energy.
40 CFR 72.81	Permits must be revised if processes are modified.	✓		CBEC must revise their permit to accommodate the addition of Unit 4.	
40 CFR 72.82	The designated representative shall serve such a copy on the Administrator, the permitting authority, and any person entitled to receive a written notice of a draft permit under the approved State operating permit program. Within 5 business days of serving such copies, the designated representative shall also give public notice by publication in a newspaper of general circulation in the area where the sources are located or in a State publication designed to give general public notice.	✓		If CBEC submits a fast-track modification, this rule will apply.	Copies will be submitted to EPA and IDNR; kept on file at MidAmerican Energy. Retain documentation of public notice on file.
40 CFR 72.83 – 72.85	Administrative instructions for permit amendments and re-openings.	✓		Administrative guidelines and requirements apply to permitting authority and are not an obligation of MidAmerican Energy.	

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Council Bluffs Energy Center Unit 4
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Applicable Requirement	Summary of Requirement	Applicable to Unit 4?		Comments	Methods Used to Demonstrate Compliance[1]
		Yes	No		
40 CFR 72.90 – 72.96	For each calendar year in which a unit is subject to the Acid Rain emissions limitations, the designated representative of the source at which the unit is located shall submit to the Administrator, within 60 days after the end of the calendar year, an annual compliance certification report for the unit.	✓		CBEC will need to submit an annual compliance certification as long as it is required to have an acid rain permit. Specific requirements for certification are detailed in this part.	Submit certification annually, retain copies on file.
40 CFR 73, Sulfur Dioxide Allowance System					
40 CFR 73	Sulfur dioxide allowance system.	✓		The plant must have sufficient allowances available to account for each ton of annual SO_2 emissions. MidAmerican will need to obtain the necessary new allowances.	CEMS and quarterly EDRs (pursuant to 40 CFR Part 75).
40 CFR 74, Sulfur Dioxide Opt-Ins					
40 CFR 74	Guidelines for Sulfur Dioxide Opt-In program		✓	MidAmerican Energy is not eligible for the Opt-In program; therefore, these rules do not apply.	
40 CFR 75 Continuous Emission Monitoring					
40 CFR 75.1 – 75.3	Definitions and general information regarding 40 CFR 75.	✓		This is not an applicable standard or limitation; however, these definitions do apply when evaluating other applicable requirements.	
40 CFR 75.4	The owner or operator of each new affected unit shall ensure that all monitoring systems required under this part for monitoring of SO2, NOx, CO2, opacity, and volumetric flow are installed and all certification tests are completed no later than 90 days after the date the unit commences commercial operation.	✓		MidAmerican Energy must install monitoring equipment prior to startup and complete certification tests as specified.	Retain documentation of installation and certification testing on file, suitable for agency inspection, for a minimum of 10 years.
40 CFR 75.5	Prohibitions – these rules clarify a variety of acts, omissions or other events that constitute a violation of the CAA, relative to the acid rain monitoring provisions in Part 75.	✓			Quarterly EDRs, periodic inspection of CEMS Monitoring Plans.

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4?		Comments	Methods Used to Demonstrate Compliance[1]
		Yes	No		
40 CFR 75.6	Incorporates several ASTM, ASME and other methods by reference.	✓		Not an applicable standard or limitation; however, information does apply when evaluating other applicable requirements.	
40 CFR 75.10	The owner or operator shall install, certify, operate, and maintain, in accordance with all the requirements of this part, a continuous emission monitoring system for SO2, NOx, and CO2, volumetric stack flow and opacity.	✓		Specific requirements in this part. Refer to full text of rule.	Retain records of all activities specified.
40 CFR 75.11 – 75.14	Specific provisions for monitoring SO2, NOx and CO2 emissions, stack diluent (O2 or CO2), stack flow and opacity.	✓		Specific and extensive provisions. MidAmerican Energy will ensure that CEMS meet these requirements.	CEMS Monitoring Plan (required under §75.53) and CEMS certification report. Retain records of all activities specified.
40 CFR 75.15	Specific provisions for monitoring SO2 emissions removal by qualifying Phase I technology. This generally applies to units in existence during calendar years 1997 through 1999.		✓	The SO2 removal system planned for Unit 4 does not meet the definition of a qualifying Phase I technology. Therefore, this rule does not apply.	
40 CFR 75.16	Special provisions for monitoring SO2 emissions from (and determining heat input for) common, bypass and multiple stacks.		✓	The generating units at CBEC (including Unit 4) have separate stacks. Therefore, this rule does not apply.	
40 CFR 75.17	Special provisions for monitoring NOX from common, bypass and multiple stacks.		✓	The generating units at CBEC (including Unit 4) have separate stacks. Therefore, this rule does not apply.	
40 CFR 75.18	Special provisions for monitoring opacity from common and bypass stacks.		✓	The generating units at CBEC (including Unit 4) have separate stacks. Therefore, this rule does not apply.	

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Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4?		Comments	Methods Used to Demonstrate Compliance[1]
		Yes	No		
40 CFR 75.19	Optional SO2, NOx and CO2 emissions calculation for low mass emission units.		✓	Coal-fired boilers do not qualify as low mass emission units. Therefore, these rules do not apply. In addition, the rule does not apply to auxiliary boilers, diesel fire pumps, etc.	
40 CFR 75.20	The owner or operator shall ensure that each continuous emission or opacity monitoring system required by this part meets the initial certification and recertification requirements of this section and shall ensure that all applicable initial certifications and recertifications are completed by the deadlines specified.	✓		Initial certification tests must be conducted for all CEMs, in accordance with this section and Appendix A of this Part.	Copies of initial certification and recertification testing reports will be submitted to EPA and IDNR, retained on file at MidAmerican Energy. Retain records of all certification tests and activities.
40 CFR 75.21	Details quality control and quality assurance requirements.	✓		The CEMS must be operated and maintained in accordance with this section and Appendix B of this Part.	Retain records of all QA/QC activities specified.
40 CFR 75.22	Reference Test Methods.	✓		Identifies the EPA Reference Test Methods (provided in Appendix A of 40 CFR Part 60) that shall be used for certification tests, calibrations and other measurements.	Certification and periodic audit reports will be retained on file at MidAmerican Energy.
40 CFR 75.23	Alternatives to standards incorporated by reference.		✓	MidAmerican Energy has no plans to petition the Administrator for an alternative to any standard incorporated by reference, pursuant to §75.66(c).	

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 75.24	Out-of-Control periods and adjustment for system bias.	✓		Out-of-control periods can be declared, based on daily calibration, quarterly audit or linearity check results. During these periods, the data is considered not QA'ed and shall not be used in calculating monitor availability.	QA/QC information transmitted with quarterly EDR.
40 CFR 75.30 – 75. 37	Subpart D – Missing Data Substitution procedures.	✓		This Subpart provides extensive guidance and requirements for substituting a variety of empirically derived emissions values, which are usually much higher than actual emissions, during periods when the CEMS does not accurately measure SO2, NOx, CO2, heat input and moisture.	Substituted data are identified in the quarterly EDR.
40 CFR 75.40 – 75.48	Guidelines for using an alternative monitoring system, which must have the same or better precision, reliability, accessibility and timeliness as that provided by a CEMS meeting the requirements of this Part.		✓	CBEC will not use alternative monitoring system; therefore, these rules do not apply.	
40 CFR 70.53	Specific guidelines and requirements for CEMS Monitoring Plans.	✓		These provisions are very specific and extensive. Refer to full text of rule.	Monitoring Plan submittal, pursuant to §75.62.
40 CFR 75.54	General recordkeeping provisions.		✓	This rule applies to facilities in existence prior to 04/01/2000. Unit 4 will be constructed after that date; therefore this rule does not apply.	
40 CFR 75.55	Recordkeeping provisions for specific situations.		✓	This rule applies to facilities in existence prior to 04/01/2000. Unit 4 will be constructed after that date; therefore this rule does not apply.	

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Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 75.56	Certification, QA/QC record provisions.		✓	This rule applies to facilities in existence prior to 04/01/2000. Unit 4 will be constructed after that date; therefore this rule does not apply.	
40 CFR 75.57	General recordkeeping provisions.	✓		These provisions are very specific and extensive. Refer to full text of rule. All records of measurements, data, reports and other information required under Part 75 shall be maintained in a file at the plant, suitable for agency inspection, for a minimum of 3 years.	CEMS records on file at the plant, available for EPA/ IDNR inspection.
40 CFR 75.58	General recordkeeping provisions for specific situations.		✓	This section provides recordkeeping provisions for alternative or parametric monitoring allowed for gaseous or liquid fuel-fired units only. Unit 4 is coal-fired; therefore this rule does not apply.	
40 CFR 75.59	Certification, QA/QC record provisions.	✓		These provisions are very specific and extensive. Refer to full text of rule.	CEMS Monitoring Plan, quarterly EDRs, certification reports, RATA test reports, CEMS O&M records maintained at CBEC.
40 CFR 75.60	Reporting Requirements – General Provisions.	✓		This section details the schedules and criteria for the submittal of initial certification reports, recertification reports, monitoring plans, EDRs, RATA reports and other communications. In addition, provisions governing the confidentiality of data are provided.	Copies of these submittals will be kept on file at the plant for a minimum of 3 years.

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Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 75.61	Reporting Requirements – Notifications.	✓		This section details the schedules and criteria for notifying the EPA and IDNR of planned testing dates, installation of new units, retiring units, changes in fuels used or monitoring system components.	Records of notifications will be maintained at the plant, in a file suitable for agency inspection for a minimum of 3 years.
40 CFR 75.62	Monitoring plan submittals.	✓		This section details the schedules and criteria for submittal of the electronic and hardcopy CEMS Monitoring Plan, including any revisions to the Monitoring plan.	Records of the Monitoring Plan submittals will be maintained at the plant, in a file suitable for agency inspection for a minimum of 3 years.
40 CFR 75.63	Initial certification or recertification application submittals.	✓		This section details the schedules and criteria for the submittal of initial certification reports and recertification applications.	Records of the certification and recertification submittals will be maintained at the plant, in a file suitable for agency inspection for a minimum of 3 years.

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Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 75.64	Quarterly Electronic Data Reports.	✓		This section details the content and submittal format requirements for the submission of CEMS measurements data, along with a variety of QA/QC activities and results for the preceding calendar quarter. Each EDR is due on or before the 30^{th} calendar day following the end of the subject calendar quarter.	Electronic copies of each EDR will be maintained at the plant, in a file suitable for agency inspection for a minimum of 3 years.
40 CFR 75.65	Opacity reports.	✓		This section requires that excess opacity emissions measured by the CEMS be reported to the local APCD (in this case, IDNR)	Copies of excess opacity reports submitted to IDNR will be maintained at the plant, in a file suitable for agency inspection for a minimum of 3 years.
40 CFR 75.66	Petitions to the Administrator.	✓		This section provides the procedures for petitioning the EPA for alternatives to the monitoring requirements of Part 75. MidAmerican Energy has no current plan to petition for alternative monitoring arrangements.	
40 CFR 75.67	Retired units petitions.		✓	This section applies to combustion sources seeking to enter the Opt-in Program and then retired (creating an availability of SO2 allowances for use by other sources). MidAmerican Energy has no such qualifying units; therefore this rule does not apply.	

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 75.70 – 75.75	Subpart H - NOx Mass Emissions Provisions.		✓	This section, which was added when the federal acid rain program NOx limitations were revised, clarifies the source obligations for units subject to a state or federal NOx mass emissions reduction program. However, CBEC plant is not subject to such a state or federal program (other than the federal acid rain NOx limitations); therefore this rule does not apply. It is presumed that IDNR permit limits for NOx mass emissions (e.g. lbs/hour or tons/year) do not constitute a "state reduction program".	
40 CFR 76, Nitrogen Oxides					
40 CFR 76.1 – 76.4	Definitions and general information regarding 40 CFR 76.		✓	Not an applicable standard or limitation; however, these definitions do apply when evaluating other applicable requirements.	
40 CFR 76.5 – 76.6	NOX limitations for Group I, Phase I boilers and for Group II boilers.		✓	Unit 4 will be considered a Group I Phase II boiler; therefore, these rules do not apply.	
40 CFR 76.7	The owner or operator of a Group 1, Phase II coal-fired utility unit with a tangentially fired boiler or a dry bottom wall-fired boiler shall not discharge, or allow to be discharged, emissions of NOX to the atmosphere in excess of the following limits, except as provided in §§ 76.8, 76.10, or 76.11: (1) 0.40 lb/mmBtu of heat input on an annual average basis for tangentially fired boilers. (2) 0.46 lb/ mmBtu of heat input on an annual average basis for dry bottom wall-fired boilers (other than units applying cell burner technology).	✓		CBEC may not discharge emissions greater than what is allowed.	CEMS documentation.

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Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 76.8	The owner or operator of a Phase II coal-fired utility unit with a Group 1 boiler may elect to have the unit become subject to the applicable emissions limitation for NOX under § 76.5, starting no later than January 1, 1997.		✓	Not applicable. Unit 4 is not yet constructed.	
40 CFR 76.9	The designated representative of any source with an affected unit subject to this part shall submit, by the applicable deadline under paragraph (b) of this section, a complete Acid Rain permit application (or, if the unit is covered by an Acid Rain permit, a complete permit revision) that includes a complete compliance plan for NOX emissions covering the unit.	✓		MidAmerican Energy has already obtained a Title IV permit that is included as part of the Title V permit. A modification will be applied for separately to account for the addition of Unit 4.	Permit was received and is retained. A separate acid rain application will be submitted to accommodate for the addition of Unit 4.
40 CFR 76.10	The designated representative of an affected unit that is not an early election unit and cannot meet the applicable emission limitation, for Group 1 boilers, either low NOX burner technology or an alternative or, for tangentially fired boilers, separated overfire air, may petition the permitting authority for an alternative emission limitation less stringent than the applicable emission limitation.		✓	Unit 4 will be able to meet the applicable emission limitation; therefore, this rule does not apply.	
40 CFR 76.11	Details emissions averaging plan.		✓	CBEC units 1-3 have a Phase 1 NOx early election plan. CBEC Unit 4 will be subject to standards for Phase 2, Group 1 boilers.	
40 CFR 76.12	Details Phase I NOX compliance extension.		✓	CBEC units 1-3 have a Phase 1 NOx early election plan. CBEC Unit 4 will be subject to standards for Phase 2, Group 1 boilers.	
40 CFR 76.13	Provides calculations for excess emissions of nitrogen oxides.	✓		If Unit 4 has excess emissions of NOx, the guidelines detailed in this section must be followed.	If NOx is ever exceeded, document actions required by this section.

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Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 76.14 – 76.15	Details requirements for alternative monitoring equipment and alternative emission limitations.		✓	CBEC will not have either alternative; therefore, these rules do not apply.	
40 CFR 77, Excess Emissions					
40 CFR 77.01 – 77.06	This part of the Acid Rain Regulations specifies the requirements for addressing excess emissions of SO_2 (exceeding allowances).	✓		If MidAmerican Energy has excess emissions of sulfur dioxide in any calendar year it shall be liable to offset the amount of such excess emissions by an equal amount of allowances from the unit's Allowance Tracking System account in accordance with these rules.	If emissions are ever exceeded, the requirements set forth in these rules will be followed and documentation retained.
40 CFR 78, Appeal Procedures for Acid Rain Program					
40 CFR 78	Guidelines and requirements for Acid Rain Program Appeals.	✓		This section provides the procedure for appealing under the Acid Rain program. MidAmerican does not have any appeals planned at this time, but the procedures would be applicable to any future appeals.	
40 CFR 79, Registration of Fuels and Fuel Additives					
40 CFR 79	Guidelines and requirements for the registration of fuels and fuel additives.		✓	CBEC does not produce fuels or fuel additives; therefore, this rule does not apply.	
40 CFR 80, Regulation of Fuels and Fuel Additives					

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Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 80	Guidelines and requirements for the production and distribution of fuels and fuel additives.		✓	CBEC does not produce fuels or fuel additives; therefore, this rule does not apply.	
40 CFR 81, Designation of Areas for Air Quality Planning Purposes					
40 CFR 81	Administrative guidelines and requirements.		✓	This rule applies to regulators, and is not an obligation of CBEC.	
40 CFR 82, Protection of Stratospheric Ozone					
40 CFR 82	Administrative guidelines and requirements.		✓	This rule applies to regulators, and is not an obligation of CBEC.	
40 CFR 85, Control of Air Pollution From Mobile Sources					
40 CFR 85	Guidelines and requirements for mobile sources.		✓	This rule applies to automobile manufacturers, distributors and emissions certifications; therefore, it does not apply to CBEC.	
40 CFR 86, Control of Emissions From New and In-Use Highway Vehicles and Engines					
40 CFR 86	Guidelines and requirements for highway vehicles and engines.		✓	Guidelines and requirements for highway vehicles and engines.	
40 CFR 87, Control of Air Pollution From Aircraft and Aircraft Engines					
40 CFR 87	Guidelines and requirements for aircraft and engines.		✓	CBEC does not own or produce aircraft or aircraft engines; therefore, these rules do not apply.	
40 CFR 88, Clean-Fuel Vehicles					

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Council Bluffs Energy Center Unit 4
Federal Air Quality Regulation Review

Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 88	Guidelines and requirements for clean fuel vehicles.		✓	Guidelines for manufacturers of clean fuel vehicles; therefore, this rule does not apply to CBEC.	
40 CFR 89, Control of Emissions From New and In-Use Nonroad Compression-Ignition Engines					
40 CFR 89	Guidelines and requirements for nonroad compression-ignition engines.		✓	CBEC does not own or operate nonroad compression-ignition engines; therefore, this rule does not apply.	
40 CFR 90, Control of Emissions From Nonroad Spark-Ignition Engines					
40 CFR 90	Guidelines and requirements for nonroad spark-ignition engines.		✓	CBEC does not own or operate nonroad spark-ignition engines; therefore, this rule does not apply.	
40 CFR 91, Control of Emissions From Marine Spark-Ignition Engines					
40 CFR 91	Guidelines and requirements for marine spark-ignition engines.		✓	CBEC does not own or operate marine spark-ignition engines; therefore, this rule does not apply.	
40 CFR 92, Control of Air Pollution From Locomotives and Locomotive Engines					
40 CFR 92	Guidelines and requirements for locomotives and locomotive engines.		✓	CBEC does not own or operate locomotives or locomotive engines; therefore, this rule does not apply.	
40 CFR 93, Determining Conformity of Federal Actions to State or Federal Implementation Plans					
40 CFR 93	Guidelines for determining conformity of federal actions to SIP.		✓	This rule applies to federal agencies and is not an obligation of CBEC.	
40 CFR 94, Control of Air Pollution From Marine Compression-Ignition Engines					

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Applicable Requirement	Summary of Requirement	Applicable to Unit 4? Yes	No	Comments	Methods Used to Demonstrate Compliance[1]
40 CFR 94	Guidelines and requirements for marine compression-ignition engines.		✓	CBEC does not own or operate marine compression-ignition engines; therefore, this rule does not apply.	
40 CFR 95, Mandatory Patent Licenses					
40 CFR 95	Guidelines and requirements for mandatory patent licenses.		✓	CBEC is not required to obtain a patent; therefore, this rule does not apply.	
40 CFR 96, NOx Budget Trading Program for State Implementation Plans					
40 CFR 96	Authorizes States to implement a NOx trading program.		✓	CBEC is not trading NOx credits; therefore, this rule does not apply.	
40 CFR 97, Federal NOx Budget Trading Program					
40 CFR 97	Provisions for the federal NOx Budget Trading Program.		✓	CBEC is not trading NOx credits; therefore, this rule does not apply.	
Notes: The summary of applicable requirements is intended to provide a summary of the portion of the applicable requirement applying to the generating units. It is not intended to replace a regulatory document. Please see the actual regulations for specific information.					

CBEC4 Project	
BPIP and ISC-PRIME Input/Output Files	
/ISC-PRIME_BPIP	
Unit 4 Load Analysis	
CB_LOAD_87_CO	ISC-PRIME input (.DTA) and output (.LST) files for CO load analysis (100%, 75%, 50% loads) with 1987 meteorological data
CB_LOAD_88_CO	ISC-PRIME input (.DTA) and output (.LST) files for CO load analysis (100%, 75%, 50% loads) with 1988 meteorological data
CB_LOAD_89_CO	ISC-PRIME input (.DTA) and output (.LST) files for CO load analysis (100%, 75%, 50% loads) with 1989 meteorological data
CB_LOAD_90_CO	ISC-PRIME input (.DTA) and output (.LST) files for CO load analysis (100%, 75%, 50% loads) with 1990 meteorological data
CB_LOAD_91_CO	ISC-PRIME input (.DTA) and output (.LST) files for CO load analysis (100%, 75%, 50% loads) with 1991 meteorological data
CB_LOAD_87_SO2	ISC-PRIME input (.DTA) and output (.LST) files for SO2 load analysis (100%, 75%, 50% loads) with 1987 meteorological data
CB_LOAD_88_SO2	ISC-PRIME input (.DTA) and output (.LST) files for SO2 load analysis (100%, 75%, 50% loads) with 1988 meteorological data
CB_LOAD_89_SO2	ISC-PRIME input (.DTA) and output (.LST) files for SO2 load analysis (100%, 75%, 50% loads) with 1989 meteorological data
CB_LOAD_90_SO2	ISC-PRIME input (.DTA) and output (.LST) files for SO2 load analysis (100%, 75%, 50% loads) with 1990 meteorological data
CB_LOAD_91_SO2	ISC-PRIME input (.DTA) and output (.LST) files for SO2 load analysis (100%, 75%, 50% loads) with 1991 meteorological data
CB_LOAD_87_PM	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 load analysis (100%, 75%, 50% loads) with 1987 meteorological data
CB_LOAD_88_PM	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 load analysis (100%, 75%, 50% loads) with 1988 meteorological data
CB_LOAD_89_PM	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 load analysis (100%, 75%, 50% loads) with 1989 meteorological data
CB_LOAD_90_PM	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 load analysis (100%, 75%, 50% loads) with 1990 meteorological data
CB_LOAD_91_PM	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 load analysis (100%, 75%, 50% loads) with 1991 meteorological data
Unit 4 Preliminary Analysis	
CB_PRE_87_CO	ISC-PRIME input (.DTA) and output (.LST) files for CO preliminary analysis with 1987 meteorological data
CB_PRE_88_CO	ISC-PRIME input (.DTA) and output (.LST) files for CO preliminary analysis with 1988 meteorological data
CB_PRE_89_CO	ISC-PRIME input (.DTA) and output (.LST) files for CO preliminary analysis with 1989 meteorological data
CB_PRE_90_CO	ISC-PRIME input (.DTA) and output (.LST) files for CO preliminary analysis with 1990 meteorological data
CB_PRE_91_CO	ISC-PRIME input (.DTA) and output (.LST) files for CO preliminary analysis with 1991 meteorological data
CB_PRE_87_SO2	ISC-PRIME input (.DTA) and output (.LST) files for SO2 preliminary analysis with 1987 meteorological data
CB_PRE_88_SO2	ISC-PRIME input (.DTA) and output (.LST) files for SO2 preliminary analysis with 1988 meteorological data
CB_PRE_89_SO2	ISC-PRIME input (.DTA) and output (.LST) files for SO2 preliminary analysis with 1989 meteorological data
CB_PRE_90_SO2	ISC-PRIME input (.DTA) and output (.LST) files for SO2 preliminary analysis with 1990 meteorological data
CB_PRE_91_SO2	ISC-PRIME input (.DTA) and output (.LST) files for SO2 preliminary analysis with 1991 meteorological data
CB_PRE_87_NOx	ISC-PRIME input (.DTA) and output (.LST) files for NOx preliminary analysis with 1987 meteorological data
CB_PRE_88_NOx	ISC-PRIME input (.DTA) and output (.LST) files for NOx preliminary analysis with 1988 meteorological data
CB_PRE_89_NOx	ISC-PRIME input (.DTA) and output (.LST) files for NOx preliminary analysis with 1989 meteorological data
CB_PRE_90_NOx	ISC-PRIME input (.DTA) and output (.LST) files for NOx preliminary analysis with 1990 meteorological data
CB_PRE_91_NOx	ISC-PRIME input (.DTA) and output (.LST) files for NOx preliminary analysis with 1991 meteorological data
CB_PRE_91_NOx_FINE	ISC-PRIME input (.DTA) and output (.LST) files for NOx preliminary analysis with 1991 meteorological data (fine grid)
CB_PRE_PM_87	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 preliminary analysis with 1987 meteorological data
CB_PRE_PM_88	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 preliminary analysis with 1988 meteorological data
CB_PRE_PM_89	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 preliminary analysis with 1989 meteorological data
CB_PRE_PM_90	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 preliminary analysis with 1990 meteorological data
CB_PRE_PM_91	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 preliminary analysis with 1991 meteorological data

CBEC4 Project	
BPIP and ISC-PRIME Input/Output Files	
CBEC Lead (Pb) Analysis	
CB_Pb_87_1	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1987 meteorological data (1st quarter)
CB_Pb_87_2	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1987 meteorological data (2nd quarter)
CB_Pb_87_3	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1987 meteorological data (3rd quarter)
CB_Pb_87_4	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1987 meteorological data (4th quarter)
CB_Pb_88_1	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1988 meteorological data (1st quarter)
CB_Pb_88_2	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1988 meteorological data (2nd quarter)
CB_Pb_88_3	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1988 meteorological data (3rd quarter)
CB_Pb_88_4	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1988 meteorological data (4th quarter)
CB_Pb_89_1	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1989 meteorological data (1st quarter)
CB_Pb_89_2	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1989 meteorological data (2nd quarter)
CB_Pb_89_3	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1989 meteorological data (3rd quarter)
CB_Pb_89_4	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1989 meteorological data (4th quarter)
CB_Pb_90_1	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1990 meteorological data (1st quarter)
CB_Pb_90_2	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1990 meteorological data (2nd quarter)
CB_Pb_90_3	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1990 meteorological data (3rd quarter)
CB_Pb_90_4	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1990 meteorological data (4th quarter)
CB_Pb_91_1	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1991 meteorological data (1st quarter)
CB_Pb_91_2	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1991 meteorological data (2nd quarter)
CB_Pb_91_3	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1991 meteorological data (3rd quarter)
CB_Pb_91_4	ISC-PRIME input (.DTA) and output (.LST) files for Pb analysis with 1991 meteorological data (4th quarter)

CBEC4 Project	
BPIP and ISC-PRIME Input/Output Files	
Full-Impact Analysis for SO_2 and PM-10	
CB_INC_SO2_87	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 increment consumption with 1987 meteorological data
CB_INC_SO2_88	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 increment consumption with 1988 meteorological data
CB_INC_SO2_89	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 increment consumption with 1989 meteorological data
CB_INC_SO2_90	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 increment consumption with 1990 meteorological data
CB_INC_SO2_91	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 increment consumption with 1991 meteorological data
CB_INC_SO2_ReducedGrid_87	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 increment consumption with 1987 meteorological data (reduced grid)
CB_INC_SO2_ReducedGrid_88	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 increment consumption with 1988 meteorological data (reduced grid)
CB_INC_SO2_ReducedGrid_89	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 increment consumption with 1989 meteorological data (reduced grid)
CB_INC_SO2_ReducedGrid_90	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 increment consumption with 1990 meteorological data (reduced grid)
CB_INC_SO2_ReducedGrid_91	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 increment consumption with 1991 meteorological data (reduced grid)
CB_NAAQS_SO2_87	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 NAAQS with 1987 meteorological data
CB_NAAQS_SO2_88	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 NAAQS with 1988 meteorological data
CB_NAAQS_SO2_89	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 NAAQS with 1989 meteorological data
CB_NAAQS_SO2_90	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 NAAQS with 1990 meteorological data
CB_NAAQS_SO2_91	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 NAAQS with 1991 meteorological data
CB_NAAQS_SO2_ReducedGrid_87	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 increment consumption with 1987 meteorological data (reduced grid)
CB_NAAQS_SO2_ReducedGrid_88	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 increment consumption with 1988 meteorological data (reduced grid)
CB_NAAQS_SO2_ReducedGrid_89	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 increment consumption with 1989 meteorological data (reduced grid)
CB_NAAQS_SO2_ReducedGrid_90	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 increment consumption with 1990 meteorological data (reduced grid)
CB_NAAQS_SO2_ReducedGrid_91	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 increment consumption with 1991 meteorological data (reduced grid)
CB_INC_PM_87	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 increment consumption with 1987 meteorological data
CB_INC_PM_88	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 increment consumption with 1988 meteorological data
CB_INC_PM_89	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 increment consumption with 1989 meteorological data
CB_INC_PM_90	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 increment consumption with 1990 meteorological data
CB_INC_PM_91	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 increment consumption with 1991 meteorological data
CB_NAAQS_PM_87	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 NAAQS with 1987 meteorological data
CB_NAAQS_PM_88	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 NAAQS with 1988 meteorological data
CB_NAAQS_PM_89	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 NAAQS with 1989 meteorological data
CB_NAAQS_PM_90	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 NAAQS with 1990 meteorological data
CB_NAAQS_PM_91	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 NAAQS with 1991 meteorological data
CB_PRE_PM_ReducedGrid_87	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 significant impact with 1987 meteorological data (reduced grid)
CB_PRE_PM_ReducedGrid_88	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 significant impact with 1988 meteorological data (reduced grid)
CB_PRE_PM_ReducedGrid_89	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 significant impact with 1989 meteorological data (reduced grid)
CB_PRE_PM_ReducedGrid_90	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 significant impact with 1990 meteorological data (reduced grid)
CB_PRE_PM_ReducedGrid_91	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 significant impact with 1991 meteorological data (reduced grid)

CBEC4 Project	
BPIP and ISC-PRIME Input/Output Files	
NAAQS Analysis for Auxiliary Equipment (short-term PM-10 and SO_2)	
CB_AUXFULL_87_[PM10]	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 NAAQS with 1987 meteorological data (CBEC4 aux equip only)
CB_AUXFULL_88_[PM10]	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 NAAQS with 1988 meteorological data (CBEC4 aux equip only)
CB_AUXFULL_89_[PM10]	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 NAAQS with 1989 meteorological data (CBEC4 aux equip only)
CB_AUXFULL_90_[PM10]	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 NAAQS with 1990 meteorological data (CBEC4 aux equip only)
CB_AUXFULL_91_[PM10]	ISC-PRIME input (.DTA) and output (.LST) files for PM-10 NAAQS with 1991 meteorological data (CBEC4 aux equip only)
CB_AUXFULL_87_SO2	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 NAAQS with 1987 meteorological data (CBEC4 aux equip only)
CB_AUXFULL_88_SO2	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 NAAQS with 1988 meteorological data (CBEC4 aux equip only)
CB_AUXFULL_89_SO2	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 NAAQS with 1989 meteorological data (CBEC4 aux equip only)
CB_AUXFULL_90_SO2	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 NAAQS with 1990 meteorological data (CBEC4 aux equip only)
CB_AUXFULL_91_SO2	ISC-PRIME input (.DTA) and output (.LST) files for SO_2 NAAQS with 1991 meteorological data (CBEC4 aux equip only)
Receptor Files	
CB_30KM.REC	Base receptor grid for ISC-PRIME modeling
FINE_NOX.REC	100-meter grid used to refine preliminary analysis for NOx
PM_ROI.REC	Radius of impact grid for PM-10
SO2_ROI.REC	Radius of impact grid for SO2
PM_HIGH.REC	High impact receptors for PM-10 increment
SO2_REDUCED.REC	CBEC4 significant impact receptors for SO2
BPIP Files	
CB_NAAQS_PM.PIP	BPIP input file from PM-10 NAAQS model run (includes CBEC and Bunge)
CB_NAAQS_PM.SO	ISC-ready output from BPIP
CB_NAAQS_PM.SUM	BPIP summary output file
CB_NAAQS_PM.TAB	BPIP detailed output file
Graphics (XYZ) Files	
CB_PRE_87_SO2.GRF	XYZ plot file from preliminary SO2 analysis used to determine significant receptors for CBEC4 (1987)
CB_PRE_88_SO2.GRF	XYZ plot file from preliminary SO2 analysis used to determine significant receptors for CBEC4 (1988)
CB_PRE_89_SO2.GRF	XYZ plot file from preliminary SO2 analysis used to determine significant receptors for CBEC4 (1989)
CB_PRE_90_SO2.GRF	XYZ plot file from preliminary SO2 analysis used to determine significant receptors for CBEC4 (1990)
CB_PRE_91_SO2.GRF	XYZ plot file from preliminary SO2 analysis used to determine significant receptors for CBEC4 (1991)
CB_INC_PM_87.GRF	XYZ plot file from PM-10 increment analysis used to determine high receptors for outside sources (1987)
CB_INC_PM_88.GRF	XYZ plot file from PM-10 increment analysis used to determine high receptors for outside sources (1988)
CB_INC_PM_89.GRF	XYZ plot file from PM-10 increment analysis used to determine high receptors for outside sources (1989)
CB_INC_PM_90.GRF	XYZ plot file from PM-10 increment analysis used to determine high receptors for outside sources (1990)
CB_INC_PM_91.GRF	XYZ plot file from PM-10 increment analysis used to determine high receptors for outside sources (1991)
Meteorological Input Data	
1494287a.ASC	Meteorological input file for ISC-PRIME (Omaha NWS data, 1987)
1494288a.ASC	Meteorological input file for ISC-PRIME (Omaha NWS data, 1988)
1494289a.ASC	Meteorological input file for ISC-PRIME (Omaha NWS data, 1989)
1494290a.ASC	Meteorological input file for ISC-PRIME (Omaha NWS data, 1990)
1494291a.ASC	Meteorological input file for ISC-PRIME (Omaha NWS data, 1991)

CBEC4 Project	
VISCREEN and SACTI Files	
/VISCREEN	
VIS_CBM2.OUT	Detailed VISCREEN output file for Council Bluffs Municipal Airport
VIS_CBM2.SUM	Summary VISCREEN output file for Council Bluffs Municipal Airport
VIS_LCM2.OUT	Detailed VISCREEN output file for Lewis and Clark Monument
VIS_LCM2.SUM	Summary VISCREEN output file for Lewis and Clark Monument
VIS_LMP2.OUT	Detailed VISCREEN output file for Lake Manawa State Park
VIS_LMP2.SUM	Summary VISCREEN output file for Lake Manawa State Park
VIS_MNW2.OUT	Detailed VISCREEN output file for Mingo Nat Wildlife Refuge
VIS_MNW2.SUM	Summary VISCREEN output file for Mingo Nat Wildlife Refuge
VIS_WTN2.OUT	Detailed VISCREEN output file for Wabash Trace Nature Trail
VIS_WTN2.SUM	Summary VISCREEN output file for Wabash Trace Nature Trail
/SACTI	
CBEC4a.xls	Excel Input data file - Used to create input files required by individual modules
CBECe.INP	Input data file - Used by the PREP module
CBECe90.OUT	Standard output file - Created by the TABLES module - Summarizes input/output data
CBECe90b.bin	Internal binary file -Created by the PREP module - Contains information for data tables
CBECe90F9.txt	Formatted output file - Created by the TABLES module - Input to spreadsheet program
CBECe90out.txt	Standard output file - Created by the PREP module - Summarizes input/output data
CBECe90p.txt	Internal data file - Created by the PREP module - Used by the PLUME module
CBECe90t.txt	Internal data file - Created by the PREP module - Used by the TABLES module
MH90.dat	Mixing Height Data for SACTI Modeling CD1440 format (Omaha WSFO #94918, 1990)
MidAm5.INP	Input data file - Used by the PLUME module
MidAm590out.TXT	Standard output file - Created by the PLUME module - Summarizes input/output data
MidAm590t.TXT	Internal data file - Created by the PLUME module - Used by the TABLES module
Omah90sf.dat	SAMSON metdata file 1990 surface data (Omaha WSFO #94918, 1990)
Omah90up.dat	EPA mixing height 1990 data file (Omaha WSFO #94918, 1990)
surf90.dat	Surface Data for SACTI Modeling CD1440 format (Omaha WSFO #94918, 1990)

CBEC: Material Handling Point Sources

EPN	Description	Height Above Grade (Feet)	Height Above Grade (Meters)	Duct Size (Feet)	Exhaust Area (ft^2)	Duct Size (Feet)	Duct Size (Meters)	Stack Test (actual flow, ACFM)	Stack Test EV (ft/sec)	Stack Test EV (m/s)	Rated Velocity (ft/s)	Rated Velocity (m/s)	Temp. (°F)	Temp. (K)
EP-6_7	Emissions from dust collection system exhaust fan - Dumper Building.	90	27.43		36.67	6.83	2.08				68.17	20.78	Ambient	293
EP-9	Emissions from dust collection system exhaust fan - Transfer House 1.	11.5	3.51		6.70	2.92	0.89	22,261	55.4	16.9	52.07	15.87	Ambient	293
EP-10	Emissions from dust collection system exhaust fan - Transfer House 2.	12	3.66		8.30	3.25	0.99	30,946	62.2	18.9	49.22	15.00	Ambient	293
EP-11	Emissions from dust collection system exhaust fan - Transfer House 3.	12	3.66		6.70	2.92	0.89	19,947	49.6	15.1	52.57	16.02	Ambient	293
EP-13	Emissions from dust collection system exhaust fan - Transfer House 4 (Crusher House).	50	15.24		8.30	3.25	0.99				54.07	16.48	Ambient	293
EP-14	Emissions from dust collection system exhaust fan - East Coal Silos Bay Unit 3.	193	58.82		7.07	3.00	0.91	21,948	51.8	15.8	62.50	19.05	Ambient	293
EP-15	Emissions from dust collection system exhaust fan - West Coal Silos Bay Unit 3.	193	58.82		7.07	3.00	0.91	18,813	44.4	13.5	53.90	16.43	Ambient	293
EP-16	Emissions from dust collection system exhaust fan - Crusher House Units 1 and 2.	12	3.66		3.98	2.25	0.69				49.91	15.21	Ambient	293
EP-17	Emissions from dust collection system exhaust fan - Coal Silos Units 1 and 2.	127	38.71		8.30	3.25	0.99				53.04	16.17	Ambient	293
EP-20	Emissions from fly ash truck loading vent filter Fly ash Silo Unit 3.	13	3.96		2.19	1.67	0.51				9.17	2.79	Ambient	293
EP-21	Emissions from fly ash truck loading vent filter Fly ash Silo Units 1 and 2.	13	3.96		2.19	1.67	0.51				9.17	2.79	Ambient	293
EP-119A	Emissions from silo bag vent filter Fly Ash Storage Silo Units 1 and 2.	13	3.96	1.67 x 0.75	1.25	1.26	0.38				43.00	13.11	Ambient	293
EP-119B	Emissions from silo bag vent filter Fly Ash Storage Silo Units 1 and 2.	64	19.51	1.67 x 0.75	1.25	1.26	0.38				43.00	13.11	Ambient	293
EP-159	Emissions from dust collection system exhaust fan - Transfer Conveyor Bay.	305	92.96		4.91	2.50	0.76				66.67	20.32	Ambient	293
EP-160	Emissions from dust collection system exhaust fan - East Silos Bay Unit 4.	305	92.96		8.71	3.33	1.01				66.67	20.32	Ambient	293
EP-161	Emissions from dust collection system exhaust fan - West Silos Bay Unit 4.	305	92.96		6.51	2.88	0.88				66.67	20.32	Ambient	293

CBEC: Material Handling Point Sources

EPN	Description	Height Above Grade (Feet)	Height Above Grade (Meters)	Duct Size (Feet)	Exhaust Area (ft^2)	Duct Size (Feet)	Duct Size (Meters)	Stack Test (actual flow, ACFM)	Stack Test EV (ft/sec)	Stack Test EV (m/s)	Rated Velocity (ft/s)	Rated Velocity (m/s)	Temp. (°F)	Temp. (K)
EP-162	Emissions from lime filter separator vacuum exhauster - Unit 4.	12	3.66		0.54	0.83	0.25				60.00	18.29	Ambient	293
EP-163	Emissions from lime silo bag vent filter Unit 4.	90	27.43		2.16	1.66	0.51				11.46	3.49	Ambient	293
EP-164A	Emissions from urea silo # 1bag vent filter Unit 4.	40	12.19		0.79	1.00	0.30				8.33	2.54	Ambient	293
EP-164B	Emissions from urea silo # 2 bag vent filter Unit 4.	40	12.19		0.79	1.00	0.30				8.33	2.54	Ambient	293
EP-167	Emissions from Flyash/FGD waste silo bag vent filter Unit 4	100	30.48		3.14	2.00	0.61				15.92	4.85	Ambient	293
EP-168	Emissions from fly ash/FGD waste vacuum system exhauster # 1 - Unit 4.	12	3.66		0.79	1.00	0.30				53.00	16.15	Ambient	293
EP-169	Emissions from fly ash/FGD waste vacuum system exhauster # 2 - Unit 4.	12	3.66		0.79	1.00	0.30				53.00	16.15	Ambient	293
EP-170	Emissions from fly ash/FGD waste vacuum system exhauster # 3 - Unit 4.	12	3.66		0.79	1.00	0.30				53.00	16.15	Ambient	293

from Don M (MEC, 8/27/02): EP-10 flow should be 24,500 ACFM, diam = 39", ht = 12'
from Don M (MEC, 8/27/02): EP-17 flow should be 26,400 ACFM, diam = 39", ht = 127'

TABLE D-1
NSR RACT/BACT/LAER Clearinghouse Database
BACT-PSD Sources for CO
Coal Fired Boilers

RBLC ID	Company Name and Location	# of Units	Unit and Size	Control Technology	Control Efficiency	Emission Limit		Permit Date and Permit No.
MO-0050	Kansas City Power & Light Co. Hawthorn Station Kansas City, Missouri	1	Coal Fired Boiler 384 TPH	Good Combustion Practices	not given	0.16	lb/MMBTU	8/17/1999 No. 888
WY-0039	Two Elk Generation Partners, LTD Wright, Wyoming	1	Pulverized Coal Fired Boiler 250 MW	No Controls Feasible	not given	0.15	lb/MMBTU	2/27/1998 No. CT-1352
WY-0047	ENCOAL Corporation North Rochelle Facility 15 miles SE Wright, Wyoming	1	Pulverized Coal Fired Boiler 3960 MMBTU/HR 240 MW	Combustion Technology	not given	0.15	lb/MMBTU	10/10/1997 No. CT-1324
WY-0048	Black Hills Power and Light Company Wygen Plant Gillette, Wyoming	1	Pulverized Coal Fired Boiler 80 MW	No Controls Feasible	not given	0.15	lb/MMBTU	9/6/1996 No. CT-1236
PA-0133	Mon Valley Energy LTD Poland Mines, Pennsylvania	1	Pulverized Coal Fired Boiler 966 MMBTU/hr 80 MW Cogen	No Controls Feasible	not given	Primary = .20 lb/MMBTU	Secondary = 847 TPY	8/8/1995 No. 30-306-001
NJ-0019	Crown/Vista Energy Project (CVEP) West Deptford, New Jersey	2	Pulverized Coal Fired Boilers 1789 MMBTU/hr each 181 MW each	Good Combustion Practice	not given	Primary = .11 lb/MMBTU	Secondary = 100 ppmvd @ 7%O_2	10/1/1993 No. 01-92-0857
VA-0213	SEI Birchwood King George, Virginia SIC Code: 4931	1	Pulverized Coal Fired Boiler 2200 MMBTU/hr	Combustion Technology	not given	Primary = 440 lb/hr	Secondary = 1927 TPY	8/23/1993 No.40809
WY-0046	Black Hills Power and Light Company Neil Simpson Plant Gillette, Wyoming	1	Pulverized Coal Fired Boiler Steam Electric Power 80 MW	Combustion Control	not given	Primary = .15 lb/MMBTU	Secondary = 152.0 lb/hr	4/14/1993 No. CT-1028
MI-0228	INDELK Energy Services of Otsego Michigan	1	Coal Fired Boiler 778 MMBTU/HR	Combustion Control	not given	0.10	lb/MMBTU	3/16/1993 No. 143-90
NC-0057	Roanoke Valley Project II Weldon Township, North Carolina	1	Pulverized Coal Fired Boiler 517 MMBTU/hr	Combustion Technology	not given	0.20	lb/MMBTU	11/20/1992 No. 6964R2
SC-0027	South Carolina Electric and Gas Company Cope, South Carolina	3	Pulverized Coal Fired Boiler Units 1, 2 and 3 385 MW each	Combustion Efficiency	not given	0.15	lb/MMBTU	7/15/1992 No. 1860-0044
FL-0044	Orlando Utilities Commission Stanton Energy Center, Unit 2 Orlando, Florida	1	Pulverized Coal Fired Boiler 4286 MMBTU/HR	Combustion Control	not given	0.15	lb/MMBTU	12/23/1991

TABLE D-1
NSR RACT/BACT/LAER Clearinghouse Database
BACT-PSD Sources for CO
Coal Fired Boilers

RBLC ID	Company Name and Location	# of Units	Unit and Size	Control Technology	Control Efficiency	Emission Limit		Permit Date and Permit No.
NJ-0015	Keystone Cogeneration Systems, Inc. New Jersey	1	Pulverized Coal Fired Boiler 2116 MMBTU/hr	Advanced Combustion Control	not given	0.11	lb/MMBTU	9/6/1991 No.01-89-3983
VA-0181	Old Dominion Electric Cooperative Clover, Virginia	1	Coal Fired Boiler 4085 MMBTU/hr (≈ 400 MW)	Boiler Design	not given	0.10	lb/MMBTU	4/29/1991 No. 30867
NC-0054	Roanoke Valley Project Weldon, North Carolina	1	Pulverized Coal Fired Boiler 1700 MMBTU/HR	Combustion Control	not given	0.20	lb/MMBTU	1/24/1991 No. 6964
NJ-0014	Chambers Cogeneration Limited Partnership Carneys Point, New Jersey	2	Pulverized Coal Fired Boiler 1389 MMBTU/hr each	Advanced Combustion Control	not given	0.11	lb/MMBTU	12/26/1990 No. 01-89-3086
SC-0028	Santee Cooper Public Service Authority Moncks Corner, South Carolina	1	Pulverized Coal Fired Boiler Cross Unit No. 1 5200 MMBTU/hr (500 MW)	Combustion Efficiency	not given	0.10	lb/MMBTU	11/28/1990 No. 0420-0030
VA-0171	Mecklenburg Cogeneration Limited Mecklenburg, Virginia	4	Pulverized Coal Fired Boiler 834.5 MMBTU/hr each	Good Combustion Practices	not given	Primary = .20 lb/MMBTU	Secondary = 166.9 lb/hr	5/9/1990 No. 30861

Notes:
NSR RACT/BACT/LAER Clearinghouse database (http://www.epa.gov/ttn/catc) was queried for the following:
- RBLC Determinations added during or after January 1990
- SIC Code: 4911
- Process Type Code: 11.002 - Coal Combustion
- BACT-PSD

TABLE D-2
NSR RACT/BACT/LAER Clearinghouse Database
BACT-PSD Sources for VOC
Coal Fired Boilers

RBLC ID	Company Name and Location	# of Units	Unit and Size	Control Technology	Control Efficiency	Emission Limit		Permit Date and Permit No.
MO-0050	Kansas City Power & Light Co. Hawthorn Station Kansas City, Missouri	1	Coal Fired Boiler 384 TPH	Good Combustion Practices	not given	0.0036	lb/MMBTU	8/17/1999 No. 888
WY-0039	Two Elk Generation Partners, LTD Wright, Wyoming	1	Pulverized Coal Fired Boiler 250 MW	No Controls Feasible	not given	0.015	lb/MMBTU	2/27/1998 No. CT-1352
WY-0047	ENCOAL Corporation North Rochelle Facility 15 miles SE Wright, Wyoming	1	Pulverized Coal Fired Boiler 3960 MMBTU/HR 240 MW	Combustion Technology	not given	0.05	lb/MMBTU	10/10/1997 No. CT-1324
WY-0048	*Black Hills Power and Light Company* Wygen Plant Gillette, Wyoming	1	*Pulverized Coal Fired Boiler* 80 MW	*No Controls Feasible*	*not given*	0.015	lb/MMBTU	9/6/1996 No. CT-1236
PA-0133	Mon Valley Energy LTD Poland Mines, Pennsylvania	1	Pulverized Coal Fired Boiler 966 MMBTU/hr 80 MW Cogen	No Controls Feasible	not given	Primary = 0.01 lb/MMBTU	Secondary = 42.3 TPY	8/8/1995 No. 30-306-001
NJ-0019	Crown/Vista Energy Project (CVEP) West Deptford, New Jersey	2	Pulverized Coal Fired Boilers 1789 MMBTU/hr each 181 MW each	Good Combustion Practice	not given	Primary = .0031 lb/MMBTU	Secondary = 4.5 ppmvd @ 7%O_2	10/1/1993 No. 01-92-0857 Methane
VA-0213	SEI Birchwood *King George, Virginia* SIC Code: 4931	1	Pulverized Coal Fired Boiler *2200 MMBTU/hr*	Combustion Technology	not given	Primary = 22 lb/hr	Secondary = 96.4 TPY	8/23/1993 No.40809
WY-0046	Black Hills Power and Light Company Neil Simpson Plant Gillette, Wyoming	1	Pulverized Coal Fired Boiler 80 MW	Combustion Control	not given	Primary = 0.015 lb/MMBTU	Secondary = 15.0 lb/hr	4/14/1993 No. CT-1028
MI-0228	INDELK Energy Services of Otsego Michigan	1	Coal Fired Boiler 778 MMBTU/HR	Combustion Control	not given	0.01	lb/MMBTU	3/16/1993 No. 143-90
NC-0057	Roanoke Valley Project II Weldon Township, North Carolina	1	Pulverized Coal Fired Boiler 517 MMBTU/hr	Combustion Technology	not given	0.03	lb/MMBTU	11/20/1992 No. 6964R2
SC-0027	South Carolina Electric and Gas Company Cope, South Carolina	3	Pulverized Coal Fired Boiler Units 1, 2 and 3 385 MW each	Combustion Efficiency	not given	0.01	lb/MMBTU	7/15/1992 No. 1860-0044
FL-0044	Orlando Utilities Commission Stanton Energy Center, Unit 2 Orlando, Florida	1	Pulverized Coal Fired Boiler 4286 MMBTU/HR	Combustion Control	not given	0.015	lb/MMBTU	12/23/1991
NJ-0015	Keystone Cogeneration Systems, Inc. New Jersey	1	Coal Fired Boiler 2116 MMBTU/hr	Advanced Combustion Control	not given	0.0036	lb/MMBTU	9/6/1991 No.01-89-3983

TABLE D-2
NSR RACT/BACT/LAER Clearinghouse Database
BACT-PSD Sources for VOC
Coal Fired Boilers

RBLC ID	Company Name and Location	# of Units	Unit and Size	Control Technology	Control Efficiency	Emission Limit		Permit Date and Permit No.
VA-0181	Old Dominion Electric Cooperative Clover, Virginia	1	Coal Fired Boiler 4085 MMBTU/hr (≈ 400 MW)	Boiler Design	not given	0.01	lb/MMBTU	4/29/1991 No. 30867
NC-0054	Roanoke Valley Project Weldon, North Carolina	1	Pulverized Coal Fired Boiler 1700 MMBTU/HR	Combustion Control	not given	0.03	lb/MMBTU	1/24/1991 No. 6964
NJ-0014	Chambers Cogeneration Limited Partnership Carneys Point, New Jersey	2	Pulverized Coal Fired Boiler 1389 MMBTU/hr each	Advanced Combustion Control	not given	0.0036	lb/MMBTU	12/26/1990 No. 01-89-3086
SC-0028	Santee Cooper Public Service Authority Moncks Corner, South Carolina	1	Pulverized Coal Fired Boiler Cross Unit No. 1 5200 MMBTU/hr (500 MW)	Combustion Efficiency	not given	0.012	lb/MMBTU	11/28/1990 No. 0420-0030
VA-0171	Mecklenburg Cogeneration Limited Mecklenburg, Virginia	4	Pulverized Coal Fired Boiler 834.5 MMBTU/hr each	Good Combustion Practices	not given	Primary = 0.0027 lb/MMBTU	Secondary = 2.3 lb/hr	5/9/1990 No. 30861

Notes:
NSR RACT/BACT/LAER Clearinghouse database (http://www.epa.gov/ttn/catc) was queried for the following:
- RBLC Determinations added during or after January 1990
- SIC Code: 4911
- Process Type Code: 11.002 - Coal Combustion
- BACT-PSD

TABLE D-3
NSR RACT/BACT/LAER Clearinghouse Database
BACT-PSD Sources for PM
Coal Fired Boilers

RBLC ID	Company Name and Location	# of Units	Unit and Size	Control Technology	Control Efficiency	Emission Limit		Permit Date and Permit No.
WY-0039	Two Elk Generation Partners, LTD Wright, Wyoming	1	Pulverized Coal Fired Boiler 250 MW	Fabric Filter	99.50%	0.02	lb/MMBTU	2/27/1998 No. CT-1352
WY-0047	ENCOAL Corporation North Rochelle Facility 15 miles SE Wright, Wyoming	1	Pulverized Coal Fired Boiler 3960 MMBTU/HR 240 MW	Fabric Filter	99%	0.02	lb/MMBTU	10/10/1997 No. CT-1324
WY-0048	Black Hills Power and Light Company Wygen Plant Gillette, Wyoming	1	Pulverized Coal Fired Boiler 80 MW	Electrostatic Precipitator	99%	0.02	lb/MMBTU	9/6/1996 No. CT-1236
NJ-0019	Crown/Vista Energy Project (CVEP) West Deptford, NJ	2	Pulverized Coal Fired Boilers 1789 MMBTU/hr each 181 MW each	Fabric Filters	99.9%	Primary = 32.2 lb/hr	Secondary = 0.018 lb/MMBTU	10/1/1993 No. 01-92-0857
VA-0213	SEI Birchwood King George, VA SIC Code: 4931	1	Pulverized Coal Fired Boiler 2200 MMBTU/hr	Fabric Filter	99.9%	Primary = 44 lb/hr	Secondary = 192.7 TPY	8/23/1993 No.40809
WY-0046	Black Hills Power and Light Company Neil Simpson Plant Gillette, Wyoming	1	Pulverized Coal Fired Boiler 80 MW	Electrostatic Precipitator	99%	Primary = .02 lb/MMBTU	Secondary = 20.0 lb/hr	4/14/1993 No. CT-1028
MI-0228	INDELK Energy Services of Otsego Michigan	1	Coal Fired Boiler 778 MMBTU/HR	Fabric Filter	99.9%	0.03	lb/MMBTU	3/16/1993 No. 143-90
NC-0057	Roanoke Valley Project II Weldon Township, NC	1	Pulverized Coal Fired Boiler 517 MMBTU/hr	Fabric Filter	99.75%	0.02	lb/MMBTU	11/20/1992 No. 6964R2
SC-0027	South Carolina Electric and Gas Company Cope, South Carolina	3	Pulverized Coal Fired Boiler 385 MW each	Fabric Filters	99.5%	0.02	lb/MMBTU	7/15/1992 No. 1860-0044
FL-0044	Orlando Utilities Commission Stanton Energy Center, Unit 2 Orlando, Florida	1	Pulverized Coal Fired Boiler 4286 MMBTU/HR	Electrostatic Precipitator	not given	0.02	lb/MMBTU	12/23/1991
VA-0181	Old Dominion Electric Cooperative Clover, Virginia	1	Coal Fired Boiler 4085 MMBTU/hr (400 MW)	Fabric Filter	99.9%	0.02	lb/MMBTU	4/29/1991 No. 30867
NC-0054	Roanoke Valley Project Weldon, North Carolina	1	Pulverized Coal Fired Boiler 1700 MMBTU/HR	Fabric Filter	99%	0.02	lb/MMBTU	1/24/1991 No. 6964

TABLE D-3
NSR RACT/BACT/LAER Clearinghouse Database
BACT-PSD Sources for PM
Coal Fired Boilers

RBLC ID	Company Name and Location	# of Units	Unit and Size	Control Technology	Control Efficiency	Emission Limit		Permit Date and Permit No.
SC-0028	Santee Cooper Public Service Authority Moncks Corner, South Carolina	1	Pulverized Coal Fired Boiler Cross Unit No. 1 5200 MMBTU/hr (500 MW)	Electrostatic Precipitator	99.5%	0.03	lb/MMBTU[1]	11/28/1990 No. 0420-0030
VA-0171	Mecklenburg Cogeneration Limited, Mecklenburg, VA	4	Pulverized Coal Fired Boiler 834.5 MMBTU/hr each	Fabric Filters	99.9%	Primary = .02 lb/MMBTU	Secondary = 16.7 lb/hr	5/9/1990 No. 30861

Notes:
[1] - Listed in database as 0.25 lb/MMBTU, changed to 0.03 lb/MMBTU per phone conversation with Joe Eller and Larry Ragsdale, South Carolina Department of Health and Environmental Control on April 4, 2001.

NSR RACT/BACT/LAER Clearinghouse database (http://www.epa.gov/ttn/catc/) was queried for the following:
- RBLC Determinations added during or after January 1990
- SIC Code: 4911
- Process Type Code: 11.002 - Coal Combustion
- BACT-PSD

TABLE D-4
NSR RACT/BACT/LAER Clearinghouse Database
BACT-PSD Sources for PM_{10}
Coal Fired Boilers

RBLC ID	Company Name and Location	# of Units	Unit and Size	Control Technology	Control Efficiency	Emission Limit		Permit Date and Permit No.
MO-0050	Kansas City Power & Light Co. Hawthorn Station Kansas City, Missouri	1	Coal Fired Boiler 384 TPH	Fabric Filter	not given	0.018	lb/MMBTU	8/17/1999 No. 888
FL-0178	JEA Northside Generating Station Jacksonville, Florida	1	Coal Fired Boiler 2764 MMBTU/hr	Fabric Filter or Electrostatic Precipitator	not given	0.011	lb/MMBTU	7/14/1999 No.PSD-FL-265
UT-0053	Deseret Generation and Transmission Company Near Bonanza, Utah	1	Coal Fired Boiler 500 MW	Fabric Filter	99.8%	0.0286	lb/MMBTU[1]	3/16/1998 No. DAQE-186-98
PA-0133	Mon Valley Energy LTD Poland Mines, Pennsylvania	1	Pulverized Coal Fired Boiler (Unit 2) 966 MMBTU/hr (97 MW)	Fabric Filter	99.95%	Primary = 0.15 lb/MMBTU	Secondary = 63.5 TPY	8/8/1995 No. 30-306-001
NJ-0019	Crown/Vista Energy Project (CVEP) West Deptford, New Jersey	2	Pulverized Coal Fired Boilers 1789 MMBTU/hr each 181 MW each	Fabric Filters	99.9%	Primary = 32.2 lb/hr	Secondary = 0.018 lb/MMBTU	10/1/1993 No. 01-92-0857
VA-0213	SEI Birchwood King George, Virginia SIC Code: 4931	1	Pulverized Coal Fired Boiler 2200 MMBTU/hr	Fabric Filter	99.9%	Primary = 39.6 lb/hr	Secondary = 173.5 TPY	8/23/1993 No.40809
NC-0057	Roanoke Valley Project II Weldon Township, North Carolina	1	Pulverized Coal Fired Boiler 517 MMBTU/hr	Fabric Filter	99.75%	0.018	lb/MMBTU	11/20/1992 No. 6964R2
SC-0027	South Carolina Electric and Gas Company Cope, South Carolina	3	Pulverized Coal Fired Boiler 385 MW each	Fabric Filters	99.5%	0.018	lb/MMBTU	7/15/1992 No. 1860-0044
FL-0044	Orlando Utilities Commission Stanton Energy Center, Unit 2 Orlando, Florida	1	Pulverized Coal Fired Boiler 4286 MMBTU/HR	Electrostatic Precipitator	not given	0.02	lb/MMBTU	12/23/1991
NJ-0015	Keystone Cogeneration Systems, Inc. New Jersey	1	Coal Fired Utility Boiler 2116 MMBTU/hr	Fabric Filter	99.9%	0.018	lb/MMBTU	9/6/1991 No.01-89-3983
VA-0181	Old Dominion Electric Cooperative Clover, Virginia	1	Coal Fired Boiler 4085 MMBTU/hr (400 MW)	Fabric Filter	99.9%	0.018	lb/MMBTU	4/29/1991 No. 30867
NC-0054	Roanoke Valley Project Weldon, North Carolina	1	Pulverized Coal Fired Boiler 1700 MMBTU/HR	Fabric Filter	99%	0.018	lb/MMBTU	1/24/1991 No. 6964
NJ-0014	Chambers Cogeneration Limited Partnership Carneys Point, New Jersey	2	Pulverized Coal Fired Boiler 1389 MMBTU/hr each	Fabric Filters	99.9%	0.018	lb/MMBTU	12/26/1990 No. 01-89-3086

TABLE D-4
NSR RACT/BACT/LAER Clearinghouse Database
BACT-PSD Sources for PM_{10}
Coal Fired Boilers

RBLC ID	Company Name and Location	# of Units	Unit and Size	Control Technology	Control Efficiency	Emission Limit		Permit Date and Permit No.
SC-0028	Santee Cooper Public Service Authority Moncks Corner, South Carolina	1	Pulverized Coal Fired Boiler Cross Unit No. 1 5200 MMBTU/hr (500 MW)	Electrostatic Precipitator	99.5%	0.023	lb/MMBTU	11/28/1990 No. 0420-0030
VA-0171	Mecklenburg Cogeneration Limited Mecklenburg, Virginia	4	Pulverized Coal Fired Boiler 834.5 MMBTU/hr each	Fabric Filters	99.9%	Primary = 0.018 lb/MMBTU	Secondary = 15.0 lb/hr	5/9/1990 No. 30861

Notes:
[1] - Listed in database as 0.286 lb/MMBTU, changed to 0.0286 lb/MMBTU per conversation with Tim Blanchard, Utah Department of Environmental Quality on April 4, 2001.

NSR RACT/BACT/LAER Clearinghouse database (http://www.epa.gov/ttn/catc) was queried for the following:
- RBLC Determinations added during or after January 1990
- SIC Code: 4911
- Process Type Code: 11.002 - Coal Combustion
- BACT-PSD

TABLE D-5
NSR RACT/BACT/LAER Clearinghouse Database
BACT-PSD Sources for PM
Cooling Towers

RBLC ID	Company Name and Location	# of Units	Unit and Size	Control Technology	Control Efficiency	Emission Limit		Permit Date and Permit No.
NJ-0019	Crown/Vista Energy Project (CVEP) West Deptford, New Jersey	2	Pulverized Coal Fired Boilers 1789 MMBTU/hr each 181 MW each	Drift Eliminator	0.001% of Circulation Water	5.9	lb/hr	10/1/1993 No. 01-92-0857
FL-0050	Florida Power Corporation Crystal River, Florida	4	735,000 gallons/hour Salt Water	Drift Eliminator	0.004% of Circulation Water	0.0040%	of Circulation Water	8/30/1990 No. PSD-FL-139

Notes:
NSR RACT/BACT/LAER Clearinghouse database (http://www.epa.gov/ttn/catc/) was queried for the following:
- RBLC Determinations added during or after January 1990
- SIC Code: 4931
- Process Type Code: 99.009 - Cooling Tower
- BACT-PSD

TABLE D-6
NSR RACT/BACT/LAER Clearinghouse Database
BACT-PSD Sources for Lead
Coal Fired Boilers

RBLC ID	Company Name and Location	# of Units	Unit and Size	Control Technology	Control Efficiency	Emission Limit		Permit Date and Permit No.
NJ-0019	Crown/Vista Energy Project (CVEP) West Deptford, New Jersey	2	Pulverized Coal Fired Boilers 1789 MMBTU/hr each 181 MW each	Spray Dryer Absorber and Fabric Filter	93.0%	0.03	lb/hr	10/1/1993 No. 01-92-0857
VA-0213	SEI Birchwood, Inc. King George, Virginia	1	Pulverized Coal Fired Boiler 2,200 MMBTU/HR	Lime Spray Dryer Absorber and Fabric Filter	95.0%	Primary = 0.2 lb/hr	Secondary = 0.9 TPY	8/23/1993 No. 40809
VA-0181	Old Dominion Electric Cooperative Clover, Virginia	1	Coal Fired Boiler 4085 MMBTU/hr (400 MW)	FGD and Fabric Filter	99.9%*	Primary = 0.00042 lb/mmbtu	Secondary = 7.5 TPY	4/29/1991 No. 30867
SC-0028	Santee Cooper Public Service Authority Moncks Corner, South Carolina	1	Pulverized Coal Fired Boiler Cross Unit No. 1 5200 MMBTU/hr (500 MW)	Limestone FGD and Electrostatic Precipitator	75.0%	0.00033	lb/MMBTU	11/28/1990 No. 0420-0030

Notes:
* Control Efficiency for Fabric Filter

NSR RACT/BACT/LAER Clearinghouse database (http://www.epa.gov/ttn/catc/) was queried for the following:
• RBLC Determinations added during or after January 1990
• Pollutant name - Pb
• Process Name Contains Coal

TABLE D-7
NSR RACT/BACT/LAER Clearinghouse Database
BACT-PSD Sources for Fluorides
Coal Fired Boilers

RBLC ID	Company Name and Location	# of Units	Unit and Size	Control Technology	Control Efficiency	Emission Limit		Permit Date and Permit No.
NJ-0019	Crown/Vista Energy Project (CVEP) West Deptford, New Jersey	2	Pulverized Coal Fired Boilers 1789 MMBTU/hr each 181 MW each	Spray Dryer Absorber and Fabric Filter	93%	4.31	lb/hr	10/1/1993 No. 01-92-0857
VA-0213	SEI Birchwood, Inc. King George, Virginia	1	Pulverized Coal Fired Boiler 2,200 MMBTU/HR	Lime Spray Dryer Absorber and Fabric Filter	94%*	3.6	lb/hr	8/23/1993 No. 40809
SC-0027	South Carolina Electric and Gas Company Cope, South Carolina	3	Pulverized Coal Fired Boiler 385 MW each	Spray Dryer Absorber and Fabric Filter	93%*	0.01	lb/MMBTU	7/15/1992 No. 1860-0044
NC-0054	Roanoke Valley Project Weldon, North Carolina	1	Pulverized Coal Fired Boiler 1700 MMBTU/HR	Lime Spray Dryer Absorber and Fabric Filter	90%	0.000538	lb/MMBTU	1/24/1991 No. 6964
SC-0028	Santee Cooper Public Service Authority Moncks Corner, South Carolina	1	Pulverized Coal Fired Boiler Cross Unit No. 1 5200 MMBTU/hr (500 MW)	Limestone FGD and Electrostatic Precipitator	82%	0.01	lb/MMBTU	11/28/1990 No. 0420-0030
VA-0165	Hadson Power II Southampton, Virginia	2	Coal Fired Boiler 379 MMBTU/HR each	Spray Dryer Absorber and Fabric Filter	92%*	9.7	lb/day	1/1/1990 No. 61093

Notes:
* Control Efficiency for SO_2 FGD System

NSR RACT/BACT/LAER Clearinghouse database (http://www.epa.gov/ttn/catc/) was queried for the following:
• RBLC Determinations added during or after January 1990
• Pollutant name - Fluoride
• Process Name Contains Coal

TABLE D-8
NSR RACT/BACT/LAER Clearinghouse Database
BACT-PSD Sources for SO_2
Coal Fired Boilers

RBLC ID	Company Name and Location	# of Units	Unit and Size	Control Technology	Control Efficiency	Emission Limit		Permit Date and Permit No.
MO-0050	Kansas City Power & Light Co. Hawthorn Station Kansas City, Missouri	1	Coal Fired Boiler 384 TPH	Dry FGD and Low Sulfur Coal	not given	0.12	lb/MMBTU 30-day average	8/17/1999 No. 888
FL-0178	JEA Northside Generating Station Jacksonville, Florida	1	Coal Fired Boiler 2764 MMBTU/hr	Circulating Fluidized Bed Scrubber or Spray Dryer Absorber	not given	0.20	lb/MMBTU	7/14/1999 No.PSD-FL-265
PA-0162	Edison Mission Energy Homer City, Pennsylvania	1	Pulverized Coal Fired Boiler Unit 3 6600 MMBTU/hr	Wet Limestone FGD	92%	0.40	lb/MMBTU	5/25/1999 No. 32-0055C
UT-0053	Deseret Generation and Transmission Company Near Bonanza, Utah	1	Coal Fired Boiler 500 MW	Wet Limestone FGD	90%	0.0976	lb/MMBTU 12-month average	3/16/1998 No. DAQE-186-98
WY-0039	Two Elk Generation Partners, LTD Wright, Wyoming	1	Pulverized Coal Fired Boiler 250 MW	Lime Spray Dryer	91%	0.20	lb/MMBTU 2-hour fixed	2/27/1998 No. CT-1352
WY-0047	ENCOAL Corporation North Rochelle Facility 15 miles SE Wright, Wyoming	1	Pulverized Coal Fired Boiler 3960 MMBTU/HR 240 MW	Lime Spray Dryer	73%	0.20	lb/MMBTU 2-hour fixed	10/10/1997 No. CT-1324
WY-0048	Black Hills Power and Light Company *Wygen Plant* Gillette, Wyoming	1	Pulverized Coal Fired Boiler 80 MW	Circulating Dry Scrubber	80% **	0.20	lb/MMBTU 2-hour rolling	9/6/1996 No. CT-1236
PA-0133	Mon Valley Energy LTD Poland Mines, Pennsylvania	1	Pulverized Coal Fired Boiler 966 MMBTU/hr 80 MW Cogen	Spray Dryer Absorber	92%	0.25	lb/MMBTU	8/8/1995 No. 30-306-001
NJ-0019	Crown/Vista Energy Project (CVEP) West Deptford, New Jersey	2	Pulverized Coal Fired Boilers 1789 MMBTU/hr each 181 MW each	Spray Dryer Absorber	93%	0.18	lb/MMBTU	10/1/1993 No. 01-92-0857
VA-0213	SEI Birchwood King George, Virginia SIC Code: 4931	1	Pulverized Coal Fired Boiler 2200 MMBTU/hr	Lime Spray Dryer	94%	220	lb/hr	8/23/1993 No.40809
WY-0046	Black Hills Power and Light Company Neil Simpson Plant Gillette, Wyoming	1	Pulverized Coal Fired Boiler Steam Electric Power 80 MW	Circulating Dry Scrubber	80% **	0.20	lb/MMBTU 2-hour rolling	4/14/1993 No. CT-1028
MI-0228	INDELK Energy Services of Otsego Michigan	1	Coal Fired Boiler 778 MMBTU/HR	Dry Scrubber	90%	0.32	lb/MMBTU	3/16/1993 No. 143-90
NC-0057	Roanoke Valley Project II Weldon Township, North Carolina	1	Pulverized Coal Fired Boiler 517 MMBTU/hr	Dry Lime Scrubber	93%	0.187	lb/MMBTU	11/20/1992 No. 6964R2

TABLE D-8
NSR RACT/BACT/LAER Clearinghouse Database
BACT-PSD Sources for SO_2
Coal Fired Boilers

RBLC ID	Company Name and Location	# of Units	Unit and Size	Control Technology	Control Efficiency	Emission Limit		Permit Date and Permit No.
SC-0027	South Carolina Electric and Gas Company Cope, South Carolina	2	Pulverized Coal Fired Boiler Units 2 and 3 385 MW each	Spray Dryer Absorber	93%	0.17	lb/MMBTU	7/15/1992 No. 1860-0044
SC-0027	South Carolina Electric and Gas Company Cope, South Carolina	1	Pulverized Coal Fired Boiler Unit 1 385 MW each	Spray Dryer Absorber	93%	0.25	lb/MMBTU	7/15/1992 No. 1860-0044
FL-0044	Orlando Utilities Commission Stanton Energy Center, Unit 2 Orlando, Florida	1	Pulverized Coal Fired Boiler 4286 MMBTU/HR	Wet Lime FGD	92%	0.25	lb/MMBTU	12/23/1991
NJ-0015	Keystone Cogeneration Systems, Inc. New Jersey	1	Pulverized Coal Fired Boiler 2116 MMBTU/hr	Spray Dryer Absorber	93%	0.16	lb/MMBTU	9/6/1991 No.01-89-3983
VA-0181	Old Dominion Electric Cooperative Clover, Virginia	1	Coal Fired Boiler 4085 MMBTU/hr (= 400 MW)	FGD and 1.0-1.3% Bituminous Sulfur Coal	94%	0.10	lb/MMBTU	4/29/1991 No. 30867
NC-0054	Roanoke Valley Project Weldon, North Carolina	1	Pulverized Coal Fired Boiler 1700 MMBTU/HR	Dry Lime FGD	92%	0.213	lb/MMBTU	1/24/1991 No. 6964
NJ-0014	Chambers Cogeneration Limited Partnership Carneys Point, New Jersey	2	Pulverized Coal Fired Boiler 1389 MMBTU/hr each	Spray Dryer Absorber	93%	0.22	lb/MMBTU	12/26/1990 No. 01-89-3086
SC-0028	Santee Cooper Public Service Authority Moncks Corner, South Carolina	1	Pulverized Coal Fired Boiler Cross Unit No. 1 5200 MMBTU/hr (500 MW)	Promoted Limestone FGD	95%	0.34	lb/MMBTU	11/28/1990 No. 0420-0030
VA-0171	Mecklenburg Cogeneration Limited Mecklenburg, Virginia	4	Pulverized Coal Fired Boiler 834.5 MMBTU/hr each	Spray Dryer Absorber	92%	0.172	lb/MMBTU	5/9/1990 No. 30861

Notes:
NSR RACT/BACT/LAER Clearinghouse database (http://www.epa.gov/ttn/catc) was queried for the following:
- RBLC Determinations added during or after January 1990
- SIC Code: 4911
- Process Type Code: 11.002 - Coal Combustion
- *BACT-PSD*

** Control efficiency in RBLC is incorrect. Correct data suupplied by Fred Carl, Black Hills Corporation.

TABLE D-9
NSR RACT/BACT/LAER Clearinghouse Database
BACT-PSD Sources for NO_x
Coal Fired Boilers

RBLC ID	Company Name and Location	# of Units	Unit and Size	Control Technology	Control Efficiency	Emission Limit		Permit Date and Permit No.
MO-0050	Kansas City Power & Light Co. Hawthorn Station Kansas City, Missouri	1	Coal Fired Boiler 384 TPH	SCR and Good Combustion	not given	0.08	lb/MMBTU 30-day average	8/17/1999 No. 888
FL-0178	JEA Northside Generating Station Jacksonville, Florida	1	Coal Fired Boiler 2764 MMBTU/hr	SNCR	not given	0.09	lb/MMBTU 30-day rolling average	7/14/1999 No.PSD-FL-265
PA-0162	Edison Mission Energy Homer City, Pennsylvania	3	Pulverized Coal Fired Boiler Units 1 & 2 (5700 MMBTU/hr each) Unit 3 (6600 MMBTU/hr)	SCR	70%	0.15	lb/MMBTU	5/25/1999 No. 32-0055C
UT-0053	Deseret Generation and Transmission Company Near Bonanza, Utah	1	Coal Fired Boiler 500 MW	Boiler Design	99.6%	0.55	lb/MMBTU 30-day average	3/16/1998 No. DAQE-186-98
WY-0039	Two Elk Generation Partners, LTD Wright, Wyoming	1	Pulverized Coal Fired Boiler 250 MW	Low-NOx Burners, Overfire Air and SCR	75%	0.15	lb/MMBTU 30-day rolling average	2/27/1998 No. CT-1352
WY-0047	ENCOAL Corporation North Rochelle Facility 15 miles SE Wright, Wyoming	1	Pulverized Coal Fired Boiler 3960 MMBTU/HR 240 MW	Low NOx Burners with Flue Gas Recirculation	not given	0.16	lb/MMBTU	10/10/1997 No. CT-1324
WY-0048	Black Hills Power and Light Company Wygen Plant Gillette, Wyoming	1	Pulverized Coal Fired Boiler 80 MW	Low NOx Burners with Overfire Air	56%	0.22	lb/MMBTU	9/6/1996 No. CT-1236
PA-0133	Mon Valley Energy LTD Poland Mines, Pennsylvania	1	Pulverized Coal Fired Boiler 966 MMBTU/hr 80 MW Cogen	Low NOx Burners and SCR	50%	0.15	lb/MMBTU	8/8/1995 No. 30-306-001
NJ-0019	Crown/Vista Energy Project (CVEP) West Deptford, New Jersey	2	Pulverized Coal Fired Boilers 1789 MMBTU/hr each 181 MW each	Low NOx Burners and SCR	48%	0.17	lb/MMBTU	10/1/1993 No. 01-92-0857
VA-0213	SEI Birchwood King George, Virginia SIC Code: 4931	1	Pulverized Coal Fired Boiler 2200 MMBTU/hr	SCR	80%	330	lb/hr	8/23/1993 No.40809
WY-0046	Black Hills Power and Light Company Neil Simpson Plant Gillette, Wyoming	1	Pulverized Coal Fired Boiler Steam Electric Power 80 MW	Combustion Control	not given	0.23	lb/MMBTU 30-day rolling average	4/14/1993 No. CT-1028
MI-0228	INDELK Energy Services of Otsego Michigan	1	Coal Fired Boiler 778 MMBTU/HR	SNCR/Dry Control	50%	0.25	lb/MMBTU	3/16/1993 No. 143-90

TABLE D-9
NSR RACT/BACT/LAER Clearinghouse Database
BACT-PSD Sources for NO_x
Coal Fired Boilers

RBLC ID	Company Name and Location	# of Units	Unit and Size	Control Technology	Control Efficiency	Emission Limit		Permit Date and Permit No.
NC-0057	Roanoke Valley Project II Weldon Township, North Carolina	1	Pulverized Coal Fired Boiler 517 MMBTU/hr	Low NOx Burners, Advanced Overfire Air and SNCR	not given	0.17	lb/MMBTU	11/20/1992 No. 6964R2
SC-0027	South Carolina Electric and Gas Company *Cope, South Carolina*	3	Pulverized Coal Fired Boiler Units 1, 2 and 3 385 MW each	Low NOx Burners with Overfire Air	not given	0.32	lb/MMBTU	7/15/1992 No. 1860-0044
FL-0044	Orlando Utilities Commission Stanton Energy Center, Unit 2 Orlando, Florida	1	Pulverized Coal Fired Boiler 4286 MMBTU/HR	Low NOx Burners and SCR	70%	0.17	lb/MMBTU	12/23/1991
NJ-0015	Keystone Cogeneration Systems, Inc. New Jersey	1	Pulverized Coal Fired Boiler 2116 MMBTU/hr	SNCR or SCR	37%	0.17	lb/MMBTU	9/6/1991 No.*01-89-3983*
VA-0181	Old Dominion Electric Cooperative Clover, Virginia	1	Coal Fired Boiler 4085 MMBTU/hr (≈ 400 MW)	Low NOx Burners and Advanced Overfire Air	50%	0.30	lb/MMBTU	4/29/1991 No. 30867
NC-0054	Roanoke Valley Project *Weldon, North Carolina*	1	Pulverized Coal Fired Boiler *1700 MMBTU/HR*	Low NOx Burners and Advanced Overfire Air	not given	0.33	lb/MMBTU	1/24/1991 No. 6964
NJ-0014	Chambers Cogeneration Limited Partnership Carneys Point, New Jersey	2	Pulverized Coal Fired Boiler 1389 MMBTU/hr each	SCR	37%	0.17	lb/MMBTU	12/26/1990 No. 01-89-3086
SC-0028	Santee Cooper Public Service Authority Moncks Corner, *South Carolina*	1	Pulverized Coal Fired Boiler *Cross Unit No. 1* 5200 MMBTU/hr (500 MW)	Low NOx Burners	not given	0.39	lb/MMBTU	11/28/1990 No. 0420-0030
VA-0171	Mecklenburg Cogeneration Limited Mecklenburg, Virginia	4	Pulverized Coal Fired Boiler 834.5 MMBTU/hr each	Low NOx Burners and Advanced Overfire Air	45%	0.33	lb/MMBTU	5/9/1990 No. 30861

Notes:
NSR RACT/BACT/LAER Clearinghouse database (http://www.epa.gov/ttn/catc) was queried for the following:
- RBLC Determinations added during or after January 1990
- SIC Code: 4911
- Process Type Code: 11.002 - Coal Combustion
- BACT-PSD

Council Bluffs Energy Center Unit 4
Selective Catalytic Reduction
Cost Estimate

Capital Cost Factors

DIRECT COSTS	Cost Factors					
(1) Purchased Equipment						
(a) Basic Equipment and auxiliaries						
Capital Cost of SCR System				=	$	28,245,000
Capital Cost of Spare Catalyst	(Spare Catalyst not included)					
Total Capital Cost				=	$	28,245,000
(b) Instruments and controls [0.1 * (a)]	(Included in Purchased Equipment Costs)					
(c) Taxes [0.07(a)]	0.07	*	(a)	=	$	1,977,150
Total Equipment Cost (TEC)				=	$	30,222,150
(2) Construction Costs						
(a) Foundations and supports	(Included in Total Construction Costs)					
(b) Handling and Erection	(Included in Total Construction Costs)					
(c) Electrical	(Included in Total Construction Costs)					
(d) Piping	(Included in Total Construction Costs)					
(e) Insulation	(Included in Total Construction Costs)					
(f) Painting	(Included in Total Construction Costs)					
Total Construction Costs (TCC)				=	$	20,600,500
TOTAL DIRECT COSTS (TDC)	(TEC)	+	(TCC)	=	$	50,822,650
INDIRECT COSTS						
(3) Engineering and supervision	(Included in Total Indirect Costs)					
(4) Construction and field expenses	(Included in Total Indirect Costs)					
(5) Construction fee	(Included in Total Indirect Costs)					
(6) Start-up	(Included in Total Indirect Costs)					
(7) Performance test	(Included in Total Indirect Costs)					
TOTAL INDIRECT COSTS (TIC)				=	$	14,653,650
TOTAL DIRECT AND INDIRECT COSTS (TDIC)	(TDC)	+	(TIC)	=	$	65,476,300
(8) Contingency	(Included in Total Indirect Costs)					
TOTAL INSTALLED CAPITAL COSTS (TICC)				=	$	65,476,300

Council Bluffs Energy Center Unit 4
Selective Catalytic Reduction
Cost Estimate (continued)

Annualized Cost Factors

DIRECT COSTS	Cost Factors					
Fixed O&M Costs						
(1) Operating Labor	(Included in Total Fixed O&M Costs)					
(2) Supervisory Labor	(Included in Total Fixed O&M Costs)					
(3) Maintenance Labor	(Included in Total Fixed O&M Costs)					
(4) Parts and Materials	(Included in Total Fixed O&M Costs)					
Total Fixed O&M Costs				=	$	350,000
Variable O&M Costs						
(5) Ammonia Reagent Cost:				=	$	481,111
(6) Catalyst Replacement Cost:				=	$	1,095,556
(7) Auxiliary Power Cost:				=	$	1,015,556
Total Variable O&M Costs					$	2,592,222
TOTAL DIRECT COSTS (TDAC)				=	$	2,942,222
INDIRECT COSTS						
(8) Overhead	60%	of	Fixed O&M Costs	=	$	210,000
(9) Property Tax	1%	of	(TICC)	=	$	654,763
(10) Insurance	1%	of	(TICC)	=	$	654,763
(11) G&A Charges	2%	of	(TICC)	=	$	1,309,526
(12) Capital Recovery	0.110	*	(TICC - Catalyst Cost)	=	$	7,068,660
TOTAL INDIRECT COSTS (TIAC)				=	$	9,897,712
TOTAL ANNUALIZED COSTS		TDAC + TIAC		=	$	12,839,934
TOTAL TONS REMOVED PER YEAR (NO_x)				=		4,034
COST EFFECTIVENESS ($ per ton of pollutant removed)				=	$	3,183

Notes:

1) Cost factors - from OAQPS Control Cost Manual, Chapter 3

2) Capital Recovery Factor for System - Based on a 15-year equipment life and 7% interest rate, base cost excludes cost of catalyst because equipment life will be less than 15 years. Catalyst replacement included as an operating and maintenance cost.

3) Sargent & Lundy provided SCR purchased equipment cost, direct installation cost, indirect installation cost and annual fixed and variable O&M costs.

4) Cost effectiveness, $ per ton of NOx removed, based on SCR only. Does not include removal by Low NOx burners.

Council Bluffs Energy Center Unit 4
SCR NO_x Removal Calculation

Net Unit Output (nominal MW net)	750 MW	Provided by MidAmerican
Coal Heating Value =	8,000 Btu/lb	Provided by MidAmerican
Unit Capacity Factor =	100 %	Provided by MidAmerican
Annual Heat Input (at 100% CF) =	67,233,000 MMBtu/year	7,675 MMBtu/hr x 8760 hours x 100%
Annual Coal Use (at 100% CF) =	4,202,063 tons/year	Calculated
SCR Design Collection Efficiency =	60 %	Provided by Sargent & Lundy
NO_x Emission rate after Low Nox Burners =	0.20 lb/MMBtu	Provided by Sargent & Lundy
NO_x Emission rate after SCR (stack) =	0.08 lb/MMBtu	Provided by Sargent & Lundy
NO_x annual tons before SCR =	6,723 tons/year	Calculated
NO_x annual tons after SCR =	2,689 tons/year	Calculated
NO_x annual tons removed by SCR =	4,034 tons/year	Calculated

Council Bluffs Energy Center Unit 4
Dry Lime Flue Gas Desulfurization System
Cost Estimate

Capital Cost Factors

DIRECT COSTS	Cost Factors					
(1) Purchased Equipment						
(a) Basic Equipment and auxiliaries						
Capital Cost of Dry Scrubber System				=	$	27,358,000
Total Capital Cost				=	$	27,358,000
(b) Instruments and controls [0.1 * (a)]	(Included in Purchased Equipment Costs)					
(c) Taxes [0.07(a)]	0.07	*	(a)	=	$	1,915,060
Total Equipment Cost (TEC)				=	$	29,273,060
(2) Construction Costs						
(a) Foundations and supports	(Included in Total Construction Costs)					
(b) Handling and Erection	(Included in Total Construction Costs)					
(c) Electrical	(Included in Total Construction Costs)					
(d) Piping	(Included in Total Construction Costs)					
(e) Insulation	(Included in Total Construction Costs)					
(f) Painting	(Included in Total Construction Costs)					
(g) Buildings				=	$	1,200,000
Total Construction Costs (TCC)				=	$	23,581,000
TOTAL DIRECT COSTS (TDC)	(TEC)	+	(TCC)	=	$	52,854,060
INDIRECT COSTS						
(3) Engineering and supervision	(Included in Total Indirect Costs)					
(4) Construction and field expenses	(Included in Total Indirect Costs)					
(5) Construction fee	(Included in Total Indirect Costs)					
(6) Start-up	(Included in Total Indirect Costs)					
(7) Performance test	(Included in Total Indirect Costs)					
TOTAL INDIRECT COSTS (TIC)				=	$	14,921,700
TOTAL DIRECT AND INDIRECT COSTS (TDIC)	(TDC)	+	(TIC)	=	$	67,775,760
(8) Contingency	(Included in Total Indirect Costs)					
TOTAL INSTALLED CAPITAL COSTS (TICC)				=	$	67,775,760

Council Bluffs Energy Center Unit 4
Dry Lime Flue Gas Desulfurization System
Cost Estimate (continued)

Annualized Cost Factors

DIRECT COSTS	Cost Factors					
Fixed O&M Costs						
(1) Operating Labor	(Included in Total Fixed O&M Costs)					
(2) Supervisory Labor	(Included in Total Fixed O&M Costs)					
(3) Maintenance Labor	(Included in Total Fixed O&M Costs)					
(4) Parts and Materials	(Included in Total Fixed O&M Costs)					
Total Fixed O&M Costs				=	$	2,500,000
Variable O&M Costs						
(5) Lime Reagent Cost:				=	$	3,186,667
(6) FGD Waste Disposal Cost:				=	$	3,321,111
(7) Auxiliary Power Cost:				=	$	2,323,333
Total Variable O&M Costs					$	8,831,111
TOTAL DIRECT COSTS (TDAC)				=	$	11,331,111
INDIRECT COSTS						
(8) Overhead	60%	of	Fixed O&M Costs	=	$	1,500,000
(9) Property Tax	1%	of	(TICC)	=	$	677,758
(10) Insurance	1%	of	(TICC)	=	$	677,758
(11) G&A Charges	2%	of	(TICC)	=	$	1,355,515
(12) Capital Recovery	0.110	*	(TICC)	=	$	7,441,414
TOTAL INDIRECT COSTS (TIAC)				=	$	11,652,445
TOTAL ANNUALIZED COSTS		TDAC + TIAC		=	$	22,983,556
TOTAL TONS REMOVED PER YEAR (SO_2)				=		37,987
COST EFFECTIVENESS ($ per ton of pollutant removed)				=	$	605

Notes:

1) Cost factors - from OAQPS Control Cost Manual, Chapter 3

2) Capital Recovery Factor for System - Based on a 15-year equipment life and 7% interest rate

3) Sargent & Lundy provided Dry Lime FGD purchased equipment cost, direct installation cost, indirect installation cost and annual fixed and variable O&M costs.

Council Bluffs Energy Center Unit 4
Dry Lime FGD SO_2 Removal Calculation

Net Unit Output (nominal MW net)	750 MW	Provided by MidAmerican
Coal Heating Value =	8,000 Btu/lb	Provided by MidAmerican
Unit Capacity Factor =	100 %	Provided by MidAmerican
Annual Heat Input (at 100% CF) =	67,233,000 MMBtu/year	7,675 MMBtu/hr x 8760 hours x 100%
Annual Coal Use (at 100% CF) =	4,202,063 tons/year	Calculated
Design Coal Sulfur Content =	0.50 %	Provided by MidAmerican
Dry Lime FGD Design Collection Efficiency =	90.4 %	Provided by Sargent & Lundy
SO_2 emission rate before FGD =	1.25 lb/MMBtu	Provided by Sargent & Lundy
SO_2 annual tons before FGD =	42,021 tons/year	Calculated
SO_2 emission rate after FGD =	0.12 lb/MMBtu	Calculated based on 90.4% CE
SO_2 annual tons after FGD =	4,034 tons/year	Calculated based on 90.4% CE
SO_2 annual tons removed by FGD =	37,987 tons/year	Calculated

Council Bluffs Energy Center Unit 4
Wet Limestone Flue Gas Desulfurization System
Cost Estimate

Capital Cost Factors

DIRECT COSTS	Cost Factors					
(1) Purchased Equipment						
(a) Basic Equipment and auxiliaries						
Capital Cost of Wet Limestone Scrubber System				=	$	62,108,000
Total Capital Cost				=	$	62,108,000
(b) Instruments and controls [0.1 * (a)]	(Included in Purchased Equipment Costs)					
(c) Taxes [0.07(a)]	0.07	*	(a)	=	$	4,347,560
Total Equipment Cost (TEC)				=	$	66,455,560
(2) Construction Costs						
(a) Foundations and supports	(Included in Total Construction Costs)					
(b) Handling and Erection	(Included in Total Construction Costs)					
(c) Electrical	(Included in Total Construction Costs)					
(d) Piping	(Included in Total Construction Costs)					
(e) Insulation	(Included in Total Construction Costs)					
(f) Painting	(Included in Total Construction Costs)					
(g) Buildings				=	$	2,000,000
Total Construction Costs (TCC)				=	$	41,131,000
TOTAL DIRECT COSTS (TDC)	(TEC)	+	(TCC)	=	$	107,586,560
INDIRECT COSTS						
(3) Engineering and supervision	(Included in Total Indirect Costs)					
(4) Construction and field expenses	(Included in Total Indirect Costs)					
(5) Construction fee	(Included in Total Indirect Costs)					
(6) Start-up	(Included in Total Indirect Costs)					
(7) Performance test	(Included in Total Indirect Costs)					
TOTAL INDIRECT COSTS (TIC)				=	$	30,371,700
TOTAL DIRECT AND INDIRECT COSTS (TDIC)	(TDC)	+	(TIC)	=	$	137,958,260
(8) Contingency	(Included in Total Indirect Costs)					
TOTAL INSTALLED CAPITAL COSTS (TICC)				=	$	137,958,260

Council Bluffs Energy Center Unit 4
Wet Limestone Flue Gas Desulfurization System
Cost Estimate (continued)

Annualized Cost Factors

DIRECT COSTS	**Cost Factors**					
Fixed O&M Costs						
(1) Operating Labor	(Included in Total Fixed O&M Costs)					
(2) Supervisory Labor	(Included in Total Fixed O&M Costs)					
(3) Maintenance Labor	(Included in Total Fixed O&M Costs)					
(4) Parts and Materials	(Included in Total Fixed O&M Costs)					
Total Fixed O&M Costs				=	$	3,800,000
Variable O&M Costs						
(5) Limestone Reagent Cost:				=	$	1,280,000
(6) FGD Waste Disposal Cost:				=	$	2,225,556
(7) Auxiliary Power Cost:				=	$	3,271,111
Total Variable O&M Costs					$	6,776,667
TOTAL DIRECT COSTS (TDAC)				=	$	10,576,667
INDIRECT COSTS						
(8) Overhead	60%	of	Fixed O&M Costs	=	$	2,280,000
(9) Property Tax	1%	of	(TICC)	=	$	1,379,583
(10) Insurance	1%	of	(TICC)	=	$	1,379,583
(11) G&A Charges	2%	of	(TICC)	=	$	2,759,165
(12) Capital Recovery	0.110	*	(TICC)	=	$	15,147,075
TOTAL INDIRECT COSTS (TIAC)				=	$	22,945,406
TOTAL ANNUALIZED COSTS	TDAC + TIAC			=	$	33,522,072
TOTAL TONS REMOVED PER YEAR (SO_2)				=		39,920
COST EFFECTIVENESS ($ per ton of pollutant removed)				=	$	840

INCREMENTAL COST ANALYSIS BETWEEN DRY LIME FGD AND WET LIMESTONE FGD

INCREMENTAL ANNUALIZED COSTS (Wet Limestone FGD Total Annualized Costs - Dry Lime FGD Total Annualized Costs)	=	$	10,538,517
INCREMENTAL TONS OF SO2 REMOVED (Wet Limestone FGD - Dry Lime FGD)	=		1,933
INCREMENTAL COST EFFECTIVENESS ($ per ton of pollutant removed differential between Wet FGD and Dry FGD)	=	$	5,452
INCREMENTAL ANNUALIZED COSTS (Fabric Filter with Wet FGD - Fabric Filter with Dry FGD)	=	$	1,313,912
TOTAL INCREMENTAL COST EFFECTIVENESS ($ per ton of pollutant removed differential between Wet FGD and Dry FGD including Fabric Filter cost difference)	=	$	6,132

Notes:

1) Cost factors - from OAQPS Control Cost Manual, Chapter 3

2) Capital Recovery Factor for System - Based on a 15-year equipment life and 7% interest rate

3) Sargent & Lundy provided Wet Limestone FGD purchased equipment cost, direct installation cost, indirect installation cost and annual fixed and variable O&M costs.

4) Reference Dry Lime FGD and Fabric Filter cost calculation spreadsheets for information shown in incremental cost analysis.

Council Bluffs Energy Center Unit 4
Wet Limestone FGD SO_2 Removal Calculation

Net Unit Output (nominal MW net)	750 MW	Provided by MidAmerican
Coal Heating Value =	8,000 Btu/lb	Provided by MidAmerican
Unit Capacity Factor =	100 %	Provided by MidAmerican
Annual Heat Input (at 100% CF) =	67,233,000 MMBtu/year	7,675 MMBtu/hr x 8760 hours x 100%
Annual Coal Use (at 100% CF) =	4,202,063 tons/year	Calculated
Design Coal Sulfur Content =	0.50 %	Provided by MidAmerican
Wet Limestone FGD Design Collection Efficiency =	95.0 %	Provided by Sargent & Lundy
SO_2 emission rate before FGD =	1.25 lb/MMBtu	Provided by Sargent & Lundy
SO_2 annual tons before FGD =	42,021 tons/year	Calculated
SO_2 emission rate after FGD =	0.06 lb/MMBtu	Calculated based on 95% CE
SO_2 annual tons after FGD =	2,101 tons/year	Calculated based on 95% CE
SO_2 annual tons removed by FGD =	39,920 tons/year	Calculated

Council Bluffs Energy Center Unit 4
Pulse-Jet Fabric Filter
Cost Estimate

Capital Cost Factors

DIRECT COSTS	Cost Factors					Fabric Filter with Dry FGD		Fabric Filter with Wet FGD
(1) Purchased Equipment								
(a) Basic Equipment and auxiliaries								
Capital Cost of Fabric Filter System				=	$	13,150,000	$	13,939,000
Total Capital Cost				=	$	13,150,000	$	13,939,000
(b) Instruments and controls [0.1 * (a)]	(Included in Purchased Equipment Costs)							
(c) Taxes [0.07(a)]	0.07	*	(a)	=	$	920,500	$	975,730
Total Equipment Cost (TEC)				=	$	14,070,500	$	14,914,730
(2) Construction Costs								
(a) Foundations and supports	(Included in Total Construction Costs)							
(b) Handling and Erection	(Included in Total Construction Costs)							
(c) Electrical	(Included in Total Construction Costs)							
(d) Piping	(Included in Total Construction Costs)							
(e) Insulation	(Included in Total Construction Costs)							
(f) Painting	(Included in Total Construction Costs)							
Total Construction Costs (TCC)				=	$	18,049,000	$	19,131,940
TOTAL DIRECT COSTS (TDC)	(TEC)	+	(TCC)	=	$	32,119,500	$	34,046,670
INDIRECT COSTS								
(3) Engineering and supervision	(Included in Total Indirect Costs)							
(4) Construction and field expenses	(Included in Total Indirect Costs)							
(5) Construction fee	(Included in Total Indirect Costs)							
(6) Start-up	(Included in Total Indirect Costs)							
(7) Performance test	(Included in Total Indirect Costs)							
TOTAL INDIRECT COSTS (TIC)				=	$	9,359,700	$	9,921,280
TOTAL DIRECT AND INDIRECT COSTS (TDIC)	(TDC)	+	(TIC)	=	$	41,479,200	$	43,967,950
(8) Contingency	(Included in Total Indirect Costs)							
TOTAL INSTALLED CAPITAL COSTS (TICC)				=	$	41,479,200	$	43,967,950

Council Bluffs Energy Center Unit 4
Pulse-Jet Fabric Filter
Cost Estimate (continued)

Annualized Cost Factors

DIRECT COSTS	Cost Factors				Fabric Filter with Dry FGD	Fabric Filter with Wet FGD
Fixed O&M Costs						
(1) Operating Labor	(Included in Total Fixed O&M Costs)					
(2) Supervisory Labor	(Included in Total Fixed O&M Costs)					
(3) Maintenance Labor	(Included in Total Fixed O&M Costs)					
(4) Parts and Materials	(Included in Total Fixed O&M Costs)					
Total Fixed O&M Costs				=	$ 300,000	$ 300,000
Variable O&M Costs						
(5) Bags & Cages Replacement Cost:				=	$ 553,333	$ 553,333
(6) Auxiliary Power Cost:				=	$ 1,124,444	$ 1,124,444
(7) Ash Disposal Cost				=	N/A	$ 941,111
Total Variable O&M Costs					$ 1,677,778	$ 2,618,889
TOTAL DIRECT COSTS (TDAC)				=	$ 1,977,778	$ 2,918,889
INDIRECT COSTS						
(8) Overhead	60%	of	Fixed O&M Costs	=	$ 180,000	$ 180,000
(9) Property Tax	1%	of	(TICC)	=	$ 414,792	$ 439,680
(10) Insurance	1%	of	(TICC)	=	$ 414,792	$ 439,680
(11) G&A Charges	2%	of	(TICC)	=	$ 829,584	$ 879,359
(12) Capital Recovery	0.110	*	(TICC)	=	$ 4,554,193	$ 4,827,445
TOTAL INDIRECT COSTS (TIAC)				=	$ 6,393,361	$ 6,766,163
TOTAL ANNUALIZED COSTS	TDAC + TIAC			=	$ 8,371,139	$ 9,685,051
TOTAL TONS REMOVED PER YEAR (PM_{10})				=	33,221	33,221
COST EFFECTIVENESS ($ per ton of pollutant removed)				=	$ 252	$ 292
DIFFERENTIAL ANNUALIZED COSTS (WET FGD FABRIC FILTER - DRY FGD FABRIC FILTER)				=	$ 1,313,912	

Notes:

1) Cost factors - from OAQPS Control Cost Manual, Chapter 3

2) Capital Recovery Factor for System - Based on a 15-year equipment life and 7% interest rate.

3) Sargent & Lundy provided Pulse-Jet Fabric Filter purchased equipment cost, direct installation cost, indirect installation cost and annual fixed and variable O&M costs for both Dry FGD and Wet FGD configurations.

4) Total tons PM_{10} removed per year = 605 tpy controlled emissions/[(100 - Fabric Filter Collection Efficiency)/100] = 605/[(100 - 99.74)/100] = 605/0.0026 = 232,692 tpy uncontrolled emissions. Tons PM_{10} removed = 232,692 - 605 = 232,087.

MidAmerican Energy
Council Bluffs Energy Center
Unit 4
Emissions Calculations

Emission Workbook sheets include:

Source Number	Source Name
EP-141	Unit 4 Boiler Criteria Emissions
EP-001, EP-002, EP-003	Units 1, 2 and 3 Boiler Criteria Emissions
EP-145	Unit 4 Cooling Tower
EP-112	Units 1/2 Auxilliary Boiler
EP-004	Unit 3 Auxiliary Boiler
EP-142	Unit 4 Auxiliary Boiler
EP-144	Unit 4 Fire Pump
EP-143	Unit 4 Emergency Generator
EP-141	Unit 4 Boiler Trace Metal HAPs
EP-141	Unit 4 Boiler Acid Gas HAPs
EP-141	Unit 4 Boiler Organic HAPs
F-31, F-32, F-33, F-117	Units 1, 2 and 3 Coal Handling - Fugitives
F-151A, F-151C	Unit 4 Coal Handling - Fugitives
EP-159, EP-160, EP-161, EP-6, EP-9, EP-10, EP-11, EP-13, EP-14, EP-15, EP-16, EP-17, EP-117, EP-20, EP-21, EP-119A, EP-119B, EP-167, EP-168, EP-169, EP-170, EP-162, EP-163, EP-164A, EP-164B	Total CBEC Material Handling (NAAQS) (Includes Coal, Flyash, Lime and Urea Handling)
EP-159, EP-160, EP-161, EP-6, EP-9, EP-10, EP-11, EP-13, EP-14, EP-15, EP-20, EP-21, EP-119A, EP-119B, EP-167, EP-168, EP-169, EP-170, EP-162, EP-163, EP-164A, EP-164B	Total CBEC Material Handling (Increment) (Includes Coal, Flyash, Lime and Urea Handling)
F-5A, F-5B	Unit 4 Inactive Coal Pile - Fugitives
F-4A, F-4B, F-151B	Unit 4 Active Coal Pile - Fugitives
F-903	Units 1, 2 and 3 Paved Ash Haul Road
F-904	Unit 4 Paved Ash Haul Road

MidAmerican CBEC Unit 4 Project
Unit 4 Boiler (EP-141)
Criteria Pollutant Potential To Emit

Powder River Basin Coal

	Maximum 105% Load	75% Load	50% Load	Information Source
Nominal Net Unit Output (MW)	750	563	375	Sargent & Lundy
Coal Feed Rate (tons/hr)	480	343	238	Sargent & Lundy
Coal Percent Sulfur (%)	0.50	0.50	0.50	Sargent & Lundy
Heat Input to Boiler (MMBtu/hr)	7,675	5,480	3,801	Sargent & Lundy
Fuel Heat Value (Btu/lb)	8,000	8,000	8,000	Sargent & Lundy
Annual Capacity Factor (%/yr)	100	100	100	MidAmerican
NOx [PSD sig level = 40 tpy]				
NOx Boiler Emissions (lb/MMBtu)	0.20	0.20	0.20	Sargent & Lundy
NOx Boiler Emissions (lb/hr)	1535.0	1096.0	760.2	Calculated
SCR Control Efficiency (%)	60	60	60	Sargent & Lundy
NOx Stack Emissions (lb/MMBtu)	0.080	0.080	0.080	Sargent & Lundy
NOx Stack Emissions (lb/hr)	614.0	438.4	304.1	Calculated
NOx Stack Emissions (tpy)	2,689	1,920	1,332	Calculated
SO_2 [PSD sig level = 40 tpy]				
SO_2 Boiler Emissions (lb/MMBtu)	1.25	1.25	1.25	Sargent & Lundy
SO_2 Boiler Emissions (lb/hr)	9,594	6,850	4,751	Calculated
FGD Control Efficiency (%)	90.4	90.4	90.4	Sargent & Lundy
SO_2 Stack Emissions (lb/MMBtu)	0.120	0.120	0.120	Sargent & Lundy
SO_2 Stack Emissions (lb/hr)	921.0	657.6	456.1	Calculated
SO_2 Stack Emissions (tpy)	4,034	2,880	1,998	Calculated
CO [PSD sig level = 100 tpy]				
CO Emission Factor (lb/MMBtu)	0.154	0.154	0.154	Sargent & Lundy
CO Stack Emissions (lb/hr)	1179.4	842.1	584.1	Calculated
CO Stack Emissions (tpy)	5,166	3,689	2,558	Calculated
Filterable PM [PSD sig level = 25 tpy]				
Filterable PM Boiler Emissions (lb/hr)	53,727	38,361	26,606	Calculated based on Coal
Baghouse Control Efficiency (%)	99.74	99.74	99.74	Sargent & Lundy
Filterable PM Stack Emissions (lb/MMBtu)	0.020	0.020	0.020	Sargent & Lundy
Filterable PM Stack Emissions (lb/hr)	153.5	109.6	76.0	Calculated
Filterable PM Stack Emissions (tpy)	672	480	333	Calculated
PM_{10} [PSD sig level = 15 tpy]				
Filterable PM_{10}				
Filterable PM_{10} Boiler Emissions (lb/hr)	7,723	5,514	3,825	Calculated based on AP-42
Baghouse Control Efficiency (%)	98.21	98.21	98.21	Calculated
Filterable PM_{10} Stack Emissions (lb/MMBtu)	0.018	0.018	0.018	Sargent & Lundy
Filterable PM_{10} Stack Emissions (lb/hr)	138.2	98.6	68.4	Calculated
Filterable PM_{10} Stack Emissions (tpy)	605	432	300	Calculated
Condensable PM_{10} [2]				
Cond. PM_{10} Stack Emissions (lb/MMBtu)	0.007	0.007	0.007	Sargent & Lundy
Cond. PM_{10} Stack Emissions (lb/hr)	56.9	40.6	28.2	Sargent & Lundy
Cond. PM_{10} Stack Emissions (tpy)	249	178	123	Calculated
Total PM_{10}				
Total PM_{10} Stack Emissions (lb/MMBtu)	0.025	0.025	0.025	Calculated Total
Total PM_{10} Stack Emissions (lb/hr)	195.1	139.3	96.6	Calculated Total
Total PM_{10} Stack Emissions (tpy)	854	610	423	Calculated Total
Lead [PSD sig level = 0.6 tpy]				
Lead Emission Factor (lb/ton)	4.2E-04	4.2E-04	4.2E-04	AP-42 Table 1.1-18
Lead Emissions (lb/hr)	0.20	0.14	0.10	Calculated
Lead Emissions (tpy)	0.88	0.63	0.44	Calculated
VOC [PSD sig level = 40 tpy[3]]				
VOC Emission Factor (lb/ton)	0.06	0.06	0.06	AP-42 Table 1.1-19
VOC Emissions (lb/hr)	28.8	20.6	14.3	Calculated
VOC Emissions (tpy)	126.1	90.0	62.4	Calculated

MidAmerican CBEC Unit 4 Project
Unit 4 Boiler (EP-141)
Criteria Pollutant Potential To Emit

	Powder River Basin Coal			
	Maximum 105% Load	75% Load	50% Load	Information Source
Sulfuric Acid Mist [PSD sig level = 7 tpy]				
Uncontrolled H_2SO_4 Emissions (lb/hr)	323.2	230.8	160.0	Sargent & Lundy
FGD Control Efficiency for H_2SO_4 (%)	90	90	90	Sargent & Lundy
H_2SO_4 Stack Emissions (lb/MMBtu)	0.00421	0.00421	0.00421	Sargent & Lundy
H_2SO_4 Stack Emissions (lb/hr)	32.3	23.1	16.0	Calculated
H_2SO_4 Stack Emissions (tpy)	142	101	70	Calculated
Fluorides [PSD sig level = 3 tpy]				
Uncontrolled HF Emissions (lb/hr)	50.6	36.1	25.0	Sargent & Lundy
FGD Control Efficiency for HF (%)	90.0	90.0	90.0	Sargent & Lundy
HF Stack Emissions (lb/MMBtu)	0.00066	0.00066	0.00066	Sargent & Lundy
HF Stack Emissions (lb/hr)	5.1	3.6	2.5	Calculated
HF Stack Emissions (tpy)	22	16	11	Calculated
Hydrogen Chloride [No PSD sig level]				
Uncontrolled HCL Emissions (lb/hr)	136.7	97.6	67.7	Sargent & Lundy
FGD Control Efficiency for HCL (%)	90.0	90.0	90.0	Sargent & Lundy
HCL Stack Emissions (lb/MMBtu)	0.00178	0.00178	0.00178	Sargent & Lundy
HCL Stack Emissions (lb/hr)	13.7	9.8	6.8	Calculated
HCL Stack Emissions (tpy)	60	43	30	Calculated
Ammonium Sulfate [No PSD sig level]				
Uncontrolled $(NH_4)_2SO_4$ Emissions (lb/hr)	58.6	41.9	29.0	Sargent & Lundy
FGD Control Efficiency for $(NH_4)_2SO_4$ (%)	90.0	90.0	90.0	Sargent & Lundy
$(NH_4)_2SO_4$ Stack Emissions (lb/MMBtu)	0.00076	0.00076	0.00076	Sargent & Lundy
$(NH_4)_2SO_4$ Stack Emissions (lb/hr)	5.9	4.2	2.9	Calculated
$(NH_4)_2SO_4$ Stack Emissions (tpy)	26	18	13	Calculated
Total Reduced Sulfur [PSD sig level = 10 tpy[4]]				
TRS Stack Emissions (lb/MMBtu)	0.001	0.001	0.001	AP-42 Table 1.1-3 (b)
TRS Stack Emissions (lb/hr)	6.8	4.8	3.4	Calculated
TRS Stack Emissions (tpy)	30	21	15	Calculated
Reduced Sulfur Compounds [PSD sig level = 10 tpy[4]]				
RSC Stack Emissions (lb/MMBtu)	0.001	0.001	0.001	AP-42 Table 1.1-3 (b)
RSC Stack Emissions (lb/hr)	6.8	4.8	3.4	Calculated
RSC Stack Emissions (tpy)	30	21	15	Calculated
Stack Conditions				
Stack Exit Flow (acfm)	2,660,982	1,899,961	1,413,332	Sargent & Lundy
Stack Height (feet)	550	550	550	Sargent & Lundy
Stack Exit Diameter (feet)	24.65	24.65	24.65	Sargent & Lundy
Stack Exit Temperature (degF)	165	165	165	Sargent & Lundy
Stack Exit Velocity (fps)	92.94	66.36	49.37	Sargent & Lundy

Notes:

(1) Emissions based on design data from Sargent & Lundy

(2) Condensible PM_{10} includes HCL, HF, H_2SO_4 and $(NH_4)_2SO_4$.

(3) No modeling significance level has been established for VOC. From the EPA NSR Workshop Manual: *No significant ambient concentration has been established. Instead any net emission increase of 100 tpy of VOC subject to PSD would be required to perform an ambient impact analysis.*

(4) Emission Factor for Total Reduced Sulfur and Reduced Sulfur Compounds based on Footnote b of AP-42 Table 1.1-3.

(5) HCL, HF, H_2SO_4 and $(NH_4)_2SO_4$ estimated emissions from Sargent & Lundy.

(6) Annual ton estimate for each pollutant based on 100% capacity factor for Unit 4 operation.

MidAmerican CBEC Unit 4 Project
Units 1, 2 and 3 Boilers (EP-001, EP-002, EP-003)
Criteria Emissions

	2000/2001 Emission Inventory Average				
	Unit 1	Unit 2	Unit 3	Total	Information Source
Unit Design Information					
Design Net Output (MW)	43	88	690		MidAmerican
Design Boiler Heat Input (mmBtu/hr)	656	935	7,300		Title V Permit
Operating Hours (hours)	7,059	7,705	7,999	22,762	Supplied by Chad Teply, MidAmerican
Coal Burned (tons)	183,863	306,873	3,044,057	3,534,792	2000/2001 EI
Fuel Oil Burned (gallons)	0	0	381,810	381,810	2000/2001 EI
Natural Gas Burned (MMscf)	13.18	27.11	0	40.28	2000/2001 EI
Coal Heating Value (Btu/lb)	8,403	8,397	8,406		2000/2001 EI
Fuel Oil Heating Value (Btu/gal)	136,000	136,000	136,000		Supplied by Chad Teply, MidAmerican
Stack Parameters					
Stack Height (ft):	250	250	550		Title V Renewal Application
Stack Exit Diameter (ft):	12.0	12.0	25.0		Title V Renewal Application
Stack Temperature (F):	305	340	293		Title V Renewal Application
Exhaust Flow (scfh) (100% Load)	9,200,000	15,300,000	102,000,000		Title V Renewal Application
Exhaust Flow (acfm) (100% Load)	186,366	282,898	2,382,000		Title V Renewal Application
Exit Velocity (ft/s) (100% Load)	27.5	41.7	80.9		Calculated
Permit Limits					
NO_x (lb/mmBtu) (short term 3-hour)	None	None	0.7		Title V Permit
NO_x (lb/mmBtu) (Acid Rain annual average)	0.50	0.45	0.50		Title V Permit
SO_2 (lb/mmBtu)	1.2	1.2	1.2		Title V Permit and NAAQS Compliance Permit Modificati
PM_{10} (lb/mmBtu)	0.49	0.49	0.1		Title V Permit
Emissions					
NO_x (tons)	743	1,010	11,929	13,683	2000/2001 EI
NO_x (lb/hr)	210.62	262.30	2,982.91		Calculated
NO_x (short-term PTE, lb/hr)	N/A	N/A	5,110.00		Calculated
SO_2 (tons)	1,137	1,808	17,859	20,804	2000/2001 EI
SO_2 (lb/hr)	322.02	469.28	4,465.70		Calculated
SO_2 (short-term PTE, lb/hr)	787.20	1,122.00	8,760.00		Calculated
Filterable PM_{10} (tons)	72.49	76.11	440.43	589.02	2000/2001 EI, includes emissions from Nat gas usage
Filterable PM_{10} (lb/hr)	20.54	19.76	110.13		Calculated
Filterable PM_{10} (short-term PTE, lb/hr)	321.44	458.15	730.00		Calculated
HCL (tons)	6.9	11.5	115	133.05	2000/2001 EI
HCL (lb/hr)	1.96	3.00	28.66		Calculated
HF (tons)	7.27	12.14	121	139.93	2000/2001 EI
HF (lb/hr)	2.06	3.15	30.14		
H_2SO_4 (tons)[7]	0.87	1.39	6.84	9.10	Calculation Based on Southern Company Method
H_2SO_4 (lb/hr)	0.25	0.36	1.71		Calculated
Condensable PM_{10} (total, tons)	15.04	25.06	241.97	282.07	Calculated
Condensable PM_{10} (total, lb/hr)	4.26	6.51	60.50		Calculated

MidAmerican CBEC Unit 4 Project
Units 1, 2 and 3 Boilers (EP-001, EP-002, EP-003)
Criteria Emissions

	2000/2001 Emission Inventory Average				Information Source
	Unit 1	Unit 2	Unit 3	Total	
CO (tons)	45.97	76.72	761.01	883.70	Calculated
CO (lb/hr)	13.02	19.92	190.29		Calculated
CO (oil, tons)	0.00	0.00	0.95	0.95	Calculated
CO (oil, lb/hr)	0.00	0.00	0.24		Calculated
VOC (tons)	5.55	9.28	91.37	106.20	2000/2001 EI, includes emissions from Nat gas usage
VOC (lb/hr)	1.57	2.41	22.85		Calculated
VOC (oil, tons)	0.00	0.00	0.04	0.04	Calculated
VOC (oil, lb/hr)	0.00	0.00	0.01		Calculated
Lead (tons)	0.04	0.07	0.64	0.74	Calculated
Lead (lb/hr)	0.01	0.02	0.16		Calculated

Notes:

1) Unit design information and stack parameters based on Title V Permit, Title V Renewal Application, plant personnel, and the average of 2000 and 2001 Emission Inventories.

2) NO_x, SO_2 and PM_{10} permit limits based on Title V Permit.

3) Emissions based on the average of Year 2000 and Year 2001 emission inventories.

4) Emissions of CO and VOC for fuel oil combustion based on AP-42 factors. (5.0 lbs CO/1000 gallons oil burned, 0.2 lbs VOC/1000 gallons oil burned).

5) Short-term Potential to Emit (PTE) lb/hr emission rates for NO_x, SO_2 and PM_{10} were determined by multiplying the IDNR permit limits times the maximum boiler hourly heat input.

6) H2SO4 emissions calculated based on "An Updated Method for Estimating Total Sulfuric Acid Emissions from Stationary Power Plants, May 2001". Reduction factors are as follows:

Fuel Impact Factor for sub-bituminous PC Boiler	F1	0.000556
Technology Impact Factor for sub-bituminous air preheater	F2	0.9
Technology Impact Factor for hot-side ESP	F2	1
Technology Impact Factor for cold-side ESP	F2	0.5
	MW H2SO4/MW SO2	1.53

7) Condensable PM_{10} emissions include HCL, HF and H_2SO_4. Emissions based on average of 2000 and 2001 emission inventories.

MidAmerican Unit 4 Project
Unit 4 Cooling Tower (EP-145)

Method from AP 42, Sect.13.4-1

Emissions

Water Flow Rate (gal/min)	349,400
Flow of cooling water (lbs/hr)	174,839,760
TDS of makeup water (mg/l or ppmw)	1,050
Cycles of Concentration	7
TDS of blowdown (mg/l or ppmw)	7,350
Flow of dissolved solids (lbs/hr)	1,285,072
Fraction of flow producing PM_{10} drift (See Note 2)	0.200
Control efficiency of drift eliminators (gal drift/gal flow)	0.000005
PM emissions from tower (lb/hr)	6.425
PM_{10} emissions from tower (lb/hr)	1.285
PM emissions from tower (tpy)	28.143
PM_{10} emissions from tower (tpy)	5.629
Particulate (PM-10) emissions from each tower cell (lb/hr)	0.071

Other Parameters

Number of cells per tower (outlet fans)	18
Height at cell release (ft):	48.0
Discharge flow per cell (ACFM):	1,401,485
Diameter of each cell (ft):	34.2
Area of cell discharge (ft^2):	919
Average Temperature of cell discharge (degF):	103
Exit Velocity (ft/s):	25.4

Notes:

(1) Cooling Tower design data from Sargent & Lundy.

(2) From "Calculating Realistic PM_{10} Emissions From Cooling Towers" (J. Reisman, G. Frisbie). Presented at 2001 AWMA Annual Meeting.

(3) TDS based on data from Sargent & Lundy.

MidAmerican CBEC Unit 4 Project
Units 1/2 Auxiliary Boiler- EP 112

Other Parameters

Stack Height (ft):	80
Stack Exit Diameter (ft):	1.17
Area of Discharge (ft^2):	1.1
Temperature of cell discharge (F):	300
Exhaust Flow (ACFM):	2,175
Exit Velocity (ft/s):	33.910
Maximum Fuel Firing Rate (gal/hr):	50.00
Maximum Hours of Operation (hr/yr):	1,440
Fuel Oil Heating Value (Btu/gal):	141,000

Emissions

											Annual Emissions						Maximum Hourly Emissions					
Heater/Boiler Heat Input Rating (MMBTU/hr)	Fuel Type (Diesel, LPG, or Natural Gas)	Fuel Consumption	Fuel Usage Units	NO_x Emission Factor	CO Emission Factor	SO_2 Emission Factor	PM_{10} Emission Factor	VOC Emission Factor	Lead Emission Factor	Emission Factor Units	NO_x Emissions (TPY)	CO Emissions (TPY)	SO_2 Emissions (TPY)	PM_{10} Emissions (TPY)	VOC Emissions (TPY)	Lead Emissions (TPY)	NO_x Emissions (lbs/hr)	CO Emissions (lbs/hr)	SO_2 Emissions (lbs/hr)	PM_{10} Emissions (lbs/hr)	VOC Emissions (lbs/hr)	Lead Emissions (lbs/hr)
6.55	Natural Gas	335,000	scf/yr	170.0	24.0	0.6	7.6	5.5	8.30E-06	lbs/10^6 scf	0.028	0.004	0.000	0.001	0.001	1.39E-03	1.11	0.16	0.00	0.05	0.04	3.97E-04

Notes:

1.) Other Parameters based on MidAmerican data for the auxiliary boiler.
2.) Fuel consumption based on average of 2000/2001 actual usage from Emission Inventories.
3.) Diesel emission factors obtained from Tables 1.3-1 through 1.3-7 in AP-42 Guidance Document dated October 1996. Sulfur content was assumed to be 0.05% of diesel fuel.
4.) Stack height 5 feet above boiler building.

MidAmerican CBEC Unit 4 Project
Unit 3 Auxiliary Boiler- EP-004

Other Parameters

Stack Height (ft):	45.5
Stack Exit Diameter (ft):	4
Area of Discharge (ft^2):	12.6
Temperature of cell discharge (F):	450
Exhaust Flow (ACFM):	29,581
Exit Velocity (ft/s):	39.2
Maximum Fuel Firing Rate (gal/hr):	487.00
Maximum Hours of Operation (hr/yr):	1,440
Fuel Oil Heating Value (Btu/gal):	141,000

Emissions

Heater/Boiler Heat Input Rating (MMBTU/hr)	Fuel Type (Diesel, LPG, or Natural Gas)	Fuel Consumption	Fuel Usage Units	NO_x Emission Factor	CO Emission Factor	SO_2 Emission Factor	PM_{10} Emission Factor	VOC Emission Factor	Lead Emission Factor	Emission Factor Units	Annual Emissions						Maximum Hourly Emissions					
											NO_x Emissions (TPY)	CO Emissions (TPY)	SO_2 Emissions (TPY)	PM_{10} Emissions (TPY)	VOC Emissions (TPY)	Lead Emissions (TPY)	NO_x Emissions (lbs/hr)	CO Emissions (lbs/hr)	SO_2 Emissions (lbs/hr)	PM_{10} Emissions (lbs/hr)	VOC Emissions (lbs/hr)	Lead Emissions (lbs/hr)
68.7	Diesel	39,265	gal/yr	0.020	0.005	0.0071	0.002	0.00034	8.30E-06	lbs/gal	0.393	0.098	0.139	0.039	0.007	1.63E-04	10.02	2.51	3.56	1.00	0.17	4.16E-03

Notes:

1.) Other Parameters based on MidAmerican data for the auxiliary boiler.
2.) Fuel consumption based on average of 2000/2001 actual usage from Emission Inventories.
3.) Diesel emission factors obtained from Tables 1.3-1 through 1.3-7 in AP-42 Guidance Document dated October 1996. Sulfur content was assumed to be 0.05% of diesel fuel.

MidAmerican CBEC Unit 4 Project
Unit 4 Auxiliary Boiler

Other Parameters

Stack Height (ft):	310
Stack Exit Diameter (ft):	3.24
Area of Discharge (ft^2):	*8.2*
Temperature of cell discharge (F):	400
Exhaust Flow (ACFM):	49,300
Exit Velocity (ft/s):	100
Maximum Fuel Firing Rate (gal/hr):	974.21
Maximum Hours of Operation (hr/yr):	2,500
Fuel Oil Heating Value (Btu/gal):	141,000

Emissions

Heater/Boiler Heat Input Rating (MMBTU/hr)	Fuel Type (Diesel, LPG, or Natural Gas)	Fuel Consumption	Fuel Usage Units	NO_x Emission Factor	CO Emission Factor	SO_2 Emission Factor	PM_{10} Emission Factor	VOC Emission Factor	Lead Emission Factor	Emission Factor Units	Annual Emissions NO_x Emissions (TPY)	Annual Emissions CO Emissions (TPY)	Annual Emissions SO_2 Emissions (TPY)	Annual Emissions PM_{10} Emissions (TPY)	Annual Emissions VOC Emissions (TPY)	Annual Emissions Lead Emissions (TPY)	NO_x Emissio (lbs/hr)
137.400	Diesel	2,435,525	gal/yr	0.020	0.005	0.0071	0.002	0.00034	8.30E-06	lbs/gal	24.355	6.089	8.646	2.436	0.414	1.01E-02	20.06

Notes:

1.) Other Parameters based on Sargent & Lundy data for the auxiliary boiler.
2.) Fuel consumption based on 974.21 gal/hr max fuel firing rate times max annual hours of operation.
3.) Diesel emission factors obtained from Tables 1.3-1 through 1.3-7 in AP-42 Guidance Document dated October 1996. Sulfur content was assumed to be 0.05% of diesel fuel.
4.) Stack height 10 feet above boiler building.

Maximum Hourly Emissions					
...s	CO Emissions (lbs/hr)	SO_2 Emissions (lbs/hr)	PM_{10} Emissions (lbs/hr)	VOC Emissions (lbs/hr)	Lead Emissions (lbs/hr)
	5.01	7.12	2.01	0.34	8.32E-03

MidAmerican CBEC Unit 4 Project
Unit 4 Fire Pump

Engine Power (BHP)	Hours of Operation (hrs/yr)	Potential Hours of Operation (hrs/yr)	Fuel Type (Diesel or Mogas)	NO_x Emission Factor (lbs/hp-hr)	CO Emission Factor (lbs/hp-hr)	SO_2 Emission Factor (lbs/hp-hr)	PM_{10} Emission Factor (lbs/hp-hr)	VOC Emission Factor (lbs/hp-hr)	NO_x Emissions (TPY)	NO_x Annual (lbs/hr)	NO_x Maximum (lbs/hr)	CO Emissions (TPY)	CO Annual (lbs/hr)	CO Maximum (lbs/hr)	SO_2 Emissions (TPY)	SO_2 Annual (lbs/hr)	SO_2 Maximum (lbs/hr)	PM_{10} Emissions (TPY)	PM_{10} Annual (lbs/hr)	PM_{10} Maximum (lbs/hr)	VOC Emissions (TPY)	VOC Annual (lbs/hr)	VOC Maximum (lbs/hr)
250	500	500	Diesel	3.10E-02	6.70E-03	2.10E-03	2.20E-03	2.50E-03	1.938	0.004	7.750	0.419	0.001	1.675	0.131	0.000	0.525	0.138	0.000	0.550	0.156	0.000	0.625

Notes:
1) Based on data from Sargent & Lundy
2) Emission Factors are from AP -42 Section 3.3

MidAmerican Unit 4 Project
Unit 4 Emergency Generator

Engine Power (BHP)	Hours of Operation (hrs/yr)	Potential Hours of Operation (hrs/yr)	Fuel Type (Diesel or Mogas)	NO_x Emission Factor (lbs/hp-hr)	CO Emission Factor (lbs/hp-hr)	SO_2 Emission Factor (lbs/hp-hr)	PM_{10} Emission Factor (lbs/hp-hr)	VOC Emission Factor (lbs/hp-hr)	NO_x Emissions (TPY)	NO_x Annual (lbs/hr)	NO_x Maximum (lbs/hr)	CO Emissions (TPY)	CO Annual (lbs/hr)	CO Maximum (lbs/hr)	SO_2 Emissions (TPY)	SO_2 Annual (lbs/hr)	SO_2 Maximum (lbs/hr)	PM_{10} Emissions (TPY)	PM_{10} Annual (lbs/hr)	PM_{10} Maximum (lbs/hr)	VOC Emissions (TPY)	VOC Annual (lbs/hr)	VOC Maximum (lbs/hr)
1341	500	500	Diesel	2.40E-02	5.50E-03	4.05E-04	7.00E-04	6.42E-04	8.046	0.016	32.184	1.844	0.004	7.376	0.136	0.000	0.542	0.235	0.000	0.939	0.215	0.000	0.860

Notes:
1) Based on data from Sargent & Lundy
2) Emission Factors are from AP -42 Section 3.4
3) Sulfur Content of Fuel Oil = 0.05 %

MidAmerican CBEC Unit 4 Project
Unit 4 Boiler (EP-141)
Trace Metal HAP Emissions

Maximum Hourly Coal Input (tons/hour)	480	Convert tpy to lb/hr	0.228	
Maximum Annual Input (tons/year)	4202197	Convert lb/hr to g/s	0.126	100% Capacity Factor

Compounds[1]	Controlled Emission Factor[3] (lb/ton coal)	Short-Term Emissions		Annual Emissions			Uncontrolled[5] lbs/yr	Controlled lbs/yr
		lb/hr	g/s	tpy	lb/hr	g/s		
Trace Metals AP-42 Table 1.1-18								
Antimony	1.80E-05	8.63E-03	0.001	0.038	8.63E-03	0.001	25,213.2	75.6
Arsenic	4.10E-04	1.97E-01	0.025	0.861	1.97E-01	0.025	574,300.2	1,722.9
Beryllium	2.10E-05	1.01E-02	0.001	0.044	1.01E-02	0.001	29,415.4	88.2
Cadmium	5.10E-05	2.45E-02	0.003	0.107	2.45E-02	0.003	71,437.3	214.3
Chromium	2.60E-04	1.25E-01	0.016	0.546	1.25E-01	0.016	364,190.4	1,092.6
Cobalt	1.00E-04	4.80E-02	0.006	0.210	4.80E-02	0.006	140,073.2	420.2
Lead	4.20E-04	2.01E-01	0.025	0.882	2.01E-01	0.025	588,307.6	1,764.9
Manganese	4.90E-04	2.35E-01	0.030	1.030	2.35E-01	0.030	686,358.8	2,059.1
Mercury[4]	8.02E-05	3.85E-02	0.005	0.169	3.85E-02	0.005	421.3	337.0
Nickel	2.58E-04	1.24E-01	0.016	0.542	1.24E-01	0.016	361,388.9	1,084.2
Selenium	1.30E-03	6.24E-01	0.079	2.731	6.24E-01	0.079	1,820,952.0	5,462.9

Total Trace Metal HAPs 7.161 tpy

Notes:

[1] AP-42 Section 1.1, Table 1.1-18, (9/1998)

[2] USEPA - TTN, Unified Air Toxics website, Section 112 Hazardous Air Pollutants, (8/21/2000)

[3] Emission factor for controlled coal combustion; for facilities using venturi scrubbers, spray dryers, or wet limestone scrubbers with ESP or Fabric Filter

[4] Estimated Mercury emissions based on testing completed at CBEC in 1999. Uncontrolled mercury emissions estimated to be 0.0481 lb/hr at maximum load, 20% control efficiency based on fabric filter/dry lime FGD combination, controlled mercury emissions of 0.0385 lb/hr at maximum load. Controlled Emission Factor = 0.0385 lb/hr divided by 480 tons/hr = 8.021E-05 lb/ton.

[5] Uncontrolled emissions were calculated based on the control efficiency of the fabric filter (99.7%). Uncontrolled emissions for mercury were calculated using a control efficiency of 20%.

MidAmerican CBEC Unit 4 Project
Unit 4 Boiler (EP-141)
Acid Gas HAP Emissions

Maximum Hourly Coal Input (tons/hour)	480	Convert tpy to lb/hr	0.228	
Maximum Annual Input (tons/year)	4,202,197	Convert lb/hr to g/s	0.126	100% Capacity Factor

Compounds	Uncontrolled Emissions lb/hr	FGD Control Efficiency	Short-Term Emissions lb/hr	Short-Term Emissions g/s	Annual Emissions tpy	Annual Emissions lb/hr	Annual Emissions g/s	Uncontrolled lbs/yr	Controlled lbs/yr
HCL	136.70	90	13.67	1.72	59.87	13.67	1.72	1,197,458.0	119,745.8
HF	50.58	90	5.06	0.64	22.15	5.06	0.64	443,059.5	44,305.9

Total Acid Gas HAPs **82.03** **tpy**

Notes:

1) HCL and HF uncontrolled emissions and FGD control efficiency provided by Sargent & Lundy.

MidAmerican CBEC Unit 4 Project
Unit 4 Boiler (EP-141)
Organic HAP Emissions

Maximum Hourly Coal Input (tons/hour)	480	Convert tpy to lb/hr	0.228	
Maximum Annual Input (tons/year)	4,202,197	Convert lb/hr to g/s	0.126	100% Capacity Factor

Compounds[1]	Controlled Emission Factor[3] (lb/ton coal)	Hourly		Annual			Uncontrolled[4] lbs/yr	Controlled lbs/yr
		lb/hr	g/s	tpy	lb/hr	g/s		
Polynuclear Aromatic Hydrocarbons (PAH) AP-42 Table 1.1-13								
Biphenyl	1.70E-06	8.15E-04	1.03E-04	0.004	8.15E-04	1.03E-04	71.4	7.1
Acenaphthene	5.10E-07	2.45E-04	3.08E-05	0.001	2.45E-04	3.08E-05	21.4	2.1
Acenaphthylene	2.50E-07	1.20E-04	1.51E-05	0.001	1.20E-04	1.51E-05	10.5	1.1
Anthracene	2.10E-07	1.01E-04	1.27E-05	0.000	1.01E-04	1.27E-05	8.8	0.9
Benzo(a)anthracene	8.00E-08	3.84E-05	4.84E-06	0.000	3.84E-05	4.84E-06	3.4	0.3
Benzo(a)pyrene	3.80E-08	1.82E-05	2.30E-06	0.000	1.82E-05	2.30E-06	1.6	0.2
Benzo(b,j,k)fluoranthene	1.10E-07	5.28E-05	6.65E-06	0.000	5.28E-05	6.65E-06	4.6	0.5
Benzo(g,h,i)perylene	2.70E-08	1.30E-05	1.63E-06	0.000	1.30E-05	1.63E-06	1.1	0.1
Chrysene	1.00E-07	4.80E-05	6.04E-06	0.000	4.80E-05	6.04E-06	4.2	0.4
Fluoranthene	7.10E-07	3.41E-04	4.29E-05	0.001	3.41E-04	4.29E-05	29.8	3.0
Fluorene	9.10E-07	4.37E-04	5.50E-05	0.002	4.37E-04	5.50E-05	38.2	3.8
Indeno(1,2,3-cd)pyrene	6.10E-08	2.93E-05	3.69E-06	0.000	2.93E-05	3.69E-06	2.6	0.3
Naphthalene	1.30E-05	6.24E-03	7.86E-04	0.027	6.24E-03	7.86E-04	546.3	54.6
Phenanthrene	2.70E-06	1.30E-03	1.63E-04	0.006	1.30E-03	1.63E-04	113.5	11.3
Pyrene	3.30E-07	1.58E-04	1.99E-05	0.001	1.58E-04	1.99E-05	13.9	1.4
5-Methyl chrysene	2.20E-08	1.06E-05	1.33E-06	0.000	1.06E-05	1.33E-06	0.9	0.1
Organic Compounds AP-42 Table 1.1-14								
Acetaldehyde	5.70E-04	2.73E-01	3.45E-02	1.198	2.73E-01	3.45E-02	23,952.5	2,395.3
Acetophenone	1.50E-05	7.20E-03	9.07E-04	0.032	7.20E-03	9.07E-04	630.3	63.0
Acrolein	2.90E-04	1.39E-01	1.75E-02	0.609	1.39E-01	1.75E-02	12,186.4	1,218.6
Benzene	1.30E-03	6.24E-01	7.86E-02	2.731	6.24E-01	7.86E-02	54,628.6	5,462.9
Benzyl chloride	7.00E-04	3.36E-01	4.23E-02	1.471	3.36E-01	4.23E-02	29,415.4	2,941.5
Bis(2-ethylhexyl)phthalate (DEHP)	7.30E-05	3.50E-02	4.41E-03	0.153	3.50E-02	4.41E-03	3,067.6	306.8
Bromoform	3.90E-05	1.87E-02	2.36E-03	0.082	1.87E-02	2.36E-03	1,638.9	163.9
Carbon disulfide	1.30E-04	6.24E-02	7.86E-03	0.273	6.24E-02	7.86E-03	5,462.9	546.3
2-Chloroacetophenone	7.00E-06	3.36E-03	4.23E-04	0.015	3.36E-03	4.23E-04	294.2	29.4
Chlorobenzene	2.20E-05	1.06E-02	1.33E-03	0.046	1.06E-02	1.33E-03	924.5	92.4
Chloroform	5.90E-05	2.83E-02	3.57E-03	0.124	2.83E-02	3.57E-03	2,479.3	247.9
Cumene	5.30E-06	2.54E-03	3.20E-04	0.011	2.54E-03	3.20E-04	222.7	22.3
Cyanide	2.50E-03	1.20E+00	1.51E-01	5.253	1.20E+00	1.51E-01	105,054.9	10,505.5
2,4-Dinitrotoluene	2.80E-07	1.34E-04	1.69E-05	0.001	1.34E-04	1.69E-05	11.8	1.2
Dimethyl sulfate	4.80E-05	2.30E-02	2.90E-03	0.101	2.30E-02	2.90E-03	2,017.1	201.7
Ethyl benzene	9.40E-05	4.51E-02	5.68E-03	0.198	4.51E-02	5.68E-03	3,950.1	395.0
Ethyl chloride	4.20E-05	2.01E-02	2.54E-03	0.088	2.01E-02	2.54E-03	1,764.9	176.5
Ethylene dichloride	4.00E-05	1.92E-02	2.42E-03	0.084	1.92E-02	2.42E-03	1,680.9	168.1
Ethylene dibromide	1.20E-06	5.76E-04	7.25E-05	0.003	5.76E-04	7.25E-05	50.4	5.0
Formaldehyde	2.40E-04	1.15E-01	1.45E-02	0.504	1.15E-01	1.45E-02	10,085.3	1,008.5
Hexane	6.70E-05	3.21E-02	4.05E-03	0.141	3.21E-02	4.05E-03	2,815.5	281.5
Isophorone	5.80E-04	2.78E-01	3.51E-02	1.219	2.78E-01	3.51E-02	24,372.7	2,437.3
Methyl bromide	1.60E-04	7.68E-02	9.67E-03	0.336	7.68E-02	9.67E-03	6,723.5	672.4
Methyl chloride	5.30E-04	2.54E-01	3.20E-02	1.114	2.54E-01	3.20E-02	22,271.6	2,227.2
Methyl ethyl ketone	3.90E-04	1.87E-01	2.36E-02	0.819	1.87E-01	2.36E-02	16,388.6	1,638.9
Methyl hydrazine	1.70E-04	8.15E-02	1.03E-02	0.357	8.15E-02	1.03E-02	7,143.7	714.4
Methyl methacrylate	2.00E-05	9.59E-03	1.21E-03	0.042	9.59E-03	1.21E-03	840.4	84.0
Methyl tert butyl ether	3.50E-05	1.68E-02	2.12E-03	0.074	1.68E-02	2.12E-03	1,470.8	147.1
Methylene chloride	2.90E-04	1.39E-01	1.75E-02	0.609	1.39E-01	1.75E-02	12,186.4	1,218.6
Phenol	1.60E-05	7.68E-03	9.67E-04	0.034	7.68E-03	9.67E-04	672.4	67.2
Propionaldehyde	3.80E-04	1.82E-01	2.30E-02	0.798	1.82E-01	2.30E-02	15,968.3	1,596.8
Tetrachloroethylene	4.30E-05	2.06E-02	2.60E-03	0.090	2.06E-02	2.60E-03	1,806.9	180.7
Toluene	2.40E-04	1.15E-01	1.45E-02	0.504	1.15E-01	1.45E-02	10,085.3	1,008.5
1,1,1-Trichloroethane	2.00E-05	9.59E-03	1.21E-03	0.042	9.59E-03	1.21E-03	840.4	84.0
Styrene	2.50E-05	1.20E-02	1.51E-03	0.053	1.20E-02	1.51E-03	1,050.5	105.1
Xylenes	3.70E-05	1.77E-02	2.24E-03	0.078	1.77E-02	2.24E-03	1,554.8	155.5
Vinyl acetate	7.60E-06	3.65E-03	4.59E-04	0.016	3.65E-03	4.59E-04	319.4	31.9
Polychlorinated Dibenzo-P-Dioxons AP-42 Table 1.1-12								
Total PCDD/PCDF	2.44E-07	1.17E-04	1.47E-05	0.001	1.17E-04	1.47E-05	10.3	1.03E+00
Total Organic HAPs				19.346	tpy			

Notes:

[1] AP-42 Section 1.1, Tables 1.1-12, 1.1-13, and 1.1-14 (9/1998)
[2] USEPA - TTN, Unified Air Toxics website, Section 112 Hazardous Air Pollutants, (8/21/2000)
[3] Emission factor (AP-42, Section 1.1) for controlled coal combustion; for facilities using spray dryers or wet limestone scrubbers with ESP or Fabric Filter
[4] Uncontrolled emissions were calculated based on a control efficiency of 90%.

MidAmerican CBEC Unit 4 Project
Units 1, 2 & 3 Coal Handling - Fugitives

Emission factor from AP-42, Section 13.2.4: *Aggregate Handling and Storage Piles* (1/95), Equation (1) - batch or continuous drop operation

E (lb PM_{10} per ton material handled) = k (0.0032) (U/5)^1.3 / [(M/2)^1.4]
where:
k = 0.35 [particles < 10um]
k = 0.74 [particles < 30um]
U = 10.5 [mph, based on Omaha data]
[used for exposed sources and to conservatively estimate internal ventilation for enclosed sources]
M = 4.5 [%, mean moisture content for coal (as received), S&L data)

E (lb PM_{10} per ton handled) = 9.44E-04
E (lb PM per ton handled) = 2.00E-03

Source ID	Source Name	Process Rate (tph)	Max # Transfers	Uncontrolled Emissions (lb PM_{10}/hr)	Uncontrolled Emissions (lb PM/hr)	Control %	Controlled Emissions (lb PM_{10}/hr)	Controlled Emissions (lb PM/hr)	Controlled PM_{10} Emissions (tpy)	Controlled PM Emissions (tpy)	Control System and Comments
F-31	Fugitive from transfer of coal from conveyor C-3 to Stacker conveyor	3500	1	3.30	6.99	75	0.826	1.747	3.62	7.65	Chemical Binding
F-32	Fugitive from transfer of coal from Stacker Conveyor to Active Pile	3500	1	3.30	6.99	75	0.826	1.747	3.62	7.65	Chemical Binding
F-33	Fugitive from transfer of coal from Reclaimer wheel to Reclaimer Conveyor	1600	1	1.51	3.19	95	0.076	0.160	0.33	0.70	Chemical Binding
F-117	Fugitives from dumping of coal into the emergency reclaim hopper	1200	1	1.13	2.40	75	0.283	0.599	1.24	2.62	Chemical Binding
						Total	**2.0**	**4.3**	**8.8**	**18.6**	

Notes:
1) Control efficiencies from *Reasonably Available Control Measures for Fugitive Dust*, Section 2.1 General Fugitive Dust Emission Sources. Environmental Protection Agency, Ohio.
2) All sources are assumed to operate 8760 hours per year as worst case.

Sample calculations (F-31):
Uncontrolled emissions (lb PM_{10} per hour): hourly process rate (3500 tons/hour) x 1 transfers x emission factor (9.44E-04 lb/ton) = 3.30 lb/hr
Controlled emissions (lb PM_{10} per hour): uncontrolled emissions (3.30 lb/hr) x control efficiency [1-(control%/100)] = 3.30 x 0.25 = 0.83 lb/hr

MidAmerican CBEC Unit 4 Project
Unit 4 Coal Handling - Fugitives

Emission factor from AP-42, Section 13.2.4: *Aggregate Handling and Storage Piles* (1/95), Equation (1) - batch or continuous drop operation

E (lb PM_{10} per ton material handled) = k (0.0032) (U/5)^1.3 / [(M/2)^1.4]

where:

k = 0.35	[particles < 10um]
k = 0.74	[particles < 30um]
U = 10.5	[mph, based on Omaha data]
	[used for exposed sources and to conservatively estimate internal ventilation for enclosed sources]
M = 4.5	[%, mean moisture content for coal (as received), Table 13.2.4-1 (coal-fired power plant)

E (lb PM_{10} per ton handled) = 9.44E-04
E (lb PM per ton handled) = 2.00E-03

Source ID	Source Name	Process Rate (ton/hour)	Max # Transfers	Uncontrolled Emissions (lb PM_{10}/hr)	Uncontrolled Emissions (lb PM/hr)	Control %	Controlled Emissions (lb PM_{10}/hr)	Controlled Emissions (lb PM/hr)	Controlled PM_{10} Emissions (tpy)	Controlled PM Emissions (tpy)	Control System and Comments
F-151A	Fugitive from transfer of coal from Conveyor C-11 to Rail Unloading Coal Stockout Pile	3500	1	3.30	6.99	75	0.826	1.747	3.62	7.65	Chemical Binding
F-151C	Fugitives from dumping of coal into the emergency reclaim hopper	1200	1	1.13	2.40	75	0.283	0.599	1.24	2.62	Chemical Binding
						Total	**1.1**	**2.3**	**4.9**	**10.3**	

Notes:
1) Control efficiencies from *Reasonably Available Control Measures for Fugitive Dust*, Section 2.1 General Fugitive Dust Emission Sources. Environmental Protection Agency, Ohio.
2) All sources are assumed to operate 8760 hours per year as worst case.

Sample calculations (F-151A):
Uncontrolled emissions (lb PM_{10} per hour): hourly process rate (3500 tons/hour) x 1 transfers x emission factor (9.44E-04 lb/ton) = 3.30 lb/hr
Controlled emissions (lb PM_{10} per hour): uncontrolled emissions (3.30 lb/hr) x control efficiency [1-(control%/100)] = 3.30 x 0.25 = 0.83 lb/hr

MidAmerican CBEC Unit 4 Project
Total CBEC Material Handling (Grain Loading Method)

PM_{10} ratio 90% (See Note 2)

Source ID	Source Name	Flow Rate (cfm)	Dust Collector Grain Loading (gr/dscf)	Controlled Emissions (lb PM_{10}/hr)	Controlled Emissions (lb PM/hr)	Controlled PM_{10} Emissions (tpy)	Controlled PM Emissions (tpy)	Control System and Comments
NEW Coal Handling Sources								
EP-159	Transfer Conveyor Bay	19,500	0.010	1.51	1.67	6.60	7.34	Dust collector bag filter
EP-160	Unit 4 East Silos	34,800	0.010	2.69	2.99	11.78	13.09	Dust collector bag filter
EP-161	Unit 4 West Silos	26,100	0.010	2.02	2.24	8.84	9.82	Dust collector bag filter
			Total	**6.2**	**6.9**	**27.2**	**30.2**	
Existing/ Modified Coal Handling Sources (Modified sources highlighted in yellow)								
EP-6	Rotary Car Dumper	150,000	0.010	11.60	12.88	50.79	56.43	Dust collector bag filter
EP-9	Transfer House 1	20,900	0.013	2.10	2.33	9.20	10.22	Dust collector bag filter
EP-10	Transfer House 2	12,500	0.013	1.26	1.40	5.50	6.11	Dust collector bag filter
EP-11	Transfer House 3	21,100	0.013	2.12	2.36	9.29	10.32	Dust collector bag filter
EP-13	Transfer House 4	26,900	0.010	2.08	2.31	9.11	10.12	Dust collector bag filter
EP-14	East Coal Silos Unit 3	26,500	0.030	6.15	6.83	26.92	29.91	Dust collector bag filter
EP-15	West Coal Silos Unit 3	22,850	0.030	5.30	5.89	23.21	25.79	Dust collector bag filter
EP-16	Crusher House Units 1&2	11,900	0.013	1.20	1.33	5.24	5.82	Dust collector bag filter
EP-17	Coal Silos Units 1&2	11,200	0.013	1.13	1.25	4.93	5.48	Dust collector bag filter
EP-117	Emergency Reclaim Hopper	-	-	-	-	-	-	See Note 4
			Total	**32.9**	**36.6**	**144.2**	**160.2**	
Fly Ash Handling								
Existing								
EP-20	Fly ash truck loading- Silo Unit 3			1.08	1.30	4.73	5.69	Unloading Spout (values from Title V)
EP-21	Fly ash truck loading- Silo Units1&2			0.21	0.25	0.92	1.10	Unloading Spout (values from Title V)
EP-119A	Fly ash storage silo units 1&2	954	0.100	0.74	0.82	3.23	3.59	Vent bag filter
EP-119B	Fly ash storage silo units 1&2	6	0.100	0.00	0.01	0.02	0.02	Vent bag filter

Source ID	Source Name	Flow Rate (cfm)	Dust Collector Grain Loading (gr/dscf)	Controlled Emissions (lb PM_{10}/hr)	Controlled Emissions (lb PM/hr)	Controlled PM_{10} Emissions (tpy)	Controlled PM Emissions (tpy)	Control System and Comments
Fly Ash Handling								
New								
EP-167	Flyash/ FGD Waste Silo	3,000	0.020	0.46	0.52	2.03	2.26	Vent bag filter
EP-168	Flyash/ FGD Waste Vacuum system exhauster # 1	2,500	0.010	0.19	0.21	0.85	0.94	Filter separator
EP-169	Flyash/ FGD Waste Vacuum system exhauster # 2	2,500	0.010	0.19	0.21	0.85	0.94	Filter separator
EP-170	Flyash/ FGD Waste Vacuum system exhauster # 3	2,500	0.010	0.19	0.21	0.85	0.94	Filter separator
			Total	**3.1**	**3.5**	**13.5**	**15.5**	

Source ID	Source Name	Flow Rate (cfm)	Dust Collector Grain Loading (gr/dscf)	Controlled Emissions (lb PM_{10}/hr)	Controlled Emissions (lb PM/hr)	Controlled PM_{10} Emissions (tpy)	Controlled PM Emissions (tpy)	Control System and Comments
Other Material Handling - New								
EP-162	Lime filter separator	2,000	0.010	0.15	0.17	0.68	0.75	Filter separator
EP-163	Lime silo	1,500	0.020	0.23	0.26	1.02	1.13	Vent bag filter
EP-164A	Urea Silo #1	500	0.020	0.08	0.09	0.34	0.38	Vent bag filter
EP-164B	Urea Silo #2	500	0.020	0.08	0.09	0.34	0.38	Vent bag filter
			Total	**0.5**	**0.6**	**2.4**	**2.6**	
			SHEET TOTAL	**42.8**	**47.6**	**187.2**	**208.6**	

Notes:

(1) All material handling sources are assumed to operate 8760 hours per year as worst case.
(2) PM_{10} estimated as 90% of Total PM based on IDNR guidance.
(3) Rotary Car Dumper Emission Points EP-6 and EP-7 will be modified to include single combined dust collector and stack (EP-6).
(4) EP-117 emissions are captured by Transfer House 2 dust collector (EP-10).
(5) Coal Handling emissions from Transfer House 5 are captured by Transfer House 4 dust collector (EP-13).

sample calculation (EP161):

PM lb/hr = 0.01 gr/dscf * 26,100 cfm * 60 min/hr * 1 lb/6985.4 gr = 2.24 lb/hr

PM_{10} lb/hr = 0.01 gr/dscf * 26,100 cfm * 60 min/hr * 1 lb/6985.4 gr * 90% = 2.02 lb/hr

MidAmerican CBEC Unit 4 Project
Total CBEC Material Handling INCREMENT/ACTUAL (Grain Loading Method)

PM10 ratio 90% *From IDNR*

Source ID	Source Name	Flow Rate (cfm)	Dust Collector Grain Loading (gr/dscf)	Controlled Emissions (lb PM_{10}/hr)	Controlled Emissions (g/s)	Controlled Emissions (lb PM/hr)	Controlled PM_{10} Emissions (tpy)	Controlled PM Emissions (tpy)	Control System and Comments
NEW Coal handling Sources									
EP-159	Transfer Conveyor Bay	19,500	0.010	1.51	0.190	1.67	6.60	7.34	Dust collector bag filter
EP-160	Unit 4 East Silos	34,800	0.010	2.69	0.339	2.99	11.78	13.09	Dust collector bag filter
EP-161	Unit 4 West Silos	26,100	0.010	2.02	0.254	2.24	8.84	9.82	Dust collector bag filter
Existing Coal Handling Sources									
EP-6	Rotary Car Dumper	150,000	0.0100	11.60	1.461	12.88	50.79	56.43	Dust collector bag filter
EP-9	Transfer House 1	22,261	0.0034	0.59	0.074	0.65	2.56	2.85	Dust collector bag filter
EP-10	Transfer House 2	30,946	0.0047	1.12	0.142	1.25	4.92	5.47	Dust collector bag filter
EP-11	Transfer House 3	19,947	0.0036	0.56	0.070	0.62	2.43	2.70	Dust collector bag filter
EP-13	Transfer House 4	26,900	0.0100	2.08	0.262	2.31	9.11	10.12	Dust collector bag filter
EP-14	East Coal Silos Unit 3	21,948	0.0165	2.80	0.353	3.11	12.26	13.62	Dust collector bag filter
EP-15	West Coal Silos Unit 3	18,813	0.0162	2.36	0.297	2.62	10.32	11.47	Dust collector bag filter
Fly Ash handling									
Existing									
EP-20	Fly ash truck loading- Silo Unit 3			1.29	0.163	1.44	5.67	6.30	Unloading Spout (lb/hr values from IDNR modeling)
EP-21	Fly ash truck loading- Silo Units1&2			0.19	0.024	0.21	0.84	0.93	Unloading Spout (lb/hr values from IDNR modeling)
EP-119A	Fly ash storage silo units 1&2			0.01	0.001	0.01	0.04	0.05	Vent bag filter (lb/hr values from IDNR modeling)
EP-119B	Fly ash storage silo units 1&2			0.01	0.001	0.01	0.04	0.05	Vent bag filter (lb/hr values from IDNR modeling)
New									
EP-167	FlyAsh/FGD waste silo	3,000	0.020	0.46	0.058	0.52	2.03	2.26	Vent bag filter
EP-168	FlyAsh/FGD Waste Vacuum system exhauster # 1	2,500	0.010	0.19	0.024	0.21	0.85	0.94	Filter separator
EP-169	FlyAsh/FGD Waste Vacuum system exhauster # 2	2,500	0.010	0.19	0.024	0.21	0.85	0.94	Filter separator
EP-170	FlyAsh/FGD Waste Vacuum system exhauster # 3	2,500	0.010	0.19	0.024	0.21	0.85	0.94	Filter separator
Other material handling									
EP-162	Lime filter separator	2,000	0.010	0.15	0.019	0.17	0.68	0.75	Filter separator
EP-163	Lime silo	1,500	0.020	0.23	0.029	0.26	1.02	1.13	Vent bag filter
EP-164A	Urea Silo #1	500	0.020	0.08	0.010	0.09	0.34	0.38	Vent bag filter
EP-164B	Urea Silo #2	500	0.020	0.08	0.010	0.09	0.34	0.38	Vent bag filter

Note 1: Highlighted dust collector grain loadings and flow rates were obtained from stack testing data, as provided by MidAmerican.

MidAmerican CBEC Unit 4 Project
Inactive Coal Pile- After Unit 4 Modification

Wind Erosion
Reference: Control of Open Fugitive Dust Sources, Section 4.1.3, EPA-450/3-98-008
[Wind Emissions From Continuously Active Piles]

E (lb PM *per day per acre*) = 1.7 (s/1.5) (365-p/235) (f/15)

where:

s =	2.2	silt content % [from AP-42 Table 13.2.4-1 (coal as received at coal-fired power plant)
p =	60	number of days with >0.01 inches precip. per year [from AP-42 Figure 13.2.2-1]
f =	30	percentage of time that wind speed exceeds 5.4 m/s at mean pile height [from Omaha data wind data 1991]
E =	6.5	lb PM per day per acre
E =	3.3	lb PM-10 per day per acre [using PM-10 to PM ratio of 0.5 from EPA-450/3-98-008]

Source ID	Source Name	Coal pile size (acres)	Uncontrolled Emissions (lb PM_{10}/hr)	Uncontrolled Emissions (lb PM/hr)	Control %	Controlled Emissions (lb PM_{10}/hr)	Controlled Emissions (lb PM/hr)	Controlled PM_{10} Emissions (tpy)	Controlled PM Emissions (tpy)	Control System (Note 2)
F-5A	Inactive Coal Storage Pile	14.9	2.02	4.04	99	0.02	0.04	0.09	0.18	Chemical binding
					Total	**0.02**	**0.04**	**0.09**	**0.18**	

Maintenance of Active Pile (Bulldozing)
Reference: AP-42, Table 11.9-1 (Western Surface Coal Mining)

E (lb PM per hour) = 78.4 (s)^1.2 / (M)^1.3
E (lb PM-10 per hour) = (0.75) 18.6 (s)^1.5 / (M)^1.4

where:

s =	2.2	silt content % [from AP-42 Table 13.2.4-1 (coal as received at coal-fired power plant)
M =	4.5	*moisture %* [from AP-42 Table 13.2.4-1 (coal as received at coal-fired power plant)
E =	28.58	lb/hr PM
E =	5.54	lb/hr PM-10

Source ID	Source Name	Coal pile size (acres)	Uncontrolled Emissions (lb PM_{10}/hr)	Uncontrolled Emissions (lb PM/hr)	Control %	Controlled Emissions (lb PM_{10}/hr)	Controlled Emissions (lb PM/hr)	Controlled PM_{10} Emissions (tpy)	Controlled PM Emissions (tpy)	Control System (Note 2)
F-5B	Inactive Coal Storage Pile (See Note 3)		5.54	28.58	75	0.46	2.38	2.02	10.43	Chemical binding
					Total	**0.46**	**2.38**	**2.02**	**10.43**	
	Totals Active Pile (Wind Erosion + Maintenance)					**0.48**	**2.42**	**2.11**	**10.61**	

Notes:
1) Coal pile was ratioed between Units 1-3 and the addition of Unit 4. Units 1-3 burned 3,534,792 tons of coal based on average of years 2000 and 2001. Unit 4 has maximum tpy estimate of 4,202,197 (based on 100% Capacity Factor). Units 4 coal pile = 27.5 acres x 54.3% = 14.9 acres.
2) Control efficiencies from *Reasonably Available Control Measures for Fugitive Dust*, Section 2.1 General Fugitive Dust Emission Sources. Environmental Protection Agency, Ohio.
3) In addition to control % on maintenance of inactive pile, *a factor of 8/24 is incorporated into lb/hr and tpy emission rates to account for maximum daily maintenance of the active pile* (8 hours per day)

MidAmerican CBEC Unit 4 Project
Active Coal Pile- After Unit 4 Modification

Wind Erosion
Reference: Control of Open Fugitive Dust Sources, Section 4.1.3, EPA-450/3-98-008
[Wind Emissions From Continuously Active Piles]

E (lb PM per day per acre) = 1.7 (s/1.5) (365-p/235) (f/15)

where:

s =	2.2	silt content % [from AP-42 Table 13.2.4-1 (coal as received at coal-fired power plant)
p =	60	number of days with >0.01 inches precip. per year [from AP-42 Figure 13.2.2-1]
f =	30	percentage of time that wind speed exceeds 5.4 m/s at mean pile height [from Omaha data wind data 1991]
E =	6.5	lb PM per day per acre
E =	3.3	lb PM-10 per day per acre [using PM-10 to PM ratio of 0.5 from EPA-450/3-98-008]

Source ID	Source Name	Coal pile size (acres)	Uncontrolled Emissions (lb PM_{10}/hr)	Uncontrolled Emissions (lb PM/hr)	Control %	Controlled Emissions (lb PM_{10}/hr)	Controlled Emissions (lb PM/hr)	Controlled PM_{10} Emissions (tpy)	Controlled PM Emissions (tpy)	Control System (Note 2)
F-4A	Active Coal Storage Pile	3.9	0.53	1.06	75	0.13	0.26	0.58	1.16	Chemical binding
F-151B (Unit 4)	Rail Unloading Coal Stockout Pile	0.65	0.09	0.18	75	0.02	0.04	0.10	0.19	Chemical binding
					Total	**0.15**	**0.31**	**0.68**	**1.35**	

Maintenance of Active Pile (Bulldozing)
Reference: AP-42, Table 11.9-1 (Western Surface Coal Mining)

E (lb PM per hour) = 78.4 (s)^1.2 / (M)^1.3

E (lb PM-10 per hour) = (0.75) 18.6 (s)^1.5 / (M)^1.4

where:

s =	2.2	silt content % [from AP-42 Table 13.2.4-1 (coal as received at coal-fired power plant)
M =	4.5	moisture % [from AP-42 Table 13.2.4-1 (coal as received at coal-fired power plant)
E =	28.58	lb/hr PM
E =	5.54	lb/hr PM-10

Source ID	Source Name	Coal pile size (acres)	Uncontrolled Emissions (lb PM_{10}/hr)	Uncontrolled Emissions (lb PM/hr)	Control %	Controlled Emissions (lb PM_{10}/hr)	Controlled Emissions (lb PM/hr)	Controlled PM_{10} Emissions (tpy)	Controlled PM Emissions (tpy)	Control System (Note 2)
F-4B (Unit 4)	Active Coal Storage Pile (See Note 3)		5.54	28.58	75	0.46	2.38	2.02	10.43	Chemical binding
					Total	**0.46**	**2.38**	**2.02**	**10.43**	
	Totals Active Pile (Wind Erosion + Maintenance)					**0.62**	**2.69**	**2.70**	**11.78**	

Notes:

1) Coal pile was ratioed between Units 1-3 and the addition of Unit 4. Units 1-3 burned 3,534,792 tons of coal based on average of years 2000 and 2001. Unit 4 has maximum tpy estimate of 4,202,197 (based on 100% Capacity Factor). Units 4 coal pile = 7.1 acres x 54.3% = 3.9 acres.
2) Control efficiencies from *Reasonably Available Control Measures for Fugitive Dust*, Section 2.1 General Fugitive Dust Emission Sources. Environmental Protection Agency, Ohio.
3) In addition to control % on maintenace of active pile, a factor of 8/24 is incorporated into lb/hr and tpy emission rate to account for maximum daily maintenance of the active pile (8 hours per day)

MidAmerican Unit 4 Project
Units 1, 2 & 3 Paved Ash Haul Roads (F-903)

Paved Roads emission factor from AP-42, Section 13.2.1: Paved Roads (10/97)

k(sL/2)^.65(W/3)^1.5

where:

k = 0.016	[Table 13.2.1-1, for PM_{10}]		
k = 0.082	[Table 13.2.1-1, for Total PM]		
s = 8.2	[silt loading (%) for quarry road, Table 13.2.1-3]		
W= 32.5	[mean vehicle weight(tons)]	[empty truck= 17.5 tons, loaded = 47.5 tons]	Provided by MidAmerican
E_U = 1.427	[PM_{10}]		
E_U = 7.316	[PM]		

Haul truck maximum load =	30 tons per truck		Provided by MidAmerican
Amount Fly Ash produced =	151,800 tons		Average of 2000/2001 inventory
Percentage trucked =	91.4%		Actual for 2000/2001
Flyash hauled (per year) =	138,745 tons		
Amount FGD Waste produced:	0 tons		
Percentage trucked =	100%		
FGD Waste hauled (per year) =	0 tons		
Total amount hauled (per year) =	138,745 tons		
Amount hauled (per day) =	271.5 tons	[10 hr/day, 5 days/wk]	Provided by MidAmerican
Hauling hours per day =	10 hours		
Amount hauled (per hour) =	27.2 tons		
Haul road round trip =	2.50 miles	[6,596 ft one way]	Provided by MidAmerican
Round trips per hour =	0.91		
Round trips per year =	4,624.84		
VMT (per hour) =	2.3 miles		
VMT (annual) =	11,555 miles		

Source ID	Source Name	Maximum Uncontrolled Emissions (lb PM/hr)	Annual Uncontrolled PM Emissions (tpy)	Maximum Uncontrolled Emissions (lb PM_{10}/hr)	Annual Uncontrolled PM_{10} Emissions (tpy)	Control %	Maximum Controlled Emissions (lb PM_{10}/hr)	Maximum Controlled Emissions (lb PM/hr)	Annual Controlled PM_{10} Emissions (tpy)	Annual Controlled PM Emissions (tpy)	Control System
F-903	Paved haul roads	16.54	42.27	3.23	8.25	75.00	0.81	4.14	2.06	10.57	Street Sweeper and Covered Ash Trucks

Notes:

1) Flyash produced in 2000 was 147,300 tons. 26,600 tons were sold and transferred off site by truck. Flyash prodcued in 2001 was 156,300 tons. 55,100 tons were sold, 42,000 transferred off site by truck and 13,100 by rail. The average percentage trucked on haul roads was calculated as the average flyash produced for 2000 and 2001 minus the ash sold that was transferred by rail.

2) Flyash from Units 1, 2 and 3 will be disposed of in off site landfill.

3) Control efficiencies from *Reasonably Available Control Measures for Fugitive Dust*, Section 2.1 General Fugitive Dust Emission Sources. Environmental Protection Agency, Ohio.

MidAmerican Unit 4 Project
Unit 4 Paved Ash Haul Roads (F-904)

Paved Roads emission factor from AP-42, Section 13.2.1: Paved Roads (10/97)

k(sL/2)^.65(W/3)^1.5

where:

k = 0.016	[Table 13.2.1-1, for PM_{10}]		
k = 0.082	[Table 13.2.1-1, for Total PM]		
s = 8.2	[silt loading (%) for quarry road, Table 13.2.1-3]		
W= 32.5	[mean vehicle weight(tons)]	[empty truck= 17.5 tons, loaded = 47.5 tons]	Provided by MidAmerican
E_U = 1.427	[PM_{10}]		
E_U = 7.316	[PM]		

Haul truck maximum load =	30 tons per truck		Provided by MidAmerican
Amount Fly Ash produced =	188,257 tons		Provided by Sargent & Lundy
Percentage trucked =	100%		Based on worst case
Flyash hauled (per year) =	188,257 tons		
Amount FGD Waste produced:	165,989 tons		Provided by Sargent & Lundy
Percentage trucked =	100%		
FGD Waste hauled (per year) =	165,989 tons		
Total amount hauled (per year) =	354,246 tons		
Amount hauled (per day) =	693.2 tons	[10 hr/day, 5 days/wk]	Provided by MidAmerican
Hauling hours per day =	10 hours		
Amount hauled (per hour) =	69.3 tons		
Haul road round trip =	2.08 miles	[5,484 ft one way]	Provided by MidAmerican
Round trips per hour =	2.31		
Round trips per year =	11,808.20		
VMT (per hour) =	4.8 miles		
VMT (annual) =	24,529 miles		

Source ID	Source Name	Maximum Uncontrolled Emissions (lb PM/hr)	Annual Uncontrolled PM Emissions (tpy)	Maximum Uncontrolled Emissions (lb PM_{10}/hr)	Annual Uncontrolled PM_{10} Emissions (tpy)	Control %	Maximum Controlled Emissions (lb PM_{10}/hr)	Maximum Controlled Emissions (lb PM/hr)	Annual Controlled PM_{10} Emissions (tpy)	Annual Controlled PM Emissions (tpy)	Control System
F-904	Paved haul roads	35.12	89.73	6.85	17.51	75.00	1.71	8.78	4.38	22.43	Street Sweeper and Covered Ash Trucks

Notes:

1) The combination of flyash and FGD waste product will be collected from the Unit 4 baghouse, stored in a silo, and transported to an off site landfill.
2) Control efficiencies from *Reasonably Available Control Measures for Fugitive Dust*, Section 2.1 General Fugitive Dust Emission Sources. Environmental Protection Agency, Ohio.

CLEAN COAL TECHNOLOGY

The JEA Large-Scale CFB Combustion Demonstration Project

The JEA Large-Scale CFB Combustion Demonstration Project

A report on a project conducted jointly under
a Cooperative Agreement between:
The U.S. Department of Energy and JEA

Cover Picture:

Three views of JEA Northside Station, Jacksonville, Florida

CLEAN COAL TECHNOLOGY

The JEA Large-Scale CFB Combustion Demonstration Project

Executive Summary

The Clean Coal Technology (CCT) Demonstration Program is a government and industry co-funded effort to demonstrate a new generation of innovative coal utilization processes in a series of facilities built across the country. These projects are carried out on a commercial scale to prove technical feasibility and provide the information required for future applications.

The goal of the CCT Program is to furnish the marketplace with a number of advanced, more efficient coal-based technologies that meet strict environmental standards. Use of these technologies is intended to minimize the economic and environmental barriers that limit the full utilization of coal.

To achieve this goal, beginning in 1985, a multi-phased effort consisting of five separate solicitations was administered by the U.S. Department of Energy's (DOE) National Energy Technology Laboratory (NETL). Projects selected through these solicitations have demonstrated technology options with the potential to meet the needs of energy markets while satisfying relevant environmental requirements.

Part of this Program is the demonstration of advanced electric power generation technologies, including circulating fluidized bed combustion (CFB). This report discusses the JEA Large-Scale CFB Combustion Demonstration Project which is testing the CFB concept using inexpensive feedstocks such as high sulfur coal and coal fuel blends.

The project is being conducted at the Northside Generating Station of JEA (formerly Jacksonville Electric Authority) in Jacksonville, Florida, and JEA is the project Participant. Foster Wheeler Energy Corporation, the technology supplier, is an additional team member.

To date, the JEA Project has operated CFBs to generate electricity at a scale larger than previously demonstrated. The boilers at the Northside Station are the largest CFBs in the world. Power production on coal feed meets the target goal of 297.5 MWe gross (265 MWe net). Emissions of atmospheric pollutants are below the stringent limits set for this project. A two-year demonstration test program is planned to evaluate the operational and environmental performance of the CFB system.

JEA plant with CFB boilers in center and fuel storage domes in background

The JEA Large-Scale CFB Combustion Demonstration Project

Background

The Clean Coal Technology (CCT) Demonstration Program, sponsored by the U.S. Department of Energy (DOE) and administered by the National Energy Technology Laboratory (NETL), has been conducted since 1985 to develop innovative, environmentally friendly coal utilization processes for the world energy marketplace.

The CCT Program, which is co-funded by industry and government, involves a series of demonstration projects that provide data for design, construction, operation, and technical/economic evaluation of full-scale applications. The goal of the CCT Program is to enhance the utilization of coal as a major energy source.

Fluidized Bed Combustion

Among the technologies being demonstrated in the CCT Program is fluidized bed combustion (FBC). FBC is an advanced electric power generation process that minimizes the formation of gaseous pollutants by controlling coal combustion parameters and by injecting a sorbent (such as crushed limestone) into the combustion chamber along with the fuel. In the JEA project described in this report, the fuel is coal or a blend of coal and petroleum coke. Crushed fuel mixed with the sorbent is fluidized on jets of air in the combustion chamber. Sulfur released from the fuel as sulfur dioxide (SO_2) is captured by the sorbent in the bed to form a solid compound that is removed with the ash. The resultant by-product is a dry, benign solid that can be disposed of easily or used in agricultural and construction applications. More than 90% of the sulfur in the fuel is captured in this process.

An additional environmental benefit of FBC power plants results from their relatively low operating temperature, which significantly reduces formation of nitrogen oxides (NOx).

Five FBC demonstration projects are included in the CCT Program under Advanced Electric Power Generation: (1) the JEA Large-Scale CFB Combustion Demonstration Project, (2) the Nucla CFB Demonstration Project, (3) the Tidd PFBC Demonstration Project, (4) the McIntosh Unit 4A PCFB Demonstration Project, and (5) the McIntosh Unit 4B Topped PCFB Demonstration Project. This Topical Report describes the JEA project.

Panoramic view of JEA site

Project Description

The JEA Large-Scale CFB Combustion Demonstration Project consists of installing a new 300-MWe (297.5-MWe nameplate) atmospheric circulating fluidized bed (ACFB) boiler in conjunction with an existing turbine generator at JEA's Northside Generating Station (Unit 2) in Jacksonville, Florida. In parallel with this project, JEA replaced the Unit 1 oil/gas fired boiler with an identical ACFB unit. Unit 1 continues to use its existing turbine generator.

These boilers are designed to burn fuel blends consisting of coal and petroleum coke, thereby greatly reducing plant fuel costs and maintaining fuel flexibility while meeting stringent emissions limits. These units are the world's largest ACFB boilers.

In this project, the existing Unit 2 turbine generator was upgraded, and other existing balance-of-plant (BOP) equipment and systems were either upgraded or replaced. The existing turbine building and some piping systems were re-utilized.

Steam from the combustor is used in an existing General Electric 297.5-MWe (nameplate) turbine to produce electric power. With parasitic power consuming 32.5 MWe, net power output is 265 MWe.

JEA Large-Scale CFB Combustion Demonstration Project

Project Participants and Responsibilities

JEA

- Overall project and construction management
- Funding ($234 million)
- Environmental permitting

U.S. DOE

- Funding ($75 million)
- Technology support/dissemination

Foster Wheeler Energy Corporation (Clinton, NJ)

- Design and supply of CFBs
- Engineering/procurement/construction for the extended boiler island, including CFBs, scrubbers, fabric filters, stack, and fuel and limestone preparation facilities

Black & Veatch (Kansas City, MO)

- Design of BOP and materials handling systems

Zachry Construction Corporation (San Antonio, TX)

- Procurement and construction of BOP system upgrades and replacements, including condensate, feedwater, and circulating water systems; water and wastewater treatment systems; distributed control system; station electric distribution system; and substation equipment

Fluor Global Services (Irvine, CA)

- Upgrade/uprate of turbine/generators
- Procurement and construction of materials handling systems, including continuous ship unloader (purchased by JEA), pier, conveyors, fuel storage domes, and fuel and limestone reclaim equipment

Project Participant

The Participant is JEA, who provided the host site. An additional team member is Foster Wheeler Energy Corporation (FWEC), who supplied the ACFB technology.

Fuel Supply

Coal feed is an Eastern bituminous coal having a sulfur content of 3.39 wt%. Petroleum coke having a sulfur content as high as 8% also serves as feed, either alone or in combination with coal.

Project Scale

The JEA project represents a scale-up of previous ACFB installations. The Nucla project, completed in 1992, had a capacity of 100 MWe (net) and the Tidd project, completed in 1995, had a capacity of 70 MWe (net). The McIntosh Unit 4A project (currently on hold) is designed for a capacity of 137 MWe (net), and the McIntosh Unit 4B project (also on hold) has a design capacity of an additional 103 MWe (net). At a nominal design capacity of 300 MWe gross (265 MWe net), the JEA project is the largest scale demonstration of FBC technology to date.

Jacksonville

A half century after Ponce de Leon claimed Florida for Spain, Frenchman Jean Ribault sailed into the St. Johns River to establish Fort Caroline for French Huguenot settlers. Within several years, Spanish forces from the military garrison at St. Augustine would destroy this small settlement.

In 1821, Spain ceded Florida to the United States, and one year later Isaiah D. Hart surveyed the village. He named it Jacksonville for General Andrew Jackson, the territory's first military governor.

Today, located at the crossroads of two transcontinental highways, Jacksonville is one of the Nation's largest cities in land area (841 square miles), a major port, site of Navy bases, and home of the NFL Jacksonville Jaguars, a Mayo Clinic medical center, and the Jacksonville Zoological Gardens. The area boasts beautiful beaches and numerous waterways for over 700,000 residents.

Process Description

Coal fuel blends, along with primary air and a solid sorbent such as limestone, are introduced into the lower part of the combustor, where initial combustion occurs. As the fuel particles decrease in size due to combustion, they are carried higher in the combustor where secondary air is introduced. As the particles continue to be reduced in size the fuel, along with some of the sorbent, is carried out of the combustor, collected in a cyclone separator, and recycled to the lower portion of the combustor. Primary removal of sulfur is achieved by reaction with the sorbent in the bed. Additional SO_2 removal is achieved through the use of a downstream polishing scrubber using a spray dryer absorber (SDA). Fabric filters are used for particulate control.

Furnace temperature is maintained in the range of 1500 to 1700°F by efficient heat transfer between the fluid bed and the water walls in the boiler. This relatively low operating temperature inherently results in appreciably lower NOx emissions compared with PC-fired power plants. However, the project also includes a new selective non-catalytic reduction (SNCR) system, using reaction with ammonia to further reduce NOx emissions to very low levels as required by the stringent environmental regulations for the JEA project.

Steam is generated in tubes placed along the walls of the combustor and superheated in tube bundles placed downstream of the particulate separator to protect against erosion. The system produces approximately 2 million lb/hr of main steam at 2,500 psig and 1,000°F, and 1.73 million lb/hr of reheat steam at 548 psig and 1,000°F. The steam flows to the turbine/generator, where electric power is produced. The design heat rate is 9,950 Btu/kWh (34% overall thermal efficiency, higher heating value basis).

The JEA CCT project incorporates several advanced features including a patented integrated recycle heat exchanger (INTREX™) in the furnace.

Two 400-foot diameter by 140-foot high aluminum geodesic domes for fuel storage

Limestone conveyors

Details of the JEA Project Systems

Limestone Preparation System

The limestone preparation system grinds and dries raw limestone and pneumatically transports it to the limestone storage silo for each Unit. The limestone grinding system consists of three rod mills with accessories. The mills are sized for grinding limestone at a maximum feed size of 1 inch to a product size of -2000 microns (approximately 1/16 inch), meeting the CFB desired product distribution curve, with a residual moisture content of 1% maximum.

Three pneumatic transfer systems are provided to convey the prepared limestone from the preparation building to the unit's silo. Each silo has a bin vent filter to control dust emissions. Each system is sized for 50 tons per hour (tph) capacity and is capable of transferring limestone to either Unit 1 or 2.

The control system for the limestone preparation system uses a programmable logic controller (PLC) with a cathode ray tube (CRT)-based operator interface located in the material handling control room. A digital communication interface is furnished to tie this local control system into the plant's distributed control system (DCS).

Air Quality Control System

To optimize overall plant performance, a polishing SO_2 scrubber was included in the design. The polishing scrubber is an SDA/baghouse combination. The SDA utilizes a dual fluid nozzle atomized with air, and the baghouse is a pulse-jet design. A key feature of the polishing scrubber is a recycle system which adds fly ash to the reagent feed, thus utilizing the unreacted lime in the fly ash from the CFB boiler and reducing the amount of fresh lime required.

The polishing scrubber for each unit, provided by Wheelabrator Air Pollution Control, consists of:

- A two-fluid nozzle SDA
- A medium-pressure pulse jet fabric filter (FF)
- A feed slurry preparation system
- A common sorbent preparation system, consisting of a lime storage silo, redundant vertical ball mill slaking systems, and redundant transfer/storage tanks and pumps
- A common air compressor system to provide atomizing air for the SDA, dried pulse air for the FF, and instrument air. The compressors are provided with a closed loop cooling system. Waste heat from the compressor is used to preheat the reuse water feed to the SDA feed slurry system.

Turbine Generator and Balance of Plant Systems

The Units 1 and 2 turbine generators were upgraded to maximize output and improve turbine heat rate as much as practical. The high pressure/intermediate pressure rotor, diaphragms, and inner casing were replaced with a GE Dense Pack design, which added four stages to the turbine and increased turbine efficiency. The normal operating throttle pressure was also increased from 2400 psig to 2500 psig. In addition, the original mechanical linkage type turbine control system was replaced with a state-of-the-art Mark VI electrohydraulic control system to allow better response to load changes and for complete integrated control, protection, and monitoring of the turbine generator and accessories. A new brushless excitation system was also installed on each generator, and a new turbine lube-oil conditioner was installed (Unit 2 only).

Unit 2 was originally designed to provide power to the JEA grid at 138 kV. However, to better interface with present and future grid capabilities, the output from Unit 2 was increased to 230 kV. This required replacement of the generator step-up transformer and associated substation upgrades.

The once-through circulating water system was upgraded by replacing the original 90% copper/10% nickel heat-transfer surfaces in the condenser damaged by erosion/corrosion with modular bundles consisting of titanium tubes welded to solid titanium tubesheets. The existing circulating water pumps were replaced with larger capacity pumps. The traveling screens were replaced with those that have man-made basket material to increase their life. Debris filters were added to minimize condenser tube pluggage and possible damage. A sodium hypochlorite shock-treatment system was installed to prevent sea life from adhering to the titanium components of the condenser.

Upgrades to the condensate system in Units 1 and 2 included upgrading the condensate pumps and condensate booster pumps, replacement of the steam packing exhausters, replacement of the LP feedwater heaters, including replacement of the tube bundle in the lowest pressure heater (located in the condenser neck), replacement of the deaerator and storage tank, installation of a new con-

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Environmental Considerations

The JEA project site is located in North Jacksonville, an environmentally sensitive area surrounded by wetlands. A major goal of the project is to minimize emissions of solid, liquid and gaseous wastes. JEA is committed to making Jacksonville "the premier city in the Southeast in which to live and do business." Through consultation with community and environmental groups including the Sierra Club Northeast Florida Group, JEA agreed to emissions limits that are significantly lower than those specified by current EPA regulations.

Sierra Club Agreement

As part of the agreement with the Sierra Club, baseline stack emission rates at JEA for Units 1, 2, and 3 in 1994-1995, in tons/yr of certain substances, were identified. Target annual emissions rates representing a 10% reduction in each of these components were calculated, and a penalty of $1000/ton was established for any emissions exceeding these rates regardless of whether such emissions are allowable under any permit or authorization. Payments are to be made to the Jacksonville Environmental Protection Board, earmarked for public environmental education. The stack emissions involved in this agreement are NOx, SO_2, particulate matter, CO, and volatile organic compounds (VOCs). In addition, the utility negotiated limits for trace metals.

JEA also agreed to reduce groundwater consumption by at least 10%, and a penalty of $1000/million gallons was established for any groundwater usage at JEA exceeding the agreed upon rate of 208.4 million gallons/yr, regardless of whether such usage is allowable under any permit or authorization.

These reductions in stack emissions and groundwater consumption are especially significant in light of the fact that total power production at JEA after repowering is about 2.7 times as great as the baseline level.

Wetlands adjoining the JEA Plant site

Timucuan Ecological and Historic Preserve

Designated February 16, 1988

The 46,000 acre Timucuan Ecological and Historic Preserve was established in 1988 to protect one of the last unspoiled coastal wetlands on the Atlantic Coast and to preserve historic and prehistoric sites within the area. The estuarine ecosystem includes salt marsh, coastal dunes, and hardwood hammock as well as salt, fresh, and brackish waters. All of these are rich in native vegetation and animal life.

The Preserve was inhabited by the native Timucuan people for over 4,000 years before the arrival of the first Europeans. The Timucuan Preserve has within its boundaries federal, state, and city park lands and over 300 private landowners.

densate polisher (Unit 2 only), and installation of new chemical feed systems (Unit 2 only). The new feedwater heaters included Type 304 N stainless steel tubes (welded to tubesheets), instead of the aluminum brass tubes rolled into the tubesheets of the original heaters.

Upgrades to the feedwater system in Unit 2 included replacement of the HP feedwater heaters, upgrading of boiler feed pumps and fluid drives, and replacement of the boiler feed pump drive motor. Again, the new feedwater heaters included Type 304 N stainless steel tubes (welded to tubesheets), instead of the aluminum brass tubes rolled into the tubesheets of the original heaters.

The capability of existing piping systems and components was reviewed to confirm adequacy for the new operating and design conditions, and where necessary they were upgraded or replaced. Existing 2-inch and larger valves in Unit 2 were either refurbished or replaced. Nearly all 2-inch and smaller piping and valves in Unit 2 were replaced. Essentially all instrumentation in Unit 2 was replaced.

The original control systems in Units 1 and 2 were replaced with a new DCS provided by ABB Inc, to provide control, monitoring, and protection of the boiler, turbine interfaces, and BOP systems. Foster Wheeler provided the logic design for the CFB boiler, and Black & Veatch provided the logic design for the BOP systems, including provisions for turbine water induction prevention. ABB provided the programming to implement the logic design for the boiler and BOP systems.

The Units 1 and 2 auxiliary electric systems (switchgear and motor control centers) were replaced because of equipment obsolescence. All power and control wiring was replaced due to the age of the wiring and because the existing control wiring was not segregated from the power wiring, thus not meeting the requirements of the new DCS.

Other miscellaneous modifications included the installation of additional air dryers and screw-type air compressors as well as the installation of titanium plate-type heat exchangers for the Unit 2 closed cooling water system, similar to those previously installed in Unit 1.

Fuel Handling System

The function of the fuel handling system is to receive petroleum coke, coal, and limestone and convey it to stock-out and storage areas. The materials are reclaimed and conveyed to the in-plant fuel silos and to the limestone preparation system for limestone sorbent.

Receiving System

Solid fuels and limestone are received at the Northside river terminal. A new 800-ft dock and over 2 miles of new belt conveyors were installed as part of the project. Fuels are delivered in 60,000-ton capacity ships and limestone in 40,000-ton ships. The fuel ships are unloaded by a state-of-the-art continuous bucket type unloader rated at 1,666 tph for coal and 1,500 tph for petroleum coke. The unloader is guided by a sophisticated electronic control system. Limestone is unloaded at a rate of 2,800 tph.

Solid fuels are stored in two 400-ft diameter by 140-ft high geodesic domes, made of aluminum, having a capacity of 60,000 tons. These domes serve to keep the fuel dry and to reduce fugitive dust emissions as well as storm water runoff. They are built with only outside support structures to eliminate pyramiding of coal dust in the interior.

Reclaim Systems

The reclaim systems used for moving feed materials from storage to the boilers are redundant. Each storage facility can provide sufficient reclaim rate for the two operating units. With two storage domes and two stacker/reclaimers, the coal and petroleum coke can be blended. Each reclaim system can deliver coal or petroleum coke at a rate of up to 600 tph.

Common Equipment

Dust suppression systems are provided at all material transfer points. The systems are of the foam type and directly control dust emissions at all transfer areas except the crusher building and the area adjacent to and above the in-plant storage silos, which have dust collectors. Reuse water is used for the foam type dust suppression system.

Dust collection systems collect and return the dust to the surge bins, or downstream of the collection points in the case of the collection points in the crusher building. The dust collected in the in-plant storage silo area is returned to one of two in-plant fuel storage silos.

A PLC based control system controls the fuel handling system and is provided with remote control for belt conveyors and associated equipment and necessary interlock control for the conveyors and machines (ship unloader and stacker/reclaimers).

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Emissions Targets

Design emission rate for NOx is 0.09 lb/million Btu, which is achieved by the use of relatively low operating temperatures in the CFB coupled with post-combustion reduction of NOx via SNCR.

For SO_2, the design emission rate is 0.15 lb/million Btu, which is achieved through the use of a sorbent for sulfur capture in the combustor, coupled with scrubbing of the flue gas.

For particulate matter having a diameter of 10 microns (µm) or less (PM_{10}), the design emission rate is 0.011 lb/million Btu. Fabric filters are used to achieve this low level of particulate emissions.

Fugitive emissions are controlled by minimizing the number of bulk material transfer points, enclosing conveyors and drop points, enclosing the fuel storage area, and using wet suppression for particulates.

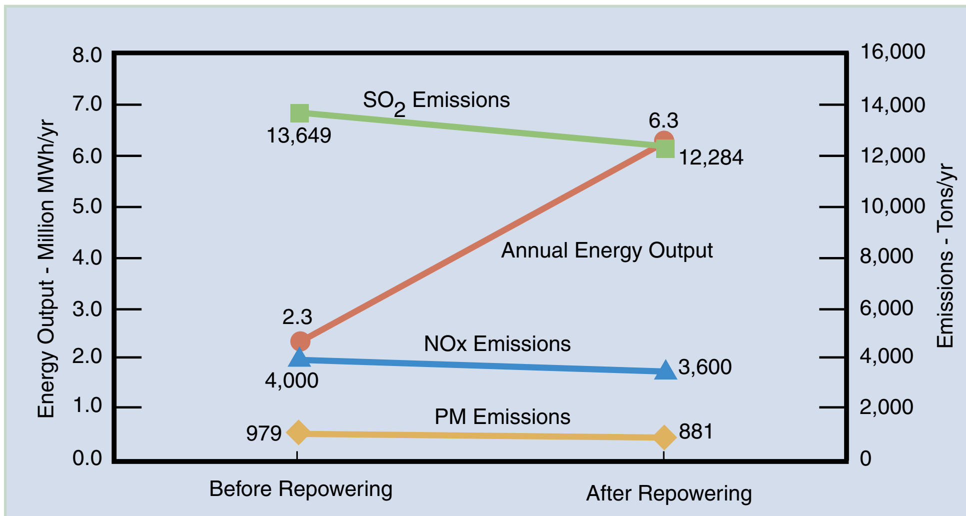
The reduction in groundwater consumption is achieved by using treated wastewater from a nearby municipal facility for certain plant applications.

Project Cost

The estimated cost of the JEA Large-Scale CFB Combustion Demonstration Project is $309 million, of which the Participant provided $234 million (76%) and DOE provided $75 million (24%). The repowering of Unit 1, which is not cost shared by DOE, is not included in this cost figure.

Stack Emission Rates in Sierra Club Agreement

Parameter	Existing Facility Units 1 and 3, tons/yr	Reductions from 1994/1995 Base-line, tons/yr (10% reduction)	Proposed Facility Units 1, 2, and 3, tons/yr
NOx	4,000	400	3,600
SO_2	13,649	1,365	12,284
Particulate Matter	979	98	881
CO	--	--	3,066
VOC (computed as 4% of CO)	--	--	123



Comparison of anticipated annual energy output and emissions before and after repowering

Fuel storage dome under construction

Ash Handling System

The ash handling system transports bed ash from the outlets of the stripper coolers to the bed ash silos, and fly ash from the economizer, air heater hoppers, and baghouse hoppers to the fly ash silos. Two sets of ash handling systems and associated equipment are provided, one for Unit 1 and the other for Unit 2. The bed ash mechanical conveying system and fly ash vacuum conveying system in turn consist of two fully independent parallel lines. Normally any one line is in operation and the other is an installed spare; however, in an emergency upset condition, both lines can be operated simultaneously.

The bed ash and fly ash from the ash silos is slurried using reclaimed water, mixed together, and pumped as a dense slurry to the by-product storage area.

Reuse Water System

Reuse water is domestic wastewater that has been treated and disinfected to a high degree and reused for beneficial purposes. The reuse water used at Northside Generating Station is obtained from the District II Water Reclamation Facility, transported via an eight-mile pipeline. The wastewater is treated through primary, secondary and advanced treatment. During primary treatment, large solids are removed. Secondary treatment uses microorganisms to remove the remaining solids and organic material.

After secondary treatment, the wastewater travels through cloth membrane filters, with a pore size of approximately 10 microns, to remove virtually all remaining solids. During advanced or final treatment, the wastewater is disinfected using chlorine or ultraviolet light to destroy bacteria, viruses and other pathogens.

Consumption of reuse water is expected to be more than 1 million gallons/day when all three units are operating. The reuse water is used for circulating water pump seals, boiler/precipitation area drains, polishing scrubbers, ash slurry preparation, and fuel handling dust suppression and wash down. Future uses may include irrigation.

Limestone preparation system

Project History

DOE selected the Large-Scale CFB Combustion Demonstration Project in June 1989 as part of Round I of the CCT Program. After a number of host sites were considered, the project was resited in August 1997 to Jacksonville, Florida. The Cooperative Agreement was signed in September 1997.

The Environmental Impact Statement for the Jacksonville site, as required by the National Environmental Policy Act, was completed in December 2001.

JEA Background

JEA is the largest municipal power company in Florida and the eighth largest municipal utility in the United States. JEA currently serves nearly 350,000 customers and is experiencing a load growth rate of more than 3% per year. Most municipal utilities in the United States do not generate their own power. Those that do so are relatively small, generating 25 MWe or less. Many of these small utilities use diesel engines for power generation. JEA is one of very few municipal utilities having an installed capacity of greater than 300 MWe.

Prior to the Large-Scale CFB Demonstration Project, JEA's Northside Station consisted of three oil/gas fired steam electric generating units. Units 1 and 2 were each nominally rated at 275 MWe and Unit 3 at 518 MWe. Units 1 & 3 had been in service since 1966 and 1977 respectively. Unit 2 was completed in 1972, but had been inoperable since about 1983 due to major boiler problems.

As part of its Integrated Resource Planning Study in 1996, JEA concluded that additional base load capacity was needed to support Jacksonville's growing need for energy. With demand growing, JEA executives saw that the utility's ability to generate all of the electricity required by its customers—something JEA had done for 100 years—would be compromised early in the 21st century unless it soon began planning new facilities.

The optimum source for that additional capacity was determined to be repowering Unit 2 with a state-of-the-art ACFB boiler fueled by coal fuel blends. To provide the project with an overall environmental benefit, increase the economies of scale, and further diversify JEA's fuel mix, a decision was made to repower Unit 1 with an identical ACFB boiler as well. The DOE cost sharing does not cover the Unit 1 repowering.

The environmental benefits include a reduction in emissions of NOx, SO_2, and particulate matter by at least 10% compared to 1994/1995 levels. As a result of increased generating capacity and improved capacity factor, total power production was planned to increase from about 2.3 million MWh/yr to about 6.3 million MWh/yr, an increase of about 170%. An additional economic benefit results from the fact that, prior to the repowering project, Units 1 and 3 fired relatively high cost fuels, resulting in limited dispatch of these units. As a result of the repowering, both Unit 1 and Unit 2 are now capable of firing relatively low cost solid fuels. The use of these fuels, which can be delivered by ship, takes full advantage of JEA's existing strategic assets including access to the St. Johns River.

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Process Flowsheet

Coal or coal fuel blends are crushed to about ¼ inch diameter and mixed with limestone crushed to the size of sand. The fuel is gravimetrically metered and swept with heated combustion air into the base of the combustor. Limestone is injected into the same area of the combustor by the use of positive displacement blowers.

As the solid mixture rises, it ignites and begins a controlled “slow burn.” The slow burn process maintains temperatures below 1600°F across a large area, minimizing the production of pollutants. At temperatures above 1600°F, production of NOx increases significantly.

As the fuel particles burn, they become lighter and, with the help of additional air that constantly turns the particles over in a fluid-like motion, they are carried higher in the combustor. The limestone absorbs about 90% of the sulfur in the fuel (as SO_2).

At the cyclone inlet located at the top of the combustor, aqueous ammonia is injected into the flue gas to further reduce NOx produced in the furnace, converting it to molecular N_2. The cyclones provide for efficient mixing of the flue gas and ammonia as well as sufficient residence time at the optimum operating temperature for effective NOx reduction.

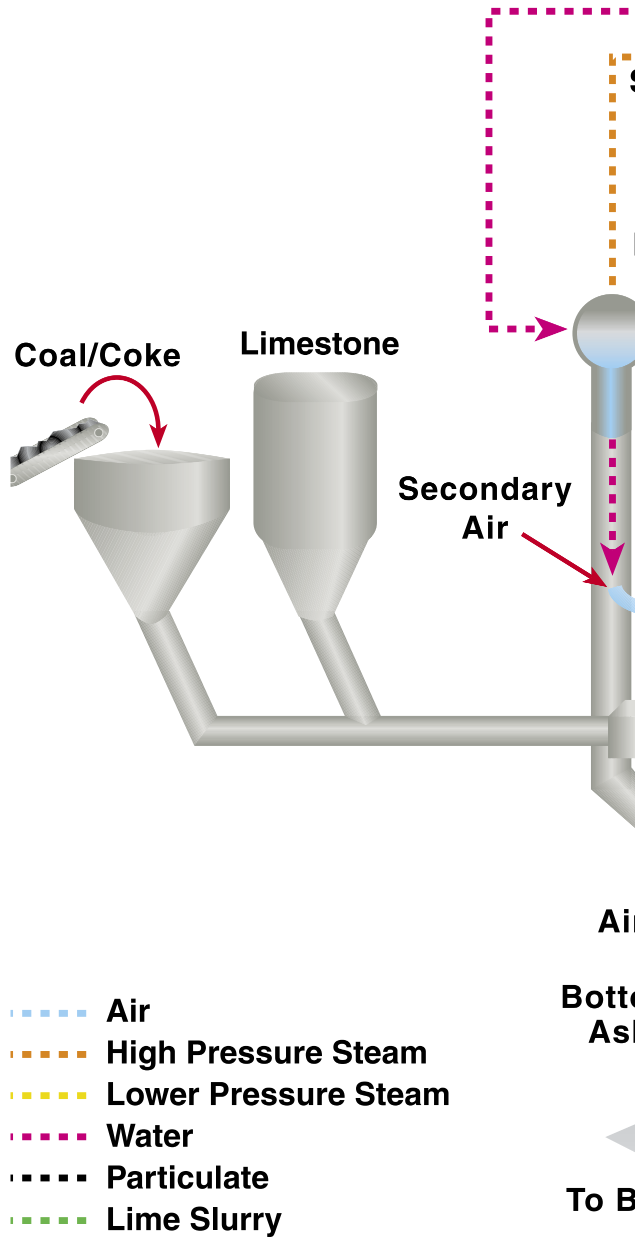
The hot ash and limestone pass through the INTREX™ exchanger before being recycled to the bottom of the combustor. In the INTREX™ exchanger, superheated steam is produced in tubes over which the hot ash returning to the combustor flows.

The steam flows into the cyclone inlet panels, through the cyclone walls, into the convection cage wall, through the primary superheater, and into the intermediate and finishing superheaters which reside within the INTREX™ exchanger. Solid material, consisting primarily of ash and $CaSO_4$, is removed from the bottom of the combustor and sent to by-product storage.

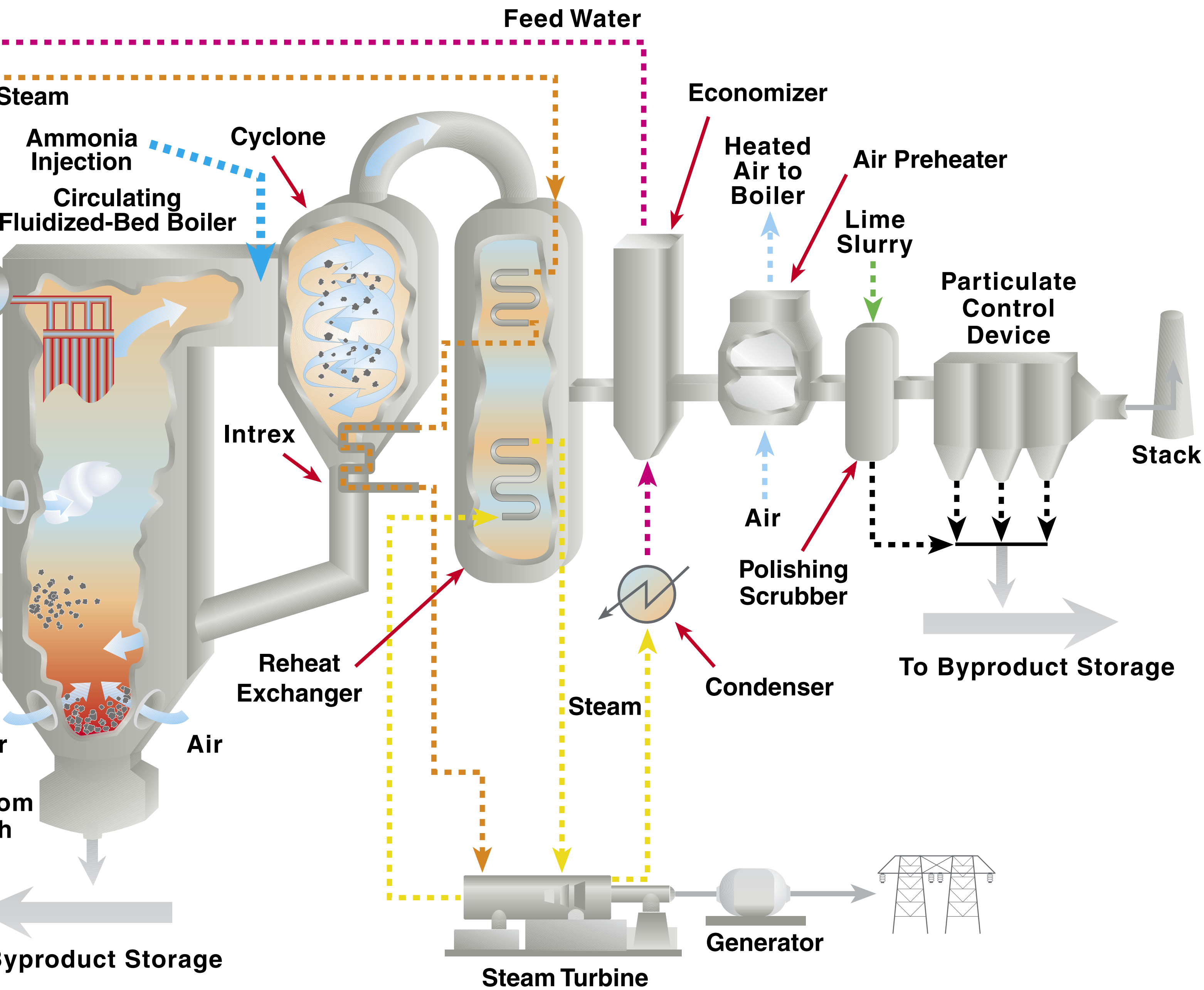
The hot gases leaving the top of the cyclone enter additional reheater/superheater tubes that also generate steam for the turbines. The still hot flue gas is used to preheat the main combustion air before it is introduced to the bottom of the furnace.

After the reheater/superheater, the flue gas enters an air quality control system, where it travels downward through a polishing scrubber that applies a lime slurry to absorb SO_2. Following the scrubber, the flue gas passes through a baghouse containing fabric filters to further clean the gas before it is sent up the stack. The collected particulates, which are sent to by-product storage, include trace metals captured in the fabric filters.

JEA Large-



-Scale CFB Combustion Demonstration Project



Fluidized Bed Combustion

Fluidized bed combustion (FBC) is one of the major technologies being developed under Advanced Electric Power Generation in DOE's CCT Program. FBC reduces emissions of SO_2 and NOx by controlling combustion parameters and by injecting a sorbent, such as crushed limestone, into the combustion chamber along with the coal.

Pulverized coal mixed with the limestone is fluidized on jets of air in the combustion chamber. Sulfur released from the coal as SO_2 is captured by the sorbent in the bed to form a solid calcium compound that is removed with the ash. The resultant by-product is a dry, benign solid that can be disposed of easily or used in agricultural and construction applications. More than 90% of the SO_2 can be captured in this manner.

At combustion temperatures of 1,400 to 1600°F, the fluidized mixing of the fuel and sorbent enhances both combustion and sulfur capture. The operating temperature range is much lower than that of a conventional pulverized-coal boiler and below the temperature at which thermal NOx is formed. In fact, NOx emissions from FBC units are about 70 to 80% lower than those for conventional boilers. Thus, FBC units substantially reduce both SO_2 and NOx emissions. Also, FBC has the capability of using high-ash coal, whereas conventional pulverized-coal units must limit ash content in the coal to relatively low levels.

Two parallel paths have been pursued in FBC development—bubbling and circulating beds. Bubbling FBCs use a dense fluid bed and low fluidization velocity to effect good heat transfer and mitigate erosion of an in-bed heat exchanger. Circulating FBCs use a relatively high fluidization velocity that entrains the bed material, in conjunction with hot cyclones, to separate and recirculate the bed material from the flue gas before it passes to a heat exchanger. Hybrid systems have evolved from these two basic approaches.

Fluidized bed combustion can be either atmospheric (AFBC) or pressurized (PFBC). As implied by the name, AFBC operates at atmospheric pressure. PFBCs, which operate at pressures 6 to 16 times higher, offer higher efficiency by expanding the hot combustion products through a gas turbine and utilizing the steam generated within the combustor to operate a steam turbine. Consequently, operating costs and waste are reduced relative to AFBC, as well as boiler size per unit of power output.

Second-generation PFBC integrates the combustor with a pyrolyzer (coal gasifier) to fuel a gas turbine (topping cycle), and the waste heat is used to generate steam for a steam turbine (bottoming cycle). The inherent efficiency of the gas turbine and waste heat recovery in this combined-cycle mode significantly increases overall efficiency. Such advanced PFBC systems have the potential for overall thermal efficiencies approaching 50%.

Since PFBCs have not yet been demonstrated on a commercial scale, AFBCs were chosen for the JEA project.

Natural gas was rejected as an option because northeastern Florida was served by only one pipeline at that time. Orimulsion was not considered seriously because it was not held in high regard by regulatory authorities and it did not offer a cost advantage.

In early 1997, detailed condition assessments of Unit 1 and Unit 2 BOP equipment and systems were conducted by JEA and Black & Veatch. The results of that study indicated that both Unit 1 and Unit 2 were good candidates for repowering and were capable of operating for many more years, provided various equipment and system upgrades were made.

In April 1997, JEA approved the project and authorized staff to begin working with Foster Wheeler (FW) on contract negotiations and environmental permitting.

Project Organization

JEA contracted with Foster Wheeler Energy Corporation (FWEC) to provide the design and supply of the ACFB boilers. Foster Wheeler USA (FWUSA) provided engineering, procurement, and construction management services for installation of the boilers and for furnishing and erecting the air pollution control systems, stack, limestone preparation system, and ash handling system. Foster Wheeler Environmental Corporation, a subsidiary of FWUSA, was also contracted to provide environmental permitting services.

The remaining portions of the project were implemented by JEA staff, supplemented by Black & Veatch through a pre-existing alliance with JEA for engineering services. Procurement, construction and related services were provided through other pre-existing alliances between JEA and Zachry Construction Corporation, Fluor Global Services, W.W. Gay Mechanical Contractor, Inc., and Williams Industrial Services Inc. This work included upgrades of the existing turbine island equipment, construction of the receiving and handling facilities for the fuel and reagent required for solid fuel firing, upgrading of the electrical switchyard facilities, and construction of an ash management system.

Project Status

Environmental permitting work was initiated by FW in the latter part of 1997. This work and associated preliminary engineering proceeded through 1998 and into early 1999. FW began detailed engineering for the boiler island, including the air quality control system, stack, and limestone preparation system, in December 1998. Black & Veatch began detailed engineering for BOP systems, including the fuel handling system, in February 1999. Permits necessary to begin construction were issued in July 1999, with site clearing and construction beginning in August 1999.

Initial synchronization was achieved for Unit 2 on February 19, 2002, and for Unit 1 on May 29, 2002. The JEA project will include two years of demonstration test runs, during which a variety of coal fuel blends will be fired.

Design Parameters

Fuel Specifications	Coal	Petroleum Coke
Heating Value, Btu/lb	>11,600	>13,000
Sulfur, %	0.5-4.5	3.0-8.0
Ash, %	7-15	<3
Volatile Matter, %	30-60	>7
Steam Flow and Conditions	Reheat	Main
Flow, 1000 lb/hr	1994	1773
Pressure, psi	2,500	548
Temperature, °F	1,000	1,000

JEA plant view from by-product storage area

Project Objectives

The JEA project objectives are (1) to demonstrate ACFB technology at 297.5 MWe gross (265 MWe net), representing a scale-up from previously constructed facilities; (2) to verify expectations of the technology's economic, environmental, and technical performance to provide potential users with the data necessary for evaluating large-scale ACFBs as a commercial alternative; (3) to accomplish greater than 90% SO_2 removal; and (4) to reduce NOx emissions by 60% compared with conventional pulverized-coal (PC) fired boilers not equipped with post-combustion NOx removal.

Initial Performance Results

Emissions	Guarantee Value	100% Coal Test	100% Coke Test
SO_2, lb/10^6 Btu	<0.15	0.00-0.04	0.03-0.13
NOx, lb/10^6 Btu	<0.09	0.04-0.06	0.02
CO, lb/10^6 Btu	<0.22	0.044-0.054	0.013-0.015
Particulates, lb/10^6 Btu	<0.011	0.004	0.007
PM_{10}, lb/10^6 Btu	<0.011	0.006	0.0044
SO_3, lb/hr	1.1	0.43	0.00
Fluoride, lb/hr	0.43	0.29	0.261
Lead, lb/hr	0.070	0.015	0.016
Mercury, lb/hr	0.03	0.0027	0.0008
VOC, lb/hr	14.0	<0.1	<0.1
Opacity, %	<10	0.36-1.12	0.21-2.64
Ammonia Slip, ppm	40	0.9	n/a
Boiler Parameters			
Steam Flow, 1000 lb/hr	>1794	1950	1937
Main Steam Temperature, °F	>980	996	992
Reheat Steam Temperature, °F	>980	1001	993
Main Steam - Reheat Steam Temperature, °F	<30	6	5
Boiler Efficiency, %	81.8	88.2	92.0

Project Scope

The JEA project involves the construction and operation of a new 300-MWe ACFB boiler fired with coal fuel blends to repower an existing steam turbine. ACFB boilers are capable of removing about 90% of the SO_2 generated, using limestone at a design Ca/S ratio of < 2/1. Greater percentage removal can be achieved by increasing the Ca/S ratio, but the added cost for limestone sorbent becomes prohibitive. To optimize the overall economics and to meet environmental requirements, a polishing scrubber was included in the JEA project. This added feature is required when firing higher sulfur fuels, including petroleum coke containing up to 8.0% sulfur.

A key feature of the polishing scrubber is a recycle system which adds fly ash to the lime sorbent, thereby taking advantage of the unreacted lime in the fly ash to reduce the amount of fresh lime required. The resulting savings in sorbent and ash disposal costs offset the added capital and operating costs for the scrubber. In addition, the scrubber offers reductions in emissions of trace elements. The JEA installation represents the first use of a polishing scrubber in conjunction with a CFB in the United States.

As indicated previously, the project includes an SNCR system to reduce NOx emissions to the very low levels required. A new baghouse was installed to achieve over 99.8% reduction in particulate emissions.

In addition to the ACFB combustor itself and the air pollution control systems, new equipment for the project includes an approximately 500-ft high stack as well as handling systems for fuel, limestone, and ash. This includes facilities for delivery of solid fuel to the site by ship. The project also required overhaul and/or modifications of existing systems such as the steam turbines, condensate and feedwater systems, circulating water systems, water treatment systems, plant electrical distribution systems, the switchyard, and the plant control systems.

JEA plant with ship unloading dock in foreground

A significant aspect of the JEA project design is that many of the boiler components are at the leading edge of technology, but have been applied successfully in commercial service at least once before. Integrating all these components while significantly scaling up boiler size is a major project accomplishment.

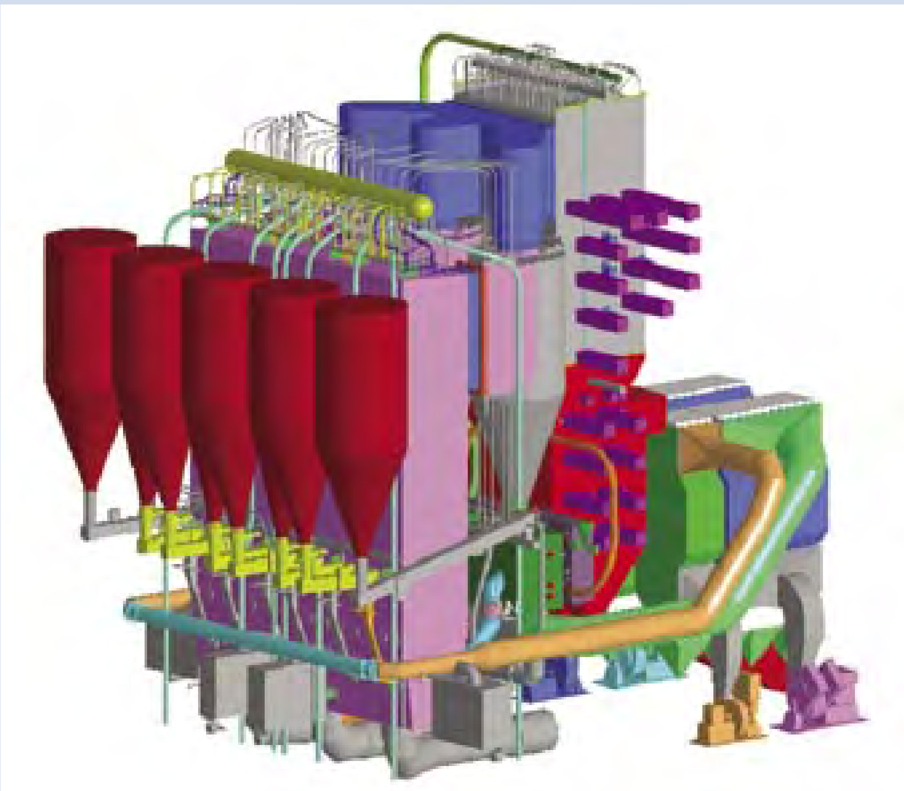
Wherever possible, existing facilities and infrastructure were used. These include the intake and discharge system for cooling water, the wastewater treatment system, and the electric transmission lines and towers.

Project activities include engineering and design, permitting, procurement, construction, startup, and a twenty-four month demonstration of the commercial feasibility of the technology. During the demonstration test program, Unit 2 will be operated on several different types of coal fuel blends to enhance the viability of the technology. Upon completion of the demonstration test program, Unit 2 will continue in commercial operation. As long as petroleum coke is less expensive than coal, it will continue to be the preferred fuel for the JEA plant.

Fuel unloader at dock

Advantages of CFB Boilers

Combustion efficiency is improved in circulating fluidized bed (CFB) boilers compared to bubbling bed boilers. This is primarily because the elutriated particles are separated from the flue gas in cyclone collectors (hot cyclones with vortex finders) and returned to the furnace for further exposure to combustion temperature and high turbulence. This fact results in an increase of up to 4% in overall combustion efficiency. The particles captured in the cyclone collectors make up the circulating bed material within the "hot loop." The hot loop is a term given for the circulating path of bed material inside the boiler.



Schematic diagram of CFB boiler at JEA

Other advantages of CFB boilers over conventional PC-fired boilers are:

- Lower capital cost
- Ability to burn a wide range of low- to high-grade fuels
- Increased sulfur capture with less limestone consumption and low SO_2 emissions
- Lower operating temperatures compared with other types of boilers, thereby reducing slag formation and excess stack emissions
- Improved heat transfer with the increase in residence time for fuel and limestone
- Lower NOx emissions because of low operating temperatures

Lower operating temperatures mean fewer pollutants and less equipment needed to clean up the combustion process while burning a variety of fuels. The ratios between operating gas velocity and minimum solids entrainment velocity allow turndown ratios as high as four to one. Operation over a wide range of boiler loads is possible without starting and stopping burners and auxiliary equipment.

Fluidized Bed Combustion Systems

The ACFB boiler technology selected for the JEA project is an advanced method for utilizing coal and other solid fuels in an environmentally acceptable manner. The low combustion temperature allows SO_2 capture via limestone injection while minimizing NOx emissions. The technology provides the capability to burn a wide range of coal fuel blends. Presently, there are two types of fluidized bed boilers in commercial operation: bubbling bed and circulating bed.

Bubbling Bed Boilers

In the bubbling bed type boiler, a layer of solid particles (mostly limestone, sand, ash and calcium sulfate) is contained on a grid near the bottom of the boiler. This layer is maintained in a turbulent state as low velocity air is forced into the bed from a plenum chamber beneath the grid. Fuel is added to this bed and combustion takes place. Normally, raw fuel in the bed does not exceed 2% of the total bed inventory. Velocity of the combustion air is kept at a minimum, yet high enough to maintain turbulence in the bed. Velocity is not high enough to carry significant quantities of solid particles out of the furnace.

This turbulent mixing of air and fuel results in a residence time of up to five seconds. The combination of turbulent mixing and residence time permits bubbling bed boilers to operate at a furnace temperature below 1650°F. At this temperature, the presence of limestone mixed with fuel in the furnace achieves greater than 90% sulfur removal.

Boiler efficiency is the percentage of total energy in the fuel that is used to produce steam. Combustion efficiency is the percentage of complete combustion of carbon in the fuel. Incomplete combustion results in the formation of carbon monoxide (CO) plus unburned carbon in the solid particles leaving the furnace. In a typical bubbling bed fluidized boiler, combustion efficiency can be as high as 92%. This is a good figure, but is lower than that achieved by pulverized coal or cyclone-fired boilers. In addition, some fuels that are very low in volatile matter cannot be completely burned within the available residence time in bubbling bed-type boilers.

CFB boiler under construction

Circulating Fluidized Bed Boilers

The need to improve combustion efficiency (which also increases overall boiler efficiency and reduces operating costs) and the desire to burn a much wider range of fuels has led to the development and application of the CFB boiler. Through the years, boiler suppliers have been increasing the size of these high-efficiency steam generators. FW has designed (but not built) CFB boilers that are capable of producing 400 MWe of power.

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The Clean Coal Technology Program

The Clean Coal Technology (CCT) Program is a unique partnership between the federal government and industry that has as its primary goal the successful introduction of new clean coal utilization technologies into the energy marketplace. With its roots in the acid rain debate of the 1980s, the program has met its early objective of broadening the range of technological solutions available to eliminate environmental concerns associated with the use of coal for electric power production. As the program has evolved, it has expanded to address the need for new, high-efficiency power generating technologies that will allow coal to continue to be a fuel option well into the 21st century.

Begun in 1985 and expanded in 1987 consistent with the recommendations of the U.S. and Canadian Special Envoys on Acid Rain, the program has been implemented through a series of five nationwide competitive solicitations, or rounds. Each solicitation was associated with specific government funding and program objectives. After five rounds, the CCT Program comprises a total of 38 projects located in 18 states with a total investment value of over $5.2 billion. DOE's share of the total project costs is about $1.8 billion, or approximately 34% of the total. The projects' industrial participants (i.e., the non-DOE participants) are providing the remainder—about $3.5 billion.

Processes being demonstrated under the CCT Program have established a technology base that will enable the nation to meet more stringent energy and environmental goals. Also ready is a new generation of technologies that can produce electricity and other commodities, such as steam and synthesis gas, at high efficiencies consistent with concerns about global climate change.

Most of the CCT demonstrations are being conducted at commercial scale, in actual user environments, and under circumstances typical of commercial operations. These features allow the potential of the technologies to be evaluated in their intended commercial applications.

Each application addresses one of the following four market sectors:

- Advanced electric power generation
- Environmental control devices
- Coal processing for clean fuels
- Industrial applications

Given its programmatic success, the CCT Program serves as a model for other cooperative government/industry programs aimed at introducing new technologies into the commercial marketplace.

Two follow-on programs have been developed that build on the successes of the CCT Program. The Power Plant Improvement Initiative (PPII) is a cost shared program, patterned after the CCT Program, directed toward improved reliability and environmental performance of the nation's coal-burning power plants. Authorized by the U.S. Congress in 2001, the PPII involves eight projects having a total cost of $95 million. Private sector sponsors are expected to contribute nearly $61 million, exceeding the 50% private sector cost sharing mandated by Congress. Most of the PPII projects focus on technologies enabling coal-fired power plants to meet increasingly stringent environmental regulations at the lowest possible cost.

The second program is the Clean Coal Power Initiative (CCPI), also patterned on the CCT Program, authorized in early 2002. Valued at $330 million for the initial stage, this initiative will accelerate the commercial deployment of technology advancements that result in efficiency, environmental and economic improvement compared with available state-of-the-art alternatives. Proposals submitted under the CCPI are currently being evaluated.

CFBs offer a number of advantages:

Fuel Flexibility – The relatively low furnace temperatures are below the ash softening temperature for nearly all fuels. As a result, furnace design is independent of ash characteristics, thus allowing a given furnace to handle a wide range of fuels.

Low SO_2 Emissions – Limestone is an effective sulfur sorbent in the temperature range of 1500 to 1700°F. SO_2 removal efficiency of 90% has been demonstrated with good sorbent utilization.

Low NOx Emissions – The combination of low furnace temperatures and staging of air feed to the furnace produces very low NOx emissions.

High Combustion Efficiency – The long solids residence time in the furnace resulting from the collection/recirculation of solids via the cyclone, plus the vigorous solids/gas contact in the furnace caused by the fluidization air flow, results in high combustion efficiency, even with difficult-to-burn fuels.

Characteristics of CFB Boilers

In the furnace of a circulating fluidized bed boiler, gas velocity is increased to more than that in a bubbling bed boiler. This increase in velocity causes the dense mixture of solids (fuel, limestone and ash) to be carried up through the furnace. There is a minimum gas entrainment velocity required for the particles to lift and separate (elutriate) and flow up, through and out of the furnace.

Reaching this entrainment velocity marks the change from a bubbling bed boiler to a circulating bed boiler. At approximately 500°F bed temperature, air flows are above minimum and the entrainment velocity is reached.

Solids move up through the furnace at lower velocities than the air and gas mixture. This fact, coupled with the elongated furnace in a CFB boiler and recirculating bed material, allows particle residence times of up to several minutes in the furnace. During this long residence period, the crushed fuel particles are consumed in the combustion process.

The fuel is reduced in size during the combustion process and thoroughly mixed with limestone and the balance of the bed material. This action produces the "fines" (small particles of bed material) necessary to have circulating bed material in the "hot loop." Long residence time, coupled with small particle size and high turbulence, results in a better sulfur removal rate with less limestone than in a bubbling fluidized bed boiler. In addition, higher gas velocity produces heat transfer rates that are greater than in the bubbling bed.

In normal operation there is no defined fixed bed depth in a CFB boiler. There are different densities of circulating bed material depending on the weight of the particles. Heavy particles stay in the lower region of the furnace. As the height within the furnace increases, the smaller bed particles (less dense) enter the circulation path of the hot loop. When the particles break down enough, they are carried out of the hot loop (circulating path) with the flue gas as fly ash.

New 500-foot stack in foreground, with inset showing the stack interior

Sulfur Removal in CFB Boilers

Most of the sulfur in the fuel combines chemically with oxygen during the combustion process to form SO_2 and, to a limited extent, sulfur trioxide (SO_3). These sulfur oxides must be removed from the flue gas to comply with environmental regulations.

The mechanism for removing SO_2 with limestone is as follows:

Calcination of limestone:

$CaCO_3$ + Heat → $CaO + CO_2$

Reaction with sulfur oxides (sulfation):

$CaO + O_2 + SO_2 \rightarrow CaSO_4$

The product, $CaSO_4$, is an inert substance known as gypsum. Limestone continuously reacts with the fuel at normal operating temperatures. The sulfation reaction requires that there always be an excess of limestone. The amount of excess limestone required depends on several factors, such as the amount of sulfur in the fuel, the temperature of the bed material in the furnace, and the physical and chemical characteristics of the limestone (reactivity). The ideal reaction temperature range is 1500 to 1700°F.

There is little limestone reaction when the bed temperature is below 1500°F or above 1700°F. Within the optimum temperature range, about 90% of the SO_2 can be removed at an acceptable Ca/S ratio. Outside this temperature range, significant increases in limestone feed rate are required to maintain emission levels within regulated limits.

The CFB bed material typically contains limestone products as the predominant component, with smaller amounts of fuel, ash and impurities (for example, rocks or tramp iron). Calcium oxide content rises with decreasing fuel sulfur content and high removal rates. The ash content increases with higher ash fuels and those that are less friable, i.e., brittle.

Fresh limestone enters the furnace and, at the normal operating temperature, calcines by liberating CO_2. It then absorbs SO_2 from the burning fuel that sulfates the limestone, converting limestone to gypsum. In the calcining stage, limestone is physically weak and is easily decrepitated (crumbled) into dust and carried out of the bed (elutriated) by the furnace draft.

With a sulfur content in the fuel of 2.5% or more, enough SO_2 is produced during combustion that the limestone can readily sulfate (combine with the SO_2). This strengthens the limestone and reduces loss of limestone from decrepitation and elutriation. A low sulfur content can lead to loss of limestone through attrition. This loss must be compensated for by increasing limestone feed to maintain bed inventory and SO_2 capture. Gypsum and some excess limestone are carried out of the CFB furnace and trapped by the downstream flue gas cleanup equipment.

Demonstration Test Program

The demonstration test program will be conducted in accordance with the plan developed in coordination with DOE. The test program consists of the following major components.

Operational Testing will be performed to:

- Demonstrate unit functionality
- Establish initial operating, maintenance and inspection criteria
- Establish constraints related to dispatch of the unit
- Demonstrate continuous full- and part-load capability and performance

Operational testing includes a series of operability, reliability, and performance tests.

Operability involves tests of cold startups, warm startups, hot restarts, dispatch, minimum stable load, and operation at maximum continuous rating.

Reliability testing includes availability, capacity factor, and forced outage rate.

Performance testing will be conducted in conjunction with fuel flexibility testing, which involves burning four different fuels and fuel blends. The specific fuels to be tested are as follows:

- 100% Pittsburgh No. 8 high-sulfur coal
- 90% petroleum coke and 10% Pittsburgh No. 8 high-sulfur coal
- 50% petroleum coke and 50% Pittsburgh No. 8 high-sulfur coal
- 100% Illinois No. 6 high-sulfur coal

Fuel Flexibility Testing includes boiler capacity and controllability, load following capability, bed/cyclone agglomeration potential, and air quality control system performance.

Long Term Durability Testing consists of reviewing significant maintenance issues experienced with major equipment throughout the demonstration period.

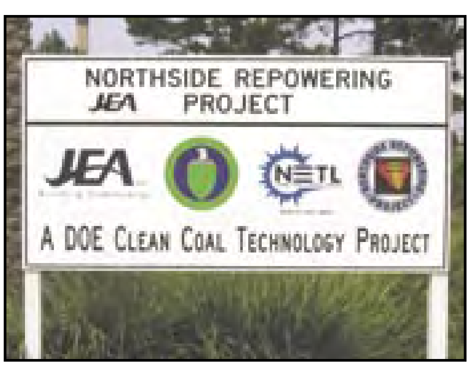
Interior of fuel storage dome

Operating Results

The JEA Unit 2 CFB boiler has operated at full load, achieving rated output in May 2002. The unit can maintain operation on both coal and coal fuel blends. However, satisfactory operation on 100% petroleum coke has not yet been demonstrated. One major problem when operating on 100% petroleum coke has been plugging in the hot gas path, specifically in the cyclone and the INTREX™ heat exchanger. Steps are being taken to remedy this situation.

Initial results indicate that the JEA plant is capable of meeting emissions guarantees when operating on both coal and coal fuel blends.

JEA receives the *Power* magazine 2002 Powerplant award. On hand for the award ceremony were (left to right): Mike Hightower, JEA's Board Chairman; Joey Duncan, JEA's Project Manager; the Honorable Corrine Brown, U.S. House of Representatives; Rita Bajura, Director of U.S. DOE's National Energy Technology Laboratory; and Bob Schwieger, *Power* magazine consulting editor



Awards

The JEA project received the 2002 Powerplant Award from *Power* magazine. This award recognizes outstanding achievement in "the development of a successful repowering strategy for converting existing oil/gas-fired steam plants to solid fuels to increase efficiency while reducing both emissions and the cost of electricity."

Bob Dyr, JEA's Boiler Island Project Manager, was presented the Engineer of the Year award by the Florida Engineers Society in 2002 for outstanding technical achievement, on behalf of the project team.

Commercial Applications

ACFB technology has potential application in both the industrial and utility sectors, for use in repowering existing plants a well as in new facilities. ACFB is attractive for both baseload and dispatchable power applications because it can be efficiently turned down to as low as 25% of full load. While the efficiency of ACFB is on a par with conventional PC-fired plants, the advantage of ACFB is that coal of any sulfur or ash content can be used, and any type or size unit can be repowered. In repowering applications, an existing plant area is used, and coal- and waste-handling equipment as well as steam turbine equipment are retained, thereby extending the life of the plant.

In its commercial configuration, ACFB technology offers several potential benefits compared with conventional PC-fired systems:

- Lower capital costs
- Reduced SO_2 and NOx emissions at lower cost
- Higher combustion efficiency
- A high degree of fuel flexibility, including use of renewable fuels
- Dry, granular solid by-product material that is easily disposed of or sold.

Recently, two other commercial scale ACFB projects in the U.S. have been announced, one at Reliant Energy's Seward Station in Pennsylvania and the other at Tractabel's Red Hills Station in Mississippi.

Conclusions

The JEA Large-Scale CFB Combustion Demonstration Project is demonstrating the commercial application of this advanced technology for generating electricity. The two boilers at the Northside Station are the largest CFBs in the world burning coal fuel blends. Despite the large furnace size, solids distribution is good, lending confidence to the CFB design.

Power production from each boiler on coal feed meets the target goal of 297.5 MWe gross (265 MWe net). Emissions of atmospheric pollutants are below the stringent requirements set for the project.

Bibliography

P.T. Nielsen, J.L. Hebb, R. Aquino, and S.L. Darling, "Large-Scale CFB Combustion Demonstration Project," Sixth Clean Coal Technology Conference (Reno NV), May 1998.

U.S. Department of Energy, Clean Coal Technology Demonstration Program -- Program Update 2000, July 2002.

R. Dyr and G. Graham, "The Northside 1 and 2 Repowering Project: An Overview," 7th Foster Wheeler Fluidized Bed Customer Conference, San Diego CA, August 14-16, 2002.

R. Schwieger, "Northside's CFB Repowering Halves Power Cost, Reduces Emissions," Power, September 2002, p. 20.

R.A. Dyr and A.L. Compaan, "JEA Northside Repowering: 2002 Powerplant of the Year," presented at FMEA 2002 Energy Connections Workshop and Trade Show, St. Petersburg FL, October 15-17, 2002.

JEA, "Public Design Report for the JEA Large-Scale CFB Combustion Demonstration Project," March 2003.

List of Acronyms and Abbreviations

ACFB	atmospheric circulating fluidized bed
AFBC	atmospheric fluidized bed combustor
AQCS	air quality control system
BOP	balance of plant
Btu	British thermal unit
$CaCO_3$	calcium carbonate
CaO	calcium oxide
$Ca(OH)_2$	calcium hydroxide
$CaSO_4$	calcium sulfate
CAAA	Clean Air Act Amendments of 1990
CCPI	Clean Coal Power Initiative
CCT	Clean Coal Technology
CFB	circulating fluidized bed
CO_2	carbon dioxide
CRT	cathode ray tube
DCS	distributed control system
DOE	U.S. Department of Energy
EPA	U.S. Environmental Protection Agency
FBC	fluidized bed combustion
FF	fabric filters

Stack shortly after 9/11/2001

kWh .... kilowatt hour
micron .... one millionth of a meter
MCR .... maximum continuous rating
$MgCO_3$ .... magnesium carbonate
$Mg(OH)_2$ .... magnesium hydroxide
MWe .... megawatts of electric power
MWh .... megawatt hours of electric power
NETL............................ National Energy Technology Laboratory
NOx .... nitrogen oxides
PC .... pulverized coal
PFBC .... pressurized fluidized bed combustor
PLC .... programmable logic controller
PM .... particulate matter
PM_{10} .... particulate matter having a diameter of 10 microns (μm) or less
PPII............................... Power Plant Improvement Initiative
psig .... pressure, pounds per square inch (gauge)
SDA .... spray dryer absorber
SO_2 .... sulfur dioxide
SO_3 .... sulfur trioxide
tph................................. tons/hr
VOC .... volatile organic compound
wt % .... percent by weight

Sunset at JEA

To Receive Additional Information

To be placed on the Department of Energy's distribution list for future information on the Clean Coal Technology Program, the demonstration projects it is financing, or other Fossil Energy Programs, please contact:

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Pollutant Test

This Ad hoc report allows query of the stack test report data, including the test dates, audit levels and actual measurements.
Data for this Report is One Day Old PRODUCTION Data.
Table or View: POLL_TEST_VW

Ad Hoc Reporting

OWNER/COMPANY NAME	AIRS ID	SITE NAME	FACILITY OFFICE	FACILITY COUNTY NAME	FACILITY STATUS	TITLE V	EU ID	EU DESCRIPTION	EU STATUS	POLLUTANT	TEST DATE	TEST ACTUAL	TEST ACTUAL UNIT DESCRIPTION	COMMENTS
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	5	DUCT BURNER SYSTEM ASSOCIATED WITH HRSG	A	NOX	4/29/2003	0.063	POUNDS PER MILLION BTU HEAT INPUT	pec test team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	5	DUCT BURNER SYSTEM ASSOCIATED WITH HRSG	A	CO	4/29/2003	0.04	POUNDS PER MILLION BTU HEAT INPUT	pec test team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	7	NEW LM6000PC-ESPRINT COMBUSTION TURBINE	A	SO2	4/11/2007	0.033	OTHER (SPECIFY IN COMMENT)	permit limit 1.0 grain sulfur per 100 scf of fuel. Actual was 0.033
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	7	NEW LM6000PC-ESPRINT COMBUSTION TURBINE	A	SO2	4/25/2006	0.081	OTHER (SPECIFY IN COMMENT)	.081 grain sulfur per 100 scf of fuel. C.E.M. Solutions, Inc. 7990 W. Gult-to-Lake Hwy., Cr River, FL 34429. (352) 564-0441
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	7	NEW LM6000PC-ESPRINT COMBUSTION TURBINE	A	CO	4/11/2007	24.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	24.4 lbs/hr. C.E.M. Solutions, Hernado, FL, 352.486.4337
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	7	NEW LM6000PC-ESPRINT COMBUSTION TURBINE	A	CO	4/25/2006	31.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	C.E.M. Solutions, Inc. 7990 W. Gult-to-Lake H Crystal River, FL 34429. (352) 564-0441
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	7	NEW LM6000PC-ESPRINT COMBUSTION TURBINE	A	CO	4/26/2005	22.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	7	NEW LM6000PC-ESPRINT COMBUSTION TURBINE	A	CO	4/25/2006	31.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	C.E.M. Solutions, Inc. 7990 W. Gult-to-Lake H Crystal River, FL 34429. (352) 564-0441
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	7	NEW LM6000PC-ESPRINT COMBUSTION TURBINE	A	NOX	4/11/2007	19.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	28.3 lbs/hr. C.E.M. Solutions, Hernado, FL, 352.486.4337
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	7	NEW LM6000PC-ESPRINT COMBUSTION TURBINE	A	NOX	4/25/2006	16.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	C.E.M. Solutions, Inc. 7990 W. Gult-to-Lake H Crystal River, FL 34429. (352) 564-0441
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	7	NEW LM6000PC-ESPRINT COMBUSTION TURBINE	A	NOX	4/26/2005	20.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	C.E.M. Solutions, Inc. (Crystal River, Fla)
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	7	NEW LM6000PC-ESPRINT COMBUSTION TURBINE	A	SO2	4/26/2005	0.068	PERCENT SULFUR IN FUEL	C.E.M. Solutions, Inc. (Crystal River, Fla)
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	7	NEW LM6000PC-ESPRINT COMBUSTION TURBINE	A	NOX	5/6/2004	19.35	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fired with Natural Gas (NG). Progress Energy Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	7	NEW LM6000PC-ESPRINT COMBUSTION TURBINE	A	NOX	4/26/2005	20.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	C.E.M. Solutions, Inc. (Crystal River, Fla)
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	7	NEW LM6000PC-ESPRINT COMBUSTION TURBINE	A	NOX	4/25/2006	16.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	C.E.M. Solutions, Inc. 7990 W. Gult-to-Lake H Crystal River, FL 34429. (352) 564-0441
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	7	NEW LM6000PC-ESPRINT COMBUSTION TURBINE	A	CO	5/6/2004	18	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fired on natural Gas (NG). Progress Energy Te Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0010001	U OF FL COGEN	NED	ALACHUA	A	Y	7	NEW LM6000PC-ESPRINT COMBUSTION TURBINE	A	CO	4/26/2005	22.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
GAINESVILLE REGIONAL UTILITIES	0010005	JOHN R KELLY POWER PLANT	NED	ALACHUA	A	Y	10	Combined-Cycle Unit No. 1 (CC-1)	A	CO	8/15/2007	1.75	PARTS PER MILLION DRY GAS VOLUME	
GAINESVILLE REGIONAL UTILITIES	0010005	JOHN R KELLY POWER PLANT	NED	ALACHUA	A	Y	10	Combined-Cycle Unit No. 1 (CC-1)	A	CO	9/30/2005	2.68	PARTS PER MILLION DRY GAS VOLUME	oil with water injection.
GAINESVILLE REGIONAL UTILITIES	0010005	JOHN R KELLY POWER PLANT	NED	ALACHUA	A	Y	10	Combined-Cycle Unit No. 1 (CC-1)	A	CO	5/24/2006	4.82	PARTS PER MILLION DRY GAS VOLUME	
GAINESVILLE REGIONAL UTILITIES	0010005	JOHN R KELLY POWER PLANT	NED	ALACHUA	A	Y	10	Combined-Cycle Unit No. 1 (CC-1)	A	CO	7/21/2004	10.81	PARTS PER MILLION DRY GAS VOLUME	
GAINESVILLE REGIONAL UTILITIES	0010005	JOHN R KELLY POWER PLANT	NED	ALACHUA	A	Y	10	Combined-Cycle Unit No. 1 (CC-1)	A	CO	9/30/2005	2.9	PARTS PER MILLION DRY GAS VOLUME	Natural Gas
GAINESVILLE REGIONAL UTILITIES	0010005	JOHN R KELLY POWER PLANT	NED	ALACHUA	A	Y	10	Combined-Cycle Unit No. 1 (CC-1)	A	CO	10/24/2003	8.18	PARTS PER MILLION DRY GAS VOLUME	898.1 mmbtu/hr average heat input using natura gas.
GAINESVILLE REGIONAL UTILITIES	0010005	JOHN R KELLY POWER PLANT	NED	ALACHUA	A	Y	7	Fossil Fuel Fired Steam Generator Unit No. 7	A	PM	11/20/2007	0.1324	POUNDS PER MILLION BTU HEAT INPUT	Soot Blowing
GAINESVILLE REGIONAL UTILITIES	0010005	JOHN R KELLY POWER PLANT	NED	ALACHUA	A	Y	7	Fossil Fuel Fired Steam Generator Unit No. 7	A	PM	11/19/2007	0.0961	POUNDS PER MILLION BTU HEAT INPUT	Normal Operation
GAINESVILLE REGIONAL UTILITIES	0010005	JOHN R KELLY POWER PLANT	NED	ALACHUA	A	Y	7	Fossil Fuel Fired Steam Generator Unit No. 7	A	PM	9/6/2006	0.1244	POUNDS PER MILLION BTU HEAT INPUT	soot blowing
GAINESVILLE REGIONAL UTILITIES	0010005	JOHN R KELLY POWER PLANT	NED	ALACHUA	A	Y	7	Fossil Fuel Fired Steam Generator Unit No. 7	A	PM	11/19/2007	0.0961	POUNDS PER MILLION BTU HEAT INPUT	
GAINESVILLE REGIONAL UTILITIES	0010005	JOHN R KELLY POWER PLANT	NED	ALACHUA	A	Y	7	Fossil Fuel Fired Steam Generator Unit No. 7	A	PM	9/5/2006	0.048	POUNDS PER MILLION BTU HEAT INPUT	normal operation
GAINESVILLE REGIONAL UTILITIES	0010005	JOHN R KELLY POWER PLANT	NED	ALACHUA	A	Y	7	Fossil Fuel Fired Steam Generator Unit No. 7	A	PM	7/21/2004	0.0573	POUNDS PER MILLION BTU HEAT INPUT	
GAINESVILLE REGIONAL UTILITIES	0010005	JOHN R KELLY POWER PLANT	NED	ALACHUA	A	Y	7	Fossil Fuel Fired Steam Generator Unit No. 7	A	PM	8/18/2005	0.0648	POUNDS PER MILLION BTU HEAT INPUT	Normal Operation. Heat Input can't exceed 266 mmbtu/hr.
GAINESVILLE REGIONAL	0010005	JOHN R KELLY	NED	ALACHUA	A	Y	7	Fossil Fuel Fired Steam	A	PM	8/18/2005	0.1181	POUNDS PER MILLION BTU	Soot Blowing Mode. Heat Input Limited to 266

UTILITIES		POWER PLANT						Generator Unit No. 7					HEAT INPUT	mmbtu/hr.
GAINESVILLE REGIONAL UTILITIES	0010005	JOHN R KELLY POWER PLANT	NED	ALACHUA	A	Y	7	Fossil Fuel Fired Steam Generator Unit No. 7	A	PM	7/21/2004	0.1206	POUNDS PER MILLION BTU HEAT INPUT	soot blowing mode
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	3	Fossil Fuel Fired Steam Generator #1(Phase II AR Unit)	A	PM	8/30/2007	0.0979	POUNDS PER MILLION BTU HEAT INPUT	soot blowing
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	3	Fossil Fuel Fired Steam Generator #1(Phase II AR Unit)	A	PM	8/30/2007	0.0831	POUNDS PER MILLION BTU HEAT INPUT	non-soot blowing
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	3	Fossil Fuel Fired Steam Generator #1(Phase II AR Unit)	A	PM	8/18/2006	0.0582	POUNDS PER MILLION BTU HEAT INPUT	soot blowing
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	3	Fossil Fuel Fired Steam Generator #1(Phase II AR Unit)	A	PM	8/18/2006	0.0496	POUNDS PER MILLION BTU HEAT INPUT	non-soot blowing
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	5	Fossil Fuel Fired Steam Generator #2 (Phase I & II AR Unit)	A	PM	8/15/2005	0.0122	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	5	Fossil Fuel Fired Steam Generator #2 (Phase I & II AR Unit)	A	PM	6/8/2004	0.017	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	5	Fossil Fuel Fired Steam Generator #2 (Phase I & II AR Unit)	A	PM	7/20/2006	0.018	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	5	Fossil Fuel Fired Steam Generator #2 (Phase I & II AR Unit)	A	PM	10/18/2007	0.0185	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	5	Fossil Fuel Fired Steam Generator #2 (Phase I & II AR Unit)	A	SO2	6/23/2003	0.991	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	5	Fossil Fuel Fired Steam Generator #2 (Phase I & II AR Unit)	A	SO2	8/15/2005	1.02	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	5	Fossil Fuel Fired Steam Generator #2 (Phase I & II AR Unit)	A	SO2	6/8/2004	1.075	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	5	Fossil Fuel Fired Steam Generator #2 (Phase I & II AR Unit)	A	SO2	7/20/2006	0.961	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	5	Fossil Fuel Fired Steam Generator #2 (Phase I & II AR Unit)	A	SO2	10/18/2007	1.087	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	5	Fossil Fuel Fired Steam Generator #2 (Phase I & II AR Unit)	A	NOX	6/23/2003	0.572	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	5	Fossil Fuel Fired Steam Generator #2 (Phase I & II AR Unit)	A	NOX	8/15/2005	0.517	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	5	Fossil Fuel Fired Steam Generator #2 (Phase I & II AR Unit)	A	NOX	6/8/2004	0.581	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	5	Fossil Fuel Fired Steam Generator #2 (Phase I & II AR Unit)	A	NOX	7/20/2006	0.524	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	5	Fossil Fuel Fired Steam Generator #2 (Phase I & II AR Unit)	A	NOX	10/18/2007	0.463	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	5	Fossil Fuel Fired Steam Generator #2 (Phase I & II AR Unit)	A	PM	6/23/2003	0.00338	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	3	Fossil Fuel Fired Steam Generator #1(Phase II AR Unit)	A	PM	8/16/2005	0.0616	POUNDS PER MILLION BTU HEAT INPUT	Non-Soot Blowing. Heat input can't exceed 929 mmbtu/hr.
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	3	Fossil Fuel Fired Steam Generator #1(Phase II AR Unit)	A	PM	6/26/2003	0.0607	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	3	Fossil Fuel Fired Steam Generator #1(Phase II AR Unit)	A	PM	6/25/2003	0.0473	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	3	Fossil Fuel Fired Steam Generator #1(Phase II AR Unit)	A	PM	8/16/2005	0.064	POUNDS PER MILLION BTU HEAT INPUT	Soot Blowing Mode. Heat inputcan't exceed 92 mmbtu/hr.
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	3	Fossil Fuel Fired Steam Generator #1(Phase II AR Unit)	A	PM	6/11/2004	0.061	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	3	Fossil Fuel Fired Steam Generator #1(Phase II AR Unit)	A	PM	6/10/2004	0.0448	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF GAINESVILLE, GRU	0010006	DEERHAVEN GENERATING STATION	NED	ALACHUA	A	Y	6	Simple Cycle Comb Turbine No. 3 (Phase II Acid Rain Unit)	A	NOX	7/29/2003	8.35	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	DIOX	3/20/2003	0.67	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	PM	3/18/2003	0.0203	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	PM	8/19/2004	0.0213	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	PM	9/23/2005	0.0237	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	0.204 lbs/hr.
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	SO2	3/18/2003	4.07	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	PM	9/23/2005	0.0237	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	0.204 lbs/hr.
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	H106	3/18/2003	0.53	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	

N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	H106	9/23/2005	1.36	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	CO	8/19/2004	22.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	CO	9/23/2005	19.58	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	NOX	3/18/2003	171.45	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	CO	9/23/2005	19.58	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	CO	3/18/2003	2.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	H106	8/19/2004	10.05	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	H114	3/19/2003	0.02	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	H106	9/23/2005	0.008	POUNDS/HOUR	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	H027	5/8/2003	0.014	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	H027	3/19/2003	0.25	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0010041	GAINESVILLE	NED	ALACHUA	A	Y	6	HMIW INCINERATOR	A	PB	3/19/2003	0.42	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	SAM	4/8/2003	0.16	POUNDS/HOUR	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	DIOX	1/7/2008	0.0004	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	DIOX	7/19/2005	0.008	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Raw Mill Not-Operating.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	DIOX	4/6/2005	0.045	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	NESHAP for Portland Cement Mfg , 40 CFR 6 Subpart LLL. Firing coal (7.4 TPH), WTDF(.9 TPH), Pet Coke (2.7 TPH), and flyash HCFA (TPH). Raw Mill was operating, the feed rate to preheater averaged 169 TPH. ESP inlet tempera averaged 195 degrees F. Permits 0010087-009- & 001008-012-AC.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	DIOX	3/31/2003	0.1624	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RAW MILL NOT OPERATING
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	DIOX	1/15/2003	0.00974	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	raw mill operating. ESP inlet temp. 231 F.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	DIOX	1/15/2003	0.0085	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	DIOX	7/21/2005	0.004	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Raw Mill Operating.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	DIOX	4/3/2003	0.0637	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RAW MILL OPERATING
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	4	Clinker Cooler & Handling	A	PM	1/29/2008	0.0191	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	4	Clinker Cooler & Handling	A	PM	2/22/2007	0.01	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	4	Clinker Cooler & Handling	A	PM	3/8/2006	0.02	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	4	Clinker Cooler & Handling	A	PM10	3/8/2006	0.02	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	4	Clinker Cooler & Handling	A	PM10	2/22/2007	0.01	POUNDS PER TON OF PRODUCT	PM = 1.4 lb/hr.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	PM	3/7/2006	0.05	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	PM	2/20/2007	0.03	POUNDS PER TON OF PRODUCT	Emission Rate = 3.88 lbs/hr
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	PM	1/11/2008	0.04	POUNDS PER TON OF PRODUCT	
													POUNDS PER	

FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	SAM	7/18/2005	0.0016	TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	SAM	7/19/2004	0.00087	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	SAM	3/7/2006	0	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	SAM	2/20/2007	0	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	SAM	1/29/2008	0	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	SAM	1/29/2008	0.00034	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	VOC	2/15/2007	0.04	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	VOC	2/21/2007	0.001	POUNDS PER TON OF PRODUCT	Total hydrocarbons = 5.64 lb/hr. 0.034 lb/ton f
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	VOC	1/29/2008	0.059	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	PM	4/3/2003	0.02	POUNDS PER TON OF FEED MATERIAL	RAW MILL OPERATING
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	PM	3/31/2003	0.025	POUNDS PER TON OF FEED MATERIAL	RAW MILL NOT OPERATING
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	PM	1/15/2003	0.009	POUNDS PER TON OF FEED MATERIAL	raw mill operating. COM 7.1-8%
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	PM	1/15/2003	0.051	POUNDS PER TON OF FEED MATERIAL	raw mill not operating. COM 8.3-9.6%.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	PM	4/6/2005	0.022	POUNDS PER TON OF PRODUCT	NESHAP for Portland Cement Mfg , 40 CFR 6 Subpart LLL. Firing coal (7.4 TPH), WTDF(.9 TPH), Pet Coke (2.7 TPH), and flyash HCFA (TPH). Raw Mill was operating, the feed rate to preheater averaged 169 TPH. ESP inlet tempera averaged 195 degrees F. Permits 0010087-009- & 001008-012-AC.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	PM	7/20/2004	0.025	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	CO	11/16/2007	2.13	POUNDS PER TON OF PRODUCT	CO = 220 lbs/Hr; 292 PPM. Coal Feed = 12.7T WTDF = 1.0 TPH. Petcoke = 0.0 TPH.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	CO	1/11/2008	2.3	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	VOC	2/27/2003	0.059	POUNDS PER TON OF PRODUCT	Clinker production 109.7 T/hr. VOC (THC) 6.5 lb/hr / 109.7 = 0.059 lb/Ton of Product.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	VOC	8/14/2003	0.077	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	VOC	2/10/2005	0.082	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	VOC	7/18/2005	0.0937	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	VOC	7/20/2004	0.085	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	VOC	3/7/2006	0.09	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	VOC	6/7/2006	0.07	POUNDS PER TON OF PRODUCT	Test requested by District due to high averages 1st Qtr 2006 VOC (Hydrocarbon) Emissions R
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	SO2	2/27/2003	0.0146	POUNDS PER TON OF PRODUCT	Clinker production 109.7 T/hr. SO2 1.6 lb/hr / = 0.0146 lb/Ton of Product.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	SO2	7/18/2005	0.002	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	SO2	7/20/2004	0.03	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	PM10	7/18/2005	0.0753	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	PM10	3/7/2006	0.05	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	PM10	2/20/2007	0.03	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	NOX	2/27/2003	2.151	POUNDS PER TON OF PRODUCT	Clinker production 109.7 T/hr. NOx 236 lb/hr / 109.7 = 2.151 lb/Ton of Product.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	NOX	7/18/2005	2.142	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	NOX	7/20/2004	1.22	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	CO	2/27/2003	2.033	POUNDS PER TON OF PRODUCT	Clinker production 109.7 T/hr. CO 223 lb/hr / 1 = 2.033 lb/Ton of Product.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	CO	4/12/2005	2.465	POUNDS PER TON OF PRODUCT	249 lb/hr / 101 TPH Clinker = 2.465. NESHAP Portland Cement Mfg , 40 CFR 63, Subpart LL Firing coal (8 TPH), WTDF(.85 TPH), Pet Cok (2.7 TPH), and flyash HCFA (1.3 TPH). Raw M was operating, the feed rate to preheater averag 170 TPH. Permits 0010087-009-AV & 001008 AC.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	CO	7/18/2005	2.5	POUNDS PER TON OF PRODUCT	
													POUNDS PER	

FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	CO	8/20/2004	1.34	TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	CO	12/28/2005	1.21	POUNDS PER TON OF PRODUCT	11.8 t/h coal, 0.67 t/h wtdf, 0.7 t/h petcoke.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	CO	8/25/2006	1.14	POUNDS PER TON OF PRODUCT	Quarterly Test as per 0010087-015-AC. CO = 2 ppm; 198 T/hr. Pre-heater feed = 173 T/hr; Coa 10.4 T/hr; Whole Tire Derived Fuel (WTDF) = T/hr; Pet Coke = 1.2 T/hr; Flyash = 0.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	CO	6/23/2006	1.41	POUNDS PER TON OF PRODUCT	Coal = 10.7 T/hr; WTDF = 1.13 T/hr; Pet. Cok 1.9 T/hr.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	CO	2/14/2006	1.46	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	CO	12/20/2006	2.37	POUNDS PER TON OF PRODUCT	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	CO	6/4/2007	1.23	POUNDS PER TON OF PRODUCT	CO = 208 TPH; 266 PPM. Coal Feed = 10.5 TI WTDF = 1.03 TPH. Petcoke = 1.2 TPH.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	CO	2/15/2007	2.82	POUNDS PER TON OF PRODUCT	CO: 283 lb/hr (permit limit = 276 lb/hr). The ki and precalciner were fired with average rates o at 11.4 Tons/hr, waste tire derived fuel (WTDF 0.73 Tons/hr, and pet coke at 1.1 Tons/hr.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	CO	2/22/2007	2.17	POUNDS PER TON OF PRODUCT	Retested due to stack test failure on 02/15/07. C 225 lb/hr. The kiln and precalciner were fired w coal at 12.1 Tons/hr, waste tire derived fuel (W at 0.87 Tons/hr, and pet coke at 1.1 Tons/hr.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	3	Kiln/Raw Mill System Line 1	A	CO	8/31/2007	1.54	POUNDS PER TON OF PRODUCT	CO = 164 lbs/Hr; 234 PPM. Coal Feed = 12.03 TPH. WTDF = 0.90 TPH. Petcoke = 0.97 TPH.
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	4	Clinker Cooler & Handling	A	PM	1/22/2003	0.004	POUNDS PER TON OF FEED MATERIAL	
FLORIDA ROCK INDUSTRIES, INC.	0010087	THOMPSON S. BAKER CEMENT PLANT	NED	ALACHUA	A	Y	4	Clinker Cooler & Handling	A	PM10	7/22/2005	0.099	POUNDS PER TON OF PRODUCT	
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	34	Thermal Oxidizer with caustic scrubber	A	H2S	9/12/2007	3.7	TONS/YEAR	3.7 tons emitted at the outlet of the scrubber ba on 6% caustic and 50 gpm scrubber flow
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	36	Regenerative Thermal Oxidizer	A	VOC	9/11/2007	2.3	TONS/YEAR	
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	34	Thermal Oxidizer with caustic scrubber	A	VOC	9/12/2007	3.9	TONS/YEAR	
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	34	Thermal Oxidizer with caustic scrubber	A	SO2	9/12/2007	4.8	TONS/YEAR	
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	34	Thermal Oxidizer with caustic scrubber	A	VOC	9/1/2006	1.752	TONS/YEAR	
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	15	BOILER #2	A	SO2	8/29/2006	0.06	POUNDS PER MILLION BTU HEAT INPUT	
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	15	BOILER #2	A	PM	8/17/2004	0.0178	POUNDS PER MILLION BTU HEAT INPUT	
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	15	BOILER #2	A	NOX	1/14/2003	0.239	POUNDS PER MILLION BTU HEAT INPUT	
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	15	BOILER #2	A	NOX	8/23/2005	0.081	POUNDS PER MILLION BTU HEAT INPUT	NOx testing done for verification not required annually. See next test date.
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	15	BOILER #2	A	NOX	9/12/2007	0.166	POUNDS PER MILLION BTU HEAT INPUT	
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	15	BOILER #2	A	PM	8/5/2003	0.0226	POUNDS PER MILLION BTU HEAT INPUT	
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	15	BOILER #2	A	PM	8/4/2005	0.007	POUNDS PER MILLION BTU HEAT INPUT	
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	15	BOILER #2	A	SO2	8/23/2005	0.0003	POUNDS PER MILLION BTU HEAT INPUT	
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	15	BOILER #2	A	SO2	8/5/2003	0.188	POUNDS PER MILLION BTU HEAT INPUT	
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	15	BOILER #2	A	PM	9/12/2007	0.0093	POUNDS PER MILLION BTU HEAT INPUT	
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	15	BOILER #2	A	PM	8/29/2006	0.02	POUNDS PER MILLION BTU HEAT INPUT	
ARIZONA CHEMICAL COMPANY	0050001	PANAMA CITY FACILITY	NWDP	BAY	A	Y	15	BOILER #2	A	SO2	8/17/2004	0.0665	POUNDS PER MILLION BTU HEAT INPUT	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	21	#1 SMELT DISSOLVING TANK (Venturi Scrubber)	A	PM	10/5/2004	0.137	POUNDS PER TON BLACK LIQUOR SOLIDS	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	21	#1 SMELT DISSOLVING TANK (Venturi Scrubber)	A	PM	10/10/2006	0.153	POUNDS PER TON BLACK LIQUOR SOLIDS	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	PM	10/21/2003	0.06	POUNDS PER MILLION BTU HEAT INPUT	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	PM	2/6/2006	0.068	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	PM	10/11/2006	0.0516	POUNDS PER MILLION BTU HEAT INPUT	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	PM	10/12/2005	0.05	POUNDS PER MILLION BTU HEAT INPUT	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	PM	6/26/2007	0.014	POUNDS PER MILLION BTU HEAT INPUT	40 CFR 63 DDDDD PM Standard = 0.07 poun per million BTU
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	4	LIME KILN BURNS LIME MUD TO PRODUCE CALCIUM OXIDE	A	PM	5/13/2004	0.049	GRAINS PER DRY STANDARD CUBIC FOOT @	

													10% O2	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	4	LIME KILN BURNS LIME MUD TO PRODUCE CALCIUM OXIDE	A	PM	10/5/2004	0.0524	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	4	LIME KILN BURNS LIME MUD TO PRODUCE CALCIUM OXIDE	A	PM	10/12/2006	0.0303	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	4	LIME KILN BURNS LIME MUD TO PRODUCE CALCIUM OXIDE	A	PM	10/13/2005	0.057	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	4	LIME KILN BURNS LIME MUD TO PRODUCE CALCIUM OXIDE	A	PM	10/15/2007	0.049	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	Weston Solutions
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	H114	6/26/2007	0.000003	POUNDS PER MILLION BTU HEAT INPUT	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	PM	10/21/2003	0.1	POUNDS PER MILLION BTU HEAT INPUT	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	H106	6/26/2007	0.0002	POUNDS PER MILLION BTU HEAT INPUT	40CFR63 DDDDD
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	21	#1 SMELT DISSOLVING TANK (Venturi Scrubber)	A	PM	10/10/2005	0.082	POUNDS PER TON BLACK LIQUOR SOLIDS	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	20	DISSOLVING TANK #2 (Venturi Scrubber)	A	PM	10/11/2006	0.148	POUNDS PER TON BLACK LIQUOR SOLIDS	Envrionmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	20	DISSOLVING TANK #2 (Venturi Scrubber)	A	PM	10/12/2005	0.075	POUNDS PER TON BLACK LIQUOR SOLIDS	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	H114	6/27/2007	0.56	POUNDS PER BILLION BTU HEAT INPUT	40 CFR 63 DDDDD MACT standard = 9 lb/bil Btu
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	20	DISSOLVING TANK #2 (Venturi Scrubber)	A	PM	10/5/2004	0.186	POUNDS PER TON BLACK LIQUOR SOLIDS	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	21	#1 SMELT DISSOLVING TANK (Venturi Scrubber)	A	PM	10/18/2007	0.1	POUNDS PER TON BLACK LIQUOR SOLIDS	Weston Solutions
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	20	DISSOLVING TANK #2 (Venturi Scrubber)	A	PM	10/17/2007	0.12	POUNDS PER TON BLACK LIQUOR SOLIDS	Weston Solutions
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	H106	6/27/2007	0.0003	POUNDS PER MILLION BTU HEAT INPUT	40 CFR 63 DDDDD Mact standard = 0.09 lb/m Btu
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	5	LIME SLAKER	A	PM	10/15/2007	1.53	POUNDS/HOUR	Weston Solutions
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	5	LIME SLAKER	A	PM	10/13/2005	3.18	POUNDS/HOUR	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	5	LIME SLAKER	A	PM	10/21/2003	3.61	POUNDS/HOUR	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	SO2	10/16/2007	344	POUNDS/HOUR	Weston Solutions
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	5	LIME SLAKER	A	PM	10/5/2004	1.25	POUNDS/HOUR	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	5	LIME SLAKER	A	PM	10/12/2006	2.53	POUNDS/HOUR	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	SO2	10/12/2005	454	POUNDS/HOUR	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	SO2	10/8/2004	16.5	POUNDS/HOUR	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	CO	8/24/2006	120	POUNDS/HOUR	Weston Solutions; Test for compliance of 0050 023-AC
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	PM	10/7/2004	46.924	POUNDS/HOUR	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	PM	8/24/2006	36	POUNDS/HOUR	Weston Solutions
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	PM	8/24/2006	36	POUNDS/HOUR	Weston Solutions; Test in compliance of 00500 023-AC
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	PM	10/10/2006	64.48	POUNDS/HOUR	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	PM	10/11/2005	55.385	POUNDS/HOUR	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	PM	6/27/2007	19.8	POUNDS/HOUR	PM - 0.047 lb/MMBtu x 421 MMBtu/hr = 19.8
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	SO2	10/21/2003	1.7	POUNDS/HOUR	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	SO2	10/21/2003	122	POUNDS/HOUR	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	SO2	10/7/2004	308	POUNDS/HOUR	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	SO2	10/10/2006	262.7	POUNDS/HOUR	Environmental Source Samplers

SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	SO2	10/11/2005	399	POUNDS/HOUR	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	SO2	10/17/2007	199	POUNDS/HOUR	Weston Solutions
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	NOX	8/24/2006	165	POUNDS/HOUR	Weston Solutions; Test in compliance of 00500 023-AC
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	SO2	10/11/2006	390	POUNDS/HOUR	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	19	RECOVERY BOILER #2 BURNING BLS FROM KRAFT PULPING PROCESS	A	PM	10/6/2004	0.0172	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	19	RECOVERY BOILER #2 BURNING BLS FROM KRAFT PULPING PROCESS	A	PM	10/11/2006	0.0061	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	19	RECOVERY BOILER #2 BURNING BLS FROM KRAFT PULPING PROCESS	A	PM	10/11/2005	0.0133	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	19	RECOVERY BOILER #2 BURNING BLS FROM KRAFT PULPING PROCESS	A	PM	10/11/2005	0.008	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	19	RECOVERY BOILER #2 BURNING BLS FROM KRAFT PULPING PROCESS	A	PM	10/11/2006	0.0061	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	19	RECOVERY BOILER #2 BURNING BLS FROM KRAFT PULPING PROCESS	A	PM	10/17/2007	0.019	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Weston Solutions
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	1	RECOVERY BOILER #1 WITH ESP	A	PM	10/10/2006	0.003	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	1	RECOVERY BOILER #1 WITH ESP	A	PM	10/10/2005	0.004	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	20	DISSOLVING TANK #2 (Venturi Scrubber)	A	TRS	10/17/2007	0.03	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	Weston Solutions
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	20	DISSOLVING TANK #2 (Venturi Scrubber)	A	TRS	10/12/2005	0.015	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	Envirnmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	20	DISSOLVING TANK #2 (Venturi Scrubber)	A	TRS	10/11/2006	0.017	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	20	DISSOLVING TANK #2 (Venturi Scrubber)	A	TRS	10/5/2004	0.013	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	20	DISSOLVING TANK #2 (Venturi Scrubber)	A	TRS	10/21/2003	0.02	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	21	#1 SMELT DISSOLVING TANK (Venturi Scrubber)	A	TRS	10/18/2007	0.029	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	Weston Solutions
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	21	#1 SMELT DISSOLVING TANK (Venturi Scrubber)	A	TRS	10/10/2005	0.01	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	21	#1 SMELT DISSOLVING TANK (Venturi Scrubber)	A	TRS	10/10/2006	0.018	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	21	#1 SMELT DISSOLVING TANK (Venturi Scrubber)	A	TRS	10/5/2004	0.0001	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	21	#1 SMELT DISSOLVING TANK (Venturi Scrubber)	A	TRS	10/21/2003	0.021	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	TRS	10/17/2007	0.5	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	TRS	10/11/2005	0.78	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	TRS	10/10/2006	0.18	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	TRS	10/7/2004	0.01	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	TRS	10/21/2003	0.56	PARTS PER MILLION DRY GAS VOLUME	

													@ 10% O2	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	TRS	10/16/2007	0.76	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	TRS	10/12/2005	0.55	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	TRS	10/11/2006	0.17	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	TRS	10/8/2004	0.01	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	TRS	10/21/2003	0.67	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	4	LIME KILN BURNS LIME MUD TO PRODUCE CALCIUM OXIDE	A	TRS	10/15/2007	1.91	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	4	LIME KILN BURNS LIME MUD TO PRODUCE CALCIUM OXIDE	A	TRS	10/13/2005	7.71	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	4	LIME KILN BURNS LIME MUD TO PRODUCE CALCIUM OXIDE	A	TRS	10/12/2006	3.34	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	4	LIME KILN BURNS LIME MUD TO PRODUCE CALCIUM OXIDE	A	TRS	10/5/2004	0.46	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	4	LIME KILN BURNS LIME MUD TO PRODUCE CALCIUM OXIDE	A	TRS	5/13/2004	1.95	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	20	DISSOLVING TANK #2 (Venturi Scrubber)	A	PM	10/21/2003	0.02	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	1	RECOVERY BOILER #1 WITH ESP	A	PM	10/21/2003	1.3	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	21	#1 SMELT DISSOLVING TANK (Venturi Scrubber)	A	PM	10/21/2003	0.021	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	19	RECOVERY BOILER #2 BURNING BLS FROM KRAFT PULPING PROCESS	A	PM	10/21/2003	0.8	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	1	RECOVERY BOILER #1 WITH ESP	A	PM	10/18/2007	0.009	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Weston Solutions
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	1	RECOVERY BOILER #1 WITH ESP	A	PM	10/10/2005	0.01	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	1	RECOVERY BOILER #1 WITH ESP	A	PM	10/10/2006	0.005	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Environmental Source Samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	1	RECOVERY BOILER #1 WITH ESP	A	PM	10/7/2004	0.0066	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Environmental Source Samplers, Inc
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	15	BARK BOILER #3	A	VOC	8/24/2006	4.6	POUNDS/HOUR	Weston Solutions; Test in compliance of 00500 023-AC
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	4	LIME KILN BURNS LIME MUD TO PRODUCE CALCIUM OXIDE	A	PM	10/21/2003	23.6	POUNDS/HOUR	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	4	LIME KILN BURNS LIME MUD TO PRODUCE CALCIUM OXIDE	A	PM	10/24/2003	33.1	POUNDS/HOUR	111% of permit limit
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	16	BARK BOILER #4 (FLY ASH ARRESTOR & WET SCRUBBER)	A	PM	10/8/2004	38.077	POUNDS/HOUR	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	19	RECOVERY BOILER #2 BURNING BLS FROM KRAFT PULPING PROCESS	A	TRS	10/6/2004	7.77	PARTS PER MILLION DRY GAS VOLUME	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	4	LIME KILN BURNS LIME MUD TO PRODUCE CALCIUM OXIDE	A	PM	10/22/2003	34.5	POUNDS/HOUR	115.7% of allowable limit
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	4	LIME KILN BURNS LIME MUD TO PRODUCE CALCIUM OXIDE	A	TRS	10/21/2003	3.6	PARTS PER MILLION DRY GAS VOLUME	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0050009	PANAMA CITY MILL	NWDP	BAY	A	Y	1	RECOVERY BOILER #1 WITH ESP	A	TRS	10/7/2004	3.14	PARTS PER MILLION DRY GAS VOLUME	Environmental Source Samplers, Inc.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	CO	7/26/2007	0.39	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gulf Power Environmental Affairs Field Servic group responsible for testing.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	CO	7/24/2007	1.46	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Testing was done by Gulf Power's Environmen Affairs Field Services group
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	CO	7/26/2005	0.499	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Normal mode. 1691 MMBtu/hr at 90 degrees F adjusts to 1754 MMBtu/hr at the reference temp 65 degress.6
													PARTS PER	

GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	CO	2/19/2003	0.46	MILLION DRY GAS VOLUME @ 15% O2	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	CO	8/1/2006	0.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Duct Burner
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	CO	8/1/2006	2.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Power Augmentation
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	CO	7/27/2005	1.567	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Power Augmentation Mode. 1801 MMBtu/hr L at 90 degrees F, adjusts to 1868 MMBtu/hr LH ref temp.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	CO	7/27/2004	1.514	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	CO	7/27/2004	0.573	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	CO	7/27/2004	2.061	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Duct burner on. Power Aug on.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	CO	2/19/2003	0.55	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	CO	8/1/2006	1.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Duct Burner
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	CO	8/1/2006	6.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Power Augmentation
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	CO	8/2/2005	0.508	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Normal mode. 1790 MMBtu/hr LHV at 90 deg Adjusts to 1856 MMBtu/hr LHV at reference t 90.5 % capacity.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	CO	8/3/2005	3.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	CO	7/25/2007	1.15	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	testing by Gulf Pwr Envr Affairs Field Serv gr
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	CO	7/25/2007	1.15	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	testing by Gulf Power Envr Affairs Field Serv g
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	CO	8/27/2003	2.12	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Tested by Gulf Power's Enviromental Affairs F Services
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	CO	8/27/2003	0.51	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Tested by Gulf Power's Enviromental Affairs F Services
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	CO	2/19/2003	0.55	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	CO	3/20/2003	0.55	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	CO	9/3/2003	1.72	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	CO	9/3/2003	0.48	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Tested by Gulf Power's Enviromental Affairs F Services
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	CO	2/19/2003	0.47	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	CO	3/19/2003	0.47	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test done in-house.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	CO	7/27/2004	0.53	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Duct burner on. Power Aug off.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	NOX	7/24/2007	62.6	POUNDS/HOUR	Testing by Gulf Power Env Affairs Field Serv g
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	NOX	7/26/2005	55.5	POUNDS/HOUR	Normal mode. 1691 MMBtu/hr LHV at 90 deg F: adjusts to 1754 MMBtu/hr LHV at the refer temp of 65 degress F. Tested at 86% capacity.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	NOX	7/27/2005	61.6	POUNDS/HOUR	Power augmentation mode. 1801 MMBtu/hr L 90 degrees F adjusts to 1868 at the reference te 86% capacity.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	NOX	7/26/2007	77.6	POUNDS/HOUR	Testing by Gulf Power Envr Affairs Field Serv group
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	NOX	8/1/2006	55.8	POUNDS/HOUR	Power augmentation.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	NOX	2/19/2003	56.4	POUNDS/HOUR	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	NOX	7/27/2004	53.9	POUNDS/HOUR	Duct burner on. Power Aug off.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	NOX	8/1/2006	75	POUNDS/HOUR	Power Augmetation
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	NOX	8/2/2005	55.7	POUNDS/HOUR	Normal mode. 1790 MMBtu/hr LHV at 90 deg Adjusts to 1856 MMBtu/hr LHV at reference t 90.5 % capacity.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	NOX	8/3/2005	82.2	POUNDS/HOUR	Power augmentation mode. 1861 MMBtu/hr L 90 degrees F. Adjusts to 1915 MMBtu/hr LHV at reference temp. 87% capacity.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	NOX	7/26/2007	102.6	POUNDS/HOUR	testing by Gulf Power Envr Affairs Field Serv g

GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	NOX	7/26/2007	74.6	POUNDS/HOUR	testing by Gulf Power Envir Affairs Serv group
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	NOX	9/3/2003	77.7	POUNDS/HOUR	Tested by Gulf Power's Enviromental Affairs F Services
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	NOX	9/3/2003	52.6	POUNDS/HOUR	Tested by Gulf Power's Enviromental Affairs F Services
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	NOX	3/19/2003	56.8	POUNDS/HOUR	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	NOX	3/19/2003	56.8	POUNDS/HOUR	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	NOX	8/27/2003	47	POUNDS/HOUR	Tested by Gulf Power's Enviromental Affairs F Services
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	NOX	8/27/2003	67.6	POUNDS/HOUR	Tested by Gulf Power's Enviromental Affairs F Services
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	NOX	2/19/2003	59.9	POUNDS/HOUR	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	NOX	3/20/2003	59.9	POUNDS/HOUR	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	NOX	7/27/2004	53.3	POUNDS/HOUR	C
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	NOX	7/27/2004	66.4	POUNDS/HOUR	Duct burner on. Power aug on.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	NOX	2/19/2003	59.9	POUNDS/HOUR	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	5	UNIT 5: 170 MW CT2 with HRSG and duct burner	A	NOX	8/1/2006	51	POUNDS/HOUR	Duct Burner
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	NOX	7/24/2004	80.9	POUNDS/HOUR	Duct Burner + Power Augment
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	4	UNIT 4: 170 MW CT1 with HRSG and duct burner	A	NOX	8/1/2006	58.4	POUNDS/HOUR	Duct Burner
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	1	BOILER NUMBER 1 - 1,944.8 MMBTU/HOUR (PHASE II ACID RAIN)	A	SO2	6/11/2007	1.29	POUNDS PER MILLION BTU HEAT INPUT	testing by Gulf Power Personnel
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	1	BOILER NUMBER 1 - 1,944.8 MMBTU/HOUR (PHASE II ACID RAIN)	A	SO2	5/24/2005	1.356	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	1	BOILER NUMBER 1 - 1,944.8 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	6/12/2007	0.012	POUNDS PER MILLION BTU HEAT INPUT	steady state; SO2 testing by Gulf Power person
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	1	BOILER NUMBER 1 - 1,944.8 MMBTU/HOUR (PHASE II ACID RAIN)	A	SO2	6/10/2003	1.504	POUNDS PER MILLION BTU HEAT INPUT	Done in conjunction with RATA.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	1	BOILER NUMBER 1 - 1,944.8 MMBTU/HOUR (PHASE II ACID RAIN)	A	SO2	5/11/2006	1.141	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	1	BOILER NUMBER 1 - 1,944.8 MMBTU/HOUR (PHASE II ACID RAIN)	A	SO2	6/1/2004	0.867	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	1	BOILER NUMBER 1 - 1,944.8 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	6/11/2007	0.009	POUNDS PER MILLION BTU HEAT INPUT	soot blowing
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	2	BOILER NUMBER 2 - 2,246.2 MMBTU/HOUR (PHASE II ACID RAIN)	A	SO2	6/10/2003	1.412	POUNDS PER MILLION BTU HEAT INPUT	in house; Done during RATA on 6/10/2003
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	2	BOILER NUMBER 2 - 2,246.2 MMBTU/HOUR (PHASE II ACID RAIN)	A	SO2	5/25/2005	1.631	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	2	BOILER NUMBER 2 - 2,246.2 MMBTU/HOUR (PHASE II ACID RAIN)	A	SO2	6/8/2004	1.017	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	2	BOILER NUMBER 2 - 2,246.2 MMBTU/HOUR (PHASE II ACID RAIN)	A	SO2	5/22/2006	1.144	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	2	BOILER NUMBER 2 - 2,246.2 MMBTU/HOUR (PHASE II ACID RAIN)	A	SO2	5/8/2007	1.3	POUNDS PER MILLION BTU HEAT INPUT	testing by Gulf Power personnel
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	1	BOILER NUMBER 1 - 1,944.8 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	5/21/2003	0.015	POUNDS PER MILLION BTU HEAT INPUT	MW limited to 188 until tested.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	1	BOILER NUMBER 1 - 1,944.8 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	5/22/2003	0.01	POUNDS PER MILLION BTU HEAT INPUT	MW limited to 188 until tested.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	1	BOILER NUMBER 1 - 1,944.8 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	5/25/2005	0.0135	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	1	BOILER NUMBER 1 - 1,944.8 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	5/24/2005	0.0132	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	1	BOILER NUMBER 1 - 1,944.8 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	6/1/2004	0.056	POUNDS PER MILLION BTU HEAT INPUT	Soot Blow
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	1	BOILER NUMBER 1 - 1,944.8 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	6/2/2004	0.0162	POUNDS PER MILLION BTU HEAT INPUT	Steady State
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	1	BOILER NUMBER 1 - 1,944.8 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	5/10/2006	0.012	POUNDS PER MILLION BTU HEAT INPUT	Steady State
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	1	BOILER NUMBER 1 - 1,944.8 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	5/11/2006	0.008	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	2	BOILER NUMBER 2 - 2,246.2 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	5/19/2003	0.013	POUNDS PER MILLION BTU HEAT INPUT	Limited to 215 MW until retested.
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	2	BOILER NUMBER 2 - 2,246.2 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	5/31/2005	0.0127	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	2	BOILER NUMBER 2 - 2,246.2 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	6/1/2005	0.0131	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	2	BOILER NUMBER 2 - 2,246.2 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	6/8/2004	0.013	POUNDS PER MILLION BTU HEAT INPUT	Soot Blow
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	2	BOILER NUMBER 2 - 2,246.2 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	6/9/2004	0.009	POUNDS PER MILLION BTU HEAT INPUT	Steady State
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	2	BOILER NUMBER 2 - 2,246.2 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	5/22/2006	0.015	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	2	BOILER NUMBER 2 - 2,246.2 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	5/22/2006	0.016	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER	0050014	LANSING SMITH	NWDP	BAY	A	Y	2	BOILER NUMBER 2 - 2,246.2 MMBTU/HOUR	A	PM	5/8/2007	0.015	POUNDS PER MILLION BTU	soot blowing

COMPANY		PLANT						(PHASE II ACID RAIN)					HEAT INPUT	
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	2	BOILER NUMBER 2 - 2,246.2 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	5/8/2007	0.02	POUNDS PER MILLION BTU HEAT INPUT	steady state
GULF POWER COMPANY	0050014	LANSING SMITH PLANT	NWDP	BAY	A	Y	2	BOILER NUMBER 2 - 2,246.2 MMBTU/HOUR (PHASE II ACID RAIN)	A	PM	5/20/2003	0.02	POUNDS PER MILLION BTU HEAT INPUT	Limited to 215 MW until retested.
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	PB	6/29/2005	0.000374	POUNDS/HOUR	The Air Compliance Group
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	H114	6/27/2005	0.000871	POUNDS/HOUR	THE AIR COMPLIANCE GROUP
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	PB	12/4/2004	0.035	POUNDS/HOUR	THE AIR COMPLIANCE GROUP, LLC
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	PB	11/11/2003	0.04	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	H114	11/11/2003	0.005	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	CO	11/11/2003	43.51	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	VOC	11/11/2003	1.52	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	VOC	6/28/2005	0.41	POUNDS/HOUR	The Air Compliance Group
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	VOC	11/2/2005	0.31	POUNDS/HOUR	THE AIR COMPLIANCE GROUP, LLC
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	VOC	11/15/2006	0.37	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	VOC	11/8/2007	0.31	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	H027	10/31/2005	0.0003	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	H027	11/19/2006	0.0004	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	H027	11/9/2007	0.00293	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	CO	11/11/2003	29.91	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	CO	6/29/2005	13.3	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	NOX	11/12/2003	19.88	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	NOX	6/29/2005	24.71	POUNDS/HOUR	The AIR COMPLIANCE GROUP
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	FL	6/28/2005	0.014	POUNDS/HOUR	THE AIR COMPLIANCE GROUP
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	SO2	11/12/2003	13	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	SO2	6/29/2005	12.43	POUNDS/HOUR	The Air Compliance Group
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	FL	6/28/2005	0.014	POUNDS/HOUR	The Air Compliance Group
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	CO	6/27/2005	16.81	POUNDS/HOUR	THE AIR COMPLIANCE GROUP
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	H114	10/31/2005	0.0077	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	DIOX	11/10/2007	14.8	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	DIOX	11/2/2005	47.15	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Of ten 1-hr runs, two, which were done on the s day, were extraordinairly high. All others were low. Diagonistic tests done testing in Jan 06 we unable to determine why these runs and one rur Unit 1, again all on the same day were very hig
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	DIOX	11/1/2005	19.54	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	DIOX	11/16/2006	14.7	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	DIOX	11/10/2007	0.31	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	DIOX	1/5/2006	4.15	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	cake removal from bags.
													NANOGRAMS	

BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	DIOX	1/4/2006	4.38	PER DRY STANDARD CUBIC METER @ 7% O2	Retesting because check out test in Nov 05 fail dioxins.
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	DIOX	1/6/2006	2.38	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	no carbon feed.
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	DIOX	11/17/2006	5	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	H114	11/16/2006	0.0025	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	PB	11/3/2005	0.0027	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	H114	11/9/2007	0.01303	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	PB	11/18/2006	0.0098	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	PB	11/10/2007	0.00317	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	VOC	11/8/2007	0.78	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	VOC	11/1/2005	0.38	POUNDS/HOUR	THE AIR COMPLIANCE GROUP, LLC
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	VOC	6/28/2005	0.47	POUNDS/HOUR	THE AIR COMPLIANCE GROUP
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	VOC	11/16/2006	0.47	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	VOC	11/12/2003	0.99	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	PB	12/4/2004	0.069	POUNDS/HOUR	The Air Compliance Group, LLC
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	PB	11/13/2003	0.12	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	H021	11/12/2003	0.000002	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	NOX	11/11/2003	23.64	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	NOX	6/27/2005	23.19	POUNDS/HOUR	THE AIR COMPLIANCE GROUP
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	H021	11/13/2003	0.000002	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	H021	6/29/2005	0.000005	POUNDS/HOUR	The Air Compliance Group
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	H114	11/12/2003	0.008	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	H114	6/29/2005	0.000989	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	SO2	11/11/2003	14.46	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	SO2	6/27/2005	6.08	POUNDS/HOUR	THE AIR COMPLIANCE GROUP
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	H021	6/29/2005	0.000001	POUNDS/HOUR	THE AIR COMPLIANCE GROUP
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	PB	1/12/2004	0.0356	POUNDS/HOUR	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	PB	6/27/2005	0.00216	POUNDS/HOUR	THE AIR COMPLIANCE GROUP
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	PM	11/11/2003	0.014	GRAINS PER DRY STANDARD CUBIC FOOT @ 12% CO2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	PM	6/28/2005	0.0024	GRAINS PER DRY STANDARD CUBIC FOOT @ 12% CO2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	PM	6/28/2005	0.001	GRAINS PER DRY STANDARD CUBIC FOOT @ 12% CO2	THE AIR COMPLIANCE GROUP
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	PM	11/10/2003	0.018	GRAINS PER DRY STANDARD CUBIC FOOT @ 12% CO2	
BAY COUNTY BOARD OF COUNTY	0050031	BAY COUNTY WASTE-TO-ENERGY	NWDP	BAY	A	Y	2	MSW combustion Unit #2	A	H027	11/10/2007	0.00026	MILLIGRAMS PER DRY STANDARD	

COMMISSIONERS		FACILITY						(South)					CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	H027	11/18/2006	0.001	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	H027	11/3/2005	0.0027	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	PB	11/9/2007	0.04337	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	PB	11/16/2006	0.002	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	PB	10/31/2005	0.0038	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	H114	11/10/2007	0.00587	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	H114	11/18/2006	0.0018	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	H114	11/3/2005	0.0031	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	PM	11/10/2007	17.674	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	PM	11/18/2006	6.9	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	PM	11/3/2005	1.56	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	THE AIR COMPLIANCE GROUP, LLC
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	PM	11/9/2007	0.01303	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	PM	11/19/2006	13.8	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	PM	10/31/2005	1.49	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	H106	11/8/2007	7.31	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	H106	11/16/2006	1.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	1	MSW Combustion Unit #1 (North)	A	H106	11/1/2005	8.32	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	THE AIR COMPLIANCE GROUP, LLC
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	H106	11/9/2007	6.18	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	H106	11/15/2006	2.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BAY COUNTY BOARD OF COUNTY COMMISSIONERS	0050031	BAY COUNTY WASTE-TO-ENERGY FACILITY	NWDP	BAY	A	Y	2	MSW combustion Unit #2 (South)	A	H106	11/2/2005	3.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
E.I. DUPONT DE NEMOURS & CO INC HIGHLAND	0070001	E.I. DUPONT DE NEMOURS & CO INC HIGHLAND	NED	BRADFORD	A	Y	1	DRYER ROTARY ILMENITE W/CYCLONE A	A	PM	11/24/2003	16.11	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	SO2	5/9/2007	0.0198	POUNDS/HOUR	Operating rate = 3834 bhp (permitted to 4000 b 95%
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	SO2	7/28/2003	0.0557	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	SO2	7/22/2004	0.042	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	SO2	6/20/2006	0.0388	POUNDS/HOUR	Based on fuel sulfur analysis
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	SO2	7/22/2004	0.042	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	SO2	6/10/2005	0.021	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	CO	6/12/2007	11.8	PARTS PER MILLION DRY GAS VOLUME	Full load. 1.57 lbs/hr.

													@ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	CO	6/2/2004	4.48	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	CO	5/2/2003	4.02	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	CO	3/6/2003	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	CO	3/25/2004	9.59	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	CO	3/6/2003	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	CO	8/11/2005	1.81	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	CO	6/9/2005	1.57	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	CO	6/2/2004	4.48	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	CO	6/20/2006	2.38	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	NOX	5/2/2003	11.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	NOX	3/6/2003	11.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	NOX	3/25/2004	14.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	NOX	3/6/2003	11.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	NOX	8/11/2005	16.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	NOX	6/9/2005	14.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	NOX	6/2/2004	12.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	NOX	6/2/2004	12.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	NOX	6/20/2006	13.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	NOX	6/12/2007	15.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Full load. 3.36 lbs/hr NOX.
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	SO2	5/2/2003	0.151	TEST REQUIRED (NO ALLOWABLE EMISSION)	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	SO2	8/11/2005	0.594	TEST REQUIRED (NO ALLOWABLE EMISSION)	SO2 = 0.594 Total sulfur in fuel (grains per 10 of NG)
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	SO2	6/12/2007	0.443	TEST REQUIRED (NO ALLOWABLE EMISSION)	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	SO2	6/20/2006	0.516	TEST REQUIRED (NO ALLOWABLE EMISSION)	Fuel sulfur analysis
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	SO2	6/2/2004	0.0601	TEST REQUIRED (NO ALLOWABLE EMISSION)	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	SO2	6/2/2004	0.369	TEST REQUIRED (NO ALLOWABLE EMISSION)	SO2 = 0.369 Total sulfur in fuel (grains S per 1 SCF of NG)
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	SO2	6/9/2005	2.04	TEST REQUIRED (NO ALLOWABLE EMISSION)	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	SO2	3/6/2003	0.299	TEST REQUIRED (NO ALLOWABLE EMISSION)	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	3	Gas Turbine Compressor (FGT Unit No. 1607)	A	SO2	3/6/2003	0.299	TEST REQUIRED (NO ALLOWABLE EMISSION)	reported as (grains/100 scf of fuel)
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	NOX	5/9/2007	13.2	POUNDS/HOUR	Operating rate = 3834 bhp (permitted to 4000 b 95%
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	NOX	7/22/2004	9.76	POUNDS/HOUR	

FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	NOX	6/10/2005	4.07	POUNDS/HOUR	Control Pane Horsepower = 3876.
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	CO	6/20/2006	7.22	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	CO	6/10/2005	9.91	POUNDS/HOUR	Control Panel Horsepower = 3876
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	CO	7/28/2003	8.16	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	CO	7/22/2004	7.97	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	CO	7/22/2004	7.97	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	CO	5/9/2007	7.35	POUNDS/HOUR	Operating rate = 3834 bhp (permitted to 4000 b 95%
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	NOX	7/28/2003	8.27	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	NOX	7/22/2004	9.76	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0070012	BRADFORD CO STATION #16	NED	BRADFORD	A	Y	2	Unit 1606 - one 4000 bhp gas-fired recip IC engine	A	NOX	6/20/2006	15.1	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PCC)	0090006	CAPE CANAVERAL PLANT	CD	BREVARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR,UNIT #1	A	PM	2/6/2007	0.04	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PCC)	0090006	CAPE CANAVERAL PLANT	CD	BREVARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR,UNIT #1	A	PM	1/24/2006	0.05	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PCC)	0090006	CAPE CANAVERAL PLANT	CD	BREVARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR,UNIT #1	A	PM	6/9/2004	0.04	POUNDS PER MILLION BTU HEAT INPUT	Florida Power and Light stack test team
FLORIDA POWER & LIGHT (PCC)	0090006	CAPE CANAVERAL PLANT	CD	BREVARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT #2	A	PM	2/13/2007	0.04	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PCC)	0090006	CAPE CANAVERAL PLANT	CD	BREVARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT #2	A	PM	1/31/2006	0.06	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PCC)	0090006	CAPE CANAVERAL PLANT	CD	BREVARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT #2	A	PM	6/8/2003	0.04	POUNDS PER MILLION BTU HEAT INPUT	Florida Power and Light stack test team
FLORIDA POWER & LIGHT (PCC)	0090006	CAPE CANAVERAL PLANT	CD	BREVARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT #2	A	PM	3/19/2003	0.03	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PCC)	0090006	CAPE CANAVERAL PLANT	CD	BREVARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT #2	A	PM	3/19/2003	0.04	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PCC)	0090006	CAPE CANAVERAL PLANT	CD	BREVARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT #2	A	PM	6/9/2004	0.05	POUNDS PER MILLION BTU HEAT INPUT	Florida Power and Light stack test team
FLORIDA POWER & LIGHT (PCC)	0090006	CAPE CANAVERAL PLANT	CD	BREVARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT #2	A	PM	1/31/2006	0.05	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PCC)	0090006	CAPE CANAVERAL PLANT	CD	BREVARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR,UNIT #1	A	PM	3/11/2003	0.04	POUNDS PER MILLION BTU HEAT INPUT	FP&L stack test group
FLORIDA POWER & LIGHT (PCC)	0090006	CAPE CANAVERAL PLANT	CD	BREVARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR,UNIT #1	A	PM	3/11/2003	0.03	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PCC)	0090006	CAPE CANAVERAL PLANT	CD	BREVARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR,UNIT #1	A	PM	6/9/2004	0.05	POUNDS PER MILLION BTU HEAT INPUT	Florida Power and Light stack test team
FLORIDA POWER & LIGHT (PCC)	0090006	CAPE CANAVERAL PLANT	CD	BREVARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR,UNIT #1	A	PM	1/24/2006	0.06	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	7	35 MW Simple Cycle Combustion Turbine B	A	NOX	8/20/2007	26.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	STACS
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	7	35 MW Simple Cycle Combustion Turbine B	A	NOX	8/14/2003	30.57	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	7	35 MW Simple Cycle Combustion Turbine B	A	NOX	8/25/2004	27.93	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test conducted by STACS (Stack Testing and Consulting Service)
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	5	129 MW Simple Cycle Combustion Turbine C(Acid Rain Phase II)	A	NOX	9/23/2004	22.43	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test conducted by STACS (Stack Testing and Consulting Service)
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	6	129 MW Simple Cycle Combustion Turbine D(Acid Rain Phase II)	A	NOX	8/23/2007	16.79	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	STACS
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	6	129 MW Simple Cycle Combustion Turbine D(Acid Rain Phase II)	A	NOX	8/12/2003	21.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	STACS
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	6	129 MW Simple Cycle Combustion Turbine D(Acid Rain Phase II)	A	NOX	8/24/2004	18.33	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	STACS (Source Testing and Consulting Servic
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	5	129 MW Simple Cycle Combustion Turbine C(Acid Rain Phase II)	A	NOX	8/12/2003	21.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Source Testing and Consulting Service (STAC
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	4	35 MW Simple Cycle Combustion Turbine A	A	NOX	8/14/2003	36.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	4	35 MW Simple Cycle Combustion Turbine A	A	NOX	8/25/2004	38.63	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test conducted by STACS (Stack Testing and Consulting Service)
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	4	35 MW Simple Cycle Combustion Turbine A	A	NOX	8/20/2007	35.19	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	STACS

ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	5	129 MW Simple Cycle Combustion Turbine C(Acid Rain Phase II)	A	NOX	8/22/2007	20.39	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	STACS
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	6	129 MW Simple Cycle Combustion Turbine D(Acid Rain Phase II)	A	CO	8/23/2007	0.79	PARTS PER MILLION DRY GAS VOLUME	STACS
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	6	129 MW Simple Cycle Combustion Turbine D(Acid Rain Phase II)	A	CO	8/24/2004	1.03	PARTS PER MILLION DRY GAS VOLUME	STACS (Source Testing and Consulting Servic
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	5	129 MW Simple Cycle Combustion Turbine C(Acid Rain Phase II)	A	CO	8/15/2005	0.66	PARTS PER MILLION DRY GAS VOLUME	
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	5	129 MW Simple Cycle Combustion Turbine C(Acid Rain Phase II)	A	CO	8/14/2003	0.08	PARTS PER MILLION DRY GAS VOLUME	
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	5	129 MW Simple Cycle Combustion Turbine C(Acid Rain Phase II)	A	CO	9/23/2004	0.63	PARTS PER MILLION DRY GAS VOLUME	STACS (Source Testing and Consulting Servic
ORLANDO UTLITIES COMMISSION	0090008	INDIAN RIVER PLANT - OUC	CD	BREVARD	A	Y	5	129 MW Simple Cycle Combustion Turbine C(Acid Rain Phase II)	A	CO	8/22/2007	1.17	PARTS PER MILLION DRY GAS VOLUME	STACS
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	1	I. C. Engine No. 1901 (2600) NG fired 4 Stroke Lean Burn	A	CO	7/19/2007	9.05	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	1	I. C. Engine No. 1901 (2600) NG fired 4 Stroke Lean Burn	A	CO	7/11/2006	9.49	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	1	I. C. Engine No. 1901 (2600) NG fired 4 Stroke Lean Burn	A	CO	8/17/2004	10.5	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	1	I. C. Engine No. 1901 (2600) NG fired 4 Stroke Lean Burn	A	CO	8/20/2003	10.9	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	3	I. C. Engine No. 1903 (5000) NG fired 2 Stroke Lean	A	CO	7/11/2006	12.88	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	3	I. C. Engine No. 1903 (5000) NG fired 2 Stroke Lean	A	CO	8/28/2003	16.8	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	3	I. C. Engine No. 1903 (5000) NG fired 2 Stroke Lean	A	CO	8/18/2004	16	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	3	I. C. Engine No. 1903 (5000) NG fired 2 Stroke Lean	A	CO	7/28/2005	18.2	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	3	I. C. Engine No. 1903 (5000) NG fired 2 Stroke Lean	A	CO	7/19/2007	15.93	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	1	I. C. Engine No. 1901 (2600) NG fired 4 Stroke Lean Burn	A	CO	8/17/2004	10.3	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	1	I. C. Engine No. 1901 (2600) NG fired 4 Stroke Lean Burn	A	CO	7/27/2005	10.3	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	2	I. C. Engine No. 1902 (2600) NG fired 4 Stroke Lean Burn	A	SO2	7/27/2005	0.0383	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	2	I. C. Engine No. 1902 (2600) NG fired 4 Stroke Lean Burn	A	NOX	8/16/2004	6.75	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	2	I. C. Engine No. 1902 (2600) NG fired 4 Stroke Lean Burn	A	NOX	7/27/2005	4.17	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	2	I. C. Engine No. 1902 (2600) NG fired 4 Stroke Lean Burn	A	NOX	7/12/2006	4.48	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	2	I. C. Engine No. 1902 (2600) NG fired 4 Stroke Lean Burn	A	NOX	7/19/2007	6.67	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	1	I. C. Engine No. 1901 (2600) NG fired 4 Stroke Lean Burn	A	SO2	8/20/2003	0.03	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	1	I. C. Engine No. 1901 (2600) NG fired 4 Stroke Lean Burn	A	SO2	7/27/2005	0.04	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	2	I. C. Engine No. 1902 (2600) NG fired 4 Stroke Lean Burn	A	CO	8/21/2003	13.5	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	2	I. C. Engine No. 1902 (2600) NG fired 4 Stroke Lean Burn	A	CO	8/16/2004	11.7	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	2	I. C. Engine No. 1902 (2600) NG fired 4 Stroke Lean Burn	A	CO	7/27/2005	11.7	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	2	I. C. Engine No. 1902 (2600) NG fired 4 Stroke Lean Burn	A	NOX	8/21/2003	3.67	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	2	I. C. Engine No. 1902 (2600) NG fired 4 Stroke Lean Burn	A	CO	7/12/2006	9.01	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	2	I. C. Engine No. 1902 (2600) NG fired 4 Stroke Lean Burn	A	CO	7/19/2007	10	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	1	I. C. Engine No. 1901 (2600) NG fired 4 Stroke Lean Burn	A	NOX	8/20/2003	5.87	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	1	I. C. Engine No. 1901 (2600) NG fired 4 Stroke Lean Burn	A	NOX	8/17/2004	11.5	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	1	I. C. Engine No. 1901 (2600) NG fired 4 Stroke Lean Burn	A	NOX	8/17/2004	6.63	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	1	I. C. Engine No. 1901 (2600) NG fired 4 Stroke Lean Burn	A	NOX	7/27/2005	7.91	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	1	I. C. Engine No. 1901 (2600) NG fired 4 Stroke Lean Burn	A	NOX	7/11/2006	5.39	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	1	I. C. Engine No. 1901 (2600) NG fired 4 Stroke Lean Burn	A	NOX	7/19/2007	2.62	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	3	I. C. Engine No. 1903 (5000) NG fired 2 Stroke Lean	A	NOX	8/28/2003	7.99	POUNDS/HOUR	

FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	3	I. C. Engine No. 1903 (5000) NG fired 2 Stroke Lean	A	NOX	8/18/2004	9.16	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	3	I. C. Engine No. 1903 (5000) NG fired 2 Stroke Lean	A	NOX	7/28/2005	6.44	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	3	I. C. Engine No. 1903 (5000) NG fired 2 Stroke Lean	A	NOX	7/11/2006	5.88	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	3	I. C. Engine No. 1903 (5000) NG fired 2 Stroke Lean	A	NOX	7/19/2007	13.48	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0090106	FGTC COMPRESSOR STATION 19	CD	BREVARD	A	Y	2	I. C. Engine No. 1902 (2600) NG fired 4 Stroke Lean Burn	A	SO2	8/21/2003	0.0253	POUNDS/HOUR	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	5	190 MW COMBUSTION TURBINE	C	PM10	12/7/2007	0	PERCENT OPACITY	VE on both gas and oil was zero
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	5	190 MW COMBUSTION TURBINE	C	SO2	12/6/2007	0.002	GRAINS SULFUR PER 100 STANDARD CUBIC FEET OF GAS	Natural gas analysis from Florida Gas Transmis Brooker 24
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	5	190 MW COMBUSTION TURBINE	C	PM	12/6/2007	0.002	GRAINS SULFUR PER 100 STANDARD CUBIC FEET OF GAS	Natural Gas analysis from Florida Gas Transmi Brooker 24.
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	5	190 MW COMBUSTION TURBINE	C	PM10	12/6/2007	0.002	GRAINS SULFUR PER 100 STANDARD CUBIC FEET OF GAS	Natural gas analysis from Florida Gas Transmis Brooker 24
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	5	190 MW COMBUSTION TURBINE	C	PM	12/7/2007	0	PERCENT OPACITY	Opacity on both gs and oil was zero
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	1	190 MW Combustion Turbine	A	CO	6/20/2007	0.1	PARTS PER MILLION DRY GAS VOLUME	Test conducted by Gulf Power
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	1	190 MW Combustion Turbine	A	CO	5/17/2004	0.07	PARTS PER MILLION DRY GAS VOLUME	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	2	190 MW COMBUSTION TURBINE	A	CO	9/30/2005	0.038	PARTS PER MILLION DRY GAS VOLUME	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	2	190 MW COMBUSTION TURBINE	A	CO	6/19/2007	0	PARTS PER MILLION DRY GAS VOLUME	Test conducted by Gulf Power
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	4	190 MW COMBUSTION TURBINE	A	CO	7/22/2003	0.38	PARTS PER MILLION DRY GAS VOLUME	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	4	190 MW COMBUSTION TURBINE	A	CO	6/4/2006	0.12	PARTS PER MILLION DRY GAS VOLUME	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	4	190 MW COMBUSTION TURBINE	A	CO	9/30/2005	0.48	PARTS PER MILLION DRY GAS VOLUME	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	4	190 MW COMBUSTION TURBINE	A	CO	6/22/2007	0.1	PARTS PER MILLION DRY GAS VOLUME	Test conducted by Gulf Power
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	1	190 MW Combustion Turbine	A	CO	5/15/2003	0.31	PARTS PER MILLION DRY GAS VOLUME	Costal Air Consulting
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	1	190 MW Combustion Turbine	A	CO	4/26/2005	0.1	PARTS PER MILLION DRY GAS VOLUME	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	1	190 MW Combustion Turbine	A	CO	4/20/2005	0.1	PARTS PER MILLION DRY GAS VOLUME	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	3	190 MW COMBUSTION TURBINE	A	CO	7/21/2003	0.62	PARTS PER MILLION DRY GAS VOLUME	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	3	190 MW COMBUSTION TURBINE	A	CO	6/3/2006	0.14	PARTS PER MILLION DRY GAS VOLUME	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	3	190 MW COMBUSTION TURBINE	A	CO	9/30/2005	0.38	PARTS PER MILLION DRY GAS VOLUME	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	3	190 MW COMBUSTION TURBINE	A	CO	6/21/2007	0.05	PARTS PER MILLION DRY GAS VOLUME	Test conducted by Gulf Power
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	2	190 MW COMBUSTION TURBINE	A	CO	4/11/2003	0.23	PARTS PER MILLION DRY GAS VOLUME	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	2	190 MW COMBUSTION TURBINE	A	CO	4/11/2003	2.2	PARTS PER MILLION DRY GAS VOLUME	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	2	190 MW COMBUSTION TURBINE	A	CO	4/27/2005	0.32	PARTS PER MILLION DRY GAS VOLUME	Coastal Air Consulting
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	2	190 MW COMBUSTION TURBINE	A	CO	5/18/2004	0.32	PARTS PER MILLION DRY GAS VOLUME	Costal Air Consulting, Teting conducted at 162 megawatts, fuel was natural gas
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	2	190 MW COMBUSTION TURBINE	A	CO	6/2/2006	0.11	PARTS PER MILLION DRY GAS VOLUME	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	1	190 MW Combustion Turbine	A	CO	5/17/2004	0.07	PARTS PER MILLION DRY GAS VOLUME	Costal Air Consulting, Testing conducted at 15 megawatts, fuel was natural gas
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	1	190 MW Combustion Turbine	A	CO	6/1/2006	0.24	PARTS PER MILLION DRY GAS VOLUME	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	1	190 MW Combustion Turbine	A	CO	6/1/2006	0.24	PARTS PER MILLION DRY GAS VOLUME	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	2	190 MW COMBUSTION TURBINE	A	SO2	6/19/2007	0.00349	PERCENT SULFUR IN FUEL	sullfur content of gas is 0.349 grains/100 SCF. conducted by Gulf Power
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	2	190 MW COMBUSTION TURBINE	A	NOX	9/30/2005	7.22	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	2	190 MW COMBUSTION TURBINE	A	NOX	5/18/2004	7.15	PARTS PER MILLION DRY GAS VOLUME	Costal Air Consulting, Testing conductd at 162 megawatts, fuel was natural gas

													@ 15% O2	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	2	190 MW COMBUSTION TURBINE	A	NOX	4/11/2003	36	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	5	190 MW COMBUSTION TURBINE	C	NOX	12/7/2007	36.42	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test performed by Spectrum. Burning oil. Actu average of 3 runs. Heat input based on lower hε value
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	5	190 MW COMBUSTION TURBINE	C	SO2	12/7/2007	0.0138	PERCENT SULFUR IN FUEL	fuel analysis #2 fuel oil
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	5	190 MW COMBUSTION TURBINE	C	NOX	12/6/2007	7.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test performed by Spectrum. Burning natural g from FGT Brooker 24. Actual is average of 9 rı Heat input based on lower heating value
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	5	190 MW COMBUSTION TURBINE	C	PM	12/7/2007	0.0138	PERCENT SULFUR IN FUEL	Fuel analysis #2 oil
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	3	190 MW COMBUSTION TURBINE	A	SO2	6/21/2007	0.00203	PERCENT SULFUR IN FUEL	Sulfur contest of fuel was 0.203 grains/100 SCI Test conducted by Gulf Power
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	1	190 MW Combustion Turbine	A	NOX	5/15/2003	6.18	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Costal Air Consulting
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	1	190 MW Combustion Turbine	A	NOX	4/26/2005	6.61	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Costal Air Consulting
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	1	190 MW Combustion Turbine	A	NOX	5/17/2004	7.06	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Costal Air Consulting Test conducted at 157 M
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	1	190 MW Combustion Turbine	A	NOX	6/1/2006	6.617	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	1	190 MW Combustion Turbine	A	NOX	6/20/2007	8.91	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test conducted by Gulf Power
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	4	190 MW COMBUSTION TURBINE	A	NOX	7/22/2003	6.32	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	4	190 MW COMBUSTION TURBINE	A	NOX	6/4/2006	5.76	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	5	190 MW COMBUSTION TURBINE	C	PM10	12/7/2007	0.005	PERCENT SULFUR IN FUEL	Natural gas. Fuel analysis from Florida Gas Transmission
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	4	190 MW COMBUSTION TURBINE	A	NOX	9/30/2005	6.32	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	4	190 MW COMBUSTION TURBINE	A	NOX	6/22/2007	8.77	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test conducted by Gulf Power
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	3	190 MW COMBUSTION TURBINE	A	NOX	7/21/2003	5.25	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	3	190 MW COMBUSTION TURBINE	A	NOX	6/3/2006	7.34	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	3	190 MW COMBUSTION TURBINE	A	NOX	9/30/2005	7.22	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	3	190 MW COMBUSTION TURBINE	A	NOX	6/21/2007	7.25	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test conducted by Gulf Power
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	1	190 MW Combustion Turbine	A	SO2	6/20/2007	0.00349	PERCENT SULFUR IN FUEL	Sulfur content of gas was 0.349 grain/100 SCF. conducted by Gulf Power
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	2	190 MW COMBUSTION TURBINE	A	NOX	4/11/2003	7.05	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	2	190 MW COMBUSTION TURBINE	A	NOX	4/27/2005	6.24	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Coastal Air Consulting
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	2	190 MW COMBUSTION TURBINE	A	NOX	6/2/2006	6.604	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	4	190 MW COMBUSTION TURBINE	A	SO2	6/22/2007	0.00249	PERCENT SULFUR IN FUEL	Gulf Power
OLEANDER POWER PROJECT, LP	0090180	OLEANDER POWER PROJECT	CD	BREVARD	A	Y	2	190 MW COMBUSTION TURBINE	A	NOX	6/19/2007	7.78	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test conducted by Gulf Power
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	SO2	9/12/2007	1.323	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	SO2	5/1/2005	1.499	POUNDS PER MILLION BTU HEAT INPUT	Coastal Air Consulting, test conducted June 7, :
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	3	328 MW Unit No. 3 Boiler (Phase II Acid Rain Unit)	A	SO2	9/11/2007	1.473	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	3	328 MW Unit No. 3 Boiler (Phase II Acid Rain Unit)	A	SO2	5/12/2004	1.625	POUNDS PER MILLION BTU HEAT INPUT	Costal Air Consulting
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	1	87 MW Unit No.1 Boiler (Phase II Acid Rain Unit)	A	PM	5/30/2003	0.08	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	1	87 MW Unit No.1 Boiler (Phase II Acid Rain Unit)	A	PM	5/30/2003	0.22	POUNDS PER MILLION BTU HEAT INPUT	
													POUNDS PER	

RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	1	87 MW Unit No.1 Boiler (Phase II Acid Rain Unit)	A	PM	5/11/2004	0.06	MILLION BTU HEAT INPUT	Costal Air Consulting
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	1	87 MW Unit No.1 Boiler (Phase II Acid Rain Unit)	A	PM	5/11/2004	0.139	POUNDS PER MILLION BTU HEAT INPUT	Costal Air Consulting
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	1	87 MW Unit No.1 Boiler (Phase II Acid Rain Unit)	A	PM	4/7/2005	0.04	POUNDS PER MILLION BTU HEAT INPUT	Costal Air Consulting
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	1	87 MW Unit No.1 Boiler (Phase II Acid Rain Unit)	A	PM	6/21/2006	0.189	POUNDS PER MILLION BTU HEAT INPUT	Costal Air Consulting
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	1	87 MW Unit No.1 Boiler (Phase II Acid Rain Unit)	A	PM	6/21/2006	0.085	POUNDS PER MILLION BTU HEAT INPUT	Costal Air Consulting
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	1	87 MW Unit No.1 Boiler (Phase II Acid Rain Unit)	A	PM	8/8/2007	0.032	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	1	87 MW Unit No.1 Boiler (Phase II Acid Rain Unit)	A	PM	8/8/2007	0.093	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	3	328 MW Unit No. 3 Boiler (Phase II Acid Rain Unit)	A	PM	5/12/2004	0.088	POUNDS PER MILLION BTU HEAT INPUT	Costal Air Consulting
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	3	328 MW Unit No. 3 Boiler (Phase II Acid Rain Unit)	A	PM	6/20/2006	0.036	POUNDS PER MILLION BTU HEAT INPUT	Coastal Air Consulting
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	3	328 MW Unit No. 3 Boiler (Phase II Acid Rain Unit)	A	PM	6/20/2006	0.048	POUNDS PER MILLION BTU HEAT INPUT	Costal Air Consulting
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	3	328 MW Unit No. 3 Boiler (Phase II Acid Rain Unit)	A	PM	9/11/2007	0.051	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	3	328 MW Unit No. 3 Boiler (Phase II Acid Rain Unit)	A	PM	9/11/2007	0.076	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	PM	5/12/2003	0.04	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	PM	5/12/2003	0.06	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	PM	4/5/2004	0.05	POUNDS PER MILLION BTU HEAT INPUT	Costal Air Consulting Consulting
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	PM	4/5/2004	0.1	POUNDS PER MILLION BTU HEAT INPUT	Costal Air Consulting
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	1	87 MW Unit No.1 Boiler (Phase II Acid Rain Unit)	A	SO2	5/11/2004	1.436	POUNDS PER MILLION BTU HEAT INPUT	Fuel sulfur content determined by Reliant
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	1	87 MW Unit No.1 Boiler (Phase II Acid Rain Unit)	A	SO2	6/21/2006	1.352	POUNDS PER MILLION BTU HEAT INPUT	SO2 emissions are calulated from fuel analysis.
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	1	87 MW Unit No.1 Boiler (Phase II Acid Rain Unit)	A	SO2	8/8/2007	1.49	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	3	328 MW Unit No. 3 Boiler (Phase II Acid Rain Unit)	A	PM	5/27/2003	0.05	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	3	328 MW Unit No. 3 Boiler (Phase II Acid Rain Unit)	A	PM	5/27/2003	0.09	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	3	328 MW Unit No. 3 Boiler (Phase II Acid Rain Unit)	A	PM	7/21/2005	0.036	POUNDS PER MILLION BTU HEAT INPUT	Coastal AirConsulting
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	3	328 MW Unit No. 3 Boiler (Phase II Acid Rain Unit)	A	PM	7/21/2005	0.13	POUNDS PER MILLION BTU HEAT INPUT	Coastal Air Consulting
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	3	328 MW Unit No. 3 Boiler (Phase II Acid Rain Unit)	A	PM	5/12/2004	0.05	POUNDS PER MILLION BTU HEAT INPUT	Costal Air Consulting
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	PM	5/1/2005	0.13	POUNDS PER MILLION BTU HEAT INPUT	Coastal Air Consulting, test conducted June 7,
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	PM	5/1/2005	0.07	POUNDS PER MILLION BTU HEAT INPUT	Coastal Air Consulting, test conducted June 7,
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	PM	5/24/2006	0.08	POUNDS PER MILLION BTU HEAT INPUT	Steady State
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	PM	5/24/2006	0.13	POUNDS PER MILLION BTU HEAT INPUT	soot blowing
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	PM	5/24/2006	0.008	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	PM	5/24/2006	0.13	POUNDS PER MILLION BTU HEAT INPUT	Costal Air Consulting
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	PM	9/12/2007	0	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	PM	9/12/2007	0.049	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	3	328 MW Unit No. 3 Boiler (Phase II Acid Rain Unit)	A	SO2	6/20/2006	1.238	POUNDS PER MILLION BTU HEAT INPUT	SO2 emissions clulated from fuel analysis
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	SO2	5/12/2004	1.625	POUNDS PER MILLION BTU HEAT INPUT	Sulfur content of oil is done by Reliant
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	SO2	5/24/2006	1.188	POUNDS PER MILLION BTU HEAT INPUT	
RELIANT ENERGY FLORIDA, L.L.C.	0090196	RELIANT INDIAN RIVER PLANT	CD	BREVARD	A	Y	2	188 MW Unit No. 2 Boiler (Phase II Acid Rain Unit)	A	SO2	5/24/2006	1.188	POUNDS PER MILLION BTU HEAT INPUT	SO2 emissions are calulated from fuel analysis
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	DIOX	6/9/2004	1.6	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD	0110002	MEMORIAL REGIO HOSP/SO BROWARD	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR	A	DIOX	6/30/2003	1.1	NANOGRAMS PER DRY STANDARD	Review conducted by c.pitters.

HOSP DIST		HOSP DIST						1550 TYPES 0-IV					CUBIC METER @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	DIOX	6/30/2005	2.2	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	PM	6/30/2003	0.008	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Review conducted by c.pitters.
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	PM	6/9/2004	0.012	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	PM	6/28/2006	0.009	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Test conducted by Air Testing & Consulting.
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	CO	6/30/2005	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	CO	6/28/2006	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test conducted by Air Testing & Consulting
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	SO2	7/30/2003	24	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Review conducted by c.pitters.
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	H114	6/9/2004	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	H114	6/30/2005	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	H114	6/30/2003	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	PB	6/9/2004	0.12	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	PB	6/30/2005	0.04	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	PB	6/30/2003	0.01	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Review conducted by c.pitters.
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	H027	6/9/2004	0.01	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	H027	6/30/2005	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	H027	6/30/2003	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Review conducted by c.pitters.
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	H106	7/27/2007	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testing conducted by Air Testing & Consulting
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	H106	6/28/2006	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test conducted by Air Testing & Consulting
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	H106	6/9/2004	2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	H106	6/30/2005	2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	H106	6/30/2003	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Review conducted by c.pitters.
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	NOX	6/9/2004	134	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	NOX	6/30/2005	101	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	NOX	6/30/2003	132	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Review conducted by c.pitters.
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	SO2	6/9/2004	11	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	SO2	6/30/2005	5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
MEMORIAL REGIO		MEMORIAL REGIO						CLEAVER BROOKS					PARTS PER MILLION DRY	

HOSP/SO BROWARD HOSP DIST	0110002	HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	1900/95 INCINERATOR 1550 TYPES 0-IV	A	CO	7/27/2007	0	GAS VOLUME @ 7% O2	Test conducted by Air Testing & Consulting
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	CO	6/9/2004	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	CO	6/30/2003	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Review conducted by c.pitters.
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	PM	7/27/2007	0.015	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Test conducted by Air Testing & Consulting.
MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	0110002	MEMORIAL REGIO HOSP/SO BROWARD HOSP DIST	SEBR	BROWARD	A	Y	3	CLEAVER BROOKS 1900/95 INCINERATOR 1550 TYPES 0-IV	A	PM	6/30/2005	0.013	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
HIGH SIERRA TERMINALING, LLC	0110034	HIGH SIERRA TERMINALING, LLC	SEBR	BROWARD	A	Y	21	BLOWING STILL #2 and #3 / Neuces Incinerator	A	PM	1/19/2005	0.6	KILOGRAMS PER MEGAGRAM OF SOLVENT FEED	Weston Solution conducted testing.
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT 2 (Acid Rain, Phase II)	A	PM	3/21/2007	0.007	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT 2 (Acid Rain, Phase II)	A	PM	10/13/2005	0.01	POUNDS PER MILLION BTU HEAT INPUT	Testing by FPL test group. Test done at 84% of maximum load.
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT 2 (Acid Rain, Phase II)	A	PM	2/22/2005	0.07	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT 2 (Acid Rain, Phase II)	A	PM	3/4/2003	0.03	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	4	FOSSIL FUEL STEAM GENERATOR, UNIT 4 (Acid Rain, Phase II)	A	PM	7/18/2006	0.019	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	4	FOSSIL FUEL STEAM GENERATOR, UNIT 4 (Acid Rain, Phase II)	A	PM	7/18/2006	0.046	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	4	FOSSIL FUEL STEAM GENERATOR, UNIT 4 (Acid Rain, Phase II)	A	PM	7/18/2006	0.019	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	4	FOSSIL FUEL STEAM GENERATOR, UNIT 4 (Acid Rain, Phase II)	A	PM	7/18/2006	0.046	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	4	FOSSIL FUEL STEAM GENERATOR, UNIT 4 (Acid Rain, Phase II)	A	PM	7/19/2005	0.077	POUNDS PER MILLION BTU HEAT INPUT	test by FPL test group
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	4	FOSSIL FUEL STEAM GENERATOR, UNIT 4 (Acid Rain, Phase II)	A	PM	7/19/2005	0.031	POUNDS PER MILLION BTU HEAT INPUT	Test by FPL test Group.
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	4	FOSSIL FUEL STEAM GENERATOR, UNIT 4 (Acid Rain, Phase II)	A	PM	5/22/2007	0.003	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	4	FOSSIL FUEL STEAM GENERATOR, UNIT 4 (Acid Rain, Phase II)	A	PM	5/22/2007	0.003	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT 2 (Acid Rain, Phase II)	A	PM	2/17/2004	0.08	POUNDS PER MILLION BTU HEAT INPUT	Test by FPL test group
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	3	FOSSIL FUEL STEAM GENERATOR, UNIT 3 (Acid Rain, Phase II)	A	PM	1/28/2003	0.06	POUNDS PER MILLION BTU HEAT INPUT	Testing by FPL test group.
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	3	FOSSIL FUEL STEAM GENERATOR, UNIT 3 (Acid Rain, Phase II)	A	PM	1/28/2003	0.1	POUNDS PER MILLION BTU HEAT INPUT	Testing by FPL test group.
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	3	FOSSIL FUEL STEAM GENERATOR, UNIT 3 (Acid Rain, Phase II)	A	PM	1/27/2004	0.03	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	3	FOSSIL FUEL STEAM GENERATOR, UNIT 3 (Acid Rain, Phase II)	A	PM	1/27/2004	0.04	POUNDS PER MILLION BTU HEAT INPUT	Test by FPL Test Group
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	3	FOSSIL FUEL STEAM GENERATOR, UNIT 3 (Acid Rain, Phase II)	A	PM	3/22/2005	0.02	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	3	FOSSIL FUEL STEAM GENERATOR, UNIT 3 (Acid Rain, Phase II)	A	PM	3/22/2005	0.05	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	3	FOSSIL FUEL STEAM GENERATOR, UNIT 3 (Acid Rain, Phase II)	A	PM	3/7/2006	0.04	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	3	FOSSIL FUEL STEAM GENERATOR, UNIT 3 (Acid Rain, Phase II)	A	PM	3/7/2006	0.06	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR, UNIT 1 (Acid Rain, Phase II)	A	PM	2/18/2003	0.06	POUNDS PER MILLION BTU HEAT INPUT	Testing by FPL test group.
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR, UNIT 1 (Acid Rain, Phase II)	A	PM	2/18/2003	0.09	POUNDS PER MILLION BTU HEAT INPUT	Testing by FPL test group.
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR, UNIT 1 (Acid Rain, Phase II)	A	PM	3/16/2004	0.05	POUNDS PER MILLION BTU HEAT INPUT	Test by FPL test group
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR, UNIT 1 (Acid Rain, Phase II)	A	PM	3/16/2004	0.08	POUNDS PER MILLION BTU HEAT INPUT	Test by FPL test group.
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR, UNIT 1 (Acid Rain, Phase II)	A	PM	3/15/2005	0.07	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR, UNIT 1 (Acid Rain, Phase II)	A	PM	3/15/2005	0.1	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR, UNIT 1 (Acid Rain, Phase II)	A	PM	3/22/2006	0.001	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR, UNIT 1 (Acid Rain, Phase II)	A	PM	3/22/2006	0.002	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	1	FOSSIL FUEL STEAM GENERATOR, UNIT 1 (Acid Rain, Phase II)	A	PM	3/14/2007	0.026	POUNDS PER MILLION BTU HEAT INPUT	
								FOSSIL FUEL STEAM					POUNDS PER	

FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	1	GENERATOR, UNIT 1 (Acid Rain, Phase II)	A	PM	3/14/2007	0.023	MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	4	FOSSIL FUEL STEAM GENERATOR, UNIT 4 (Acid Rain, Phase II)	A	PM	8/5/2003	0.09	POUNDS PER MILLION BTU HEAT INPUT	Testing by FPL Test Group.
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	4	FOSSIL FUEL STEAM GENERATOR, UNIT 4 (Acid Rain, Phase II)	A	PM	8/5/2003	0.12	POUNDS PER MILLION BTU HEAT INPUT	Testing by FPL test group.
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	4	FOSSIL FUEL STEAM GENERATOR, UNIT 4 (Acid Rain, Phase II)	A	PM	7/27/2004	0.03	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	4	FOSSIL FUEL STEAM GENERATOR, UNIT 4 (Acid Rain, Phase II)	A	PM	7/27/2004	0.06	POUNDS PER MILLION BTU HEAT INPUT	Test by FPL Test Group.
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT 2 (Acid Rain, Phase II)	A	PM	2/17/2004	0.09	POUNDS PER MILLION BTU HEAT INPUT	Test by FPl test group
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT 2 (Acid Rain, Phase II)	A	PM	3/4/2003	0.07	POUNDS PER MILLION BTU HEAT INPUT	Test by FPL test group
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT 2 (Acid Rain, Phase II)	A	PM	2/22/2005	0.09	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT 2 (Acid Rain, Phase II)	A	PM	10/13/2005	0.017	POUNDS PER MILLION BTU HEAT INPUT	Test by FPL test group. Testing done at 84% maximum load.
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	2	FOSSIL FUEL STEAM GENERATOR, UNIT 2 (Acid Rain, Phase II)	A	PM	3/21/2007	0.007	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PPE)	0110036	PORT EVERGLADES POWER PLANT	SEBR	BROWARD	A	Y	5	12 SIMPLE CYCLE GAS TURBINES, GT1 THROUGH GT12	A	NOX	9/23/2005	0.351	POUNDS PER MILLION BTU HEAT INPUT	Testing by Coastal Air Consulting with assistar from FPL.
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	38	CCCT WITH HRSG (CT 5B) (PHASE II ACID RAIN UNIT)	A	CO	10/25/2007	1.21	POUNDS/HOUR	tets done by FPL test group
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	36	CCCT WITH HRSG (CT 4B) (PHASE II ACID RAIN UNIT)	A	CO	9/16/2003	5.33	POUNDS/HOUR	Test by FPL Test Group.
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	36	CCCT WITH HRSG (CT 4B) (PHASE II ACID RAIN UNIT)	A	CO	8/24/2004	4.5	POUNDS/HOUR	Testing by FPL Test Group.
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	36	CCCT WITH HRSG (CT 4B) (PHASE II ACID RAIN UNIT)	A	CO	12/12/2005	1.74	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	36	CCCT WITH HRSG (CT 4B) (PHASE II ACID RAIN UNIT)	A	CO	8/17/2005	1.05	POUNDS/HOUR	Test by FPL test group
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	36	CCCT WITH HRSG (CT 4B) (PHASE II ACID RAIN UNIT)	A	CO	11/8/2006	1.22	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	36	CCCT WITH HRSG (CT 4B) (PHASE II ACID RAIN UNIT)	A	CO	11/15/2007	1.09	POUNDS/HOUR	Test completed by FPL test group
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	37	CCCT WITH HRSG (CT 5A) (PHASE II ACID RAIN UNIT)	A	CO	9/16/2003	5.86	POUNDS/HOUR	Test by FPL test group.
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	37	CCCT WITH HRSG (CT 5A) (PHASE II ACID RAIN UNIT)	A	CO	8/25/2004	4.35	POUNDS/HOUR	Testing by FPL Test Group.
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	37	CCCT WITH HRSG (CT 5A) (PHASE II ACID RAIN UNIT)	A	CO	1/26/2006	0.5	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	37	CCCT WITH HRSG (CT 5A) (PHASE II ACID RAIN UNIT)	A	CO	11/15/2006	0.06	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	37	CCCT WITH HRSG (CT 5A) (PHASE II ACID RAIN UNIT)	A	CO	10/24/2007	0.99	POUNDS/HOUR	Test done by FPL test group
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	35	CCCT WITH HRSG (CT 4A) (PHASE II ACID RAIN UNIT)	A	NOX	9/15/2003	183	POUNDS/HOUR	Test by FPL Test Group.
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	35	CCCT WITH HRSG (CT 4A) (PHASE II ACID RAIN UNIT)	A	NOX	8/23/2004	188	POUNDS/HOUR	Testing by FPL Test Group.
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	35	CCCT WITH HRSG (CT 4A) (PHASE II ACID RAIN UNIT)	A	NOX	12/8/2005	194	POUNDS/HOUR	Testing by FPL test group
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	35	CCCT WITH HRSG (CT 4A) (PHASE II ACID RAIN UNIT)	A	NOX	8/16/2005	184	POUNDS/HOUR	Testing by FPL test group
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	35	CCCT WITH HRSG (CT 4A) (PHASE II ACID RAIN UNIT)	A	NOX	11/7/2006	191	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	35	CCCT WITH HRSG (CT 4A) (PHASE II ACID RAIN UNIT)	A	NOX	11/14/2007	191	POUNDS/HOUR	Test done by FPL test group
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	36	CCCT WITH HRSG (CT 4B) (PHASE II ACID RAIN UNIT)	A	NOX	8/17/2005	190	POUNDS/HOUR	Test by FPL test group
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	36	CCCT WITH HRSG (CT 4B) (PHASE II ACID RAIN UNIT)	A	NOX	11/8/2006	190	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	36	CCCT WITH HRSG (CT 4B) (PHASE II ACID RAIN UNIT)	A	NOX	11/15/2007	218	POUNDS/HOUR	Test done by FPL test group
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	35	CCCT WITH HRSG (CT 4A) (PHASE II ACID RAIN UNIT)	A	CO	9/15/2003	8.18	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	35	CCCT WITH HRSG (CT 4A) (PHASE II ACID RAIN UNIT)	A	CO	8/23/2004	4.92	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	35	CCCT WITH HRSG (CT 4A) (PHASE II ACID RAIN UNIT)	A	CO	12/8/2005	1.07	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	35	CCCT WITH HRSG (CT 4A) (PHASE II ACID RAIN UNIT)	A	CO	8/16/2005	1.52	POUNDS/HOUR	Testing by FPL test group
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	35	CCCT WITH HRSG (CT 4A) (PHASE II ACID RAIN UNIT)	A	CO	11/7/2006	0.95	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	35	CCCT WITH HRSG (CT 4A) (PHASE II ACID RAIN UNIT)	A	CO	11/14/2007	1.01	POUNDS/HOUR	Test done by FPLtest group.
FLORIDA POWER &	0110037	FT. LAUDERDALE	SEBR	BROWARD	A	Y	36	CCCT WITH HRSG (CT 4B) (PHASE II ACID RAIN	A	NOX	9/16/2003	198	POUNDS/HOUR	Test by FPL Test Group.

LIGHT (PFL)		POWER PLANT						UNIT)						
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	36	CCCT WITH HRSG (CT 4B) (PHASE II ACID RAIN UNIT)	A	NOX	8/24/2004	216	POUNDS/HOUR	Testing by FPL Test Group.
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	36	CCCT WITH HRSG (CT 4B) (PHASE II ACID RAIN UNIT)	A	NOX	12/12/2005	234	POUNDS/HOUR	Test by FPL test group
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	38	CCCT WITH HRSG (CT 5B) (PHASE II ACID RAIN UNIT)	A	CO	1/27/2006	0.86	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	38	CCCT WITH HRSG (CT 5B) (PHASE II ACID RAIN UNIT)	A	CO	9/17/2003	4.93	POUNDS/HOUR	Test by FPL test group. Low test heat input resu in a new heat input limit of 1757 until next test.
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	38	CCCT WITH HRSG (CT 5B) (PHASE II ACID RAIN UNIT)	A	CO	8/24/2004	3.9	POUNDS/HOUR	Testing by FPL Test Group.
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	38	CCCT WITH HRSG (CT 5B) (PHASE II ACID RAIN UNIT)	A	CO	11/13/2006	0.7	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	15	BANK OF 12 COMBUSTION TURBINES (NO. 13 TO 24)	A	VOC	9/22/2005	0.0027	POUNDS PER MILLION BTU HEAT INPUT	Testing by Coastal Air Consulting.
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	3	BANK OF 12 COMBUSTION TURBINES (NOS. 1 TO 12)	A	VOC	9/21/2005	0.0013	POUNDS PER MILLION BTU HEAT INPUT	testing by Coastal Air Consulting
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	3	BANK OF 12 COMBUSTION TURBINES (NOS. 1 TO 12)	A	VOC	9/21/2005	0	POUNDS PER MILLION BTU HEAT INPUT	Testing by Coastal Air Consulting
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	15	BANK OF 12 COMBUSTION TURBINES (NO. 13 TO 24)	A	VOC	9/22/2005	0	POUNDS PER MILLION BTU HEAT INPUT	Testing by Coastal Air Consulting
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	37	CCCT WITH HRSG (CT 5A) (PHASE II ACID RAIN UNIT)	A	NOX	10/24/2007	205	POUNDS/HOUR	Test done by FPL test group
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	37	CCCT WITH HRSG (CT 5A) (PHASE II ACID RAIN UNIT)	A	NOX	11/15/2006	197	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	37	CCCT WITH HRSG (CT 5A) (PHASE II ACID RAIN UNIT)	A	NOX	8/25/2004	200	POUNDS/HOUR	Testing by FPL Test Group.
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	37	CCCT WITH HRSG (CT 5A) (PHASE II ACID RAIN UNIT)	A	NOX	9/16/2003	214	POUNDS/HOUR	Test by FPL test group.
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	37	CCCT WITH HRSG (CT 5A) (PHASE II ACID RAIN UNIT)	A	NOX	1/26/2006	218	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	38	CCCT WITH HRSG (CT 5B) (PHASE II ACID RAIN UNIT)	A	NOX	9/17/2003	189	POUNDS/HOUR	Test by FPL test group.
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	38	CCCT WITH HRSG (CT 5B) (PHASE II ACID RAIN UNIT)	A	NOX	8/24/2004	167	POUNDS/HOUR	Testing by FPL Test Group.
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	38	CCCT WITH HRSG (CT 5B) (PHASE II ACID RAIN UNIT)	A	NOX	1/27/2006	219	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	38	CCCT WITH HRSG (CT 5B) (PHASE II ACID RAIN UNIT)	A	NOX	11/13/2006	214	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFL)	0110037	FT. LAUDERDALE POWER PLANT	SEBR	BROWARD	A	Y	38	CCCT WITH HRSG (CT 5B) (PHASE II ACID RAIN UNIT)	A	NOX	10/25/2007	223	POUNDS/HOUR	Test done by FPL group
MARATHON PETROLEUM COMPANY LLC	0110048	SPANGLER TERMINAL	SEBR	BROWARD	A	Y	15	Loading Rack with VRU	I	VOC	1/19/2006	2.72	MILLIGRAMS PER LITER OF LIQUID LOADED	Stack testing conducted by Marathon Stack Tes group and monitored by P. Shelton, EPD/AQD.
MARATHON PETROLEUM COMPANY LLC	0110048	SPANGLER TERMINAL	SEBR	BROWARD	A	Y	23	Loading Rack with VRU & Portable VCU	A	VOC	11/6/2007	1.3	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
MARATHON PETROLEUM COMPANY LLC	0110048	SPANGLER TERMINAL	SEBR	BROWARD	A	Y	23	Loading Rack with VRU & Portable VCU	A	VOC	9/11/2007	1.97	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
MARATHON PETROLEUM COMPANY LLC	0110048	SPANGLER TERMINAL	SEBR	BROWARD	A	Y	14	Vapor Recovery System	I	VOC	2/17/2005	1.86	MILLIGRAMS PER LITER OF LIQUID LOADED	Stack testing was conducted by John Jordan Se Co., Kentucky.
MARATHON PETROLEUM COMPANY LLC	0110048	SPANGLER TERMINAL	SEBR	BROWARD	A	Y	14	Vapor Recovery System	I	VOC	2/19/2004	1.97	MILLIGRAMS PER LITER OF LIQUID LOADED	Compliance emission testing conducted by Jord Service Co., Kentucky.
MARATHON PETROLEUM COMPANY LLC	0110048	SPANGLER TERMINAL	SEBR	BROWARD	A	Y	14	Vapor Recovery System	I	VOC	2/19/2003	1.46	MILLIGRAMS PER LITER OF LIQUID LOADED	Test conducted by The John Jordan Serv., Co., Kentucky
MARATHON PETROLEUM COMPANY LLC	0110048	SPANGLER TERMINAL	SEBR	BROWARD	A	Y	15	Loading Rack with VRU	I	VOC	2/1/2007	0.35	MILLIGRAMS PER LITER OF LIQUID LOADED	Testing conducted by Marathon Petroleum Company LLC, Stack testing group.
MOTIVA ENTERPRISES LLC	0110050	MOTIVA ENTERPRISES - SOUTH	SEBR	BROWARD	A	Y	1	Loading Rack with a VRU and a Backup VCU	A	VOC	10/22/2003	32.28	MILLIGRAMS PER LITER OF LIQUID LOADED	Testing done Jordan Service Co., Kentucky
MOTIVA ENTERPRISES LLC	0110050	MOTIVA ENTERPRISES - SOUTH	SEBR	BROWARD	A	Y	1	Loading Rack with a VRU and a Backup VCU	A	VOC	10/13/2005	5.68	MILLIGRAMS PER LITER OF LIQUID LOADED	Test conducted by the Jordan Serv., Co., Kentu
MOTIVA ENTERPRISES LLC	0110050	MOTIVA ENTERPRISES - SOUTH	SEBR	BROWARD	A	Y	1	Loading Rack with a VRU and a Backup VCU	A	VOC	10/25/2006	0.47	MILLIGRAMS PER LITER OF LIQUID LOADED	Stack testing conducted by Jordan Technologie Inc., Kentucky
MOTIVA ENTERPRISES LLC	0110050	MOTIVA ENTERPRISES - SOUTH	SEBR	BROWARD	A	Y	1	Loading Rack with a VRU and a Backup VCU	A	VOC	10/26/2006	2.1	MILLIGRAMS PER LITER OF LIQUID LOADED	Stack testing conducted Jordan Technologies, I Kentucky
MOTIVA ENTERPRISES LLC	0110050	MOTIVA ENTERPRISES - SOUTH	SEBR	BROWARD	A	Y	1	Loading Rack with a VRU and a Backup VCU	A	VOC	10/12/2005	12.23	MILLIGRAMS PER LITER OF LIQUID LOADED	Test conducted by the Jordan Serv., Co., Kentu
MOTIVA ENTERPRISES LLC	0110050	MOTIVA ENTERPRISES - SOUTH	SEBR	BROWARD	A	Y	1	Loading Rack with a VRU and a Backup VCU	A	VOC	10/20/2004	2.52	MILLIGRAMS PER LITER OF LIQUID LOADED	The compliance emission testing was condlucte Jordan Service Co., Kentucky.
MOTIVA		MOTIVA						Loading Rack with a VRU					MILLIGRAMS PER LITER OF	Testing conducted by The Jordan Service Co.,

ENTERPRISES LLC	0110050	ENTERPRISES - SOUTH	SEBR	BROWARD	A	Y	1	and a Backup VCU	A	VOC	10/23/2003	3.53	LIQUID LOADED	Kentucky
MOTIVA ENTERPRISES LLC	0110050	MOTIVA ENTERPRISES - SOUTH	SEBR	BROWARD	A	Y	1	Loading Rack with a VRU and a Backup VCU	A	VOC	10/19/2004	34.06	MILLIGRAMS PER LITER OF LIQUID LOADED	Compliance emission testing conducted Jordan Service Co., Kentucky.
BP PRODUCTS NORTH AMERICA, INC.	0110051	BP PRODUCTS - PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	1	Petroleum Loading Rack with two VRUs	A	VOC	10/8/2003	0.2	MILLIGRAMS PER LITER OF LIQUID LOADED	Testing conducted by John Jordan Serv., Co., Kentucky
BP PRODUCTS NORTH AMERICA, INC.	0110051	BP PRODUCTS - PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	1	Petroleum Loading Rack with two VRUs	A	VOC	11/4/2004	1.8	MILLIGRAMS PER LITER OF LIQUID LOADED	Compliance emission testing conducted by Jorc Service Co., Kentucky.
BP PRODUCTS NORTH AMERICA, INC.	0110051	BP PRODUCTS - PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	1	Petroleum Loading Rack with two VRUs	A	VOC	12/7/2005	8.91	MILLIGRAMS PER LITER OF LIQUID LOADED	Stack testing conducted by Jordan Service Co., Kentucky.
BP PRODUCTS NORTH AMERICA, INC.	0110051	BP PRODUCTS - PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	1	Petroleum Loading Rack with two VRUs	A	VOC	11/16/2006	0.45	MILLIGRAMS PER LITER OF LIQUID LOADED	Stack testing conducted by Jordan Technologie Inc., Kentucky
BP PRODUCTS NORTH AMERICA, INC.	0110051	BP PRODUCTS - PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	1	Petroleum Loading Rack with two VRUs	A	VOC	11/15/2006	0.26	MILLIGRAMS PER LITER OF LIQUID LOADED	Stack testing conducted Jordan Technologies Ir Kentucky
BP PRODUCTS NORTH AMERICA, INC.	0110051	BP PRODUCTS - PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	1	Petroleum Loading Rack with two VRUs	A	VOC	12/6/2005	0.47	MILLIGRAMS PER LITER OF LIQUID LOADED	Stack testing conducted by Jordan Service Co., Kentucky.
BP PRODUCTS NORTH AMERICA, INC.	0110051	BP PRODUCTS - PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	1	Petroleum Loading Rack with two VRUs	A	VOC	11/3/2004	1.3	MILLIGRAMS PER LITER OF LIQUID LOADED	Compliance emission testing conducted by Jorc Service Co., Kentucky.
BP PRODUCTS NORTH AMERICA, INC.	0110051	BP PRODUCTS - PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	1	Petroleum Loading Rack with two VRUs	A	VOC	10/9/2003	9.6	MILLIGRAMS PER LITER OF LIQUID LOADED	Testing conducted by The Jordan Serv., Co., Kentucky
TRANSMONTAIGNE PRODUCT SERVICES INC.	0110053	TRANSMONTAIGNE - PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	1	Petroleum liquid loading rack with a VCU and backup unit	A	VOC	7/14/2003	1.37	MILLIGRAMS PER LITER OF LIQUID LOADED	
TRANSMONTAIGNE PRODUCT SERVICES INC.	0110053	TRANSMONTAIGNE - PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	1	Petroleum liquid loading rack with a VCU and backup unit	A	VOC	7/31/2006	3.81	MILLIGRAMS PER LITER OF LIQUID LOADED	Emission testing monitored by P. Shelton, EPD/AQD.
TRANSMONTAIGNE PRODUCT SERVICES INC.	0110053	TRANSMONTAIGNE - PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	1	Petroleum liquid loading rack with a VCU and backup unit	A	VOC	6/29/2004	9.18	MILLIGRAMS PER LITER OF LIQUID LOADED	
TRANSMONTAIGNE PRODUCT SERVICES INC.	0110053	TRANSMONTAIGNE - PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	1	Petroleum liquid loading rack with a VCU and backup unit	A	VOC	7/26/2005	5.63	MILLIGRAMS PER LITER OF LIQUID LOADED	
EXXONMOBIL OIL CORPORATION	0110059	EXXONMOBIL PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	13	Distillate Loading Rack with VCU	A	VOC	10/16/2003	11	MILLIGRAMS PER LITER OF LIQUID LOADED	Compliance testing conducted by Jordan Serv., Kentucky
EXXONMOBIL OIL CORPORATION	0110059	EXXONMOBIL PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	13	Distillate Loading Rack with VCU	A	VOC	10/12/2004	26.35	MILLIGRAMS PER LITER OF LIQUID LOADED	Compliance emission testing was conducted by Jordan Service Co., Kentucky.
EXXONMOBIL OIL CORPORATION	0110059	EXXONMOBIL PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	12	Gasoline Loading Racks with 2 VRU	A	VOC	10/14/2003	3.57	MILLIGRAMS PER LITER OF LIQUID LOADED	Compliance testing conducted by Jordan Servs, Kentucky for VRU # A
EXXONMOBIL OIL CORPORATION	0110059	EXXONMOBIL PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	12	Gasoline Loading Racks with 2 VRU	A	VOC	10/16/2003	11	MILLIGRAMS PER LITER OF LIQUID LOADED	Compliance testing conducted by Jordan Serv., Kentucky
EXXONMOBIL OIL CORPORATION	0110059	EXXONMOBIL PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	12	Gasoline Loading Racks with 2 VRU	A	VOC	10/15/2003	6.36	MILLIGRAMS PER LITER OF LIQUID LOADED	Compliance testing conducted by Jordan SERV Co., Kentucky
EXXONMOBIL OIL CORPORATION	0110059	EXXONMOBIL PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	12	Gasoline Loading Racks with 2 VRU	A	VOC	10/6/2004	0.83	MILLIGRAMS PER LITER OF LIQUID LOADED	Compliance emission testing for the VRU # B v conducted by Jordan Service Co., Kentucky.
EXXONMOBIL OIL CORPORATION	0110059	EXXONMOBIL PORT EVERGLADES TERMINAL	SEBR	BROWARD	A	Y	12	Gasoline Loading Racks with 2 VRU	A	VOC	10/7/2004	1.09	MILLIGRAMS PER LITER OF LIQUID LOADED	Compliance emission testing for the VRU # A v conducted by Jordan Service Co., Kentucky.
COASTAL TERMINALS, LLC	0110069	COASTAL - PORT EVERGLADES	SEBR	BROWARD	A	Y	30	Marine Loading/Unloading and Vessel Bunkering with Gas. VRU	A	VOC	7/29/2003	1.02	MILLIGRAMS PER LITER OF LIQUID LOADED	
COASTAL TERMINALS, LLC	0110069	COASTAL - PORT EVERGLADES	SEBR	BROWARD	A	Y	31	Gasoline Loading Rack (3 lanes) with Vapor Recovery Unit	A	VOC	7/30/2007	3.31	MILLIGRAMS PER LITER OF LIQUID LOADED	
COASTAL TERMINALS, LLC	0110069	COASTAL - PORT EVERGLADES	SEBR	BROWARD	A	Y	31	Gasoline Loading Rack (3 lanes) with Vapor Recovery Unit	A	VOC	7/28/2006	5.46	MILLIGRAMS PER LITER OF LIQUID LOADED	Stack testing was monitored by P. Shelton, EPD/AQD.
COASTAL TERMINALS, LLC	0110069	COASTAL - PORT EVERGLADES	SEBR	BROWARD	A	Y	30	Marine Loading/Unloading and Vessel Bunkering with Gas. VRU	A	VOC	12/1/2004	2.34	MILLIGRAMS PER LITER OF LIQUID LOADED	
COASTAL TERMINALS, LLC	0110069	COASTAL - PORT EVERGLADES	SEBR	BROWARD	A	Y	31	Gasoline Loading Rack (3 lanes) with Vapor Recovery Unit	A	VOC	7/22/2005	3.33	MILLIGRAMS PER LITER OF LIQUID LOADED	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	PM	11/9/2004	0.008	GRAINS PER DRY STANDARD CUBIC FOOT	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	H027	11/8/2005	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	H027	10/13/2004	0.01	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test conducted by Air Testing & Consulting
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	H027	11/9/2004	0.01	MILLIGRAMS PER DRY STANDARD CUBIC METER	

													@ 7% O2	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	H114	11/8/2005	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	H114	10/13/2004	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	H114	11/9/2004	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	NOX	11/8/2005	55	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	NOX	11/9/2004	70	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing & Consulting
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	NOX	11/9/2004	70	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	PM	10/26/2006	0.012	GRAINS PER DRY STANDARD CUBIC FOOT	Testing conducted by Air Testing & Consulting
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	PM	10/17/2007	0.009	GRAINS PER DRY STANDARD CUBIC FOOT	Air Testing & Consulting conducted the testing
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	PM	11/8/2005	0.012	GRAINS PER DRY STANDARD CUBIC FOOT	next test date depends on pass/fail of previous t (see permit)
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	PM	10/13/2004	0.008	GRAINS PER DRY STANDARD CUBIC FOOT	Testing conducted by Air Testing & Consulting
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	CO	10/17/2007	3	PARTS PER MILLION DRY GAS VOLUME	Testing conducted by ATC.
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	H106	10/17/2007	2	PARTS PER MILLION DRY GAS VOLUME	Testing conducted by ATC
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	H106	11/8/2005	1	PARTS PER MILLION DRY GAS VOLUME	next test date depends on pass/fail of previous t (see permit)
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	SO2	11/9/2004	2	PARTS PER MILLION DRY GAS VOLUME	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	SO2	11/9/2004	2	PARTS PER MILLION DRY GAS VOLUME	Test conducted by Air Testing & Consulting
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	SO2	11/8/2005	1	PARTS PER MILLION DRY GAS VOLUME	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	H106	11/9/2004	1	PARTS PER MILLION DRY GAS VOLUME	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	H106	10/13/2004	1	PARTS PER MILLION DRY GAS VOLUME	Test conducted by Air Testing & Consulting
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	H106	10/26/2006	2	PARTS PER MILLION DRY GAS VOLUME	Testing conducted by Air Testing & Consulting
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	CO	11/9/2004	3	PARTS PER MILLION DRY GAS VOLUME	Review conducted by c.pitters.
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	CO	10/26/2006	9	PARTS PER MILLION DRY GAS VOLUME	Testing conducted by Air Testing & Consulting
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	CO	11/8/2005	1	PARTS PER MILLION DRY GAS VOLUME	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	CO	10/13/2004	3	PARTS PER MILLION DRY GAS VOLUME	Test conducted by Air Testing & Consulting
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	PB	11/9/2004	0.15	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	PB	10/13/2004	0.15	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test conducted by Air Testing & Consulting
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	DIOX	11/9/2004	0.6	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test conducted by Air Testing & Consulting
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	DIOX	11/9/2004	0.6	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	DIOX	11/8/2005	1.3	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HOLY CROSS HOSPITAL	0111019	HOLY CROSS HOSPITAL	SEBR	BROWARD	A	Y	2	1300 LB/HR WASTE INCIN FUELED-NATURED GAS (NEW) MODEL 1300 A	A	PB	11/8/2005	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
WASTE MANAGEMENT INC. OF FLORIDA	0112094	CENTRAL DISPOSAL	SEBR	BROWARD	A	Y	11	LFGCS, Treatment system, 2 enclosed flares, 1 open flare	A	NMOC	4/12/2006	0.093	PARTS PER MILLION DRY GAS VOLUME AS HEXANE @ 3% O2	
													PARTS PER	

WASTE MANAGEMENT INC. OF FLORIDA	0112094	CENTRAL DISPOSAL	SEBR	BROWARD	A	Y	8	Turbines (3), Gas Collection, Desulfurization System, Flare	I	SO2	4/3/2003	3.61	MILLION DRY GAS VOLUME @ 15% O2	
WASTE MANAGEMENT INC. OF FLORIDA	0112094	CENTRAL DISPOSAL	SEBR	BROWARD	A	Y	8	Turbines (3), Gas Collection, Desulfurization System, Flare	I	SO2	3/19/2004	8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
WASTE MANAGEMENT INC. OF FLORIDA	0112094	CENTRAL DISPOSAL	SEBR	BROWARD	A	Y	10	Small Gas Fired Turbines (3) & Open Flare	A	NOX	4/13/2006	25.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
WASTE MANAGEMENT INC. OF FLORIDA	0112094	CENTRAL DISPOSAL	SEBR	BROWARD	A	Y	8	Turbines (3), Gas Collection, Desulfurization System, Flare	I	NOX	4/3/2003	102.5	PARTS PER MILLION DRY GAS VOLUME	
WASTE MANAGEMENT INC. OF FLORIDA	0112094	CENTRAL DISPOSAL	SEBR	BROWARD	A	Y	8	Turbines (3), Gas Collection, Desulfurization System, Flare	I	NOX	3/19/2004	89.63	PARTS PER MILLION DRY GAS VOLUME	
WASTE MANAGEMENT INC. OF FLORIDA	0112094	CENTRAL DISPOSAL	SEBR	BROWARD	A	Y	8	Turbines (3), Gas Collection, Desulfurization System, Flare	I	CO	3/19/2004	15.4	TONS/YEAR	
WASTE MANAGEMENT INC. OF FLORIDA	0112094	CENTRAL DISPOSAL	SEBR	BROWARD	A	Y	8	Turbines (3), Gas Collection, Desulfurization System, Flare	I	VOC	4/3/2003	3	TONS/YEAR	
WASTE MANAGEMENT INC. OF FLORIDA	0112094	CENTRAL DISPOSAL	SEBR	BROWARD	A	Y	8	Turbines (3), Gas Collection, Desulfurization System, Flare	I	VOC	3/19/2004	4	TONS/YEAR	
WASTE MANAGEMENT INC. OF FLORIDA	0112094	CENTRAL DISPOSAL	SEBR	BROWARD	A	Y	8	Turbines (3), Gas Collection, Desulfurization System, Flare	I	CO	4/3/2003	37.6	TONS/YEAR	
SUN CHEMICAL	0112103	SUN GRAPHIC, INC.	SEBR	BROWARD	I	Y	17	mixers,churns,spreaders, ovens, grinders,SRS, cutting/gluing	I	VOC	10/6/2004	99.79	PERCENT REDUCTION IN EMISSIONS	Testing by Arlington Environmental
SUN CHEMICAL	0112103	SUN GRAPHIC, INC.	SEBR	BROWARD	I	Y	17	mixers,churns,spreaders, ovens, grinders,SRS, cutting/gluing	I	VOC	9/1/2005	98.17	PERCENT REDUCTION IN EMISSIONS	testing by Arlington Environmental
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H114	3/24/2003	34	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/13/2007	98.8	PERCENT REDUCTION IN EMISSIONS	RN (Inlet= 534 ppmdv@7% O2 vs Outlet =6.3 ppmvd@7%O2)
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/16/2005	98	PERCENT REDUCTION IN EMISSIONS	RN: run #1 inlet failed a leak check and was no inluded into comptn of % reduction.
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/24/2003	99	PERCENT REDUCTION IN EMISSIONS	RN; HCL=4.3 ppmvd@7%O2(outlet)
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/16/2006	99.6	PERCENT REDUCTION IN EMISSIONS	RN: modfd 26A method was used on INLET.
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/11/2004	99	PERCENT REDUCTION IN EMISSIONS	RN- 2004 tst;Inlet HCL=518ppmdv @7% O2 v ppmvd @ 7%O2
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	6/3/2003	69	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN- 2nd qtr, 2003 hg test; Hg=0.019#/hr= 0.000062#/mmbtu/The allowable units were corrected to "Micro" from "Nano"
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H106	3/25/2003	96	PERCENT REDUCTION IN EMISSIONS	RN HCL=21mg/dscf@7%O2
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H106	3/10/2004	99	PERCENT REDUCTION IN EMISSIONS	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H106	3/15/2005	99	PERCENT REDUCTION IN EMISSIONS	RN, see HCL test in ppmvd at the same day.
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H106	3/14/2006	98.7	PERCENT REDUCTION IN EMISSIONS	RN: mdfd mtd 26 A used on inlet . cmlnce with ppm.
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H106	3/14/2007	99.4	PERCENT REDUCTION IN EMISSIONS	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	3/25/2003	17	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/26/2003	99	PERCENT REDUCTION IN EMISSIONS	RN- HCL=2.9ppmvd @7%O2
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/17/2005	99	PERCENT REDUCTION IN EMISSIONS	RN: ppmvd@7%O2 and % removal were dtrmi
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/15/2007	98.6	PERCENT REDUCTION IN EMISSIONS	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/9/2004	99	PERCENT REDUCTION IN EMISSIONS	RN: HCL=688 ppmvd@7%O2 vs 3.9
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/15/2006	99	PERCENT REDUCTION IN EMISSIONS	RN: note that modified mth 26 A used on inlet wrtn apprvl) but they comply with ppm limit.
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	3/24/2003	17	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	FL	3/13/2007	0.00061	POUNDS PER MILLION BTU HEAT INPUT	RN: FL=0.19# /hr
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	FL	3/10/2004	0.00036	POUNDS PER MILLION BTU HEAT INPUT	RN: 2004 stack test.
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	FL	3/15/2007	0.00083	POUNDS PER MILLION BTU HEAT INPUT	RN: FL=0.28#/hr
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	FL	3/15/2005	0.00011	POUNDS PER MILLION BTU HEAT INPUT	RN: HF=0.040#/hr; T ilet bghse=312F
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	FL	3/26/2003	0.00054	POUNDS PER MILLION BTU HEAT INPUT	RN
WHEELABRATOR		WHEELABRATOR						863 TPD MSW Combustor					POUNDS PER	

SOUTH BROWARD, INC	0112119	SOUTH BROWARD	SED	BROWARD	A	Y	3	& Auxiliary Burners-Unit 3	A	FL	3/16/2006	0.000092	MILLION BTU HEAT INPUT	RN; HF= <0.025#/hr
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	FL	3/11/2004	0.00029	POUNDS PER MILLION BTU HEAT INPUT	RN; FL=0.092#/hr
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	FL	3/26/2003	0.00059	POUNDS PER MILLION BTU HEAT INPUT	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	FL	3/17/2005	0.00011	POUNDS PER MILLION BTU HEAT INPUT	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	FL	3/13/2007	0.00048	POUNDS PER MILLION BTU HEAT INPUT	RN: FL=0.15#/hr
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	FL	3/11/2004	0.00033	POUNDS PER MILLION BTU HEAT INPUT	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	FL	3/14/2006	0.000079	POUNDS PER MILLION BTU HEAT INPUT	RN: HF=<0.026#/hr
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	FL	3/27/2003	0.00064	POUNDS PER MILLION BTU HEAT INPUT	RN; FL=0.22#/hr
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	FL	3/14/2006	0.000079	POUNDS PER MILLION BTU HEAT INPUT	RN: HF= <0.026#/hr
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	FL	3/15/2005	0.00012	POUNDS PER MILLION BTU HEAT INPUT	RN: Fl=0.039#/hr
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H106	3/25/2003	21	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN- see tst screen for %red eff.
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H106	3/15/2005	6.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: Run 1 PM/HCL glass liner broken, Failed check?,An average of the 2, 3, and 4th runs are
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H106	3/10/2004	4.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H106	3/14/2007	3.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/11/2004	7.7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: 2004 stack tst
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/16/2006	2.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: Fab flt inlt T=312 F
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/24/2003	4.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN-2003 tsts, see screen for % rdctn tst.
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/16/2005	12.33	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: Fabric inlet T= 320 F
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	PB	3/13/2007	0.0032	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	PB	3/14/2006	0.014	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	PB	3/15/2005	0.013	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	PB	3/24/2003	0.0086	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	PB	3/9/2004	0.00086	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PB	3/13/2007	0.00004	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PB	3/15/2006	0.033	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PB	3/15/2005	0.0013	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PB	3/9/2004	0.0035	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PB	3/24/2003	0.0027	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H021	3/13/2007	0.000029	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H021	3/14/2006	0.000028	MILLIGRAMS PER DRY STANDARD CUBIC METER	RN

													@ 7% O2	
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H021	3/15/2005	0.000027	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Be is below 0.000027
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H021	3/9/2004	0.00003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H021	3/24/2003	0.00003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/13/2007	6.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/15/2006	6.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H027	3/13/2007	0.000064	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H027	3/15/2006	0.0026	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H027	3/15/2005	0.0011	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H027	3/9/2004	0.00037	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H027	3/24/2003	0.00017	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H027	3/14/2006	0.00026	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H027	3/16/2005	0.0097	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H027	3/10/2004	0.0003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H027	3/25/2003	0.00009	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	8/28/2007	0.013	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: =0.0041#/hr; SDA Outlet T=310F. (about tons processed). This is an average of 2nd, 3rd 4th runs. Run #1 failed a leak check during witi the test.
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	3/14/2007	0.018	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	3/14/2006	0.014	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	4/14/2005	0.014	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	3/16/2005	0.0833	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: SG wtnsd retest on3/17/05 and failed with larger number of 0.363milgr per dscm@7%O2; case.
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H021	3/13/2007	0.000028	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H021	3/15/2006	0.000031	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H021	3/15/2005	0.000027	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; Be< 0.000027mg@7% O2; NOTE run 1 w not used in the avrgng for all METALS (only fi data prvdd). Reason malfunction was not discvi run was done (slurry flow reduction-pump, NE CHECK IF THE NOTIFICATION WAS SENT THE OFFICE).
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H021	3/9/2004	0.00003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H021	3/24/2003	0.00003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR													MILLIGRAMS PER DRY	

SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H027	3/14/2007	0.00058	STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	6/14/2005	0.03	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=0.0094#/hr;SDA outlet T=304F.
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	6/15/2004	0.0085	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: 2nd qtr, 2004 Hg tst; Hg=9.8E-06#/MMB Hg=0.0032#/hr
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	3/10/2004	0.021	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PM	3/13/2007	2	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM=<0.58#/hr =0.0018#/MMBTU
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PM	3/15/2006	5.9	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM=1.8 #/hr; PM=0.0053#/MMBTU
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PM	3/16/2005	0.95	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	rN: PM=<0.28#/hr;=< 0.00085#/MMBTU; T ir bghse=320F.
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PM	3/9/2004	0.63	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; PM=0.19#/hr;= 0.00056#/MMBTU
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PM	3/24/2003	0.52	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM<0.16#?hr;<0.00047#/mmbtu and PM< mg/dscf@7%O2
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/9/2004	3.9	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN;
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/15/2007	7.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: T fab. flt=320F
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/17/2005	7.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/26/2003	2.9	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN-see %redctn screen test.
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H106	3/14/2006	8.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	8/28/2003	0.022	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN-3rd QTR, 2003
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	3/9/2004	0.013	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	3/15/2005	0.02	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	8/26/2004	0.032	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN-3rd qtr, 2004 test.St.T=300F; Hg=0.0099#/ =2.9E-05#/MMBTU
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	3/15/2006	0.055	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	6/15/2006	0.004	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg= 0.0015# /hr
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	6/7/2007	0.014	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=0.0041#/hr; SDA T=315F
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PM	3/11/2004	0.57	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN- 2004 test ; PM=0.18#/hr;=0.00051#/MMB
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PM	3/16/2006	1.5	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM=0.44 #/hr; PM=0.0014#/MMBTU
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	DIOX	3/10/2004	3	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; Dioxin=1.6E-08 #/hr; =4.9E-11#/MMBTU
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	DIOX	3/15/2006	3	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F=8.2E-07#/hr;D/F= 2.4E-11#/MMBTU inlet filter T=320 F drng the test.
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	DIOX	3/14/2007	0.87	NANOGRAMS PER DRY STANDARD CUBIC METER	RN D/F= 2.7E07 #/hr ;D/F =7.8E-10#/MMBTU Audit Samples?

													@ 7% O2	
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H114	3/13/2007	0.018	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H114	8/29/2006	0.04	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; SDA T=310F; Hg=1.3E-02 #/hr
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H114	12/13/2005	0.013	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=0.0041#/hr =1.2E-05 #/mmbtu; T sda = 298F
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H114	3/14/2006	0.017	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H114	12/7/2004	0.012	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: 4th QTR, 2004. Hg=0.0039#/hr,= 0.00001 #/mmbtu
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H114	3/15/2005	0.0084	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H114	3/9/2004	0.0078	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H114	12/9/2003	0.029	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN-4th QTR, 2003;Hg= 0.0066 #/hr
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PM	3/15/2007	0.78	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM <0.78 mg/dscf; PM= <0.23#/hr;<0.00070#/mmbtu; fab. flt inlet T =3
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H027	3/9/2004	0.00032	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PB	3/14/2007	0.0058	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PB	3/14/2006	0.00092	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PB	3/16/2005	0.008	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PB	3/10/2004	0.0034	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PB	3/25/2003	0.00033	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H021	3/14/2007	0.000028	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: BE <0.000028
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H021	3/14/2006	0.00003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H021	3/16/2005	0.000029	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	DIOX	3/16/2006	14	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F=4.2E-06 #/hr;D/F=1.3E-08#/MMBTU of inlet Fltr=320 F during the test.
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	DIOX	3/16/2007	1.2	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F= 3.6E-07 #/hr ; =1.1E-09#/mmbtu D/I Audit Samples?
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	DIOX	3/25/2003	1.8	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN-Steam Rate=184.8Klb/hr; every year dfrnt tstsd for D/F,dpng on the result. (prmt cndtn).
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	DIOX	3/14/2006	1	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F=2.8E-07#/hr;D/F= 9.2E-10#/MMBTU inlet flt=320 F(limit for this year).
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	DIOX	3/13/2007	4	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F= 1.2E-06#/hr ;D/F=3.6E-09#/MMBTU inlet fab fltr=320F
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H027	3/13/2007	0.00024	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
													MILLIGRAMS	

WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H027	3/14/2006	0.015	PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H027	3/15/2005	0.0013	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H027	3/24/2003	0.00049	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	DIOX	3/17/2005	17.3	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Dioxin/Furan= 5.4 E-06 #/hr ;= 1.6E08#/MMBTU;SDA outlet T=320F
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H021	3/10/2004	0.00003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H021	3/25/2003	0.00003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	PM	3/14/2007	0.77	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM<0.22#/hr and < 0.00069 #/MMBTU
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	PM	3/14/2006	7.3	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; PM= 2.1#/hr;PM=0.0066#/MMBTU
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	PM	3/15/2005	3.7	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM= 1.2 #/hr = 0.0034#/MMBTU
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	PM	3/10/2004	0.57	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM= 0.17#/hr=0.00051#/mmbtu
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	PM	3/25/2003	0.54	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; PM,0.52mg/dscf@7%O2; PM<0.16#/hr ar <0.00048#/MMBTU
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	3	863 TPD MSW Combustor & Auxiliary Burners-Unit 3	A	H114	12/6/2007	0.008	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=8.8micrg/dscm@7%O2; Hg= 2.8E-03#/hr=7.9E-06#/MMBTU;T SDAout=315F
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PM	3/17/2005	1.3	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM=0.40#/hr;=0/0012#/mmbtu
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	1	863 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PM	3/26/2003	0.49	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM<0.49mg/dscf@7%O2;PM<0.15#/hr ar <0.00044#/MMNTU;
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	3/13/2007	0.015	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR SOUTH BROWARD, INC	0112119	WHEELABRATOR SOUTH BROWARD	SED	BROWARD	A	Y	2	863 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	9/22/2005	0.0073	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: 3rd qtr, 2005. Hg=0.0020#/hr=6.53E-06#/mmbtu
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	3/20/2006	0.041	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	rN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	6/13/2006	0.011	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: T= 325 F; rvsd rprt with a summary was submitted on9/11/06 after my rqst ;orgnl data submtd on 7/31/06
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	6/14/2006	0.036	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=1.3E-02@/hr ; This is a second set of t runs,need to ask what was wrong with the FIRS SET of three runs.
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	6/5/2007	0.0086	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=0.0028#/hr ;SDA outlet T=320F (dura of each run-2hrs)
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	6/17/2004	0.0061	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:2nd QTR, 2004 , Hg test. Hg=5.5E-06#/mr
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	3/19/2003	0.013	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; mtd 29 used.
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	6/5/2003	0.019	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN- 2nd qtr, 2003. Hg=0.00055#/hr; =0.0000017#/mmbtu
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	3/15/2004	0.006	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR NORTH BROWARD,	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PM	3/21/2007	0.69	MILLIGRAMS PER DRY STANDARD	RN; PM=,0.21#/HR,< 0.00062#/MMBTU

INC.													CUBIC METER @ 7% O2	
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PM	3/21/2006	2.2	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM=0.68#/hr; PM =0.0020 # /MMBTU
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PM	3/21/2005	0.56	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN PM< 0.56 mg/dscm@7%O2=< 0.17#/hr=<0.00050#/MMBTU
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PM	3/18/2003	0.63	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN- PM<0.63 mg/dscf@7%;PM<0.20#/hr;PM<0.00057#/MM
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PM	3/15/2004	1.5	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM=0.44#/hr =0.0013#/MMBTU
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	DIOX	3/15/2004	7.7	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: dioxin/furan=2.3E-06#/hr=6.9E-09#/MME T= 315F (max).
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	DIOX	3/20/2007	4.8	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F= 1.5E-06#/hr;=4.3E-09#/MMBTU
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	8/30/2007	0.016	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: 3rd Qtr, 2007 ; Hg=0.0049#/hr ;SDA outle T=320F; about 72/hr tons drng the test.
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	11/14/2006	0.055	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=1.7E-03 #/hr; SDA T outlet=320 F
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	3/19/2007	0.011	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN (all metals have about twice more flow at tl test).
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	12/15/2005	0.016	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: 4th qtr, 2005; Hg= 0.0050#/hr; SDA outlet =325F
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	3/21/2006	0.0078	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H114	3/21/2005	0.0074	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PM	3/20/2003	0.54	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN- THE RESULT WAS BELOW MIN DETECTBLE LIMIT FOR MTHD 5 (<0.54) ; PM<0.16 # / HR ;PM< 0.00048#/MMBTU; the testing believes that the baghouse was oprtd on optimum ;T=320 F(inlet)
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	DIOX	3/21/2005	1.9	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F=6.3E-07#/hr=1.7E-09#/MMBTU
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	DIOX	3/19/2003	0.71	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN-2003 test;Fabric Filt T=320
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	DIOX	3/21/2006	6.8	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F= 2.0E-06 #/hr; D/F= 6.1E-09#/MMBT (Fd); T inlet max = 322 F
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PM	3/22/2006	8.9	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: 2006 test; PM=2.7#/hr
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PM	3/19/2007	0.68	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM= <0.00061#/MMBTU; PM<0.21#/hr
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PM	3/23/2005	0.67	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; PM=<0.21#/hr;PM=<0.00060#/mmbtu
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PM	3/16/2004	1.1	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM=0.31#/hr,=0.00096#/MMBTU
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	3/20/2007	0.017	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/19/2005	97.2	PERCENT REDUCTION IN EMISSIONS	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/23/2005	99	PERCENT REDUCTION IN EMISSIONS	RN: % removal (reduction efficiency).
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/16/2004	99	PERCENT REDUCTION IN EMISSIONS	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/20/2003	98	PERCENT REDUCTION IN EMISSIONS	RN-PM/HCL was condtd simultnsly with mtd 5 (back half analss;Outlet HCL=8.5ppmvd@7%(
WHEELABRATOR NORTH BROWARD,	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/22/2006	98	PERCENT REDUCTION IN	RN

INC.													EMISSIONS	
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/20/2003	8.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:ppmvd and reduction eff were conducted ir 2003. Outlet T=304 F
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/23/2005	6.9	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/16/2004	7.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H106	3/17/2004	14.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: T=279F(av)
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H106	3/19/2003	25	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN-2003 tst, Also see screen for allw seq. 2(% reduction coeff).
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/21/2007	13	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/21/2006	5.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/21/2005	6.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/15/2004	23	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN; T==297F(av)
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/18/2003	17	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN- see screen for Allw Sequence 2 (coef. redc
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/22/2006	11	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H106	3/19/2007	15	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: (audit sample one of two fail)
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H027	3/19/2003	0.00032	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	PB	3/19/2007	0.000096	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	PB	3/20/2006	0.0017	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	PB	3/21/2005	0.0019	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	PB	3/17/2004	0.017	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	PB	3/18/2003	0.0017	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H106	3/20/2007	8.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H106	3/20/2006	9.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H106	3/22/2005	12	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	3/22/2005	0.011	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	6/16/2005	0.03	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=0.0090#/hr;=0.000027#/MMBTU (Fd base)
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	8/24/2004	0.012	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN- 3rd QTR, 2004; Hg= 0.0038#/hr
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	8/26/2003	0.011	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN-3rd QTR, 2003
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	3/16/2004	0.011	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H114	3/19/2003	0.018	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; mtd 29 was used. Fliter fabric inlet T=318

WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H114	12/4/2007	0.0048	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg= 1.5 E-03 #/hr ;Hg=4.3E-06 #/MMBT of the SDA outlet=320 F
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H114	3/19/2007	0.01	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H114	9/20/2005	0.006	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=1.9E-03#/hr=5.3E-06#/mmbtu.
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H114	8/31/2006	0.011	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg= 3.2 E-03#/hr
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H114	3/20/2006	0.0061	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H114	12/9/2004	0.0031	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: 4 th QTR, 2004. Mercury+ 0.00093#/hr;=0.0000028#/mmbtu.
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H114	3/21/2005	0.0085	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H114	3/17/2004	0.017	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H114	12/11/2003	0.021	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: 2003 Hg test;Hg=0.0058#/hr;=1.8E-05 #/ MMBTU
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H114	3/18/2003	19	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H027	3/19/2007	0.000096	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H027	3/20/2006	0.00025	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H027	3/21/2005	0.00029	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H027	3/17/2004	0.0018	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H027	3/18/2003	0.0014	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H021	3/19/2007	0.000024	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H021	3/20/2006	0.000029	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H021	3/21/2005	0.000027	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Be< 0.000027
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H021	3/17/2004	0.000029	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H021	3/18/2003	0.00003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PB	3/22/2005	0.0016	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PB	3/16/2004	0.011	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PB	3/19/2003	0.0037	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H021	3/20/2007	0.000025	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR		WHEELABRATOR						807 TPD MSW Combustor					MILLIGRAMS PER DRY	

NORTH BROWARD, INC.	0112120	NORTH BROWARD	SED	BROWARD	A	Y	2	& Auxiliary Burners- Unit 2	A	H021	3/20/2006	0.000028	STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H021	3/22/2005	0.000026	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: 2005 tst.
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H021	3/16/2004	0.00003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H021	3/19/2003	0.00003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN- Be<0.000030 mg/dscf@ 7%O2
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H027	3/19/2007	0.00012	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PB	3/21/2005	0.0029	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H021	3/19/2003	0.00003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN-Be<0.000030 mg / dscf @7%O2
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H021	3/15/2004	0.00003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	PM	3/20/2007	1.1	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: P=0.33#/HR; =0.00095#/MMBTU
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	PM	3/20/2006	1.6	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM=0.48#/Hr; PM=0.0014#/MMBTU
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	PM	3/22/2005	0.62	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM<0.62 mg/dscm@7%O2=< 0.19#/hr;= 0.00055#/MMBTU
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	PM	3/17/2004	2.98	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN;PM=0.91#/hr=0.00267#/MMBTU
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	PM	3/19/2003	0.68	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM<0.68mg/dscf@7%O2;PM<0.20#/hr a <0.00061#/MMbtu
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PB	3/20/2007	0.0012	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	PB	3/20/2006	0.0077	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H021	3/19/2007	0.000026	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H021	3/21/2006	0.000028	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H021	3/21/2005	0.000027	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H027	3/21/2006	0.0029	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H027	3/21/2005	0.00037	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H027	3/19/2003	0.00012	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	H027	3/15/2004	0.00048	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H027	3/20/2007	0.00027	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H027	3/20/2006	0.000075	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H027	3/22/2005	0.00016	MILLIGRAMS PER DRY STANDARD CUBIC METER	RN

													@ 7% O2	
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H027	3/16/2004	0.00003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	FL	3/19/2007	0.00037	POUNDS PER MILLION BTU HEAT INPUT	RN: FL=0.13#/hr
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	FL	3/19/2003	0.00038	POUNDS PER MILLION BTU HEAT INPUT	RN-O2=9,CO2=10.4%, FfT=320F;F=0.12 #/hr
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	FL	3/23/2005	0.000015	POUNDS PER MILLION BTU HEAT INPUT	RN: FL= 0.0055 #/hr
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	FL	3/20/2006	0.000046	POUNDS PER MILLION BTU HEAT INPUT	RN: HF< 0.000046 #/MMBTU; HF=< 0.015#/
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	FL	3/21/2007	0.0003	POUNDS PER MILLION BTU HEAT INPUT	RN: FL=0.11#/hr =0.34mg/dscm (audit sample
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	FL	3/20/2003	0.00054	POUNDS PER MILLION BTU HEAT INPUT	RN: FL=0.19#/hr
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	FL	3/16/2004	0.000002	POUNDS PER MILLION BTU HEAT INPUT	RN: FL<0.00082#/hr
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	FL	3/22/2005	0.000016	POUNDS PER MILLION BTU HEAT INPUT	RN; HF=< 0.0059#/hr
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	FL	3/22/2006	0.000032	POUNDS PER MILLION BTU HEAT INPUT	RN: HF=<0.011#/hr
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	FL	3/21/2007	0.00028	POUNDS PER MILLION BTU HEAT INPUT	RN ; FL=0.10#/HR
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	FL	3/17/2004	0.000002	POUNDS PER MILLION BTU HEAT INPUT	RN: FL=<0.00076#/hr
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	FL	3/17/2004	0.000002	POUNDS PER MILLION BTU HEAT INPUT	RN: FL<0.00073#/hr
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	FL	3/22/2006	0.000034	POUNDS PER MILLION BTU HEAT INPUT	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	FL	3/20/2003	0.00053	POUNDS PER MILLION BTU HEAT INPUT	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	FL	3/23/2005	0.000017	POUNDS PER MILLION BTU HEAT INPUT	RN: HF=<0.0062#/hr < 0.000017#/mmbtu
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PB	3/19/2007	0.0001	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/21/2005	99	PERCENT REDUCTION IN EMISSIONS	RN: % reduction
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/21/2006	99	PERCENT REDUCTION IN EMISSIONS	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/21/2007	97.6	PERCENT REDUCTION IN EMISSIONS	RN:
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H106	3/19/2003	95	PERCENT REDUCTION IN EMISSIONS	RN: HCL smltnsly with mtd 5 (back half analy HCL=25 ppmvd@7%O2(outlet)
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H106	3/17/2004	98	PERCENT REDUCTION IN EMISSIONS	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PB	3/19/2003	0.0013	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PB	3/15/2004	0.4	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb=0.0040mg/dscm
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H106	3/20/2007	98.6	PERCENT REDUCTION IN EMISSIONS	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H106	3/22/2005	98	PERCENT REDUCTION IN EMISSIONS	RN: % reduction
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/15/2004	97	PERCENT REDUCTION IN EMISSIONS	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	2	807 TPD MSW Combustor & Auxiliary Burners- Unit 2	A	H106	3/18/2003	97	PERCENT REDUCTION IN EMISSIONS	RN: HCL simltnsly with Mthd 5(back half anal HCL= 17 ppmvd@7%O2 (outlet).
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	3	807 TPD MSW Combustor & Auxiliary Burners- Unit 3	A	H106	3/20/2006	98	PERCENT REDUCTION IN EMISSIONS	RN
WHEELABRATOR NORTH BROWARD, INC.	0112120	WHEELABRATOR NORTH BROWARD	SED	BROWARD	A	Y	1	807 TPD MSW Combustor & Auxiliary Burners- Unit 1	A	PB	3/21/2006	0.029	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	rN
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	15	Cooling Towers for FFSG Units 4 & 5	A	PM	2/7/2008	42	POUNDS/HOUR	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	SO2	1/11/2007	1.01	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	SO2	2/11/2004	0.989	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	1	Fossil Fuel Steam Generator Unit 1 (Phase II Acid Rain Unit)	A	PM	9/14/2007	0.0931	POUNDS PER MILLION BTU HEAT INPUT	sootblowing
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	1	Fossil Fuel Steam Generator Unit 1 (Phase II Acid Rain Unit)	A	PM	3/28/2006	0.02	POUNDS PER MILLION BTU HEAT INPUT	

FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	1	Fossil Fuel Steam Generator Unit 1 (Phase II Acid Rain Unit)	A	SO2	8/6/2003	1.66	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	NOX	3/12/2003	0.567	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	NOX	2/11/2004	0.548	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	NOX	1/25/2005	0.57	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	NOX	1/19/2006	0.47	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	NOX	1/11/2007	0.54	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	Fossil Fuel Steam Generator-5 (Phase I & II Acid Rain Unit)	A	SO2	4/19/2006	1.0096	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	Fossil Fuel Steam Generator-5 (Phase I & II Acid Rain Unit)	A	SO2	1/18/2007	0.973	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	1	Fossil Fuel Steam Generator Unit 1 (Phase II Acid Rain Unit)	A	PM	8/5/2003	0.0359	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	1	Fossil Fuel Steam Generator Unit 1 (Phase II Acid Rain Unit)	A	PM	8/5/2003	0.0227	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	1	Fossil Fuel Steam Generator Unit 1 (Phase II Acid Rain Unit)	A	PM	5/18/2004	0.028	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	1	Fossil Fuel Steam Generator Unit 1 (Phase II Acid Rain Unit)	A	PM	5/18/2004	0.011	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	1	Fossil Fuel Steam Generator Unit 1 (Phase II Acid Rain Unit)	A	PM	6/29/2005	0.04	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	1	Fossil Fuel Steam Generator Unit 1 (Phase II Acid Rain Unit)	A	PM	6/29/2005	0.02	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	1	Fossil Fuel Steam Generator Unit 1 (Phase II Acid Rain Unit)	A	PM	3/28/2006	0.02	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	2	Fossil Fuel Steam Generator Unit 2 (Phase II Acid Rain Unit)	A	SO2	8/6/2003	1.66	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	PM	8/12/2003	0.0104	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	PM	6/27/2005	0.01	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	PM	6/16/2004	0.03	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	PM	7/26/2006	0.02	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	PM	1/11/2007	0.02	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	PM	1/31/2008	0.006	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	2	Fossil Fuel Steam Generator Unit 2 (Phase II Acid Rain Unit)	A	PM	8/6/2003	0.0112	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	2	Fossil Fuel Steam Generator Unit 2 (Phase II Acid Rain Unit)	A	PM	8/7/2003	0.0145	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	2	Fossil Fuel Steam Generator Unit 2 (Phase II Acid Rain Unit)	A	PM	5/19/2004	0.027	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	2	Fossil Fuel Steam Generator Unit 2 (Phase II Acid Rain Unit)	A	PM	5/19/2004	0.021	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	2	Fossil Fuel Steam Generator Unit 2 (Phase II Acid Rain Unit)	A	PM	3/30/2006	0.002	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	2	Fossil Fuel Steam Generator Unit 2 (Phase II Acid Rain Unit)	A	PM	3/30/2006	0.003	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	2	Fossil Fuel Steam Generator Unit 2 (Phase II Acid Rain Unit)	A	PM	9/20/2005	0.1	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	Fossil Fuel Steam Generator-5 (Phase I & II Acid Rain Unit)	A	PM	8/12/2003	0.0225	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	Fossil Fuel Steam Generator-5 (Phase I & II Acid Rain Unit)	A	PM	6/28/2005	0.02	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	Fossil Fuel Steam Generator-5 (Phase I & II Acid Rain Unit)	A	PM	6/16/2004	0.06	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	Fossil Fuel Steam Generator-5 (Phase I & II Acid Rain Unit)	A	PM	6/5/2006	0.004	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	Fossil Fuel Steam Generator-5 (Phase I & II Acid Rain Unit)	A	PM	5/22/2006	0.003	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	Fossil Fuel Steam Generator-5 (Phase I & II Acid Rain Unit)	A	PM	1/18/2007	0.01	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	2	Fossil Fuel Steam Generator Unit 2 (Phase II Acid Rain Unit)	A	PM	9/22/2005	0.1	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	2	Fossil Fuel Steam Generator Unit 2 (Phase II Acid Rain Unit)	A	PM	9/14/2007	0.0108	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	2	Fossil Fuel Steam Generator Unit 2 (Phase II Acid Rain Unit)	A	PM	9/14/2007	0.0669	POUNDS PER MILLION BTU HEAT INPUT
FLORIDA POWER								Fossil Fuel Steam Generator-					POUNDS PER

CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	5 (Phase I & II Acid Rain Unit)	A	NOX	3/10/2003	0.545	MILLION BTU HEAT INPUT	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	Fossil Fuel Steam Generator-5 (Phase I & II Acid Rain Unit)	A	NOX	2/26/2004	0.501	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	Fossil Fuel Steam Generator-5 (Phase I & II Acid Rain Unit)	A	NOX	2/1/2005	0.55	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	Fossil Fuel Steam Generator-5 (Phase I & II Acid Rain Unit)	A	NOX	4/19/2006	0.4611	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	Fossil Fuel Steam Generator-5 (Phase I & II Acid Rain Unit)	A	NOX	1/18/2007	0.498	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	Fossil Fuel Steam Generator-5 (Phase I & II Acid Rain Unit)	A	SO2	3/10/2003	0.884	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	Fossil Fuel Steam Generator-5 (Phase I & II Acid Rain Unit)	A	SO2	2/26/2004	0.94	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	3	Fossil Fuel Steam Generator-5 (Phase I & II Acid Rain Unit)	A	SO2	2/1/2005	1	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	1	Fossil Fuel Steam Generator Unit 1 (Phase II Acid Rain Unit)	A	PM	9/11/2007	0.1	POUNDS PER MILLION BTU HEAT INPUT	actual emissions 0.1247 lb/mmbtu rounded to 0 (per standard) non-sootblowing
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	SO2	3/12/2003	1.092	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	SO2	1/25/2004	1.1	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0170004	CRYSTAL RIVER POWER PLANT	SWD	CITRUS	A	Y	4	Fossil Fuel Steam Generator-4 (Phase I & II Acid Rain Unit)	A	SO2	1/19/2006	1.02	POUNDS PER MILLION BTU HEAT INPUT	
ILUKA RESOURCES INC.	0190007	GREEN COVE SPRINGS	NED	CLAY	A	Y	1	#1 Dryer aka Primary Dryer w/cyclone for product recovery	A	PM	5/16/2007	7	POUNDS/HOUR	0.0821 grains per dry standard cubic foot.
ILUKA RESOURCES INC.	0190007	GREEN COVE SPRINGS	NED	CLAY	A	Y	1	#1 Dryer aka Primary Dryer w/cyclone for product recovery	A	PM	3/9/2004	21.9	POUNDS/HOUR	
ILUKA RESOURCES INC.	0190007	GREEN COVE SPRINGS	NED	CLAY	A	Y	1	#1 Dryer aka Primary Dryer w/cyclone for product recovery	A	PM	4/20/2006	16.91	POUNDS/HOUR	
ILUKA RESOURCES INC.	0190007	GREEN COVE SPRINGS	NED	CLAY	A	Y	1	#1 Dryer aka Primary Dryer w/cyclone for product recovery	A	PM	4/6/2005	12.71	POUNDS/HOUR	On spec oil. Sulfur<2%
ILUKA RESOURCES INC.	0190007	GREEN COVE SPRINGS	NED	CLAY	A	Y	2	#2 Dryer (Zircon Sand) w/Cylone for product recovery	A	PM	5/8/2007	1.43	POUNDS/HOUR	0.0754 grains per dry standard cubic foot (gr/S(
ILUKA RESOURCES INC.	0190007	GREEN COVE SPRINGS	NED	CLAY	A	Y	2	#2 Dryer (Zircon Sand) w/Cylone for product recovery	A	PM	6/30/2006	2.49	POUNDS/HOUR	Retested at higher production rate of 5.45 TPH
ILUKA RESOURCES INC.	0190007	GREEN COVE SPRINGS	NED	CLAY	A	Y	3	ZIRCON CALCINER WITH CYCLONE FOR PRODUCT RECOVERY	A	PM	4/21/2006	1.78	POUNDS/HOUR	
ILUKA RESOURCES INC.	0190007	GREEN COVE SPRINGS	NED	CLAY	A	Y	3	ZIRCON CALCINER WITH CYCLONE FOR PRODUCT RECOVERY	A	PM	4/2/2004	0.36	POUNDS/HOUR	1
ILUKA RESOURCES INC.	0190007	GREEN COVE SPRINGS	NED	CLAY	A	Y	3	ZIRCON CALCINER WITH CYCLONE FOR PRODUCT RECOVERY	A	PM	4/25/2005	1.44	POUNDS/HOUR	On spec oil. Sulfur<2%
ILUKA RESOURCES INC.	0190007	GREEN COVE SPRINGS	NED	CLAY	A	Y	3	ZIRCON CALCINER WITH CYCLONE FOR PRODUCT RECOVERY	A	PM	6/30/2006	1.04	POUNDS/HOUR	Retested at higher production rate of 6.5 TPH
ILUKA RESOURCES INC.	0190007	GREEN COVE SPRINGS	NED	CLAY	A	Y	2	#2 Dryer (Zircon Sand) w/Cylone for product recovery	A	PM	4/26/2005	1.12	POUNDS/HOUR	On spec oil. Sulfur<2%
ILUKA RESOURCES INC.	0190007	GREEN COVE SPRINGS	NED	CLAY	A	Y	2	#2 Dryer (Zircon Sand) w/Cylone for product recovery	A	PM	3/10/2004	0.91	POUNDS/HOUR	
ILUKA RESOURCES INC.	0190007	GREEN COVE SPRINGS	NED	CLAY	A	Y	2	#2 Dryer (Zircon Sand) w/Cylone for product recovery	A	PM	4/21/2006	1.81	POUNDS/HOUR	
E.I. DUPONT DE NEMOURS & CO - TRAILRIDGE	0190011	E.I. DUPONT DE NEMOURS & CO - TRAILRIDGE	NED	CLAY	A	Y	1	#1 DRYER ILMENITE W/CYCLONE	I	PM	8/12/2004	0.51	POUNDS/HOUR	
E.I. DUPONT DE NEMOURS & CO - TRAILRIDGE	0190011	E.I. DUPONT DE NEMOURS & CO - TRAILRIDGE	NED	CLAY	A	Y	2	ZIRCORE DRYER W/ DUCON 185 VM TYPE MODEL 700 CYCLONE <2.8%S	A	SO2	7/28/2004	0.92	PERCENT SULFUR IN FUEL	
E.I. DUPONT DE NEMOURS & CO - TRAILRIDGE	0190011	E.I. DUPONT DE NEMOURS & CO - TRAILRIDGE	NED	CLAY	A	Y	2	ZIRCORE DRYER W/ DUCON 185 VM TYPE MODEL 700 CYCLONE <2.8%S	A	PM	7/28/2004	1.45	POUNDS/HOUR	
E.I. DUPONT DE NEMOURS & CO - TRAILRIDGE	0190011	E.I. DUPONT DE NEMOURS & CO - TRAILRIDGE	NED	CLAY	A	Y	3	ZIRCON KILN ROTARY W/CYCLONE #6F0 2.8%S 20.5MMBTU/H, 18TPH	A	PM	5/27/2004	5.68	POUNDS/HOUR	
BREITBURN FLORIDA, LLC	0210031	RACCOON POINT	SD	COLLIER	A	Y	13	800 kW Gas turbine/generator set,	A	NOX	12/8/2005	99.7	PARTS PER MILLION DRY GAS VOLUME	
BREITBURN FLORIDA, LLC	0210031	RACCOON POINT	SD	COLLIER	A	Y	13	800 kW Gas turbine/generator set,	A	NOX	1/7/2003	85	PARTS PER MILLION DRY GAS VOLUME	
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0230019	LAKE CITY	NED	COLUMBIA	I	Y	5	BIOLOGICAL WASTE INCINERATOR BURNING NATURAL GAS	I	PM	12/3/2003	0.014	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Air Testing and Consulting, Inc. (ATC), 333 Falkenburg Rd., Suite B214, Tampa 33619. Ke Given, PE.
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0230019	LAKE CITY	NED	COLUMBIA	I	Y	5	BIOLOGICAL WASTE INCINERATOR BURNING NATURAL GAS	I	PM	10/6/2004	0.027	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Air Testing & Consulting, Inc. 333 Falkenburg Suite B-214, Tampa, FL 33619. (
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0230019	LAKE CITY	NED	COLUMBIA	I	Y	5	BIOLOGICAL WASTE INCINERATOR BURNING NATURAL GAS	I	CO	12/3/2003	3.49	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing and Consulting, Inc. (ATC), 333 Falkenburg Rd., Suite B214, Tampa 33619. Ke Given, PE.
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0230019	LAKE CITY	NED	COLUMBIA	I	Y	5	BIOLOGICAL WASTE INCINERATOR BURNING NATURAL GAS	I	H106	12/3/2003	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing and Consulting, Inc. (ATC), 333 Falkenburg Rd., Suite B214, Tampa 33619. Ke Given, PE.
N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0230019	LAKE CITY	NED	COLUMBIA	I	Y	5	BIOLOGICAL WASTE INCINERATOR BURNING NATURAL GAS	I	H106	10/6/2004	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing & Consulting, Inc. 333 Falkenburg Suite B-214, Tampa, FL 33619.

N. FLA/SOUTH GA VETERANS HEALTH SYSTEM	0230019	LAKE CITY	NED	COLUMBIA	I	Y	5	BIOLOGICAL WASTE INCINERATOR BURNING NATURAL GAS	I	CO	10/6/2004	4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing & Consulting, Inc. 333 Falkenburg Suite B-214, Tampa, FL 33619.
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	9	Unit 5A Combustion Turbine (170 MW) with HRSG	A	NOX	4/5/2007	1.61	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	TESTING BY AIR HYGENE INTERNATION
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	10	Unit 5B Combustion Turbine (170 MW) with HRSG	A	VOC	4/5/2007	1.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TESTING BY AIR HYGIENE
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	10	Unit 5B Combustion Turbine (170 MW) with HRSG	A	VOC	4/5/2007	0.29	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TESTING BY AIR HYGENE
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	9	Unit 5A Combustion Turbine (170 MW) with HRSG	A	VOC	4/5/2007	0.17	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TESTING BY AIR HYGENE INTERNATION
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	9	Unit 5A Combustion Turbine (170 MW) with HRSG	A	VOC	5/4/2007	0.11	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	testing by Air Hygiene
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	9	Unit 5A Combustion Turbine (170 MW) with HRSG	A	NOX	4/5/2007	7.73	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	9	Unit 5A Combustion Turbine (170 MW) with HRSG	A	CO	4/5/2007	0.87	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TESTING BY AIR HYGENE INT.
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	9	Unit 5A Combustion Turbine (170 MW) with HRSG	A	CO	4/5/2007	0.45	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	12	Unit 5D Combustion Turbine (170 MW) with HRSG	A	VOC	4/5/2007	0.35	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TESTING BY AIR HYGIENE
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	12	Unit 5D Combustion Turbine (170 MW) with HRSG	A	VOC	4/5/2007	0.73	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	11	Unit 5C Combustion Turbine (170 MW) with HRSG	A	VOC	4/5/2007	1.23	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	11	Unit 5C Combustion Turbine (170 MW) with HRSG	A	VOC	4/5/2006	1.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TEST BY AIR HYGIENE
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	10	Unit 5B Combustion Turbine (170 MW) with HRSG	A	NOX	4/5/2007	7.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TESTING BY AIR HYGIENE
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	10	Unit 5B Combustion Turbine (170 MW) with HRSG	A	CO	4/5/2007	0.74	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	10	Unit 5B Combustion Turbine (170 MW) with HRSG	A	CO	5/4/2007	0.55	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TESTING BY AIR HYGIENE
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	12	Unit 5D Combustion Turbine (170 MW) with HRSG	A	NOX	4/5/2007	1.36	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TEST BY AIR HYGIENE
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	12	Unit 5D Combustion Turbine (170 MW) with HRSG	A	NOX	4/5/2007	7.15	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TESTING BY AIR HYGIENE
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	12	Unit 5D Combustion Turbine (170 MW) with HRSG	A	CO	4/5/2007	0.31	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TEST BY AIR HYGIENE
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	12	Unit 5D Combustion Turbine (170 MW) with HRSG	A	CO	4/5/2007	0.48	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TESTING BY AIR HYGIENE
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	11	Unit 5C Combustion Turbine (170 MW) with HRSG	A	CO	4/5/2007	0.56	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TEST BY AIR HYGIENE
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	11	Unit 5C Combustion Turbine (170 MW) with HRSG	A	CO	4/5/2007	0.67	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TESTING BY AIR HYGIENE
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	11	Unit 5C Combustion Turbine (170 MW) with HRSG	A	NOX	4/5/2007	1.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TESTING BY AIR HYGIENE
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	11	Unit 5C Combustion Turbine (170 MW) with HRSG	A	NOX	4/5/2007	6.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TESTING BY AIR HYGIENE
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	10	Unit 5B Combustion Turbine (170 MW) with HRSG	A	NOX	4/5/2007	1.58	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TEST BY AIR HYGENE INTERNATIONAL
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	1	440 MW Boiler- Phase II, Acid Rain Unit 1 (Fossil Plant)	A	PM	2/20/2007	0.016	POUNDS PER MILLION BTU HEAT INPUT	STEADY STATE /FPL EMISSIONS TEST GROUP CONDUCTED THE TEST.
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	2	440 MW Boiler- Phase II, Acid Rain Unit 2 (Fossil Plant)	A	PM	6/2/2004	0.04	POUNDS PER MILLION BTU HEAT INPUT	team fple technical services
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	2	440 MW Boiler- Phase II, Acid Rain Unit 2 (Fossil Plant)	A	PM	6/2/2004	0.05	POUNDS PER MILLION BTU HEAT INPUT	team FPL technical services
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	2	440 MW Boiler- Phase II, Acid Rain Unit 2 (Fossil Plant)	A	PM	1/17/2006	0.03	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	2	440 MW Boiler- Phase II, Acid Rain Unit 2 (Fossil Plant)	A	PM	1/17/2006	0.02	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	1	440 MW Boiler- Phase II, Acid Rain Unit 1 (Fossil Plant)	A	PM	1/14/2004	0.03	POUNDS PER MILLION BTU HEAT INPUT	test done with 100% fuel oil
								440 MW Boiler- Phase II,					POUNDS PER	

FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	1	Acid Rain Unit 1 (Fossil Plant)	A	PM	1/14/2004	0.04	MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	1	440 MW Boiler- Phase II, Acid Rain Unit 1 (Fossil Plant)	A	PM	7/15/2003	0.04	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	1	440 MW Boiler- Phase II, Acid Rain Unit 1 (Fossil Plant)	A	PM	7/15/2003	0.06	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	1	440 MW Boiler- Phase II, Acid Rain Unit 1 (Fossil Plant)	A	PM	2/1/2005	0.04	POUNDS PER MILLION BTU HEAT INPUT	FPL'S EMISSION TEST GROUP CONDUCTI THE TEST.
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	2	440 MW Boiler- Phase II, Acid Rain Unit 2 (Fossil Plant)	A	PM	1/15/2003	0.03	POUNDS PER MILLION BTU HEAT INPUT	100 FUEL OIL WAS USED.
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	2	440 MW Boiler- Phase II, Acid Rain Unit 2 (Fossil Plant)	A	PM	1/15/2003	0.04	POUNDS PER MILLION BTU HEAT INPUT	100 FUEL OIL WAS USED.
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	2	440 MW Boiler- Phase II, Acid Rain Unit 2 (Fossil Plant)	A	PM	4/19/2005	0.03	POUNDS PER MILLION BTU HEAT INPUT	FPL'S ASSURANCE TEST GROUP CONDUCTED THE TEST.
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	2	440 MW Boiler- Phase II, Acid Rain Unit 2 (Fossil Plant)	A	PM	4/19/2005	0.04	POUNDS PER MILLION BTU HEAT INPUT	FPL'S ASSURANCE TEST GROUP CONDUCTED THE TEST.
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	1	440 MW Boiler- Phase II, Acid Rain Unit 1 (Fossil Plant)	A	PM	1/10/2006	0.04	POUNDS PER MILLION BTU HEAT INPUT	FPL'S PRODUCTION ASSURANCE EMISSI TEST GROUP PERFORMED THE TEST.
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	1	440 MW Boiler- Phase II, Acid Rain Unit 1 (Fossil Plant)	A	PM	1/10/2006	0.03	POUNDS PER MILLION BTU HEAT INPUT	FPL'S PRODUCTION ASSURANCE EMISSI TEST GROUP PERFORMED THE TESTS.
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	1	440 MW Boiler- Phase II, Acid Rain Unit 1 (Fossil Plant)	A	PM	2/20/2007	0.019	POUNDS PER MILLION BTU HEAT INPUT	SOOT BLOWING /FPL EMISSIONS TEST GROUP CONDUCTED THE TEST
FLORIDA POWER & LIGHT (PTF)	0250003	TURKEY POINT POWER PLANT	SEDA	MIAMI-DADE	A	Y	1	440 MW Boiler- Phase II, Acid Rain Unit 1 (Fossil Plant)	A	PM	2/1/2005	0.06	POUNDS PER MILLION BTU HEAT INPUT	FPL'S EMISSION TEST GROUP CONDUCTI THE TEST.
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	14	25 TON/HR STONE DRYER & 40 TPH SOIL THERMAL TREATMENT FACIL.	A	VOC	9/10/2005	0.02	POUNDS/HOUR	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	14	25 TON/HR STONE DRYER & 40 TPH SOIL THERMAL TREATMENT FACIL.	A	SO2	8/16/2007	6.35	POUNDS/HOUR	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	14	25 TON/HR STONE DRYER & 40 TPH SOIL THERMAL TREATMENT FACIL.	A	SO2	9/10/2005	0.64	POUNDS/HOUR	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	14	25 TON/HR STONE DRYER & 40 TPH SOIL THERMAL TREATMENT FACIL.	A	SO2	9/20/2006	4.08	POUNDS/HOUR	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	H114	1/18/2006	0.002	POUNDS/HOUR	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	H114	8/6/2004	0.00099	POUNDS/HOUR	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	H114	9/8/2005	0.0251	POUNDS/HOUR	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	PB	8/6/2004	0.0026	POUNDS/HOUR	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	PB	9/8/2005	0.01	POUNDS/HOUR	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	PM	9/1/2005	10.95	POUNDS/HOUR	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	PM	9/19/2006	10.3	POUNDS/HOUR	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	NOX	8/5/2004	346	POUNDS/HOUR	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	SO2	8/5/2004	4.3	POUNDS/HOUR	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	DIOX	3/28/2007	0.693	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	DIOX	3/29/2007	0.005	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	DIOX	4/11/2007	0.26	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	DIOX	4/25/2007	0.02	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	DIOX	8/5/2004	0.113	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	BAGHOUSE INLET TEMPERATURE AVERAGED 512 DEGREES FARENHEIT.
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	DIOX	8/4/2004	0.122	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	BAGHOUSE INLET TEMPERATURE AVERAGED 314 DEGREES FARENHEIT.
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	PM	8/12/2007	0.043	POUNDS PER TON OF FEED MATERIAL	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	CO	8/14/2007	1.25	POUNDS PER TON OF PRODUCT	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	CO	9/19/2006	1.55	POUNDS PER TON OF PRODUCT	

RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	VOC	8/12/2007	0.098	POUNDS PER TON OF PRODUCT	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	VOC	8/31/2005	0.102	POUNDS PER TON OF PRODUCT	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	VOC	6/12/2003	0.08	POUNDS PER TON OF PRODUCT	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	PM10	9/24/2003	0.04	POUNDS PER TON OF FEED MATERIAL	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	PM10	8/5/2004	0.07	POUNDS PER TON OF FEED MATERIAL	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	14	25 TON/HR STONE DRYER & 40 TPH SOIL THERMAL TREATMENT FACIL.	A	CO	9/20/2006	8.7	PARTS PER MILLION DRY GAS VOLUME	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	14	25 TON/HR STONE DRYER & 40 TPH SOIL THERMAL TREATMENT FACIL.	A	CO	8/16/2007	12.9	PARTS PER MILLION DRY GAS VOLUME	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	VOC	3/27/2003	0.09	POUNDS PER TON OF PRODUCT	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	VOC	9/23/2003	0.09	POUNDS PER TON OF PRODUCT	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	VOC	8/5/2004	0.091	POUNDS PER TON OF PRODUCT	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	VOC	9/19/2006	0.08	POUNDS PER TON OF PRODUCT	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	SAM	8/31/2005	0.0012	POUNDS PER TON OF PRODUCT	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	SAM	8/6/2004	0.003	POUNDS PER TON OF PRODUCT	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	CO	9/23/2003	1.84	POUNDS PER TON OF PRODUCT	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	CO	8/5/2004	1.69	POUNDS PER TON OF PRODUCT	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	18	KILN SYSTEM(raw mill,kiln PH/PC and clinker cooler)	A	CO	8/31/2005	1.9	POUNDS PER TON OF PRODUCT	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	14	25 TON/HR STONE DRYER & 40 TPH SOIL THERMAL TREATMENT FACIL.	A	PM	9/20/2006	0.0282	GRAINS PER DRY STANDARD CUBIC FOOT	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	14	25 TON/HR STONE DRYER & 40 TPH SOIL THERMAL TREATMENT FACIL.	A	PM	9/10/2005	0.0128	GRAINS PER DRY STANDARD CUBIC FOOT	
RINKER MATERIALS CORPORATION.	0250014	MIAMI CEMENT PLANT	SEDA	MIAMI-DADE	A	Y	14	25 TON/HR STONE DRYER & 40 TPH SOIL THERMAL TREATMENT FACIL.	A	PM	9/19/2007	0.0092	GRAINS PER DRY STANDARD CUBIC FOOT	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	20	125 ton per hour slag dryer	I	PM	4/2/2003	0.0065	GRAINS PER DRY STANDARD CUBIC FOOT	production rate averaged 80 tph for all three ru
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	H114	10/21/2004	0.005	POUNDS/HOUR	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	6	142 TPH KILN #3 W/DROPOUT BOX& DUAL CHAMBER E.S.P.	I	PM	5/20/2003	0.197	POUNDS PER TON OF FEED MATERIAL	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	PM10	11/18/2004	0.03	POUNDS PER TON OF FEED MATERIAL	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	PM10	12/4/2005	0.037	POUNDS PER TON OF FEED MATERIAL	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	PM10	2/15/2007	0.033	POUNDS PER TON OF FEED MATERIAL	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	7	88 TPH COOLER#3 W/DROPOUT BOX & BAGHOUSE	I	PM	5/6/2003	0.074	POUNDS PER TON OF FEED MATERIAL	clinker production rate was 87/5 tph.
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	6	142 TPH KILN #3 W/DROPOUT BOX& DUAL CHAMBER E.S.P.	I	SO2	5/20/2003	2.96	POUNDS PER TON OF PRODUCT	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	SO2	10/20/2004	0	POUNDS/HOUR	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	SAM	10/20/2004	1.14	POUNDS/HOUR	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	PM	11/17/2007	0.039	POUNDS PER TON OF FEED MATERIAL	CATALYST AIR MANAGEMENT
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	6	142 TPH KILN #3 W/DROPOUT BOX& DUAL CHAMBER E.S.P.	I	NOX	5/20/2003	5.88	POUNDS PER TON OF PRODUCT	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	DIOX	11/8/2005	0.0403	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	DIOX	11/16/2004	0.013	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	DIOX	11/7/2005	0.0013	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	DIOX	11/16/2004	0.01	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	

TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	5	25 TPH COOLER #2 W/MULTICLONE & DUAL CHAMBER E.S.P.	I	PM	5/7/2003	13.9	POUNDS/HOUR	clinker production rate was 24.5 tph.
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	PB	10/21/2004	0.011	POUNDS/HOUR	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	CO	12/4/2005	192.8	POUNDS/HOUR	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	VOC	11/4/2004	26.43	POUNDS/HOUR	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	NOX	10/21/2004	446.7	POUNDS/HOUR	`
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	4	41 TPH KILN #2 W/DOUBLE CHAMBER E.S.P.	I	NOX	5/21/2003	98.07	POUNDS/HOUR	clinker production rate was 24.5 TPH.
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	4	41 TPH KILN #2 W/DOUBLE CHAMBER E.S.P.	I	CO	5/21/2003	23.67	POUNDS/HOUR	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	4	41 TPH KILN #2 W/DOUBLE CHAMBER E.S.P.	I	SO2	5/21/2003	21.54	POUNDS/HOUR	production rate was 39 TPH.
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	4	41 TPH KILN #2 W/DOUBLE CHAMBER E.S.P.	I	VOC	5/21/2003	10.75	POUNDS/HOUR	
TARMAC AMERICA LLC	0250020	TARMAC-PENNSUCO CEMENT	SEDA	MIAMI-DADE	A	Y	28	Raw Mill & Pyroprocessing System	A	CO	10/21/2004	113.6	POUNDS/HOUR	
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	PM	9/6/2007	1.93	POUNDS/HOUR	ARLINGTON ENVIRONMENTAL CONDUC THE TEST.
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	PM	5/17/2006	2.46	POUNDS/HOUR	test conducted by arlington environmental.
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	PM	6/8/2004	2.23	POUNDS/HOUR	tesr performed by arlington environmental
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	CO	5/24/2005	7.68	POUNDS/HOUR	
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	CO	5/17/2006	28.6	POUNDS/HOUR	Arlington Environmental conducted the test.
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	CO	11/17/2004	16.6	POUNDS/HOUR	
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	CO	11/7/2006	3.6	POUNDS/HOUR	test conducted by Arlington Environmental Ser
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	CO	9/6/2007	20.29	POUNDS/HOUR	ARLINGTON ENVIRONMENTAL SERVICE PERFORMED THE TEST.
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	PM	5/24/2005	0.92	POUNDS/HOUR	Test by Arlington Environmental
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	PM	5/8/2003	5.63	POUNDS/HOUR	ARLINGTON ENVIRONMENTAL CONDUC THE TEST. AVERAGED PRODUCTION RA WAS 21.6 TPH.
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	SO2	9/6/2007	0.13	POUNDS PER MILLION BTU HEAT INPUT	ARLINGTON ENVIRONMENTAL CONDUC THE TEST.
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	SO2	6/8/2004	0.05	POUNDS PER MILLION BTU HEAT INPUT	Test by Arlington Environmental
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	SO2	5/24/2005	0.17	POUNDS PER MILLION BTU HEAT INPUT	Test by Arlington Environmental
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	SO2	5/8/2003	0.19	POUNDS PER MILLION BTU HEAT INPUT	ARLINGTON ENVIRONMENTAL CONDUC THE TEST. AVERAGED PRODUCTION RA WAS 21.6 TPH.
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	SO2	5/17/2006	0.02	POUNDS PER MILLION BTU HEAT INPUT	test conducted by arlington environmental.
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	15	DISA Cold Box Core Machine with Packed Gas Scrubber	A	PM	3/25/2004	0.0032	POUNDS/HOUR	
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	15	DISA Cold Box Core Machine with Packed Gas Scrubber	A	PM	6/28/2006	0.012	POUNDS/HOUR	
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	PM	10/8/2007	0.0024	GRAINS PER DRY STANDARD CUBIC FOOT	TEST BY ARLINGTON ENVIRONMENTAL
U S FOUNDRY MANUFACTURING CORP.	0250022	U S FOUNDRY MANUFACTURING CORP.	SEDA	MIAMI-DADE	A	Y	3	Foundry Cupola with afterburner and Wheelabrator Baghouse	A	VOC	10/8/2007	7.1	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	TEST BY ARLINGTON ENVIRONMENTAL
DEPARTMENT OF VETERANS AFFAIRS	0250157	VA MEDICAL CENTER	SEDA	MIAMI-DADE	A	Y	2	CLEAVER BROOKS MODEL SH850E NAT. GAS FIRED 1000LBH INCINERAT	A	PM	9/17/2004	0.0137	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
DEPARTMENT OF VETERANS AFFAIRS	0250157	VA MEDICAL CENTER	SEDA	MIAMI-DADE	A	Y	2	CLEAVER BROOKS MODEL SH850E NAT. GAS FIRED 1000LBH INCINERAT	A	H106	10/5/2006	0.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	1000 lbs/hour.
DEPARTMENT OF VETERANS AFFAIRS	0250157	VA MEDICAL CENTER	SEDA	MIAMI-DADE	A	Y	2	CLEAVER BROOKS MODEL SH850E NAT. GAS FIRED 1000LBH INCINERAT	A	CO	9/17/2004	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
DEPARTMENT OF VETERANS AFFAIRS	0250157	VA MEDICAL CENTER	SEDA	MIAMI-DADE	A	Y	2	CLEAVER BROOKS MODEL SH850E NAT. GAS FIRED 1000LBH INCINERAT	A	CO	8/12/2005	7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
DEPARTMENT OF VETERANS AFFAIRS	0250157	VA MEDICAL CENTER	SEDA	MIAMI-DADE	A	Y	2	CLEAVER BROOKS MODEL SH850E NAT. GAS FIRED 1000LBH INCINERAT	A	CO	10/5/2006	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	1000 lbs/hour.
DEPARTMENT OF VETERANS AFFAIRS	0250157	VA MEDICAL CENTER	SEDA	MIAMI-DADE	A	Y	2	CLEAVER BROOKS MODEL SH850E NAT. GAS FIRED 1000LBH INCINERAT	A	H106	8/12/2005	0.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
DEPARTMENT OF VETERANS AFFAIRS	0250157	VA MEDICAL CENTER	SEDA	MIAMI-DADE	A	Y	2	CLEAVER BROOKS MODEL SH850E NAT. GAS FIRED 1000LBH INCINERAT	A	H106	9/17/2004	1.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
DEPARTMENT OF	0250157	VA MEDICAL CENTER	SEDA	MIAMI-DADE	A	Y	2	CLEAVER BROOKS MODEL SH850E NAT.	A	PM	8/12/2005	0.0178	GRAINS PER DRY STANDARD	

VETERANS AFFAIRS								GAS FIRED 1000LBH INCINERAT					CUBIC FOOT @ 7% O2	
DEPARTMENT OF VETERANS AFFAIRS	0250157	VA MEDICAL CENTER	SEDA	MIAMI-DADE	A	Y	2	CLEAVER BROOKS MODEL SH850E NAT. GAS FIRED 1000LBH INCINERAT	A	PM	1/13/2006	0.0141	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	1000 lbs/hr charge rate.
DEPARTMENT OF VETERANS AFFAIRS	0250157	VA MEDICAL CENTER	SEDA	MIAMI-DADE	A	Y	2	CLEAVER BROOKS MODEL SH850E NAT. GAS FIRED 1000LBH INCINERAT	A	PM	10/2/2006	0.0145	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	1000 lbs/hour.
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	10	Standby Diesel Engine Generator # 5, EMD model 20-645F4B	A	NOX	5/11/2005	2.87	POUNDS PER HOUR PER TON OF MATERIAL STORED	RN; NOX=72.91#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	10	Standby Diesel Engine Generator # 5, EMD model 20-645F4B	A	NOX	7/31/2007	2.39	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	10	Standby Diesel Engine Generator # 5, EMD model 20-645F4B	A	NOX	9/6/2006	2.16	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	10	Standby Diesel Engine Generator # 5, EMD model 20-645F4B	A	NOX	8/9/2004	1.88	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	10	Standby Diesel Engine Generator # 5, EMD model 20-645F4B	A	NOX	8/19/2003	2.4	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	6	Standby Diesel Engine Generator # 1, EMD model 20-645E4	A	NOX	9/7/2006	1.5	POUNDS PER MILLION BTU HEAT INPUT	RN:
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	6	Standby Diesel Engine Generator # 1, EMD model 20-645E4	A	NOX	8/11/2004	1.4	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	7	Standby Diesel Engine Generator # 2, EMD model 20-645E4	A	NOX	8/1/2007	1.57	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	12	Standby Diesel Engine Generator # 7, EMD model 20-645F4B	A	NOX	5/13/2005	2.61	POUNDS PER MILLION BTU HEAT INPUT	RN: NOX=66.11 #/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	12	Standby Diesel Engine Generator # 7, EMD model 20-645F4B	A	NOX	8/10/2004	2.13	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	12	Standby Diesel Engine Generator # 7, EMD model 20-645F4B	A	NOX	9/5/2006	2.92	POUNDS PER MILLION BTU HEAT INPUT	RN:
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	12	Standby Diesel Engine Generator # 7, EMD model 20-645F4B	A	NOX	7/31/2007	3.05	POUNDS PER MILLION BTU HEAT INPUT	RN:
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	11	Standby Diesel Engine Generator # 6, EMD model 20-645F4B	A	NOX	8/19/2003	2.62	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	11	Standby Diesel Engine Generator # 6, EMD model 20-645F4B	A	NOX	5/11/2005	2.5	POUNDS PER MILLION BTU HEAT INPUT	RN; NOx=63.3 # / hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	11	Standby Diesel Engine Generator # 6, EMD model 20-645F4B	A	NOX	8/10/2004	1.79	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	11	Standby Diesel Engine Generator # 6, EMD model 20-645F4B	A	NOX	9/5/2006	2.23	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	11	Standby Diesel Engine Generator # 6, EMD model 20-645F4B	A	NOX	7/31/2007	2.56	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	1	Lime recalc. kiln w/cooler,twin cyclone & scrubbing twr-8.9T	A	NOX	9/17/2004	0.34	POUNDS PER MILLION BTU HEAT INPUT	RN: 2004 test.
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	1	Lime recalc. kiln w/cooler,twin cyclone & scrubbing twr-8.9T	A	NOX	9/11/2006	0.18	POUNDS PER MILLION BTU HEAT INPUT	RN: NOX=6.12 #/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	1	Lime recalc. kiln w/cooler,twin cyclone & scrubbing twr-8.9T	A	NOX	8/3/2007	0.2	POUNDS PER MILLION BTU HEAT INPUT	RN: NOX=6#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	8	Standby Diesel Engine Generator # 3, EMD model 20-645E4	A	NOX	8/21/2003	1.48	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	8	Standby Diesel Engine Generator # 3, EMD model 20-645E4	A	NOX	5/13/2005	1.5	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	8	Standby Diesel Engine Generator # 3, EMD model 20-645E4	A	NOX	8/11/2004	1.29	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	8	Standby Diesel Engine Generator # 3, EMD model 20-645E4	A	NOX	9/7/2006	1.76	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	8	Standby Diesel Engine Generator # 3, EMD model 20-645E4	A	NOX	8/1/2007	1.7	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	12	Standby Diesel Engine Generator # 7, EMD model 20-645F4B	A	NOX	8/19/2003	2.83	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	9	Standby Diesel Engine Generator # 4, EMD model 20-645F4B	A	NOX	8/20/2003	2.15	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	9	Standby Diesel Engine Generator # 4, EMD model 20-645F4B	A	NOX	5/11/2005	2.6	POUNDS PER MILLION BTU HEAT INPUT	RN; NOX=66.01#/hr.
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	9	Standby Diesel Engine Generator # 4, EMD model 20-645F4B	A	NOX	8/9/2004	1.63	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	9	Standby Diesel Engine Generator # 4, EMD model 20-645F4B	A	NOX	9/6/2006	2.15	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	9	Standby Diesel Engine Generator # 4, EMD model 20-645F4B	A	NOX	7/30/2007	2.43	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	1	Lime recalc. kiln w/cooler,twin cyclone & scrubbing twr-8.9T	A	NOX	8/18/2003	0.17	POUNDS PER MILLION BTU HEAT INPUT	RN- NOx=6.71#/hr; NG drng the test.
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	1	Lime recalc. kiln w/cooler,twin cyclone & scrubbing twr-8.9T	A	NOX	5/10/2005	0.15	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=4.63#/hr =121.8ppm
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	7	Standby Diesel Engine Generator # 2, EMD model 20-645E4	A	NOX	8/21/2003	1.49	POUNDS PER MILLION BTU HEAT INPUT	RN- 2003 test.

MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	7	Standby Diesel Engine Generator # 2, EMD model 20-645E4	A	NOX	5/13/2005	1.7	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	7	Standby Diesel Engine Generator # 2, EMD model 20-645E4	A	NOX	9/16/2004	1.31	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=34.09#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	7	Standby Diesel Engine Generator # 2, EMD model 20-645E4	A	NOX	9/8/2006	1.47	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	6	Standby Diesel Engine Generator # 1, EMD model 20-645E4	A	NOX	8/20/2003	1.51	POUNDS PER MILLION BTU HEAT INPUT	RN-2003 NOx test.
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	6	Standby Diesel Engine Generator # 1, EMD model 20-645E4	A	NOX	9/29/2005	1.66	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=42.26#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	6	Standby Diesel Engine Generator # 1, EMD model 20-645E4	A	NOX	9/5/2007	1.54	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx= 38.88#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	1	Lime recalc. kiln w/cooler,twin cyclone & scrubbing twr-8.9T	A	PM	8/3/2007	1.3	POUNDS/HOUR	RN:
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	1	Lime recalc. kiln w/cooler,twin cyclone & scrubbing twr-8.9T	A	PM	8/18/2003	1.83	POUNDS/HOUR	RN- NG drng the test. PM=0.031GR/DSCFM
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	1	Lime recalc. kiln w/cooler,twin cyclone & scrubbing twr-8.9T	A	PM	5/10/2005	1.18	POUNDS/HOUR	RN: av prcss wt =6.93T/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	1	Lime recalc. kiln w/cooler,twin cyclone & scrubbing twr-8.9T	A	PM	9/11/2006	6.12	POUNDS/HOUR	RN: 2006 tst; production rate: 62.4* % solids(0 * CFM FEED (9.3) * min/hr (60)/[2000 lbs/ton 6.0 tph in (dry) for run #1.
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250281	HIALEAH/PRESTON WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	1	Lime recalc. kiln w/cooler,twin cyclone & scrubbing twr-8.9T	A	PM	9/17/2004	1.83	POUNDS/HOUR	RN: note that allw for the test is 9.24 (procee w table calc.)
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	10	Diesel Engine Generator # 2, EMD model No. 20-645F4B	A	NOX	6/12/2007	2.25	POUNDS PER MILLION BTU HEAT INPUT	RN:
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	18	New pump engine # 3; nat gas fueled Caterpillar G3512 LE-130	A	NOX	7/26/2006	2.1	POUNDS/HOUR	RN: it is unregulated unit (initial test); NOx= 1.756#/MMBTU
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	19	New pump engine # 4; nat gas fueled Caterpillar G3512 LE-130	A	NOX	7/26/2006	2.8	POUNDS/HOUR	RN: unreg unit, initial stack test ; NOX=2.156#/MMBTU
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	10	Diesel Engine Generator # 2, EMD model No. 20-645F4B	A	NOX	9/15/2005	2.61	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=63.36 #/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	10	Diesel Engine Generator # 2, EMD model No. 20-645F4B	A	NOX	4/19/2006	2.24	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	10	Diesel Engine Generator # 2, EMD model No. 20-645F4B	A	NOX	9/9/2003	2.33	POUNDS PER MILLION BTU HEAT INPUT	RN-duesel drng the tst.
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	10	Diesel Engine Generator # 2, EMD model No. 20-645F4B	A	NOX	9/22/2004	2.14	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=51.97#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	24	Unit 5 in Standby Generating Bank (units 1 - 6)	A	NOX	9/4/2007	1.48	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=35.66#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	12	Diesel Engine Generator # 4, EMD model No. 20-645F4B	A	NOX	9/14/2005	2.41	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=58.08 #/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	12	Diesel Engine Generator # 4, EMD model No. 20-645F4B	A	NOX	6/11/2007	2.08	POUNDS PER MILLION BTU HEAT INPUT	RN:
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	11	Diesel Engine Generator # 3, EMD model No. 20-645F4B	A	NOX	9/10/2003	2.32	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	11	Diesel Engine Generator # 3, EMD model No. 20-645F4B	A	NOX	9/22/2004	2.56	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=62.52#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	11	Diesel Engine Generator # 3, EMD model No. 20-645F4B	A	NOX	4/19/2006	2.38	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	11	Diesel Engine Generator # 3, EMD model No. 20-645F4B	A	NOX	9/14/2005	2.49	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx = 60.70 #/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	11	Diesel Engine Generator # 3, EMD model No. 20-645F4B	A	NOX	6/12/2007	2.32	POUNDS PER MILLION BTU HEAT INPUT	RN:
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	23	Rm Emer. Diesel Engine Gen., Cater. Model 3508 TA-130, 900kW	C	NOX	6/11/2007	2.74	POUNDS PER MILLION BTU HEAT INPUT	RN:
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	6	ENGINE #6; 2113 HP DUAL-FUEL DRIVING 26000 GPM PUMP	A	NOX	9/12/2003	1.61	POUNDS PER MILLION BTU HEAT INPUT	RN: 344 rpm load drng the tst.
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	12	Diesel Engine Generator # 4, EMD model No. 20-645F4B	A	NOX	9/11/2003	2.39	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	12	Diesel Engine Generator # 4, EMD model No. 20-645F4B	A	NOX	9/23/2004	2.19	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=52.71#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	12	Diesel Engine Generator # 4, EMD model No. 20-645F4B	A	NOX	4/20/2006	1.42	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	6	ENGINE #6; 2113 HP DUAL-FUEL DRIVING 26000 GPM PUMP	A	NOX	9/23/2004	1.44	POUNDS PER MILLION BTU HEAT INPUT	RN; NOx=7.176#/hr; Load=344 rpm
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	9	Diesel Engine Generator # 1, EMD model No. 20-645F4B	A	NOX	9/9/2003	2.17	POUNDS PER MILLION BTU HEAT INPUT	RN: diesel drng the tst.
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	9	Diesel Engine Generator # 1, EMD model No. 20-645F4B	A	NOX	9/15/2005	2.42	POUNDS PER MILLION BTU HEAT INPUT	RN; NOx= 58.34#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	9	Diesel Engine Generator # 1, EMD model No. 20-645F4B	A	NOX	4/18/2006	2.39	POUNDS PER MILLION BTU HEAT INPUT	RN: load 2600 vs 2300
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	9	Diesel Engine Generator # 1, EMD model No. 20-645F4B	A	NOX	9/4/2007	2.08	POUNDS PER MILLION BTU HEAT INPUT	RN: Nox= 50.08#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	9	Diesel Engine Generator # 1, EMD model No. 20-645F4B	A	NOX	9/22/2004	1.69	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=40.90#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	7	Rotary Lime Recalcining Kiln designed to produce 150 TPD CaO	A	NOX	6/14/2007	2.42	POUNDS PER TON OF PRODUCT	RN: NOx=15.09#/hr
MIAMI-DADE		ALEXANDER ORR						Rotary Lime Recalcining					POUNDS PER	

WATER AND SEWER DEPARTMENT	0250314	WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	7	Kiln designed to produce 150 TPD CaO	A	NOX	9/24/2004	2.19	TON OF PRODUCT	RN: NOX=18.8 #/hr 597978 dscfh
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	7	Rotary Lime Recalcining Kiln designed to produce 150 TPD CaO	A	PM	9/8/2003	0.37	POUNDS PER TON OF FEED MATERIAL	RN-PM=3.52#/hr;PM=0.67#/Ton (output)
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	7	Rotary Lime Recalcining Kiln designed to produce 150 TPD CaO	A	PM	9/24/2004	0.22	POUNDS PER TON OF FEED MATERIAL	RN: PM=9.8#/hr; Q= 597978 dscfh
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	7	Rotary Lime Recalcining Kiln designed to produce 150 TPD CaO	A	PM	4/21/2006	0.29	POUNDS PER TON OF FEED MATERIAL	RN: PM=3.14#/hr; Load: 10.73T/hr dry in
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	7	Rotary Lime Recalcining Kiln designed to produce 150 TPD CaO	A	PM	9/16/2005	0.28	POUNDS PER TON OF FEED MATERIAL	RN: PM=2.91#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	7	Rotary Lime Recalcining Kiln designed to produce 150 TPD CaO	A	PM	6/14/2007	0.35	POUNDS PER TON OF FEED MATERIAL	RN: PM= 0.67#/ton output; PM=4.17#/hr vs 9. (limit)
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	7	Rotary Lime Recalcining Kiln designed to produce 150 TPD CaO	A	NOX	9/8/2003	1.7	POUNDS PER TON OF PRODUCT	RN: NOx==9.02 #/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	7	Rotary Lime Recalcining Kiln designed to produce 150 TPD CaO	A	NOX	4/21/2006	1.95	POUNDS PER TON OF PRODUCT	RN: NOx=11.71#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250314	ALEXANDER ORR WATER TREATMENT PLANT	SED	MIAMI-DADE	A	Y	7	Rotary Lime Recalcining Kiln designed to produce 150 TPD CaO	A	NOX	9/16/2005	2.12	POUNDS PER TON OF PRODUCT	RN: NOx=12.34#/hr; Q=596344 dscfh
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	DIOX	8/12/2003	19.8	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	900 lbs/hr.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	DIOX	8/22/2006	1.41	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	851 lbs/hr.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	PM	9/19/2003	0.0121	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	AIR TESTING AND CONSULTING CONDUCTED THE TEST.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	PM	11/5/2004	0.0102	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	AIR TESTING AND CONSULTING CONDUCTED THE TEST.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	PM	7/12/2005	0.0134	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	PM	8/12/2003	0.0136	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	900 lbs/hr.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	SO2	8/22/2006	1.64	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	890 lbs/hr.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	CO	9/19/2003	0.19	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	AIR TESTING AND CONSULTING CONDUCTED THE TEST.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	CO	7/12/2005	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	CO	10/25/2007	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	H110	8/12/2003	0.1554	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	900 lbs/hr.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	H110	8/22/2006	0.0546	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	883 lbs/hr.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	H027	8/12/2003	0.014	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	900 lbs/hr.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	H027	8/22/2006	0.0048	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	883 lbs/hr.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	H106	10/25/2007	1.93	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	H106	8/12/2003	0.042	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	900 lbs/hr.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	H106	8/22/2006	0.56	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	883 lbs/hr.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	H106	7/12/2005	1.14	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	H106	9/1/2004	1.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	AIR TESTING AND CONSULTING CONDUCTED THE TEST.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	H106	9/19/2003	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	AIR TESTING AND CONSULTING CONDUCTED THE TEST.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	NOX	8/22/2006	90	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	851 lbs/hr.

MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	H114	8/12/2003	0.0052	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	900 lbs/hr.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	H114	8/22/2006	0.005	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	883 lbs/hr.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	CO	8/22/2006	0.21	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	883 lbs/hr.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	CO	9/1/2004	0.9	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	AIR TESTING AND CONSULTING CONDUCTED THE TEST.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	SO2	8/12/2003	1.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	900 lbs/hr.
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	PM	10/25/2007	0.012	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	PM	8/22/2006	0.0072	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	883 lbs/hr
MERCY HOSPITAL	0250337	MERCY HOSPITAL	SEDA	MIAMI-DADE	A	Y	1	Simonds MD# 4AF-5C Incinerator with heat recovery boiler	A	PM	9/1/2004	0.0169	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	AIR TESTING CONSULTING CONDUCTED THE TEST.
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	PM	12/15/2003	0.0025	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN ;PM=1.44 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	PM	12/10/2004	0.0023	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN: 2004 test.PM=1.26#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H114	12/15/2007	0.00187	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=5.11E-04#/hr; Av carbon Flow= 9.6#/ (10); av spd fdr= 0.62(0.7)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H114	12/9/2006	0.00328	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=7.11E-04#/hr ; loading within 10%
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H114	12/2/2005	0.00253	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg= 5.59E-04#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H114	12/12/2004	0.00534	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Mercury= 1.54E-03 #/hr; all metals one da test.
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H114	12/17/2003	0.00244	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Mercury=6.66E-04#/hr; Max T=331F?(+3 for compl).;Av carbon mass=19.65#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H114	12/15/2007	0.00209	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: 5.56E-04#/hr; Av Crbn fd = 10.00(11); Ca Fdr Spd= 0.54(0.5)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H114	12/9/2006	0.00287	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=7.09E-04#/hr (171.5Klb/hr vs 180)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H114	12/1/2005	0.00131	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg= 3.14E-04#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H114	12/9/2004	0.00274	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Mercury= 7.67E-04 #/hr ; all metals one d test.
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H114	12/18/2003	0.00452	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN. H114=1.14E-03 #/hr; Max T=337.1 F? (+ for compl.)Av carbon mass 20.16 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H114	12/17/2007	0.00219	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg= 5.43E-04#/hr;Av cbn= 10.3 #/hr (10); crb spd= 0.74 rpm (0.7)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H114	12/8/2006	0.00229	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=5.75E-04 #/hr ; loading within 10%
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H114	12/2/2005	0.00162	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg= 4.01E-04#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H114	12/10/2004	0.0284	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Mercury= 7.71E-04 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H114	12/13/2003	0.00281	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: mercury=7.36E-04 #/hr; Max T= 346.5 F? 30F for compl prpse); need vrfy if this is stack Tdrng mercury tst; Av carbon mass= 20.27#/hr

MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H106	12/11/2007	5.87	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL= 2.35#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H106	2/21/2007	16.98	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL=6.75#/hr ; See comnts for un 1 (HCI retest on Feb20, 07)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H106	12/6/2006	20.73	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL= 6.80#/hr ; loading within 10% ;FAI 2 AUDIT samples .
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H106	12/2/2005	24.7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL=8.78#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H106	12/13/2004	20.86	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL= 7.44 #/hr; one day test.
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H106	12/12/2003	17.03	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL=7.93 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	VOC	12/12/2007	2.98	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC= 1.35#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	VOC	12/10/2006	1.04	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:VOC= 0.44#/hr ; run #1 delay due to FF fa (Notice?)for 51 min. (loading within 10%)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	VOC	12/7/2005	8.47	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC=3.64#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	VOC	12/16/2004	2.92	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC=1.36#/hr; Method 25-method 18=V
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	VOC	12/15/2003	1.51	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN NMOC=0.78#/hr (as propane)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	VOC	12/11/2007	3.26	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC = 1.52#/HR
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	VOC	12/12/2006	3.17	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC= 1.40 #/hr ; Loading within 10%
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	VOC	12/1/2005	3.46	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC= 1.51#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	VOC	12/13/2004	3.46	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC=1.63 # / hr; one day test.No staem fl prvdd.
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	VOC	12/11/2003	2.77	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: NMOC=1.15#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	VOC	12/11/2007	0.85	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC=0.41#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	VOC	12/11/2006	2.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC=1.10 #/hr ; loading within 10%
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	VOC	12/2/2005	0.62	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC=0.27#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	VOC	12/13/2004	1.39	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC=0.59#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	VOC	12/11/2003	3.24	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC=1.81 # / hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H106	12/11/2007	17.99	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL= 6.97#/HR
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H106	2/21/2007	11.48	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL=4.54#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H106	12/6/2006	21.22	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL= 7.63 #/hr ; loading within 10%; tst inconclusive; HCL audit smples failed (2).
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H106	12/27/2005	15.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: mtd 26 A
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H106	12/1/2005	27.31	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: test failed, cse rfrl;HCL=9.91#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H106	12/13/2004	10.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL=4.21#/hr ; one day test.
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H106	12/11/2003	15.26	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL=5.75#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H106	12/12/2007	14.66	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL= 5.50#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H106	2/21/2007	14.48	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: this is av of runs 3,4 and 5. HCL=5.70#/hr Run#1=30.68 for inf? Drng run 2 the blr had a leak, blr done to fix Need look in to.

MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H106	12/10/2006	10.59	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL=3.65#/hr ; 2 audt smples failed. (loac within 10%)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H106	12/7/2005	19.15	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL=6.80#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H106	12/16/2004	18.61	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: average of the first three runs is used; 4 ru prfrmd due to low steam flow on 1st run; HCL= 7.13 #/hr (with 4th run instd of the 1st= 6.55#/
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H106	12/15/2003	14.19	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN HCL=5.92#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H106	12/12/2007	14.59	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL=5.83#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H106	2/20/2007	16.73	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL retest ; HCL =6/08#/hr (1 st tests inconclusive for 4 units, 2 of 2 audits failed); Loading 90.27%
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H106	12/11/2006	7.46	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL=2.86#/hr (steam 172.1 Klb/hr vs 180 Audit samles (2) failed. They will retest.
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H106	12/4/2005	17.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL=6.25#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H106	12/9/2004	13.54	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL=5.38#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H106	2/10/2004	5.86	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: RETEST of HCL=2.32 # / hr ; T=330 F,A Carbon Flow=19.88 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H106	12/16/2003	31.73	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL=11.75 # / hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	VOC	12/12/2007	4.23	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC=2.05#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	VOC	12/11/2006	1.27	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC= 0.59#/hr (steam 172.1 Klb/hr vs 18
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	VOC	12/4/2005	1.51	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC= 0.66#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	VOC	12/9/2004	7.15	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: VOC=3.38#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	VOC	12/15/2003	7.91	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN;VOC=3.64#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	PM	12/8/2007	0.0064	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN: PM= 3.79#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	PM	12/7/2006	0.0011	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN: PM= 0.59 #/hr ; loading within 10%
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	PM	12/1/2005	0.0012	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN: PM=0.71#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	PM	12/10/2004	0.0023	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN: 2004 tst; PM= 1.48 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	PM	12/11/2003	0.0028	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN:PM=1.43 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	PM	12/11/2007	0.0043	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN: PM 2.46#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	PM	12/7/2006	0.0014	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN: PM= 0.73#/hr ; loading within 10% of production
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	PM	12/1/2005	0.005	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN: PM= 2.88#/hr ; cndtd 4 runs due to some malfunction that may effect the result of the firs that did not give an opacity exceedance and wa rprtd to DEP but we were told and explnd in th tst rprt. The av of the 3 first runs is input in AR 4th run not data was not used for cml
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	PM	12/12/2004	0.0046	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN: 2004 ; PM=2.60 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	PM	12/11/2003	0.0037	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN:PM= 2.52#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	PM	12/11/2007	0.0026	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN: PM= 1.51#/hr
													GRAINS PER	

MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	PM	12/11/2006	0.0012	DRY STANDARD CUBIC FOOT @ 7% O2	RN: PM= 0.61#/hr (Loading within 10%)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	PM	12/3/2005	0.0012	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN: PM=0.70#/hr; steam flow flow 165700 lb/
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	PM	12/12/2004	0.0042	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN: 2004 test ; PM=2.73 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	PM	12/15/2003	0.0025	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN:Air compliance group, LLC-tester ;PM=2.53#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	PM	12/10/2007	0.0014	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN: PM=0.80#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	PM	12/11/2006	0.0008	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN: PM= 0.47#/hr (steam 171.7Klb/hr vs 180)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	PM	12/3/2005	0.0008	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	RN: tested by The Air compliance group, LLC. PM=0.46#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H114	12/12/2003	0.00305	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg= 9.31E-04 #/hr; Max T=343.5F(? vrfy this T fdrng the mercury tst) (+ 30F for compl); carbon flow=20.16#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H114	12/3/2005	0.00559	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg= 1.28E-03#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	DIOX	12/14/2003	13.58	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Dioxin/Furan=4.11E-06 #/hr; Max T=343. 62.6F for compl);Max steam flow=176600#/hr; carbon mass=19.88#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	DIOX	12/14/2004	25.06	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: conducted 4 runs; this is the average of rur and 4 and cnsdrd as a retest. This av demonstra compliance , See commnts for the test on 12/13/04,Dioxin/Furan= 2.08E006#/hr; MAX s flow=180.6 #/hr (R4); Max ilet T= 344.3 F,Av carbon flw =18.62 (3 runs av).
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	DIOX	12/13/2004	33.25	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: an avrage of the runs1,2, and 3 shows viol The average of the runs 2,3, and 4 demonstrate compliance, See stack test on 12/14/04
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	DIOX	12/4/2005	18.54	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F=4.29E-06#/hr; Max stm flw=170600# (run3);Tbghsinlt= 308F;Av carbon=22.32#/hr (=22.32#/hr (metals)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	DIOX	12/13/2006	4.68	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F= 1.07E-06 #/hr ; Loading within 10% steam load=172.4Klb/hr; T baghse inlt=306 F; carbon flow 15#/hr for cmplnce.
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	DIOX	12/15/2007	12.42	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F = 3.19E-06#/hr; Max T= 306.8F; Av Flw = 9.7 #/hr (10); Av spd fdr= 0.93 rpm (0.9)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	DIOX	12/15/2004	28.43	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: 2004;Not Accptd by DEP, incnclsve; D/F=7.5E-06#/hr ;1st and 2nd runs on 12/8/04- run on 12/15/04 >5 days con. Aver. 3 and 4 run below 20 % of the limit (FL rule 52-297.310). is not acceptd. Will retest. Max steam flw=183. (R2);T inlet bghse= 339.6F;Crbn flw av=19.05
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	DIOX	4/17/2005	153.67	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: run # 2 was not cmpltd due to several malf of the runs 1,3 and 4 was used.
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	DIOX	12/2/2005	13.61	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F=3.14E-06 #/hr; Max flow drng tst=172100#/hr; T baghse inlt=305.2(run#1); A Carbon=22.12#/hr (D/F) and 22.49#/hr (metals
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	DIOX	4/14/2006	1.19	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F= 2.69 E-07 #/hr; no RO certification (for RATAs) ; 2nd QTR, 2006
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	DIOX	2/15/2006	9.29	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	DIOX	12/13/2006	1.86	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: F/D run #2 partial was voided due to fuel l [T= 305F] ; [max staem flow flow=172.8Klb/h [av carbon feed to complnce=14lb/hr] ; also ne check a notification to us(none) , hrs that was tested , cntrl log; hrly flows on 12/10/06 for un and #3
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	DIOX	12/14/2007	8.02	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F=2.22E-06 #/hr; Max T= 308.2F; Av Carbon Flow = 10.6 #/hr (11); Av Carbn Fdr Spd=0.52(.5)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	DIOX	12/13/2003	14.26	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: dioxin/furan= 3.30 E-06#/hr; Max T=346. (+62.6F for compl);Ma steam flow=179500#/h carbon mass=20.12 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	DIOX	12/12/2004	26.58	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Dioxin=8.37E-06#/hr; 4 runs were condctd ;drng run 1 plugs occrd; used av of the 3 runs; 12/11/04 (runs 1 nad 2) 12/12/04 (3rd) 12/14/04 (4th run); Max stm flow=186.6 #/hr (Max T ilet =340.5 F; Av carbn flow= 18.89 #/h of 3 runs).

MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	DIOX	12/17/2003	7.89	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: dioxin/furan=1.96E-06#/hr; Max T= 331F 62.6F for compl); Av carbon mass =19.90#/hr RUNS 1,4 AND 5 was used for compl. Need to about runs 2 and 3.
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	DIOX	12/17/2004	10.45	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Dixin=2.72E-06#/hr; 12/16/04 (1 and 2 ru 12/17/04 (3rd). Max stm flow=181.8#/hr (R1); inlet bghse T= 335.7 F; Av carbn flow= 18.74
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	DIOX	12/1/2005	11.21	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F-2.65E-06#/hr; Max Stm flow= 30920 Tbghse inlt=309.2F(run2);Av Carbon flow= 22.24#/hr (D/F_= 22.57#/hr (Metals)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	DIOX	12/13/2006	5.31	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F=1.15E-06 #/hr ; ; loading within 10% stm flw=172.7Klb/hr ; T inlt bghse=306F; Av carbon flw for for cmplnce=15#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	DIOX	12/14/2007	6	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F=1.55E-06#/ hr; max T = 305.2F; Av 9.8#/hr(10); spd crbn fdr= 0.66 rpm(0.7)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	DIOX	12/14/2003	38.58	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN- Dioxin/furan = 9.54 E-06#/hr; Max T=337 (+62.6 F for compl.);Max steam flow=180.7 #/ Av Carbon mass= 20.18#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	DIOX	2/10/2004	10.59	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN-retest ; Dioxin/furan=2.84E-06#/hr; T=330F;Av.Carbon mass=19.88#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	DIOX	5/24/2005	29.3	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: run #1 has D/F = 38.1 >30 ;2nd and 3rd 26 and 23.6 < 30;received day is e-mail day no RC certif receved yet, will mail. O2 was dtrmnd 3 Method 3 A mon. was not calibr. pwr fail. for t last 13 min lost run #3 data and calbr. Loss was realize till the office.CEMs data & Fyrite bags
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	DIOX	12/4/2005	13.76	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F= 3.20E-06#/hr;Max stm flw= 170000#/hr;Tbgh inlt= 306.6F;Av carbn flw= 22.32#/hr (D/F)= 22.32#/hr (metals).
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	DIOX	12/13/2006	6.73	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F=1.58E-06 #/hr (loading within 10%); stm flw=174.9Klb/hr; T inlt bghse=305F; Av c flw for cmplnce=10#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	DIOX	12/7/2007	31.47	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F= 8.36E-06#/hr FAILED THE TEST. max= 305.2 F; Av Carb = 10.2#/hr (10)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	DIOX	1/26/2008	11.98	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F RETEST of the Dec. of 07 tst, D/F=3. 06 #/hr Carb Flow=10.77(11); Max T = 306.6 Spd 0.75rpm(0.8); Cndtd by ACG (The Air Compliance Group, LLC).
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H114	12/13/2007	0.0019	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=4.70E-04#/hr; Av Carbn = 9.8(10)#/h Crn fdr Spd= 0.90 rpm (0.9)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H114	12/10/2006	0.00429	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=9.52E-04 #/hr ; loading within 10%
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H114	12/11/2004	0.0512	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; Mercury= 1.34E-03 #/hr, see cmnts for Be
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	FL	12/17/2004	98.14	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: 4 runs were cndtd (on Page 13) because o steam flow was less then desired durng the 1 st avrge of first 3 runs=171.6 klb/hr and av of 2, 3 4 runs was 181.6, no point to have a 4 th run. F 0.025#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H015	12/17/2003	1.24	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:2003 tst; Ar=3.39E-04#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H021	12/1/2005	0.12	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Be=2.77E-05#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H021	12/18/2003	0.27	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Be= 6.84E-05#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H021	12/9/2004	0.13	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Be= <3.5E-05#/hr (below). Av Mass carb flow=19.14 #/hr, also, see dixin/furan test.
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H021	12/9/2006	0.14	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Be= <3.48E-05 #/hr (The Air Compliance Group)(Steam production: 171600#/hr vs 180000#/hr)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H015	12/12/2003	1.04	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Ar<1.04; Ar=3.15E-04#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H027	12/13/2007	1.19	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd= 2.98E-04#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H015	12/18/2003	1.23	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:Ar=3.11E-04 #/hr
													MICROGRAMS	

MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	FL	12/13/2004	72.2	PER DRY STANDARD CUBIC METER @ 7% O2	RN: 2004 tst; FL=0.019# /hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H027	12/18/2003	0.45	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd=1.13E-04#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H027	12/9/2004	0.58	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd=1.6E-04 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H027	12/10/2004	1.77	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd=4.69E-04 #/hr See comnts for Be test.
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H027	12/13/2003	0.34	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd=8.85E-05 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H027	12/15/2007	0.44	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd= 1.18E-04#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H027	12/1/2005	0.36	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd= 8.60E-05#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	H027	12/9/2006	0.6	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd= 1.49E-04#/hr , seam prodctn 171.6 Kl vs 180
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H027	12/12/2003	0.71	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:Cd=2.19E-04 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H027	12/11/2004	3.59	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; Cd=9.51E-04 #/hr , see cmnts for Be.
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H027	12/3/2005	0.9	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd=2.07E-04#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H027	12/10/2006	0.32	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd= 7.09E-05 #/hr ; loading within 10%
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H027	12/13/2007	0.9	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd= 2.28 E-04#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	PB	12/13/2003	4.31	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb=1.13E-03 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	PB	12/10/2004	44.68	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb=1.18E-02 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	PB	12/2/2005	3.17	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb=7.76E-04#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	PB	12/8/2006	19.61	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb=4.97E-03 #/hr ; loading within 10%
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	PB	12/17/2007	40.1	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb= 1.00E-02#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	PB	12/18/2003	7.72	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; PB=1.94E-03
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	PB	12/9/2004	8.01	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb= 2.22E-03 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	PB	12/1/2005	6.08	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb=1.46E-03#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	PB	12/9/2006	12.34	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb=3.05E-03#/hr (171.6Klb/hr vs 180)
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	PB	12/15/2007	5.44	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PB=1.45E-03#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	PB	12/12/2003	27.57	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb=8.44E-03 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) &	A	PB	12/11/2004	117.19	MICROGRAMS PER DRY STANDARD	RN; Pb= 3.14 E-02 #/hr , see cmnts for Be.

								auxiliary burners					CUBIC METER @ 7% O2	
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	PB	12/3/2005	31.45	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb= 7.21E-03#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	PB	12/10/2006	3.75	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb=8.31E-04 #/hr; loading within 10%
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	PB	12/13/2007	17.62	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb= 4.38E-03#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	PB	12/17/2003	3.94	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb=1.08E-03 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	PB	12/12/2004	40.91	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RNL Pb= 1.18E-02 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	PB	12/2/2005	2.34	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb= 5.15E-04#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	PB	12/9/2006	7.26	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb=1.58E-03#/hr ; loading within +-10%
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	PB	12/15/2007	6.27	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb=1.70E-03#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H027	12/17/2003	0.75	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd=2.05E-04#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H027	12/12/2004	1.7	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd= 4.94E-04 #/ hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H027	12/2/2005	0.23	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd= 5.26E-05#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H027	12/9/2006	0.31	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd=6.82E-05#/hr ; loading within +-10%
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H027	12/15/2007	0.33	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd=8.9E-05#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	1	RDF Spreader Stoker Combustor (Unit #1) & auxiliary burners	A	FL	12/10/2004	69.87	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Fl< 69.87; Fl=0.019 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H021	12/17/2003	0.25	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN-2003 tst;Be=6.8E-05 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H021	12/12/2004	0.15	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Be<4.94E-04 #/hr; Av carbn flow = 18.62 during meatls 3runs.
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H021	12/2/2005	0.15	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Be= 3.29E-05#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	2	RDF Spreader Stoker Combustor (Unit #2) & auxiliary burners	A	H021	12/9/2006	0.15	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Be=3.36E-05#/hr; loading within +-10%
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H021	12/12/2003	0.23	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:Be<0.23;Be=7.05E-05#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H021	12/11/2004	0.14	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; Be= <3.60E-05 #/hr ;ALL metals were conducted: run1 (12/08/04),run 2 (12/08/04), r (12/11/04) -during 4 days from the 1st -to 3 rd Av carbon flow= 18.58 #/hr during metals (av runs).
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H021	12/3/2005	0.13	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Be=2.98E-05#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	H021	12/11/2006	0.16	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Be=3.53E-05 #/hr ; within 10%
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H015	12/13/2003	1.3	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Ar=3.42E-04 #/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	4	RDF Spreader Stoker Combustor (Unit #4) & auxiliary burners	A	FL	12/13/2004	72.15	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: FL=0.018 #/hr (note that a detection limit used for 4 units , data not detected.

MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H021	12/13/2003	0.26	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Be= 6.85E-05#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H021	12/10/2004	0.12	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:Be=< 3.27E-05 #/hr; seam flow was not provided for metall, I used PM as for units 1 an
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H021	12/2/2005	0.11	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Be= 2.74E-05#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H021	12/8/2006	0.14	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Be= 3.52E-05 #/hr ;loading within 10%
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H027	12/2/2005	0.42	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd=1.03E-04#/hr
MIAMI DADE RRF	0250348	MIAMI DADE RRF/MONTENAY	SED	MIAMI-DADE	A	Y	3	RDF Spreader Stoker Combustor (Unit #3) & auxiliary burners	A	H027	12/8/2006	0.21	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd= 5.42E-05 #/hr ; loading within 10%
NAILITE INTERNATIONAL	0250407	NAILITE INTERNATIONAL	SEDA	MIAMI-DADE	A	Y	1	Line 1: 3 spraybooths w/curing oven routed to RTO	A	VOC	4/12/2007	97	PERCENT REDUCTION IN EMISSIONS	
NAILITE INTERNATIONAL	0250407	NAILITE INTERNATIONAL	SEDA	MIAMI-DADE	A	Y	1	Line 1: 3 spraybooths w/curing oven routed to RTO	A	VOC	7/21/2006	99.16	PERCENT REDUCTION IN EMISSIONS	103 lb/hr for both lines (EU 001 and 004).
NAILITE INTERNATIONAL	0250407	NAILITE INTERNATIONAL	SEDA	MIAMI-DADE	A	Y	1	Line 1: 3 spraybooths w/curing oven routed to RTO	A	VOC	2/23/2003	2.08	POUNDS/HOUR	99.54% DESTRUCTION EFFICIENCY. INLE 454 LB/HR/OUTLET 2.98 LB/HR.
NAILITE INTERNATIONAL	0250407	NAILITE INTERNATIONAL	SEDA	MIAMI-DADE	A	Y	1	Line 1: 3 spraybooths w/curing oven routed to RTO	A	VOC	3/12/2004	4.48	POUNDS/HOUR	CAPTURE EFFICIENCY 99.18%
NAILITE INTERNATIONAL	0250407	NAILITE INTERNATIONAL	SEDA	MIAMI-DADE	A	Y	1	Line 1: 3 spraybooths w/curing oven routed to RTO	A	VOC	9/2/2005	98.86	PERCENT REDUCTION IN EMISSIONS	98.86% destruction effeciency at 128.5 gallons/
NAILITE INTERNATIONAL	0250407	NAILITE INTERNATIONAL	SEDA	MIAMI-DADE	A	Y	1	Line 1: 3 spraybooths w/curing oven routed to RTO	A	VOC	4/17/2007	99.21	PERCENT REDUCTION IN EMISSIONS	Test conducted with both lines in operation RT temp averaged 1708 deg f
NAILITE INTERNATIONAL	0250407	NAILITE INTERNATIONAL	SEDA	MIAMI-DADE	A	Y	4	Line 2: 3 spraybooths w/curing oven routed to RTO	A	VOC	4/18/2007	99.21	PERCENT REDUCTION IN EMISSIONS	
NAILITE INTERNATIONAL	0250407	NAILITE INTERNATIONAL	SEDA	MIAMI-DADE	A	Y	4	Line 2: 3 spraybooths w/curing oven routed to RTO	A	VOC	4/28/2007	99.21	PERCENT REDUCTION IN EMISSIONS	
NAILITE INTERNATIONAL	0250407	NAILITE INTERNATIONAL	SEDA	MIAMI-DADE	A	Y	4	Line 2: 3 spraybooths w/curing oven routed to RTO	A	VOC	9/2/2005	98.86	PERCENT REDUCTION IN EMISSIONS	98.86% destruction effeciency at 128.5 gallons/
NAILITE INTERNATIONAL	0250407	NAILITE INTERNATIONAL	SEDA	MIAMI-DADE	A	Y	4	Line 2: 3 spraybooths w/curing oven routed to RTO	A	VOC	3/12/2004	4.8	POUNDS/HOUR	DISTRUCTION EFFICIENCY 99.18%
NAILITE INTERNATIONAL	0250407	NAILITE INTERNATIONAL	SEDA	MIAMI-DADE	A	Y	4	Line 2: 3 spraybooths w/curing oven routed to RTO	A	VOC	1/23/2003	2.08	POUNDS/HOUR	VOC DESTRUCTION EFFICIENCY WAS 99.54%.
NAILITE INTERNATIONAL	0250407	NAILITE INTERNATIONAL	SEDA	MIAMI-DADE	A	Y	4	Line 2: 3 spraybooths w/curing oven routed to RTO	A	VOC	7/21/2006	99.16	PERCENT REDUCTION IN EMISSIONS	106 lb/hr for both lines (EU 001 and 004).
NAILITE INTERNATIONAL	0250407	NAILITE INTERNATIONAL	SEDA	MIAMI-DADE	A	Y	4	Line 2: 3 spraybooths w/curing oven routed to RTO	A	VOC	4/19/2007	97.72	PERCENT REDUCTION IN EMISSIONS	Test on line 2 only, RTO temp averaged 1562 c This will be operating temp for RTO
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	10	1.2 MW Digester Gas Electric Generator; # 3	A	NOX	8/7/2007	2.64	POUNDS/HOUR	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	10	1.2 MW Digester Gas Electric Generator; # 3	A	NOX	6/3/2003	6.48	POUNDS/HOUR	RN, flow=3175scft/min
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	11	1.2 MW Digester Gas Electric Generator; # 4	A	NOX	4/27/2006	4.5	POUNDS/HOUR	
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	11	1.2 MW Digester Gas Electric Generator; # 4	A	NOX	4/22/2004	3.1	POUNDS/HOUR	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	7	1.2 MW Digester Gas Electric Generator; # 1	A	NOX	6/5/2003	5.17	POUNDS/HOUR	RN-, Flow=2990.79 scft/min
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	7	1.2 MW Digester Gas Electric Generator; # 1	A	NOX	4/29/2004	5.4	POUNDS/HOUR	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	7	1.2 MW Digester Gas Electric Generator; # 1	A	NOX	5/18/2005	7	POUNDS/HOUR	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	7	1.2 MW Digester Gas Electric Generator; # 1	A	NOX	4/24/2006	5.6	POUNDS/HOUR	
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	7	1.2 MW Digester Gas Electric Generator; # 1	A	NOX	8/6/2007	6.58	POUNDS/HOUR	RN:
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	11	1.2 MW Digester Gas Electric Generator; # 4	A	NOX	6/2/2003	5.22	POUNDS/HOUR	RN, flow=3149 scft/min
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	11	1.2 MW Digester Gas Electric Generator; # 4	A	NOX	5/18/2005	7.4	POUNDS/HOUR	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	11	1.2 MW Digester Gas Electric Generator; # 4	A	NOX	9/27/2007	4.44	POUNDS/HOUR	RN: NOx=0.31#/MMBTU
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	10	1.2 MW Digester Gas Electric Generator; # 3	A	NOX	4/21/2004	6.9	POUNDS/HOUR	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	10	1.2 MW Digester Gas Electric Generator; # 3	A	NOX	5/2/2006	5.6	POUNDS/HOUR	
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	10	1.2 MW Digester Gas Electric Generator; # 3	A	NOX	5/16/2005	6.5	POUNDS/HOUR	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	9	1.2 MW Digester Gas Electric Generator; # 2	A	NOX	8/7/2007	4.39	POUNDS/HOUR	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	9	1.2 MW Digester Gas Electric Generator; # 2	A	NOX	7/2/2003	4.67	POUNDS/HOUR	RN,flow 2620 scft/min

MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	9	1.2 MW Digester Gas Electric Generator; # 2	A	NOX	4/20/2004	5.8	POUNDS/HOUR	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	9	1.2 MW Digester Gas Electric Generator; # 2	A	NOX	4/25/2006	4.5	POUNDS/HOUR	
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	9	1.2 MW Digester Gas Electric Generator; # 2	A	NOX	5/16/2005	4.8	POUNDS/HOUR	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	13	2.5 MW Diesel Electric Generator; EMD # 1	A	NOX	8/9/2007	1.26	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	13	2.5 MW Diesel Electric Generator; EMD # 1	A	NOX	7/2/2003	1.41	POUNDS PER MILLION BTU HEAT INPUT	RN, flow=9293cft/min, NOx=35.46#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	15	2.5 MW Diesel Electric Generator; EMD # 3	A	NOX	6/5/2003	1.72	POUNDS PER MILLION BTU HEAT INPUT	RN, NOx=43.38#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	15	2.5 MW Diesel Electric Generator; EMD # 3	A	NOX	4/23/2004	1.7	POUNDS PER MILLION BTU HEAT INPUT	RN:(EMD3); NOx= 42 #/hr;Load=2300KW
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	15	2.5 MW Diesel Electric Generator; EMD # 3	A	NOX	5/20/2005	1.78	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=45#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	15	2.5 MW Diesel Electric Generator; EMD # 3	A	NOX	4/27/2006	1.79	POUNDS PER MILLION BTU HEAT INPUT	
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	15	2.5 MW Diesel Electric Generator; EMD # 3	A	NOX	9/18/2007	1.69	POUNDS PER MILLION BTU HEAT INPUT	RN; NOX=42.34#/HR
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	19	2.865 MW Diesel Engine Generator; EMD # 4	C	NOX	9/27/2007	1.69	POUNDS PER MILLION BTU HEAT INPUT	RN; NOX=42.41#/HR
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	14	2.5 MW Diesel Electric Generator; EMD # 2	A	NOX	7/2/2003	1.36	POUNDS PER MILLION BTU HEAT INPUT	RN, NOx= 34.16 # / hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	14	2.5 MW Diesel Electric Generator; EMD # 2	A	NOX	4/22/2004	1.7	POUNDS PER MILLION BTU HEAT INPUT	RN:(EMD2) NOx= 43 #/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	14	2.5 MW Diesel Electric Generator; EMD # 2	A	NOX	4/27/2006	1.55	POUNDS PER MILLION BTU HEAT INPUT	
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	14	2.5 MW Diesel Electric Generator; EMD # 2	A	NOX	8/9/2007	1.25	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	13	2.5 MW Diesel Electric Generator; EMD # 1	A	NOX	4/22/2004	1.6	POUNDS PER MILLION BTU HEAT INPUT	RN: (EMD1) NOx= 39#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	13	2.5 MW Diesel Electric Generator; EMD # 1	A	NOX	4/26/2006	1.41	POUNDS PER MILLION BTU HEAT INPUT	
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250476	CENTRAL DISTRICT WASTEWATER TRTMNT PLANT	SED	MIAMI-DADE	A	Y	13	2.5 MW Diesel Electric Generator; EMD # 1	A	NOX	5/19/2005	1.42	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx==38#/hr ; note NOx limit in rprt=2.1 units 13,14, and 15 and here is 4.75 #/MMBTU
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	8	Standby Generator Set (model 20E4B) #3	A	NOX	4/6/2006	1.99	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=47.95#/hr; Unit oprtd in 2006/2007 =105.1 hrs <400
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	7	Standby Generator Set (model 20E4B) #2	A	NOX	7/20/2004	1.75	POUNDS PER MILLION BTU HEAT INPUT	RN:
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	9	Standby Generator Set (model 20E4B) #4	A	NOX	4/6/2006	2.12	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=51.11#/hr; Unit oprtd in 2006/2007 f yr =91.0Hr <400
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	9	Standby Generator Set (model 20E4B) #4	A	NOX	7/1/2003	1.97	POUNDS PER MILLION BTU HEAT INPUT	RN; NOx=47.49#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	9	Standby Generator Set (model 20E4B) #4	A	NOX	7/21/2004	2.06	POUNDS PER MILLION BTU HEAT INPUT	RN(2005 < 400 hrs).
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	7	Standby Generator Set (model 20E4B) #2	A	NOX	7/1/2003	1.62	POUNDS PER MILLION BTU HEAT INPUT	RN-NOx=39.04#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	7	Standby Generator Set (model 20E4B) #2	A	NOX	4/5/2006	2	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=48.19 #/hr ;RNon 11/2/07 unit oprtd hr in 2006/2007 no test is required,<400hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	13	Standby Generator Set (model 20F4B) #6	C	NOX	4/4/2006	1.87	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=45.45#/hr; Unit oprtd in 2006/07 =1 hrs < 400 hr no stack test is needed in 2007. Le rcvd by LH on 10/26/07
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	8	Standby Generator Set (model 20E4B) #3	A	NOX	7/20/2004	1.78	POUNDS PER MILLION BTU HEAT INPUT	RN (2005 <400hrs).
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	8	Standby Generator Set (model 20E4B) #3	A	NOX	5/29/2003	1.81	POUNDS PER MILLION BTU HEAT INPUT	RN- NOx=43.68#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	6	Standby Generator Set (model 20E4B) #1	A	NOX	4/5/2006	2.19	POUNDS PER MILLION BTU HEAT INPUT	RN; NOx=52.91#/hr; RN on 11/2/07 Un oprtd 2006/2007 fscl yr-140.8 hrs ; rcvd on 10/26/07
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	3	Digester gas-fired cogeneration Engine #3	A	NOX	9/12/2005	6.77	POUNDS/HOUR	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	3	Digester gas-fired cogeneration Engine #3	A	NOX	9/27/2006	7.876	POUNDS/HOUR	RN; NOx=0.803#/MMBTU; MD wtnssd the te fuel flow drng the test= 3428 vs 2750 cftm
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	2	Digester gas-fired cogeneration Engine #2	A	NOX	10/4/2004	9	POUNDS/HOUR	RN; note in ppm was 304@ 15% O2. (constrtn had allwble9.7#/hr and satndard= 250 ppm @1 O2).
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	2	Digester gas-fired cogeneration Engine #2	A	NOX	4/11/2006	8.2	POUNDS/HOUR	RN: see un #1 comnts
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	2	Digester gas-fired cogeneration Engine #2	A	NOX	9/12/2005	8.19	POUNDS/HOUR	RN:
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	6	Standby Generator Set (model 20E4B) #1	A	NOX	7/19/2004	1.86	POUNDS PER MILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	6	Standby Generator Set (model 20E4B) #1	A	NOX	5/28/2003	1.73	POUNDS PER MILLION BTU HEAT INPUT	RN, NOx=41.7#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	10	Standby Generator Set (model 16G4A) #5	A	NOX	5/28/2003	1.98	POUNDS PER MILLION BTU HEAT INPUT	RN, NOx=48.27#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	10	Standby Generator Set (model 16G4A) #5	A	NOX	7/19/2004	2	POUNDS PER MILLION BTU HEAT INPUT	RN: (in 2005 <400hrs)
MIAMI-DADE		SOUTH DISTRICT											POUNDS PER	

WATER AND SEWER DEPARTMENT	0250520	WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	10	Standby Generator Set (model 16G4A) #5	A	NOX	4/5/2006	2.68	MILLION BTU HEAT INPUT	RN: NOx=65.08#/hr; unit oprtd in 2006/07= 11 hrs<400 hrs , no test is needed in 2007.
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	1	Digester gas-fired cogeneration Engine #1	A	NOX	9/12/2005	2.41	POUNDS/HOUR	RN: 2005 stack test.
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	1	Digester gas-fired cogeneration Engine #1	A	NOX	4/10/2006	9	POUNDS/HOUR	RN: hard copy rcvd on 5/22/06; e-mail on 5/17/
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	2	Digester gas-fired cogeneration Engine #2	A	NOX	5/28/2003	182.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN-Nox=6.67#/hr NOx=1.013#/mmbtu
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	1	Digester gas-fired cogeneration Engine #1	A	NOX	5/27/2003	165.21	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN- NOx=5.68#/hr, NOx=0.61#/mmbtu; flow=2290scft/min
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	1	Digester gas-fired cogeneration Engine #1	A	NOX	7/15/2004	60.74	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NOx=2.81#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	3	Digester gas-fired cogeneration Engine #3	A	NOX	5/27/2003	197.58	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN-NOx=7.4 #/hr NOx=1.123 #/mmbtu
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250520	SOUTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	3	Digester gas-fired cogeneration Engine #3	A	NOX	7/22/2004	131.13	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NOx=8.89#/hr
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250600	NORTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	8	Diesel Engine Standby Generator #6, CAT model No. 3612	A	NOX	7/14/2004	3.83	POUNDS PER MILLION BTU HEAT INPUT	RN: 2004 test on oil #2.
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250600	NORTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	8	Diesel Engine Standby Generator #6, CAT model No. 3612	A	NOX	5/22/2003	3.44	POUNDS PER MILLION BTU HEAT INPUT	This test was not required by the existing 2003 permit. LT
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250600	NORTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	8	Diesel Engine Standby Generator #6, CAT model No. 3612	A	NOX	4/6/2004	4.11	POUNDS PER BILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250600	NORTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	7	Diesel Engine Standby Generator #5, EMD model No. 16-710G4A	A	NOX	7/13/2004	2.53	POUNDS PER MILLION BTU HEAT INPUT	RN: 2004 test.
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250600	NORTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	5	Diesel Engine Standby Generator #4, EMD model No. 20-645E4B	A	NOX	4/6/2004	1.78	POUNDS PER BILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250600	NORTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	4	Diesel Engine Standby Generator #3, EMD model No. 20-645E4B	A	NOX	4/7/2004	2.5	POUNDS PER BILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250600	NORTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	7	Diesel Engine Standby Generator #5, EMD model No. 16-710G4A	A	NOX	4/8/2004	2.8	POUNDS PER BILLION BTU HEAT INPUT	RN
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250600	NORTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	2	Diesel Engine Standby Generator #1, EMD model No. 20-645E4B	A	NOX	4/8/2004	2.32	POUNDS PER BILLION BTU HEAT INPUT	RN: there is NOx RACT Rule allwble.
MIAMI-DADE WATER AND SEWER DEPARTMENT	0250600	NORTH DISTRICT WASTEWATER TREATMNT PLANT	SED	MIAMI-DADE	A	Y	3	Diesel Engine Standby Generator #2, EMD model No. 20-645E4B	A	NOX	4/7/2004	2.48	POUNDS PER BILLION BTU HEAT INPUT	RN
MIAMI-DADE SOLID WASTE MANAGEMENT	0250603	MIAMI DADE SOLID WSTE MGMT/NO DADE LF	SED	MIAMI-DADE	A	Y	2	Enclosed Flare model GF-1000	A	NMOC	1/22/2003	8.97	PARTS PER MILLION DRY GAS VOLUME	RN this is rslt for the blank-corrected VOC as Hexane ppmdry@3%O2 with leachate air stripp off (DE=65%)
MIAMI-DADE SOLID WASTE MANAGEMENT	0250603	MIAMI DADE SOLID WSTE MGMT/NO DADE LF	SED	MIAMI-DADE	A	Y	2	Enclosed Flare model GF-1000	A	NMOC	1/22/2003	5.35	PARTS PER MILLION DRY GAS VOLUME	RN-this result with blank-corrected VOC as He @3% O2 and w/air strippers on(the DE was 67 this condtions vs. 98%).Prmt rqrs comply with of the limits.
WASTE MANAGEMENT INC. OF FLORIDA	0250615	MEDLEY LANDFILL	SEDA	MIAMI-DADE	A	Y	5	Enclosed 6,000 scfm primary flare	A	VOC	4/20/2005	2.09	PARTS PER MILLION DRY GAS VOLUME AS HEXANE @ 3% O2	
WASTE MANAGEMENT INC. OF FLORIDA	0250615	MEDLEY LANDFILL	SEDA	MIAMI-DADE	A	Y	5	Enclosed 6,000 scfm primary flare	A	VOC	4/11/2006	0.19	PARTS PER MILLION DRY GAS VOLUME AS HEXANE @ 3% O2	
WASTE MANAGEMENT INC. OF FLORIDA	0250615	MEDLEY LANDFILL	SEDA	MIAMI-DADE	A	Y	5	Enclosed 6,000 scfm primary flare	A	VOC	3/26/2007	0.43	PARTS PER MILLION DRY GAS VOLUME AS HEXANE @ 3% O2	
GOODRICH CORPORATION	0250827	LANDING SYSTEMS SERVICES	SEDA	MIAMI-DADE	A	Y	9	Hard Chromium Electroplating, one tank	A	H046	1/10/2007	0.002	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Tested at 2 in of water pressure drop across scrubber.
GOODRICH CORPORATION	0250827	LANDING SYSTEMS SERVICES	SEDA	MIAMI-DADE	A	Y	3	Hard Chromium Electroplating, three chromium tanks	A	H046	1/9/2007	0.003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Tested at 1 in of water pressure drop across scrubber.
PEACE RIVER CITRUS PRODUCTS	0270003	PEACE RIVER CITRUS PRODUCTS	SWD	DESOTO	A	Y	1	CITRUS PEEL DRYER WASTE HEAT EVAPORATOR	A	PM	2/6/2008	8.02	POUNDS/HOUR	ATC
PEACE RIVER CITRUS PRODUCTS	0270003	PEACE RIVER CITRUS PRODUCTS	SWD	DESOTO	A	Y	1	CITRUS PEEL DRYER WASTE HEAT EVAPORATOR	A	PM	1/28/2003	10.557	POUNDS/HOUR	29.5 TPH
PEACE RIVER CITRUS PRODUCTS	0270003	PEACE RIVER CITRUS PRODUCTS	SWD	DESOTO	A	Y	1	CITRUS PEEL DRYER WASTE HEAT EVAPORATOR	A	PM	2/5/2004	4.406	POUNDS/HOUR	
PEACE RIVER CITRUS PRODUCTS	0270003	PEACE RIVER CITRUS PRODUCTS	SWD	DESOTO	A	Y	1	CITRUS PEEL DRYER WASTE HEAT EVAPORATOR	A	PM	2/1/2007	6.3	POUNDS/HOUR	ATC
PEACE RIVER CITRUS PRODUCTS	0270003	PEACE RIVER CITRUS PRODUCTS	SWD	DESOTO	A	Y	1	CITRUS PEEL DRYER WASTE HEAT EVAPORATOR	A	PM	2/2/2006	8.437	POUNDS/HOUR	
PEACE RIVER CITRUS PRODUCTS	0270003	PEACE RIVER CITRUS PRODUCTS	SWD	DESOTO	A	Y	1	CITRUS PEEL DRYER WASTE HEAT EVAPORATOR	A	PM	1/26/2005	8.1	POUNDS/HOUR	Air Testing and Consulting, 9.75 TPH dary, 29. TPH wet, scrubber pump 62 psi
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	NOX	8/19/2007	8.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	NAT. GAS
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	NOX	6/25/2004	40.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil. Heat input 1607.9 mmBTU/hr (LHV) C.E.M. Solutions
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	NOX	4/28/2004	6.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	The test was performed on time, we received th results from Dave Meyer via phone call.
													PARTS PER	

DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	NOX	6/17/2003	6.7	MILLION DRY GAS VOLUME @ 15% O2	1517 MMBtu/hr C.E.M. Solutions, Inc.
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	NOX	5/13/2003	7.785	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	A RATA was run on 5/13/03 but SWD never g copy of the report. This data was received 11/2.
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	NOX	4/30/2004	5.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test performed on time. Results received via pl call from Dave Meyer, Progress Energy. Values were not averaged in the report.
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	NOX	6/7/2005	8.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Method 7E. C.E.M. Solutions. Hea input 1463 MMBtu/hr.
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	NOX	5/23/2006	8.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	CEM Solutions
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	NOX	9/30/2006	0.000001	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	< 400 HRS ON OIL - DATA INPUT TO PREVENT TEST DUE FLAGGING
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	NOX	8/18/2007	8.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	NAT. GAS
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	NOX	8/14/2007	37.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FUEL OIL
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	SO2	6/9/2003	0.0344	PERCENT SULFUR IN FUEL	INTERTEK TESTING SERVICES
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	SO2	6/25/2004	0.048	PERCENT SULFUR IN FUEL	Fuel oil. Method 19 84.6 lbs/hr C.E.M. solutior
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	NOX	6/18/2003	37.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	1688 MMBtu/hr C.E.M. Solutions, Inc.
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	NOX	6/7/2005	7.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Method 7E. C.E.M. Solutions. Hea input 1450 mmBtu/hr.
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	NOX	5/23/2006	7.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	CEM Solutions
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	NOX	6/30/2006	0.00001	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	< 400 HRS ON OIL - DATA INPUT TO PREVENT TEST DUE FLAGGING
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	SO2	5/23/2006	0.052	OTHER (SPECIFY IN COMMENT)	CEM Solutions
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	CO	6/7/2005	0.4	PARTS PER MILLION DRY GAS VOLUME	Natural gas. C.E.M. Solutions. Heat input 1463 MMBtu/hr.
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	CO	5/23/2006	0.4	PARTS PER MILLION DRY GAS VOLUME	CEM Solutions
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	CO	9/30/2006	0.000001	PARTS PER MILLION DRY GAS VOLUME	< 400 HRS ON OIL - DATA INPUT TO PREVENT TEST DUE FLAGGING
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	CO	8/18/2007	0.75	PARTS PER MILLION DRY GAS VOLUME	NAT. GAS
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	CO	8/14/2007	1.29	PARTS PER MILLION DRY GAS VOLUME	FUEL OIL
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	SO2	6/17/2003	0.1	OTHER (SPECIFY IN COMMENT)	gr/100scf
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	SO2	5/23/2006	0.0582	OTHER (SPECIFY IN COMMENT)	CEM Solution
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	VOC	6/17/2003	0	PARTS PER MILLION DRY GAS VOLUME	1517 MMBtu/hr C.E.M. Solutions, Inc. Test re: actually -0.2
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	VOC	6/18/2003	0	OTHER (SPECIFY IN COMMENT)	1688 MMBtu/hr Actual result reported as -0.2 ppmvw C.E.M. Solutions, Inc.
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	VOC	9/20/2007	0.29	PARTS PER MILLION DRY GAS VOLUME	NAT. GAS
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	CO	6/17/2003	1.6	PARTS PER MILLION DRY GAS VOLUME	1517 MMBtu/hr C.E.M. Solutions, Inc.
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	CO	6/18/2003	0.3	PARTS PER MILLION DRY GAS VOLUME	1688 MMBtu/hr C.E.M. Solutions, Inc.
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	CO	4/28/2004	0.18	PARTS PER MILLION DRY GAS VOLUME	Progress Energy Environmental Test Team Hea input 1452 MMBtu/hr
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	CO	6/7/2005	0	PARTS PER MILLION DRY GAS VOLUME	Natural gas. C.E.M. Solutions. Heat input 1450 mmBtu/hr.
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	CO	6/25/2004	0.5	PARTS PER MILLION DRY GAS VOLUME	Fuel oil. Heat input 1607.9 mmBTU/hr (LHV) C.E.M. Solutions
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	CO	5/23/2006	0.5	PARTS PER MILLION DRY GAS VOLUME	CEM Solutions
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	CO	9/30/2006	0.000001	PARTS PER MILLION DRY GAS VOLUME	< 400 HRS ON OIL - DATA INPUT TO PREVENT TEST DUE FLAGGING
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	VOC	8/18/2007	0.04	PARTS PER MILLION DRY GAS VOLUME	NAT. GAS
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	VOC	8/14/2007	0.58	OTHER (SPECIFY IN COMMENT)	FUEL OIL
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	CO	5/13/2003	0.19	PARTS PER MILLION DRY GAS VOLUME	Progress Energy Environmental Test Team. He input 1463.2 MMBtu/hr.

DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	2	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	CO	4/30/2004	0.28	PARTS PER MILLION DRY GAS VOLUME	Progress Energy Environmental Test Team Hea input 1437 MMBtu/hr
DESOTO COUNTY GENERATING COMPANY, LLC	0270016	DESOTO COUNTY ENERGY PARK	SWD	DESOTO	A	Y	1	170MW Simple Cycle Comb Turbine (Phase II Acid Rain unit)	A	CO	8/19/2007	0.6	PARTS PER MILLION DRY GAS VOLUME	NAT . GAS
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	522	Stored Product Handling System	A	PM	5/27/2004	0.0063	POUNDS/HOUR	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	537	GFM Bean Separator	A	PM	6/1/2004	0.0029	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	537	GFM Bean Separator	A	PM	5/1/2007	0.0048	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	504	Probat Roasters	A	PM	4/18/2003	0.0099	GRAINS PER DRY STANDARD CUBIC FOOT	# 7
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	504	Probat Roasters	A	PM	4/23/2003	0.011	GRAINS PER DRY STANDARD CUBIC FOOT	# 8 roster afterbunner
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	534	GFIC Majors Dump Station Receiving	A	PM	5/1/2007	0.0027	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	534	GFIC Majors Dump Station Receiving	A	PM	5/25/2004	0.00013	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	504	Probat Roasters	A	PM	6/16/2004	0.0084	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	504	Probat Roasters	A	PM	3/24/2005	0.0083	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	503	Thermalo Roasters	A	PM	4/18/2007	0.0193	GRAINS PER DRY STANDARD CUBIC FOOT	#1 roaster 3100#hr *2 for process rate(as per)
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	503	Thermalo Roasters	A	PM	3/8/2006	0.0075	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	503	Thermalo Roasters	A	PM	3/25/2005	0.0077	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	503	Thermalo Roasters	A	PM	6/23/2004	0.0107	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	503	Thermalo Roasters	A	PM	4/25/2003	0.0088	GRAINS PER DRY STANDARD CUBIC FOOT	# 1 thermalo
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	504	Probat Roasters	A	PM	3/29/2007	0.0193	GRAINS PER DRY STANDARD CUBIC FOOT	#6 3100#/hr per roaster (10 roasters)
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	504	Probat Roasters	A	PM	3/30/2007	0.0151	GRAINS PER DRY STANDARD CUBIC FOOT	#5 Probat Roaster(3100#/hr per roaster(10 roas
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	504	Probat Roasters	A	PM	3/14/2006	0.0084	GRAINS PER DRY STANDARD CUBIC FOOT	#4 pro roaster car
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	504	Probat Roasters	A	PM	3/9/2006	0.014	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	504	Probat Roasters	A	PM	3/10/2004	0.0074	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	553	Roasted Whole Bean Handling	A	PM	1/19/2007	0.0016	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	553	Roasted Whole Bean Handling	A	PM	1/17/2007	0.0023	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	553	Roasted Whole Bean Handling	A	PM	2/14/2007	0.002	GRAINS PER DRY STANDARD CUBIC FOOT	Test allowable is 0.0017 gr/DSCF
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	553	Roasted Whole Bean Handling	A	PM	1/19/2007	0.0025	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	553	Roasted Whole Bean Handling	A	PM	1/17/2007	0.0023	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	554	Green Bean Storage	A	PM	2/14/2007	0.0018	GRAINS PER DRY STANDARD CUBIC FOOT	Breen Bean stor (North)
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	554	Green Bean Storage	A	PM	1/31/2007	0.0017	GRAINS PER DRY STANDARD CUBIC FOOT	Green Bean Stor (south) w/DFF BH
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	508	Green Bean Scalpers	I	PM	6/27/2003	0.0018	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	508	Green Bean Scalpers	I	PM	6/27/2003	0.0024	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL	0310004	KRAFT FOODS, MAXWELL HOUSE	NEDV	DUVAL	A	Y	521	Continuous Cooling System	A	PM	5/26/2004	0.0046	GRAINS PER DRY	

HOUSE COFFEE		COFFEE											STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	539	Green Coffee Silos	A	PM	3/26/2007	0.0045	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	539	Green Coffee Silos	A	PM	6/28/2003	0.0028	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	551	GFM Drying Zone 2	A	PM	3/12/2007	0.0066	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	551	GFM Drying Zone 2	A	PM	11/4/2003	0.0048	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	514	Thermalo Destoners	A	PM	5/11/2007	0.0052	GRAINS PER DRY STANDARD CUBIC FOOT	Thermalo Destoner Baghouse
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	514	Thermalo Destoners	A	PM	3/17/2006	0.0019	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	514	Thermalo Destoners	A	PM	6/2/2004	0.0022	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	513	Thermalo Cooling Cars	A	PM	3/16/2006	0.0018	GRAINS PER DRY STANDARD CUBIC FOOT	#1 thermalo car
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	513	Thermalo Cooling Cars	A	PM	3/1/2005	0.0024	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	513	Thermalo Cooling Cars	A	PM	3/1/2005	0.0017	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	513	Thermalo Cooling Cars	A	PM	6/10/2004	0.0014	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	513	Thermalo Cooling Cars	A	PM	6/10/2004	0.0013	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	513	Thermalo Cooling Cars	A	PM	4/11/2003	0.0019	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	513	Thermalo Cooling Cars	A	PM	4/11/2003	0.0024	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	518	Probat Cold Chaff System	A	PM	3/8/2007	0.0025	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	518	Probat Cold Chaff System	A	PM	5/28/2004	0.002	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	517	Probat Destoner Cooling Cars	A	PM	6/11/2004	0.0017	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	517	Probat Destoner Cooling Cars	A	PM	6/11/2004	0.0014	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	517	Probat Destoner Cooling Cars	A	PM	4/23/2003	0.0018	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	517	Probat Destoner Cooling Cars	A	PM	4/18/2003	0.0014	GRAINS PER DRY STANDARD CUBIC FOOT	# 7
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	538	GFM Process	A	PM	3/8/2007	0.0073	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	538	GFM Process	A	PM	11/5/2003	0.00071	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	513	Thermalo Cooling Cars	A	PM	3/7/2007	0.004	GRAINS PER DRY STANDARD CUBIC FOOT	#2
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	513	Thermalo Cooling Cars	A	PM	3/6/2007	0.005	GRAINS PER DRY STANDARD CUBIC FOOT	#1 car
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	513	Thermalo Cooling Cars	A	PM	3/16/2006	0.0016	GRAINS PER DRY STANDARD CUBIC FOOT	#2 Thermalo cooling Car
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	550	GFM Drying Zone 1	A	PM	3/12/2007	0.0052	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	550	GFM Drying Zone 1	A	PM	10/31/2003	0.0054	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	550	GFM Drying Zone 1	A	PM	10/31/2003	0.0054	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	506	Batch Roasters	A	PM	9/10/2007	0.0172	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS		KRAFT FOODS,											GRAINS PER	

GLOBAL, MAXWELL HOUSE COFFEE	0310004	MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	506	Batch Roasters	A	PM	9/13/2007	0.0183	DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	506	Batch Roasters	A	PM	10/5/2007	0.0181	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	506	Batch Roasters	A	PM	8/23/2007	0.0181	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	506	Batch Roasters	A	PM	3/9/2007	0.0099	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	506	Batch Roasters	A	PM	3/7/2006	0.0184	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	509	Hot Chaff System	A	PM	6/14/2007	0.0137	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	509	Hot Chaff System	A	PM	6/28/2003	0.0114	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	519	Probat Scales	A	PM	3/15/2007	0.0043	GRAINS PER DRY STANDARD CUBIC FOOT	#3 PSC
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	519	Probat Scales	A	PM	3/17/2006	0.0015	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	519	Probat Scales	A	PM	3/1/2005	0.0012	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	519	Probat Scales	A	PM	6/23/2004	0.0012	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	519	Probat Scales	A	PM	4/14/2003	0.0011	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	505	Continuous Roaster	A	PM	5/26/2004	0.0089	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	507	Green Bean Separators	I	PM	6/26/2003	0.0012	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	530	SIG-VAC Packaging Machines	A	PM	5/25/2004	0.0016	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	540	Green Coffee Silo Airveying	A	PM	4/26/2007	0.0035	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	540	Green Coffee Silo Airveying	A	PM	2/5/2004	0.0015	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	552	GFM Drying Zone 3	A	PM	3/8/2007	0.0052	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	552	GFM Drying Zone 3	A	PM	11/4/2003	0.007	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	510	(22) Bunkers	A	PM	4/10/2007	0.0043	GRAINS PER DRY STANDARD CUBIC FOOT	Bunkers Baghouse
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	510	(22) Bunkers	A	PM	5/28/2004	0.0019	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	506	Batch Roasters	A	PM	3/29/2005	0.0058	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	506	Batch Roasters	A	PM	6/24/2004	0.09	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	506	Batch Roasters	A	PM	4/25/2003	0.0105	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	517	Probat Destoner Cooling Cars	A	PM	3/28/2007	0.0042	GRAINS PER DRY STANDARD CUBIC FOOT	#6
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	517	Probat Destoner Cooling Cars	A	PM	3/27/2007	0.0034	GRAINS PER DRY STANDARD CUBIC FOOT	#5 Probat Destoner cooling car
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	517	Probat Destoner Cooling Cars	A	PM	3/30/2006	0.0021	GRAINS PER DRY STANDARD CUBIC FOOT	#4 Probat Destoner Cooling Car
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	517	Probat Destoner Cooling Cars	A	PM	3/20/2006	0.0018	GRAINS PER DRY STANDARD CUBIC FOOT	#3 car
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	517	Probat Destoner Cooling Cars	A	PM	3/3/2005	0.0013	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	514	Thermalo Destoners	A	PM	3/15/2005	0.0022	GRAINS PER DRY STANDARD CUBIC FOOT	

KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	536	GFM Surge Bins	A	PM	6/1/2004	0.0023	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	541	Whole Roasted Bean Storage	A	PM	4/18/2007	0.0025	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	541	Whole Roasted Bean Storage	A	PM	5/27/2004	0.0018	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	504	Probat Roasters	A	PM	6/16/2004	0.0077	GRAINS PER DRY STANDARD CUBIC FOOT	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	520	Continuous Green Bean Feed System	A	PM	5/26/2004	0.0073	POUNDS/HOUR	
KRAFT FOODS GLOBAL, MAXWELL HOUSE COFFEE	0310004	KRAFT FOODS, MAXWELL HOUSE COFFEE	NEDV	DUVAL	A	Y	523	Continuous Destoner	A	PM	6/24/2004	0.11	POUNDS/HOUR	
ANCHOR GLASS CONTAINER CORPORATION	0310005	JACKSONVILLE PLANT 07	NEDV	DUVAL	A	Y	3	#3 GLASS MELTING FURNACE	A	NOX	2/13/2007	61.2	POUNDS/HOUR	
ANCHOR GLASS CONTAINER CORPORATION	0310005	JACKSONVILLE PLANT 07	NEDV	DUVAL	A	Y	4	#4 GLASS MELTING FURNACE	A	PM	10/1/2003	15.16	POUNDS/HOUR	
ANCHOR GLASS CONTAINER CORPORATION	0310005	JACKSONVILLE PLANT 07	NEDV	DUVAL	A	Y	4	#4 GLASS MELTING FURNACE	A	PM	9/10/2003	20.52	POUNDS/HOUR	
ANCHOR GLASS CONTAINER CORPORATION	0310005	JACKSONVILLE PLANT 07	NEDV	DUVAL	A	Y	4	#4 GLASS MELTING FURNACE	A	PM	9/29/2006	8.61	POUNDS/HOUR	
ANCHOR GLASS CONTAINER CORPORATION	0310005	JACKSONVILLE PLANT 07	NEDV	DUVAL	A	Y	4	#4 GLASS MELTING FURNACE	A	PM	9/29/2005	7.2	POUNDS/HOUR	
ANCHOR GLASS CONTAINER CORPORATION	0310005	JACKSONVILLE PLANT 07	NEDV	DUVAL	A	Y	4	#4 GLASS MELTING FURNACE	A	PM	11/8/2007	6.95	POUNDS/HOUR	
ANCHOR GLASS CONTAINER CORPORATION	0310005	JACKSONVILLE PLANT 07	NEDV	DUVAL	A	Y	3	#3 GLASS MELTING FURNACE	A	PM	9/11/2003	10.7	POUNDS/HOUR	
ANCHOR GLASS CONTAINER CORPORATION	0310005	JACKSONVILLE PLANT 07	NEDV	DUVAL	A	Y	3	#3 GLASS MELTING FURNACE	A	PM	2/13/2007	13.4	POUNDS/HOUR	
ANCHOR GLASS CONTAINER CORPORATION	0310005	JACKSONVILLE PLANT 07	NEDV	DUVAL	A	Y	3	#3 GLASS MELTING FURNACE	A	PM	9/30/2005	6.78	POUNDS/HOUR	
ANCHOR GLASS CONTAINER CORPORATION	0310005	JACKSONVILLE PLANT 07	NEDV	DUVAL	A	Y	3	#3 GLASS MELTING FURNACE	A	SO2	2/13/2007	17.08	POUNDS/HOUR	
ANCHOR GLASS CONTAINER CORPORATION	0310005	JACKSONVILLE PLANT 07	NEDV	DUVAL	A	Y	3	#3 GLASS MELTING FURNACE	A	PM	7/22/2004	11.77	POUNDS/HOUR	k&a eqd was not notifed of testing beforehand
ANCHOR GLASS CONTAINER CORPORATION	0310005	JACKSONVILLE PLANT 07	NEDV	DUVAL	A	Y	3	#3 GLASS MELTING FURNACE	A	PM	9/28/2006	7.66	POUNDS/HOUR	
ANCHOR GLASS CONTAINER CORPORATION	0310005	JACKSONVILLE PLANT 07	NEDV	DUVAL	A	Y	3	#3 GLASS MELTING FURNACE	A	PM	11/9/2007	8.74	POUNDS/HOUR	
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	3	BOILER #3 - FUEL OIL/NATURAL GAS/BIO-GAS	A	NOX	7/12/2006	12.5	POUNDS/HOUR	Test method 7E used (New Permit)
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	28	DUCT BURNER & HEAT RECOVERY BOILER	A	NOX	2/24/2005	5.2	POUNDS/HOUR	
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	28	DUCT BURNER & HEAT RECOVERY BOILER	A	NOX	2/27/2003	0.56	POUNDS/HOUR	
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	28	DUCT BURNER & HEAT RECOVERY BOILER	A	NOX	2/22/2006	0	POUNDS/HOUR	
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	1	BOILER #1 - FUEL OIL/NATURAL GAS/BIO-GAS	A	NOX	7/11/2006	14	POUNDS/HOUR	
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	4	BOILER #4 - FUEL OIL/NATURAL GAS/BIO-GAS	A	NOX	7/11/2006	11.9	POUNDS/HOUR	Test Method 7E used
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	2	BOILER #2 - FUEL OIL/NATURAL GAS/BIO-GAS	A	NOX	7/12/2006	13.4	POUNDS/HOUR	Test Method 7E used
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	33	H2S SCRUBBER FOR ANEROBIC TREATMENT FACILITY	A	H2S	2/28/2003	0	POUNDS/HOUR	
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	33	H2S SCRUBBER FOR ANEROBIC TREATMENT FACILITY	A	H2S	2/8/2007	0.004	POUNDS/HOUR	
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	28	DUCT BURNER & HEAT RECOVERY BOILER	A	NOX	2/7/2007	2.25	POUNDS/HOUR	
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	27	97.7 MMBTU/HR SOLAR MARS GAS-FIRED TURBINE	A	NOX	2/7/2007	142	PARTS PER MILLION DRY GAS VOLUME	
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	27	97.7 MMBTU/HR SOLAR MARS GAS-FIRED TURBINE	A	SO2	2/24/2005	0.33	PARTS PER MILLION DRY GAS VOLUME	
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	27	97.7 MMBTU/HR SOLAR MARS GAS-FIRED TURBINE	A	SO2	2/7/2007	1.8	PARTS PER MILLION DRY GAS VOLUME	
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	27	97.7 MMBTU/HR SOLAR MARS GAS-FIRED TURBINE	A	NOX	2/24/2005	123.6	PARTS PER MILLION DRY GAS VOLUME	
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	27	97.7 MMBTU/HR SOLAR MARS GAS-FIRED TURBINE	A	NOX	2/27/2003	78	PARTS PER MILLION DRY GAS VOLUME	
ANHEUSER BUSCH, INC. JACKSONVILLE	0310006	ANHEUSER BUSCH, INC. JACKSONVILLE	NEDV	DUVAL	A	Y	27	97.7 MMBTU/HR SOLAR MARS GAS-FIRED TURBINE	A	NOX	2/22/2006	135	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	3	NATCO COMBUSTION TURBINE GENERATOR (T-1)	A	NOX	3/16/2006	107.4	PARTS PER MILLION DRY GAS VOLUME	Sulfur content 0.8%
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	3	NATCO COMBUSTION TURBINE GENERATOR (T-1)	A	NOX	1/20/2004	97.3	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	5	SOLAR COMBUSTION TURBINE (T-2), NATURAL GAS FIRED, (#2 OIL)	A	NOX	1/22/2003	109.5	PARTS PER MILLION DRY GAS VOLUME	

BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	5	SOLAR COMBUSTION TURBINE (T-2), NATURAL GAS FIRED, (#2 OIL)	A	NOX	1/12/2005	113.2	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	5	SOLAR COMBUSTION TURBINE (T-2), NATURAL GAS FIRED, (#2 OIL)	A	NOX	2/14/2006	141	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	13	SOLAR H COMBUSTION GENERATOR T-4	A	NOX	1/20/2004	83.4	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	13	SOLAR H COMBUSTION GENERATOR T-4	A	NOX	1/22/2003	71.84	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	13	SOLAR H COMBUSTION GENERATOR T-4	A	NOX	1/11/2005	81.3	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	13	SOLAR H COMBUSTION GENERATOR T-4	A	NOX	2/14/2006	106	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	13	SOLAR H COMBUSTION GENERATOR T-4	A	NOX	1/17/2007	99.2	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	13	SOLAR H COMBUSTION GENERATOR T-4	A	NOX	2/12/2008	89.4	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	12	VALLEY COMBUSTION TURBINE GENERATOR T-3	A	NOX	1/20/2004	92.1	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	12	VALLEY COMBUSTION TURBINE GENERATOR T-3	A	NOX	1/21/2003	99.44	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	12	VALLEY COMBUSTION TURBINE GENERATOR T-3	A	NOX	1/11/2005	91.1	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	12	VALLEY COMBUSTION TURBINE GENERATOR T-3	A	NOX	3/16/2006	119	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	12	VALLEY COMBUSTION TURBINE GENERATOR T-3	A	NOX	1/17/2007	111.8	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	12	VALLEY COMBUSTION TURBINE GENERATOR T-3	A	NOX	2/13/2008	114	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	5	SOLAR COMBUSTION TURBINE (T-2), NATURAL GAS FIRED, (#2 OIL)	A	NOX	1/20/2004	115	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	3	NATCO COMBUSTION TURBINE GENERATOR (T-1)	A	NOX	1/21/2003	95.18	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	3	NATCO COMBUSTION TURBINE GENERATOR (T-1)	A	NOX	1/11/2005	97.9	PARTS PER MILLION DRY GAS VOLUME	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	3	NATCO COMBUSTION TURBINE GENERATOR (T-1)	A	NOX	1/16/2007	87.9	TONS/YEAR	test allowable 209 PPM Actual 107.7
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	5	SOLAR COMBUSTION TURBINE (T-2), NATURAL GAS FIRED, (#2 OIL)	A	NOX	3/4/2008	7.83	PERCENT BY VOLUME ON A DRY BASIS	
BAPTIST MEDICAL CENTER	0310010	BAPTIST MEDICAL CENTER	NEDV	DUVAL	A	Y	5	SOLAR COMBUSTION TURBINE (T-2), NATURAL GAS FIRED, (#2 OIL)	A	NOX	1/16/2007	12.6	PERCENT BY VOLUME ON A DRY BASIS	Allow 202 PPM Actual 169.3
SUPPORT TERMINAL OPERATING PART. L.P.	0310028	SUPPORT TERMINAL SERVICES, INC.	NEDV	DUVAL	A	Y	34	Loading Rack Operation - Annex II	A	VOC	4/18/2006	29.43	TONS/YEAR	Tst Team Jordan Alt TsT Method 40CFR 60.18
SUPPORT TERMINAL OPERATING PART. L.P.	0310028	SUPPORT TERMINAL SERVICES, INC.	NEDV	DUVAL	A	Y	23	Loading Rack Operation - Annex I	A	VOC	4/19/2006	22.16	TONS/YEAR	Tst Team Jordan Alt Meth 40CFR 60.18b 2.60 allowable is 265.18
SUPPORT TERMINAL OPERATING PART. L.P.	0310028	SUPPORT TERMINAL SERVICES, INC.	NEDV	DUVAL	A	Y	23	Loading Rack Operation - Annex I	A	VOC	1/8/2003	19.02	MILLIGRAMS PER LITER OF LIQUID LOADED	
SUPPORT TERMINAL OPERATING PART. L.P.	0310028	SUPPORT TERMINAL SERVICES, INC.	NEDV	DUVAL	A	Y	34	Loading Rack Operation - Annex II	A	VOC	1/9/2003	21.62	MILLIGRAMS PER LITER OF LIQUID LOADED	
SUPPORT TERMINAL OPERATING PART. L.P.	0310028	SUPPORT TERMINAL SERVICES, INC.	NEDV	DUVAL	A	Y	23	Loading Rack Operation - Annex I	A	VOC	4/24/2007	3.12	OTHER (SPECIFY IN COMMENT)	Alt Test Method 40CFR 60.18(b) Units ft/sec T Team Jordan Service Co.
SUPPORT TERMINAL OPERATING PART. L.P.	0310028	SUPPORT TERMINAL SERVICES, INC.	NEDV	DUVAL	A	Y	34	Loading Rack Operation - Annex II	A	VOC	4/25/2007	10.36	OTHER (SPECIFY IN COMMENT)	Alt Test Method 40CFR 60.18(b) Test Team Jo Services
SUPPORT TERMINAL OPERATING PART. L.P.	0310028	SUPPORT TERMINAL SERVICES, INC.	NEDV	DUVAL	A	Y	34	Loading Rack Operation - Annex II	A	VOC	4/26/2005	4.37	OTHER (SPECIFY IN COMMENT)	TEAM Jordan Ser. 4.35 FT/Sec. (Testing as pe CFR 60.18(b))
SUPPORT TERMINAL OPERATING PART. L.P.	0310028	SUPPORT TERMINAL SERVICES, INC.	NEDV	DUVAL	A	Y	23	Loading Rack Operation - Annex I	A	VOC	4/27/2005	1.13	OTHER (SPECIFY IN COMMENT)	1.13 FT. SEC. (Testing as per 40 CFR 60.18(b)
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	CO	3/14/2007	75.85	POUNDS/HOUR	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	CO	6/1/2007	208.63	PARTS PER MILLION DRY GAS VOLUME	Test Team Costal Air Consultants
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	CO	4/10/2006	0.0901	PARTS PER MILLION DRY GAS VOLUME	Tst Team Web&Leeper Method 10 used
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	CO	11/9/2006	258.01	PARTS PER MILLION DRY GAS VOLUME	Not Req Test Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	CO	11/8/2006	68.4	PARTS PER MILLION DRY GAS VOLUME	CO Not Required Test team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	CO	3/31/2007	148.22	PARTS PER MILLION DRY GAS VOLUME	Test Team Coastal Air Consulting , CO not req Value Per WW
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	CO	5/13/2004	37.22	POUNDS/HOUR	

JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	CO	1/9/2004	96.61	POUNDS/HOUR	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	CO	3/15/2005	65.6	POUNDS/HOUR	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	CO	3/8/2006	57.3	POUNDS/HOUR	Method 10 used Test Team, Grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	33	NGS - Limestone Dryers/Mills Building	A	PM	8/1/2003	0.0122	GRAINS PER DRY STANDARD CUBIC FOOT	METHOD 5
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	33	NGS - Limestone Dryers/Mills Building	A	PM	7/30/2003	0.0043	GRAINS PER DRY STANDARD CUBIC FOOT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	33	NGS - Limestone Dryers/Mills Building	A	PM	7/31/2003	0.0279	GRAINS PER DRY STANDARD CUBIC FOOT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	33	NGS - Limestone Dryers/Mills Building	A	PM	9/4/2003	0.0199	GRAINS PER DRY STANDARD CUBIC FOOT	method 5 used
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	33	NGS - Limestone Dryers/Mills Building	A	PM	9/17/2003	0.0179	GRAINS PER DRY STANDARD CUBIC FOOT	METHOD 5
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	33	NGS - Limestone Dryers/Mills Building	A	PM	10/8/2003	0.0063	GRAINS PER DRY STANDARD CUBIC FOOT	method 17
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	33	NGS - Limestone Dryers/Mills Building	A	PM	4/24/2003	0.0069	GRAINS PER DRY STANDARD CUBIC FOOT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	33	NGS - Limestone Dryers/Mills Building	A	PM	9/4/2003	0.0199	GRAINS PER DRY STANDARD CUBIC FOOT	METHOD 5 USED
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	SAM	10/24/2007	320.9	TEST REQUIRED (NO ALLOWABLE EMISSION)	Method 8 used Test Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	SAM	11/6/2006	545.2	TEST REQUIRED (NO ALLOWABLE EMISSION)	Test Method 8 Test team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	SAM	4/10/2006	278.5	TEST REQUIRED (NO ALLOWABLE EMISSION)	Method 8 used Test Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	SAM	10/23/2007	297.3	TEST REQUIRED (NO ALLOWABLE EMISSION)	Method 8 Used Test Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	SAM	11/7/2006	551.4	TEST REQUIRED (NO ALLOWABLE EMISSION)	Test method 8 Teat Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	33	NGS - Limestone Dryers/Mills Building	A	PM	4/25/2003	0.0056	GRAINS PER DRY STANDARD CUBIC FOOT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	33	NGS - Limestone Dryers/Mills Building	A	PM	9/19/2003	0.0053	GRAINS PER DRY STANDARD CUBIC FOOT	METHOD 5 USED
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	33	NGS - Limestone Dryers/Mills Building	A	PM	9/5/2003	0.018	GRAINS PER DRY STANDARD CUBIC FOOT	method 5 used
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	VOC	6/19/2007	3.75	POUNDS/HOUR	Test Team Grace Consultants
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	CO	3/7/2006	25.2	POUNDS/HOUR	Test Method 10 Test Team , Grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	CO	6/15/2005	51	POUNDS/HOUR	TEST TEAM GCI METHOD 10
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	CO	8/27/2003	58.3	POUNDS/HOUR	method 10
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	CO	2/16/2005	61.08	POUNDS/HOUR	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	VOC	6/20/2007	3.67	POUNDS/HOUR	Test Team Grace Consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	CO	3/13/2007	61.5	POUNDS/HOUR	Method 10 used Test Team, Grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	35	NGS - Limestone Silos Bin Vent Filters	A	PM	9/4/2003	0.58	PERCENT OPACITY	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	SO2	3/8/2006	0.157	POUNDS PER BILLION BTU HEAT INPUT	Method 6C used Test Team, Grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	SO2	6/15/2005	0.0564	POUNDS PER BILLION BTU HEAT INPUT	TEST TEAM CGI METHOD 6C
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	SO2	3/13/2007	0.151	POUNDS PER BILLION BTU HEAT INPUT	Method 6C Test Team Grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	SO2	3/7/2006	0.13	POUNDS PER BILLION BTU HEAT INPUT	Test Method 6c Test Team, Grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	SO2	2/16/2005	0.082	POUNDS PER BILLION BTU HEAT INPUT	grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	SO2	8/27/2003	0.057	POUNDS PER BILLION BTU HEAT INPUT	method 6c
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	SO2	3/14/2007	0.148	POUNDS PER BILLION BTU HEAT INPUT	Method 6C used Test Team Grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	SO2	3/15/2005	0.158	POUNDS PER BILLION BTU HEAT INPUT	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	34	NGS - Limestone Prep Building Dust Collectors x 3	A	PM	2/17/2005	0.98	PERCENT OPACITY	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	34	NGS - Limestone Prep Building Dust Collectors x 3	A	PM	2/18/2005	1.12	PERCENT OPACITY	GRACE C. LIMESTONE PREP.
								SJRPP Boiler No. 2 (Phase I					POUNDS PER	

JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	& II Acid Rain Unit)	A	PM	6/11/2003	0.005	MILLION BTU HEAT INPUT	Grace, PM10 .003lb/mmBtu
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	PM	10/27/2003	0.003	POUNDS PER MILLION BTU HEAT INPUT	costal air
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	PM	11/1/2004	0.0022	POUNDS PER MILLION BTU HEAT INPUT	CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	PM	11/7/2005	0.0032	POUNDS PER MILLION BTU HEAT INPUT	Test Team Costal Air
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	PM	4/10/2006	0.0054	POUNDS PER MILLION BTU HEAT INPUT	Tst Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	PM	11/6/2006	0.0083	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	PM	10/24/2007	0.0026	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	SO2	1/9/2004	0.095	POUNDS PER BILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	34	NGS - Limestone Prep Building Dust Collectors x 3	A	PM	2/15/2005	0.93	PERCENT OPACITY	GRACE METHON E.P.A. 5
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	NOX	1/9/2004	0.088	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	NOX	3/15/2005	0.077	POUNDS PER MILLION BTU HEAT INPUT	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	NOX	5/13/2004	0.05	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	NOX	3/8/2006	0.08	POUNDS PER MILLION BTU HEAT INPUT	TsT Team Grace Method 7E used
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	NOX	3/14/2007	0.07	POUNDS PER MILLION BTU HEAT INPUT	Method 7E used Test Team, Grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	NOX	10/29/2003	0.44	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	NOX	10/29/2003	0.441	POUNDS PER MILLION BTU HEAT INPUT	costal air
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	NOX	11/3/2004	0.474	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	NOX	11/9/2005	0.3457	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	NOX	4/10/2006	0.4406	POUNDS PER MILLION BTU HEAT INPUT	Tst Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	NOX	11/9/2006	0.477	POUNDS PER MILLION BTU HEAT INPUT	Tst Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	PM	10/27/2003	0.003	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM10	6/11/2003	0.003	POUNDS PER MILLION BTU HEAT INPUT	grace consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM10	12/12/2003	0.002	POUNDS PER MILLION BTU HEAT INPUT	grace.
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM10	11/23/2004	0.002	POUNDS PER MILLION BTU HEAT INPUT	Grace Consultants
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM10	6/4/2005	0.002	POUNDS PER MILLION BTU HEAT INPUT	Test Team Grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM10	3/9/2004	0.003	POUNDS PER MILLION BTU HEAT INPUT	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM10	8/19/2004	0.004	POUNDS PER MILLION BTU HEAT INPUT	grace consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM10	5/21/2004	0.002	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM10	2/23/2006	0.0012	POUNDS PER MILLION BTU HEAT INPUT	Test Team Grace Consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM10	2/28/2007	0.0006	POUNDS PER MILLION BTU HEAT INPUT	Test team Grace Consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	NOX	3/2/2005	0.432	POUNDS PER MILLION BTU HEAT INPUT	gci
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	NOX	5/4/2005	0.263	POUNDS PER MILLION BTU HEAT INPUT	Test Team GE Energy
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	NOX	7/19/2006	0.3	POUNDS PER MILLION BTU HEAT INPUT	N/A On Tst allowable Test Team GCI
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	NOX	6/22/2007	0.288	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM10	9/19/2003	0.006	POUNDS PER MILLION BTU HEAT INPUT	grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM10	10/16/2003	0.004	POUNDS PER MILLION BTU HEAT INPUT	GRACE CONSULTING
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM10	10/7/2003	0.005	POUNDS PER MILLION BTU HEAT INPUT	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM10	9/25/2003	0.003	POUNDS PER MILLION BTU HEAT INPUT	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM10	10/28/2003	0.003	POUNDS PER MILLION BTU HEAT INPUT	grace

JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM	3/25/2004	0.004	POUNDS PER MILLION BTU HEAT INPUT	grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM	5/20/2004	0.005	POUNDS PER MILLION BTU HEAT INPUT	grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM	2/22/2006	0.0037	POUNDS PER MILLION BTU HEAT INPUT	Test Team Grace Consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM	2/27/2007	0.0036	POUNDS PER MILLION BTU HEAT INPUT	Test Team Grace consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	SO2	8/29/2003	1.586	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	SO2	12/13/2003	1.476	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	SO2	5/23/2003	1.643	POUNDS PER MILLION BTU HEAT INPUT	# 3 power boiler
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	SO2	3/2/2005	0.785	POUNDS PER MILLION BTU HEAT INPUT	gci
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	SO2	5/4/2005	1.48	POUNDS PER MILLION BTU HEAT INPUT	Test Team GE Energy
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	NOX	10/29/2003	0.564	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	NOX	10/30/2003	0.564	POUNDS PER MILLION BTU HEAT INPUT	costal
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	NOX	11/10/2005	0.3696	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	NOX	11/8/2006	0.408	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	NOX	3/31/2007	0.431	POUNDS PER MILLION BTU HEAT INPUT	Method 7E Test Team Coastal Air Consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	NOX	6/1/2007	0.585	POUNDS PER MILLION BTU HEAT INPUT	Test Team Costal Air Consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	NOX	10/25/2007	0.4967	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM	9/19/2003	0.007	POUNDS PER MILLION BTU HEAT INPUT	grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM	10/16/2003	0.003	POUNDS PER MILLION BTU HEAT INPUT	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	PM	9/26/2003	0.079	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	PM	9/26/2003	0.147	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	PM	6/16/2005	0.143	POUNDS PER MILLION BTU HEAT INPUT	Test Team GCI Whitt Vineyard
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	PM	6/15/2005	0.081	POUNDS PER MILLION BTU HEAT INPUT	Test Team GCI
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	PM	5/5/2004	0.077	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	PM	6/15/2006	0.142	POUNDS PER MILLION BTU HEAT INPUT	Test Team GCI
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	PM	7/18/2006	0.052	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	PM	7/11/2007	0.06	POUNDS PER MILLION BTU HEAT INPUT	Test Team, Grace consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	PM	7/10/2007	0.053	POUNDS PER MILLION BTU HEAT INPUT	test Team, Grace Consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	PM	10/27/2003	0.003	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	PM	10/28/2003	0.0028	POUNDS PER MILLION BTU HEAT INPUT	COSTAL AIR
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	PM	11/2/2004	0.0033	POUNDS PER MILLION BTU HEAT INPUT	CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	PM	11/8/2005	0.0017	POUNDS PER MILLION BTU HEAT INPUT	Test Team Costal Air
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	PM	11/7/2006	0.0041	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	PM	10/23/2007	0.0032	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	SO2	10/29/2003	0.412	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	SO2	10/29/2003	0.413	POUNDS PER MILLION BTU HEAT INPUT	costal air
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	SO2	11/3/2004	0.485	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	SO2	11/9/2005	0.4089	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	SO2	4/10/2006	0.5213	POUNDS PER MILLION BTU HEAT INPUT	
													POUNDS PER	

JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	SO2	11/9/2006	0.398	MILLION BTU HEAT INPUT	TsT Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	17	SJRPP Boiler No. 2 (Phase I & II Acid Rain Unit)	A	SO2	10/24/2007	0.1501	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	SO2	10/29/2003	0.418	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	SO2	10/30/2003	0.418	POUNDS PER MILLION BTU HEAT INPUT	costal testers
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	SO2	11/4/2004	0.484	POUNDS PER MILLION BTU HEAT INPUT	CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	SO2	11/4/2004	0.484	POUNDS PER MILLION BTU HEAT INPUT	CAC Webb,Righter,Smith
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	SO2	11/10/2005	0.4626	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	SO2	11/8/2006	0.432	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	SO2	3/31/2007	0.429	POUNDS PER MILLION BTU HEAT INPUT	Method 6C Test Team Coastal Ait Consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	SO2	6/1/2007	0.423	POUNDS PER MILLION BTU HEAT INPUT	Test Team Costal Air Consuling
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	16	SJRPP Boiler No. 1 (Phase I & II Acid Rain Unit)	A	SO2	10/25/2007	0.0303	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM	10/7/2003	0.006	POUNDS PER MILLION BTU HEAT INPUT	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM	9/25/2003	0.005	POUNDS PER MILLION BTU HEAT INPUT	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM	10/28/2003	0.005	POUNDS PER MILLION BTU HEAT INPUT	grace.
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM	2/28/2003	0.0087	POUNDS PER MILLION BTU HEAT INPUT	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM	2/28/2003	0.0043	POUNDS PER MILLION BTU HEAT INPUT	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM	3/3/2005	0.0044	POUNDS PER MILLION BTU HEAT INPUT	grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM	8/19/2004	0.004	POUNDS PER MILLION BTU HEAT INPUT	grace consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM	3/25/2004	0.005	POUNDS PER MILLION BTU HEAT INPUT	grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	SO2	7/19/2006	1.373	POUNDS PER MILLION BTU HEAT INPUT	TestTeam GCI
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	SO2	6/22/2007	1.375	POUNDS PER MILLION BTU HEAT INPUT	Test Team Grace Consultants
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	NOX	8/27/2003	0.088	POUNDS PER MILLION BTU HEAT INPUT	method 7e
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	NOX	6/15/2005	0.0672	POUNDS PER MILLION BTU HEAT INPUT	TEST TEAM CGI METHOD 7E
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	NOX	2/16/2005	0.082	POUNDS PER MILLION BTU HEAT INPUT	grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	NOX	3/7/2006	0.072	POUNDS PER MILLION BTU HEAT INPUT	Test Method 7E Test Team Grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	NOX	3/13/2007	0.051	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	3	NGS Boiler No. 3 (Phase II Acid Rain Unit)	A	NOX	12/13/2003	0.437	POUNDS PER MILLION BTU HEAT INPUT	Annual RATA results; CEMS 30-day rolling average is actual compliance standard - no viol
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM10	3/3/2005	0.0025	POUNDS PER MILLION BTU HEAT INPUT	grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM10	8/19/2004	0.003	POUNDS PER MILLION BTU HEAT INPUT	grace consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM10	5/20/2004	0.003	POUNDS PER MILLION BTU HEAT INPUT	grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM10	2/22/2006	0.0026	POUNDS PER MILLION BTU HEAT INPUT	Test Team Grace Consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	26	NGS - Circulating Fluidized Bed Boiler No. 2	A	PM10	2/27/2007	0.0031	POUNDS PER MILLION BTU HEAT INPUT	Test Team grace Consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM10	9/18/2003	0.003	POUNDS PER MILLION BTU HEAT INPUT	grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM10	9/17/2003	0.005	POUNDS PER MILLION BTU HEAT INPUT	grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM10	9/24/2003	0.004	POUNDS PER MILLION BTU HEAT INPUT	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM	9/18/2003	0.007	POUNDS PER MILLION BTU HEAT INPUT	grace consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM	9/17/2003	0.007	POUNDS PER MILLION BTU HEAT INPUT	grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM	9/24/2003	0.005	POUNDS PER MILLION BTU HEAT INPUT	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized	A	PM	6/11/2003	0.0053	POUNDS PER MILLION BTU	grace

								Bed Boiler No. 1					HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM	12/12/2003	0.004	POUNDS PER MILLION BTU HEAT INPUT	grace consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM	2/27/2003	0.003	POUNDS PER MILLION BTU HEAT INPUT	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM	2/27/2003	0.0037	POUNDS PER MILLION BTU HEAT INPUT	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM	3/9/2004	0.005	POUNDS PER MILLION BTU HEAT INPUT	grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM	11/23/2004	0.004	POUNDS PER MILLION BTU HEAT INPUT	Test Team Grace consultants
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM	6/14/2005	0.003	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM	3/9/2004	0.005	POUNDS PER MILLION BTU HEAT INPUT	GRACE
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM	8/19/2004	0.005	POUNDS PER MILLION BTU HEAT INPUT	grace consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM	5/21/2004	0.005	POUNDS PER MILLION BTU HEAT INPUT	grace
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM	2/23/2006	0.0013	POUNDS PER MILLION BTU HEAT INPUT	Test Team Grace Consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	PM	2/28/2007	0.0006	POUNDS PER MILLION BTU HEAT INPUT	Test Team Grace Consulting
JEA	0310045	NORTHSIDE/SJRPP	NEDV	DUVAL	A	Y	27	NGS - Circulating Fluidized Bed Boiler No. 1	A	SO2	5/13/2004	0.076	POUNDS PER MILLION BTU HEAT INPUT	
JEA	0310047	KENNEDY	NEDV	DUVAL	A	Y	15	170 MW Simple Cycle Combustion Turbine # 7	A	CO	9/27/2007	0.064	PARTS PER MILLION DRY GAS VOLUME	Test Team Costal Air
JEA	0310047	KENNEDY	NEDV	DUVAL	A	Y	15	170 MW Simple Cycle Combustion Turbine # 7	A	CO	7/31/2006	0.24	PARTS PER MILLION DRY GAS VOLUME	Test Team CAC ,Webb Leeper
JEA	0310047	KENNEDY	NEDV	DUVAL	A	Y	15	170 MW Simple Cycle Combustion Turbine # 7	A	CO	7/22/2004	1.23	PARTS PER MILLION DRY GAS VOLUME	
JEA	0310047	KENNEDY	NEDV	DUVAL	A	Y	15	170 MW Simple Cycle Combustion Turbine # 7	A	CO	7/18/2003	1.05	PARTS PER MILLION DRY GAS VOLUME	
JEA	0310047	KENNEDY	NEDV	DUVAL	A	Y	15	170 MW Simple Cycle Combustion Turbine # 7	A	CO	10/6/2005	0.15	PARTS PER MILLION DRY GAS VOLUME	Test Tean CAC
JEA	0310047	KENNEDY	NEDV	DUVAL	A	Y	15	170 MW Simple Cycle Combustion Turbine # 7	A	NOX	9/27/2007	8.32	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team Costal Air
JEA	0310047	KENNEDY	NEDV	DUVAL	A	Y	15	170 MW Simple Cycle Combustion Turbine # 7	A	NOX	10/6/2005	9.33	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team CAC
JEA	0310047	KENNEDY	NEDV	DUVAL	A	Y	15	170 MW Simple Cycle Combustion Turbine # 7	A	NOX	7/31/2006	9.13	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Method 7E used Test Team CAC ,Webb,Leeper
JEA	0310047	KENNEDY	NEDV	DUVAL	A	Y	15	170 MW Simple Cycle Combustion Turbine # 7	A	NOX	7/18/2003	9.56	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
JEA	0310047	KENNEDY	NEDV	DUVAL	A	Y	15	170 MW Simple Cycle Combustion Turbine # 7	A	NOX	7/22/2004	10.17	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
OWENS-CORNING	0310050	OWENS-CORNING, JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	12	ASPHALT BLOWING STILL NOS. 1 & 2	A	PM	10/25/2007	0.0402	POUNDS PER TON OF PRODUCT	Test Team Lehder Env Ser
OWENS-CORNING	0310050	OWENS-CORNING, JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	12	ASPHALT BLOWING STILL NOS. 1 & 2	A	PM	11/16/2006	0.533	POUNDS PER TON OF PRODUCT	
OWENS-CORNING	0310050	OWENS-CORNING, JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	5	ASPHALT COATER	A	PM	11/14/2003	0.063	POUNDS PER TON OF PRODUCT	lehder env.
OWENS-CORNING	0310050	OWENS-CORNING, JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	5	ASPHALT COATER	A	PM	11/19/2004	0.021	POUNDS PER TON OF PRODUCT	
OWENS-CORNING	0310050	OWENS-CORNING, JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	5	ASPHALT COATER	A	PM	11/16/2005	0.001	POUNDS PER TON OF PRODUCT	
OWENS-CORNING	0310050	OWENS-CORNING, JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	5	ASPHALT COATER	A	PM	11/15/2006	0.004	POUNDS PER TON OF PRODUCT	Test Team Lehder Env. Ser.
OWENS-CORNING	0310050	OWENS-CORNING, JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	12	ASPHALT BLOWING STILL NOS. 1 & 2	A	PM	11/12/2003	0.93	POUNDS PER TON OF PRODUCT	lehder env. serv. allowable emisssions on sheet 23.3 #/hr
OWENS-CORNING	0310050	OWENS-CORNING, JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	12	ASPHALT BLOWING STILL NOS. 1 & 2	A	PM	11/16/2005	0.42	POUNDS PER TON OF PRODUCT	Test Team Lehder Env. Serv.
OWENS-CORNING	0310050	OWENS-CORNING, JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	34	Asphalt Coater System No. 2	C	PM	10/24/2007	0.0008	KILOGRAMS PER MEGAGRAM OF SOLVENT FEED	Test Team Lehder Env. Serv
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0310067	D/B/A SMURFIT-STONE CONTAINER CORPORATIO	NEDV	DUVAL	A	Y	26	NATURAL GAS/#2 FO FIRED PKG STEAM BOILER (#3 OF 3 BOILERS)	A	NOX	4/5/2007	0.0925	POUNDS PER MILLION BTU HEAT INPUT	Test Team ESS
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0310067	D/B/A SMURFIT-STONE CONTAINER CORPORATIO	NEDV	DUVAL	A	Y	26	NATURAL GAS/#2 FO FIRED PKG STEAM BOILER (#3 OF 3 BOILERS)	A	NOX	4/6/2004	0.129	POUNDS PER MILLION BTU HEAT INPUT	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0310067	D/B/A SMURFIT-STONE CONTAINER CORPORATIO	NEDV	DUVAL	A	Y	26	NATURAL GAS/#2 FO FIRED PKG STEAM BOILER (#3 OF 3 BOILERS)	A	NOX	3/25/2003	0.116	POUNDS PER MILLION BTU HEAT INPUT	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0310067	D/B/A SMURFIT-STONE CONTAINER CORPORATIO	NEDV	DUVAL	A	Y	26	NATURAL GAS/#2 FO FIRED PKG STEAM BOILER (#3 OF 3	A	NOX	4/26/2005	0.09	POUNDS PER MILLION BTU HEAT INPUT	E.S.S.

								BOILERS)						
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0310067	D/B/A SMURFIT-STONE CONTAINER CORPORATIO	NEDV	DUVAL	A	Y	22	NATURAL GAS/#2 FO FIRED PKG STEAM BOILER (#1 OF 3 BOILERS)	A	NOX	4/25/2006	0.083	POUNDS PER MILLION BTU HEAT INPUT	Test Team ESS
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0310067	D/B/A SMURFIT-STONE CONTAINER CORPORATIO	NEDV	DUVAL	A	Y	22	NATURAL GAS/#2 FO FIRED PKG STEAM BOILER (#1 OF 3 BOILERS)	A	NOX	4/27/2005	0.134	POUNDS PER MILLION BTU HEAT INPUT	E.S.S.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0310067	D/B/A SMURFIT-STONE CONTAINER CORPORATIO	NEDV	DUVAL	A	Y	22	NATURAL GAS/#2 FO FIRED PKG STEAM BOILER (#1 OF 3 BOILERS)	A	NOX	3/24/2003	0.133	POUNDS PER MILLION BTU HEAT INPUT	enviro source samples
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0310067	D/B/A SMURFIT-STONE CONTAINER CORPORATIO	NEDV	DUVAL	A	Y	22	NATURAL GAS/#2 FO FIRED PKG STEAM BOILER (#1 OF 3 BOILERS)	A	NOX	4/6/2004	0.119	POUNDS PER MILLION BTU HEAT INPUT	e s s graham
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0310067	D/B/A SMURFIT-STONE CONTAINER CORPORATIO	NEDV	DUVAL	A	Y	22	NATURAL GAS/#2 FO FIRED PKG STEAM BOILER (#1 OF 3 BOILERS)	A	NOX	4/4/2007	0.0852	POUNDS PER MILLION BTU HEAT INPUT	Test Team ESS
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0310067	D/B/A SMURFIT-STONE CONTAINER CORPORATIO	NEDV	DUVAL	A	Y	26	NATURAL GAS/#2 FO FIRED PKG STEAM BOILER (#3 OF 3 BOILERS)	A	NOX	4/25/2006	0.101	POUNDS PER MILLION BTU HEAT INPUT	Tst Team ESS
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0310067	D/B/A SMURFIT-STONE CONTAINER CORPORATIO	NEDV	DUVAL	A	Y	23	NATURAL GAS/#2 FO FIRED PKG STEAM BOILER (#2 OF 3 BOILERS)	A	NOX	4/4/2007	0.0822	POUNDS PER MILLION BTU HEAT INPUT	Test Team ESS
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0310067	D/B/A SMURFIT-STONE CONTAINER CORPORATIO	NEDV	DUVAL	A	Y	23	NATURAL GAS/#2 FO FIRED PKG STEAM BOILER (#2 OF 3 BOILERS)	A	NOX	4/26/2006	0.058	POUNDS PER MILLION BTU HEAT INPUT	TST Team ESS
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0310067	D/B/A SMURFIT-STONE CONTAINER CORPORATIO	NEDV	DUVAL	A	Y	23	NATURAL GAS/#2 FO FIRED PKG STEAM BOILER (#2 OF 3 BOILERS)	A	NOX	4/26/2005	0.087	POUNDS PER MILLION BTU HEAT INPUT	E.S.S.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0310067	D/B/A SMURFIT-STONE CONTAINER CORPORATIO	NEDV	DUVAL	A	Y	23	NATURAL GAS/#2 FO FIRED PKG STEAM BOILER (#2 OF 3 BOILERS)	A	NOX	4/6/2004	0.136	POUNDS PER MILLION BTU HEAT INPUT	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0310067	D/B/A SMURFIT-STONE CONTAINER CORPORATIO	NEDV	DUVAL	A	Y	23	NATURAL GAS/#2 FO FIRED PKG STEAM BOILER (#2 OF 3 BOILERS)	A	NOX	3/24/2003	0.125	POUNDS PER MILLION BTU HEAT INPUT	
ST VINCENTS MEDICAL CENTER	0310068	ST VINCENTS MEDICAL CENTER	NEDV	DUVAL	A	Y	5	GAS TURBINE COGENERATOR NO. 1	A	NOX	2/6/2008	110.3	PARTS PER MILLION DRY GAS VOLUME	
ST VINCENTS MEDICAL CENTER	0310068	ST VINCENTS MEDICAL CENTER	NEDV	DUVAL	A	Y	5	GAS TURBINE COGENERATOR NO. 1	A	NOX	2/8/2006	190.4	PARTS PER MILLION DRY GAS VOLUME	
ST VINCENTS MEDICAL CENTER	0310068	ST VINCENTS MEDICAL CENTER	NEDV	DUVAL	A	Y	5	GAS TURBINE COGENERATOR NO. 1	A	NOX	2/12/2003	133.08	PARTS PER MILLION DRY GAS VOLUME	
ST VINCENTS MEDICAL CENTER	0310068	ST VINCENTS MEDICAL CENTER	NEDV	DUVAL	A	Y	5	GAS TURBINE COGENERATOR NO. 1	A	NOX	11/16/2005	106	PARTS PER MILLION DRY GAS VOLUME	
ST VINCENTS MEDICAL CENTER	0310068	ST VINCENTS MEDICAL CENTER	NEDV	DUVAL	A	Y	5	GAS TURBINE COGENERATOR NO. 1	A	NOX	2/7/2007	104.7	PARTS PER MILLION DRY GAS VOLUME	
ST VINCENTS MEDICAL CENTER	0310068	ST VINCENTS MEDICAL CENTER	NEDV	DUVAL	A	Y	1	NATURAL GAS FIRED MEDICAL WASTE INCINERATOR	I	DIOX	8/14/2003	378	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
ST VINCENTS MEDICAL CENTER	0310068	ST VINCENTS MEDICAL CENTER	NEDV	DUVAL	A	Y	1	NATURAL GAS FIRED MEDICAL WASTE INCINERATOR	I	DIOX	8/14/2003	380.67	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
ST VINCENTS MEDICAL CENTER	0310068	ST VINCENTS MEDICAL CENTER	NEDV	DUVAL	A	Y	1	NATURAL GAS FIRED MEDICAL WASTE INCINERATOR	I	DIOX	11/19/2003	600.6	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	custom stack analysis
ST VINCENTS MEDICAL CENTER	0310068	ST VINCENTS MEDICAL CENTER	NEDV	DUVAL	A	Y	1	NATURAL GAS FIRED MEDICAL WASTE INCINERATOR	I	PM	8/14/2003	0.0022	GRAINS PER DRY STANDARD CUBIC FOOT	
UNITED STATES GYPSUM CO.	0310072	JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	61	NO. 3 BOARD PLANT STUCCO ELEVATOR, SCREEN, & ADDITIVE SCREWS	A	PM	7/18/2006	0.0024	GRAINS PER DRY STANDARD CUBIC FOOT	
UNITED STATES GYPSUM CO.	0310072	JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	48	ROTARY ROCK DRYER	A	PM	7/17/2006	0.0038	GRAINS PER DRY STANDARD CUBIC FOOT	West BH
UNITED STATES GYPSUM CO.	0310072	JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	63	NO. 3 BOARD PLANT END SAWS	A	PM	7/19/2006	0.0037	GRAINS PER DRY STANDARD CUBIC FOOT	
UNITED STATES GYPSUM CO.	0310072	JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	48	ROTARY ROCK DRYER	A	PM	7/20/2006	0.0036	GRAINS PER DRY STANDARD CUBIC FOOT	East Bh
METAL CONTAINER CORPORATION	0310097	METAL CONTAINER CORP0RATION	NEDV	DUVAL	A	Y	13	Can Coating Lines Nos. 2,3,4, and 5	A	VOC	5/3/2007	1.3	POUNDS/HOUR	79% process rate
METAL CONTAINER CORPORATION	0310097	METAL CONTAINER CORP0RATION	NEDV	DUVAL	A	Y	13	Can Coating Lines Nos. 2,3,4, and 5	A	VOC	5/14/2004	0.94	POUNDS/HOUR	DEEECO
METAL CONTAINER CORPORATION	0310097	METAL CONTAINER CORP0RATION	NEDV	DUVAL	A	Y	13	Can Coating Lines Nos. 2,3,4, and 5	A	VOC	5/24/2006	1.29	POUNDS/HOUR	
METAL CONTAINER CORPORATION	0310097	METAL CONTAINER CORP0RATION	NEDV	DUVAL	A	Y	13	Can Coating Lines Nos. 2,3,4, and 5	A	VOC	5/3/2005	0.71	POUNDS/HOUR	
METAL CONTAINER CORPORATION	0310097	METAL CONTAINER CORP0RATION	NEDV	DUVAL	A	Y	13	Can Coating Lines Nos. 2,3,4, and 5	A	VOC	5/29/2003	1.76	POUNDS/HOUR	deeco
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	PB	4/19/2007	0.013	POUNDS/HOUR	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	PB	4/8/2004	0.17	POUNDS/HOUR	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	PB	4/21/2005	0.16	POUNDS/HOUR	
GERDAU		GERDAU						BILLET REHEAT						

AMERISTEEL JACKSONVILLE MILL DIV.	0310157	AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	PM	4/20/2007	1.23	POUNDS/HOUR	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	BILLET REHEAT FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	PM	6/12/2006	2.76	POUNDS/HOUR	Failed test retested on 6/16/06 and passed
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	BILLET REHEAT FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	PM	3/22/2005	0.85	POUNDS/HOUR	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	BILLET REHEAT FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	PM	6/6/2003	1.32	POUNDS/HOUR	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	BILLET REHEAT FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	PM	5/6/2004	1.52	POUNDS/HOUR	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	BILLET REHEAT FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	PM	6/16/2006	0.78	POUNDS/HOUR	Retest of failed 6/12/06 PM test
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	PB	3/8/2006	0.17	POUNDS/HOUR	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	BILLET REHEAT FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	CO	4/20/2007	0.001	POUNDS PER MILLION BTU HEAT INPUT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	BILLET REHEAT FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	CO	5/6/2004	0.007	POUNDS PER MILLION BTU HEAT INPUT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	BILLET REHEAT FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	NOX	6/12/2006	0.1	POUNDS PER MILLION BTU HEAT INPUT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	BILLET REHEAT FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	NOX	3/22/2005	0.11	POUNDS PER MILLION BTU HEAT INPUT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	BILLET REHEAT FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	NOX	6/6/2003	0.1227	POUNDS PER MILLION BTU HEAT INPUT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	BILLET REHEAT FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	NOX	5/6/2004	0.097	POUNDS PER MILLION BTU HEAT INPUT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	BILLET REHEAT FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	NOX	4/20/2007	0.12	POUNDS PER MILLION BTU HEAT INPUT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	BILLET REHEAT FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	CO	6/6/2003	0.0003	POUNDS PER MILLION BTU HEAT INPUT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	BILLET REHEAT FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	CO	3/22/2005	0.001	POUNDS PER MILLION BTU HEAT INPUT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	2	BILLET REHEAT FURNACE, NO BAGHOUSE, NAT. GAS, PROPANE BACKUP	A	CO	6/12/2006	0.005	POUNDS PER MILLION BTU HEAT INPUT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	8	Melt Shop: Electric Arc Furnace	A	PM	2/15/2008	0.0008	GRAINS PER DRY STANDARD CUBIC FOOT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	PM	4/19/2007	0.0002	GRAINS PER DRY STANDARD CUBIC FOOT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	PM	3/8/2006	0.0013	GRAINS PER DRY STANDARD CUBIC FOOT	combined
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	PM	4/21/2005	0.0023	GRAINS PER DRY STANDARD CUBIC FOOT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	PM	4/8/2004	0.0014	GRAINS PER DRY STANDARD CUBIC FOOT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	PM	4/8/2004	0.0018	GRAINS PER DRY STANDARD CUBIC FOOT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	8	Melt Shop: Electric Arc Furnace	A	NOX	2/15/2008	0.13	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	CO	4/8/2004	0.8	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	8	Melt Shop: Electric Arc Furnace	A	CO	2/15/2008	0.83	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	VOC	4/19/2007	0.054	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	VOC	4/21/2005	0.253	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	NOX	4/8/2004	0.13	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	NOX	4/21/2005	0.136	POUNDS PER TON OF PRODUCT	

GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	NOX	3/8/2006	0.09	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	NOX	4/19/2007	0.127	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	VOC	4/8/2004	0.04	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	VOC	4/8/2004	0.15	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	VOC	4/8/2004	0.11	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	VOC	3/8/2006	0.14	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	8	Melt Shop: Electric Arc Furnace	A	VOC	2/15/2008	0.02	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	8	Melt Shop: Electric Arc Furnace	A	PB	2/15/2008	0.0002	POUNDS PER TON OF PRODUCT	test method 12
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	CO	4/8/2004	1.5	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	CO	4/19/2007	2.42	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	CO	4/21/2005	1.98	POUNDS PER TON OF PRODUCT	
GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	0310157	GERDAU AMERISTEEL JACKSONVILLE MILL DIV.	NEDV	DUVAL	A	Y	1	Electric Arc Furnace	A	CO	3/8/2006	1.85	POUNDS PER TON OF PRODUCT	
JEA	0310166	BUCKMAN ST. WASTEWATER TREATMENT PLANT	NEDV	DUVAL	A	Y	7	SLUDGE DRUM DRYER	C	PM	4/17/2003	0.47	POUNDS/HOUR	
HESS CORPORATION	0310180	HESS - JACKSONVILLE TERMINAL	NEDV	DUVAL	A	Y	5	SIX BAY TANK TRUCK LOADING RACK	A	VOC	11/5/2003	2.43	MILLIGRAMS PER LITER OF LIQUID LOADED	the jordan service company 2820 s.english stati rd. louisville ku. 40299
HESS CORPORATION	0310180	HESS - JACKSONVILLE TERMINAL	NEDV	DUVAL	A	Y	5	SIX BAY TANK TRUCK LOADING RACK	A	VOC	11/16/2005	4.23	MILLIGRAMS PER LITER OF LIQUID LOADED	Test Team J. Jordan ser.CO.
HESS CORPORATION	0310180	HESS - JACKSONVILLE TERMINAL	NEDV	DUVAL	A	Y	5	SIX BAY TANK TRUCK LOADING RACK	A	VOC	11/8/2006	6.14	MILLIGRAMS PER LITER OF LIQUID LOADED	Test Team J.Jordan service Company
HESS CORPORATION	0310180	HESS - JACKSONVILLE TERMINAL	NEDV	DUVAL	A	Y	5	SIX BAY TANK TRUCK LOADING RACK	A	VOC	10/31/2007	4.62	MILLIGRAMS PER LITER OF LIQUID LOADED	Test Team J.Jordan
BPB MANUFACTURING, INC.	0310202	JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	16	BPG/RECLAIM DRYING AND MILLING SYSTEM	A	PM	10/31/2003	0.0021	GRAINS PER DRY STANDARD CUBIC FOOT	
BPB MANUFACTURING, INC.	0310202	JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	3	LANDPLASTER PRODUCTION SYSTEM	A	PM	9/15/2003	0.051	GRAINS PER DRY STANDARD CUBIC FOOT	
BPB MANUFACTURING, INC.	0310202	JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	17	STUCCO PRODUCTION SYSTEM	A	PM	9/17/2003	0.0155	GRAINS PER DRY STANDARD CUBIC FOOT	
BPB MANUFACTURING, INC.	0310202	JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	3	LANDPLASTER PRODUCTION SYSTEM	A	PM	11/5/2003	0.0043	GRAINS PER DRY STANDARD CUBIC FOOT	
BPB MANUFACTURING, INC.	0310202	JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	16	BPG/RECLAIM DRYING AND MILLING SYSTEM	A	PM	4/13/2004	0.0019	GRAINS PER DRY STANDARD CUBIC FOOT	
BPB MANUFACTURING, INC.	0310202	JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	4	board plant mixing system	A	PM	9/16/2003	0.0042	GRAINS PER DRY STANDARD CUBIC FOOT	
BPB MANUFACTURING, INC.	0310202	JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	4	board plant mixing system	A	PM	1/25/2007	0.0017	GRAINS PER DRY STANDARD CUBIC FOOT	TST Team ESC Operating rates were input as r t/h vs ft2/hr
BPB MANUFACTURING, INC.	0310202	JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	1	GYPSUM ORE CRUSHING SYSTEM & CONVEYORS	A	PM	1/23/2007	0.19	POUNDS/HOUR	Tst Team ESC
BPB MANUFACTURING, INC.	0310202	JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	5	WALLBOARD END TRIM SYSTEM	A	PM	9/16/2003	0.05	POUNDS/HOUR	
BPB MANUFACTURING, INC.	0310202	JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	5	WALLBOARD END TRIM SYSTEM	A	PM	1/25/2007	0.03	POUNDS/HOUR	Test Team ESC
BPB MANUFACTURING, INC.	0310202	JACKSONVILLE PLANT	NEDV	DUVAL	A	Y	1	GYPSUM ORE CRUSHING SYSTEM & CONVEYORS	A	PM	9/19/2003	1.75	POUNDS/HOUR	
U S NAVAL STATION MAYPORT	0310213	MAYPORT	NEDV	DUVAL	A	Y	36	Abrasive Blast booth No. 4, Bldg. 1488	A	PM	11/20/2006	0.0016	GRAINS PER DRY STANDARD CUBIC FOOT	one time testing
UNITED STATES NAVY	0310215	NAS-JACKSONVILLE	NEDV	DUVAL	A	Y	105	PLASTIC MEDIA ABRASIVE BLAST BOOTH, HANGAR 101S	A	PM	5/16/2007	0.44	POUNDS/HOUR	
UNITED STATES NAVY	0310215	NAS-JACKSONVILLE	NEDV	DUVAL	A	Y	105	PLASTIC MEDIA ABRASIVE BLAST BOOTH, HANGAR 101S	A	PM	5/17/2006	0.64	POUNDS/HOUR	
UNITED STATES	0310215	NAS-JACKSONVILLE	NEDV	DUVAL	A	Y	105	PLASTIC MEDIA ABRASIVE BLAST	A	PM	9/22/2004	0.85	POUNDS/HOUR	

NAVY								BOOTH, HANGAR 101S						
UNITED STATES NAVY	0310215	NAS-JACKSONVILLE	NEDV	DUVAL	A	Y	105	PLASTIC MEDIA ABRASIVE BLAST BOOTH, HANGAR 101S	A	PM	6/30/2004	6.19	POUNDS/HOUR	
UNITED STATES NAVY	0310215	NAS-JACKSONVILLE	NEDV	DUVAL	A	Y	105	PLASTIC MEDIA ABRASIVE BLAST BOOTH, HANGAR 101S	A	PM	8/10/2004	3.95	POUNDS/HOUR	
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	PB	3/1/2004	0.00268	POUNDS PER MILLION BTU HEAT INPUT	costal air
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	CO	2/28/2006	0.022	POUNDS PER MILLION BTU HEAT INPUT	TsT TM CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	CO	2/22/2005	0.023	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	PM	2/20/2007	0.013	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	PM10	3/1/2006	0.003	POUNDS PER MILLION BTU HEAT INPUT	Tst Tm CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	PM10	2/21/2007	0.005	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	VOC	2/28/2006	0.0024	POUNDS PER MILLION BTU HEAT INPUT	TsT Tean CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	PM	3/4/2003	0.003	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	PM	3/4/2003	0.002	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	PM	3/4/2003	0.003	POUNDS PER MILLION BTU HEAT INPUT	Coastal Air Consulting, Inc. 386-943-9241, De Fl.
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	PM	2/22/2005	0.01	POUNDS PER MILLION BTU HEAT INPUT	COSTAL
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	PM	3/1/2004	0.005	POUNDS PER MILLION BTU HEAT INPUT	costal air
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	PM	2/28/2006	0.005	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	FL	3/6/2003	0.00008	POUNDS PER MILLION BTU HEAT INPUT	
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	FL	3/6/2003	0.00005	POUNDS PER MILLION BTU HEAT INPUT	Coastal Air Consulting, Inc. 386-943-9241, De Fl.
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	FL	2/22/2007	0.00007	POUNDS PER MILLION BTU HEAT INPUT	
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	PM10	3/5/2003	0.011	POUNDS PER MILLION BTU HEAT INPUT	costal air
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	PM10	3/5/2003	0.011	POUNDS PER MILLION BTU HEAT INPUT	Coastal Air Consulting, Inc. 386-943-9241, De Fl.
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	PM10	2/23/2005	0.007	POUNDS PER MILLION BTU HEAT INPUT	COSTAL
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	PM10	3/3/2004	0.014	POUNDS PER MILLION BTU HEAT INPUT	costal air
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	CO	3/4/2003	0.063	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	CO	3/1/2004	0.029	POUNDS PER MILLION BTU HEAT INPUT	COSTAL AIR
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	CO	2/20/2007	0.013	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	CO	12/7/2007	0.0158	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	FL	2/20/2007	0.00006	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	H114	3/4/2004	0.00116	POUNDS PER MILLION BTU HEAT INPUT	costal air
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	PM	3/5/2003	0.011	POUNDS PER MILLION BTU HEAT INPUT	Coastal Air Consulting, Inc. 386-943-9241, De Fl.
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	PM	2/23/2005	0.016	POUNDS PER MILLION BTU HEAT INPUT	COSTAL
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	PM	3/3/2004	0.015	POUNDS PER MILLION BTU HEAT INPUT	costal air
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	PM	3/1/2006	0.003	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	PM	2/21/2007	0.008	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	CO	3/5/2003	0.03	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	CO	2/23/2005	0.032	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	CO	3/3/2004	0.032	POUNDS PER MILLION BTU HEAT INPUT	COSTAL AIR
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	CO	2/21/2007	0.013	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	CO	12/6/2007	0.0215	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC

CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	PB	3/3/2004	0.00847	POUNDS PER MILLION BTU HEAT INPUT	costal air
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	H021	3/1/2004	0.000043	POUNDS PER MILLION BTU HEAT INPUT	costal air
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	NOX	3/5/2003	0.167	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	NOX	2/23/2005	0.163	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	NOX	3/3/2004	0.171	POUNDS PER MILLION BTU HEAT INPUT	Annual RATA results; CEMS 30-day rolling average is actual compliance standard - no viol
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	NOX	2/21/2007	0.148	POUNDS PER MILLION BTU HEAT INPUT	Test Tean CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	NOX	2/6/2007	0.1607	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	FL	3/5/2003	0.00016	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	FL	3/5/2003	0.000145	POUNDS PER MILLION BTU HEAT INPUT	Coastal Air Consulting, Inc. 386-943-9241, De Fl.
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	FL	2/21/2007	0.000059	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	PM10	3/4/2003	0.002	POUNDS PER MILLION BTU HEAT INPUT	Coastal Air Consulting, Inc. 386-943-9241, De Fl.
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	PM10	2/22/2005	0.01	POUNDS PER MILLION BTU HEAT INPUT	COSTAL
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	PM10	3/1/2004	0.007	POUNDS PER MILLION BTU HEAT INPUT	
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	PM10	2/28/2006	0.005	POUNDS PER MILLION BTU HEAT INPUT	Tst Tm CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	PM10	2/20/2007	0.013	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	VOC	2/28/2006	0.0023	POUNDS PER MILLION BTU HEAT INPUT	Tst TM CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	H114	3/1/2004	0.00148	POUNDS PER MILLION BTU HEAT INPUT	costal air
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	PM10	3/6/2003	0.004	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	PM10	3/6/2003	0.004	POUNDS PER MILLION BTU HEAT INPUT	Coastal Air Consulting, Inc. 386-943-9241, De Fl.
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	PM10	2/25/2005	0.004	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	PM10	2/28/2005	0.003	POUNDS PER MILLION BTU HEAT INPUT	COSTAL
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	PM10	3/4/2004	0.005	POUNDS PER MILLION BTU HEAT INPUT	costal air same # as pm/17 test
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	PM10	3/2/2006	0.007	POUNDS PER MILLION BTU HEAT INPUT	Tst Tm CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	PM10	2/22/2007	0.01	POUNDS PER MILLION BTU HEAT INPUT	Teat Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	CO	3/6/2003	0.051	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	CO	2/24/2005	0.027	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	CO	2/25/2005	0.027	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	CO	3/4/2004	0.024	POUNDS PER MILLION BTU HEAT INPUT	COSTAL AIR
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	CO	2/22/2007	0.014	POUNDS PER MILLION BTU HEAT INPUT	Test Tean CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	H114	3/3/2004	0.00116	POUNDS PER MILLION BTU HEAT INPUT	costal air
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	H021	3/3/2004	0.000251	POUNDS PER MILLION BTU HEAT INPUT	costal air
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	VOC	2/3/2003	0.0023	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	VOC	3/7/2003	0.0023	POUNDS PER MILLION BTU HEAT INPUT	coastal air consulting, inc.
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	VOC	2/25/2005	0.0008	POUNDS PER MILLION BTU HEAT INPUT	
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	VOC	3/2/2006	0.0027	POUNDS PER MILLION BTU HEAT INPUT	TST Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	SO2	3/4/2003	0.148	POUNDS PER MILLION BTU HEAT INPUT	
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	SO2	2/22/2005	0.237	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	SO2	3/1/2004	0.171	POUNDS PER MILLION BTU HEAT INPUT	COSTAL
CEDAR BAY		CEDAR BAY						CIRCULATING					POUNDS PER	

GENERATING COMPANY, L.P.	0310337	COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	FLUIDIZED BED BOILER A	A	SO2	2/28/2006	0.242	MILLION BTU HEAT INPUT	TST TEAM CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	SO2	2/20/2007	0.194	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	SO2	12/7/2007	0.1404	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	NOX	3/4/2003	0.103	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	NOX	2/22/2005	0.181	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	NOX	3/1/2004	0.148	POUNDS PER MILLION BTU HEAT INPUT	COSTAL AIR
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	NOX	2/28/2006	0.17	POUNDS PER MILLION BTU HEAT INPUT	TsT Tm CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	NOX	2/20/2007	0.17	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC STD is 30 day rolling avg. act 0.177 no excedence
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	NOX	12/7/2007	0.17	POUNDS PER MILLION BTU HEAT INPUT	Test actual 0.1799 STD is based on 30 day rolli AVG. no Violation, Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	NOX	3/6/2003	0.131	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	NOX	2/24/2005	0.169	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	NOX	2/25/2005	0.169	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	NOX	3/4/2004	0.149	POUNDS PER MILLION BTU HEAT INPUT	COSTAL AIR
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	NOX	2/22/2007	0.162	POUNDS PER MILLION BTU HEAT INPUT	
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	H021	3/4/2004	0.000036	POUNDS PER MILLION BTU HEAT INPUT	costal air
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	SO2	3/5/2003	0.176	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	SO2	2/23/2005	0.194	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	SO2	3/3/2004	0.17	POUNDS PER MILLION BTU HEAT INPUT	COSTAL
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	PM	3/6/2003	0.0006	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	PM	3/6/2003	0.006	POUNDS PER MILLION BTU HEAT INPUT	Coastal Air Consulting, Inc. 386-943-9241, De Fl.
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	PM	2/25/2005	0.004	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	PM	2/28/2005	0.008	POUNDS PER MILLION BTU HEAT INPUT	COSTAL
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	PM	3/4/2004	0.005	POUNDS PER MILLION BTU HEAT INPUT	costal air
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	PM	3/2/2006	0.01	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	PM	2/22/2007	0.011	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	SO2	3/6/2003	0.091	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	SO2	2/24/2005	0.186	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	SO2	2/25/2005	0.186	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	SO2	3/4/2004	0.167	POUNDS PER MILLION BTU HEAT INPUT	COSTAL
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	SO2	2/22/2007	0.0179	POUNDS PER MILLION BTU HEAT INPUT	Test Tean CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	SAM	3/7/2003	0.000036	POUNDS PER MILLION BTU HEAT INPUT	coastal air consulting, inc.
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	3	CIRCULATING FLUIDIZED BED BOILER C	A	PB	3/4/2004	0.00179	POUNDS PER MILLION BTU HEAT INPUT	costal air
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	FL	3/4/2003	0.000138	POUNDS PER MILLION BTU HEAT INPUT	Coastal Air Consulting, Inc. 386-943-9241, De Fl.
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	1	CIRCULATING FLUIDIZED BED BOILER A	A	FL	3/4/2003	0.000138	POUNDS PER MILLION BTU HEAT INPUT	costal
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	SO2	12/6/2007	0.2075	POUNDS PER MILLION BTU HEAT INPUT	Test Team CAC
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	SO2	3/3/2004	0.177	POUNDS PER MILLION BTU HEAT INPUT	
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	2	CIRCULATING FLUIDIZED BED BOILER B	A	SO2	2/21/2007	0.159	POUNDS PER MILLION BTU HEAT INPUT	
CEDAR BAY GENERATING COMPANY, L.P.	0310337	CEDAR BAY COGENERATION FACILITY	NEDV	DUVAL	A	Y	34	Absorber Dryer System Train 3 (Dryer and Handling System)	A	PM	8/24/2007	0.002	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Test Team CAC Test Method 5

JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	PM	12/19/2004	0	POUNDS/HOUR	AIR HYGIENE
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	7/8/2003	0.6	PARTS PER MILLION DRY GAS VOLUME	
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	12/17/2004	2.14	PARTS PER MILLION DRY GAS VOLUME	AIR HYGENE
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	7/19/2004	0.51	PARTS PER MILLION DRY GAS VOLUME	
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	12/19/2004	0.4	PARTS PER MILLION DRY GAS VOLUME	AIR HYGIENE
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	11/30/2004	1.86	PARTS PER MILLION DRY GAS VOLUME	ge engery
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	12/17/2004	1.6	PARTS PER MILLION DRY GAS VOLUME	
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	12/18/2004	0.5	PARTS PER MILLION DRY GAS VOLUME	OIL FIRED --------- AIR HYGIENE-----------
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	7/20/2004	0.85	PARTS PER MILLION DRY GAS VOLUME	
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	12/1/2004	2.99	PARTS PER MILLION DRY GAS VOLUME	GE ENERGY
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	1	Unit 1 Simple Cycle Combustion Turbine	A	CO	7/21/2004	2.14	PARTS PER MILLION DRY GAS VOLUME	
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	1	Unit 1 Simple Cycle Combustion Turbine	A	CO	8/1/2006	0.35	PARTS PER MILLION DRY GAS VOLUME	Test Team CAC Webb.Leeper
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	1	Unit 1 Simple Cycle Combustion Turbine	A	CO	10/6/2005	0.12	PARTS PER MILLION DRY GAS VOLUME	Test Team CAC (Costal Air Consulting)
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	1	Unit 1 Simple Cycle Combustion Turbine	A	CO	9/5/2007	11.35	PARTS PER MILLION DRY GAS VOLUME	Test Team Grace Consulting
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	9/6/2007	0.89	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team Grace Conculting
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	8/2/2007	2.26	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team Costal Air
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	9/8/2006	2.14	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team Grace Consulting
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	7/9/2003	1.29	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NH3	11/21/2005	0.34	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	METHOD CTM-027 TEST TEAM GRACE
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NH3	9/8/2006	0.28	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Meth CTM-027 Test Team Grace Consult
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NH3	8/2/2007	0.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	CTM-027 test method Test Team CAC
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NH3	9/6/2007	0.23	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test method CTM-027 Test Team Grace Consu
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	7/27/2005	1.61	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team Grace
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	9/6/2006	0.83	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	8/3/2007	1.23	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test team CAC
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	9/7/2007	0.82	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	CTM-027 Test Team Grace
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	7/9/2003	1.29	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	9/7/2007	2.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team Grace
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	1	Unit 1 Simple Cycle Combustion Turbine	A	NOX	7/10/2003	8.07	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	1	Unit 1 Simple Cycle Combustion Turbine	A	NOX	7/21/2004	8.46	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	1	Unit 1 Simple Cycle Combustion Turbine	A	NOX	8/1/2006	0.35	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team CAC Webb,Leeper
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	1	Unit 1 Simple Cycle Combustion Turbine	A	NOX	10/6/2005	7.65	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team CAC (Costal Air Consultants)
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	1	Unit 1 Simple Cycle Combustion Turbine	A	NOX	9/5/2007	8.49	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team Grace Consulting

JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	1	Unit 1 Simple Cycle Combustion Turbine	A	CO	7/10/2003	1.08	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NH3	12/17/2004	0.31	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Init. Performance Test as combined cycle CT - Gas fired - CTM-027 used
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NH3	12/19/2004	1.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Init. Performance Test as combined cycle CT - Oil fired - CTM-027 used
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	7/9/2003	8.49	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	12/17/2004	2.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	SHEET SHOWS 74% AT 3.5 PPM@15 O2 AI HYGIENE
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	12/18/2004	13.07	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	15.0 PPM ON SHEET (87%) AIR HYGIENE
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	7/20/2004	7.86	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	12/1/2004	2.16	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	ge energy
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	12/1/2004	3.07	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE ENERGY
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	7/26/2005	2.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team Grace
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	9/8/2006	1.91	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Meth 20 used Teat Team Grace Consultan
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	8/2/2007	2.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Teast Team Costal Air
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	9/6/2007	2.41	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team Grace Consulting (Method 20)
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	7/8/2003	5.96	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	12/17/2004	3.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	AIR HYGENE
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	7/19/2004	5.93	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	12/19/2004	12.97	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	AIR HYGIENE
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	11/30/2004	3.47	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	ge energy
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	7/27/2005	2.25	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team Grace
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	9/6/2006	1.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Method 20 Test Team Grace Consulting
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NOX	8/3/2007	2.42	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team CAC
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NH3	7/27/2005	0.51	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Method CTM-027 Test Team Grace
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NH3	11/22/2005	0.51	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	METHOD CTM-027 TEST TEAM GRACE
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NH3	9/6/2006	0.14	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Method CTM-027 Test Team Grace Cons
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NH3	8/3/2007	0.29	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Method CTM-027 Test Team CAC
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	NH3	9/7/2007	0.38	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	CTM-027 Test Team Grace
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NH3	12/17/2004	0.23	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Init. Performance Test as combined cycle CT - Gas fired - CTM-027 used
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NH3	12/18/2004	0.56	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Init. Performance Test as combined cycle CT - Oil fired - CTM-027 used
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	NH3	7/26/2005	0.71	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Method CTM-027 Test Team Grace
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	CO	7/26/2005	3.25	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team Grace

JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	VOC	12/18/2004	0.33	POUNDS/HOUR	AIR HYGIENE
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	VOC	12/17/2004	0.7	POUNDS/HOUR	Init. Performance Test as combined cycle CT - Gas Fired
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	2	Unit 2 Combined Cycle Combustion Turbine with NG fired HRSG	A	VOC	12/17/2004	1	POUNDS/HOUR	AIR HYGIENE
JEA	0310485	BRANDY BRANCH FACILITY	NEDV	DUVAL	A	Y	3	Unit 3 Combined Cycle Combustion Turbine with NG fired HRSG	A	VOC	12/19/2004	0.38	POUNDS/HOUR	Init. Performance Test as combined cycle CT - Oil fired
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	3	Dust Sources Controlled by Scrubber No.3	A	PM	10/26/2007	0.339	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	3	Dust Sources Controlled by Scrubber No.3	A	PM	12/1/2006	1.1	POUNDS/HOUR	BoardMill throughput is <90% of allowable. Fu throughput is limited to 52.8 fpm until retested.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	50	BOARD DRYER (Stacks#53 and 54)	A	PM	12/12/2003	4.6	POUNDS/HOUR	combined emissions: 6.24; limited to 47.3 fpm retested.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	50	BOARD DRYER (Stacks#53 and 54)	A	PM	12/12/2003	1.64	POUNDS/HOUR	combined emissions: 6.24; limited to 47.3 fpm retested.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	50	BOARD DRYER (Stacks#53 and 54)	A	PM	12/10/2004	3.3	POUNDS/HOUR	11 pph limit is actually both stacks combined.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	50	BOARD DRYER (Stacks#53 and 54)	A	PM	11/3/2006	1	POUNDS/HOUR	Operating at 48 board feet per minute during te
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	50	BOARD DRYER (Stacks#53 and 54)	A	PM	11/11/2005	1.4	POUNDS/HOUR	limited to 52.8 fpm until retested. CAM plan operating rate: 6.3 psia
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	50	BOARD DRYER (Stacks#53 and 54)	A	PM	11/11/2005	1.8	POUNDS/HOUR	CAM plan operating rate: 11.1 psia; limited to : fpm until retested.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	50	BOARD DRYER (Stacks#53 and 54)	A	PM	11/3/2006	4.3	POUNDS/HOUR	Operating rate of 48 board feet per minute.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	50	BOARD DRYER (Stacks#53 and 54)	A	PM	11/9/2007	3	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	50	BOARD DRYER (Stacks#53 and 54)	A	PM	11/9/2007	0.2	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	14	Dust Sources Controlled by Scrubber No. 5	A	PM	12/9/2003	4.06	POUNDS/HOUR	Operating rate 15.2 bd/min
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	14	Dust Sources Controlled by Scrubber No. 5	A	PM	12/11/2003	0.56	POUNDS/HOUR	Test rate 15.2 bd/min; limited to 16.7 bd /min u retested
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	14	Dust Sources Controlled by Scrubber No. 5	A	PM	6/18/2004	0.876	POUNDS/HOUR	Operating rate of 15.3 bd/min < 90% of permit of 20 bd/min. Limited to 16.8 bd/min until retre
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	14	Dust Sources Controlled by Scrubber No. 5	A	PM	11/16/2004	1.73	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	14	Dust Sources Controlled by Scrubber No. 5	A	PM	11/8/2005	1.44	POUNDS/HOUR	CAM-Operating rate 165 gpm; FMS Line tenor limited to 16.72 FPM until retested.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	14	Dust Sources Controlled by Scrubber No. 5	A	PM	11/1/2006	1.91	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	14	Dust Sources Controlled by Scrubber No. 5	A	PM	11/1/2007	2	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	12	Dust Sources Controlled by Scrubber No. 7	A	PM	11/5/2003	2.78	POUNDS/HOUR	Production rate limited to 27.5 bd/min until rete Operating rate during test was 25 bd/min.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	12	Dust Sources Controlled by Scrubber No. 7	A	PM	11/2/2004	1.45	POUNDS/HOUR	LIMITED TO 27.5 BD/MIN UNTIL RETESTI
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	12	Dust Sources Controlled by Scrubber No. 7	A	PM	10/18/2005	1.2	POUNDS/HOUR	PIF limited to 27.5 bd/min until retested.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	12	Dust Sources Controlled by Scrubber No. 7	A	PM	10/12/2006	2.6	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	12	Dust Sources Controlled by Scrubber No. 7	A	PM	10/3/2007	2	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	10	Dust Sources Controlled by Scrubber No. 6	A	PM	10/30/2003	1.31	POUNDS/HOUR	Limited to 27.5 bd/min until retested.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	55	Perlite Expanding (Exhaust 55)	A	PM	11/6/2003	5.08	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	55	Perlite Expanding (Exhaust 55)	A	PM	12/10/2004	3.7	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	55	Perlite Expanding (Exhaust 55)	A	PM	11/18/2005	3.6	POUNDS/HOUR	CAM plan operating rate: 191 gpm;
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	55	Perlite Expanding (Exhaust 55)	A	PM	12/1/2006	5.6	POUNDS/HOUR	6.07 TPH was Test Operating rate. New limit is 110%, or 6.677 tons of perlite expanded per ho
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	55	Perlite Expanding (Exhaust 55)	A	PM	10/26/2007	5.3	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	54	Dust Sources Controlled by Scrubber No. 9	A	PM	11/21/2003	0.902	POUNDS/HOUR	Op rate 26.2 bd/min; limited to 28.8 until retest
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	54	Dust Sources Controlled by Scrubber No. 9	A	PM	11/5/2004	0.425	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	54	Dust Sources Controlled by Scrubber No. 9	A	PM	11/18/2005	0.4	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	54	Dust Sources Controlled by Scrubber No. 9	A	PM	12/1/2006	1.2	POUNDS/HOUR	New test limits are 110% of 48 fpm on the Boa Mill Dry Saw and 27 bd/min on the PIF Slice F
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	54	Dust Sources Controlled by Scrubber No. 9	A	PM	10/26/2007	0.7	POUNDS/HOUR	
ARMSTRONG														

WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	10	Dust Sources Controlled by Scrubber No. 6	A	PM	10/28/2004	0.505	POUNDS/HOUR	Limited to 27.5 bd/min until retested.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	10	Dust Sources Controlled by Scrubber No. 6	A	PM	11/10/2005	0.3	POUNDS/HOUR	limited to 28.82 bd/min until retested. CAM pla operating rate: 20.4 psia
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	10	Dust Sources Controlled by Scrubber No. 6	A	PM	10/31/2006	1.38	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	10	Dust Sources Controlled by Scrubber No. 6	A	PM	10/11/2007	0.7	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	9	Dust Sources Controlled by Scrubber No. 4	A	PM	11/6/2003	1.3	POUNDS/HOUR	Limited to 16.7 bd/min until retested.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	9	Dust Sources Controlled by Scrubber No. 4	A	PM	11/16/2004	1.15	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	9	Dust Sources Controlled by Scrubber No. 4	A	PM	11/8/2005	1.12	POUNDS/HOUR	Limited to 16.72 bd/min until retested. CAM pl operating rate: 21 psia:
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	9	Dust Sources Controlled by Scrubber No. 4	A	PM	11/1/2006	1.16	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	9	Dust Sources Controlled by Scrubber No. 4	A	PM	11/1/2007	0.9	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	3	Dust Sources Controlled by Scrubber No.3	A	PM	11/21/2003	0.591	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	3	Dust Sources Controlled by Scrubber No.3	A	PM	11/5/2004	0.755	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	3	Dust Sources Controlled by Scrubber No.3	A	PM	11/18/2005	0.5	POUNDS/HOUR	Bd Mill Stacker limited to 52.8fpm until reteste CAM plan operating rate: 21 psia
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	11	Dust Sources Controlled by Scrubber No. 2	A	PM	10/11/2007	1.4	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	11	Dust Sources Controlled by Scrubber No. 2	A	PM	10/31/2006	1.43	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	11	Dust Sources Controlled by Scrubber No. 2	A	PM	10/13/2005	2.2	POUNDS/HOUR	PIF limited to 27.5 bd/min until retested; salvag equalizer limited to 880 sf/hr until retested.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	11	Dust Sources Controlled by Scrubber No. 2	A	PM	9/2/2004	2.05	POUNDS/HOUR	PIF PRODUCTION LIMITED TO 2725 BD/M ABD SALVAGE EQ. TO 900 SFH.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	11	Dust Sources Controlled by Scrubber No. 2	A	PM	10/30/2003	3.25	POUNDS/HOUR	Operating rate 25 bd/min; limited to 27.5 bd/mi until retested
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	56	Sources Controlled by Scrubber No. 8	A	PM	11/14/2005	0.7	POUNDS/HOUR	CAM plan operating rate: 21.2 psia; limited to fpm until retested.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	56	Sources Controlled by Scrubber No. 8	A	PM	11/15/2004	0.388	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	56	Sources Controlled by Scrubber No. 8	A	PM	11/17/2003	0.191	POUNDS/HOUR	Limited to 49.5 fpm until retested. Test rate 45
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	56	Sources Controlled by Scrubber No. 8	A	PM	11/3/2006	0.6	POUNDS/HOUR	operating at 48 board feet per minute during tes
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	56	Sources Controlled by Scrubber No. 8	A	PM	11/9/2007	0.12	POUNDS/HOUR	
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	11	Dust Sources Controlled by Scrubber No. 2	A	PM	12/4/2003	2.66	POUNDS/HOUR	Operating rate 25 bd/min; limited to 27.5 bd/mi until retested; salvage equalizer limited to 827. SFH until retested.
ARMSTRONG WORLD INDUSTRIES, INC.	0330006	PENSACOLA PLANT	NWD	ESCAMBIA	A	Y	11	Dust Sources Controlled by Scrubber No. 2	A	PM	10/28/2004	1.88	POUNDS/HOUR	PIF: Permit rate: 33 bd/min. Tested at 25 bd/mi limited to 27.5 until retested. Slavage equalizer tested at 800 SFH; LIMITED TO 876.6 UNTIL RETESTED. IIMIT 900 SFH.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	32	COGENERATION PLANT	A	CO	10/19/2004	33	POUNDS/HOUR	See test report for emissions at the low/mid/hi l and duct burner on/off runs. Entered data repres the hightest with duct burner off.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	63	ADIPIC ACID DRYER A, BLDG. 465	A	PM	2/16/2005	1.32	POUNDS/HOUR	Required for permit renewal.) Note: current per has no established limits. Must be left over fror previous pemits.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	42	NITRIC ACID PLANT E	A	NOX	2/20/2008	2.29	POUNDS PER TON OF PRODUCT	Production limited to 1221 ton/day until reteste
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	42	NITRIC ACID PLANT E	A	NOX	5/24/2006	2.5	POUNDS PER TON OF PRODUCT	LIMITED TO 1250.6 TPD UNTIL RETESTEI CONVERSION FACTOR 0.013 #NOX/TON HNO3/PPM NOX
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	42	NITRIC ACID PLANT E	A	NOX	6/11/2003	1.84	POUNDS PER TON OF PRODUCT	Conversion Factor lb NOx/ton NHO3/ppm NO 0.013; limited to 1294.13 tpd until retested.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	42	NITRIC ACID PLANT E	A	NOX	3/30/2004	2.31	POUNDS PER TON OF PRODUCT	Conversion factor 0.015 lb NOx/ Ton Nitric Ac per ppm; operating rate limited to 1275.12 tpd retested.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	42	NITRIC ACID PLANT E	A	NOX	2/23/2005	2.11	POUNDS PER TON OF PRODUCT	Limited to 1424.5 tpd until retested.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	42	NITRIC ACID PLANT E	A	NOX	3/7/2006	2.5	POUNDS PER TON OF PRODUCT	limited to 1104 until retested.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	42	NITRIC ACID PLANT E	A	NOX	2/28/2007	2.08	POUNDS PER TON OF PRODUCT	Production limited to 1259 tons/day until retest
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	79	ADIPIC ACID NIRO DRYER BUILDING 485	A	PM	2/15/2005	0.15	POUNDS/HOUR	Required for permit renewal.) Note: current per has no established limits. Must be left over fror previous pemits.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	20	CYCLOHEXANE OXIDATION PROCESS OPERATION & EXPANSION	A	CO	3/7/2005	1228.4	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	20	CYCLOHEXANE OXIDATION PROCESS OPERATION & EXPANSION	A	CO	10/31/2007	4.2	POUNDS/HOUR	75,969 lb/hr
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	20	CYCLOHEXANE OXIDATION PROCESS OPERATION & EXPANSION	A	CO	11/8/2006	19.9	POUNDS/HOUR	
								CYCLOHEXANE						INITIAL TEST OF OBUD DUE 30 DAYS AF

SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	20	OXIDATION PROCESS OPERATION & EXPANSION	A	CO	5/24/2006	24.02	POUNDS/HOUR	INITIAL OPERATION. Test flow rate 56470 p air; limited to 62,117 until retested.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	60	ADIPIC ACID BEPEX DRYER BUILDING 485	A	PM	2/15/2005	0.0016	GRAINS PER DRY STANDARD CUBIC FOOT	(Required for permit renewal.) Note: current pe has no established limits. Must be left over fror previous pemits.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	CO	11/7/2007	0	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	CO	11/14/2006	0	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	CO	10/14/2004	0.48	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	CO	10/7/2003	0.59	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	CO	12/20/2005	0	POUNDS/HOUR	Below detectable limits.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	VOC	10/12/2004	0.21	POUNDS/HOUR	For permit renewal
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	VOC	12/19/2005	0.05	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	VOC	11/16/2006	0.24	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	VOC	11/9/2007	0	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	NOX	10/7/2003	4.39	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	NOX	10/14/2004	4.03	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	NOX	12/20/2005	3.09	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	NOX	11/14/2006	4.14	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	NOX	11/7/2007	3.09	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	32	COGENERATION PLANT	A	VOC	10/19/2004	6.83	POUNDS/HOUR	See test report for emissions at the low/mid/hi l and duct burner on/off runs. Entered data repres the hightest with duct burner off.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	64	ADIPIC ACID DRYER B, BLDG. 465	A	PM	6/9/2003	1.01	POUNDS/HOUR	Method 5 test done because dryer failed VE tes 5/13/2003 ; Permit condition E.2.f. requires a P test within 30 days.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	64	ADIPIC ACID DRYER B, BLDG. 465	A	PM	2/1/2005	3.46	POUNDS/HOUR	Required for permit renewal.) Note: current per has no established limits. Must be left over fror previous pemits.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	20	CYCLOHEXANE OXIDATION PROCESS OPERATION & EXPANSION	A	VOC	3/7/2005	879.1	POUNDS/HOUR	Inhouse testing usng ASP approved Oct 1994
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	20	CYCLOHEXANE OXIDATION PROCESS OPERATION & EXPANSION	A	VOC	5/24/2006	0.33	POUNDS/HOUR	INITIAL TEST OF OBUD UNDER 0330040-(AC. Process air max 82,000 pph. Tested at 56,4 pph air. Limited to 62,117 until retested.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	20	CYCLOHEXANE OXIDATION PROCESS OPERATION & EXPANSION	A	VOC	11/8/2006	1.39	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	20	CYCLOHEXANE OXIDATION PROCESS OPERATION & EXPANSION	A	VOC	10/31/2007	0.01	POUNDS/HOUR	75,969 lb/hr
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	20	CYCLOHEXANE OXIDATION PROCESS OPERATION & EXPANSION	A	VOC	10/31/2007	0.01	POUNDS/HOUR	OBUD Unit; 0.28 ppm @ 3% O2 vs 20 ppm pe limit
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	20	CYCLOHEXANE OXIDATION PROCESS OPERATION & EXPANSION	A	VOC	11/1/2007	0.25	POUNDS/HOUR	TRU Unit; 3.41 ppm @ 3% O2 vs 20 ppm pern limit
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	CO	10/9/2003	0.63	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	CO	10/12/2004	0.62	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	CO	12/19/2005	0.02	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	CO	11/16/2006	0	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	CO	11/9/2007	1.08	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	77	DIMETHYL ESTER (DME) PRODUCTION UNIT	I	VOC	8/1/2007	0.65	POUNDS/HOUR	24 MM lb/hr for 2006 AOR - 40CFR 63 FFFF, OHAP >98% control efficiency allowed, >99.9 tested
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	61	ADIPIC ACID DRYER A, BLDG. 405	A	PM	2/17/2005	0.28	POUNDS/HOUR	Required for permit renewal.) Note: current per has no established limits. Must be left over fror previous pemits.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	32	COGENERATION PLANT	A	NOX	10/19/2004	68.7	POUNDS/HOUR	See test report for emissions at the low/mid/hi l and duct burner on/off runs. Entered data repres the hightest with duct burner off.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	VOC	10/14/2004	0.14	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	VOC	12/20/2005	0.07	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	VOC	11/14/2006	0.13	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	VOC	11/7/2007	0.02	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	62	ADIPIC ACID DRYER B, BLDG. 405	A	PM	2/18/2005	1.32	POUNDS/HOUR	(Required for permit renewal.) Note: current pe has no established limits. Must be left over fror previous pemits.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	NOX	10/9/2003	3.56	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	NOX	10/12/2004	4.02	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	NOX	12/19/2005	2.95	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	NOX	11/16/2006	4.69	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	NOX	11/9/2007	1.37	POUNDS/HOUR	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	PM	11/7/2007	0.006	POUNDS PER MILLION BTU HEAT INPUT	
													POUNDS PER	

SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	PM	10/7/2003	0.01	MILLION BTU HEAT INPUT	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	PM	11/16/2006	0.007	POUNDS PER MILLION BTU HEAT INPUT	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	82	BATCH NYLON POLYMERIZATION:4 EVAPORATORS, 12 BATCH REACTORS	A	VOC	10/29/2003	1.58	POUNDS/DAY	Lab analysis done in-house. Test done using Monsanto 1993 test protocol.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	82	BATCH NYLON POLYMERIZATION:4 EVAPORATORS, 12 BATCH REACTORS	A	VOC	12/21/2005	15.3	POUNDS/DAY	Includes emissions from EU 081.
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	82	BATCH NYLON POLYMERIZATION:4 EVAPORATORS, 12 BATCH REACTORS	A	VOC	11/6/2007	1.6	POUNDS/DAY	calculation includes EU 081
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	PM	10/14/2004	0.00926	POUNDS PER MILLION BTU HEAT INPUT	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	PM	10/9/2003	0.007	POUNDS PER MILLION BTU HEAT INPUT	Retest due to excursion on test on 9/3/03
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	PM	12/19/2005	0.008	POUNDS PER MILLION BTU HEAT INPUT	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	4	B & W BOILER #7 (STACK #2)	A	PM	11/9/2007	0.01	POUNDS PER MILLION BTU HEAT INPUT	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	PM	10/14/2004	0.009	POUNDS PER MILLION BTU HEAT INPUT	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	PM	11/14/2006	0.011	POUNDS PER MILLION BTU HEAT INPUT	
SOLUTIA INC.	0330040	SOLUTIA INC.	NWD	ESCAMBIA	A	Y	3	B & W BOILER #8 (STACK #1)	A	PM	12/20/2005	0.01	POUNDS PER MILLION BTU HEAT INPUT	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	PM	8/27/2003	0.013	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	PM	8/26/2005	0.0103	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Scrubber dp = 63.9 inches.
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	NOX	8/26/2005	128	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	CO	8/25/2004	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	CO	8/25/2005	2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	H106	8/25/2004	1.41	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	H106	8/26/2005	1.53	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	H114	8/27/2003	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	H110	8/26/2005	0.1	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	H110	8/25/2004	0.1827	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	H110	8/27/2003	0.07	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	H027	8/26/2005	0.04	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	H027	8/25/2004	0.0395	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	H027	8/27/2003	0.01	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	H114	8/26/2005	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	H114	8/25/2004	0.1827	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	SO2	8/26/2005	0.95	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	H106	8/16/2006	0.5	PARTS PER MILLION DRY GAS VOLUME	Air Testing & Consulting

													@ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	H106	8/27/2003	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	CO	8/16/2006	14	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing & Consulting
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	CO	8/27/2003	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	PM	8/25/2004	0.0143	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	PM	8/16/2006	0.013	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Air Testing & Consulting
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	DIOX	8/26/2005	93.5	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	DIOX	8/27/2003	1.5	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
SACRED HEART HEALTH SYSTEM	0330041	SACRED HEART HOSPITAL	NWD	ESCAMBIA	A	Y	4	HOSPITAL INCINERATOR	A	DIOX	8/26/2004	1.76	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	30	NO. 1 RECOVERY BOILER	A	PM	3/30/2005	19	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	51	B-LINE BLEACH PLANT SCRUBBER;	A	H038	10/11/2007	0.02	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	NOX	7/2/2003	0.0404	OTHER (SPECIFY IN COMMENT)	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	1	TALL OIL PLANT EMITS HYDROGEN SULFIDES	A	TRS	3/30/2005	0.05	POUNDS PER TON OF PRODUCT	No test conducted. Tall Oil Plant remains SHUTDOWN
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	1	TALL OIL PLANT EMITS HYDROGEN SULFIDES	A	TRS	12/13/2007	0.017	POUNDS PER TON OF PRODUCT	Production Limit - 3.74 tons/hr Tall Oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	VOC	7/2/2003	0.00026	OTHER (SPECIFY IN COMMENT)	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SAM	9/3/2003	0.871	POUNDS/HOUR	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SAM	1/7/2004	0.51	POUNDS/HOUR	ENSR Corporation - testing company
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SAM	1/19/2005	1.3	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SAM	10/12/2005	0.58	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SAM	2/22/2005	2.3	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SAM	2/23/2005	2.3	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SAM	2/24/2005	1.5	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SAM	2/24/2005	3.1	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SAM	3/17/2005	1.1	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SAM	3/30/2006	0.16	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SAM	3/8/2007	0.64	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	38	NO. 2 DISSOLVING TANK VENT WITH VENTURI SCRUBBER	A	PM	6/30/2003	4.55	POUNDS/HOUR	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	38	NO. 2 DISSOLVING TANK VENT WITH VENTURI SCRUBBER	A	PM	9/8/2004	3.1	POUNDS/HOUR	Weston Solutions; passed MACT II - 0.056 lb/t BLS vs 0.2 lb/ton BLS std
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	38	NO. 2 DISSOLVING TANK VENT WITH VENTURI SCRUBBER	A	PM	3/31/2005	7.1	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	51	B-LINE BLEACH PLANT SCRUBBER;	A	H038	3/8/2006	0.01	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	51	B-LINE BLEACH PLANT SCRUBBER;	A	H038	4/5/2005	0.01	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	51	B-LINE BLEACH PLANT SCRUBBER;	A	H038	7/18/2003	0	POUNDS/HOUR	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	38	NO. 2 DISSOLVING TANK VENT WITH VENTURI SCRUBBER	A	PM	3/29/2006	0.15	GRAINS PER DRY STANDARD CUBIC FOOT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	29	NO. 2 RECOVERY BOILER	A	PM	9/8/2004	0.59	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	Weston Solutions; passed MACT II - 0.023 grd vs 0.044 grdscf std
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	29	NO. 2 RECOVERY BOILER	A	PM	6/30/2003	0.856	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	38	NO. 2 DISSOLVING TANK VENT WITH VENTURI SCRUBBER	A	TRS	1/21/2005	0.026	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	Tested by Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	30	NO. 1 RECOVERY BOILER	A	PM	9/7/2004	0.36	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	Weston Solutions; passed MACT II - 0.018 grd vs 0.044 grdscf std

INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	30	NO. 1 RECOVERY BOILER	A	PM	7/1/2003	0.801	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	32	NO. 1 DISSOLVING TANK	A	TRS	1/22/2005	0.017	POUNDS PER 3000 POUNDS BLACK LIQUOR SOLIDS	Tested by Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	TRS	1/18/2005	3.3	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Tested by Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	NOX	3/9/2007	26	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Allowable Sequence 002 is for Nat gas., Allow 001 is for oil. A passing test result is entered ur 001, however, a test was not done using oil and not required unless oil is used during the year.
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	NOX	5/18/2006	50	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weaton Solutions, Inc. performed the test
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	NOX	3/9/2007	0	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; tested on gas (see alowable sequence 002)
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	NOX	3/6/2007	42	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; tested on oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	NOX	5/18/2006	44	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; fuel oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	NOX	5/17/2006	50	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; fuel oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	NOX	6/2/2005	47.8	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; tested firing gas; retest due t original test being done with exprired nitrous o: cylineder
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	NOX	4/6/2005	28	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; tested firing gas; test results accedpted due to testing with expired nitrous o: cylinder
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	NOX	3/29/2005	43	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; tested firing oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	NOX	11/18/2004	33	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Firing natural gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	NOX	11/17/2004	31	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	9.0 pounds NOx / hr; firing oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	NOX	7/24/2003	21.5	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	natural gas fired
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	NOX	7/30/2003	21.1	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	oil fired
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	CO	3/9/2007	10	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; tested on gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	CO	3/6/2007	4.5	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; tested on oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	CO	5/18/2006	16	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	CO	5/17/2006	13	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; fuel oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	CO	4/6/2005	13	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; tested firing gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	CO	3/29/2005	23	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions - tested firing oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	CO	12/18/2004	12	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Firing natural gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	CO	11/17/2004	29	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	5.2 lbs CO / hr; firiong oil.
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	CO	7/24/2003	28.4	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	natural gas fired
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	CO	7/30/2003	24.2	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	oil fired
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	VOC	3/9/2007	19	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; tested on gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	VOC	3/6/2007	20	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; tested on oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	VOC	5/18/2006	36	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; gas
INTERNATIONAL								LIME KILN - MUD DRYER					PARTS PER MILLION DRY	

PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	SYSTEM (LK-MDS)	A	VOC	5/17/2006	18	GAS VOLUME @ 10% O2	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	VOC	4/6/2005	11	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; tested firing gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	VOC	3/29/2005	19	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Weston Solutions; tested firing oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	VOC	11/18/2004	43	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	firing gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	VOC	11/17/2004	41	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Firing oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	VOC	7/24/2003	0.3	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	natural gas fired
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	VOC	7/30/2003	1.1	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	oil fired
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	30	NO. 1 RECOVERY BOILER	A	TRS	1/22/2005	0.8	PARTS PER MILLION DRY GAS VOLUME @ 8% O2	Tested by Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	29	NO. 2 RECOVERY BOILER	A	TRS	1/22/2005	0.72	PARTS PER MILLION DRY GAS VOLUME @ 8% O2	Tested by Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	29	NO. 2 RECOVERY BOILER	A	PM	3/27/2007	0.012	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	29	NO. 2 RECOVERY BOILER	A	PM	3/29/2006	0.005	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	30	NO. 1 RECOVERY BOILER	A	PM	3/28/2007	0.016	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	30	NO. 1 RECOVERY BOILER	A	PM	3/28/2006	0.01	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	32	NO. 1 DISSOLVING TANK	A	PM	3/28/2007	0.13	GRAINS PER DRY STANDARD CUBIC FOOT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	32	NO. 1 DISSOLVING TANK	A	PM	3/28/2006	0.08	GRAINS PER DRY STANDARD CUBIC FOOT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	38	NO. 2 DISSOLVING TANK VENT WITH VENTURI SCRUBBER	A	PM	3/27/2007	0.15	GRAINS PER DRY STANDARD CUBIC FOOT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	2	125000 LB/HR BOILER, #5 PACKAGE BOILER	A	NOX	12/5/2007	0.086	POUNDS PER MILLION BTU HEAT INPUT	Production Limit - 174.1 MMBtu/hr
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	33	BARK BOILER #3	A	SO2	11/15/2004	0.361	POUNDS PER MILLION BTU HEAT INPUT	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	33	BARK BOILER #3	A	SO2	1/25/2005	0.33	POUNDS PER MILLION BTU HEAT INPUT	Tested by Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	NOX	11/16/2004	0.038	POUNDS PER MILLION BTU HEAT INPUT	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	NOX	3/8/2005	0.05	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	NOX	1/27/2005	0.056	POUNDS PER MILLION BTU HEAT INPUT	Tested by Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	NOX	12/7/2007	0.04	POUNDS PER MILLION BTU HEAT INPUT	Production Limit - 527.1 MMBtu/hr
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	33	BARK BOILER #3	A	NOX	11/15/2004	0.457	POUNDS PER MILLION BTU HEAT INPUT	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	33	BARK BOILER #3	A	NOX	1/25/2005	0.54	POUNDS PER MILLION BTU HEAT INPUT	Tested by Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	VOC	12/17/2004	0.001	POUNDS PER MILLION BTU HEAT INPUT	Reported as less than 0.001 lbs/MMBtu
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	VOC	3/8/2005	0.001	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	VOC	3/28/2006	0	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	VOC	3/27/2007	0	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	VOC	12/7/2007	0.0002	POUNDS PER MILLION BTU HEAT INPUT	Production Limit - 527.1 MMBtu/hr
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	37	BARK BOILER #4 FUELED WITH WOOD WASTE,COAL, GAS, & OIL	A	SO2	12/7/2004	0.406	POUNDS PER MILLION BTU HEAT INPUT	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	37	BARK BOILER #4 FUELED WITH WOOD WASTE,COAL, GAS, & OIL	A	SO2	1/26/2005	0.003	POUNDS PER MILLION BTU HEAT INPUT	Tested by Weston Solutions
INTERNATIONAL								LIME KILN - MUD DRYER					GRAINS PER DRY	

PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	SYSTEM (LK-MDS)	A	PM	5/17/2006	0.053	STANDARD CUBIC FOOT @ 10% O2	Weston Solutions; natural gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	PM	5/18/2006	0.058	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	Weston Solutions; fuel oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	PM	6/22/2006	0.009	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	Weston Solutions; Oil Fired; 0.010 gr/dscf at E Outlet
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	PM	6/21/2006	0.013	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	Weston Solutions; Gas Fired; 0.012 gr/dscf at E Outlet
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	PM	3/6/2007	0.01	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	Weston Solutions; tested on oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	PM	3/9/2007	0.006	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	Weston Solutions; tested on gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	33	BARK BOILER #3	A	PM	3/29/2005	0.05	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	37	BARK BOILER #4 FUELED WITH WOOD WASTE,COAL, GAS, & OIL	A	PM	7/18/2003	0.0699	POUNDS PER MILLION BTU HEAT INPUT	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	37	BARK BOILER #4 FUELED WITH WOOD WASTE,COAL, GAS, & OIL	A	PM	12/17/2004	0.071	POUNDS PER MILLION BTU HEAT INPUT	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	37	BARK BOILER #4 FUELED WITH WOOD WASTE,COAL, GAS, & OIL	A	PM	3/30/2005	0.1	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	37	BARK BOILER #4 FUELED WITH WOOD WASTE,COAL, GAS, & OIL	A	PM	8/12/2005	0.046	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	37	BARK BOILER #4 FUELED WITH WOOD WASTE,COAL, GAS, & OIL	A	PM	5/16/2006	0.024	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	37	BARK BOILER #4 FUELED WITH WOOD WASTE,COAL, GAS, & OIL	A	PM	4/3/2007	0.02	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	33	BARK BOILER #3	A	PM	4/19/2006	0.057	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	33	BARK BOILER #3	A	PM	5/16/2007	0.071	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	CO	7/2/2003	0.00344	POUNDS PER MILLION BTU HEAT INPUT	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	CO	12/17/2004	0.027	POUNDS PER MILLION BTU HEAT INPUT	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	CO	5/8/2005	0.01	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	CO	3/28/2006	0.004	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	CO	3/27/2007	0.052	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	3	NO. 6 POWER BOILER	A	CO	12/7/2007	0.081	POUNDS PER MILLION BTU HEAT INPUT	Production Limit - 527.1 MMBtu/hr
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	37	BARK BOILER #4 FUELED WITH WOOD WASTE,COAL, GAS, & OIL	A	NOX	12/7/2004	0.43	POUNDS PER MILLION BTU HEAT INPUT	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	37	BARK BOILER #4 FUELED WITH WOOD WASTE,COAL, GAS, & OIL	A	NOX	1/26/2005	0.23	POUNDS PER MILLION BTU HEAT INPUT	Tested by Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	33	BARK BOILER #3	A	PM	7/3/2003	0.091	POUNDS PER MILLION BTU HEAT INPUT	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	33	BARK BOILER #3	A	PM	11/16/2004	0.079	POUNDS PER MILLION BTU HEAT INPUT	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	2	125000 LB/HR BOILER, #5 PACKAGE BOILER	A	NOX	7/1/2003	0.063	POUNDS PER MILLION BTU HEAT INPUT	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	2	125000 LB/HR BOILER, #5 PACKAGE BOILER	A	NOX	11/2/2006	0.079	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	2	125000 LB/HR BOILER, #5 PACKAGE BOILER	A	NOX	3/9/2005	0.08	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	2	125000 LB/HR BOILER, #5 PACKAGE BOILER	A	NOX	3/28/2007	0.06	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	2	125000 LB/HR BOILER, #5 PACKAGE BOILER	A	NOX	11/24/2004	0.063	POUNDS PER MILLION BTU HEAT INPUT	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	29	NO. 2 RECOVERY BOILER	A	PM	4/5/2005	16	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	46	LIME SLAKER	A	PM	8/11/2005	0.87	POUNDS/HOUR	Weston Solutions; scrubber flow 19.4 gpm usir water
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	46	LIME SLAKER	A	PM	8/9/2005	0.37	POUNDS/HOUR	Weston Solutions; scrubber flow 28.5 gpm usir water
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	46	LIME SLAKER	A	PM	8/18/2005	3.1	POUNDS/HOUR	Weston Solutions; scrubber flow 28.6 gpm usir water
INTERNATIONAL														

PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	46	LIME SLAKER	A	PM	1/20/2005	0.3	POUNDS/HOUR	Tested by Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	50	A-LINE BLEACH PLANT SCRUBBER	A	H038	4/5/2005	0.01	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	PM	3/8/2007	0.82	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	PM	3/17/2005	1.18	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	51	B-LINE BLEACH PLANT SCRUBBER;	A	T016	7/18/2003	0	POUNDS/HOUR	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	51	B-LINE BLEACH PLANT SCRUBBER;	A	T016	4/5/2005	0.01	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	51	B-LINE BLEACH PLANT SCRUBBER;	A	T016	3/8/2006	0.06	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	PM10	1/7/2004	0.26	POUNDS/HOUR	ENSR Corporation - testing company
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	PM10	3/30/2006	0.19	POUNDS/HOUR	Weston
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	50	A-LINE BLEACH PLANT SCRUBBER	A	T016	7/18/2003	0	POUNDS/HOUR	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	50	A-LINE BLEACH PLANT SCRUBBER	A	T016	4/5/2005	0.01	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	50	A-LINE BLEACH PLANT SCRUBBER	A	T016	3/8/2006	0.01	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	PM	7/30/2003	8.6	POUNDS/HOUR	oil fired
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	PM	7/24/2003	5.6	POUNDS/HOUR	natural gas fired
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	PM	11/19/2004	6.8	POUNDS/HOUR	Firing oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	PM	11/18/2004	5.8	POUNDS/HOUR	Firing gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	PM	9/8/2004	19	POUNDS/HOUR	Weston Solutions; passed MACT II standard - (grdscf vs 0.064 grdscf std
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	PM	9/9/2004	1.5	POUNDS/HOUR	Weston Solutions; passed MACT II - 0.006 grd vs 0.064 grdscf std
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	PM	3/29/2005	10.8	POUNDS/HOUR	Weston Solutions - tested firing oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	PM	4/6/2005	5.1	POUNDS/HOUR	Weston Solutions; tested firing gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	SO2	5/18/2006	0.9	POUNDS/HOUR	Weston Solutions; gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	SO2	3/3/2007	0.6	POUNDS/HOUR	Weston Solutions; tested on oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	SO2	3/9/2007	0.6	POUNDS/HOUR	Weston Solutions; tested on gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	PM	9/3/2003	2.68	POUNDS/HOUR	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	PM	1/7/2004	0.15	POUNDS/HOUR	ENSR Corporation - testing company
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	PM	1/19/2005	1.8	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	PM	10/12/2005	0.54	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	PM	2/22/2005	1.8	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	PM	2/24/2005	0.8	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	NOX	9/3/2003	12	POUNDS/HOUR	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	NOX	1/7/2004	6.9	POUNDS/HOUR	ENSR Corporation - testing company
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	NOX	1/24/2005	8.8	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	NOX	3/30/2006	1.9	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	NOX	3/8/2007	13.3	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SO2	3/30/2006	1.8	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SO2	3/8/2007	5.6	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	SO2	7/30/2003	0.0641	POUNDS/HOUR	oil fired
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	SO2	7/24/2003	0.116	POUNDS/HOUR	natural gas fired
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	SO2	11/17/2004	1	POUNDS/HOUR	Firing oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	SO2	11/18/2004	1	POUNDS/HOUR	Firing nat gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	SO2	3/29/2005	0.32	POUNDS/HOUR	Weston Solutions; tested firing oil
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	SO2	4/6/2005	0.3	POUNDS/HOUR	Weston Solutions; tested firing gas
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	28	LIME KILN - MUD DRYER SYSTEM (LK-MDS)	A	SO2	5/17/2006	0.27	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	TRS	9/3/2003	0	POUNDS/HOUR	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	TRS	1/19/2005	0.04	POUNDS/HOUR	Tested by Weston Solutions; pulp production - ADTUP/hr vs minimum of 60 ADTUP/hr
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	CO	9/3/2003	0	POUNDS/HOUR	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	CO	1/24/2005	0.1	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	CO	3/30/2006	0.08	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	CO	3/8/2007	0.04	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	32	NO. 1 DISSOLVING TANK	A	PM	7/1/2003	5.8	POUNDS/HOUR	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	32	NO. 1 DISSOLVING TANK	A	PM	9/7/2004	5.9	POUNDS/HOUR	Weston Solutions; passed MACT II - 0.104 lb/t BLS vs 0.2 lb/ton BLS
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	32	NO. 1 DISSOLVING TANK	A	PM	3/30/2005	3.4	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	2	125000 LB/HR BOILER, #5 PACKAGE BOILER	A	CO	7/1/2003	0.06	POUNDS/HOUR	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	2	125000 LB/HR BOILER, #5 PACKAGE BOILER	A	CO	11/24/2004	1	POUNDS/HOUR	

INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	2	125000 LB/HR BOILER, #5 PACKAGE BOILER	A	CO	3/9/2005	1.6	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	2	125000 LB/HR BOILER, #5 PACKAGE BOILER	A	CO	11/2/2006	0.3	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	2	125000 LB/HR BOILER, #5 PACKAGE BOILER	A	CO	3/28/2007	0.6	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	2	125000 LB/HR BOILER, #5 PACKAGE BOILER	A	CO	12/5/2007	3.8	POUNDS/HOUR	Production Limit - 174.1 MMBtu/hr
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	VOC	1/24/2005	0.04	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	VOC	3/30/2006	0.03	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	VOC	3/8/2007	0.03	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SO2	9/3/2003	3.47	POUNDS/HOUR	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SO2	1/7/2004	0.97	POUNDS/HOUR	ENSR Corporation - testing company
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	SO2	1/24/2005	3.8	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	67	Thermal Oxidizer	A	PM	3/30/2006	0.19	POUNDS/HOUR	Weston Solutions
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	50	A-LINE BLEACH PLANT SCRUBBER	A	H038	7/18/2003	0	POUNDS/HOUR	
INTERNATIONAL PAPER COMPANY	0330042	PENSACOLA MILL	NWD	ESCAMBIA	A	Y	50	A-LINE BLEACH PLANT SCRUBBER	A	H038	3/8/2006	0.01	POUNDS/HOUR	Weston Solutions
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	PM	11/13/2007	0.02	POUNDS PER MILLION BTU HEAT INPUT	with Bromine
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	PM	11/12/2007	0.02	POUNDS PER MILLION BTU HEAT INPUT	with out bromine
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	PM	1/23/2007	0.02	POUNDS PER MILLION BTU HEAT INPUT	Steady State
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	PM	1/25/2006	0.02	POUNDS PER MILLION BTU HEAT INPUT	Soot blow.
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	PM	1/25/2005	0.005	POUNDS PER MILLION BTU HEAT INPUT	Soot Blow; Firing rate from F-factor = 751 MMBtu/hr
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	PM	2/20/2007	0.007	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	PM	2/20/2007	0.008	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	PM	1/28/2004	0.003	POUNDS PER MILLION BTU HEAT INPUT	Steady State
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	PM	1/27/2004	0.003	POUNDS PER MILLION BTU HEAT INPUT	Soot Blow
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	PM	10/8/2003	0.0193	POUNDS PER MILLION BTU HEAT INPUT	Particulate compliance test with additives: Sodi Carbonate and GAM-60.
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	PM	9/22/2003	0.021	POUNDS PER MILLION BTU HEAT INPUT	Department requested special test be done in response to citizen complaints about PM fallou Request was made 9/19/2003
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	PM	2/5/2003	0.0045	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	PM	2/4/2003	0.0054	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	PM	1/26/2005	0.005	POUNDS PER MILLION BTU HEAT INPUT	Steady State; Firing Rate from F-Factor = 773 MMBtu/hr.
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	NOX	2/24/2006	25	PERCENT REDUCTION IN EMISSIONS	Percent reduction of NOx with SNCR operatior
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	PM	3/9/2004	0.00334	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	PM	3/10/2004	0.00358	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	PM	1/30/2003	0.005	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	PM	1/29/2003	0.006	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	PM	3/8/2005	0.00874	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	PM	3/9/2005	0.01053	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	PM	3/6/2006	0.009	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	PM	3/6/2006	0.012	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	PM	1/25/2006	0.04	POUNDS PER MILLION BTU HEAT INPUT	Steady state operation.
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	PM	1/23/2007	0.02	POUNDS PER MILLION BTU HEAT INPUT	Soot Blowing
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	PM	1/23/2007	0.02	POUNDS PER MILLION BTU HEAT INPUT	Soot Blowing
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	NOX	6/1/2006	0.24	POUNDS PER MILLION BTU HEAT INPUT	Controlled with SNCR; results in 32% reductio NOx. Urea flowrate: 415 lbs/hr.
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	6/13/2006	0.022	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	12/6/2005	0.03	POUNDS PER MILLION BTU HEAT INPUT	PM test associated with CAM

GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	SO2	9/12/2006	0.933	POUNDS PER MILLION BTU HEAT INPUT	Gulf Power Environmental Affairs Field Servic performed the tests.
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	SO2	9/25/2007	1.142	POUNDS PER MILLION BTU HEAT INPUT	Tested at approximately 19% below permitted l Heat Input limited to 5756.3
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	SO2	3/10/2004	0.981	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	SO2	9/4/2003	1.385	POUNDS PER MILLION BTU HEAT INPUT	316 MW
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	SO2	3/17/2005	1.081	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	SO2	2/24/2006	1.0005	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	SO2	2/20/2007	1.126	POUNDS PER MILLION BTU HEAT INPUT	Gulf Power Environmental Affairs Field Servic Group
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	SO2	4/27/2004	1.498	POUNDS PER MILLION BTU HEAT INPUT	IN HOUSE; mw 79
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	SO2	4/26/2003	1.07	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	NOX	1/24/2006	0.353	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	SO2	1/28/2004	1.063	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	SO2	2/7/2003	0.8	POUNDS PER MILLION BTU HEAT INPUT	In House testing-McPherson
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	SO2	1/26/2005	0.839	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	SO2	1/24/2006	0.837	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	SO2	1/23/2007	0.903	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	PM	1/27/2005	0.005	POUNDS PER MILLION BTU HEAT INPUT	Soot Blow; Firing Rate from F-Factor = 834 MMBtu/hr
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	PM	5/31/2006	0.012	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	PM	5/31/2006	0.013	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	PM	5/1/2007	0.029	POUNDS PER MILLION BTU HEAT INPUT	Steady State
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	PM	5/1/2007	0.014	POUNDS PER MILLION BTU HEAT INPUT	Soot Blowing
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	SO2	4/15/2003	0.743	POUNDS PER MILLION BTU HEAT INPUT	In-house test; McPherson
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	SO2	5/25/2004	1.446	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	SO2	6/27/2005	1.061	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	SO2	9/28/2005	0.9	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	PM	2/28/2004	0.0133	POUNDS PER MILLION BTU HEAT INPUT	mw 80.8/ LIMTED TO 89 MW UNTIL RETESTED
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	PM	10/9/2003	0.0177	POUNDS PER MILLION BTU HEAT INPUT	Particulate compliance test with additives: Sodi Carbonate and GAM-60.
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	PM	4/30/2003	0.0188	POUNDS PER MILLION BTU HEAT INPUT	Load: 82 MW; limited to 110% which is 90 MV until retested.
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	PM	4/29/2003	0.0166	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	PM	4/27/2004	0.0095	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	PM	1/28/2005	0.008	POUNDS PER MILLION BTU HEAT INPUT	Steady State; Firing rate from F-Factor = 845 MMBtu/hr
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	SO2	4/18/2005	1.108	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	SO2	6/1/2006	0.936	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	SO2	5/1/2007	1.471	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	NOX	9/28/2005	0.112	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	NOX	10/27/2005	0.09	POUNDS PER MILLION BTU HEAT INPUT	SCR system installed and tested on 10/27/05. T conditions: 5379 MMBtu/hr; 502 MW; Ammoı Injection 574.6 lb/hr; ammonia slip 0.24 ppmv.
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	NOX	2/24/2006	0.36	POUNDS PER MILLION BTU HEAT INPUT	NOx emission baseline.
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	6	Boiler # 6 (Phase I Acid Rain Unit)	A	NOX	2/24/2006	0.27	POUNDS PER MILLION BTU HEAT INPUT	NOx emission rate with SNCR operational.
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	2/12/2003	0.03	POUNDS PER MILLION BTU HEAT INPUT	
													POUNDS PER	

GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	6/17/2004	0.018	MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	6/14/2004	0.008	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	6/17/2004	0.0521	POUNDS PER MILLION BTU HEAT INPUT	Steady State Conditions. Tested for purpose of developing the CAM protocal. Authorized in 0330045-007-AC.
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	6/14/2004	0.008	POUNDS PER MILLION BTU HEAT INPUT	Soot Blow. Tested in accordance with 0330045 AC to develop a CAM protocal.
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	6/29/2005	0.013	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	6/28/2005	0.008	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	9/22/2005	0.006	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	9/23/2005	0.012	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	2/11/2003	0.075	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	6/13/2006	0.02	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	3/9/2007	0.015	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	4	Boiler #4 (Phase I & II Acid Rain Unit)	A	NOX	6/1/2006	0.353	POUNDS PER MILLION BTU HEAT INPUT	Uncontrolled by SNCR.
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	9/25/2007	0.006	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	7	Boiler #7 (Phase I Acid Rain Unit)	A	PM	9/26/2007	0.0013	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	CO	5/31/2006	12.8	PERCENT BY VOLUME ON A DRY BASIS	
GULF POWER COMPANY	0330045	CRIST ELECTRIC GENERATING PLANT	NWD	ESCAMBIA	A	Y	5	Boiler #5 (Phase I & II Acid Rain Unit)	A	NOX	5/31/2006	26.6	PERCENT REDUCTION IN EMISSIONS	Demonstration of SNCR system; NOx reductio Urea Flow Rate: 39.99 lbs/hr results in 148.7 p NOx or 0.252 lbs/MMBtu. Urea turned off resu 204.0 ppmvd NOx or 0.344 lbs/MMBtu. Efficie (1 - 0.252 / 0.344) = 26.6%. Target: 25%. Amn emissions: 0.04 ppmvd
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	NOX	12/22/2005	3.2	POUNDS/HOUR	
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	NOX	12/20/2005	3	POUNDS/HOUR	
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	NOX	12/20/2005	3.3	POUNDS/HOUR	
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	CO	12/22/2005	7.3	POUNDS/HOUR	
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	CO	12/21/2005	7.7	POUNDS/HOUR	
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	CO	12/19/2005	7.4	POUNDS/HOUR	
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	CO	12/20/2005	7.4	POUNDS/HOUR	
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	CO	12/20/2005	7.4	POUNDS/HOUR	
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	CO	12/20/2005	7.6	POUNDS/HOUR	
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	CO	12/21/2005	7.4	POUNDS/HOUR	
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	CO	12/21/2005	7.6	POUNDS/HOUR	
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	NOX	12/19/2005	3.2	POUNDS/HOUR	
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	NOX	12/20/2005	2.9	POUNDS/HOUR	
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	NOX	12/21/2005	3.4	POUNDS/HOUR	
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	NOX	12/21/2005	3.4	POUNDS/HOUR	
PENSACOLA CHRISTIAN COLLEGE, INC.	0330114	PENSACOLA CHRISTIAN COLLEGE, INC.	NWD	ESCAMBIA	A	Y	9	Eight (8) 1,818 bhp IC Engines	A	NOX	12/21/2005	3.1	POUNDS/HOUR	
WEST FRASER, INC.	0330260	MCDAVID SOFTWOOD CONVERTING FACILITY	NWD	ESCAMBIA	A	Y	2	Natural Gas Fired Boiler No.2	A	NOX	4/4/2006	0.09	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
WEST FRASER, INC.	0330260	MCDAVID SOFTWOOD CONVERTING FACILITY	NWD	ESCAMBIA	A	Y	2	Natural Gas Fired Boiler No.2	A	CO	4/4/2006	0.045	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
WEST FRASER, INC.	0330260	MCDAVID SOFTWOOD CONVERTING FACILITY	NWD	ESCAMBIA	A	Y	1	Natural Gas Fired Boiler No.1	A	CO	4/4/2006	0.13	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
WEST FRASER, INC.	0330260	MCDAVID SOFTWOOD CONVERTING FACILITY	NWD	ESCAMBIA	A	Y	1	Natural Gas Fired Boiler No.1	A	NOX	4/4/2006	0.09	POUNDS PER MILLION BTU HEAT INPUT	Weston Solutions
BASF CORPORATION	0390005	QUINCY SITE	NWDT	GADSDEN	A	Y	19	Mill #4B Scrubber	A	PM	11/17/2003	1.44	POUNDS/HOUR	Scrubber: 12.9 inches W.C. and 262 gpm.

BASF CORPORATION	0390005	QUINCY SITE	NWDT	GADSDEN	A	Y	14	High Temperature Drying Kiln No. 1	A	PM	11/17/2003	2.57	POUNDS/HOUR	Scrubber: 12.4 inches of W.C and 277 GPM du test.
BASF CORPORATION	0390005	QUINCY SITE	NWDT	GADSDEN	A	Y	2	Mill #4A Scrubber	A	PM	11/18/2003	2.4	POUNDS/HOUR	Scrubber: 16.2 inches W.C and 248 gpm.
BASF CORPORATION	0390005	QUINCY SITE	NWDT	GADSDEN	A	Y	15	High Temperature Drying Kiln No. 2	A	PM	11/26/2003	3.43	POUNDS/HOUR	Scrubber: 13.0 inches of W.C. and 392 gpm du test.
BASF CORPORATION	0390005	QUINCY SITE	NWDT	GADSDEN	A	Y	39	Ultra-Fine Grind	A	PM	1/13/2005	0.06	POUNDS/HOUR	Limited to .2 pph for this test point. Initial testi after construction.
BASF CORPORATION	0390005	QUINCY SITE	NWDT	GADSDEN	A	Y	39	Ultra-Fine Grind	A	PM	10/14/2005	0.3	POUNDS/HOUR	
BASF CORPORATION	0390005	QUINCY SITE	NWDT	GADSDEN	A	Y	39	Ultra-Fine Grind	A	PM	10/14/2005	0.05	POUNDS/HOUR	
BASF CORPORATION	0390005	QUINCY SITE	NWDT	GADSDEN	A	Y	39	Ultra-Fine Grind	A	PM	10/14/2005	0.03	POUNDS/HOUR	
BASF CORPORATION	0390005	QUINCY SITE	NWDT	GADSDEN	A	Y	39	Ultra-Fine Grind	A	PM	10/14/2005	0.01	POUNDS/HOUR	
BASF CORPORATION	0390005	QUINCY SITE	NWDT	GADSDEN	A	Y	8	Mill #4 Scrubber	A	PM	11/17/2003	3.53	POUNDS/HOUR	Scrubber: 14.6 inches W.C. and 223 gpm.
COASTAL FOREST RESOURCES COMPANY	0390009	HAVANA PLYWOOD PLANT	NWDT	GADSDEN	A	Y	5	BOILER #3	A	PM	2/6/2007	0.1078	POUNDS PER MILLION BTU HEAT INPUT	
COASTAL FOREST RESOURCES COMPANY	0390009	HAVANA PLYWOOD PLANT	NWDT	GADSDEN	A	Y	5	BOILER #3	A	PM	2/5/2004	0.1013	POUNDS PER MILLION BTU HEAT INPUT	
COASTAL FOREST RESOURCES COMPANY	0390009	HAVANA PLYWOOD PLANT	NWDT	GADSDEN	A	Y	5	BOILER #3	A	PM	2/5/2003	0.0943	POUNDS PER MILLION BTU HEAT INPUT	
COASTAL FOREST RESOURCES COMPANY	0390009	HAVANA PLYWOOD PLANT	NWDT	GADSDEN	A	Y	5	BOILER #3	A	PM	1/24/2006	0.1028	POUNDS PER MILLION BTU HEAT INPUT	
COASTAL FOREST RESOURCES COMPANY	0390009	HAVANA PLYWOOD PLANT	NWDT	GADSDEN	A	Y	5	BOILER #3	A	PM	1/27/2005	0.0732	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	4	UNIT 1404 - RECIPROCATING INTERNAL COMBUSTION (IC) ENGINE	A	SO2	6/14/2007	0.002	POUNDS/HOUR	Sulfur determined by fuel analysis. Unit is limi 19.92 MMBtu/hour based on testing (110% of testing limit)
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	4	UNIT 1404 - RECIPROCATING INTERNAL COMBUSTION (IC) ENGINE	A	SO2	6/5/2003	0.00522	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	4	UNIT 1404 - RECIPROCATING INTERNAL COMBUSTION (IC) ENGINE	A	SO2	6/21/2006	0.0048	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	6	UNIT 1406 - NATURAL GAS FIRED ENGINE-2,700BHP, ENGINE	A	NOX	6/14/2007	7.75	POUNDS/HOUR	Unit is limited to 20.97 MMBtu/hour based on testing (110% of testing limit)
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	6	UNIT 1406 - NATURAL GAS FIRED ENGINE-2,700BHP, ENGINE	A	NOX	6/22/2005	8.17	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	6	UNIT 1406 - NATURAL GAS FIRED ENGINE-2,700BHP, ENGINE	A	SO2	7/21/2004	0.00362	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	6	UNIT 1406 - NATURAL GAS FIRED ENGINE-2,700BHP, ENGINE	A	SO2	6/22/2005	0.0057	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	6	UNIT 1406 - NATURAL GAS FIRED ENGINE-2,700BHP, ENGINE	A	SO2	6/21/2006	0.0057	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	6	UNIT 1406 - NATURAL GAS FIRED ENGINE-2,700BHP, ENGINE	A	SO2	6/14/2007	0.002	POUNDS/HOUR	Sulfur is determined by fuel analysis. Unit is li to 20.97 MMBtu/hour based on testing (110% testing limit)
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	4	UNIT 1404 - RECIPROCATING INTERNAL COMBUSTION (IC) ENGINE	A	NOX	6/5/2003	16.8	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	6	UNIT 1406 - NATURAL GAS FIRED ENGINE-2,700BHP, ENGINE	A	NOX	6/5/2003	5.18	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	6	UNIT 1406 - NATURAL GAS FIRED ENGINE-2,700BHP, ENGINE	A	NOX	7/21/2004	2.12	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	6	UNIT 1406 - NATURAL GAS FIRED ENGINE-2,700BHP, ENGINE	A	NOX	6/21/2006	8.23	POUNDS/HOUR	Heat input: 19.05 MMBtu/hr. 19.05/21.69 = 87 capacity.
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	4	UNIT 1404 - RECIPROCATING INTERNAL COMBUSTION (IC) ENGINE	A	SO2	6/22/2005	0.00524	POUNDS/HOUR	0.125 grains sulfur per 100 SCF
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	6	UNIT 1406 - NATURAL GAS FIRED ENGINE-2,700BHP, ENGINE	A	SO2	6/5/2003	0.00685	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	4	UNIT 1404 - RECIPROCATING INTERNAL COMBUSTION (IC) ENGINE	A	NOX	7/21/2004	2.76	GRAMS PER HORSEPOWER-HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	4	UNIT 1404 - RECIPROCATING INTERNAL COMBUSTION (IC) ENGINE	A	NOX	6/22/2005	3.34	GRAMS PER HORSEPOWER-HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	4	UNIT 1404 - RECIPROCATING INTERNAL COMBUSTION (IC) ENGINE	A	NOX	6/21/2006	2.76	GRAMS PER HORSEPOWER-HOUR	12.47 POUNDS OF NOX PER HOUR. Heat in 15.57 MMBtu/hr
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	4	UNIT 1404 - RECIPROCATING INTERNAL COMBUSTION (IC) ENGINE	A	NOX	6/14/2007	1.94	GRAMS PER HORSEPOWER-HOUR	Unit is limited to 19.92 MMBtu/hour based on testing (110% of testing limit)
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	SO2	9/29/2004	0.0696	OTHER (SPECIFY IN COMMENT)	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	SO2	6/21/2005	0.06	OTHER (SPECIFY IN COMMENT)	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	SO2	6/20/2006	0.081	OTHER (SPECIFY IN COMMENT)	0.081 grains per 100 scf fuel.
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	SO2	3/13/2007	0.041	OTHER (SPECIFY IN COMMENT)	DeNovo
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	SO2	6/14/2007	0.0346	OTHER (SPECIFY IN COMMENT)	grains per 100 scf fuel. Determination based on analysis.
FLORIDA GAS								UNIT 1408 - 15,700 bhp					OTHER	

TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	Nuovo Pignone PGT10B gas turbine	A	SO2	9/4/2003	0.0451	(SPECIFY IN COMMENT)	grains of sulfur per 100 scf of fuel.
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	SO2	9/28/2004	0.0609	OTHER (SPECIFY IN COMMENT)	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	SO2	9/29/2004	0.115	OTHER (SPECIFY IN COMMENT)	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	SO2	10/1/2004	0.115	OTHER (SPECIFY IN COMMENT)	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	SO2	6/21/2005	0.115	OTHER (SPECIFY IN COMMENT)	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	SO2	6/21/2006	0.0675	OTHER (SPECIFY IN COMMENT)	0.0675 grains per 100 cf
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	SO2	6/13/2007	0.0263	OTHER (SPECIFY IN COMMENT)	grains per 100 standard cubic feet. Determinati based on fuel analysis.
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	6	UNIT 1406 - NATURAL GAS FIRED ENGINE- 2,700BHP, ENGINE	A	CO	7/21/2004	9.46	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	6	UNIT 1406 - NATURAL GAS FIRED ENGINE- 2,700BHP, ENGINE	A	CO	6/5/2003	7.8	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	6	UNIT 1406 - NATURAL GAS FIRED ENGINE- 2,700BHP, ENGINE	A	CO	6/22/2005	6.3	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	6	UNIT 1406 - NATURAL GAS FIRED ENGINE- 2,700BHP, ENGINE	A	CO	6/14/2007	7.45	POUNDS/HOUR	Unit is limited to 20.97 MMBtu/hour based on testing (110% of testing limit)
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	6	UNIT 1406 - NATURAL GAS FIRED ENGINE- 2,700BHP, ENGINE	A	CO	6/21/2006	7.32	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	CO	6/14/2007	8.32	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	CO	6/21/2005	5.24	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	CO	1/14/2003	4.38	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	CO	9/29/2004	10.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	NOX	9/4/2003	22.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	NOX	9/4/2003	22.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	CO	9/4/2003	2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	CO	9/4/2003	1.96	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	CO	9/4/2003	1.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	CO	9/28/2004	0.57	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	CO	9/29/2004	0.79	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	CO	10/1/2004	1.68	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	CO	6/21/2005	3.82	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	CO	6/21/2006	0.43	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	CO	6/13/2007	6.45	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	NOX	9/4/2003	19.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	NOX	9/4/2003	16.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	NOX	9/28/2004	28.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	NOX	9/29/2004	25.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	NOX	10/1/2004	19.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	NOX	6/21/2005	22.2	PARTS PER MILLION DRY GAS VOLUME	

													@ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	NOX	6/20/2006	21.14	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	NOX	6/13/2007	21.75	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	10	UNIT 1408 - 15,700 bhp Nuovo Pignone PGT10B gas turbine	A	CO	9/4/2003	0.869	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	NOX	1/14/2003	7.78	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Low Load
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	NOX	1/14/2003	12.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Mid Load
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	NOX	1/14/2003	10.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Mid Load #2
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	NOX	1/14/2003	15.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Full Load
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	NOX	9/29/2004	9.11	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	NOX	6/21/2005	13.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	NOX	6/20/2006	14.63	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	90.9 MMBtu/hr, Ambient T = 94.6 degr F. 89.5 capacity.
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	NOX	3/13/2007	11.51	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	DeNovo
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	NOX	6/14/2007	12.46	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	CO	6/20/2006	4.71	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	8	UNIT 1407 - 13,078 bhp Solar Mars T-90 Turbine Compressor	A	CO	3/13/2007	8.28	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	DeNovo; Heat Input - 103.31 MMBtu/hr
FLORIDA GAS TRANSMISSION COMPANY	0390029	COMPRESSOR STATION NO. 14	NWDT	GADSDEN	A	Y	4	UNIT 1404 - RECIPROCATING INTERNAL COMBUSTION (IC) ENGINE	A	SO2	7/21/2004	0.00085	GRAINS PER DRY STANDARD CUBIC FOOT	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	3	A POLLYPHOS PLANT GAS-FIRED CALCINER ANIMAL FEED	A	SO2	5/9/2003	0.477	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	21	C SULFURIC ACID PLT W/ DOUBLE ABSORP, BRINKS DEMISTER A	A	SAM	1/25/2006	4.75	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	21	C SULFURIC ACID PLT W/ DOUBLE ABSORP, BRINKS DEMISTER A	A	SAM	1/28/2004	1.38	POUNDS/HOUR	PCS crew. Process rate: 94.1 TPH * 24 HR = 2 TPD
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	61	GREEN SPA (SUPERPHOSPHORIC ACID) PLANT W/SCRUBBER	A	FL	11/3/2004	0.02	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	61	GREEN SPA (SUPERPHOSPHORIC ACID) PLANT W/SCRUBBER	A	FL	8/18/2006	0.06	POUNDS/HOUR	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	61	GREEN SPA (SUPERPHOSPHORIC ACID) PLANT W/SCRUBBER	A	FL	1/12/2006	0.04	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	61	GREEN SPA (SUPERPHOSPHORIC ACID) PLANT W/SCRUBBER	A	FL	3/14/2007	0.12	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	61	GREEN SPA (SUPERPHOSPHORIC ACID) PLANT W/SCRUBBER	A	FL	9/6/2007	0.06	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	44	A&B COOLERS (POLLYPHOS)COMMON STACK (EP12)	A	FL	2/26/2003	0.66	POUNDS/HOUR	pcs test crew.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	44	A&B COOLERS (POLLYPHOS)COMMON STACK (EP12)	A	FL	3/3/2005	0.15	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	44	A&B COOLERS (POLLYPHOS)COMMON STACK (EP12)	A	FL	4/28/2004	0.24	POUNDS/HOUR	pcs test crew
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	21	C SULFURIC ACID PLT W/ DOUBLE ABSORP, BRINKS DEMISTER A	A	SAM	1/8/2003	3.85	POUNDS/HOUR	White Springs Ag. Chem test team, QA ok
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	67	F SULFURIC ACID PLANT	A	SAM	2/7/2007	0.02	POUNDS PER TON OF PRODUCT	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	67	F SULFURIC ACID PLANT	A	SAM	1/16/2008	0.03	POUNDS PER TON OF PRODUCT	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	66	E SULFURIC ACID PLANT	A	SAM	2/19/2003	0.03	POUNDS PER TON OF PRODUCT	PCS Test crew.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	66	E SULFURIC ACID PLANT	A	SAM	2/11/2004	0.01	POUNDS PER TON OF PRODUCT	PCS test crew. Process rate: 102.5 lb/HR * 200 205000 TPH (98%)
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	66	E SULFURIC ACID PLANT	A	SAM	2/9/2005	0.03	POUNDS PER TON OF PRODUCT	
WHITE SPRINGS													POUNDS PER	

AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	66	E SULFURIC ACID PLANT	A	SAM	2/1/2006	0.02	TON OF PRODUCT	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	66	E SULFURIC ACID PLANT	A	SAM	1/31/2007	0.02	POUNDS PER TON OF PRODUCT	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	66	E SULFURIC ACID PLANT	A	SAM	1/10/2008	0.07	POUNDS PER TON OF PRODUCT	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	66	E SULFURIC ACID PLANT	A	SO2	2/19/2003	2.85	POUNDS PER TON OF PRODUCT	PCS Test crew.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	20	B PHOS ACID PLNT PRAYON SCRBR(F4)	A	FL	1/26/2005	0.00483	POUNDS PER TON OF FEED MATERIAL	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	20	B PHOS ACID PLNT PRAYON SCRBR(F4)	A	FL	10/27/2006	0.00275	POUNDS PER TON OF FEED MATERIAL	PCS - combined B & C stacks.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	20	B PHOS ACID PLNT PRAYON SCRBR(F4)	A	FL	11/15/2007	0.00817	POUNDS PER TON OF FEED MATERIAL	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	20	B PHOS ACID PLNT PRAYON SCRBR(F4)	A	FL	11/14/2007	0.01301	POUNDS PER TON OF FEED MATERIAL	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	71	ACID CLARIFICATION PLANT	A	FL	5/21/2003	0.023837	POUNDS PER TON OF FEED MATERIAL	PCS test crew.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	71	ACID CLARIFICATION PLANT	A	FL	6/16/2004	0.014	POUNDS PER TON OF FEED MATERIAL	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	71	ACID CLARIFICATION PLANT	A	FL	1/12/2005	0.008	POUNDS PER TON OF FEED MATERIAL	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	71	ACID CLARIFICATION PLANT	A	FL	1/26/2006	0.0299	POUNDS PER TON OF FEED MATERIAL	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	71	ACID CLARIFICATION PLANT	A	FL	2/28/2007	0.011274	POUNDS PER TON OF FEED MATERIAL	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	35	N ACF ACID CLARFICATION FLTRS OLD#2 4PRI 2SEC FLTRS B SCRUBB	A	FL	1/6/2005	0.00629	POUNDS PER TON OF FEED MATERIAL	PCS TEST TEAM
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	35	N ACF ACID CLARFICATION FLTRS OLD#2 4PRI 2SEC FLTRS B SCRUBB	A	FL	2/16/2006	0.004348	POUNDS PER TON OF FEED MATERIAL	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	35	N ACF ACID CLARFICATION FLTRS OLD#2 4PRI 2SEC FLTRS B SCRUBB	A	FL	1/24/2007	0.002132	POUNDS PER TON OF FEED MATERIAL	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	35	N ACF ACID CLARFICATION FLTRS OLD#2 4PRI 2SEC FLTRS B SCRUBB	A	FL	3/5/2008	0.003956	POUNDS PER TON OF FEED MATERIAL	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	34	S-PHOSPHORIC ACID FILTER W/SCRUB;FA&FM w/collector	A	FL	12/30/2003	0.02	POUNDS PER TON OF FEED MATERIAL	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	34	S-PHOSPHORIC ACID FILTER W/SCRUB;FA&FM w/collector	A	FL	11/3/2004	0	POUNDS PER TON OF FEED MATERIAL	Facility has own testing
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	34	S-PHOSPHORIC ACID FILTER W/SCRUB;FA&FM w/collector	A	FL	11/16/2005	0.05	POUNDS PER TON OF FEED MATERIAL	pcs. no production but scrubber controls FL for aging tanks. can't calculate actual emissions.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	34	S-PHOSPHORIC ACID FILTER W/SCRUB;FA&FM w/collector	A	FL	10/18/2006	0	POUNDS PER TON OF FEED MATERIAL	emissions 0.37 #/hr. process rate 0.0
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	34	S-PHOSPHORIC ACID FILTER W/SCRUB;FA&FM w/collector	A	FL	10/10/2007	0.05	POUNDS PER TON OF FEED MATERIAL	Actual emissions was 0.88 lb/hr.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	67	F SULFURIC ACID PLANT	A	SAM	2/19/2004	0.01	POUNDS PER TON OF PRODUCT	PCS test crew. Process rate: 100.6 lb/HR * 200 201200 TPH (96%)
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	67	F SULFURIC ACID PLANT	A	SAM	2/16/2005	0.01	POUNDS PER TON OF PRODUCT	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	67	F SULFURIC ACID PLANT	A	SAM	2/8/2006	0.03	POUNDS PER TON OF PRODUCT	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	66	E SULFURIC ACID PLANT	A	SO2	2/11/2004	2.85	POUNDS PER TON OF PRODUCT	PCS test crew. Process rate: 102.5 lb/HR * 200 205000 TPH (98%)
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	66	E SULFURIC ACID PLANT	A	SO2	2/9/2005	3.09	POUNDS PER TON OF PRODUCT	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	66	E SULFURIC ACID PLANT	A	SO2	2/1/2006	3.31	POUNDS PER TON OF PRODUCT	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	66	E SULFURIC ACID PLANT	A	SO2	1/31/2007	3.22	POUNDS PER TON OF PRODUCT	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	66	E SULFURIC ACID PLANT	A	SO2	1/10/2008	3.05	POUNDS PER TON OF PRODUCT	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	69	D PHOSPHORIC ACID PLANT	A	FL	11/2/2006	0.00244	POUNDS PER TON OF FEED MATERIAL	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	69	D PHOSPHORIC ACID PLANT	A	FL	12/7/2007	0.0018	POUNDS PER TON OF FEED MATERIAL	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	67	F SULFURIC ACID PLANT	A	SO2	2/12/2003	3.01	POUNDS PER TON OF PRODUCT	PCS TEST TEAM
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	70	C & D Superphosphoric Acid Plts & LR Limerock Bin	A	FL	6/16/2003	0.00114	POUNDS PER TON OF FEED MATERIAL	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	70	C & D Superphosphoric Acid Plts & LR Limerock Bin	A	FL	2/11/2005	0.00867	POUNDS PER TON OF FEED MATERIAL	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	70	C & D Superphosphoric Acid Plts & LR Limerock Bin	A	FL	2/21/2007	0.00135	POUNDS PER TON OF FEED MATERIAL	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	36	A&B SPA PLANT W/EMISSIONS TO ACF-S SCRUBBER	A	FL	12/3/2004	0.0012	POUNDS PER TON OF FEED MATERIAL	
WHITE SPRINGS		WHITE SPRS AG						A&B SPA PLANT					POUNDS PER	

AGRICULTURAL CHEMICALS,INC	0470002	CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	36	W/EMISSIONS TO ACF-S SCRUBBER	A	FL	2/16/2006	0.0003	TON OF FEED MATERIAL	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	67	F SULFURIC ACID PLANT	A	SO2	6/25/2003	3.65	POUNDS PER TON OF PRODUCT	Process rate: 105.6 tons/hour
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	67	F SULFURIC ACID PLANT	A	SO2	2/19/2004	3.16	POUNDS PER TON OF PRODUCT	PCS test crew. Process rate: 100.6 lb/HR * 200 201200 TPH (96%)
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	67	F SULFURIC ACID PLANT	A	SO2	2/16/2005	3.35	POUNDS PER TON OF PRODUCT	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	67	F SULFURIC ACID PLANT	A	SO2	2/8/2006	3.31	POUNDS PER TON OF PRODUCT	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	67	F SULFURIC ACID PLANT	A	SO2	2/7/2007	3.23	POUNDS PER TON OF PRODUCT	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	67	F SULFURIC ACID PLANT	A	SO2	1/16/2008	3.31	POUNDS PER TON OF PRODUCT	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	FL	1/15/2003	0.0099	POUNDS PER TON OF FEED MATERIAL	White Springs Ag Chem, QA ok
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	FL	1/21/2004	0.01049	POUNDS PER TON OF FEED MATERIAL	Process rate = 70.54 TPH; FL emission = 0.74 Performed by PCS team.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	FL	6/10/2005	0.004777	POUNDS PER TON OF FEED MATERIAL	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	FL	1/27/2005	0.006	POUNDS PER TON OF FEED MATERIAL	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	FL	5/5/2006	0.00222	POUNDS PER TON OF FEED MATERIAL	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	FL	6/9/2006	0.00173	POUNDS PER TON OF FEED MATERIAL	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	FL	4/6/2006	0.005318	POUNDS PER TON OF FEED MATERIAL	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	FL	5/3/2007	0.00637	POUNDS PER TON OF FEED MATERIAL	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	61	GREEN SPA (SUPERPHOSPHORIC ACID) PLANT W/SCRUBBER	A	FL	12/23/2003	0.01	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	61	GREEN SPA (SUPERPHOSPHORIC ACID) PLANT W/SCRUBBER	A	FL	2/27/2005	0.05	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	21	C SULFURIC ACID PLT W/ DOUBLE ABSORP, BRINKS DEMISTER A	A	SAM	2/18/2005	2.9	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	21	C SULFURIC ACID PLT W/ DOUBLE ABSORP, BRINKS DEMISTER A	A	SAM	1/17/2007	1.96	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	20	B PHOS ACID PLNT PRAYON SCRBR(F4)	A	FL	1/26/2005	0.35	POUNDS/HOUR	PCS TEST TEAM
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	20	B PHOS ACID PLNT PRAYON SCRBR(F4)	A	FL	1/29/2003	0.06	POUNDS/HOUR	PCS crew. Process rate = 76.8 TPH, 102%
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	21	C SULFURIC ACID PLT W/ DOUBLE ABSORP, BRINKS DEMISTER A	A	SAM	2/27/2008	2.46	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	20	B PHOS ACID PLNT PRAYON SCRBR(F4)	A	FL	1/23/2004	0.03	POUNDS/HOUR	White Springs Chemical Test Team. Process ra 73.80 TPH
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	3	A POLLYPHOS PLANT GAS-FIRED CALCINER ANIMAL FEED	A	FL	6/23/2004	0.42	POUNDS/HOUR	In house testing
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	4	X-TRAIN(DICAL)2 OPN MDS:D-18.5,D-21; CNTS-SCBRS&BGCLR	A	PM	10/17/2007	6.44	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	4	X-TRAIN(DICAL)2 OPN MDS:D-18.5,D-21; CNTS-SCBRS&BGCLR	A	PM	10/12/2006	16.01	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	4	X-TRAIN(DICAL)2 OPN MDS:D-18.5,D-21; CNTS-SCBRS&BGCLR	A	PM	4/8/2004	10.8	POUNDS/HOUR	PCS Test Team
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	42	POLLYPHOS FEED PREP W/EPs-11,10,9,L1,L2,SA1,SA2.	A	PM	8/27/2003	0.84	POUNDS/HOUR	tested by PCS staff
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	42	POLLYPHOS FEED PREP W/EPs-11,10,9,L1,L2,SA1,SA2.	A	PM	8/26/2004	0.98	POUNDS/HOUR	Testing performed by the facility.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	10	#1 MAP/DAP/GTSP STRGE BLDG W/ BUFLO SCRUBR FL/GTSP PM/ALL 3	A	PM	10/8/2003	0.85	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	10	#1 MAP/DAP/GTSP STRGE BLDG W/ BUFLO SCRUBR FL/GTSP PM/ALL 3	A	PM	11/10/2004	0.24	POUNDS/HOUR	PCS test team
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	10	#1 MAP/DAP/GTSP STRGE BLDG W/ BUFLO SCRUBR FL/GTSP PM/ALL 3	A	PM	12/7/2005	0.35	POUNDS/HOUR	production rate can not exceed 125 tons / hr.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	10	#1 MAP/DAP/GTSP STRGE BLDG W/ BUFLO SCRUBR FL/GTSP PM/ALL 3	A	PM	3/29/2006	0.41	POUNDS/HOUR	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	10	#1 MAP/DAP/GTSP STRGE BLDG W/ BUFLO SCRUBR FL/GTSP PM/ALL 3	A	PM	4/4/2007	0.38	POUNDS/HOUR	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	4	X-TRAIN(DICAL)2 OPN MDS:D-18.5,D-21; CNTS-SCBRS&BGCLR	A	PM	3/13/2003	24.71	POUNDS/HOUR	PCS test crew.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	38	B POLLYPHOS PLANT GAS CALCINER ANIMAL FEED SUPPL	A	FL	6/9/2004	0.43	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	38	B POLLYPHOS PLANT GAS CALCINER ANIMAL FEED SUPPL	A	FL	5/25/2005	0.56	POUNDS/HOUR	PCS TESTERS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	22	D SULFURIC ACID PLT W/DOUBLE ABSORP & BRINKS ELIMINATOR A	A	SAM	12/17/2003	12.95	POUNDS/HOUR	White Springs Agricultural Chemicals Test Tea conducted.

WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	22	D SULFURIC ACID PLT W/DOUBLE ABSORP & BRINKS ELIMINATOR A	A	SAM	12/8/2004	3.65	POUNDS/HOUR	PCS test team
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	22	D SULFURIC ACID PLT W/DOUBLE ABSORP & BRINKS ELIMINATOR A	A	SAM	12/13/2006	1.48	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	22	D SULFURIC ACID PLT W/DOUBLE ABSORP & BRINKS ELIMINATOR A	A	SAM	12/14/2005	6.97	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	22	D SULFURIC ACID PLT W/DOUBLE ABSORP & BRINKS ELIMINATOR A	A	SAM	11/26/2007	2.7	POUNDS/HOUR	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	4	X-TRAIN(DICAL)2 OPN MDS:D-18.5,D-21; CNTS-SCBRS&BGCLR	A	FL	3/13/2003	0.12	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	4	X-TRAIN(DICAL)2 OPN MDS:D-18.5,D-21; CNTS-SCBRS&BGCLR	A	FL	4/8/2004	0.3	POUNDS/HOUR	PCS test Team
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	69	D PHOSPHORIC ACID PLANT	A	PM	10/27/2004	0	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	38	B POLLYPHOS PLANT GAS CALCINER ANIMAL FEED SUPPL	A	SO2	5/8/2003	0.57	POUNDS/HOUR	pcs test team
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	20	B PHOS ACID PLNT PRAYON SCRBR(F4)	A	PM	1/23/2004	0	POUNDS/HOUR	White Springs Chemical Test Team. Process Ra 73.8 TPH
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	20	B PHOS ACID PLNT PRAYON SCRBR(F4)	A	PM	1/29/2003	0.73	POUNDS/HOUR	PCS crew. Process rate = 76.8 TPH
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	2	A PHOS ACID PLANT WPPA DORR-OLIVER W CYC SCRUBBER	A	PM	1/22/2003	0.07	POUNDS/HOUR	PCS crew. Process rate = 35.09 TPH
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	2	A PHOS ACID PLANT WPPA DORR-OLIVER W CYC SCRUBBER	A	PM	2/4/2004	0	POUNDS/HOUR	PCS test crew.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	2	A PHOS ACID PLANT WPPA DORR-OLIVER W CYC SCRUBBER	A	PM	4/23/2004	0	POUNDS/HOUR	Performed by PCS White Springs test team. Pro Rate was 34.4 TPH = 104%
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	38	B POLLYPHOS PLANT GAS CALCINER ANIMAL FEED SUPPL	A	PM	4/30/2003	9.46	POUNDS/HOUR	pcs test team
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	38	B POLLYPHOS PLANT GAS CALCINER ANIMAL FEED SUPPL	A	PM	6/9/2004	7.94	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	38	B POLLYPHOS PLANT GAS CALCINER ANIMAL FEED SUPPL	A	PM	5/25/2005	11.06	POUNDS/HOUR	PCS TESTERS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	10	#1 MAP/DAP/GTSP STRGE BLDG W/ BUFLO SCRUBR FL/GTSP PM/ALL 3	A	FL	10/8/2003	0	POUNDS/HOUR	Pcs performed testing.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	10	#1 MAP/DAP/GTSP STRGE BLDG W/ BUFLO SCRUBR FL/GTSP PM/ALL 3	A	FL	3/29/2006	0	POUNDS/HOUR	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	PM	1/15/2003	1.79	POUNDS/HOUR	white sprins ag chem test team, QA ok
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	PM	1/21/2004	2.09	POUNDS/HOUR	Performed by PCS team.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	PM	6/10/2005	2.19	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	PM	1/27/2005	4.84	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	PM	5/5/2006	3.18	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	PM	6/9/2006	2.37	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	PM	6/14/2006	1.43	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	PM	4/6/2006	2.81	POUNDS/HOUR	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	32	#2 DAP (Z) W/ VENTURI & CYC SCRUBR;DAP,MAP VIA 30&50/40 P	A	PM	5/3/2007	5.95	POUNDS/HOUR	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	22	D SULFURIC ACID PLT W/DOUBLE ABSORP & BRINKS ELIMINATOR A	A	SO2	12/17/2003	345.33	POUNDS/HOUR	White Springs Agricultural Chemicals conducte test.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	22	D SULFURIC ACID PLT W/DOUBLE ABSORP & BRINKS ELIMINATOR A	A	SO2	12/8/2004	277.31	POUNDS/HOUR	PCS test team
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	22	D SULFURIC ACID PLT W/DOUBLE ABSORP & BRINKS ELIMINATOR A	A	SO2	12/13/2006	256	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	22	D SULFURIC ACID PLT W/DOUBLE ABSORP & BRINKS ELIMINATOR A	A	SO2	12/14/2005	220.05	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	22	D SULFURIC ACID PLT W/DOUBLE ABSORP & BRINKS ELIMINATOR A	A	SO2	11/26/2007	273.6	POUNDS/HOUR	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	15	MAP/DAP SCREEN/SHIP W/CYCLONE& VENTURI SCRUBBER	A	PM	2/11/2005	0.6	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	2	A PHOS ACID PLANT WPPA DORR-OLIVER W CYC SCRUBBER	A	FL	1/22/2003	0.02	POUNDS/HOUR	PCS crew. Process rate Avg.= 35.1 TPH.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	2	A PHOS ACID PLANT WPPA DORR-OLIVER W CYC SCRUBBER	A	FL	2/4/2004	0.02	POUNDS/HOUR	PCS Test Crew.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	2	A PHOS ACID PLANT WPPA DORR-OLIVER W CYC SCRUBBER	A	FL	4/23/2004	0.03	POUNDS/HOUR	Performed by PCS White Springs test team. Pro Rate was 34.4 TPH = 104%
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	2	A PHOS ACID PLANT WPPA DORR-OLIVER W CYC SCRUBBER	A	FL	5/11/2005	0.02	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	65	SCM SILOS	A	PM	5/14/2003	4.67	POUNDS/HOUR	pcs
WHITE SPRINGS														

AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	65	SCM SILOS	A	PM	2/9/2005	6.32	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	65	SCM SILOS	A	PM	7/7/2004	3.08	POUNDS/HOUR	PCS TEST TEAM
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	64	SCM Rock Dryer	A	PM	4/23/2003	3.94	POUNDS/HOUR	west dryer (east dryer was 3.15) PCS test team.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	64	SCM Rock Dryer	A	PM	1/13/2005	7.63	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	64	SCM Rock Dryer	A	PM	6/30/2004	2.87	POUNDS/HOUR	In house testing
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	64	SCM Rock Dryer	A	PM	5/4/2006	1.6	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	64	SCM Rock Dryer	A	PM	5/3/2006	2.26	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	21	C SULFURIC ACID PLT W/ DOUBLE ABSORP, BRINKS DEMISTER A	A	SO2	1/8/2003	156.05	POUNDS/HOUR	white Springs Ag Chem test team, QA ok
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	21	C SULFURIC ACID PLT W/ DOUBLE ABSORP, BRINKS DEMISTER A	A	SO2	1/28/2004	262.31	POUNDS/HOUR	PCS test crew. Process rate: 94.1 TPH * 24 HR 2258 TPD
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	21	C SULFURIC ACID PLT W/ DOUBLE ABSORP, BRINKS DEMISTER A	A	SO2	2/18/2005	254.53	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	21	C SULFURIC ACID PLT W/ DOUBLE ABSORP, BRINKS DEMISTER A	A	SO2	1/25/2006	240	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	21	C SULFURIC ACID PLT W/ DOUBLE ABSORP, BRINKS DEMISTER A	A	SO2	1/17/2007	236	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	21	C SULFURIC ACID PLT W/ DOUBLE ABSORP, BRINKS DEMISTER A	A	SO2	2/27/2008	276.51	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	FL	5/5/2004	6.67	POUNDS/HOUR	PCS test team. Producing MAP at 45.5 TPH =
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	FL	5/7/2004	2.42	POUNDS/HOUR	PCS test team. Retest for failure on 5/5/04 prod MAP. Production rate = 34.9 TPH MAP.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	FL	2/6/2003	0.65	POUNDS/HOUR	PCS crew. Process rate = 50.4 TPH
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	FL	3/18/2004	1.54	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	FL	2/3/2005	0.49	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	FL	3/22/2005	1.43	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	FL	8/6/2004	1.01	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	FL	8/6/2004	2.86	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	FL	3/17/2006	0.39	POUNDS/HOUR	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	FL	4/19/2006	0.45	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	FL	2/9/2007	0.58	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	FL	1/31/2008	0.35	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	PM	5/5/2004	49.96	POUNDS/HOUR	PCS test team. Producing MAP at 45.5 TPH =
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	PM	5/5/2004	4.47	POUNDS/HOUR	PCS test team. Retest for failure on 5/5/04 prod MAP. Production rate = 34.9 TPH MAP.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	PM	2/6/2003	3.33	POUNDS/HOUR	PCS crew. Process rate = 50.4 TPH
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	PM	3/18/2004	2	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	PM	2/3/2005	11.46	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	PM	3/22/2005	3.23	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	PM	8/6/2004	4.69	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	PM	8/6/2004	26.3	POUNDS/HOUR	

WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	PM	6/21/2006	5.79	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	PM	3/17/2006	3.79	POUNDS/HOUR	PCS
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	PM	4/19/2006	3.35	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	PM	2/9/2007	1.78	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	8	#1 DAP PLNT "Y"(5 MODES) SCRUBBER,NG,#4FO 1.5% S 34MMBTUH	A	PM	1/31/2008	4.25	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	69	D PHOSPHORIC ACID PLANT	A	FL	11/19/2003	1.22	POUNDS/HOUR	process rate 101.3 T/hr.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	69	D PHOSPHORIC ACID PLANT	A	FL	10/27/2004	0.09	POUNDS/HOUR	On-site test crew.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	69	D PHOSPHORIC ACID PLANT	A	FL	10/20/2005	0.29	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	44	A&B COOLERS (POLLYPHOS)COMMON STACK (EP12)	A	PM	2/26/2003	16.11	POUNDS/HOUR	pcs test crew.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	44	A&B COOLERS (POLLYPHOS)COMMON STACK (EP12)	A	PM	3/3/2005	20.9	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	44	A&B COOLERS (POLLYPHOS)COMMON STACK (EP12)	A	PM	4/28/2004	14.15	POUNDS/HOUR	pcs test crew
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	38	B POLLYPHOS PLANT GAS CALCINER ANIMAL FEED SUPPL	A	FL	4/30/2003	0.21	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	4	X-TRAIN(DICAL)2 OPN MDS:D-18.5,D-21; CNTS-SCBRS&BGCLR	A	FL	5/5/2005	0.28	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	4	X-TRAIN(DICAL)2 OPN MDS:D-18.5,D-21; CNTS-SCBRS&BGCLR	A	FL	10/12/2006	0.24	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	4	X-TRAIN(DICAL)2 OPN MDS:D-18.5,D-21; CNTS-SCBRS&BGCLR	A	FL	2/14/2007	0.21	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	4	X-TRAIN(DICAL)2 OPN MDS:D-18.5,D-21; CNTS-SCBRS&BGCLR	A	FL	10/17/2007	0.27	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	3	A POLLYPHOS PLANT GAS-FIRED CALCINER ANIMAL FEED	A	PM	5/7/2003	8.3	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	3	A POLLYPHOS PLANT GAS-FIRED CALCINER ANIMAL FEED	A	PM	6/15/2005	6.56	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	3	A POLLYPHOS PLANT GAS-FIRED CALCINER ANIMAL FEED	A	PM	6/23/2004	8.12	POUNDS/HOUR	In house testing.
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	4	X-TRAIN(DICAL)2 OPN MDS:D-18.5,D-21; CNTS-SCBRS&BGCLR	A	PM	5/5/2005	12.48	POUNDS/HOUR	
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	4	X-TRAIN(DICAL)2 OPN MDS:D-18.5,D-21; CNTS-SCBRS&BGCLR	A	PM	2/14/2007	12.36	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	3	A POLLYPHOS PLANT GAS-FIRED CALCINER ANIMAL FEED	A	FL	5/7/2003	0.42	POUNDS/HOUR	pcs
WHITE SPRINGS AGRICULTURAL CHEMICALS,INC	0470002	WHITE SPRS AG CHEM-SR/SC CMPLX	NED	HAMILTON	A	Y	3	A POLLYPHOS PLANT GAS-FIRED CALCINER ANIMAL FEED	A	FL	6/15/2005	0.24	POUNDS/HOUR	
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	SO2	11/4/2005	2.4	POUNDS/HOUR	Derived from natural gas analysis.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	SO2	11/9/2004	2.8	POUNDS/HOUR	Determined by natural gas analysis.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	SO2	11/11/2003	1.8	POUNDS/HOUR	Derived from analysis of natural gas on 11/13-11/15/2003.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	SO2	11/4/2005	2.4	POUNDS/HOUR	Derived from analysis of natural gas.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	SO2	11/8/2004	2.85	POUNDS/HOUR	Derived from analysis of natural gas. TECO Environmental Services Air Services Group
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	CO	11/10/2003	0.6	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 828 mmBTU/hr (LHV) new input limit of 911 mmBTU/hr. TECO Air Services Group.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	CO	11/8/2004	1	PARTS PER MILLION DRY GAS VOLUME	Sets new heat input limit of 919 mmBTU/hr, T Environmental Services Air Services Group
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	CO	11/1/2006	1	PARTS PER MILLION DRY GAS VOLUME	
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	CO	11/4/2005	1.7	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 815.9 MMBtu/hr (LHV TECO Environmental Services Air Services Gr
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	CO	12/11/2007	0.87	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Test team: TECO Air Services Gro
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	SO2	11/12/2003	1.8	POUNDS/HOUR	Derived from natural gas analysis 11/13-11/15/
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	SO2	11/10/2004	2.3	POUNDS/HOUR	Value derived from natural gas analysis.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	SO2	11/14/2005	1.64	POUNDS/HOUR	Derived from natural gas analysis.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	VOC	11/12/2003	0.2	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 803 mmBTU/hr (LHV) new input limit of 883 mmBTU/hr. TECO Air Services Group.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	VOC	11/10/2004	0.1	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Sets new heat input limit of 893 mmBTU/hr. TECO Environmental Services Ai Services Group
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	VOC	11/1/2006	0	PARTS PER MILLION DRY GAS VOLUME	

HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	VOC	11/14/2005	0.23	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 836.5 MMBtu/hr (LHV TECO Environmental Services Air Services Gr
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	VOC	12/7/2007	0.02	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Test team: TECO Air Services Gro
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	5	Unit 2B - 75 MW gas turbine	A	VOC	11/13/2003	0.2	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 827 mmBTU/hr. TECO Services Group.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	VOC	11/11/2003	0.2	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 804 mmBTU/hr (LHV) new input limit of 884 mmBTU/hr. TECO Air Services Group.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	VOC	11/9/2004	0.3	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Sets new heat input limit of 927 mmBTU/hr. TECO Environemntal Services Ai Services Group
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	VOC	11/1/2006	0	PARTS PER MILLION DRY GAS VOLUME	
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	VOC	11/4/2005	1	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 810.9 MMBtu/hr. TEC Environmental Services Air Services Group
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	VOC	12/12/2007	0	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Test team: TECO Air Services Gro
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	CO	11/12/2003	0.6	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 803 mmBTU/hr (LHV) new input limit of 883 mmBTU/hr. TECO Air Services Group.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	CO	11/10/2004	1.2	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Sets new heat input limit of 893 mmBTU/hr. TECO Environmental Services Ai Service Group
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	CO	11/1/2006	1.1	PARTS PER MILLION DRY GAS VOLUME	
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	CO	11/14/2005	0.81	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 836.5 MMBtu/hr (LHV TECO Environmental Services Air Services Gr
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	CO	12/7/2007	0.9	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Test team: TECO Air Services Gro
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	CO	11/11/2003	0.7	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 804 mmBTU/hr (LHV) new limit of 884 mmBTU/hr. TECO Air Servic Group.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	CO	11/9/2004	1.6	PARTS PER MILLION DRY GAS VOLUME	Natural gas. New heat input limit 927 mmBTU
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	CO	11/1/2006	1	PARTS PER MILLION DRY GAS VOLUME	
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	CO	11/4/2005	1	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 810.9 MMBtu/hr (LHV TECO Environmental Services Air Services Gr
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	CO	12/12/2007	0.51	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Test team: TECO Air Services Gro
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	VOC	11/10/2003	0.3	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 82 mmBTU/hr (LHV). new limit of 911 mmBTU/hr. TECO Air Servic Group.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	VOC	11/8/2004	0.4	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Sets new heat input limit of 919 mmBTU/hr, TECO Environmental Services Ai Services Group
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	VOC	11/1/2006	0	PARTS PER MILLION DRY GAS VOLUME	
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	VOC	11/4/2005	1	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 815.9 mmBTU/hr (LH TECO Environmental Services Air Services Gr
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	VOC	12/11/2007	0.27	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Test team: TECO Air Services Gro
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	SO2	11/13/2003	1.8	POUNDS/HOUR	Derived from analysis of natural gas. Chromatograph was down on date of test so 11 11/14/ and 11/15 data was averabed and used f calcualtion.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	5	Unit 2B - 75 MW gas turbine	A	CO	12/6/2007	2.974	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Test team: TECO Air Services Gro
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	5	Unit 2B - 75 MW gas turbine	A	CO	11/4/2005	0.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Heat input 788 MMBtu/hr (LHV). TECO Environmental Services Air Services Gr
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	5	Unit 2B - 75 MW gas turbine	A	CO	11/1/2006	5.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	5	Unit 2B - 75 MW gas turbine	A	CO	11/11/2004	1.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Also tested on fuel oil. CO was 0. ppm with heat input of 944 mmBTU/hr. TECO Environmental Services Air Services Group
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	5	Unit 2B - 75 MW gas turbine	A	NOX	12/6/2007	6.631	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Test team: TECO Air Services Gro
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	5	Unit 2B - 75 MW gas turbine	A	NOX	11/1/2006	6.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	NOX	12/7/2007	30.335	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Test team: TECO Air Services Gro
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	NOX	11/10/2003	39.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Heat input 828 mmBTU/hr (LHV) new input limit of 911 mmBTU/hr. TECO Air Services Group
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	NOX	11/8/2004	39.24	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Method 7E. Sets new heat input li 919 mmBTU/hr (LHV). TECO Environmental Services Air Services Group
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	NOX	11/1/2006	37	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	NOX	11/4/2005	39	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Heat input 815.9 MMBtu/hr (LHV TECO Environmental Services Air Services Gr

HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	1	Combustion Turbine 1A with HRSG	A	NOX	12/11/2007	31.77	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Test team: TECO Air Services Gro
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	5	Unit 2B - 75 MW gas turbine	A	NOX	11/13/2003	6.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Heat input 827 mmBTU/hr. TECO Services Group.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	5	Unit 2B - 75 MW gas turbine	A	NOX	11/11/2004	7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. TECO Environmental Services Air Services Group
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	5	Unit 2B - 75 MW gas turbine	A	NOX	11/11/2004	37	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil. Method 7E. TECO Environmental Ser Air Services Group. Permitted heat input is 950 880 which is in ARMS for oil.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	NOX	11/11/2003	38.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Heat input 804 mmBTU/hr (LHV) new limit of 884 mmBTU/hr. TECO Air Servic Group.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	NOX	11/9/2004	33.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Method 7E. Sets new heat input lin 927 mmBTU/hr. TECO Environmental Service Services Group
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	NOX	11/1/2006	37	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	NOX	11/4/2005	38	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Heat input 810.9 MMBtu/hr (LHV TECO Environmental Services Air Services Gr
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	2	Combustion Turbine 1B with HRSG	A	NOX	12/12/2007	36.03	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Test team: TECO Air Services Gro
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	NOX	11/12/2003	42	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Heat input 803 mmBTU/hr (LHV) new input limit of 883 mmBTU/hr. TECO Air Servies Group.
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	NOX	11/10/2004	39	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Sets new heat input limit of 893 mmBTU/hr. TECO Environmental Services Ai Services Group
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	NOX	11/1/2006	33	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	3	Simple cycle Combustion Turbine 2A	A	NOX	11/14/2005	35.354	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Heat input 836.5 MMBtu/hr (LHV TECO Environmental Services Air Services Gr
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	5	Unit 2B - 75 MW gas turbine	A	NOX	11/4/2005	6.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Heat input 788 MMBtu/hr (LHV). TECO Environmental Services Air Services Gr
HARDEE POWER PARTNERS LIMITED	0490015	HARDEE POWER STATION	SWD	HARDEE	A	Y	5	Unit 2B - 75 MW gas turbine	A	CO	11/13/2003	1.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Heat input 827 mmBTU/hr.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/4/2007	39.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/4/2007	7.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/5/2006	6.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy Management Services, Inc. NATUI GAS
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/7/2005	6.14	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Heat input 1641.5 MMBtu/hr (HH GE Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/7/2004	33.03	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil. Heat input 1895.6 mmBTU/hr HHV G Energy Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/19/2003	31.26	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Heat input 1925 MMBtu/hr HHV
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/22/2003	35.44	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Heat input 1869.1 MMBtu/hr HHV
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/22/2003	6.14	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Heat input 1649 MMBtu/hr HHV
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/9/2005	6.84	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Heat input 1643.0 (HHV) GE Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/9/2005	33.92	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil. Heat input 1688.7 MMBtu/hr (HHV) (Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/10/2004	29.47	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil. Heat input 1923.4 mmBTU/hr HHV G Energy Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/10/2004	7.31	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gas. Heat input 1616.2 mmBTU/hr HHV GE Energy Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/7/2006	34.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy Management Services, Inc. FUEL (
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/7/2006	6.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy Management Services, Inc. NATUI GAS
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/4/2007	6.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy

VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/4/2007	30.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/21/2003	33.92	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Heat input 1800 MMBtu/hr HHV
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/21/2003	6.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Heat input 1641 MMBtu/hr HHV
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/8/2005	6.87	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Heat input 1658.7 MMBtu/hr (HH GE Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/8/2005	36.42	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil. Heat input 1722.3 MMBtu/hr (HHV) (Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/8/2004	38.15	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil. Heat input 1937.8 mmBTU/hr HHV G Energy Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/8/2004	6.96	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gas. Heat input 1671.8 mmBTU/hr HHV GE Energy Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/6/2006	32.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy Management Services, Inc. FUEL (
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/6/2006	6.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy Management Services, Inc. NATUI GAS
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/4/2007	7.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/4/2007	39.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/20/2003	5.82	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Heat input 1641 MMBtu/hr HHV
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/6/2005	5.72	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas. Heat input 1638.5 MMBtu/hr (HH GE Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/6/2005	36.24	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil. Heat input 1702.8 MMBtu/hr (HHV) (Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/9/2004	35.83	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil. Heat input 1911 mmBTU/hr HHV GE Energy Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/9/2004	5.99	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gas. Heat input 1635.7 mmBTU/hr GE Energy Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/8/2006	33	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy Management Services, Inc. FUEL (
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/8/2006	5.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy Management Services, Inc. NATUI GAS
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/4/2007	7.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/4/2007	35.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/20/2003	33.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Heat input 1831 MMBtu/hr HHV
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/19/2003	6.07	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Heat input 1643 MMBtu/hr. HHV
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/7/2004	6.56	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gas. Heat input 1639.6 mmBTU/hr HHV GE Energy Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/7/2005	36.73	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil. Heat input 1710.05 MMBtu/hr (HHV) Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/5/2006	33.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE Energy Management Services, Inc. FUEL (
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/4/2007	0.6	PARTS PER MILLION DRY GAS VOLUME	GE Energy
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/4/2007	0.5	PARTS PER MILLION DRY GAS VOLUME	GE Energy
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/5/2006	0.57	PARTS PER MILLION DRY GAS VOLUME	GE Energy Management Services, Inc. FUEL (
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/7/2005	0.79	PARTS PER MILLION DRY GAS VOLUME	Fuel oil. Heat input 1710.05 MMBtu/hr (HHV) Energy Management Services
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/7/2004	0.94	PARTS PER MILLION DRY GAS VOLUME	Oil. Heat input 1895.6. GE Energy Managemer Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/19/2003	0.6	PARTS PER MILLION DRY GAS VOLUME	Heat input 1925 MMBtu/hr HHV
													PARTS PER	

VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/9/2005	0.99	MILLION DRY GAS VOLUME	Fuel oil. Heat input 1688.7 MMBtu/hr (HHV) (Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/10/2004	0.05	PARTS PER MILLION DRY GAS VOLUME	Gas. Heat input 1616.2 mmBTU/hr (HHV) GE Energy Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/10/2004	0.72	PARTS PER MILLION DRY GAS VOLUME	Oil. Heat input 1923.4 mmBTU/hr (HHV) GE Energy Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/7/2006	1.41	PARTS PER MILLION DRY GAS VOLUME	GE Energy Management Services, Inc. NATUI GAS
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/7/2006	0.33	PARTS PER MILLION DRY GAS VOLUME	GE Energy Management Services, Inc. FUEL (
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/4/2007	0.5	PARTS PER MILLION DRY GAS VOLUME	GE Energy
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/4/2007	0.3	PARTS PER MILLION DRY GAS VOLUME	GE Energy
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/21/2003	0.49	PARTS PER MILLION DRY GAS VOLUME	Heat input 1641 MMBtu/hr HHV
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/21/2003	0.27	PARTS PER MILLION DRY GAS VOLUME	Heat input 1800 MMBtu/hr HHV
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/22/2003	0.29	PARTS PER MILLION DRY GAS VOLUME	Heat input 1649 MMBtu/hr HHV
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/22/2003	0.26	PARTS PER MILLION DRY GAS VOLUME	Heat input 1869.1 MMBtu/hr HHV
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	4	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/9/2005	0.82	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 1643.0 MMBtu/hr (HH GE Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/8/2005	0.76	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 1658.7 (HHV) GE Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/8/2005	0.86	PARTS PER MILLION DRY GAS VOLUME	Fuel oil. Heat input 1722.3 (HHV) GE Manage Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/8/2004	0.09	PARTS PER MILLION DRY GAS VOLUME	Gas. Heat input 1671.8 GE Energy Managemer Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/8/2004	0.64	PARTS PER MILLION DRY GAS VOLUME	Oil. Heat input 1937.8 GE Management Servic Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/6/2006	0.26	PARTS PER MILLION DRY GAS VOLUME	GE Energy Management Services, Inc. NATUI GAS
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/6/2006	0.36	PARTS PER MILLION DRY GAS VOLUME	GE Energy Management Services, Inc. FUEL (
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/4/2007	0.5	PARTS PER MILLION DRY GAS VOLUME	GE Energy
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/4/2007	0.6	PARTS PER MILLION DRY GAS VOLUME	GE Energy
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/20/2003	0.37	PARTS PER MILLION DRY GAS VOLUME	Heat input 1831 MMBtu/hr HHV
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/6/2005	0.92	PARTS PER MILLION DRY GAS VOLUME	Fuel oil. Heat input 1702.8 MMBtu/hr (HHV) (Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/9/2004	0.38	PARTS PER MILLION DRY GAS VOLUME	Gas. Heat input 1635.7 mmBTU/hr GE Energy Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/9/2004	0.65	PARTS PER MILLION DRY GAS VOLUME	Oil. Heat input 1911 GE Energy Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/6/2005	0.58	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 1638.5 MMBtu/hr (HH GE Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/8/2006	0.26	PARTS PER MILLION DRY GAS VOLUME	GE Energy Management Services, Inc. NATUI GAS
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/8/2006	0.43	PARTS PER MILLION DRY GAS VOLUME	GE Energy Management Services, Inc. FUEL (
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/4/2007	0.5	PARTS PER MILLION DRY GAS VOLUME	GE Energy
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/4/2007	0.7	PARTS PER MILLION DRY GAS VOLUME	GE Energy
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/20/2003	0.23	PARTS PER MILLION DRY GAS VOLUME	Heat input 1641 MMBtu/hr. HHV
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/19/2003	0.22	PARTS PER MILLION DRY GAS VOLUME	Heat input 1643 MMBtu/hr. HHV
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/7/2004	0.21	PARTS PER MILLION DRY GAS VOLUME	Gas, heat input 1639.6, GE Energy Managemer Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/7/2005	0.69	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 1641.5 MMBtu/hr (HH GE Management Services, Inc.
VANDOLAH POWER COMPANY, LLC	0490043	VANDOLAH POWER PROJECT	SWD	HARDEE	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/5/2006	0.13	PARTS PER MILLION DRY GAS VOLUME	GE Energy Management Services, Inc. NATUI GAS
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	5	PW Twin Pac	A	NOX	9/16/2006	46	POUNDS/HOUR	trc, combined for stack 4A and 4B
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	SO2	10/21/2003	71.563	POUNDS/HOUR	Derived from fuel analysis. Initial testing on fu Sulfur content of fuel oil was 0.05068.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	NH3	8/7/2007	1	PARTS PER MILLION DRY GAS VOLUME	teco, 1683 MMBTU/hr
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	NH3	12/16/2004	1	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Ammonia feed rate 16.5 gph. TEC Power Engineering & Construction's Air Servic Group
SEMINOLE ELECTRIC	0490340	MIDULLA GENERATING	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	CO	12/16/2004	0.2	PARTS PER MILLION DRY	Natural gas. Heat input 1831 mmBTU/hr TEC(

COOPERATIVE, INC.		STATION											GAS VOLUME	Environmental Services
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	CO	12/8/2005	0	PARTS PER MILLION DRY GAS VOLUME	
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	CO	8/7/2007	0	PARTS PER MILLION DRY GAS VOLUME	teco, 1746 MMBtu/hr
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	VOC	11/7/2003	0.5	PARTS PER MILLION DRY GAS VOLUME	Heat input 1765 mmBTU/hr. Testing on natura TECO Power Engineering & Construction.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	VOC	10/21/2003	0.19	PARTS PER MILLION DRY GAS VOLUME	Heat input 1412 mmBTU/hr. Initial testing on f oil. TECO Power Engineering & Construction.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	VOC	12/16/2004	0.2	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Heat input 1831 mmBTU/hr. TEC Environmental Services Group
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	VOC	12/8/2005	2	PARTS PER MILLION DRY GAS VOLUME	
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	VOC	8/7/2007	7	PARTS PER MILLION DRY GAS VOLUME	teco, 1746 MMBtu/hr
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	VOC	9/17/2007	0	PARTS PER MILLION DRY GAS VOLUME	teco, 1726 MMBTU/hr
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	NOX	12/6/2005	8	PARTS PER MILLION DRY GAS VOLUME	Method 7E
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	NOX	8/7/2007	7	PARTS PER MILLION DRY GAS VOLUME	teco
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	CO	11/5/2003	0.3	PARTS PER MILLION DRY GAS VOLUME	Heat input 1778 mmBTU/hr. TECO Power Engineering & Construction.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	CO	10/28/2003	0.5	PARTS PER MILLION DRY GAS VOLUME	Heat input 1659.7 mmBTU/hr. Initial testing or oil. Testing performed by Siemens Source Test and Consulting Services, Inc.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	CO	12/14/2004	0.14	PARTS PER MILLION DRY GAS VOLUME	
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	CO	12/6/2005	0	PARTS PER MILLION DRY GAS VOLUME	
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	CO	8/7/2007	0	PARTS PER MILLION DRY GAS VOLUME	teco
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	CO	11/7/2003	0.02	PARTS PER MILLION DRY GAS VOLUME	Heat input 1765 mmBTU/hr. Testing on natura TECO Power Engineering & Construction
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	CO	10/19/2003	0.03	PARTS PER MILLION DRY GAS VOLUME	Heat input 1660.9 mmBTU/hr. Initial testing or oil. Siemens Source Testing & Consulting Serv
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	VOC	8/7/2007	6	PARTS PER MILLION DRY GAS VOLUME	teco, 1695 MMBtu/hr
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	NOX	11/7/2003	8	PARTS PER MILLION DRY GAS VOLUME	Heat input 1765. Testing on natural gas. TECO Power Engineering & Construction. Derived fr CEMs data.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	NOX	10/21/2003	38	PARTS PER MILLION DRY GAS VOLUME	Heat input 1412 mmBTU/hr. Initial testing on f oil. TECO Power Engineering & Construction. Derived from CEMs data.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	NOX	12/16/2004	8.28	PARTS PER MILLION DRY GAS VOLUME	Natural gas. Method 7E. Heat input 1831 mmBTU/hr. TECO Environmental Services
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	NOX	12/8/2005	8	PARTS PER MILLION DRY GAS VOLUME	Method 7E
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	NOX	8/7/2007	8	PARTS PER MILLION DRY GAS VOLUME	teco
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	NOX	11/5/2003	8.06	PARTS PER MILLION DRY GAS VOLUME	Heat input 1778 mmBTU/hr. Derived from CE data. TECO Power Engineering & Constructio
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	NOX	10/29/2003	34.9	PARTS PER MILLION DRY GAS VOLUME	Heat input 1424 mmBTU/hr. Initial testing on f oil. Emissions derived from CEMs data. TECO Power Engineering & Construction.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	NOX	12/14/2004	8.79	PARTS PER MILLION DRY GAS VOLUME	Natural gas. TECO Power Engineering & Construction, Air Services Group
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	NH3	12/6/2005	1	PARTS PER MILLION DRY GAS VOLUME	
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	NH3	8/9/2007	1	PARTS PER MILLION DRY GAS VOLUME	teco, 1695 MMBtu/hr
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	VOC	11/5/2003	0.25	PARTS PER MILLION DRY GAS VOLUME	Heat input 1778 mmBTU/hr. TECO Power Engineering & Construction.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	VOC	10/29/2003	0.23	PARTS PER MILLION DRY GAS VOLUME	Heat input 1424 mmBTU/hr. Initial testing on f oil. TECO Power Engineering & Construction.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	VOC	12/14/2004	0.000001	PARTS PER MILLION DRY GAS VOLUME	
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	VOC	12/6/2005	1	PARTS PER MILLION DRY GAS VOLUME	
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	VOC	9/17/2007	2	PARTS PER MILLION DRY GAS VOLUME	teco, 1658 MMBtu/hr
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	NH3	12/8/2005	1	PARTS PER MILLION DRY GAS VOLUME	Load during test 169 Mwe
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	SO2	11/7/2003	0.12	POUNDS/HOUR	Derived from average daily content of gas strea
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	SO2	12/16/2004	0.24	POUNDS/HOUR	Natural gas. Analysis of natural gas stream. TE Environmental Services Group.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	SO2	8/7/2007	0	POUNDS/HOUR	teco
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	SO2	12/8/2005	2	POUNDS/HOUR	Results derived from fuel analysis

SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	6	PW Twin Pac	A	NOX	9/9/2006	37	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	trc
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	8	PW Twin Pac	A	NOX	8/18/2006	23.706	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FIRING PNG - FAILED ON PPM BUT PASS COMBINED LB/HR (UNIT 7A 23.032 + UNI 23.706=46.738) ALLOWABLE IS 51.0
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	8	PW Twin Pac	A	CO	8/18/2006	3.667	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FIRING PNG
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	7	PW Twin Pac	A	CO	8/24/2006	3.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FIRING PNG
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	7	PW Twin Pac	A	CO	8/24/2006	4.27	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	7	PW Twin Pac	A	CO	8/24/2006	0.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FIRING OIL
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	7	PW Twin Pac	A	CO	8/24/2006	0.26	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FIRING OIL
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	5	PW Twin Pac	A	CO	9/16/2006	4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	trc, combined for stack 4A and 4B
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	5	PW Twin Pac	A	CO	9/16/2006	1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	trc, combined stack 4A and 4B
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	5	PW Twin Pac	A	CO	9/16/2006	4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	trc, combined stack 4A and 4B
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	8	PW Twin Pac	A	CO	8/18/2006	0.55	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FIRING OIL
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	8	PW Twin Pac	A	CO	8/18/2006	0.445	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FIRING OIL
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	9	PW Twin Pac	A	CO	9/22/2006	4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	trc, combined total of 8A and 8B
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	9	PW Twin Pac	A	CO	9/22/2006	5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TRC
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	9	PW Twin Pac	A	CO	9/22/2006	1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	trc, combined stack 8A and 8B
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	9	PW Twin Pac	A	CO	9/22/2006	1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	trc, combined for stack 8A and 8B
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	5	PW Twin Pac	A	NOX	9/16/2006	38	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	trc, combined stack 4A and 4B
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	8	PW Twin Pac	A	CO	8/18/2006	2.93	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FIRING PNG
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	8	PW Twin Pac	A	NOX	8/18/2006	37.81	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FIRING OIL
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	9	PW Twin Pac	A	NOX	9/22/2006	36	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	trc, combined for stacks 8A and 8B
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	9	PW Twin Pac	A	NOX	9/22/2006	36	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	trc, combined stack 8A and 8B
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	8	PW Twin Pac	A	NOX	8/18/2006	21.29	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FIRING PNG - TEST FAILED AS PPM BUT PASSED ON LB/HR EQUIVALENT PER PERMIT (UNIT A 23.03+UNIT B 23.706=46. ALLOWABLE IS 51.0
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	8	PW Twin Pac	A	NOX	8/18/2006	38.72	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FIRING OIL
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	NH3	12/14/2004	1	PARTS PER MILLION DRY GAS VOLUME	
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	6	PW Twin Pac	A	NOX	9/9/2006	46	POUNDS/HOUR	combined for 5A and 5B
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	SAM	8/7/2007	1	POUNDS/HOUR	teco
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	SAM	12/14/2004	0	POUNDS/HOUR	Natural gas. TECO Power Engineering & Construction, Air Services Group
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	SAM	11/5/2003	0	POUNDS/HOUR	Heat input 1778 mmBTU/hr. Natural gas. TEC Power Engineering & Construction.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	PM	10/29/2003	15.4	POUNDS/HOUR	Heat input 1424 mmBTU/hr. Initial testing on f oil. TECO Power Engineering & Construction.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	SAM	10/21/2003	20.3	POUNDS/HOUR	Heat input 1402 mmBTU/hr. Initial testing on f oil. TECO Power Engineering & Construction.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	SAM	12/16/2004	0	POUNDS/HOUR	Natural gas. TECO Environmental Services Gr
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	SAM	12/8/2005	0	POUNDS/HOUR	

SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	SAM	8/7/2007	3	POUNDS/HOUR	teco
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	SAM	9/17/2007	0	POUNDS/HOUR	teco
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	SO2	11/5/2003	0.12	POUNDS/HOUR	Derived from average daily sulfur content of ga stream 10/14-11/15 because the FGT SO2 analy was down during the test date.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	SO2	10/29/2003	57.876	POUNDS/HOUR	Derived from fuel analysis. Initial testing on fu Heat input 1424 mmBTU/hr.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	SO2	12/6/2005	1	POUNDS/HOUR	Derived from Fuel Analysis
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	SO2	8/7/2007	0	POUNDS/HOUR	teco
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	SAM	11/7/2003	0	POUNDS/HOUR	Heat input 1765 mmBTU/hr. Testing on natura
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	9	PW Twin Pac	A	NOX	9/22/2006	48	POUNDS/HOUR	combied total for stack 8A and 8B
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	SAM	10/29/2003	12.749	POUNDS/HOUR	Heat input 1424 mmBTU/hr. Initial testing on f oil. TECO Power Engineering & Construction.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	2	CTG/HRSG Unit 2	A	SAM	12/6/2005	0	POUNDS/HOUR	
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	1	CTG/HRSG Unit 1	A	PM	10/21/2003	29.1	POUNDS/HOUR	Heat input 1422 mmBTU/hr. Initial testing on f oil. TECO Power Engineering & Construction. method 5B.
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	6	PW Twin Pac	A	CO	9/9/2006	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	trc
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	6	PW Twin Pac	A	CO	9/9/2006	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	7	PW Twin Pac	A	NOX	8/24/2006	19.92	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	7	PW Twin Pac	A	NOX	8/24/2006	37.42	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FIRING OIL
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	7	PW Twin Pac	A	NOX	8/24/2006	38.08	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FIRING OIL
SEMINOLE ELECTRIC COOPERATIVE, INC.	0490340	MIDULLA GENERATING STATION	SWD	HARDEE	A	Y	7	PW Twin Pac	A	NOX	8/24/2006	19.89	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FIRING PNG
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	CO	1/24/2008	0.295	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	VOC	1/24/2008	0.003	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	VOC	1/5/2006	0.008	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	CO	1/13/2006	2.34	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	CO	12/1/2006	4.19	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	CO	11/14/2007	2.614	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	PM	11/21/2003	0.127	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	PM	11/24/2004	0.129	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	PM	1/13/2006	0.092	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	PM	12/1/2006	0.09	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	PM	11/14/2007	0.108	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	VOC	2/4/2005	0.006	POUNDS PER MILLION BTU HEAT INPUT	POUNDS PER MILLION BTU HEAT INPUT
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	VOC	11/24/2004	0.51	POUNDS PER MILLION BTU HEAT INPUT	actual calculated after backing methane out due high drift
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	VOC	1/13/2006	0.083	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	VOC	12/1/2006	0.209	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	VOC	11/14/2007	0.15	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	PM	12/30/2003	0.015	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	PM	2/4/2005	0.021	POUNDS PER MILLION BTU HEAT INPUT	POUNDS PER MILLION BTU HEAT INPUT
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	PM	1/5/2006	0.015	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP.	0510003	U.S. SUGAR CLEWISTON MILL	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr	A	PM	1/25/2007	0.028	POUNDS PER MILLION BTU	

CLEWISTON MILL		AND REFINERY						steam rate (1-hr max.)					HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	PM	1/24/2008	0.005	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	NOX	12/30/2003	0.203	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	NOX	10/1/2003	0.158	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	NOX	2/4/2005	0.21	POUNDS PER MILLION BTU HEAT INPUT	POUNDS PER MILLION BTU HEAT INPUT
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	NOX	1/5/2006	0.199	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	NOX	1/25/2007	0.212	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	NOX	1/24/2008	0.154	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	CO	11/21/2003	3.926	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	CO	11/24/2004	3.803	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	2	Boiler 2 - 230,000 lb/hr steam rate (1-hr max.)	A	PM	11/12/2004	0.152	POUNDS PER MILLION BTU HEAT INPUT	test started on 11/12 aborted on run 3 whe boile blew a tube completed on the 17th
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	2	Boiler 2 - 230,000 lb/hr steam rate (1-hr max.)	A	PM	12/14/2005	0.185	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	2	Boiler 2 - 230,000 lb/hr steam rate (1-hr max.)	A	PM	11/21/2006	0.175	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	2	Boiler 2 - 230,000 lb/hr steam rate (1-hr max.)	A	PM	11/4/2007	0.188	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	VOC	3/24/2005	0.012	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	VOC	1/10/2006	0.012	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	VOC	1/5/2007	0.031	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	VOC	11/29/2007	0.025	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	VOC	11/21/2003	0.443	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	PM	3/24/2005	0.004	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	PM	1/10/2006	0.021	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	PM	6/2/2006	0.0023	POUNDS PER MILLION BTU HEAT INPUT	Low Steam MACT testing
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	PM	1/5/2007	0.0111	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	PM	1/5/2007	0.01	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	PM	11/29/2007	0.015	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	3	Boiler 3 - 130,000 lb/hr steam rate (1-hr max.)	I	PM	11/11/2003	0.28	POUNDS PER MILLION BTU HEAT INPUT	Production is limited on this boiler. Steam Rate not exceed 75692 lbs/ hr.
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	3	Boiler 3 - 130,000 lb/hr steam rate (1-hr max.)	I	PM	11/9/2004	0.184	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	2	Boiler 2 - 230,000 lb/hr steam rate (1-hr max.)	A	PM	11/18/2003	0.199	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	SO2	3/25/2005	0.025	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	SO2	1/10/2006	0.021	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	SO2	1/6/2007	0.032	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	SO2	11/29/2007	0.014	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	NOX	3/25/2005	0.131	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	NOX	9/16/2005	0.099	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	NOX	6/2/2006	0.11	POUNDS PER MILLION BTU HEAT INPUT	Low Steam MACT Testing
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	CO	3/24/2005	0.354	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	CO	9/16/2005	0.461	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	CO	11/29/2007	0.447	POUNDS PER MILLION BTU HEAT INPUT	Info purpose only comp. based on 30 day ave. v CEM, this is ave. of 10 RATA runs
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	1	Boiler 1 - 255,000 lb/hr steam rate (1-hr max.)	A	PM	11/14/2003	0.175	POUNDS PER MILLION BTU HEAT INPUT	Production is limited. Steam rate is 204,000 lbs +/- 10%

U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	1	Boiler 1 - 255,000 lb/hr steam rate (1-hr max.)	A	PM	1/13/2005	0.188	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	1	Boiler 1 - 255,000 lb/hr steam rate (1-hr max.)	A	PM	12/16/2005	0.209	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	1	Boiler 1 - 255,000 lb/hr steam rate (1-hr max.)	A	PM	11/28/2006	0.121	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	1	Boiler 1 - 255,000 lb/hr steam rate (1-hr max.)	A	PM	11/9/2007	0.177	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	VOC	1/25/2007	0.0017	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	CO	12/30/2003	0.619	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	CO	1/25/2007	0.341	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	CO	1/5/2006	0.216	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	CO	2/4/2005	0.167	POUNDS PER MILLION BTU HEAT INPUT	POUNDS PER MILLION BTU HEAT INPUt
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	SO2	1/24/2008	0.039	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	NOX	11/14/2007	0.081	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	NOX	1/13/2006	0.06	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	NOX	2/9/2005	0.107	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	29	White Sugar Dryer No. 2	A	PM	2/20/2007	9	POUNDS/HOUR	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	17	Granular carbon regeneration furnace	A	VOC	9/28/2005	0.0927	POUNDS/HOUR	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	1	Boiler 1 - 255,000 lb/hr steam rate (1-hr max.)	A	SO2	2/7/2005	0	POUNDS/HOUR	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	NOX	11/21/2003	0.135	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	NOX	11/24/2004	0.101	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	9	Boiler 4 - 300,000 lb/hr steam rate (1-hr max.)	A	NOX	12/1/2006	0.083	POUNDS PER MILLION BTU HEAT INPUT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	14	Boiler 7 - 385,000 lb/hr steam rate (1-hr max.)	A	SO2	2/4/2005	0.065	POUNDS PER MILLION BTU HEAT INPUT	POUNDS PER MILLION BTU HEAT INPUT
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	17	Granular carbon regeneration furnace	A	PM	9/28/2005	0.386	POUNDS/HOUR	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	29	White Sugar Dryer No. 2	A	PM10	2/20/2007	0.00269	GRAINS PER DRY STANDARD CUBIC FOOT	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	NH3	1/10/2006	14.47	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	NH3	1/5/2007	20.67	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	NH3	1/25/2008	20.37	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	28	Boiler 8 - Bagasse boiler rated at 500,000 lb/hour steam	A	NH3	11/29/2007	22.16	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
U.S. SUGAR CORP. CLEWISTON MILL	0510003	U.S. SUGAR CLEWISTON MILL AND REFINERY	SD	HENDRY	A	Y	29	White Sugar Dryer No. 2	A	PM	12/7/2005	0.014	GRAINS PER DRY STANDARD CUBIC FOOT	test resched. for 01/26/06 notified that morning is down
SOUTHERN GARDENS CITRUS PROCESSING CORP.	0510015	SOUTHERN GARDENS CITRUS PROCESSING CORP.	SD	HENDRY	A	Y	20	No. 4 Pellet Cooler	A	PM	4/26/2007	0.21	POUNDS/HOUR	
SOUTHERN GARDENS CITRUS PROCESSING CORP.	0510015	SOUTHERN GARDENS CITRUS PROCESSING CORP.	SD	HENDRY	A	Y	19	Backup Peel Dryer No. 2	A	PM	1/28/2003	8.04	POUNDS/HOUR	
SOUTHERN GARDENS CITRUS PROCESSING CORP.	0510015	SOUTHERN GARDENS CITRUS PROCESSING CORP.	SD	HENDRY	A	Y	3	CITRUS FEED MILL WITH WASTE HEAT EVAPORATOR	A	PM	2/22/2006	12.5	POUNDS/HOUR	
SOUTHERN GARDENS CITRUS PROCESSING CORP.	0510015	SOUTHERN GARDENS CITRUS PROCESSING CORP.	SD	HENDRY	A	Y	3	CITRUS FEED MILL WITH WASTE HEAT EVAPORATOR	A	PM	4/25/2007	11.95	POUNDS/HOUR	Facility is limited to 80 MMBtu/Hr
SOUTHERN GARDENS CITRUS PROCESSING CORP.	0510015	SOUTHERN GARDENS CITRUS PROCESSING CORP.	SD	HENDRY	A	Y	3	CITRUS FEED MILL WITH WASTE HEAT EVAPORATOR	A	PM	2/21/2008	7.57	POUNDS/HOUR	
SOUTHERN GARDENS CITRUS PROCESSING CORP.	0510015	SOUTHERN GARDENS CITRUS PROCESSING CORP.	SD	HENDRY	A	Y	19	Backup Peel Dryer No. 2	A	PM	4/14/2004	9.66	POUNDS/HOUR	
SOUTHERN GARDENS CITRUS PROCESSING CORP.	0510015	SOUTHERN GARDENS CITRUS PROCESSING CORP.	SD	HENDRY	A	Y	19	Backup Peel Dryer No. 2	A	PM	4/14/2004	9.66	POUNDS/HOUR	
SOUTHERN GARDENS CITRUS PROCESSING CORP.	0510015	SOUTHERN GARDENS CITRUS PROCESSING CORP.	SD	HENDRY	A	Y	20	No. 4 Pellet Cooler	A	PM	1/29/2003	0.723	POUNDS/HOUR	production rate, 13.5TPH, for test
SOUTHERN GARDENS CITRUS PROCESSING CORP.	0510015	SOUTHERN GARDENS CITRUS PROCESSING CORP.	SD	HENDRY	A	Y	19	Backup Peel Dryer No. 2	A	PM	3/1/2007	1.6	POUNDS/HOUR	C.E.M. Solutions
SOUTHERN GARDENS CITRUS	0510015	SOUTHERN GARDENS CITRUS PROCESSING	SD	HENDRY	A	Y	19	Backup Peel Dryer No. 2	A	PM	3/1/2007	3.5	POUNDS/HOUR	C. E. M. Solutions

PROCESSING CORP.		CORP.												
SOUTHERN GARDENS CITRUS PROCESSING CORP.	0510015	SOUTHERN GARDENS CITRUS PROCESSING CORP.	SD	HENDRY	A	Y	9	PELLET COOLER #3	A	PM	3/1/2007	0.2	POUNDS/HOUR	C.E.M. Solutions
SOUTHERN GARDENS CITRUS PROCESSING CORP.	0510015	SOUTHERN GARDENS CITRUS PROCESSING CORP.	SD	HENDRY	A	Y	9	PELLET COOLER #3	A	PM	4/26/2007	0.39	POUNDS/HOUR	
SOUTHERN GARDENS CITRUS PROCESSING CORP.	0510015	SOUTHERN GARDENS CITRUS PROCESSING CORP.	SD	HENDRY	A	Y	3	CITRUS FEED MILL WITH WASTE HEAT EVAPORATOR	A	NOX	2/21/2008	0.11	POUNDS PER MILLION BTU HEAT INPUT	
CITRUS SERVICE, INC.	0530004	CITRUS SERVICE, INC.	SWD	HERNANDO	I	Y	3	CITRUS PEEL DRYER W/WASTE HEAT EVAPORATOR	I	PM	12/22/2003	1.17	POUNDS/HOUR	
CITRUS SERVICE, INC.	0530004	CITRUS SERVICE, INC.	SWD	HERNANDO	I	Y	5	PEEL COOLER	I	PM	12/17/2003	2.767	POUNDS/HOUR	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	5	FINISH MILLS #1 & #2 WITH TWO DUST COLLECTORS	A	PM	9/11/2007	1.81	POUNDS/HOUR	50% rate
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	5	FINISH MILLS #1 & #2 WITH TWO DUST COLLECTORS	A	PM	9/29/2005	0.91	POUNDS/HOUR	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	9	Portland Cement Storage Silos Nos. 1-5	A	PM	3/3/2003	0.07	POUNDS/HOUR	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	5	FINISH MILLS #1 & #2 WITH TWO DUST COLLECTORS	A	PM	9/26/2005	0.91	POUNDS/HOUR	0.05 CFM FINAL LEAK CHECK --- TEST VOLUME ADJUSTED.
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	PM	8/27/2003	9.42	POUNDS/HOUR	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	PM	11/4/2005	8.7	POUNDS/HOUR	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	PM	9/11/2007	8.1	POUNDS/HOUR	RAW MILL ON
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	15	NO. 2 CLINKER COOLER W/BAGHOUSE K-09	A	PM	8/27/2003	7.73	POUNDS/HOUR	93tph preheater feed rate
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	15	NO. 2 CLINKER COOLER W/BAGHOUSE K-09	A	PM	9/10/2004	4.73	POUNDS/HOUR	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	15	NO. 2 CLINKER COOLER W/BAGHOUSE K-09	A	PM	9/13/2006	7.97	POUNDS/HOUR	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	15	NO. 2 CLINKER COOLER W/BAGHOUSE K-09	A	PM	11/4/2005	9.29	POUNDS/HOUR	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	5	FINISH MILLS #1 & #2 WITH TWO DUST COLLECTORS	A	PM	9/12/2006	5.18	POUNDS/HOUR	Finish mill 1: 1.00 lb/hr PM. Finish mill 2: 5.1 lb/hr PM. Total: 6.18 lb/hr.
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	5	FINISH MILLS #1 & #2 WITH TWO DUST COLLECTORS	A	PM	9/10/2007	0.39	POUNDS/HOUR	50% rate
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	DIOX	8/26/2003	0.074	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	DIOX	8/29/2003	23.59	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	raw mill off baghouse 436 F
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	DIOX	1/24/2007	0.307	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RAW MILL OFF BAGHOUSE INLET 371 F
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	DIOX	1/4/2007	0.003	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RAW MILL ON W/TIRES 1.4 TPH BAGHOU 268 DEG F
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	DIOX	6/16/2005	0.0902	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RAW MILL OFF BAGHOUSE 371 DEG F
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	DIOX	11/21/2003	29.2	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	DIOX	4/2/2005	2.48441	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	DIOX	8/6/2004	0.166	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RAW MILL OFF -- BAGHOUSE 399 DEG F
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	DIOX	1/18/2006	0.0139	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RAW MILL ON -- BAGHOUSE 251 F 30 M TEST
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	DIOX	1/24/2007	0.307	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RAW MILL OFF BAGHOUSE 371 DEG F
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	NOX	9/12/2007	0.859	POUNDS PER TON OF FEED MATERIAL	raw mill on - using wtf
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	NOX	9/12/2007	0.859	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	NOX	12/13/2006	0.902	POUNDS PER TON OF FEED MATERIAL	sncr average feed 1.4 gpm

CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	NOX	9/29/2005	1.77	POUNDS PER TON OF FEED MATERIAL	SNCR OFF
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	NOX	12/20/2005	1.13	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	NOX	9/11/2003	1.14667	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	4	CEMENT PLANT CLINKER COOLER NO. 1 (BAGHOUSE F-18)	A	PM	9/12/2007	0.00912	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	4	CEMENT PLANT CLINKER COOLER NO. 1 (BAGHOUSE F-18)	A	PM	9/28/2005	0.032	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	SO2	3/10/2003	0.0133	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	SO2	8/26/2003	0.00897	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	SO2	9/10/2004	0.0127	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	SO2	9/28/2005	0.0096	POUNDS PER TON OF FEED MATERIAL	SNCR ON
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	SO2	9/28/2005	0.016	POUNDS PER TON OF FEED MATERIAL	SNCR OFF
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	SO2	9/13/2006	0.035	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	SO2	11/4/2005	0.029	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	SO2	9/11/2007	0.011	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	SO2	9/11/2007	0.011	POUNDS PER TON OF FEED MATERIAL	rm on
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	SO2	2/6/2008	0.01049	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	CO	9/11/2003	0.87	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	CO	9/21/2004	0.382	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	CO	12/20/2005	0.61	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	CO	9/28/2005	0.36	POUNDS PER TON OF FEED MATERIAL	SNCR ON
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	CO	9/29/2005	0.42	POUNDS PER TON OF FEED MATERIAL	SNCR OFF
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	CO	9/13/2006	0.632	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	CO	12/13/2006	0.645	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	CO	9/12/2007	0.701	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	CO	9/12/2007	0.701	POUNDS PER TON OF FEED MATERIAL	raw mill on - using wtf
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	PM	9/13/2007	0.0858	POUNDS PER TON OF FEED MATERIAL	raw mill off
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	PM	9/11/2007	0.0558	POUNDS PER TON OF FEED MATERIAL	raw mill on
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	PM	2/6/2008	0.0459	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	SO2	9/11/2003	0.0233	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	SO2	9/21/2004	0.00066	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	SO2	12/20/2005	0.008	POUNDS PER TON OF FEED MATERIAL	
		BROOKSVILLE						CEMENT KILN NO. 1					POUNDS PER	

CEMEX CEMENT, INC.	0530010	NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	SO2	9/28/2005	0.002	TON OF FEED MATERIAL	SNCR ON
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	SO2	9/29/2005	0.021	POUNDS PER TON OF FEED MATERIAL	SNCR OFF
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	SO2	9/13/2006	0.004	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	PM	3/10/2003	0.022	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	PM	9/10/2004	0.0787	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	PM	8/27/2003	0.0604	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	PM	9/27/2005	0.065	POUNDS PER TON OF FEED MATERIAL	SNCR ON
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	PM	9/13/2006	0.064	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	PM	9/13/2007	0.0858	POUNDS PER TON OF FEED MATERIAL	RAW MILL DOWN
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	SO2	12/13/2006	0.005	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	SO2	9/12/2007	0.0092	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	SO2	2/12/2007	0.00922	POUNDS PER TON OF FEED MATERIAL	raw mill down
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	CO	3/10/2003	0.716	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	CO	8/26/2003	0.705	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	CO	9/10/2004	0.68	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	CO	9/28/2005	0.717	POUNDS PER TON OF FEED MATERIAL	SNCR ON
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	CO	9/28/2005	0.98	POUNDS PER TON OF FEED MATERIAL	SNCR OFF
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	CO	9/13/2006	0.64	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	CO	11/4/2005	0.528	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	CO	9/11/2007	0.434	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	CO	9/11/2007	0.434	POUNDS PER TON OF FEED MATERIAL	raw mill on
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	15	NO. 2 CLINKER COOLER W/BAGHOUSE K-09	A	PM	3/7/2003	0.04	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	15	NO. 2 CLINKER COOLER W/BAGHOUSE K-09	A	PM	9/27/2005	0.011	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	15	NO. 2 CLINKER COOLER W/BAGHOUSE K-09	A	PM	9/11/2007	0.0479	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	PM	9/28/2005	0.04	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	PM	9/13/2006	0.0645	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	PM	12/13/2006	0.0925	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	PM	9/12/2007	0.0546	POUNDS PER TON OF FEED MATERIAL	RAW MILL ON
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	PM	9/13/2007	0.0726	POUNDS PER TON OF FEED MATERIAL	RAW MILL DOWN
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	PM	9/13/2007	0.0858	POUNDS PER TON OF FEED MATERIAL	raw mill off
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL	A	PM	9/12/2007	0.0726	POUNDS PER TON OF FEED MATERIAL	raw mill on - wtdf used

								CONCENTRATIONS						
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	PM	9/12/2007	0.0546	POUNDS PER TON OF FEED MATERIAL	raw mill on using wtf
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	NOX	11/4/2005	1.2	POUNDS PER TON OF FEED MATERIAL	SNCR ON
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	PM	9/11/2003	0.0468	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	PM	8/29/2003	0.013	POUNDS PER TON OF FEED MATERIAL	draft, raw mill down
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	PM	9/21/2004	0.045	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	PM	12/20/2005	0.009	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	NOX	9/13/2006	1.61	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	NOX	11/4/2005	1.203	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	NOX	9/11/2007	0.759	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	NOX	9/11/2007	0.759	POUNDS PER TON OF FEED MATERIAL	raw mill on
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	VOC	2/6/2008	0.038	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	4	CEMENT PLANT CLINKER COOLER NO. 1 (BAGHOUSE F-18)	A	PM	9/12/2003	0.052	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	4	CEMENT PLANT CLINKER COOLER NO. 1 (BAGHOUSE F-18)	A	PM	9/21/2004	0.015	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	4	CEMENT PLANT CLINKER COOLER NO. 1 (BAGHOUSE F-18)	A	PM	12/20/2005	0.07	POUNDS PER TON OF FEED MATERIAL	6 test runs due to malfunction of baghouse duri first run
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	NOX	3/10/2003	1.7	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	NOX	8/26/2003	1.31	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	NOX	9/10/2004	0.96	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	NOX	9/28/2005	1.42	POUNDS PER TON OF FEED MATERIAL	SNCR ON
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	NOX	9/28/2005	2.21	POUNDS PER TON OF FEED MATERIAL	SNCR OFF. TEST REQUIRED BY FDEP-NO NORMAL OPERATING CONDITION
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	4	CEMENT PLANT CLINKER COOLER NO. 1 (BAGHOUSE F-18)	A	PM	9/13/2006	0.0443	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	4	CEMENT PLANT CLINKER COOLER NO. 1 (BAGHOUSE F-18)	A	PM	9/12/2007	0.00518	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	NOX	9/21/2004	1.72	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	NOX	9/28/2005	1.5	POUNDS PER TON OF FEED MATERIAL	SNCR ON
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	3	CEMENT KILN NO. 1 BAGHOUSE(E-55);REVISED OIL CONCENTRATIONS	A	NOX	9/13/2006	1.36	POUNDS PER TON OF FEED MATERIAL	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	DIOX	2/7/2008	0.006	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	DIOX	3/31/2005	0.02212	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	raw mill down baghouse temp 398.76 F
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	DIOX	8/6/2003	0.0125	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	group testing completed 8/29
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	DIOX	3/12/2003	116.5	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	baghouse inlet temp.= 552 F
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	DIOX	12/4/2003	4.8	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RAW MILL DOWN -- BAGHOUSE 391 F
CEMEX CEMENT,		BROOKSVILLE						CEMENT KILN NO. 2 BAGHOUSE(E-19);					NANOGRAMS PER DRY	NOT ACCEPTED--INSUFFICIENT SAMPLII

INC.	0530010	NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	REVISED OIL CONCENTRATIONS	A	DIOX	6/11/2004	0.109	STANDARD CUBIC METER @ 7% O2	POINTS
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	DIOX	3/12/2003	116.5	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	baghouse 552 deg f
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	DIOX	1/19/2006	0.0084	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RAW MILL ON--BAGHOUSE 254 F 30-MON TEST
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	DIOX	8/25/2003	1.079	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RAW MILL DOWN BAGHOUSE 442 DEG. F
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	DIOX	7/30/2004	0.0512	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RAW MILL OFF -- RETEST OF 6/11/4 TEST USING PROPER SAMPLING POINTS - BAGHOUSE 397 F
CEMEX CEMENT, INC.	0530010	BROOKSVILLE NORTH CEMENT PLANT	SWD	HERNANDO	A	Y	14	CEMENT KILN NO. 2 BAGHOUSE(E-19); REVISED OIL CONCENTRATIONS	A	DIOX	1/18/2007	16.88	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RAW MILL OFF BAGHOUSE INLET 395 F
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	PM	9/6/2007	44.28	POUNDS/HOUR	CP + PP
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	NOX	10/19/2004	2.09	POUNDS PER TON OF FEED MATERIAL	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	NOX	1/13/2003	2.5	POUNDS PER TON OF FEED MATERIAL	341 lb/hr, 132 tph feedrate
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	SO2	11/23/2005	0.03904	POUNDS PER TON OF FEED MATERIAL	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	SO2	3/16/2004	0.016	POUNDS PER TON OF FEED MATERIAL	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	PM	10/30/2007	0.26	POUNDS PER TON OF FEED MATERIAL	32.67 lb/hr @ 137 tph preheater feed rate (126 kiln feed rate)
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	PM	1/13/2003	0.04	POUNDS PER TON OF FEED MATERIAL	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	PM	3/16/2004	0.11	POUNDS PER TON OF FEED MATERIAL	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	PM	10/20/2004	0.05	POUNDS PER TON OF FEED MATERIAL	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	PM	11/23/2005	0.1204	POUNDS PER TON OF FEED MATERIAL	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	PM	11/24/2005	0.12	POUNDS PER TON OF FEED MATERIAL	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	PM	9/5/2006	0.319	POUNDS PER TON OF FEED MATERIAL	KILN, COOLER, AND POWER PLANT
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	PM	10/24/2006	0.1385	POUNDS PER TON OF FEED MATERIAL	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	SO2	1/13/2003	0.48	POUNDS PER TON OF FEED MATERIAL	6.4 lb/hr meth. 6C, 216 mmbtu./hr, 132 lb/hr
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	SO2	10/19/2004	0.0133	POUNDS PER TON OF FEED MATERIAL	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	SO2	11/24/2005	0.039	POUNDS PER TON OF FEED MATERIAL	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	NOX	3/16/2004	1.98	POUNDS PER TON OF FEED MATERIAL	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	NOX	11/23/2005	2.336	POUNDS PER TON OF FEED MATERIAL	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	PM	9/5/2006	40.3	POUNDS/HOUR	combined power plant, kiln, cooler
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	NOX	11/24/2005	2.34	POUNDS PER TON OF FEED MATERIAL	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	DIOX	12/12/2005	0.212	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	tested kiln, cooler, power plant within 72 hours startup. raw mill was down. baghouse 381 F
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	NOX	9/17/2004	0.306	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	NOX	5/27/2005	0.396	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	NOX	9/6/2006	0.468	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	NOX	9/5/2007	0.469	POUNDS PER MILLION BTU HEAT INPUT	Power Plant only
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	SO2	9/18/2003	0.215	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	SO2	9/17/2004	0.394	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	SO2	5/27/2005	0.132	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	SO2	9/6/2006	0.295	POUNDS PER MILLION BTU HEAT INPUT	

FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	SO2	9/5/2007	0.476	POUNDS PER MILLION BTU HEAT INPUT	Power Plant only
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	PM	9/19/2003	0.011	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	PM	9/17/2004	0.008	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	PM	5/27/2005	0.007	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	PM	9/6/2006	0.012	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	PM	9/6/2007	0.012	POUNDS PER MILLION BTU HEAT INPUT	Power Plant only
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	NOX	9/18/2003	0.451	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	DIOX	2/28/2006	0.067	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	BH inlet temp=352F, Coal feed=9.2tph (230mmBtu/hr)
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	DIOX	4/18/2006	0.31	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Cement Kiln & Cooler only. Fuel coal only 8.8 (214mmBtu/hr), BH inlet temp.=281F
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	DIOX	12/1/2005	2.11	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	kiln and cooler operating.....power plant and ra mill down. retest due on next pp shutdown.
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	DIOX	3/18/2003	2.88	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	It was determined that the results were anomalo but the results were submitted late. RAW MILL OFF, PP STARTING
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	DIOX	8/28/2003	0.041	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	runs 2&3 performed on 9/12/03. Baghouse avg 383F RAW MILL OFF PP ON
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	DIOX	8/11/2004	0.11528	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	BH inlet=352F, RM exhaust=254F POWER PLANT ON
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	DIOX	7/29/2005	0.024	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	BH inlet Temp=357 F, Cement Plant + Rawmil clinker cooler and Power Plant
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	DIOX	9/12/2003	0.041	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	18	BPP: Power Plant Boiler	A	H114	5/1/2007	0.000209	POUNDS/HOUR	7.49 lb/yr
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	NOX	10/30/2007	271	POUNDS/HOUR	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	NOX	9/6/2007	966	POUNDS/HOUR	CP + PP
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	SO2	9/5/2006	683	POUNDS/HOUR	combined kiln, power plant, cooler
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	SO2	10/24/2006	5.14	POUNDS/HOUR	Coal Feed 8.1 TPH, Tire Feed 1.02 TPH.
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	SO2	9/6/2007	614	POUNDS/HOUR	CP + PP
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	SO2	10/30/2007	5.67	POUNDS/HOUR	
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	NOX	10/24/2006	298	POUNDS/HOUR	8.1 TPH Coal feed, 1.02 TPH TDF.
FLORIDA CRUSHED STONE CO., INC.	0530021	BROOKSVILLE CEMENT AND POWER PLANTS	SWD	HERNANDO	A	Y	20	BCP: Cement Kiln1, In-line Kiln/Raw Mill & Clinker Cooler 1	A	NOX	9/5/2006	777	POUNDS/HOUR	combined kiln, power plant, cooler
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	NOX	5/23/2007	512	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	NOX	5/17/2006	512	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	NOX	6/22/2005	499	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	NOX	6/18/2003	529	POUNDS/HOUR	tampa electric co.
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	SO2	5/17/2006	377	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	SO2	6/18/2003	414	POUNDS/HOUR	tampa electric co.
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	2	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 2	A	SO2	6/18/2003	416	POUNDS/HOUR	tampa electric co.
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	2	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 2	A	SO2	6/28/2005	414	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	2	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 2	A	SO2	7/21/2004	357	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	2	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 2	A	SO2	5/17/2006	377	POUNDS/HOUR	

TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	2	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 2	A	SO2	5/23/2007	394	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	CO	6/18/2003	85	POUNDS/HOUR	tampa electric co
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	CO	6/22/2005	81	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	CO	6/22/2005	81	POUNDS/HOUR	VE @ 1%
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	CO	6/16/2004	78	POUNDS/HOUR	TECO Environmental Services
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	CO	5/17/2006	60	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	CO	5/23/2007	60	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	2	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 2	A	CO	6/18/2003	71	POUNDS/HOUR	tampa electric co.
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	2	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 2	A	CO	6/28/2005	80	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	2	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 2	A	CO	6/12/2004	61	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	2	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 2	A	CO	5/17/2006	67	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	2	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 2	A	CO	5/23/2007	68	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	SO2	6/16/2004	359	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	SO2	5/23/2007	395	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	NOX	6/22/2005	499	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	1	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 1	A	NOX	6/16/2004	432	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	2	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 2	A	NOX	5/23/2007	507	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	2	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 2	A	NOX	5/17/2006	505	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	2	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 2	A	NOX	6/28/2005	499	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	4	AUXILIARY STEAM BOILER	A	SO2	6/22/2005	1.3	POUNDS/HOUR	Results from stack test report
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	2	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 2	A	NOX	6/18/2003	536	POUNDS/HOUR	tampa electric co.
TAMPA ELECTRIC COMPANY	0550018	PHILLIPS STATION	SD	HIGHLANDS	A	Y	2	19.535 MW SLOW SPEED DIESEL GENERATING UNIT 2	A	NOX	6/16/2004	454	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	3	"B" Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SAM	3/7/2007	0.357	POUNDS/HOUR	CF stack test team
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	3	"B" Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SAM	11/5/2005	0.6	POUNDS/HOUR	.012lbs SAM/ton 100% H2SO4
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	3	"B" Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SAM	1/13/2004	0.46	POUNDS/HOUR	self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	FL	3/7/2006	0.0057	POUNDS PER TON OF PRODUCT	CF self tested. 0.26 lbs F/hr
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	FL	10/16/2007	0.01067	POUNDS PER TON OF PRODUCT	CF self tested.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	SAM	1/15/2003	0.03	POUNDS PER TON OF PRODUCT	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	SAM	3/8/2004	0.04	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	SAM	1/25/2005	0.023	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	SAM	7/16/2004	0.027	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	SAM	1/17/2006	0.03	POUNDS PER TON OF PRODUCT	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	SAM	5/1/2007	0.027	POUNDS PER TON OF PRODUCT	CF test team
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	SAM	1/17/2007	0.023333	POUNDS PER TON OF PRODUCT	CF self tested.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	SO2	1/15/2003	3.87	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	SO2	3/8/2004	3.43	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	SO2	1/25/2005	3.33	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	SO2	7/16/2004	3.05	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY	0570005	CF INDUSTRIES-PLANT CITY PHOSP	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID	A	SO2	1/17/2006	3.32	POUNDS PER TON OF	CF self tested

PHOS		COMPLEX						PLANT					PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	SO2	5/1/2007	3.24	POUNDS PER TON OF PRODUCT	CF test team
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	SO2	1/17/2007	3.347	POUNDS PER TON OF PRODUCT	CF self tested.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	2	"A' Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SO2	2/5/2003	3.36	POUNDS PER TON OF PRODUCT	CF self test
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	2	"A' Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SO2	12/10/2003	3.33	POUNDS PER TON OF PRODUCT	self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	2	"A' Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SO2	2/1/2005	3.09	POUNDS PER TON OF PRODUCT	Environmental Laboratory of CF Industries.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	2	"A' Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SO2	1/22/2004	3	POUNDS PER TON OF PRODUCT	self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	2	"A' Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SO2	1/31/2006	3.58	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	2	"A' Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SO2	2/21/2007	3.8	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	FL	7/1/2003	0.017	POUNDS PER TON OF FEED MATERIAL	self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	FL	4/30/2003	0.02	POUNDS PER TON OF FEED MATERIAL	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	FL	4/29/2003	0.02	POUNDS PER TON OF FEED MATERIAL	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	FL	7/1/2003	0.02	POUNDS PER TON OF FEED MATERIAL	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	FL	5/5/2004	0.01	POUNDS PER TON OF FEED MATERIAL	CF Industries Lab.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	FL	4/27/2004	0.02	POUNDS PER TON OF FEED MATERIAL	Test conducted by Environmental Laboratory, (industries.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	FL	4/14/2005	0.01	POUNDS PER TON OF FEED MATERIAL	CF self tested. 0.53lbs F/hr
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	FL	4/4/2006	0.01	POUNDS PER TON OF FEED MATERIAL	CF self tested. 0.52 lbs F/hr
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	FL	4/5/2005	0.02	POUNDS PER TON OF FEED MATERIAL	0.83 lbs F/ hr.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	FL	4/18/2006	0.008333	POUNDS PER TON OF FEED MATERIAL	CF self tested. 0.38lbs F/hr (<2.2lbs/hr permit r
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	FL	11/1/2005	0.02	POUNDS PER TON OF FEED MATERIAL	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	FL	11/3/2005	0.027	POUNDS PER TON OF FEED MATERIAL	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	FL	4/11/2007	0.0217	POUNDS PER TON OF FEED MATERIAL	Actual Emissions = Fl 9Lbs/hr) / Feed Material (tons/hr). Feed Material + 49.6 tons.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	FL	4/24/2007	0.037	POUNDS PER TON OF FEED MATERIAL	CF test team.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	FL	2/14/2008	0.015	POUNDS PER TON OF FEED MATERIAL	Process rate = 51.9 tph P2O5 input. Producing MAP. Actual units = lbs F/ton P2O5 input.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	SAM	1/29/2003	0.04	POUNDS PER TON OF PRODUCT	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	SAM	2/10/2004	0.048	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	SAM	1/18/2005	0.033	POUNDS PER TON OF PRODUCT	Test performed by Environmental Laboratory o Industries.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	SAM	4/21/2005	0.03	POUNDS PER TON OF PRODUCT	2.69 lbs SAM/hr
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	SAM	2/10/2004	0.048	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	SAM	1/24/2006	0.04	POUNDS PER TON OF PRODUCT	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	SAM	1/30/2007	0.07	POUNDS PER TON OF PRODUCT	Test performed by Southern Environmental Sciences.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	9	"B" PHOSPHORIC ACID PLANT	A	FL	5/9/2006	0.003	POUNDS PER TON OF PRODUCT	CF Industries, Inc. Environmental Laboratory
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	9	"B" PHOSPHORIC ACID PLANT	A	FL	5/9/2006	0.003333	POUNDS PER TON OF PRODUCT	CF self tested.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	9	"B" PHOSPHORIC ACID PLANT	A	FL	5/17/2007	0.00967	POUNDS PER TON OF PRODUCT	CF test team
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	9	"B" PHOSPHORIC ACID PLANT	A	FL	10/3/2007	0.006	POUNDS PER TON OF PRODUCT	CF self tested.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	NOX	4/22/2005	0.1037	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	NOX	1/26/2006	0.095	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	SO2	1/29/2003	3.92	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	SO2	2/10/2004	3	POUNDS PER TON OF PRODUCT	

CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	SO2	1/18/2005	3.37	POUNDS PER TON OF PRODUCT	Testing performed by Environmental laboratory CF Industries.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	SO2	4/21/2005	3.42	POUNDS PER TON OF PRODUCT	average 370 lb SO2/hr.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	SO2	2/10/2004	3.03	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	SO2	1/24/2006	3.12	POUNDS PER TON OF PRODUCT	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	8	"D" SULFURIC ACID PLANT	A	SO2	1/30/2007	3.37	POUNDS PER TON OF PRODUCT	Production Rate @ 2613 TPD
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	3	"B" Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SO2	2/12/2003	3.81	POUNDS PER TON OF PRODUCT	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	3	"B" Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SO2	1/13/2004	4.15	POUNDS PER TON OF PRODUCT	self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	3	"B" Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SO2	3/1/2005	3.194	POUNDS PER TON OF PRODUCT	Test performed by Environmental Laboratory o Industries.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	3	"B" Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SO2	11/5/2005	3	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	3	"B" Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SO2	2/22/2006	3.57	POUNDS PER TON OF PRODUCT	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	3	"B" Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SO2	3/7/2007	3.66	POUNDS PER TON OF PRODUCT	CF stack test team
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	4	"A" PHOSPHORIC ACID PLANT	A	FL	3/28/2006	0.0067	POUNDS PER TON OF PRODUCT	CF self tested. 0.39 lbs F /hr.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	4	"A" PHOSPHORIC ACID PLANT	A	FL	6/7/2007	0.033	POUNDS PER TON OF PRODUCT	Test done by CF Environmental Team. (tests conducted on 6/7, 6/11 & 6/12/07)
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	4	"A" PHOSPHORIC ACID PLANT	A	FL	6/11/2007	0.014	POUNDS PER TON OF PRODUCT	Test done by CF Environmental Team.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	4	"A" PHOSPHORIC ACID PLANT	A	FL	9/25/2007	0.007	POUNDS PER TON OF PRODUCT	CF Industries Lab conducted this test.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	12	"X" DAP/MAP PLANT	A	FL	3/21/2006	0.017	POUNDS PER TON OF PRODUCT	0.79 lb F/hr
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	12	"X" DAP/MAP PLANT	A	FL	3/27/2007	0.02	POUNDS PER TON OF PRODUCT	CF test team also 0.90 lbs F/hr
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	NOX	7/16/2004	0.1	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	NOX	1/19/2006	0.09	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	7	"C" SULFURIC ACID PLANT	A	NOX	1/18/2007	0.09	POUNDS PER TON OF PRODUCT	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	FL	3/13/2003	1.3	POUNDS/HOUR	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	FL	3/11/2003	1.3	POUNDS/HOUR	Test by CF lab personnel.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	FL	3/10/2005	0.37	POUNDS/HOUR	.0082 lbs F/ ton P2O5 input
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	FL	3/2/2004	0.69	POUNDS/HOUR	Test team-CF Industries
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	FL	10/20/2005	0.16	POUNDS/HOUR	.003 lbs F/ton P2O5
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	FL	10/18/2005	0.09	POUNDS/HOUR	.002 lbs F/ton P2O5
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	FL	3/14/2007	1.53	POUNDS/HOUR	Test done by CF Industries Environmental Tea Three runs test average @ 1.53 lbs/hr > Fluorid Limit of 1.44 lbs/hr. .
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	FL	3/16/2007	1	POUNDS/HOUR	Test done by CF Environmental Team. Initial t 3/14/07 exceeded the FL limits and it have to b repeated.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	3	"B" Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SAM	2/12/2003	0.43	POUNDS/HOUR	CF self test
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	3	"B" Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SAM	3/1/2005	0.391	POUNDS/HOUR	Test performed by Environmental Laboratory o Industries.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	3	"B" Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SAM	2/22/2006	0.47	POUNDS/HOUR	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	10	"A" DAP/MAP PLANT	A	FL	10/12/2005	0.23	POUNDS/HOUR	.009 lbs F/ton P2O5 (did not operate in 2006)
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	32	PHOSPHORIC ACID CLEAN (CLARIFICATION AND SCRUBBER)	A	PM	11/29/2005	0.25	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	32	PHOSPHORIC ACID CLEAN (CLARIFICATION AND SCRUBBER)	A	PM	6/28/2005	1.38	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	32	PHOSPHORIC ACID CLEAN (CLARIFICATION AND SCRUBBER)	A	PM	10/14/2003	0.86	POUNDS/HOUR	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	PM	3/16/2007	2.28	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	PM	10/16/2007	5.35	POUNDS/HOUR	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	4	"A" PHOSPHORIC ACID PLANT	A	FL	6/17/2003	0.83	POUNDS/HOUR	CF self tested
CF INDUSTRIES,		CF INDUSTRIES-												

INC., PLANT CITY PHOS	0570005	PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	4	"A" PHOSPHORIC ACID PLANT	A	FL	5/13/2004	0.693	POUNDS/HOUR	Test performed by Environmental Laboratory, C Industries.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	4	"A" PHOSPHORIC ACID PLANT	A	FL	11/8/2005	0.36	POUNDS/HOUR	averaged 0.006 Lbs F/ton
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	4	"A" PHOSPHORIC ACID PLANT	A	FL	11/10/2005	0.55	POUNDS/HOUR	0.010 lbs F/ton P2O5
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	4	"A" PHOSPHORIC ACID PLANT	A	FL	5/12/2005	0.273	POUNDS/HOUR	0.0047 lbs F / ton P2O5
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	NH3	3/10/2005	3.53	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	NH3	3/2/2004	5.2	POUNDS/HOUR	Test team-CF Industries
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	14	A & B STORAGE BUILDINGS	A	PM	2/26/2003	3.26	POUNDS/HOUR	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	PM	3/13/2003	4.99	POUNDS/HOUR	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	PM	3/11/2003	3.71	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	PM	3/10/2005	6.75	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	PM	3/2/2004	3.7	POUNDS/HOUR	Test team-CF Industries
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	PM	10/18/2005	2.26	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	PM	10/20/2005	2.92	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	PM	3/7/2006	3.08	POUNDS/HOUR	CF self tested.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	11	"Z" DAP/MAP PLANT	A	PM	3/14/2007	5.17	POUNDS/HOUR	Test performed by CF Environmental Team
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	12	"X" DAP/MAP PLANT	A	FL	3/25/2003	0.33	POUNDS/HOUR	Test conducted by Environmental Laboratory C Industries, Inc.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	12	"X" DAP/MAP PLANT	A	FL	4/20/2004	0.797	POUNDS/HOUR	Test performed by Environmental Laboratory C Industries.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	12	"X" DAP/MAP PLANT	A	FL	3/22/2005	0.353	POUNDS/HOUR	CF self tested. 0.008 F/ton P2O5
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	12	"X" DAP/MAP PLANT	A	FL	10/25/2005	0.65	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	12	"X" DAP/MAP PLANT	A	FL	10/27/2005	0.23	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	10	"A" DAP/MAP PLANT	A	PM	10/11/2005	4.2	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	10	"A" DAP/MAP PLANT	A	PM	10/12/2005	3.35	POUNDS/HOUR	did not operate in 2006
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	PM	4/14/2005	1.547	POUNDS/HOUR	CF self tested.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	2	"A' Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SAM	2/1/2005	0.55	POUNDS/HOUR	Environmental Laboratory of CF Industries.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	2	"A' Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SAM	1/22/2004	0.64	POUNDS/HOUR	self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	2	"A' Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SAM	1/31/2006	0.55	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	2	"A' Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SAM	2/21/2007	0.38	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	9	"B" PHOSPHORIC ACID PLANT	A	FL	5/14/2003	0.33	POUNDS/HOUR	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	9	"B" PHOSPHORIC ACID PLANT	A	FL	5/18/2004	0.803	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	9	"B" PHOSPHORIC ACID PLANT	A	FL	10/6/2005	0.29	POUNDS/HOUR	.0033 lbs F/ton P2O5
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	9	"B" PHOSPHORIC ACID PLANT	A	FL	10/4/2005	0.14	POUNDS/HOUR	.0017 lbs F/ton P2O5
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	9	"B" PHOSPHORIC ACID PLANT	A	FL	4/27/2005	0.31	POUNDS/HOUR	avg .0037 lbs F/ton P2O5 input.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	32	PHOSPHORIC ACID CLEAN (CLARIFICATION AND SCRUBBER)	A	FL	10/14/2003	0.217	POUNDS/HOUR	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	32	PHOSPHORIC ACID CLEAN (CLARIFICATION AND SCRUBBER)	A	FL	6/24/2004	0.263	POUNDS/HOUR	Test performed by Environmental Laboratory, C Industries.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	32	PHOSPHORIC ACID CLEAN (CLARIFICATION AND SCRUBBER)	A	FL	6/28/2005	0.74	POUNDS/HOUR	CF self tested.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	32	PHOSPHORIC ACID CLEAN (CLARIFICATION AND SCRUBBER)	A	FL	7/1/2005	0.2767	POUNDS/HOUR	CF self tested.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	32	PHOSPHORIC ACID CLEAN (CLARIFICATION AND SCRUBBER)	A	FL	11/29/2005	0.26	POUNDS/HOUR	CF self tested.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	32	PHOSPHORIC ACID CLEAN (CLARIFICATION AND SCRUBBER)	A	FL	6/27/2006	0.2233	POUNDS/HOUR	CF self tested.
CF INDUSTRIES, INC., PLANT CITY	0570005	CF INDUSTRIES-PLANT CITY PHOSP	SWHI	HILLSBOROUGH	A	Y	32	PHOSPHORIC ACID CLEAN (CLARIFICATION	A	FL	1/13/2006	0.085	POUNDS/HOUR	

PHOS		COMPLEX						AND SCRUBBER)						
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	32	PHOSPHORIC ACID CLEAN (CLARIFICATION AND SCRUBBER)	A	FL	8/21/2007	0.1633	POUNDS/HOUR	The Facility conducted this stack test.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	12	"X" DAP/MAP PLANT	A	PM	3/25/2003	2.51	POUNDS/HOUR	Test conducted by Environmental Laboratories Industries, Inc.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	12	"X" DAP/MAP PLANT	A	PM	4/20/2004	3.63	POUNDS/HOUR	Test performed by Environmental Laboratory C Industries.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	12	"X" DAP/MAP PLANT	A	PM	3/22/2005	1.76	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	12	"X" DAP/MAP PLANT	A	PM	3/21/2006	4.48	POUNDS/HOUR	CF self tested.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	12	"X" DAP/MAP PLANT	A	PM	10/25/2005	2.23	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	12	"X" DAP/MAP PLANT	A	PM	10/27/2005	3.34	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	12	"X" DAP/MAP PLANT	A	PM	3/27/2007	3.03	POUNDS/HOUR	CF test team
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	2	"A' Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SAM	2/5/2003	0.48	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	2	"A' Sulfuric Acid Plant (Single Absorption/Ammonia Scrubber)	A	SAM	12/10/2003	0.52	POUNDS/HOUR	self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	PM	4/4/2006	2.61	POUNDS/HOUR	CF self tested.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	PM	4/5/2005	3.54	POUNDS/HOUR	CF self tested.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	PM	4/18/2006	3.77	POUNDS/HOUR	CF self tested.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	PM	11/1/2005	3.4	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	PM	11/3/2005	4.07	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	PM	4/11/2007	6.05	POUNDS/HOUR	Test done by CF Environmental Team.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	PM	4/24/2007	3.82	POUNDS/HOUR	CF test team
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	PM	2/14/2008	6.04	POUNDS/HOUR	Process rate = 51.9 tph P2O5 input. (Producing MAP)
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	PM	7/1/2003	5.98	POUNDS/HOUR	self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	PM	4/30/2003	3	POUNDS/HOUR	CF self tested
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	PM	4/29/2003	3	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	PM	7/1/2003	5.98	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	PM	5/5/2004	4.1	POUNDS/HOUR	Test conducted by CF Industries Environmenta Laboratory. DAP Product.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	13	"Y" DAP/MAP PLANT	A	PM	4/27/2004	8.07	POUNDS/HOUR	Performed by Environmental Laboratory, CF Industries. MAP Product.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	32	PHOSPHORIC ACID CLEAN (CLARIFICATION AND SCRUBBER)	A	PM	6/24/2004	0.487	POUNDS/HOUR	Test performed by Environmental Laboratory, Industries.
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	32	PHOSPHORIC ACID CLEAN (CLARIFICATION AND SCRUBBER)	A	PM	7/1/2005	0.95	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	32	PHOSPHORIC ACID CLEAN (CLARIFICATION AND SCRUBBER)	A	PM	1/13/2006	0.476	POUNDS/HOUR	
CF INDUSTRIES, INC., PLANT CITY PHOS	0570005	CF INDUSTRIES-PLANT CITY PHOSP COMPLEX	SWHI	HILLSBOROUGH	A	Y	10	"A" DAP/MAP PLANT	A	FL	10/11/2005	0.28	POUNDS/HOUR	.012 lbs F/ton P2O5
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	FL	9/25/2003	2.02	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	PM	9/14/2007	2.28	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	PM	8/10/2006	1.98	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	PM	8/19/2004	6.84	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	FL	7/18/2003	2.79	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	FL	8/19/2004	3.96	POUNDS/HOUR	Facility also exceeded the equivalent P2O5 0.0 lbs/ton.
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	FL	8/8/2005	2.6	POUNDS/HOUR	Annual test.
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	FL	8/10/2006	3.15	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	FL	10/25/2006	3.08	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	FL	9/14/2007	2.4	POUNDS/HOUR	

MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	22	NO. 3 MAP PLANT	I	FL	6/19/2003	0.89	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	22	NO. 3 MAP PLANT	I	FL	6/19/2003	0.89	POUNDS/HOUR	test done at common stack
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	78	COMMON STACK, ANIMAL FEED PLANT No. 1	A	PM	7/29/2005	7.2	POUNDS/HOUR	The test report had an allowable PM emissions as 13.0 lbs/hr.
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Common stack animal feed plant #2	A	PM	5/8/2003	4.43	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Common stack animal feed plant #2	A	PM	5/20/2004	4.97	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Common stack animal feed plant #2	A	PM	8/4/2005	4.5	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Common stack animal feed plant #2	A	PM	10/24/2006	11.9	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Common stack animal feed plant #2	A	PM	7/11/2006	2.1	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Common stack animal feed plant #2	A	PM	5/31/2007	3.1	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	22	NO. 3 MAP PLANT	I	PM	6/19/2003	2.78	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	22	NO. 3 MAP PLANT	I	PM	6/19/2003	2.78	POUNDS/HOUR	Test done at a common stack
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	78	COMMON STACK, ANIMAL FEED PLANT No. 1	A	PM	10/10/2006	3.3	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	78	COMMON STACK, ANIMAL FEED PLANT No. 1	A	PM	6/23/2006	2.97	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	78	COMMON STACK, ANIMAL FEED PLANT No. 1	A	PM	5/15/2007	7.9	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	78	COMMON STACK, ANIMAL FEED PLANT No. 1	A	FL	5/13/2004	0.44	POUNDS/HOUR	Test Allow should be 2.11 lb/hr. See 0570008-(AC or PSD-FL-315.
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	78	COMMON STACK, ANIMAL FEED PLANT No. 1	A	FL	7/29/2005	0.8	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	78	COMMON STACK, ANIMAL FEED PLANT No. 1	A	FL	10/10/2006	0.15	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	78	COMMON STACK, ANIMAL FEED PLANT No. 1	A	FL	6/23/2006	0.21	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	78	COMMON STACK, ANIMAL FEED PLANT No. 1	A	FL	5/15/2007	0.74	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	78	COMMON STACK, ANIMAL FEED PLANT No. 1	A	PM	5/13/2004	4.5	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	PM	7/18/2003	3.47	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	PM	8/8/2005	2.4	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	PM	10/25/2006	1.45	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	23	NO. 4 MAP PLANT	I	FL	6/19/2003	0.89	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	23	NO. 4 MAP PLANT	I	FL	6/19/2003	0.89	POUNDS/HOUR	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	PM	9/4/2007	0.042	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	PM	11/11/2004	0.006	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	4	NO. 7 SULFURIC ACID PLANT	A	SO2	4/17/2003	2.9	POUNDS PER TON OF PRODUCT	Production Rate of 121.8 TPH.
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	4	NO. 7 SULFURIC ACID PLANT	A	SO2	5/12/2004	3.8	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	4	NO. 7 SULFURIC ACID PLANT	A	SO2	7/6/2006	3.3	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	4	NO. 7 SULFURIC ACID PLANT	A	SO2	4/14/2005	3.6	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	4	NO. 7 SULFURIC ACID PLANT	A	SO2	2/22/2007	3.2	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	FL	1/11/2004	0.00066	POUNDS PER TON OF FEED MATERIAL	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	FL	4/7/2005	0.011	POUNDS PER TON OF FEED MATERIAL	Emissions= RVG Stack + Cooler Stack
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	FL	5/25/2006	0.009	POUNDS PER TON OF FEED MATERIAL	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	FL	5/25/2006	0.0009	POUNDS PER TON OF FEED MATERIAL	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	FL	9/4/2007	0.015	POUNDS PER TON OF FEED MATERIAL	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	FL	9/4/2007	0.015	POUNDS PER TON OF FEED MATERIAL	
		MOSAIC FERTILIZER-											POUNDS PER	

MOSAIC FERTILIZER, LLC	0570008	RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	FL	9/4/2007	0.015	TON OF FEED MATERIAL	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	FL	9/4/2007	0.015	POUNDS PER TON OF FEED MATERIAL	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	PM	9/25/2003	0.283	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	PM	9/26/2003	0.129	POUNDS PER TON OF PRODUCT	Based on this test, the production rate will be li to 80 tph.
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	73	PHOSPHORIC ACID PRODUCTION SYSTEM (Prayon, Dorrco, No. 3)	A	FL	4/17/2003	0.002986	POUNDS PER TON OF PRODUCT	input 144 TPH P2O5. Total F emissions for all filters was 0.43 lbs/hr.
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	73	PHOSPHORIC ACID PRODUCTION SYSTEM (Prayon, Dorrco, No. 3)	A	FL	8/3/2004	0.0013	POUNDS PER TON OF PRODUCT	Reactor Stack
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	73	PHOSPHORIC ACID PRODUCTION SYSTEM (Prayon, Dorrco, No. 3)	A	FL	8/3/2004	0.0003	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	73	PHOSPHORIC ACID PRODUCTION SYSTEM (Prayon, Dorrco, No. 3)	A	FL	8/3/2004	0.0004	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	73	PHOSPHORIC ACID PRODUCTION SYSTEM (Prayon, Dorrco, No. 3)	A	FL	7/19/2005	0.0004	POUNDS PER TON OF PRODUCT	Filter No. 1 and No. 2
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	73	PHOSPHORIC ACID PRODUCTION SYSTEM (Prayon, Dorrco, No. 3)	A	FL	7/19/2005	0.0002	POUNDS PER TON OF PRODUCT	Annual Compliance Test
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	73	PHOSPHORIC ACID PRODUCTION SYSTEM (Prayon, Dorrco, No. 3)	A	FL	7/19/2005	0.0014	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	73	PHOSPHORIC ACID PRODUCTION SYSTEM (Prayon, Dorrco, No. 3)	A	FL	6/14/2006	0.00006	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	73	PHOSPHORIC ACID PRODUCTION SYSTEM (Prayon, Dorrco, No. 3)	A	FL	6/14/2006	0.0002	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	73	PHOSPHORIC ACID PRODUCTION SYSTEM (Prayon, Dorrco, No. 3)	A	FL	6/14/2006	0.006	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	73	PHOSPHORIC ACID PRODUCTION SYSTEM (Prayon, Dorrco, No. 3)	A	FL	8/2/2007	0.0001	POUNDS PER TON OF PRODUCT	Filter No. 1 and No. 2
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	73	PHOSPHORIC ACID PRODUCTION SYSTEM (Prayon, Dorrco, No. 3)	A	FL	8/2/2007	0.00004	POUNDS PER TON OF PRODUCT	Filter No. 3
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	73	PHOSPHORIC ACID PRODUCTION SYSTEM (Prayon, Dorrco, No. 3)	A	FL	8/2/2007	0.0006	POUNDS PER TON OF PRODUCT	Reactor
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	6	NO. 9 SULFURIC ACID PLANT	A	SAM	2/10/2003	0.032	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	6	NO. 9 SULFURIC ACID PLANT	A	SAM	5/6/2004	0.04	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	6	NO. 9 SULFURIC ACID PLANT	A	SAM	2/18/2005	0.042	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	6	NO. 9 SULFURIC ACID PLANT	A	SAM	2/9/2006	0.02	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	6	NO. 9 SULFURIC ACID PLANT	A	SAM	3/8/2007	0.014	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	6	NO. 9 SULFURIC ACID PLANT	A	SAM	2/22/2007	0.02	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	5	NO. 8 SULFURIC ACID PLANT	A	SO2	1/30/2003	2.97	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	5	NO. 8 SULFURIC ACID PLANT	A	SO2	2/11/2005	3.67	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	5	NO. 8 SULFURIC ACID PLANT	A	SO2	2/6/2004	3.6	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	5	NO. 8 SULFURIC ACID PLANT	A	SO2	1/31/2006	3.4	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	5	NO. 8 SULFURIC ACID PLANT	A	SO2	6/24/2005	2.9	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	5	NO. 8 SULFURIC ACID PLANT	A	SO2	6/11/2007	3.7	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	4	NO. 7 SULFURIC ACID PLANT	A	SAM	4/17/2003	0.04	POUNDS PER TON OF PRODUCT	Production Rate 121.1 TPH
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	4	NO. 7 SULFURIC ACID PLANT	A	SAM	5/12/2004	0.036	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	4	NO. 7 SULFURIC ACID PLANT	A	SAM	7/6/2006	0.04	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	4	NO. 7 SULFURIC ACID PLANT	A	SAM	4/14/2005	0.04	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	4	NO. 7 SULFURIC ACID PLANT	A	SAM	4/14/2005	0.04	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	4	NO. 7 SULFURIC ACID PLANT	A	SAM	2/22/2007	0.02	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	6	NO. 9 SULFURIC ACID PLANT	A	SO2	2/22/2007	3.2	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	23	NO. 4 MAP PLANT	I	PM	6/19/2003	0.041	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	23	NO. 4 MAP PLANT	I	PM	6/19/2003	0.041	POUNDS PER TON OF PRODUCT	test done at common stack
MOSAIC	0570008	MOSAIC FERTILIZER-RIVERVIEW	SWHI	HILLSBOROUGH	A	Y	5	NO. 8 SULFURIC ACID	A	SAM	1/30/2003	0.03	POUNDS PER TON OF	

FERTILIZER, LLC		FACILITY						PLANT					PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	5	NO. 8 SULFURIC ACID PLANT	A	SAM	2/6/2004	0.024	POUNDS PER TON OF PRODUCT	Sulfuric acid production rate 108.7 tph.
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	5	NO. 8 SULFURIC ACID PLANT	A	SAM	2/9/2005	0.056	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	5	NO. 8 SULFURIC ACID PLANT	A	SAM	1/31/2006	0.03	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	5	NO. 8 SULFURIC ACID PLANT	A	SAM	6/24/2005	0.047	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	5	NO. 8 SULFURIC ACID PLANT	A	SAM	6/11/2007	0.01	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	6	NO. 9 SULFURIC ACID PLANT	A	SO2	2/10/2003	2.87	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	6	NO. 9 SULFURIC ACID PLANT	A	SO2	5/6/2004	3.3	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	6	NO. 9 SULFURIC ACID PLANT	A	SO2	2/18/2005	3.5	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	6	NO. 9 SULFURIC ACID PLANT	A	SO2	2/9/2006	2.9	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	6	NO. 9 SULFURIC ACID PLANT	A	SO2	3/8/2007	3.1	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	PM	4/7/2005	0.091	POUNDS PER TON OF PRODUCT	Emissions = RGV stack + Cooler Stack
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	PM	9/4/2007	0.042	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	PM	9/4/2007	0.042	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	PM	5/25/2006	0.046	POUNDS PER TON OF PRODUCT	Stack Test is required each FFY
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	PM	5/25/2006	0.046	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	7	DAP Manufacturing Plant	A	PM	9/4/2007	0.042	POUNDS PER TON OF PRODUCT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	24	SOUTH COOLER	I	PM	6/19/2003	0.003	GRAINS PER DRY STANDARD CUBIC FOOT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	79	DIATOMACEOUS EARTH SILO	A	PM	5/7/2003	0.01	GRAINS PER DRY STANDARD CUBIC FOOT	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	NH3	9/14/2007	0.75	TEST REQUIRED (NO ALLOWABLE EMISSION)	NH3 emissions = .75 lb/hr, 3.4 PPM
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	NH3	8/10/2006	0.23	TEST REQUIRED (NO ALLOWABLE EMISSION)	
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	NH3	8/8/2005	0.74	TEST REQUIRED (NO ALLOWABLE EMISSION)	NH3 emissions=0.74 lbs/hr=2.7 ppm.
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	55	NO. 5 GRANULATION PLANT	A	NH3	8/19/2004	0.39	TEST REQUIRED (NO ALLOWABLE EMISSION)	emission unit is lbs/hour.
MOSAIC FERTILIZER, LLC	0570008	MOSAIC FERTILIZER-RIVERVIEW FACILITY	SWHI	HILLSBOROUGH	A	Y	63	TANK Nos. 1, 2, and 3 for molten sulfur storage w/scrubber	A	PM	3/7/2006	0.002	GRAINS PER DRY STANDARD CUBIC FOOT	
EASTERN ASSOCIATED TERMINALS CO., LLC	0570014	EASTERN ASSOCIATED TERMINAL ROCK PORT	SWHI	HILLSBOROUGH	A	Y	3	RAILCAR UNLOADING SYSTEM WITH BAGHOUSE A	A	PM	10/8/2007	0.6135	POUNDS/HOUR	Air Testing and Consulting conducted the test.
EASTERN ASSOCIATED TERMINALS CO., LLC	0570014	EASTERN ASSOCIATED TERMINAL ROCK PORT	SWHI	HILLSBOROUGH	A	Y	3	RAILCAR UNLOADING SYSTEM WITH BAGHOUSE A	A	PM	10/9/2006	1.187	POUNDS/HOUR	Air Testing & Consultanting performed the test
EASTERN ASSOCIATED TERMINALS CO., LLC	0570014	EASTERN ASSOCIATED TERMINAL ROCK PORT	SWHI	HILLSBOROUGH	A	Y	13	STORAGE BUILDING BAGHOUSE #3,NW	A	PM	10/11/2006	0.8954	POUNDS/HOUR	ASir Testing & Consultants perform the tests.
EASTERN ASSOCIATED TERMINALS CO., LLC	0570014	EASTERN ASSOCIATED TERMINAL ROCK PORT	SWHI	HILLSBOROUGH	A	Y	12	STORAGE BUILDING BAGHOUSE #2,SW	A	PM	11/19/2004	0.46	POUNDS/HOUR	Test performed by Air Testing and Consulting,
EASTERN ASSOCIATED TERMINALS CO., LLC	0570014	EASTERN ASSOCIATED TERMINAL ROCK PORT	SWHI	HILLSBOROUGH	A	Y	11	STORAGE BUILDING BAGHOUSE #1, SE	A	PM	10/8/2007	0.173	POUNDS/HOUR	Air Testing Consulting conducted the test.
EASTERN ASSOCIATED TERMINALS CO., LLC	0570014	EASTERN ASSOCIATED TERMINAL ROCK PORT	SWHI	HILLSBOROUGH	A	Y	11	STORAGE BUILDING BAGHOUSE #1, SE	A	PM	10/29/2003	0.46	POUNDS/HOUR	Test team is AT & C
EASTERN ASSOCIATED TERMINALS CO., LLC	0570014	EASTERN ASSOCIATED TERMINAL ROCK PORT	SWHI	HILLSBOROUGH	A	Y	14	STORAGE BUILDING BAGHOUSE #4,NE	A	PM	10/12/2005	0.358	POUNDS/HOUR	Air Testing & Consulting conducted by Kennet Given.
CITGO PETROLEUM CORPORATION	0570016	CITGO TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	1	LOADING RACKS W/VAPOR COMBUSTION UNIT (VCU)	A	VOC	9/25/2003	3.91	MILLIGRAMS PER LITER OF LIQUID LOADED	Destruction Efficiency @99.57%
CITGO PETROLEUM CORPORATION	0570016	CITGO TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	1	LOADING RACKS W/VAPOR COMBUSTION UNIT (VCU)	A	VOC	8/6/2006	7	MILLIGRAMS PER LITER OF LIQUID LOADED	Friday test for low loading volume.
CITGO PETROLEUM CORPORATION	0570016	CITGO TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	1	LOADING RACKS W/VAPOR COMBUSTION UNIT (VCU)	A	VOC	9/15/2005	3.4	MILLIGRAMS PER LITER OF LIQUID LOADED	total gasoline loaded = 1,421,949 liters; total te duration = 6 hours.

CITGO PETROLEUM CORPORATION	0570016	CITGO TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	1	LOADING RACKS W/VAPOR COMBUSTION UNIT (VCU)	A	VOC	8/2/2007	2.97	MILLIGRAMS PER LITER OF LIQUID LOADED	6 hr test on VCU - Total of 625,078 gal of fuel loaded
CITGO PETROLEUM CORPORATION	0570016	CITGO TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	1	LOADING RACKS W/VAPOR COMBUSTION UNIT (VCU)	A	VOC	8/7/2006	5.22	MILLIGRAMS PER LITER OF LIQUID LOADED	Monday test for high loading rate.
CITGO PETROLEUM CORPORATION	0570016	CITGO TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	1	LOADING RACKS W/VAPOR COMBUSTION UNIT (VCU)	A	VOC	9/30/2004	6.3	MILLIGRAMS PER LITER OF LIQUID LOADED	
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	3	SHIPLOADING BAGHOUSE (C13 TO C14 AND C14 TO SHIPHOLD)	A	PM	4/21/2007	0.021457	GRAINS PER DRY STANDARD CUBIC FOOT	Process rate = 663 tph AFI. 2nd retest.
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	12	CONVEYOR TRANSFER POINTS FROM RAILCAR UNLOADING & ROCK DRYER	A	PM	9/28/2006	0.005	GRAINS PER DRY STANDARD CUBIC FOOT	Emission rate = 1.03 lb/hr.
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	7	C18 TRANSFER POINT D	A	PM	3/9/2007	0.002	GRAINS PER DRY STANDARD CUBIC FOOT	
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	12	CONVEYOR TRANSFER POINTS FROM RAILCAR UNLOADING & ROCK DRYER	A	PM	6/23/2005	0.004	GRAINS PER DRY STANDARD CUBIC FOOT	load limited 253 TPH.
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	2	RAILCAR UNLOADING SCRUBBER	A	PM	9/11/2006	0.003	GRAINS PER DRY STANDARD CUBIC FOOT	Emission rate = 1.23 lb/hr. Awaiting process ra
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	3	SHIPLOADING BAGHOUSE (C13 TO C14 AND C14 TO SHIPHOLD)	A	PM	3/12/2007	0.076	GRAINS PER DRY STANDARD CUBIC FOOT	Handling AFI. Process rate = 920 tph.
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	3	SHIPLOADING BAGHOUSE (C13 TO C14 AND C14 TO SHIPHOLD)	A	PM	4/12/2007	0.155	GRAINS PER DRY STANDARD CUBIC FOOT	Process rate = 950 tph AFI. Emission rate = 15. lb/hr PM.
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	9	C19 TRANSFER POINT G	A	PM	2/22/2005	0.002	GRAINS PER DRY STANDARD CUBIC FOOT	
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	4	C17 TRANSFER POINT E	A	PM	9/25/2007	0.004	GRAINS PER DRY STANDARD CUBIC FOOT	
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	3	SHIPLOADING BAGHOUSE (C13 TO C14 AND C14 TO SHIPHOLD)	A	PM	9/24/2004	0.297	POUNDS/HOUR	Operating rate of 572 tph, 39.7% of permit rate
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	7	C18 TRANSFER POINT D	A	PM	9/24/2004	0.262	POUNDS/HOUR	
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	9	C19 TRANSFER POINT G	A	PM	10/12/2004	0.105	POUNDS/HOUR	
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	5	C12 TRANSFER POINT A	A	PM	9/24/2004	0.117	POUNDS/HOUR	Process rate is 572 tph, 26.0% of permit rate.
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	2	RAILCAR UNLOADING SCRUBBER	A	PM	11/14/2003	4.6	POUNDS/HOUR	
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	4	C17 TRANSFER POINT E	A	PM	1/14/2003	0.63	POUNDS/HOUR	
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	2	RAILCAR UNLOADING SCRUBBER	A	PM	1/14/2003	4.4	POUNDS/HOUR	Process rate automatically limited to 684 tph.
KINDER MORGAN OLP "C"	0570024	KINDER MORGAN TAMPAPLEX TERMINAL	SWHI	HILLSBOROUGH	A	Y	4	C17 TRANSFER POINT E	A	PM	11/14/2003	0.3	POUNDS/HOUR	
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	36	ROCK DRYER & CRUSHER wINSULATED RAY JET BAGHOUSE	A	PM	3/8/2005	0.924	POUNDS/HOUR	Failed to notify the test; Late submittal of tests results; Exceeded the permitted air flow rate.
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	36	ROCK DRYER & CRUSHER wINSULATED RAY JET BAGHOUSE	A	SO2	3/9/2005	0.2	POUNDS/HOUR	Failed to notify the test; Exceeded the permitte flow rate; Late submittal of tests results.
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	14	RAYMOND MILL #1 AND ASSOCIATED CONVEYOR S-1 AND FEED BIN	A	PM	3/3/2005	0.082	POUNDS/HOUR	Failed to notify the test and did not include throughput in the report; Late submittal of tests results.
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	8	BOARD PLANT #1 STUCCO STORAGE SILO	A	PM	3/2/2005	0.089	POUNDS/HOUR	Failed to notify the test and did nto include throughput in the report; Late submittal of tests results; Exceeded permitted flow rate DSCFM.
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	23	#3 CALCIDYNE UNIT	A	PM	3/1/2005	0.131	POUNDS/HOUR	Failed to notify the test and did not include throughput in the report; Late submittal of tests results.
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	23	#3 CALCIDYNE UNIT	A	SO2	3/1/2005	6.03	TONS/YEAR	
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	107	Land Plaster Surge Bin	A	PM	3/7/2005	1.585	TONS/YEAR	
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	23	#3 CALCIDYNE UNIT	A	SO2	3/1/2005	6.03	TONS/YEAR	
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	25	RAYMOND MILL #2, FEED BIN, LAND PLASTER BIN ELEVATOR	A	PM	3/4/2005	0.0063	GRAINS PER DRY STANDARD CUBIC FOOT	Failed to notify the test and did not include throughput in the report; Late submittal of tests results.
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	102	Impact Mill #1	A	PM	11/10/2005	0.0075	GRAINS PER DRY STANDARD CUBIC FOOT	
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	102	Impact Mill #1	A	PM	9/21/2004	0.0035	GRAINS PER DRY STANDARD CUBIC FOOT	Sample volumes were below required 60 dscf. Warning letter sent out on 2/18/05.
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	102	Impact Mill #1	A	PM	3/7/2005	0.0019	GRAINS PER DRY STANDARD CUBIC FOOT	Failed to notify the test; Late submittal of tests results.
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	102	Impact Mill #1	A	PM	3/7/2005	0.0019	GRAINS PER DRY STANDARD CUBIC FOOT	Failed to notify the test; Failed to include fuel c certificate in the report; Late submittal of tests results.
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	103	Impact Mill #2	A	PM	11/9/2005	0.0051	GRAINS PER DRY STANDARD CUBIC FOOT	
													GRAINS PER DRY	Added one more run during auditing to sample

NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	103	Impact Mill #2	A	PM	9/22/2004	0.0027	STANDARD CUBIC FOOT	then 60 dscf to demonstrate compliance.
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	103	Impact Mill #2	A	PM	4/19/2005	0.0032	GRAINS PER DRY STANDARD CUBIC FOOT	Failed to notify the test.
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	103	Impact Mill #2	A	PM	4/19/2005	0.0037	GRAINS PER DRY STANDARD CUBIC FOOT	Failed to notify the test and did not include fuel certificate in the report.
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	103	Impact Mill #2	A	SO2	4/20/2005	1.31	TONS/YEAR	Failed to notify the test.
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	103	Impact Mill #2	A	SO2	4/19/2005	2.87	TONS/YEAR	Failed to notify the test and did not include fuel certificate in the report.
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	108	350 Ton Gyypsum Storage Silo	A	PM	3/8/2005	0.44	TONS/YEAR	
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	102	Impact Mill #1	A	SO2	3/7/2005	1.69	TONS/YEAR	Failed to notify the test; Late submittal of tests results.
NEW NGC, INC.	0570028	NEW NGC, INC.	SWHI	HILLSBOROUGH	A	Y	102	Impact Mill #1	A	SO2	3/4/2005	3.63	TONS/YEAR	Failed to notify the test; Failed the test; Late submittal of tests results; Failed to include fuel certificate in the test report.
KINDER MORGAN PORT SUTTON TERMINAL, LLC	0570029	KINDER MORGAN HARTFORD TERMINAL	SWHI	HILLSBOROUGH	I	Y	12	Prill Rotary Drums w/ Wet Cyclones and Peabody Scrubber	I	PM	1/28/2003	5.1	POUNDS/HOUR	
KINDER MORGAN PORT SUTTON TERMINAL, LLC	0570029	KINDER MORGAN HARTFORD TERMINAL	SWHI	HILLSBOROUGH	I	Y	12	Prill Rotary Drums w/ Wet Cyclones and Peabody Scrubber	I	PM	1/27/2003	2	POUNDS/HOUR	
KINDER MORGAN PORT SUTTON TERMINAL, LLC	0570029	KINDER MORGAN HARTFORD TERMINAL	SWHI	HILLSBOROUGH	I	Y	7	Nitric Acid Plant with 2 Stacks	I	NOX	1/17/2003	57	POUNDS/HOUR	
KINDER MORGAN PORT SUTTON TERMINAL, LLC	0570029	KINDER MORGAN HARTFORD TERMINAL	SWHI	HILLSBOROUGH	I	Y	6	Ammonium Nitrate Prill Tower No. 2	I	PM	1/21/2003	20.2	POUNDS/HOUR	
KINDER MORGAN PORT SUTTON TERMINAL, LLC	0570029	KINDER MORGAN HARTFORD TERMINAL	SWHI	HILLSBOROUGH	I	Y	6	Ammonium Nitrate Prill Tower No. 2	I	PM	1/23/2003	4	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	1	Unit No. 1 Steam Generator (Phase II Acid Rain Unit)	A	PM	4/23/2004	0.02029	POUNDS PER MILLION BTU HEAT INPUT	Oversaturation conditions in run 2 and run 3.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	1	Unit No. 1 Steam Generator (Phase II Acid Rain Unit)	A	PM	4/19/2004	0.01959	POUNDS PER MILLION BTU HEAT INPUT	Oversaturation conditions
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	NOX	9/11/2007	0.07	POUNDS PER MILLION BTU HEAT INPUT	TECO self tested.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	NOX	9/11/2007	0.07	POUNDS PER MILLION BTU HEAT INPUT	TECO self tested.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	1	Unit No. 1 Steam Generator (Phase II Acid Rain Unit)	A	SO2	4/23/2004	787.28	POUNDS/HOUR	Based on operating scenario 3.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	1	Unit No. 1 Steam Generator (Phase II Acid Rain Unit)	A	SO2	10/28/2004	316	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	SO2	4/5/2004	938	POUNDS/HOUR	Calculated from CEM data 104.18 ppmvw
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	SO2	4/5/2004	938	POUNDS/HOUR	
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	SO2	2/25/2005	1037	POUNDS/HOUR	TECO Air Services Group
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	SO2	3/8/2006	609	POUNDS/HOUR	TECO EH&S Air Services Group. Source: CE data.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	SO2	5/18/2007	319	POUNDS/HOUR	Based on scenario 3 of Condition A.9.e
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	NOX	3/23/2004	0.194	POUNDS PER MILLION BTU HEAT INPUT	
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	NOX	11/17/2004	0.246	POUNDS PER MILLION BTU HEAT INPUT	TECO Environmental Health and Safety
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	NOX	4/17/2003	0.313	POUNDS PER MILLION BTU HEAT INPUT	
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	NOX	4/25/2006	0.27	POUNDS PER MILLION BTU HEAT INPUT	
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	NOX	9/12/2007	0.07	POUNDS PER MILLION BTU HEAT INPUT	TECO self tested.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	NOX	9/11/2007	0.07	POUNDS PER MILLION BTU HEAT INPUT	TECO self tested.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	PM	4/5/2007	0.02	POUNDS PER MILLION BTU HEAT INPUT	TECO test team under NON-SOOT BLOWING conditions.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	PM	4/5/2007	0.02	POUNDS PER MILLION BTU HEAT INPUT	TECO test team under SOOT BLOWING conditions.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	PM	2/25/2005	0.02	POUNDS PER MILLION BTU HEAT INPUT	TECO AIr Services Group. Method: CEMS.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	PM	4/5/2004	0.0159	POUNDS PER MILLION BTU HEAT INPUT	Non-soot blowing conditions.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	PM	4/5/2004	0.02	POUNDS PER MILLION BTU HEAT INPUT	
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	PM	4/5/2004	0.01452	POUNDS PER MILLION BTU HEAT INPUT	Soot blowing
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	PM	3/8/2006	0.02	POUNDS PER MILLION BTU HEAT INPUT	TECO EH&S AIr Services Group. Source: CE data.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	PM	4/5/2004	0.02	POUNDS PER MILLION BTU HEAT INPUT	Soot blowing conditions.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	1	Unit No. 1 Steam Generator (Phase II Acid Rain Unit)	A	PM	10/28/2004	0.02855	POUNDS PER MILLION BTU HEAT INPUT	
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	1	Unit No. 1 Steam Generator (Phase II Acid Rain Unit)	A	PM	10/28/2004	0.03156	POUNDS PER MILLION BTU HEAT INPUT	
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	1	Unit No. 1 Steam Generator (Phase II Acid Rain Unit)	A	PM	6/14/2006	0.02	POUNDS PER MILLION BTU HEAT INPUT	Soot blowing conditions. Process rate = 3746 MMBtu/hr and 351 MW.
TAMPA ELECTRIC								Unit No. 1 Steam Generator					POUNDS PER	

COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	1	(Phase II Acid Rain Unit)	A	PM	6/14/2006	0.02	MILLION BTU HEAT INPUT	Non-sootblowing conditions. 351 MW.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	PM	3/26/2003	0.01048	POUNDS PER MILLION BTU HEAT INPUT	TECO self tested.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	PM	3/23/2004	0.00472	POUNDS PER MILLION BTU HEAT INPUT	Test Performed by Tampa Electric Company Environmental Health & Safety.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	PM	11/17/2004	0.0068	POUNDS PER MILLION BTU HEAT INPUT	Test performed by TECO Environmental Healt Safety.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	PM	4/25/2006	0.01	POUNDS PER MILLION BTU HEAT INPUT	PM emissions rate was 33.6 lbs/hr
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	PM	9/11/2007	0.0083	POUNDS PER MILLION BTU HEAT INPUT	TECO self tested. 180.9 tph fuel (90%coal, 9% coke, 1% polk residual) at 420MW.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	2	Unit No. 2 Steam Generator (Phase II Acid Rain Unit)	A	PM	5/10/2003	0.03	POUNDS PER MILLION BTU HEAT INPUT	TECO self tested under non-soot blowing cond
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	2	Unit No. 2 Steam Generator (Phase II Acid Rain Unit)	A	PM	5/10/2003	0.03	POUNDS PER MILLION BTU HEAT INPUT	TECO self tested under sootblowing conditions
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	2	Unit No. 2 Steam Generator (Phase II Acid Rain Unit)	A	PM	7/13/2004	0.01721	POUNDS PER MILLION BTU HEAT INPUT	Soot blowing conditions
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	2	Unit No. 2 Steam Generator (Phase II Acid Rain Unit)	A	PM	7/13/2004	0.017	POUNDS PER MILLION BTU HEAT INPUT	non-soot blowing conditions
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	2	Unit No. 2 Steam Generator (Phase II Acid Rain Unit)	A	PM	12/15/2005	0.02	POUNDS PER MILLION BTU HEAT INPUT	; 160.3 tph fuel consumption
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	2	Unit No. 2 Steam Generator (Phase II Acid Rain Unit)	A	PM	10/26/2006	0.02	POUNDS PER MILLION BTU HEAT INPUT	under non-sootblowing conditions and a proces of 152TPH.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	2	Unit No. 2 Steam Generator (Phase II Acid Rain Unit)	A	PM	10/26/2006	0.03	POUNDS PER MILLION BTU HEAT INPUT	under soot blowing conditions and process rate 152 TPH.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	2	Unit No. 2 Steam Generator (Phase II Acid Rain Unit)	A	PM	9/29/2005	0.03	POUNDS PER MILLION BTU HEAT INPUT	Soot blowing conditions, deintegrated mode.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	2	Unit No. 2 Steam Generator (Phase II Acid Rain Unit)	A	PM	9/29/2005	0.01	POUNDS PER MILLION BTU HEAT INPUT	Non-soot blowing conditions, de-integrated mo
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	2	Unit No. 2 Steam Generator (Phase II Acid Rain Unit)	A	SO2	10/26/2006	0.02	POUNDS PER MILLION BTU HEAT INPUT	or 657 lbs SO2/hr at a process rate of 152 TPH. rate determined using CEMs.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	2	Unit No. 2 Steam Generator (Phase II Acid Rain Unit)	A	SO2	9/29/2005	0.1	POUNDS PER MILLION BTU HEAT INPUT	
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	SO2	4/17/2003	0.118	POUNDS PER MILLION BTU HEAT INPUT	SO2 data taken from Daily EPA CEM Summar
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	SO2	3/23/2004	0	POUNDS PER MILLION BTU HEAT INPUT	Emission rate of .281 lb/mmBtu.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	SO2	11/17/2004	0.293	POUNDS PER MILLION BTU HEAT INPUT	TECO Environmental Health and Safety
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	SO2	4/25/2006	0.34	POUNDS PER MILLION BTU HEAT INPUT	SO2 emission rate = 1434 lbs/hr
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	SO2	9/12/2007	0.12	POUNDS PER MILLION BTU HEAT INPUT	TECO self tested.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	SO2	9/11/2007	0.34	POUNDS PER MILLION BTU HEAT INPUT	TECO self tested.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	SO2	9/11/2007	0.34	POUNDS PER MILLION BTU HEAT INPUT	TECO self tested.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	1	Unit No. 1 Steam Generator (Phase II Acid Rain Unit)	A	SO2	6/14/2006	0.1	POUNDS PER MILLION BTU HEAT INPUT	SO2 CEM data.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	PM	4/4/2003	0.02	POUNDS PER MILLION BTU HEAT INPUT	TECO self tested under sootblowing conditions
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	PM	4/4/2003	0.02	POUNDS PER MILLION BTU HEAT INPUT	TECO self tested under non-sootblowing condi
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit No. 3 Steam Generator (Phase II Acid Rain Unit)	A	PM	2/25/2005	0.015	POUNDS PER MILLION BTU HEAT INPUT	
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	2	Unit No. 2 Steam Generator (Phase II Acid Rain Unit)	A	SO2	12/15/2005	184	POUNDS/HOUR	160.3 tph fuel consumption; 3996 mmBtu/hr he input; fuel type unreported
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	2	Unit No. 2 Steam Generator (Phase II Acid Rain Unit)	A	SO2	5/10/2003	930	POUNDS/HOUR	TECO self tested.
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit No. 4 Steam Generator (Phase II Acid Rain Unit)	A	NH3	9/12/2007	0.91	PARTS PER MILLION DRY GAS VOLUME	Trigon Engineering
TAMPA ELECTRIC COMPANY	0570039	BIG BEND STATION	SWHI	HILLSBOROUGH	A	Y	2	Unit No. 2 Steam Generator (Phase II Acid Rain Unit)	A	SO2	7/13/2004	399.38	POUNDS/HOUR	Soot blowing conditions
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit #4 187.5MW B&W Pressurized Wet Bottom Cyclonic Boiler	I	PM	6/5/2003	81.6	POUNDS/HOUR	Test team is TECO.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	22	Bayside Unit 1C - 169 MW combined cycle gas turbine	A	NH3	3/27/2007	0.0747	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO test team.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	22	Bayside Unit 1C - 169 MW combined cycle gas turbine	A	CO	6/24/2004	0.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	23	Bayside Unit 2A - 169 MW combined cycle gas turbine	A	NH3	4/4/2006	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Max CEMS CO = 1.0 and NOx = 3.0.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	23	Bayside Unit 2A - 169 MW combined cycle gas turbine	A	NH3	4/10/2007	0.103	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO test team
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	20	Bayside Unit 1A - 169 MW combined cycle gas turbine	A	CO	3/23/2005	1.502	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	

TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	20	Bayside Unit 1A - 169 MW combined cycle gas turbine	A	CO	6/30/2004	0.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	data was derived using 10, 21-minute test runs (RATA).
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	20	Bayside Unit 1A - 169 MW combined cycle gas turbine	A	CO	3/20/2007	1.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO test team
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	20	Bayside Unit 1A - 169 MW combined cycle gas turbine	A	CO	3/14/2006	1.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	20	Bayside Unit 1A - 169 MW combined cycle gas turbine	A	CO	3/20/2007	1.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Teco test team
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	26	Bayside Unit 2D - 169 MW combined cycle gas turbine	A	CO	12/17/2003	0.76	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	26	Bayside Unit 2D - 169 MW combined cycle gas turbine	A	CO	3/29/2007	0.8333	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO test team.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	26	Bayside Unit 2D - 169 MW combined cycle gas turbine	A	CO	3/2/2006	0.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	24	Bayside Unit 2B - 169 MW combined cycle gas turbine	A	NOX	4/14/2005	2.811	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	24	Bayside Unit 2B - 169 MW combined cycle gas turbine	A	NOX	4/7/2004	2.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	All averages derived using 9, 21-minute runs (RATA)
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	24	Bayside Unit 2B - 169 MW combined cycle gas turbine	A	NOX	12/16/2003	2.84	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	24	Bayside Unit 2B - 169 MW combined cycle gas turbine	A	NOX	4/6/2006	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	24	Bayside Unit 2B - 169 MW combined cycle gas turbine	A	NOX	4/12/2007	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Teco Test Team.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	22	Bayside Unit 1C - 169 MW combined cycle gas turbine	A	CO	3/15/2005	0.724	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	22	Bayside Unit 1C - 169 MW combined cycle gas turbine	A	NOX	6/24/2004	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	22	Bayside Unit 1C - 169 MW combined cycle gas turbine	A	NOX	3/27/2007	2.97	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO test team.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	22	Bayside Unit 1C - 169 MW combined cycle gas turbine	A	NOX	3/9/2006	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	21	Bayside Unit 1B - 169 MW combined cycle gas turbine	A	NOX	7/28/2004	2.805	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	CEMs used to demonstrate compliance.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	21	Bayside Unit 1B - 169 MW combined cycle gas turbine	A	NOX	6/17/2004	3.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	failed NOx emission rate of 27.6 lbs/hr (permit 23.1 lb/hr)
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	21	Bayside Unit 1B - 169 MW combined cycle gas turbine	A	NOX	3/9/2005	2.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	21	Bayside Unit 1B - 169 MW combined cycle gas turbine	A	NOX	3/16/2006	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	26	Bayside Unit 2D - 169 MW combined cycle gas turbine	A	CO	1/6/2005	1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO Environmental Health and Safety
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	26	Bayside Unit 2D - 169 MW combined cycle gas turbine	A	CO	4/29/2004	0.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	26	Bayside Unit 2D - 169 MW combined cycle gas turbine	A	NOX	1/6/2005	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO Environmental Health and Safety
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	26	Bayside Unit 2D - 169 MW combined cycle gas turbine	A	NOX	4/29/2004	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	26	Bayside Unit 2D - 169 MW combined cycle gas turbine	A	NOX	12/17/2003	3.19	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	26	Bayside Unit 2D - 169 MW combined cycle gas turbine	A	NOX	3/29/2007	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO test team.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	26	Bayside Unit 2D - 169 MW combined cycle gas turbine	A	NOX	3/2/2006	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	25	Bayside Unit 2C - 169 MW combined cycle gas turbine	A	NOX	4/19/2005	2.811	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	25	Bayside Unit 2C - 169 MW combined cycle gas turbine	A	NOX	4/27/2004	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	25	Bayside Unit 2C - 169 MW combined cycle gas turbine	A	NOX	12/20/2003	3.12	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested

TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	25	Bayside Unit 2C - 169 MW combined cycle gas turbine	A	NOX	4/11/2006	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	25	Bayside Unit 2C - 169 MW combined cycle gas turbine	A	NOX	4/24/2007	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test was done by Teco.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	23	Bayside Unit 2A - 169 MW combined cycle gas turbine	A	NOX	4/12/2005	2.8118	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	23	Bayside Unit 2A - 169 MW combined cycle gas turbine	A	NOX	4/22/2004	3.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	23	Bayside Unit 2A - 169 MW combined cycle gas turbine	A	NOX	11/22/2003	3.03	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	23	Bayside Unit 2A - 169 MW combined cycle gas turbine	A	NOX	4/10/2007	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	23	Bayside Unit 2A - 169 MW combined cycle gas turbine	A	NOX	4/10/2007	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO test team
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	23	Bayside Unit 2A - 169 MW combined cycle gas turbine	A	NOX	4/4/2006	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	20	Bayside Unit 1A - 169 MW combined cycle gas turbine	A	NOX	3/23/2005	2.8108	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	20	Bayside Unit 1A - 169 MW combined cycle gas turbine	A	NOX	6/30/2004	3.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	data derived from 10, 21-minute test runs (RAT
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	20	Bayside Unit 1A - 169 MW combined cycle gas turbine	A	NOX	3/20/2007	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO test team
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	20	Bayside Unit 1A - 169 MW combined cycle gas turbine	A	NOX	3/14/2006	3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	21	Bayside Unit 1B - 169 MW combined cycle gas turbine	A	NH3	3/16/2006	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Max CEM ppm = 0.6. NOx = 3.0.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	25	Bayside Unit 2C - 169 MW combined cycle gas turbine	A	CO	4/19/2005	0.577	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	25	Bayside Unit 2C - 169 MW combined cycle gas turbine	A	CO	4/27/2004	0.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	25	Bayside Unit 2C - 169 MW combined cycle gas turbine	A	CO	12/19/2003	0.68	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	25	Bayside Unit 2C - 169 MW combined cycle gas turbine	A	CO	4/11/2006	1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	25	Bayside Unit 2C - 169 MW combined cycle gas turbine	A	NH3	4/11/2006	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Max CEMS CO = 1.0 and NOx = 3.0
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	25	Bayside Unit 2C - 169 MW combined cycle gas turbine	A	NH3	4/24/2007	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test was done by Teco.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	24	Bayside Unit 2B - 169 MW combined cycle gas turbine	A	CO	4/14/2005	0.873	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	24	Bayside Unit 2B - 169 MW combined cycle gas turbine	A	CO	4/7/2004	0.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	All averages were derived using 9, 21-minute t runs (RATA)
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	24	Bayside Unit 2B - 169 MW combined cycle gas turbine	A	CO	12/16/2003	0.91	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	24	Bayside Unit 2B - 169 MW combined cycle gas turbine	A	CO	4/6/2006	0.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	24	Bayside Unit 2B - 169 MW combined cycle gas turbine	A	CO	4/12/2007	1.4667	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Teco Test Team.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	25	Bayside Unit 2C - 169 MW combined cycle gas turbine	A	CO	4/24/2007	0.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test was done by Teco.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	21	Bayside Unit 1B - 169 MW combined cycle gas turbine	A	CO	7/28/2004	1.441	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	CEMs was used to demonstrate compliance.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	21	Bayside Unit 1B - 169 MW combined cycle gas turbine	A	CO	6/17/2004	0.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	21	Bayside Unit 1B - 169 MW combined cycle gas turbine	A	CO	3/9/2005	0.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	21	Bayside Unit 1B - 169 MW combined cycle gas turbine	A	CO	3/16/2006	1.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	26	Bayside Unit 2D - 169 MW combined cycle gas turbine	A	NH3	1/6/2005	0.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO Environmental Health and Safety

TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	26	Bayside Unit 2D - 169 MW combined cycle gas turbine	A	NH3	12/17/2003	3.41	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO self tested.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	26	Bayside Unit 2D - 169 MW combined cycle gas turbine	A	NH3	3/2/2006	0.82	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Max CEMS CO = 0.6 and NOx = 3.0.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	26	Bayside Unit 2D - 169 MW combined cycle gas turbine	A	NH3	3/29/2007	1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO test team.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	23	Bayside Unit 2A - 169 MW combined cycle gas turbine	A	CO	4/12/2005	0.411	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	23	Bayside Unit 2A - 169 MW combined cycle gas turbine	A	CO	4/22/2004	0.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	23	Bayside Unit 2A - 169 MW combined cycle gas turbine	A	CO	11/22/2003	0.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO self test
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	23	Bayside Unit 2A - 169 MW combined cycle gas turbine	A	CO	4/10/2007	1.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO test team
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	23	Bayside Unit 2A - 169 MW combined cycle gas turbine	A	CO	4/4/2006	1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	23	Bayside Unit 2A - 169 MW combined cycle gas turbine	A	CO	4/10/2007	1.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Teco Test Team
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	22	Bayside Unit 1C - 169 MW combined cycle gas turbine	A	NOX	3/15/2005	2.8114	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	22	Bayside Unit 1C - 169 MW combined cycle gas turbine	A	CO	3/27/2007	1.233	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO test team.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	22	Bayside Unit 1C - 169 MW combined cycle gas turbine	A	NH3	3/9/2006	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Max CEMS CO = 1.3 and NOx = 3.0.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	22	Bayside Unit 1C - 169 MW combined cycle gas turbine	A	CO	3/9/2006	1.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	self tested
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	22	Bayside Unit 1C - 169 MW combined cycle gas turbine	A	CO	3/27/2007	1.23	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Teco Test Team
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	20	Bayside Unit 1A - 169 MW combined cycle gas turbine	A	NH3	3/20/2007	0.28	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TECO test team.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	20	Bayside Unit 1A - 169 MW combined cycle gas turbine	A	NH3	3/14/2006	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Maximum monitored CEM CO ppm is 1.5. NO ppm is 3.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	24	Bayside Unit 2B - 169 MW combined cycle gas turbine	A	NH3	4/6/2006	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Max CEMS CO = 0.8 and NOx = 3.0.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	6	Unit #6 414MW Riley Stoker Press. Wet Btm Turbo Furnace Boil	I	PM	8/26/2003	0.1	POUNDS PER MILLION BTU HEAT INPUT	Test performed by TECO Environmental Affair Dept. PM rate is .1235lb/MMBTU, limit is .1 lb/MMBTU.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	6	Unit #6 414MW Riley Stoker Press. Wet Btm Turbo Furnace Boil	I	PM	8/14/2003	0.106	POUNDS PER MILLION BTU HEAT INPUT	Test performed by TECO Environmental Affair Dept. Percent Isokinetic avg. is 86.5%.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	24	Bayside Unit 2B - 169 MW combined cycle gas turbine	A	NH3	4/12/2007	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Teco Test Team.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	6	Unit #6 414MW Riley Stoker Press. Wet Btm Turbo Furnace Boil	I	SO2	8/14/2003	3344	POUNDS/HOUR	Test performed by TECO Environmental Affair Dept.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit #3 179.5MW B&W Pressurized Wet Bottom Cyclonic Boiler	I	PM	7/24/2003	113.2	POUNDS/HOUR	Test team is TECO
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	4	Unit #4 187.5MW B&W Pressurized Wet Bottom Cyclonic Boiler	I	SO2	6/5/2003	3032	POUNDS/HOUR	Test team is TECO.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	6	Unit #6 414MW Riley Stoker Press. Wet Btm Turbo Furnace Boil	I	PM	8/14/2003	336.6	POUNDS/HOUR	Test performed by TECO Environmental Affair Dept.
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	3	Unit #3 179.5MW B&W Pressurized Wet Bottom Cyclonic Boiler	I	SO2	7/24/2003	2149	POUNDS/HOUR	Test team is TECO
TAMPA ELECTRIC COMPANY	0570040	H. L. CULBREATH BAYSIDE POWER STATION	SWHI	HILLSBOROUGH	A	Y	6	Unit #6 414MW Riley Stoker Press. Wet Btm Turbo Furnace Boil	I	SO2	8/26/2003	3348	POUNDS/HOUR	Test performed by TECO Environmental Affair Laboratory Services.
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	CO	8/30/2007	298.73	POUNDS/HOUR	298.73 lbs CO/hr < 320lbs CO/hr (permit limit time of test).
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	CO	7/28/2005	117.2	POUNDS/HOUR	Air Testing & Consulting
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	CO	7/24/2003	171.5	POUNDS/HOUR	Air testing & Consulting.
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	CO	7/19/2006	243.9	POUNDS/HOUR	input TPH 5.36/ Output TPH 3.12
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	SO2	7/19/2006	46.2	POUNDS PER TON OF PRODUCT	input rate 5.36 TPH / output rate 3.12 TPH
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	SO2	7/28/2005	71.2	POUNDS PER TON OF PRODUCT	
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	VOC	8/30/2007	13.5667	PARTS PER MILLION DRY GAS VOLUME	
ENVIROFOCUS													PARTS PER	

TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	VOC	7/27/2004	63.6	MILLION DRY GAS VOLUME	Test performed by Air Testing and Consulting,
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	4	BLAST FURNACE TAPPING AND CHARGING	A	VOC	7/22/2003	4.8	PARTS PER MILLION DRY GAS VOLUME	0.898 lbs VOC/hr
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	4	BLAST FURNACE TAPPING AND CHARGING	A	VOC	7/27/2005	1.3	PARTS PER MILLION DRY GAS VOLUME	
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	4	BLAST FURNACE TAPPING AND CHARGING	A	VOC	8/3/2004	2.6	PARTS PER MILLION DRY GAS VOLUME	Test performed by Air Testing and Consulting,
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	4	BLAST FURNACE TAPPING AND CHARGING	A	VOC	7/27/2006	14.5	PARTS PER MILLION DRY GAS VOLUME	input rate 4.91 TPH / output rate of 3.00 TPH
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	4	BLAST FURNACE TAPPING AND CHARGING	A	VOC	8/29/2007	2.363333	PARTS PER MILLION DRY GAS VOLUME	
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	VOC	9/29/2003	120	PARTS PER MILLION DRY GAS VOLUME	Input rate 5.37TPH & output rate 3.24TPH at a afterburner temp. of 1000 F and corrected to 4% CO2.
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	VOC	7/24/2003	27.1	PARTS PER MILLION DRY GAS VOLUME	
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	VOC	7/28/2005	136.1	PARTS PER MILLION DRY GAS VOLUME	
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	VOC	7/19/2006	40.2	PARTS PER MILLION DRY GAS VOLUME	Input rate 5.36TPH/ output rate of 3.12TPH
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	SO2	7/24/2003	60.1	POUNDS PER TON OF PRODUCT	210.3 lbs SO2/hr while producing 3.5 TPH Pb.
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	SO2	7/27/2004	52.7	POUNDS PER TON OF PRODUCT	Test performed by Air Testing and Consulting,
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	SO2	8/30/2007	70.5	POUNDS PER TON OF PRODUCT	243.33/3.45=70.5 lbsSO2/ton < 76.6 lbs SO2/to (allowed by permit at time of test).
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	CO	7/27/2004	234.7	POUNDS/HOUR	Test performed by Air Testing and Consulting,
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	11	Four Refining Kettles (Process fugitive sources)	A	PM	7/21/2003	0.000453	GRAINS PER DRY STANDARD CUBIC FOOT	0.096111 lbs PM/hr
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	11	Four Refining Kettles (Process fugitive sources)	A	PM	7/17/2006	0.003044	GRAINS PER DRY STANDARD CUBIC FOOT	
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	11	Four Refining Kettles (Process fugitive sources)	A	PM	8/28/2007	0.000732	GRAINS PER DRY STANDARD CUBIC FOOT	
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	11	Four Refining Kettles (Process fugitive sources)	A	PB	8/28/2007	0.000008	GRAINS PER DRY STANDARD CUBIC FOOT	
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	11	Four Refining Kettles (Process fugitive sources)	A	PB	7/17/2006	0.00001	GRAINS PER DRY STANDARD CUBIC FOOT	
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	11	Four Refining Kettles (Process fugitive sources)	A	PB	7/19/2004	0.00003	GRAINS PER DRY STANDARD CUBIC FOOT	Test performed by Air Testing and Consulting I
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	11	Four Refining Kettles (Process fugitive sources)	A	PB	7/26/2005	0.000007	GRAINS PER DRY STANDARD CUBIC FOOT	Air Testing & Consulting
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	11	Four Refining Kettles (Process fugitive sources)	A	PB	7/21/2003	0.000007	GRAINS PER DRY STANDARD CUBIC FOOT	0.0014 lbs Pb/hr
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	4	BLAST FURNACE TAPPING AND CHARGING	A	PM	8/29/2007	0.000241	GRAINS PER DRY STANDARD CUBIC FOOT	
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	4	BLAST FURNACE TAPPING AND CHARGING	A	PM	7/18/2006	0.00139	GRAINS PER DRY STANDARD CUBIC FOOT	input rate 4.91 TPH / output rate 3.00 TPH
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	4	BLAST FURNACE TAPPING AND CHARGING	A	PM	8/3/2004	0	GRAINS PER DRY STANDARD CUBIC FOOT	Test performed by Air Testing and Consulting,
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	4	BLAST FURNACE TAPPING AND CHARGING	A	PM	7/27/2005	0.000512	GRAINS PER DRY STANDARD CUBIC FOOT	
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	4	BLAST FURNACE TAPPING AND CHARGING	A	PM	7/22/2003	0.00188	GRAINS PER DRY STANDARD CUBIC FOOT	0.42769 lbs PM/hr
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	PM	8/30/2007	0.001382	GRAINS PER DRY STANDARD CUBIC FOOT	
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	PM	7/19/2006	0.001871	GRAINS PER DRY STANDARD CUBIC FOOT	input rate 5.36 TPH / Output rate 3.12 TPH
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	PM	7/27/2004	0.002	GRAINS PER DRY STANDARD CUBIC FOOT	Test performed by Air Testing and Consulting I
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	PM	7/28/2005	0.000979	GRAINS PER DRY STANDARD CUBIC FOOT	
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	PM	7/24/2003	0.000415	GRAINS PER DRY STANDARD CUBIC FOOT	0.1 lbs PM/hr
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	PB	8/30/2007	0.00052	GRAINS PER DRY STANDARD CUBIC FOOT	
													GRAINS PER	

ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	PB	7/19/2006	0.000292	DRY STANDARD CUBIC FOOT	input rate 5.36TPH / Output rate 3.12 TPH
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	PB	7/27/2004	0.00066	GRAINS PER DRY STANDARD CUBIC FOOT	Test performed by Air Testing and Consulting,
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	PB	7/28/2005	0.00058	GRAINS PER DRY STANDARD CUBIC FOOT	Test was conducted with 9 baghouse compartm instead of all 10.
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	1	BLAST FURNACE EXHAUST	A	PB	7/24/2003	0.000047	GRAINS PER DRY STANDARD CUBIC FOOT	0.0115 lbs PB/hr
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	4	BLAST FURNACE TAPPING AND CHARGING	A	PB	8/29/2007	0.000019	GRAINS PER DRY STANDARD CUBIC FOOT	
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	4	BLAST FURNACE TAPPING AND CHARGING	A	PB	7/18/2006	0.000025	GRAINS PER DRY STANDARD CUBIC FOOT	input rate 4.91 TPH / output rate 3 TPH
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	4	BLAST FURNACE TAPPING AND CHARGING	A	PB	8/3/2004	0.00005	GRAINS PER DRY STANDARD CUBIC FOOT	Test performed by Air Testing and Consulting,
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	4	BLAST FURNACE TAPPING AND CHARGING	A	PB	7/27/2005	0.000001	GRAINS PER DRY STANDARD CUBIC FOOT	Air Testing & Consulting
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	4	BLAST FURNACE TAPPING AND CHARGING	A	PB	7/22/2003	0.000009	GRAINS PER DRY STANDARD CUBIC FOOT	0.002069 lbs Pb/hr
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	11	Four Refining Kettles (Process fugitive sources)	A	PM	7/19/2004	0.001	GRAINS PER DRY STANDARD CUBIC FOOT	Test performed by Air Testing and Consulting,
ENVIROFOCUS TECHNOLOGIES, LLC	0570057	ENVIROFOCUS TECHNOLOGIES, LLC	SWHI	HILLSBOROUGH	A	Y	11	Four Refining Kettles (Process fugitive sources)	A	PM	7/26/2005	0.000411	GRAINS PER DRY STANDARD CUBIC FOOT	
CORONET INDUSTRIES, INC.	0570075	CORONET INDUSTRIES, INC.	SWHI	HILLSBOROUGH	I	Y	1	FEED PREP PLANT DRYER WITH WET SCRUBBER.	I	PM	3/12/2003	0.9853	POUNDS/HOUR	By ATC
CORONET INDUSTRIES, INC.	0570075	CORONET INDUSTRIES, INC.	SWHI	HILLSBOROUGH	I	Y	23	FLUORIDE PLANT NUMBER 1 WITH SCRUBBER	I	PM	3/13/2003	0.0121	POUNDS/HOUR	By ATC
CORONET INDUSTRIES, INC.	0570075	CORONET INDUSTRIES, INC.	SWHI	HILLSBOROUGH	I	Y	5	DEFLUORINATING KILNS 6 & 7	I	FL	4/17/2003	0.35	POUNDS PER TON OF FEED MATERIAL	Test team is AT@C
CORONET INDUSTRIES, INC.	0570075	CORONET INDUSTRIES, INC.	SWHI	HILLSBOROUGH	I	Y	1	FEED PREP PLANT DRYER WITH WET SCRUBBER.	I	FL	3/12/2003	0.0451	POUNDS PER TON OF PRODUCT	By ATC
CORONET INDUSTRIES, INC.	0570075	CORONET INDUSTRIES, INC.	SWHI	HILLSBOROUGH	I	Y	15	NORTH MILL ROOM W/ BAGHOUSE	I	PM	3/14/2003	3.8	POUNDS/HOUR	
CORONET INDUSTRIES, INC.	0570075	CORONET INDUSTRIES, INC.	SWHI	HILLSBOROUGH	I	Y	18	SOUTH MILL ROOM W/ BAGHOUSE	I	PM	3/14/2003	0.54	POUNDS/HOUR	
CORONET INDUSTRIES, INC.	0570075	CORONET INDUSTRIES, INC.	SWHI	HILLSBOROUGH	I	Y	21	CRANEWAY-TEMPORARY PRODUCT STORAGE CONTROLLED BY BGHS #14	I	PM	11/11/2003	0.81	POUNDS/HOUR	Baghouse # 1
CORONET INDUSTRIES, INC.	0570075	CORONET INDUSTRIES, INC.	SWHI	HILLSBOROUGH	I	Y	5	DEFLUORINATING KILNS 6 & 7	I	PM	4/17/2003	6.42	POUNDS/HOUR	Test team is AT@C
MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	2/14/2003	0.75	MILLIGRAMS PER LITER OF LIQUID LOADED	Test conducted by Environmental Field Service Stack Testing Group.
MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	2/11/2003	1.66	MILLIGRAMS PER LITER OF LIQUID LOADED	Test performed by Marathon Environmental Fi Services Section.(West VRU)
MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	12/2/2004	1.1	MILLIGRAMS PER LITER OF LIQUID LOADED	Total accountable gasoline volume = 1072514 Six hours.
MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	2/14/2003	0.51	MILLIGRAMS PER LITER OF LIQUID LOADED	Test performed at the RANE VCU
MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	2/12/2003	0.57	MILLIGRAMS PER LITER OF LIQUID LOADED	Test performed by Marathon Ashland field serv section. (East VRU)
MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	3/17/2004	1.44	MILLIGRAMS PER LITER OF LIQUID LOADED	Test done by Marathon Field Services Section.
MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	12/17/2003	0.42	MILLIGRAMS PER LITER OF LIQUID LOADED	Test done by Marathon Field Services Group.
MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	3/29/2006	0.63	MILLIGRAMS PER LITER OF LIQUID LOADED	Standard equivalency calculated as, 0.66% for t compliance test
MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	3/29/2007	1.64	MILLIGRAMS PER LITER OF LIQUID LOADED	224,981 gallons were used for measuring the vo emissions. Marathon's Refining Analytical & Dvelopment Department Environmental Field services Stack Testing Group performed the tes
MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	3/28/2007	0.63	MILLIGRAMS PER LITER OF LIQUID LOADED	325,483 gallons were used for measuring the vo emissions. Marathon's Refining Analytical & Dvelopment Department Environmental Field services Stack Testing Group performed the tes
MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	3/26/2007	1.44	MILLIGRAMS PER LITER OF LIQUID LOADED	Testing Co.: Marathon Petroleum Co. Refining Analytical & Development Dept.
MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	7/7/2006	3.92	MILLIGRAMS PER LITER OF LIQUID LOADED	this compliance test was suppose to include temperature data in order to determine an opera temperature range. Temperature data was some lost. Marathon will be retesting again in order t determine a temperature range in which to oper
MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	8/22/2006	1.58	MILLIGRAMS PER LITER OF LIQUID LOADED	This test is for the propose of setting control temperature for the VCU not a regular complia test.

MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	11/16/2005	2.36	MILLIGRAMS PER LITER OF LIQUID LOADED	2,174,899 liters gasoline was loaded into 91 tru in a 6 hour period.
MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	3/30/2006	1.72	MILLIGRAMS PER LITER OF LIQUID LOADED	
MARATHON PETROLEUM COMPANY LLC	0570080	MARATHON PETROLEUM COMPANY LLC-TAMPA 02	SWHI	HILLSBOROUGH	A	Y	1	2 Loading Racks (10Bays) , 2 Carbon Adsorbers & VCUbackup	A	VOC	3/18/2004	0.91	MILLIGRAMS PER LITER OF LIQUID LOADED	Test done by Marathon Field Services Section
TRANSMONTAIGNE PRODUCT SERVICES INC.	0570081	TRANSMONTAIGNE TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	1	Truck Loading Rack	A	VOC	7/16/2003	3.74	MILLIGRAMS PER LITER OF LIQUID LOADED	
TRANSMONTAIGNE PRODUCT SERVICES INC.	0570081	TRANSMONTAIGNE TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	1	Truck Loading Rack	A	VOC	7/17/2003	10	MILLIGRAMS PER LITER OF LIQUID LOADED	The actual mg/liter was determined by the meth outlined in CFR 60.18(f)(3).
TRANSMONTAIGNE PRODUCT SERVICES INC.	0570081	TRANSMONTAIGNE TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	1	Truck Loading Rack	A	VOC	7/28/2005	4.66	MILLIGRAMS PER LITER OF LIQUID LOADED	Method 25A on VCU exhaust and Method 25B VCU inlet; 653,533 liters loaded; DE = 99.14%
TRANSMONTAIGNE PRODUCT SERVICES INC.	0570081	TRANSMONTAIGNE TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	1	Truck Loading Rack	A	VOC	7/26/2007	3.89	MILLIGRAMS PER LITER OF LIQUID LOADED	Destruction Efficiency at 99.38%.
TRANSMONTAIGNE PRODUCT SERVICES INC.	0570081	TRANSMONTAIGNE TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	1	Truck Loading Rack	A	VOC	8/2/2006	3.16	MILLIGRAMS PER LITER OF LIQUID LOADED	
TRANSMONTAIGNE PRODUCT SERVICES INC.	0570081	TRANSMONTAIGNE TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	1	Truck Loading Rack	A	VOC	7/1/2004	6.11	MILLIGRAMS PER LITER OF LIQUID LOADED	156213 gallons of gasolines loaded in a 6 hr pe
CENTRAL FLORIDA PIPELINE	0570085	TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	3	TRUCK LOADING RACK (T/T) AREA 7	A	VOC	5/2/2003	35	MILLIGRAMS PER LITER OF LIQUID LOADED	Max Orifice Vel = 10.0 fps; Vapor Press = 6.7 H2O; Avg Heat Value = 730.1 BTU/scf
CENTRAL FLORIDA PIPELINE	0570085	TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	3	TRUCK LOADING RACK (T/T) AREA 7	A	VOC	4/22/2004	0	MILLIGRAMS PER LITER OF LIQUID LOADED	Emissions are regulated by maintaining minimu heating value of 300Btu/scf. Test heating value 643.5Btu/scf. Test performed by Catalyst Air Managent.
CENTRAL FLORIDA PIPELINE	0570085	TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	3	TRUCK LOADING RACK (T/T) AREA 7	A	VOC	4/14/2005	35	MILLIGRAMS PER LITER OF LIQUID LOADED	Vapor heating value = 476 btu/scf; Max Veloci 69.8fps; VP = 15 in wc; VE = 0 min.
CENTRAL FLORIDA PIPELINE	0570085	TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	3	TRUCK LOADING RACK (T/T) AREA 7	A	VOC	6/21/2007	35	MILLIGRAMS PER LITER OF LIQUID LOADED	Flare net heating value = 697 Btu/scf (EPA allowable > 300), Exit Velocity = 5.38 ft/sec (I allowable V Max - 88.98 ft/sec). Visible emissi @ 21 seconds/2 hrs and continuos pilot light verification.
CENTRAL FLORIDA PIPELINE	0570085	TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	3	TRUCK LOADING RACK (T/T) AREA 7	A	VOC	8/31/2006	35	MILLIGRAMS PER LITER OF LIQUID LOADED	Test Team: Jodan Technology; Vmax = 42.19 m/sec, Inlet velocity (observed) = 3.92 m/sec.
CENTRAL FLORIDA PIPELINE	0570085	TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	3	TRUCK LOADING RACK (T/T) AREA 7	A	VOC	4/14/2005	35	MILLIGRAMS PER LITER OF LIQUID LOADED	Testing company: Catalyst Air Management In made mistakes in reporting allowable and max. observed flare tip velocities. The final test repo showed 70.24 f/s allowable and 8.0 f/s for max. observed velocity.
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	H027	7/24/2006	0.00003	GRAINS PER DRY STANDARD CUBIC FOOT	
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	SO2	3/27/2003	6.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	tested by ATC
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	CO	7/16/2004	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test performed by Air Testing and Consulting I
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	CO	3/27/2003	2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	tested bt ATC
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	CO	7/17/2003	21.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	#3 Run @ 63.99 ppmv @ 7% O2, but 3 run avg Air Testing and Consulting
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	H106	5/24/2007	100	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing & Consultiong
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	H106	7/24/2006	8.11	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	H106	7/16/2004	19.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test performed by Air Testing and Consulting I
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	H106	3/27/2003	7.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	tested by ATC
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	H106	7/17/2003	3.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing and Consulting
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	SO2	7/24/2006	14	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test required for permit renewal. Section A.24 permit 0570089-013-AO
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	CO	7/5/2007	0.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing Consulting
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	CO	7/24/2006	3.7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	NOX	7/24/2006	136.345	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test is required for permit renewal. Section A.2 0570089-013-AO
ST. JOSEPH'S		ST. JOSEPH'S											GRAINS PER DRY	

HOSPITAL	0570089	HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	H114	7/24/2006	0.00003	STANDARD CUBIC FOOT	
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	PM	7/16/2004	0.002	GRAINS PER DRY STANDARD CUBIC FOOT	Test performed by Air Testing and Consulting I
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	PM	7/24/2006	0.0015	GRAINS PER DRY STANDARD CUBIC FOOT	
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	PM	7/17/2003	0.0005	GRAINS PER DRY STANDARD CUBIC FOOT	Avg of 3 runs; Air Testing and Consulting
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	PB	7/24/2006	0.00003	GRAINS PER DRY STANDARD CUBIC FOOT	
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	PM	5/24/2007	0.001	GRAINS PER DRY STANDARD CUBIC FOOT	Air Testing & Consulting
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	3	COGENERATION PLANT #1	A	NOX	6/8/2007	2.6	POUNDS/HOUR	air testing & consuling
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	3	COGENERATION PLANT #1	A	CO	6/8/2006	5.6	POUNDS/HOUR	Air Testing & Consulting
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	2	WASTE INCINERATOR	A	H058	7/24/2006	55.374	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
ST. JOSEPH'S HOSPITAL	0570089	ST. JOSEPH'S HOSPITAL	SWHI	HILLSBOROUGH	A	Y	3	COGENERATION PLANT #1	A	VOC	6/8/2007	7.7	POUNDS/HOUR	air testing & consuling
GULF COAST METALS, INC.	0570119	GULF COAST METALS	SWHI	HILLSBOROUGH	A	Y	5	ALUMINUM ROTARY FURNACE #1	A	DIOX	8/11/2005	0.0002	OTHER (SPECIFY IN COMMENT)	Test results averaging only Reuns 1 and 3. Run discarded for irregularities with nozzles. See Er Case No. 04-0804DL0119 for further details.
GULF COAST METALS, INC.	0570119	GULF COAST METALS	SWHI	HILLSBOROUGH	A	Y	5	ALUMINUM ROTARY FURNACE #1	A	PM	8/18/2005	0.00128	GRAINS PER DRY STANDARD CUBIC FOOT	See Enforcement Case 04-0804DL0119 for furt information on the results.
HESS CORPORATION	0570123	HESS CORPORATION-TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	3	TRUCK LOADING RACKS W/ VAPOR RECOVERY EQUIPMENT.	A	VOC	11/11/2003	5.14	MILLIGRAMS PER LITER OF LIQUID LOADED	Test performed by The Jordan Service Co.
HESS CORPORATION	0570123	HESS CORPORATION-TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	3	TRUCK LOADING RACKS W/ VAPOR RECOVERY EQUIPMENT.	A	VOC	11/2/2005	14.19	MILLIGRAMS PER LITER OF LIQUID LOADED	
HESS CORPORATION	0570123	HESS CORPORATION-TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	3	TRUCK LOADING RACKS W/ VAPOR RECOVERY EQUIPMENT.	A	VOC	6/19/2007	0.89	MILLIGRAMS PER LITER OF LIQUID LOADED	Test performed by Jordan Technologies Inc.
HESS CORPORATION	0570123	HESS CORPORATION-TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	3	TRUCK LOADING RACKS W/ VAPOR RECOVERY EQUIPMENT.	A	VOC	11/24/2007	2.86	MILLIGRAMS PER LITER OF LIQUID LOADED	Test performed by Jordan Technologies Inc. ; 228400 accountable gallons loaded.
HESS CORPORATION	0570123	HESS CORPORATION-TAMPA TERMINAL	SWHI	HILLSBOROUGH	A	Y	3	TRUCK LOADING RACKS W/ VAPOR RECOVERY EQUIPMENT.	A	VOC	11/2/2006	37.07	MILLIGRAMS PER LITER OF LIQUID LOADED	this test is incomplete since all 9-hr are not accounted for. results will be revised once the r is resubmitted.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	NOX	10/5/2005	139.25	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Operated at 78.6% of max capacity rating
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	NOX	10/10/2006	149.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	NOX	10/9/2007	143.81	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H106	10/11/2007	5.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H106	10/13/2006	15	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H106	10/6/2005	6.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H106	10/5/2004	15.35	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Operating at 78.4% of permit limit.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H106	10/7/2003	11	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	98% HCL reduction
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	SO2	10/11/2007	3.17	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	SO2	10/13/2006	2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	SO2	10/7/2005	0.33	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Operated at 77.8% of max permit limit
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	SO2	10/9/2007	3.86	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	SO2	10/4/2005	0.28	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Operated at 78.6% of max capacity rating
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H106	10/9/2007	5.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H106	10/12/2006	8.6	PARTS PER MILLION DRY GAS VOLUME	

		FACILITY											@ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H106	10/4/2005	4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H106	10/7/2004	2.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Operating at 78.3% of permit rate.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H106	10/9/2003	11	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	NOX	10/11/2007	136.27	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	NOX	10/13/2006	161	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	NOX	10/7/2005	143.81	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Operated at 77.8% of max permitted rate
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H106	10/8/2003	6.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	99% HCL removal.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	CO	10/11/2007	10.26	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	CO	10/13/2006	14.12	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	CO	10/7/2005	10.96	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Operated at 77.8% of max permitted rate
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	CO	10/12/2007	11.79	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	CO	10/12/2006	13	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	CO	10/6/2005	13.48	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Operated at 78.7% of capacity rating
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	SO2	10/10/2007	0.91	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	SO2	10/11/2006	9.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	PB	10/8/2004	0.0155	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 78.7% of permit limit.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	PB	10/8/2003	0.00095	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	PM	10/12/2007	1.1	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	PM	10/10/2006	1.6	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	PM	10/7/2005	4.8	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	PM	10/6/2004	3.059	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 77.7% of permit limit.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	PM	10/8/2003	1.3	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	SO2	10/12/2007	1.31	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	SO2	10/12/2006	1.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	PM	10/13/2006	0.57	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	PM	10/6/2005	1.9	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	PM	10/5/2004	2.041	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 78.4% of permit limit.
													MILLIGRAMS	

CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	PM	10/7/2003	1.1	PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	PM	10/10/2007	0.67	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	PM	10/11/2006	2.4	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	PM	10/5/2005	1	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	PM	10/8/2004	0.8973	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 78.8% of permit limit.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	PM	10/10/2003	1.1	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H114	10/6/2004	0.00221	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 78.6% of permit rate.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	PB	10/12/2007	0.0017	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	PB	10/11/2006	0.012	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	PB	10/5/2005	0.00077	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	PB	10/6/2004	0.000417	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 78.6% of permit limit.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	PB	10/10/2003	0.001	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H027	10/9/2007	0.00022	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H027	10/10/2006	0.00032	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H027	10/4/2005	0.00022	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H027	10/6/2005	0.0016	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H027	10/5/2004	0.000848	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 78.4% of permit limit.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H027	10/7/2003	0.0046	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	PB	10/11/2007	0.0048	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	PB	10/13/2006	0.012	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	PB	10/6/2005	0.019	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	PB	10/5/2004	0.00787	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 78.4% of permit limit.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	PB	10/7/2003	0.0012	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H027	10/12/2007	0.00025	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H027	10/11/2007	0.0005	MILLIGRAMS PER DRY STANDARD	

		FACILITY											CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H027	10/13/2006	0.00016	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H027	10/11/2006	0.00014	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H027	10/5/2005	0.00036	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H027	10/6/2004	0.000131	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 78.5% of permit rate.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H027	10/10/2003	0.00022	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H114	10/12/2007	0.0019	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H114	10/10/2003	0.01	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H114	10/11/2006	0.0024	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H114	10/5/2005	0.0038	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	carbon feed rate = 3 lbs/hr
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H027	10/7/2004	0.00019	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 77.9% of permit limit.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H027	10/9/2003	0.00028	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	PB	10/9/2007	0.0016	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	PB	10/10/2006	0.012	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	PB	10/4/2005	0.0015	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	PB	10/7/2004	0.00101	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 77.9% of permit limit
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	PB	10/9/2003	0.00081	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	PM	10/11/2007	1.7	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H027	10/10/2007	0.00029	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H027	10/12/2006	0.00026	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H027	10/7/2005	0.00074	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H027	10/8/2004	0.00153	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 78.7% of permit limit.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H027	10/8/2003	0.0006	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	PB	10/10/2007	0.0039	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	PB	10/12/2006	0.014	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	

CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	PB	10/7/2005	0.0062	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	SO2	10/6/2005	0.36	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Operated at 78.7% of max capacity rating
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	NOX	10/12/2007	145.54	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	NOX	10/12/2006	144	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	NOX	10/6/2005	132.18	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	operated at 78.7% of capacity rating
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H106	10/12/2007	12.7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H106	10/10/2006	5.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H106	10/7/2005	6.7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H106	10/6/2004	5.842	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Operating at 77.7% of permit limit.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H106	10/10/2007	5.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H106	10/11/2006	7.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H106	10/5/2005	5.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H106	10/8/2004	4.355	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Operating at 78.8% of permit limit.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H106	10/10/2003	10	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	98% removal eff of HCL
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	CO	10/10/2007	12.72	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	CO	10/11/2006	9.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	CO	10/4/2005	7.36	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Operated at 78.6% of max permit limit; 1 run eliminated from RATA runs
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	SO2	10/10/2006	3.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	SO2	10/5/2005	3.21	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Operated at 78.6% of maximum capacity
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	CO	10/9/2007	11.52	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	CO	10/10/2006	7.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	CO	10/5/2005	10.11	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Operated at 78.6% of max capacity rating
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	NOX	10/10/2007	116.43	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	NOX	10/11/2006	138.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	NOX	10/4/2005	142.32	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Operated at 78.6% of max permitted limit
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	PM	10/9/2003	0.66	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H114	10/7/2004	0.00322	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 77.9% of permit limit.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H114	10/10/2006	0.0018	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H114	10/9/2007	0.0026	MILLIGRAMS PER DRY STANDARD CUBIC METER	

													@ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	DIOX	10/4/2005	3.1	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	DIOX	10/7/2003	1	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Baghouse inlet temp 315 F & carbon feed rate (3lbs/hr.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	DIOX	10/11/2007	2.7	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	DIOX	10/5/2004	1.4	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 77.8% of permit limit.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H114	10/8/2003	0.0094	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H114	10/12/2006	0.0031	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H114	10/7/2005	0.011	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	carbon feed rate = 3 lbs/hr
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H114	10/8/2004	0.00589	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 78.7% of permit limit.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H114	10/11/2007	0.0029	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H114	10/7/2003	0.002	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H114	10/13/2006	0.0045	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H114	10/6/2005	0.0045	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H114	10/5/2004	0.00375	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 78.4% of permit limit.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	DIOX	10/11/2006	1.5	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H114	10/10/2007	0.0061	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H114	10/9/2003	0.0044	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H114	10/4/2005	0.0029	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	carbon feed rate = 3 lbs/hr
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	PM	10/7/2004	2.07	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Operating at 78.3% of permit rate.
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	PM	10/12/2006	0.73	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	PM	10/9/2007	0.64	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	PM	10/4/2005	1	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	H021	10/13/2006	0	POUNDS PER MILLION BTU HEAT INPUT	.0000000214 lbs Be/mmbtu
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	106	Municipal Waste Combustor & Auxiliary Burners-Unit 4	A	FL	10/5/2005	0.000063	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	H021	10/11/2006	0	POUNDS PER MILLION BTU HEAT INPUT	.0000000207lbs Be/mmbtu
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	H021	10/10/2006	0	POUNDS PER MILLION BTU HEAT INPUT	.0000000212 lbs Be/mmbtu
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	103	Municipal Waste Combustor & Auxiliary Burners-Unit 1	A	FL	10/10/2006	0.000448	POUNDS PER MILLION BTU HEAT INPUT	Passed fluoride audit sample #M13B-2539-03

CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	104	Municipal Waste Combustor & Auxiliary Burners-Unit 2	A	FL	10/13/2006	0.00049	POUNDS PER MILLION BTU HEAT INPUT	Passed fluoride audit sample #M13B-2539-03
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	FL	10/5/2005	0.000064	POUNDS PER MILLION BTU HEAT INPUT	Steam Production 61,700 lbs/hr; flow rate = 23 dscfm
CITY OF TAMPA	0570127	MCKAY BAY REFUSE-TO-ENERGY FACILITY	SWHI	HILLSBOROUGH	A	Y	105	Municipal Waste Combustor & Auxiliary Burners-Unit 3	A	H021	10/12/2006	0	POUNDS PER MILLION BTU HEAT INPUT	
BALL METAL BEVERAGE CONTAINER CORP.	0570160	BALL METAL BEVERAGE CONTAINER CORP.	SWHI	HILLSBOROUGH	A	Y	1	INTERNAL COATING, LINE 1 & 2 (Includes RTO Test Data)	A	VOC	7/31/2007	98	OTHER (SPECIFY IN COMMENT)	DE test for RTO; AIRTECH conducted the test RTO temp = 1500 F; Permit required 95% DE.
BALL METAL BEVERAGE CONTAINER CORP.	0570160	BALL METAL BEVERAGE CONTAINER CORP.	SWHI	HILLSBOROUGH	A	Y	1	INTERNAL COATING, LINE 1 & 2 (Includes RTO Test Data)	A	VOC	8/3/2005	93.5	OTHER (SPECIFY IN COMMENT)	Capture Efficiency Test; Airtech Environmenta Services
BALL METAL BEVERAGE CONTAINER CORP.	0570160	BALL METAL BEVERAGE CONTAINER CORP.	SWHI	HILLSBOROUGH	A	Y	6	INTERNAL COATING, LINE 3	A	VOC	8/2/2007	96.5	OTHER (SPECIFY IN COMMENT)	AIRTECH conducted the testing; CE test for external and internal coating for Line 3.
BALL METAL BEVERAGE CONTAINER CORP.	0570160	BALL METAL BEVERAGE CONTAINER CORP.	SWHI	HILLSBOROUGH	A	Y	1	INTERNAL COATING, LINE 1 & 2 (Includes RTO Test Data)	A	VOC	8/2/2005	97.57	OTHER (SPECIFY IN COMMENT)	RTO set point = 1,500 degrees F; Tested by AI Environmental Services
BALL METAL BEVERAGE CONTAINER CORP.	0570160	BALL METAL BEVERAGE CONTAINER CORP.	SWHI	HILLSBOROUGH	A	Y	1	INTERNAL COATING, LINE 1 & 2 (Includes RTO Test Data)	A	VOC	11/29/2006	98.1	OTHER (SPECIFY IN COMMENT)	Minimum Destruction efficiency = 95%; Test T = Airtech Environmental Services Inc.
BALL METAL BEVERAGE CONTAINER CORP.	0570160	BALL METAL BEVERAGE CONTAINER CORP.	SWHI	HILLSBOROUGH	A	Y	1	INTERNAL COATING, LINE 1 & 2 (Includes RTO Test Data)	A	VOC	8/1/2007	71.4	OTHER (SPECIFY IN COMMENT)	CE of Line 1&2 including external and internal coatings; Permitted CE = 65%, the facility faile DQO so the LCL was used as the CE instead of averaged CE during the testing.
MOTIVA ENTERPRISES LLC	0570197	MOTIVA ENTERPRISES LLC	SWHI	HILLSBOROUGH	A	Y	2	Loading Rack w/ Vapor Recovery Unit & Vapor Combustion Unit	A	VOC	11/3/2003	3.32	MILLIGRAMS PER LITER OF LIQUID LOADED	Test performed by The Jordan Service Co. Rec Efficiency = 99.65%.
MOTIVA ENTERPRISES LLC	0570197	MOTIVA ENTERPRISES LLC	SWHI	HILLSBOROUGH	A	Y	2	Loading Rack w/ Vapor Recovery Unit & Vapor Combustion Unit	A	VOC	2/11/2003	0.98	MILLIGRAMS PER LITER OF LIQUID LOADED	Total gasoline loaded = 171,835 gallons.
MOTIVA ENTERPRISES LLC	0570197	MOTIVA ENTERPRISES LLC	SWHI	HILLSBOROUGH	A	Y	2	Loading Rack w/ Vapor Recovery Unit & Vapor Combustion Unit	A	VOC	6/3/2004	1.17	MILLIGRAMS PER LITER OF LIQUID LOADED	Test performed by Jordan Service Group.
MOTIVA ENTERPRISES LLC	0570197	MOTIVA ENTERPRISES LLC	SWHI	HILLSBOROUGH	A	Y	2	Loading Rack w/ Vapor Recovery Unit & Vapor Combustion Unit	A	VOC	2/9/2006	1.34	MILLIGRAMS PER LITER OF LIQUID LOADED	
MOTIVA ENTERPRISES LLC	0570197	MOTIVA ENTERPRISES LLC	SWHI	HILLSBOROUGH	A	Y	2	Loading Rack w/ Vapor Recovery Unit & Vapor Combustion Unit	A	VOC	2/8/2005	0.89	MILLIGRAMS PER LITER OF LIQUID LOADED	
MOTIVA ENTERPRISES LLC	0570197	MOTIVA ENTERPRISES LLC	SWHI	HILLSBOROUGH	A	Y	2	Loading Rack w/ Vapor Recovery Unit & Vapor Combustion Unit	A	VOC	3/9/2005	0.9	MILLIGRAMS PER LITER OF LIQUID LOADED	Test performed by Jordan Service Company, In
MOTIVA ENTERPRISES LLC	0570197	MOTIVA ENTERPRISES LLC	SWHI	HILLSBOROUGH	A	Y	2	Loading Rack w/ Vapor Recovery Unit & Vapor Combustion Unit	A	VOC	2/9/2005	2.15	MILLIGRAMS PER LITER OF LIQUID LOADED	Test by Jordan Service Co.
MOTIVA ENTERPRISES LLC	0570197	MOTIVA ENTERPRISES LLC	SWHI	HILLSBOROUGH	A	Y	2	Loading Rack w/ Vapor Recovery Unit & Vapor Combustion Unit	A	VOC	2/8/2006	0.89	MILLIGRAMS PER LITER OF LIQUID LOADED	
MOTIVA ENTERPRISES LLC	0570197	MOTIVA ENTERPRISES LLC	SWHI	HILLSBOROUGH	A	Y	2	Loading Rack w/ Vapor Recovery Unit & Vapor Combustion Unit	A	VOC	2/21/2007	1.93	MILLIGRAMS PER LITER OF LIQUID LOADED	1.93=683,601.72 total mg/355,033total account liters. test team Jordan technology.
GOLDEN ALUMINUM EXTRUSION - PLANT CITY,	0570249	GOLDEN ALUMINUM EXTRUSION PLANT CITY, LL	SWHI	HILLSBOROUGH	A	Y	14	MELT FURNACE #1 AND #2 (CAST HOUSE NO.2)	A	H106	7/10/2007	0.27	POUNDS PER TON OF FEED MATERIAL	North furnace charge rate = 2.57 tons/hour. Ne flux rate is 0.852lbsCl/ton charged.
GOLDEN ALUMINUM EXTRUSION - PLANT CITY,	0570249	GOLDEN ALUMINUM EXTRUSION PLANT CITY, LL	SWHI	HILLSBOROUGH	A	Y	14	MELT FURNACE #1 AND #2 (CAST HOUSE NO.2)	A	PM	7/10/2007	0.374	POUNDS PER TON OF FEED MATERIAL	North Furnace Charge rate = 2.57 tons/hour
GOLDEN ALUMINUM EXTRUSION - PLANT CITY,	0570249	GOLDEN ALUMINUM EXTRUSION PLANT CITY, LL	SWHI	HILLSBOROUGH	A	Y	14	MELT FURNACE #1 AND #2 (CAST HOUSE NO.2)	A	DIOX	7/10/2007	0.275	OTHER (SPECIFY IN COMMENT)	North Furnace Charge rate = 2.57 tons/hour
GOLDEN ALUMINUM EXTRUSION - PLANT CITY,	0570249	GOLDEN ALUMINUM EXTRUSION PLANT CITY, LL	SWHI	HILLSBOROUGH	A	Y	11	VERTICAL PAINT LINE	A	VOC	7/17/2007	96.9	PERCENT REDUCTION IN EMISSIONS	
GOLDEN ALUMINUM EXTRUSION - PLANT CITY,	0570249	GOLDEN ALUMINUM EXTRUSION PLANT CITY, LL	SWHI	HILLSBOROUGH	A	Y	11	VERTICAL PAINT LINE	A	VOC	12/24/2005	97.7	PERCENT REDUCTION IN EMISSIONS	Avg RTO Temp = 1530 oF; Avg Paint Usage = gal/hr, 474 lbs/hr; Avg Line Speed = 18-20 fpm Avg 1587 pcs/hr; Avg Air Flow Inlet to RTO = 20,555 dscfm
GOLDEN ALUMINUM EXTRUSION - PLANT CITY,	0570249	GOLDEN ALUMINUM EXTRUSION PLANT CITY, LL	SWHI	HILLSBOROUGH	A	Y	11	VERTICAL PAINT LINE	A	VOC	7/27/2006	98.3	PERCENT REDUCTION IN EMISSIONS	RTO avg T=1470F ; Paint usage 504lbs/hr ; EP Method 24 results (45.8%solids & 54.2% volat
GOLDEN ALUMINUM EXTRUSION - PLANT CITY,	0570249	GOLDEN ALUMINUM EXTRUSION PLANT CITY, LL	SWHI	HILLSBOROUGH	A	Y	11	VERTICAL PAINT LINE	A	VOC	3/5/2003	95.03	PERCENT REDUCTION IN EMISSIONS	No VE because restest didn't require.
GOLDEN ALUMINUM EXTRUSION - PLANT CITY,	0570249	GOLDEN ALUMINUM EXTRUSION PLANT CITY, LL	SWHI	HILLSBOROUGH	A	Y	11	VERTICAL PAINT LINE	A	VOC	12/18/2003	98.39	PERCENT REDUCTION IN EMISSIONS	Paint usage 438.3 lbs/hr; avg combustion temp 1525 F; 23756 ACFM to RTO inlet.
GOLDEN ALUMINUM EXTRUSION - PLANT CITY,	0570249	GOLDEN ALUMINUM EXTRUSION PLANT CITY, LL	SWHI	HILLSBOROUGH	A	Y	11	VERTICAL PAINT LINE	A	VOC	10/16/2003	89.51	PERCENT REDUCTION IN EMISSIONS	
GOLDEN ALUMINUM EXTRUSION - PLANT CITY,	0570249	GOLDEN ALUMINUM EXTRUSION PLANT CITY, LL	SWHI	HILLSBOROUGH	A	Y	11	VERTICAL PAINT LINE	A	VOC	11/18/2004	98.56	PERCENT REDUCTION IN EMISSIONS	Avg paint usage 476lbs/hr, combustion temp. 1 F & 23544 acfm to RTO inlet.
GOLDEN ALUMINUM EXTRUSION - PLANT CITY,	0570249	GOLDEN ALUMINUM EXTRUSION PLANT CITY, LL	SWHI	HILLSBOROUGH	A	Y	11	VERTICAL PAINT LINE	A	VOC	11/18/2004	69.7	PERCENT REDUCTION IN EMISSIONS	Capture Efficiency Test
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H021	7/9/2007	0.0337	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	atc
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H021	7/10/2003	0.032	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc; actual is bdl and < 0.0 entered as 0.032.
													MICROGRAMS	

HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H021	7/10/2004	0.031	PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar. Results actually reported as <0.031 ug/dscm.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H021	7/10/2006	0.0311	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H021	7/18/2005	0.0301	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H021	7/19/2006	0.0311	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H021	7/14/2005	0.03101	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Below detection limit.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H021	7/9/2007	0.03	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	7/10/2003	94.2	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	7/10/2004	88.8	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	7/10/2003	99.3	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H021	7/10/2004	0.033	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar. Results actually reported as <0.033 ug/dscm.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H021	7/10/2006	0.0318	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H021	7/18/2005	0.0315	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H021	7/12/2006	0.0318	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H021	3/17/2005	0.0315	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Below detection limit.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H021	7/9/2007	0.0313	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H021	7/8/2003	0.032	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc; note actual bdl and < entered as 0.032
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H021	7/10/2003	0.032	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar. Results actually reported as <0.032 mg/dscm @ 7% O2.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H021	7/7/2004	0.031	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	7/10/2004	98.5	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	7/18/2005	99.8	PERCENT REDUCTION IN EMISSIONS	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	7/10/2003	97	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	7/10/2004	97.8	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	7/18/2005	95.6	PERCENT REDUCTION IN EMISSIONS	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	7/10/2003	96.7	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	7/10/2004	97.5	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	7/18/2005	97.2	PERCENT REDUCTION IN EMISSIONS	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	7/10/2003	90.2	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	7/10/2004	88.4	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	7/18/2005	85.2	PERCENT REDUCTION IN EMISSIONS	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H021	7/10/2003	0.032	MICROGRAMS PER DRY STANDARD CUBIC METER	Test team: Testar. Results actually reported as <0.032 mg/dscm @ 7% O2.

													@ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H021	7/11/2006	0.0319	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H021	7/10/2006	0.0319	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H021	7/10/2004	0.032	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar. Results actually reported as <0.032 ug/dscm.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H021	7/6/2004	0.032	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	7/10/2003	97.2	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	7/10/2004	97.6	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	7/18/2005	97.2	PERCENT REDUCTION IN EMISSIONS	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H021	7/9/2003	0.032	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc; note actual bdl < 0.03 entered as 0.032
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H021	7/10/2003	0.032	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar. Results actually reported as <0.032 mg/dscm @ 7% O2.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H021	7/8/2004	0.033	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H021	7/18/2005	0.0302	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H021	7/12/2005	0.0302	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Below detection limit.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PM	7/7/2003	2.06	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PM	7/9/2007	0.164	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	FL	7/11/2005	0.114	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Below detection limit.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	FL	7/20/2006	0.113	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	FL	7/18/2005	0.114	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	FL	7/10/2006	0.113	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	FL	7/10/2004	0.119	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar. Results actually reported as <0.119 mg/dscm.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	FL	7/7/2004	0.119	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	FL	7/10/2003	0.127	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar. Results actually reported as <0.127 mg/dscm @ 7% O2.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	FL	7/9/2003	0.127	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc; note that actual is bdl < 0.127 entered as 0.127
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	7/9/2007	0.0598	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	7/11/2005	1.13	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	7/10/2006	0.87	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
													MILLIGRAMS	

HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	7/18/2005	1.13	PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	7/10/2006	0.87	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	7/10/2004	2.48	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	7/10/2003	0.31	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	7/7/2003	0.31	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	FL	7/9/2007	0.12	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	FL	7/14/2005	0.086	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	DIOX	6/7/2004	11.2	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	DIOX	7/10/2004	11.2	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	DIOX	7/10/2006	21.5	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	DIOX	7/18/2005	22.5	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	DIOX	7/11/2006	21.5	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	DIOX	7/14/2005	22.5	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	DIOX	7/9/2007	23.6	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	atc
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	DIOX	7/8/2004	23.5	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	DIOX	7/10/2004	23.5	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	DIOX	7/10/2006	23.6	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	DIOX	7/18/2005	6.05	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	DIOX	7/11/2006	23.6	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	DIOX	7/12/2005	6.05	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	DIOX	7/9/2007	6.84	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	DIOX	7/9/2003	18.5	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	DIOX	7/10/2003	16.4	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar. Result is above 15 ng/dscm, units must test next year.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	DIOX	7/7/2004	14.2	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE	0570261	HILLSBOROUGH CTY. RESOURCE	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	DIOX	7/10/2004	14.2	NANOGRAMS PER DRY STANDARD	Test team: Testar

RECOVERY FAC.		RECOVERY FAC.											CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	DIOX	7/10/2006	25.6	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	DIOX	7/18/2005	24.8	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	DIOX	7/27/2006	25.6	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	DIOX	7/18/2005	24.8	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	DIOX	7/9/2007	9.71	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PM	7/9/2007	0.632	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PM	7/11/2005	1.17	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PM	7/20/2006	0.38	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PM	7/18/2005	1.17	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PM	7/10/2006	0.38	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PM	7/10/2004	6.92	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PM	7/10/2003	0.39	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	7/9/2007	0.0119	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	atc
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	7/12/2005	0.0228	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	7/11/2006	0.0112	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	7/18/2005	0.0228	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	7/10/2006	0.0112	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	7/10/2004	0.0145	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	7/6/2004	0.014	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	7/10/2003	0.0209	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	7/10/2003	0.0209	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PB	7/9/2007	0.00665	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PB	7/14/2005	0.0033	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PB	7/19/2006	0.0036	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar

HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PB	7/18/2005	0.0033	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PB	7/10/2004	0.0138	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PB	7/7/2004	0.013	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PB	7/10/2003	0.0164	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PB	7/8/2003	0.0164	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	7/9/2007	0.693	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	FL	7/10/2006	0.269	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	FL	7/18/2005	0.123	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	FL	7/10/2006	0.269	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	FL	7/10/2004	0.13	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar. Results actually reported as <0.130 mg/dscm
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	FL	7/6/2004	0.13	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	FL	7/10/2003	0.137	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar. Actual emissions reported as <0.137 mg/dscm @ 7% O2.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	FL	7/8/2003	0.137	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc; actual is bdl and is < 0.137 .
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	FL	7/9/2007	0.153	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	7/14/2005	0.0206	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	7/19/2006	0.00666	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	7/18/2005	0.0206	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	7/10/2006	0.0666	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	7/10/2004	0.0181	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	7/7/2004	0.018	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	7/10/2003	0.00801	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	7/8/2003	0.00801	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PM	7/11/2005	3.24	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PM	7/10/2003	2.06	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH		HILLSBOROUGH CTY.						Municipal Waste Combustor					MILLIGRAMS PER DRY	

CTY. RESOURCE RECOVERY FAC.	0570261	RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	& Auxiliary burners-Unit #3	A	PM	7/10/2006	0.89	STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PM	7/18/2005	3.24	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PM	7/10/2006	0.89	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PM	7/10/2004	1.26	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	7/18/2005	99.6	PERCENT REDUCTION IN EMISSIONS	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	7/10/2003	88.9	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	7/10/2004	81.8	PERCENT REDUCTION IN EMISSIONS	Test team: Testar. Passed under mg/dscm stand
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	7/18/2005	86	PERCENT REDUCTION IN EMISSIONS	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	7/10/2003	99.9	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	7/10/2004	92.4	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	7/18/2005	100	PERCENT REDUCTION IN EMISSIONS	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	7/10/2003	99.9	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	7/10/2004	90.5	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PM	7/8/2004	0.00055	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	7/9/2007	0.000303	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PM	7/7/2003	0.000171	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	7/10/2006	0.000379	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	7/6/2004	0.001	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PM	7/7/2004	0.003	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H027	7/9/2003	0.000221	MILLIGRAMS PER CUBIC METER (AMBIENT)	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	FL	7/9/2007	0.132	MILLIGRAMS PER CUBIC METER (AMBIENT)	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	FL	7/11/2005	0.115	MILLIGRAMS PER CUBIC METER (AMBIENT)	Below detection level.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	FL	7/10/2006	0.147	MILLIGRAMS PER CUBIC METER (AMBIENT)	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	FL	7/18/2005	0.115	MILLIGRAMS PER CUBIC METER (AMBIENT)	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	FL	7/10/2006	0.147	MILLIGRAMS PER CUBIC METER (AMBIENT)	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	FL	7/10/2004	0.126	MILLIGRAMS PER CUBIC METER (AMBIENT)	Test team: Testar. Results actually reported as <0.126 mg/dscm.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	FL	7/8/2004	0.126	MILLIGRAMS PER CUBIC METER (AMBIENT)	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	FL	7/10/2003	0.13	MILLIGRAMS PER CUBIC METER (AMBIENT)	Test team: Testar. Result actually reported as < mg/dscm @ 7% O2.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	FL	7/8/2003	0.13	MILLIGRAMS PER CUBIC METER (AMBIENT)	Test done by Testar, Inc; note actual bdl and < entered as 0.130
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	7/14/2005	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	

HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	7/20/2006	0.188	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	7/18/2005	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	7/10/2006	0.188	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	7/10/2004	1.76	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	7/7/2004	1.76	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	7/10/2003	0.02	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	7/8/2003	0.02	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	NOX	7/9/2007	192	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	7/12/2005	0.166	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	7/11/2006	0.15	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	7/18/2005	0.166	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	7/10/2006	0.15	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	7/10/2004	1.34	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	7/6/2004	1.34	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	7/10/2003	0.01	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	7/10/2003	0.01	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	7/9/2007	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	CO	7/11/2006	9.9	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	CO	7/10/2006	9.9	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	CO	7/10/2004	12.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	CO	7/6/2004	12.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test performed by Covanta Hillsborough, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	CO	7/11/2005	10.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	CO	7/10/2003	11.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	CO	7/10/2003	11.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	7/9/2007	23.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	atc
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	7/12/2005	17.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	NOX	7/18/2005	183	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	NOX	7/10/2006	185	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	NOX	7/10/2004	189	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	NOX	7/7/2004	189	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	

HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	NOX	7/10/2003	179	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	NOX	7/8/2003	179	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	CO	7/9/2007	10	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar,
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	CO	7/14/2005	14.7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	CO	7/20/2006	12.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	7/10/2004	0.57	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	7/8/2004	0.57	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	7/10/2003	0.173	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	7/9/2003	0.17	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	NOX	7/9/2007	177	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	NOX	7/12/2005	186	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	NOX	7/11/2006	181	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	NOX	7/18/2005	186	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	NOX	7/10/2006	181	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	7/8/2004	15.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	7/10/2003	21.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	7/9/2003	21.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	7/9/2007	17.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	7/14/2005	25.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	7/19/2006	9.64	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	7/18/2005	25.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	7/10/2006	9.64	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	7/10/2004	12.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PB	7/9/2007	0.00372	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PB	7/12/2005	0.00428	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PB	7/11/2006	0.00165	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PB	7/18/2005	0.00428	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PB	7/10/2004	0.00509	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE	0570261	HILLSBOROUGH CTY. RESOURCE	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PB	7/6/2004	0.005	MILLIGRAMS PER DRY STANDARD	

RECOVERY FAC.		RECOVERY FAC.											CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PB	7/10/2003	0.0036	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PB	7/10/2003	0.0036	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H027	7/9/2007	0.00121	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H027	7/14/2005	0.0003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H027	7/19/2006	0.000346	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H027	7/18/2005	0.0003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H027	7/10/2006	0.000346	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H027	7/10/2004	0.00141	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H027	7/7/2004	0.001	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H027	7/10/2003	0.000538	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H027	7/8/2003	0.000538	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PB	7/9/2007	0.000125	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PB	7/13/2005	0.00169	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PB	7/12/2006	0.00182	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PB	7/18/2005	0.00169	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PB	7/10/2004	0.00395	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PB	7/8/2004	0.00395	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PB	7/10/2003	0.00698	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PB	7/9/2003	0.00698	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	7/9/2007	0.017	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	7/13/2005	0.0179	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	7/12/2006	0.0181	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	7/18/2005	0.0179	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	7/10/2006	0.0181	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar

HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	7/10/2004	0.0189	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	7/8/2004	0.018	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	7/10/2003	0.0141	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	7/9/2003	0.0141	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H027	7/9/2007	0.000763	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	atc
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H027	7/12/2005	0.00053	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H027	7/11/2006	0.00018	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H027	7/18/2005	0.00053	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H027	7/10/2006	0.00018	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H027	7/10/2004	0.00029	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H027	7/6/2004	0.00029	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H027	7/10/2003	0.000221	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H027	7/10/2003	0.000221	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	CO	7/9/2007	6.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar, charging rate 33,360 lbs/hr
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	CO	7/13/2005	12.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	CO	7/12/2006	11.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	CO	7/18/2005	12.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	CO	7/10/2006	11.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	CO	7/10/2004	18	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	CO	7/8/2004	18	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	CO	7/10/2003	13	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	CO	7/9/2003	13	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	7/9/2007	18.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	7/13/2005	19.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	7/12/2006	16.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	7/18/2005	19.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	7/10/2006	16.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar

HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	7/10/2004	15.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	7/7/2004	12.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	7/10/2003	16.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	7/8/2003	16.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	7/9/2007	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	7/13/2005	0.113	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	7/12/2006	0.198	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	7/18/2005	0.113	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	7/10/2006	0.198	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	NOX	7/10/2004	182	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	NOX	7/6/2004	185	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	NOX	7/10/2003	183	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	NOX	7/10/2003	183	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test done by Testar, Inc; note - test method is v entry as system does not allow anything else tha so2 removal.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	7/18/2005	82.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	NOX	7/9/2007	182	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	NOX	7/14/2005	183	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	NOX	7/20/2006	185	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	CO	7/18/2005	14.7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	CO	7/10/2006	12.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	CO	7/10/2004	12.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	CO	7/7/2004	12.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	CO	7/10/2003	17	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	CO	7/8/2003	17	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	CO	7/9/2007	8.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	atc 156 heat input, 30,328 charging
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	CO	7/12/2005	10.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	7/11/2006	18.9	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	7/18/2005	17.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	7/10/2006	18.9	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	7/10/2004	14.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	7/6/2004	14.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	

HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	7/10/2003	14.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	7/10/2003	14.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	7/9/2007	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	NOX	7/13/2005	189	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	NOX	7/12/2006	179	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	NOX	7/18/2005	189	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	NOX	7/10/2006	179	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	NOX	7/10/2004	185	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	NOX	7/8/2004	185	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	NOX	7/10/2003	179	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	NOX	7/9/2003	179	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test done by Testar, Inc.
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H027	7/9/2007	0.000254	MILLIGRAMS PER CUBIC METER (AMBIENT)	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H027	7/13/2005	0.00022	MILLIGRAMS PER CUBIC METER (AMBIENT)	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H027	7/12/2006	0.000228	MILLIGRAMS PER CUBIC METER (AMBIENT)	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H027	7/18/2005	0.00022	MILLIGRAMS PER CUBIC METER (AMBIENT)	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H027	7/10/2006	0.000228	MILLIGRAMS PER CUBIC METER (AMBIENT)	testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H027	7/10/2004	0.00058	MILLIGRAMS PER CUBIC METER (AMBIENT)	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H027	7/8/2004	0.00058	MILLIGRAMS PER CUBIC METER (AMBIENT)	
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H027	7/10/2003	0.000221	MILLIGRAMS PER CUBIC METER (AMBIENT)	Test team: Testar
HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	0570261	HILLSBOROUGH CTY. RESOURCE RECOVERY FAC.	SWD	HILLSBOROUGH	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PM	7/9/2007	0.000276	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	testar
TAMPA BAY SHIPBUILDING & REPAIR COMPANY	0570286	TAMPA BAY SHIPBUILDING & REPAIR COMPANY	SWHI	HILLSBOROUGH	A	Y	102	Blasting/Coating Booth	A	PM	3/8/2007	0.0047	GRAINS PER DRY STANDARD CUBIC FOOT	Process rate = 2 nozzles, compressed air rangin from 122 to 134 psi, and 4791 lbs/hr steel shot
CORY PACKAGING, INC DBA MASTER PACKAGING	0570293	CORY PACKAGING, INC DBA MASTER PACKAGING	SWHI	HILLSBOROUGH	A	Y	1	FLEXOGRAPHIC PRINTING FACILITY: PRESSES	A	VOC	12/18/2007	91.1	PERCENT REDUCTION IN EMISSIONS	Run 1 @ 91.2, Run 2 @ 91.3 and Run3 @ 90.6 Total flow @ 8408 dscfm (23000 permitted). R discarded for calibration exceedance of the 3% span required by Method.
CORY PACKAGING, INC DBA MASTER PACKAGING	0570293	CORY PACKAGING, INC DBA MASTER PACKAGING	SWHI	HILLSBOROUGH	A	Y	1	FLEXOGRAPHIC PRINTING FACILITY: PRESSES	A	VOC	12/29/2006	87.1	PERCENT REDUCTION IN EMISSIONS	3 test runs resulted an average 87.1% - (88.4%, 87.1%, 85.8%)
CORY PACKAGING, INC DBA MASTER PACKAGING	0570293	CORY PACKAGING, INC DBA MASTER PACKAGING	SWHI	HILLSBOROUGH	A	Y	1	FLEXOGRAPHIC PRINTING FACILITY: PRESSES	A	VOC	12/8/2004	156.6	POUNDS/HOUR	Destruction Efficiency = 94.71%.
CORY PACKAGING, INC DBA MASTER PACKAGING	0570293	CORY PACKAGING, INC DBA MASTER PACKAGING	SWHI	HILLSBOROUGH	A	Y	1	FLEXOGRAPHIC PRINTING FACILITY: PRESSES	A	VOC	9/10/2003	405	POUNDS/HOUR	Destruction Efficiency @ 90.04%.
CORY PACKAGING, INC DBA MASTER PACKAGING	0570293	CORY PACKAGING, INC DBA MASTER PACKAGING	SWHI	HILLSBOROUGH	A	Y	1	FLEXOGRAPHIC PRINTING FACILITY: PRESSES	A	VOC	12/12/2006	76.1	PERCENT REDUCTION IN EMISSIONS	Actual Press #2 CE requirement = 70%
CORY PACKAGING, INC DBA MASTER PACKAGING	0570293	CORY PACKAGING, INC DBA MASTER PACKAGING	SWHI	HILLSBOROUGH	A	Y	1	FLEXOGRAPHIC PRINTING FACILITY: PRESSES	A	VOC	12/13/2006	97.6	PERCENT REDUCTION IN EMISSIONS	
CORY PACKAGING, INC DBA MASTER PACKAGING	0570293	CORY PACKAGING, INC DBA MASTER PACKAGING	SWHI	HILLSBOROUGH	A	Y	1	FLEXOGRAPHIC PRINTING FACILITY: PRESSES	A	VOC	12/12/2006	93.3	PERCENT REDUCTION IN EMISSIONS	Press #8 actual CE requirement = 85%
DART CONTAINER CORPORATION OF FLORIDA	0570320	DART CONTAINER CORPORATION OF FLORIDA	SWHI	HILLSBOROUGH	A	Y	3	Boiler #1 - 21 MMBtu/hr Model CB400-500	A	VOC	8/11/2005	0.74	TONS/YEAR	
DART CONTAINER CORPORATION OF FLORIDA	0570320	DART CONTAINER CORPORATION OF FLORIDA	SWHI	HILLSBOROUGH	A	Y	6	Boiler #4 - 25.2 MMBtu/hr Model CB600-150	A	VOC	8/12/2005	1.6	TONS/YEAR	
DART CONTAINER CORPORATION OF FLORIDA	0570320	DART CONTAINER CORPORATION OF FLORIDA	SWHI	HILLSBOROUGH	A	Y	4	Polystyrene Manufacturing Facility	A	VOC	3/29/2005	2.1	TONS/YEAR	
DART CONTAINER CORPORATION OF FLORIDA	0570320	DART CONTAINER CORPORATION OF FLORIDA	SWHI	HILLSBOROUGH	A	Y	4	Polystyrene Manufacturing Facility	A	VOC	11/9/2006	0.39	TONS/YEAR	dre test= 98.8%

DART CONTAINER CORPORATION OF FLORIDA	0570320	DART CONTAINER CORPORATION OF FLORIDA	SWHI	HILLSBOROUGH	A	Y	4	Polystyrene Manufacturing Facility	A	VOC	12/9/2006	98.8	OTHER (SPECIFY IN COMMENT)	DRE 98.8%
DART CONTAINER CORPORATION OF FLORIDA	0570320	DART CONTAINER CORPORATION OF FLORIDA	SWHI	HILLSBOROUGH	A	Y	4	Polystyrene Manufacturing Facility	A	VOC	2/12/2004	98.8	OTHER (SPECIFY IN COMMENT)	DE of 98.8% for Pentane VOC from Vertruder Pre-Expanders
DART CONTAINER CORPORATION OF FLORIDA	0570320	DART CONTAINER CORPORATION OF FLORIDA	SWHI	HILLSBOROUGH	A	Y	4	Polystyrene Manufacturing Facility	A	VOC	3/29/2005	97.8	OTHER (SPECIFY IN COMMENT)	Avg. Outlet VOC Emissions Rate = 0.48 lbs/hr
DART CONTAINER CORPORATION OF FLORIDA	0570320	DART CONTAINER CORPORATION OF FLORIDA	SWHI	HILLSBOROUGH	A	Y	4	Polystyrene Manufacturing Facility	A	VOC	4/8/2003	99.7	OTHER (SPECIFY IN COMMENT)	Process rates: Vertruder- 224 lb/hr; Expander- lb/hr.
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	1	WASTEWATER TREATMENT PLANT SLUDGE DRYER TRAIN NO. 2	A	VOC	12/14/2004	2.36	POUNDS/HOUR	
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	17	Engine 1 with nominal 2.9 MW generator	A	NOX	6/20/2006	10	POUNDS/HOUR	test team TECO; average unit load of 3.0MW a HHV of 1034 Btu/scf.
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	17	Engine 1 with nominal 2.9 MW generator	A	NOX	7/22/2003	12.2	POUNDS/HOUR	Test performed by TECO Environmental Servi
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	2	WASTEWATER TREATMENT PLANT SLUDGE DRYER TRAIN NO. 3	A	H114	4/16/2003	93	GRAMS/DAY (24 HOURS)	
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	1	WASTEWATER TREATMENT PLANT SLUDGE DRYER TRAIN NO. 2	A	H114	12/14/2004	331	GRAMS/DAY (24 HOURS)	
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	17	Engine 1 with nominal 2.9 MW generator	A	VOC	7/14/2006	3.511	POUNDS/HOUR	TECO Environmental Services.
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	2	WASTEWATER TREATMENT PLANT SLUDGE DRYER TRAIN NO. 3	A	VOC	4/16/2003	1.29	POUNDS/HOUR	VOC destruction Efficiency at 96.26%.
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	18	Engine 2 with nominal 2.9 MW generator	A	VOC	7/12/2006	1.8	POUNDS/HOUR	test done by TECO Environmental Services
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	17	Engine 1 with nominal 2.9 MW generator	A	NOX	6/6/2005	11.7	POUNDS/HOUR	Test performed TECO environmental Services
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	17	Engine 1 with nominal 2.9 MW generator	A	NOX	8/14/2007	10.572	POUNDS/HOUR	TECO EHS Air Services conducted the test.
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	2	WASTEWATER TREATMENT PLANT SLUDGE DRYER TRAIN NO. 3	A	PM	4/16/2003	0.0043	GRAINS PER DRY STANDARD CUBIC FOOT	
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	1	WASTEWATER TREATMENT PLANT SLUDGE DRYER TRAIN NO. 2	A	PM	12/14/2004	0.002	GRAINS PER DRY STANDARD CUBIC FOOT	
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	17	Engine 1 with nominal 2.9 MW generator	A	CO	8/14/2007	10.72	POUNDS/HOUR	TECO EHS Air Services Group conducted the testing.
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	17	Engine 1 with nominal 2.9 MW generator	A	CO	7/22/2003	10.7	POUNDS/HOUR	Test performed by TECO Environmental Servi
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	18	Engine 2 with nominal 2.9 MW generator	A	NOX	6/20/2006	10.1	POUNDS/HOUR	test team TECO; at unit load 3.0MW and HHv 1034 Btu/scf.
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	18	Engine 2 with nominal 2.9 MW generator	A	NOX	7/22/2003	12.7	POUNDS/HOUR	Test performed by TECO Environmental Servi
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	18	Engine 2 with nominal 2.9 MW generator	A	CO	7/22/2003	10.7	POUNDS/HOUR	Test performed by TECO Environmental Servi
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	18	Engine 2 with nominal 2.9 MW generator	A	CO	7/12/2006	12.1	POUNDS/HOUR	Unit burned less than 400 hours for FY 07.
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	18	Engine 2 with nominal 2.9 MW generator	A	CO	6/20/2006	12.3	POUNDS/HOUR	test team TECO; at unit load 3.0MW and HHv 1034 Btu/scf.
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	18	Engine 2 with nominal 2.9 MW generator	A	CO	12/22/2004	12	POUNDS/HOUR	TEST PERFORMED BY TECO ENVIRONMENTAL SERVICES
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	18	Engine 2 with nominal 2.9 MW generator	A	NOX	7/12/2006	8.8	POUNDS/HOUR	Unit operated less than 400 hours for FY 07.
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	18	Engine 2 with nominal 2.9 MW generator	A	NOX	12/22/2004	11.3	POUNDS/HOUR	Test performed by TECO Environmental Servi
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	17	Engine 1 with nominal 2.9 MW generator	A	CO	6/20/2006	11.3	POUNDS/HOUR	test team TECO; average unit load of 3.0MW a HHV of 1034 Btu/scf.
CITY OF TAMPA-WASTEWATER DEPT.	0570373	HOWARD F. CURREN AWT PLANT	SWHI	HILLSBOROUGH	A	Y	17	Engine 1 with nominal 2.9 MW generator	A	CO	6/6/2005	11.5	POUNDS/HOUR	Test performed by TECO Environmental Servi
OCEAN SPRAY CRANBERRIES	0610021	OCEAN SPRAY CRANBERRIES/VERO BEACH	CD	INDIAN RIVER	A	Y	5	Pellet Cooler	A	PM	11/25/2003	1.57	POUNDS/HOUR	test team = Bottorf
OCEAN SPRAY CRANBERRIES	0610021	OCEAN SPRAY CRANBERRIES/VERO BEACH	CD	INDIAN RIVER	A	Y	5	Pellet Cooler	A	PM10	10/18/2003	2.24	POUNDS/HOUR	
OCEAN SPRAY CRANBERRIES	0610021	OCEAN SPRAY CRANBERRIES/VERO BEACH	CD	INDIAN RIVER	A	Y	6	Citrus Peel Dryer #2	A	PM10	10/18/2003	2.24	POUNDS/HOUR	
OCEAN SPRAY CRANBERRIES	0610021	OCEAN SPRAY CRANBERRIES/VERO BEACH	CD	INDIAN RIVER	A	Y	4	CITRUS PEEL DRYER #1	A	PM	11/19/2003	6.57	POUNDS/HOUR	test team = Bottorf
OCEAN SPRAY CRANBERRIES	0610021	OCEAN SPRAY CRANBERRIES/VERO BEACH	CD	INDIAN RIVER	A	Y	6	Citrus Peel Dryer #2	A	PM	11/21/2003	3.41	POUNDS/HOUR	test team = Bottorf
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	5	Combined Cycle Gas Turbine Unit 5 (Phase II Acid Rain Unit)	A	NOX	7/26/2007	7.97	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	5	Combined Cycle Gas Turbine Unit 5 (Phase II Acid Rain Unit)	A	NOX	8/31/2006	5.89	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	5	Combined Cycle Gas Turbine Unit 5 (Phase II Acid Rain Unit)	A	NOX	7/14/2004	7.44	PARTS PER MILLION DRY GAS VOLUME	

													@ 15% O2	
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	5	Combined Cycle Gas Turbine Unit 5 (Phase II Acid Rain Unit)	A	NOX	7/21/2005	7.27	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	5	Combined Cycle Gas Turbine Unit 5 (Phase II Acid Rain Unit)	A	NOX	7/8/2003	6.48	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	5	Combined Cycle Gas Turbine Unit 5 (Phase II Acid Rain Unit)	A	NOX	8/31/2006	5.89	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	4	Fossil Fuel Steam Generator Unit 4 (Phase II Acid Rain Unit)	A	NOX	7/25/2007	0.163	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	4	Fossil Fuel Steam Generator Unit 4 (Phase II Acid Rain Unit)	A	NOX	7/8/2003	0.122	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	4	Fossil Fuel Steam Generator Unit 4 (Phase II Acid Rain Unit)	A	NOX	7/8/2003	0.122	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	4	Fossil Fuel Steam Generator Unit 4 (Phase II Acid Rain Unit)	A	NOX	7/20/2005	0.107	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	4	Fossil Fuel Steam Generator Unit 4 (Phase II Acid Rain Unit)	A	NOX	9/1/2006	0.16	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	4	Fossil Fuel Steam Generator Unit 4 (Phase II Acid Rain Unit)	A	NOX	9/1/2006	0.16	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	4	Fossil Fuel Steam Generator Unit 4 (Phase II Acid Rain Unit)	A	NOX	7/20/2005	0.107	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	4	Fossil Fuel Steam Generator Unit 4 (Phase II Acid Rain Unit)	A	NOX	7/13/2004	0.115	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	5	Combined Cycle Gas Turbine Unit 5 (Phase II Acid Rain Unit)	A	CO	7/14/2004	0	POUNDS PER MILLION BTU HEAT INPUT	No Co test required
CITY OF VERO BEACH	0610029	CITY OF VERO BEACH MUNICIPAL UTILITIES	CD	INDIAN RIVER	A	Y	5	Combined Cycle Gas Turbine Unit 5 (Phase II Acid Rain Unit)	A	PM	7/26/2007	0.0043	POUNDS PER MILLION BTU HEAT INPUT	
MACHO PRODUCTS, INC.	0610064	MACHO PRODUCTS, INC.	CD	INDIAN RIVER	I	Y	1	Protective Equipment Manufacturing Plant	I	VOC	11/2/2006	15.6	POUNDS/HOUR	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	PM	8/14/2007	0.011	POUNDS PER MILLION BTU HEAT INPUT	Steady state
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	PM	8/15/2006	0.017	POUNDS PER MILLION BTU HEAT INPUT	soot blowing
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	PM	8/10/2004	0.0103	POUNDS PER MILLION BTU HEAT INPUT	Steady state conditions
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	PM	8/10/2004	0.0195	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	PM	8/18/2005	0.018	POUNDS PER MILLION BTU HEAT INPUT	Steady State
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	PM	8/17/2005	0.018	POUNDS PER MILLION BTU HEAT INPUT	Soot Blow
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	PM	8/16/2006	0.0092	POUNDS PER MILLION BTU HEAT INPUT	Steady state
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	PM	8/15/2006	0.017	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	PM	9/3/2003	0.0676	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	PM	9/2/2003	0.076	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	PM	9/2/2003	0.076	POUNDS PER MILLION BTU HEAT INPUT	Soot Blow
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	PM	9/3/2003	0.068	POUNDS PER MILLION BTU HEAT INPUT	Steady state.
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	PM	8/17/2004	0.0058	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	PM	8/16/2004	0.0112	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	PM	8/24/2005	0.018	POUNDS PER MILLION BTU HEAT INPUT	Steady State
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	PM	8/23/2005	0.023	POUNDS PER MILLION BTU HEAT INPUT	Soot Blow
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	PM	8/15/2006	0.019	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	PM	8/15/2006	0.028	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	PM	9/9/2003	0.0192	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	PM	9/8/2003	0.0396	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	PM	9/8/2003	0.039	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	PM	9/9/2003	0.019	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	PM	8/14/2007	0.027	POUNDS PER MILLION BTU HEAT INPUT	Tested at 106% of permitted rate; steady state
													POUNDS PER	

GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	PM	8/14/2007	0.02	MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	PM	8/14/2007	0.02	POUNDS PER MILLION BTU HEAT INPUT	soot blowing
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	SO2	8/17/2004	1.43	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	SO2	8/18/2005	1.14	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	SO2	8/18/2006	1.2	POUNDS PER MILLION BTU HEAT INPUT	UNITS 1 & 2 SHARE A COMMON STACK. SPLIT THE EMISSIONS BETWEEN THE TV SO THEY WOULD NOT BE DOUBLE COUNTED.
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	SO2	9/9/2003	1.17	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	2	Boiler #2 (Phase I & II Acid Rain Unit)	A	SO2	8/14/2007	1.851	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	SO2	8/11/2004	1.413	POUNDS PER MILLION BTU HEAT INPUT	Method 7E. Calibration error, bias & drift are C
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	SO2	8/17/2005	1.49	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	SO2	9/11/2003	1.145	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	SO2	6/18/2006	1.2	POUNDS PER MILLION BTU HEAT INPUT	NOTE: 1 & 2 SHARE A COMMON STACK. SPLIT THE EMISSIONS BETWEEN EACH U TO PREVENT DOUBLE COUNTING.
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	SO2	9/11/2003	1.145	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	SO2	8/14/2007	1.851	POUNDS PER MILLION BTU HEAT INPUT	
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	PM	8/16/2006	0.0092	POUNDS PER MILLION BTU HEAT INPUT	Steady state
GULF POWER COMPANY	0630014	SCHOLZ ELECTRIC GENERATING PLANT	NWDP	JACKSON	A	Y	1	Boiler #1 (Phase I & II Acid Rain Unit)	A	PM	8/14/2007	0.018	POUNDS PER MILLION BTU HEAT INPUT	Soot blowing
SPANISH TRAIL LUMBER CO., LLC	0630028	MARIANNA SAWMILL	NWDP	JACKSON	A	Y	6	Lumber Drying Kilns 2, 3 and 4	A	PM	12/20/2007	0.023	POUNDS PER MILLION BTU HEAT INPUT	Environmental Monitoring Laboratories, Inc conducted the stack test
SPANISH TRAIL LUMBER CO., LLC	0630028	MARIANNA SAWMILL	NWDP	JACKSON	A	Y	6	Lumber Drying Kilns 2, 3 and 4	A	PM	8/2/2007	0.041	POUNDS PER MILLION BTU HEAT INPUT	
SPANISH TRAIL LUMBER CO., LLC	0630028	MARIANNA SAWMILL	NWDP	JACKSON	A	Y	6	Lumber Drying Kilns 2, 3 and 4	A	PM	1/10/2006	0.056	POUNDS PER MILLION BTU HEAT INPUT	Average heat input was 26.2 MMBTU/HR. Lin to 28.6 until retested.
SPANISH TRAIL LUMBER CO., LLC	0630028	MARIANNA SAWMILL	NWDP	JACKSON	A	Y	6	Lumber Drying Kilns 2, 3 and 4	A	PM	9/24/2004	0.0328	POUNDS PER MILLION BTU HEAT INPUT	Only one kiln built, #2. Heat input is 35 MMBt per kiln. The 105 rate relates to all three togeth
SPANISH TRAIL LUMBER CO., LLC	0630028	MARIANNA SAWMILL	NWDP	JACKSON	A	Y	6	Lumber Drying Kilns 2, 3 and 4	A	PM	7/27/2006	0.04	POUNDS PER MILLION BTU HEAT INPUT	Limited to 29.5 MMBtu/hr until retested.
WASTE MANAGEMENT OF LEON COUNTY, INC	0630045	SPRINGHILL REGIONAL LANDFILL	NWDP	JACKSON	A	Y	5	Landfill Gas Treatment/Electric Generation Plant	A	CO	5/18/2006	1.84	POUNDS/HOUR	
WASTE MANAGEMENT OF LEON COUNTY, INC	0630045	SPRINGHILL REGIONAL LANDFILL	NWDP	JACKSON	A	Y	5	Landfill Gas Treatment/Electric Generation Plant	A	CO	5/17/2006	2.54	POUNDS/HOUR	
WASTE MANAGEMENT OF LEON COUNTY, INC	0630045	SPRINGHILL REGIONAL LANDFILL	NWDP	JACKSON	A	Y	5	Landfill Gas Treatment/Electric Generation Plant	A	CO	5/16/2006	1.99	POUNDS/HOUR	Test Co.: RMC ENVIRONMENTAL
WASTE MANAGEMENT OF LEON COUNTY, INC	0630045	SPRINGHILL REGIONAL LANDFILL	NWDP	JACKSON	A	Y	5	Landfill Gas Treatment/Electric Generation Plant	A	CO	5/17/2006	2.31	POUNDS/HOUR	
WASTE MANAGEMENT OF LEON COUNTY, INC	0630045	SPRINGHILL REGIONAL LANDFILL	NWDP	JACKSON	A	Y	5	Landfill Gas Treatment/Electric Generation Plant	A	CO	5/16/2006	1.82	POUNDS/HOUR	
WASTE MANAGEMENT OF LEON COUNTY, INC	0630045	SPRINGHILL REGIONAL LANDFILL	NWDP	JACKSON	A	Y	5	Landfill Gas Treatment/Electric Generation Plant	A	CO	5/18/2006	1.92	POUNDS/HOUR	
SI GROUP-ENERGY, LLC	0650001	MONTICELLO PLANT	NWDT	JEFFERSON	A	Y	1	CARBONACEOUS FUEL BOILER	C	CO	10/4/2007	123.3	POUNDS/HOUR	limit of 100 is a 30-day rolling average.
SI GROUP-ENERGY, LLC	0650001	MONTICELLO PLANT	NWDT	JEFFERSON	A	Y	1	CARBONACEOUS FUEL BOILER	C	CO	7/15/2005	90	POUNDS/HOUR	
SI GROUP-ENERGY, LLC	0650001	MONTICELLO PLANT	NWDT	JEFFERSON	A	Y	1	CARBONACEOUS FUEL BOILER	C	PM	10/4/2007	0.16	POUNDS PER MILLION BTU HEAT INPUT	
SI GROUP-ENERGY, LLC	0650001	MONTICELLO PLANT	NWDT	JEFFERSON	A	Y	1	CARBONACEOUS FUEL BOILER	C	PM	7/15/2005	0.112	POUNDS PER MILLION BTU HEAT INPUT	
CUTRALE CITRUS JUICES USA INC	0690002	CUTRALE CITRUS JUICES USA - LEESBURG	CD	LAKE	A	Y	6	PELLET COOLING REEL	A	PM	2/10/2004	0.37	POUNDS/HOUR	
CUTRALE CITRUS JUICES USA INC	0690002	CUTRALE CITRUS JUICES USA - LEESBURG	CD	LAKE	A	Y	5	CITRUS PEEL DRYER	A	PM	2/11/2004	11.7	POUNDS/HOUR	
CUTRALE CITRUS JUICES USA INC	0690002	CUTRALE CITRUS JUICES USA - LEESBURG	CD	LAKE	A	Y	7	COGENERATION SYSTEM FOR TURBINE & STEAM GENERATOR	A	NOX	1/13/2003	36.29	PARTS PER MILLION DRY GAS VOLUME	
CUTRALE CITRUS JUICES USA INC	0690002	CUTRALE CITRUS JUICES USA - LEESBURG	CD	LAKE	A	Y	7	COGENERATION SYSTEM FOR TURBINE & STEAM GENERATOR	A	NOX	2/9/2004	49.59	PARTS PER MILLION DRY GAS VOLUME	
CUTRALE CITRUS JUICES USA INC	0690002	CUTRALE CITRUS JUICES USA - LEESBURG	CD	LAKE	A	Y	5	CITRUS PEEL DRYER	A	PM	1/21/2003	11.2	POUNDS/HOUR	
EAGLE-PICHER IND. WOLVERINE ADVANCED MAT	0690008	WOLVERINE ADVANCED MATERIALS	CD	LAKE	A	Y	1	Coil Coater	A	VOC	12/9/2004	1.29	POUNDS/HOUR	
EAGLE-PICHER IND. WOLVERINE ADVANCED MAT	0690008	WOLVERINE ADVANCED MATERIALS	CD	LAKE	A	Y	2	Hylene Parts Drying Line (fka Butyl Dip Coating Line)	A	VOC	12/20/2006	0.231	POUNDS/HOUR	
EAGLE-PICHER IND. WOLVERINE ADVANCED MAT	0690008	WOLVERINE ADVANCED MATERIALS	CD	LAKE	A	Y	3	Hylene Dip Coating Line	A	VOC	12/20/2006	0.02	POUNDS/HOUR	
SILVER SPRINGS CITRUS INC.	0690014	SILVER SPRINGS CITRUS PLANT	CD	LAKE	A	Y	1	CITRUS PEEL DRYER W/WASTE HEAT EVAPORATOR	A	PM	3/21/2006	3.26	POUNDS/HOUR	

SILVER SPRINGS CITRUS INC.	0690014	SILVER SPRINGS CITRUS PLANT	CD	LAKE	A	Y	1	CITRUS PEEL DRYER W/WASTE HEAT EVAPORATOR	A	PM	2/4/2004	3.15	POUNDS/HOUR	
SILVER SPRINGS CITRUS INC.	0690014	SILVER SPRINGS CITRUS PLANT	CD	LAKE	A	Y	1	CITRUS PEEL DRYER W/WASTE HEAT EVAPORATOR	A	PM	1/25/2005	3.17	POUNDS/HOUR	Allowable is 15 lb/hr
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H114	1/29/2007	97.1	PERCENT REDUCTION IN EMISSIONS	TESTAR
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H114	1/10/2005	85.9	PERCENT REDUCTION IN EMISSIONS	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H114	1/15/2004	97.87	PERCENT REDUCTION IN EMISSIONS	Testing conductd by TESTAR, Inc., Audit sam passed
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H114	1/16/2003	2.1	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test Team TESTAR, Audit Sample passed
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H114	1/16/2003	98	PERCENT REDUCTION IN EMISSIONS	
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	SO2	1/19/2006	92.3	PERCENT REDUCTION IN EMISSIONS	TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H114	1/16/2003	96	PERCENT REDUCTION IN EMISSIONS	Test Team: TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H114	1/16/2003	4	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test Team: TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H114	1/15/2004	4.02	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testing conductd by TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H114	1/15/2004	95	PERCENT REDUCTION IN EMISSIONS	Testing conductd by TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H114	1/10/2005	96.2	PERCENT REDUCTION IN EMISSIONS	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H114	1/10/2005	3.48	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H114	1/19/2006	2.34	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	TESTAR, Inc., Audit samples passed, Removal efficiency 95.5%
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H114	1/19/2006	95.5	PERCENT REDUCTION IN EMISSIONS	TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	3	ACTIVATED CARBON STORAGE SILO	A	PM	1/10/2005	0.1	POUNDS/HOUR	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	SO2	1/15/2004	95.2	PERCENT REDUCTION IN EMISSIONS	Testing conductd by TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	SO2	1/19/2006	95.8	PERCENT REDUCTION IN EMISSIONS	TESTAR, Inc
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H106	1/16/2003	99	PERCENT REDUCTION IN EMISSIONS	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H106	1/15/2004	99.5	PERCENT REDUCTION IN EMISSIONS	Testing conductd by TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H106	1/16/2006	99.2	PERCENT REDUCTION IN EMISSIONS	TESTAR, Inc. Audit sample passed
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	SO2	1/15/2004	93.1	PERCENT REDUCTION IN EMISSIONS	Testing conductd by TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H114	1/15/2004	4.367	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testing conductd by TESTAR, Inc. Audit samp passed
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H114	1/10/2005	12.1	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H114	1/19/2006	3.04	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	TESTAR Inc., Mercury removal was 95.8% , Injected carbon was analyzed for Mercury, Cadmium, and Lead.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H114	1/19/2007	9.42	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H114	1/19/2006	97.1	PERCENT REDUCTION IN EMISSIONS	TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H106	1/29/2007	97.7	PERCENT REDUCTION IN EMISSIONS	TESTAR
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H106	1/11/2005	98.2	PERCENT REDUCTION IN EMISSIONS	
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H106	1/15/2004	99.2	PERCENT REDUCTION IN EMISSIONS	Testing conductd by TESTAR, Inc. Audit samp passed.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H106	1/16/2003	99	PERCENT REDUCTION IN EMISSIONS	
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H106	1/19/2006	98.9	PERCENT REDUCTION IN EMISSIONS	TESTAR, Inc
													MILLIGRAMS	

COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	PB	1/16/2003	0.017	PER DRY STANDARD CUBIC METER @ 7% O2	Test Team TESTAR Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	PB	1/15/2004	0.00136	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testing conductd by TESTAR, Inc. Audit samp passed
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	PM	1/29/2007	16.7	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	TESTAR
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	PM	1/19/2006	4.76	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	TESTAR Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	PM	1/10/2005	2.7	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	PM	1/15/2004	2.5	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testing conductd by TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	PM	1/16/2003	3.3	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Tet Team TESTAR, INC
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	PB	1/19/2006	0.00049	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	TESTAR Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	PB	1/29/2007	0.0663	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	TESTAR
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	PB	1/10/2005	0.0112	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	DIOX	1/16/2003	1.6	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	TESTAR, Inc. After initial test on both units, te for dioxin/furan is required on one unit only
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	DIOX	1/10/2005	5.46	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	DIOX	1/19/2006	1.07	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	TESTAR Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	DIOX	1/19/2007	11.2	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	TESTAR
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	DIOX	1/15/2004	7.15	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testing conductd by TESTAR, Inc. Audit samp passed.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	DIOX	1/19/2006	0.85	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	TESTAR, Inc., Audit sample passed
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	DIOX	2/2/2008	34	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testing conducted by TESTAR
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H106	1/16/2003	5.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test Team: TESTAR Inc. Audit Sample Passed
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H106	1/15/2004	4.53	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testing conductd by TESTAR, Inc. Audit samp passed
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H106	1/19/2007	17	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	CO	1/10/2005	23	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	CO	1/15/2004	15	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testing conductd by TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	CO	1/16/2003	14	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test Team: TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H106	1/16/2006	6.29	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	TESTAR Inc., HCl removal was 98.9%
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	CO	1/19/2006	6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	SO2	1/29/2007	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	TESTAR
		LAKE COUNTY											PARTS PER	

COVANTA LAKE II, INC.	0690046	RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	SO2	1/19/2006	1	MILLION DRY GAS VOLUME @ 7% O2	TESTAR Inc, SO2 % removal was 95.8%
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	SO2	1/15/2004	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testing conductd by TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	SO2	1/16/2003	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test Team TESTAR, Inc
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	NOX	1/19/2006	179	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	TESTAR Inc
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	NOX	1/10/2005	180	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	NOX	1/15/2004	184	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testing conductd by TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	NOX	1/16/2003	185	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test Team: TESTAR, Inc
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	CO	1/29/2007	7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	TESTAR
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H027	1/15/2004	0.000285	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testing conductd by TESTAR, Inc. Audit samp passed
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H027	1/16/2003	0.0006	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test Team TESTAR, Inc. Audit sample passed
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	CO	1/29/2007	1.58	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	TESTAR
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	CO	1/19/2006	18	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	CO	1/10/2005	12	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	CO	1/15/2004	13	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testing conductd by TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	CO	1/16/2003	14	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	SO2	1/19/2006	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	SO2	1/15/2004	2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testing conductd by TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	SO2	1/16/2003	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test Team: TESTAR Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H106	1/16/2006	4.43	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	TESTAR Inc. , Audit samples passed
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H106	1/15/2004	3.84	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testing conductd by TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H106	1/16/2003	5.7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test Team TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	NOX	1/19/2006	184	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	NOX	1/10/2005	184	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	NOX	1/15/2004	187	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testing conductd by TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	NOX	1/16/2003	187	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test Team: TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	PB	1/15/2004	0.00174	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testing conductd by TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	PB	1/16/2003	0.0029	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test Team: TESTAR Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H027	1/19/2006	0.00086	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	TESTAR Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H027	1/10/2005	0.001	MILLIGRAMS PER DRY STANDARD CUBIC METER	Testar

													@ 7% O2	
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H027	1/15/2004	0.000339	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testing conductd by TESTAR, Inc. Audit samp passed
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	H027	1/16/2003	0.0003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test Team: TESTAR INC.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H027	1/19/2007	0.00951	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	TESTAR
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H027	1/19/2006	0.0006	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	TESTAR Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	1	288 TPD MSW Combustor & Auxiliary Burners-Unit 1	A	H027	1/10/2005	0.00115	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	PM	1/19/2006	5.52	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	PM	1/10/2005	3.29	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testar
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	PM	1/15/2004	1.87	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testing conductd by TESTAR, Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	PM	1/16/2003	8.5	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test Team: TESTAR Inc.
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	PB	1/19/2006	0.00839	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	TESTAR, Inc
COVANTA LAKE II, INC.	0690046	LAKE COUNTY RESOURCE RECOVERY FACILITY	CD	LAKE	A	Y	2	288 TPD MSW Combustor & Auxiliary Burners-Unit 2	A	PB	1/10/2005	0.00735	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testar
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	CO	6/20/2007	25.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	NOX	7/12/2006	24	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	NOX	6/20/2007	25	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Air Consulting and Engineering
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	NOX	12/18/2007	24.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	This is a RATA Test. Relative Accuracies for C 2.13%, for CT-2, 4.05%
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	3	Combined cycle combustion turbine w/duct burner (aka Unit 1)	A	NOX	6/10/2003	24.52	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	3	Combined cycle combustion turbine w/duct burner (aka Unit 1)	A	NOX	6/17/2004	24.22	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	3	Combined cycle combustion turbine w/duct burner (aka Unit 1)	A	NOX	11/1/2006	23.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	3	Combined cycle combustion turbine w/duct burner (aka Unit 1)	A	NOX	7/11/2006	22.67	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	3	Combined cycle combustion turbine w/duct burner (aka Unit 1)	A	NOX	6/20/2007	24.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	3	Combined cycle combustion turbine w/duct burner (aka Unit 1)	A	NOX	12/18/2007	24.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	This is a RATA Test. Relative Accuracies for C 2.13%, for CT-2, 4.05%
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	NOX	8/18/2003	24.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	NOX	6/9/2003	25	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	NOx ppm is ISO corrected
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	NOX	3/23/2005	24.65	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	NOX	7/20/2005	24	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	This test is on the lease engine
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	NOX	12/14/2004	22.64	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	This test is on a lease engine
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	NOX	6/15/2004	24.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	

LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	NOX	7/30/2004	24.84	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Value is for full load test. 4 loads were tested
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	NOX	7/30/2004	24.84	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	NOx full load test
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	NOX	7/12/2006	39.6	POUNDS/HOUR	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	NOX	3/23/2005	40.2	POUNDS/HOUR	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	3	Combined cycle combustion turbine w/duct burner (aka Unit 1)	A	CO	6/10/2003	27.09	PARTS PER MILLION DRY GAS VOLUME	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	3	Combined cycle combustion turbine w/duct burner (aka Unit 1)	A	CO	11/1/2006	21	PARTS PER MILLION DRY GAS VOLUME	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	3	Combined cycle combustion turbine w/duct burner (aka Unit 1)	A	CO	7/15/2006	8.5	PARTS PER MILLION DRY GAS VOLUME	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	3	Combined cycle combustion turbine w/duct burner (aka Unit 1)	A	CO	6/20/2007	26.7	PARTS PER MILLION DRY GAS VOLUME	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	CO	8/18/2003	27.22	PARTS PER MILLION DRY GAS VOLUME	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	CO	6/9/2003	27.3	PARTS PER MILLION DRY GAS VOLUME	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	CO	3/24/2005	19.2	PARTS PER MILLION DRY GAS VOLUME	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	CO	7/20/2005	22.75	PARTS PER MILLION DRY GAS VOLUME	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	CO	12/14/2004	26.02	PARTS PER MILLION DRY GAS VOLUME	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	CO	7/30/2004	20.75	PARTS PER MILLION DRY GAS VOLUME	Full load with duct burner
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	CO	7/12/2006	25	PARTS PER MILLION DRY GAS VOLUME	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	NOX	8/18/2003	40.27	POUNDS/HOUR	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	CO	7/20/2005	39.08	POUNDS/HOUR	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	3	Combined cycle combustion turbine w/duct burner (aka Unit 1)	A	CO	7/11/2006	29.85	POUNDS/HOUR	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	3	Combined cycle combustion turbine w/duct burner (aka Unit 1)	A	CO	6/17/2004	24.91	POUNDS/HOUR	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	3	Combined cycle combustion turbine w/duct burner (aka Unit 1)	A	NOX	11/1/2006	37.9	POUNDS/HOUR	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	3	Combined cycle combustion turbine w/duct burner (aka Unit 1)	A	NOX	7/11/2006	36.51	POUNDS/HOUR	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	3	Combined cycle combustion turbine w/duct burner (aka Unit 1)	A	CO	11/1/2006	18.83	POUNDS/HOUR	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	CO	8/18/2003	24.74	POUNDS/HOUR	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	CO	7/12/2006	22.2	POUNDS/HOUR	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	CO	3/23/2005	17.47	POUNDS/HOUR	
LAKE INVESTMENT, L.P.	0694801	LAKE COGEN C/O AQUILA	CD	LAKE	A	Y	4	Combined cycle combustion turbine w/duct burner (aka Unit 2)	A	CO	6/15/2004	24.67	POUNDS/HOUR	EU 4 is unit 2
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	4	Combustion Turbine #2	A	NOX	9/19/2006	315	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	PM	8/20/2007	5.6	POUNDS/HOUR	base load
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	PM	5/12/2003	14.3	POUNDS/HOUR	99=GE.180 MW load
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	PM	5/12/2003	0	POUNDS/HOUR	test for PM waived for this unit, sister unit,eu 2 tested.
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	PM	8/22/2007	8.8	POUNDS/HOUR	base load oil
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	PM	4/10/2003	4.76	POUNDS/HOUR	99= G.E. fired on oil.
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	PM	3/28/2003	4.9	POUNDS/HOUR	99=G.E. 180 minute test run, fired by natural g
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	4	Combustion Turbine #2	A	NOX	9/3/2003	325	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	29	100 MMBTU/HR Natural GAS HEATER #1	A	NOX	8/21/2007	0.041	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	29	100 MMBTU/HR Natural GAS HEATER #1	A	CO	8/21/2007	0.001	POUNDS PER MILLION BTU HEAT INPUT	Base Load
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	30	100 MMBTU/HR Natural GAS HEATER #2	A	NOX	4/11/2003	0.04	POUNDS PER MILLION BTU HEAT INPUT	GE Energy Service. Tested at 100% load.Only of the 2 units needed to be tested.
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	30	100 MMBTU/HR Natural GAS HEATER #2	A	CO	4/11/2003	0.001	POUNDS PER MILLION BTU HEAT INPUT	GE Energy service. Tested at 100% load
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	9	Combustion Turbine #7	A	NOX	9/5/2007	361	POUNDS/HOUR	test was reportedly sent to Ron Blackburn on da specified / I had to request copy in November
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	CO	3/28/2003	0.6	PARTS PER MILLION DRY GAS VOLUME	99= GE ,tested firing natural gas
													PARTS PER	

FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	CO	4/10/2003	0.6	MILLION DRY GAS VOLUME	99=G.E. fired on oil.
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	CO	6/28/2005	0.38	PARTS PER MILLION DRY GAS VOLUME	FPL test group
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	CO	6/22/2006	0.41	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	CO	8/17/2007	0.21	PARTS PER MILLION DRY GAS VOLUME	Base oil
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	CO	8/16/2007	0.03	PARTS PER MILLION DRY GAS VOLUME	base load
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	CO	8/16/2007	0.052	PARTS PER MILLION DRY GAS VOLUME	peak mode
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	CO	7/14/2005	0.54	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	CO	8/10/2005	0.56	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	CO	6/29/2004	1.2	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	CO	6/21/2006	0.55	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	CO	7/14/2005	0.54	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	CO	8/20/2007	0.06	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	CO	8/22/2007	0.21	PARTS PER MILLION DRY GAS VOLUME	100% oil
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	CO	8/21/2007	0.05	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	21	250MW Combined Cycle Combustion Turbine (2D)	A	CO	6/3/2003	2.77	PARTS PER MILLION DRY GAS VOLUME	FPL Test group.
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	VOC	4/28/2003	0.11	PARTS PER MILLION DRY GAS VOLUME	99=GE. 171.8 MW load
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	VOC	4/28/2003	0.15	OTHER (SPECIFY IN COMMENT)	99=GE. 179.2 Mw load
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	VOC	8/22/2007	0.72	OTHER (SPECIFY IN COMMENT)	lb/hr base on oil
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	VOC	8/21/2007	0.47	PARTS PER MILLION DRY GAS VOLUME	peek load
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	SO2	3/28/2003	0.066	OTHER (SPECIFY IN COMMENT)	99=G.E. fired on natural gas.
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	CO	4/28/2003	0.2	PARTS PER MILLION DRY GAS VOLUME	99= GE. gas firing, 171MW load
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	CO	5/12/2003	0.18	PARTS PER MILLION DRY GAS VOLUME	99=GE. oil fired, 179.2 MW load
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	22	250MW Combined Cycle Combustion Turbine (2E)	A	CO	6/3/2003	2.16	PARTS PER MILLION DRY GAS VOLUME	FPL Test Group
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	VOC	8/16/2007	0	PARTS PER MILLION DRY GAS VOLUME	base load
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	VOC	3/28/2003	0.12	PARTS PER MILLION DRY GAS VOLUME	99=G.E. tested firing natural gas.
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	VOC	8/17/2007	0	OTHER (SPECIFY IN COMMENT)	base oil
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	23	250MW Combined Cycle Combustion Turbine (2F)	A	CO	6/4/2003	1.95	PARTS PER MILLION DRY GAS VOLUME	FPL Test Group
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	9	Combustion Turbine #7	A	NOX	9/5/2007	321	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	NOX	8/16/2007	8.71	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	base load
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	NOX	8/17/2007	32.37	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	base oil
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	NOX	4/10/2003	37.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	99= G.E. fired on oil
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	NOX	3/28/2003	8.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	99= G.E. tested firing natural gas
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	18	250MW Combined Cycle Combustion Turbine (2A)	A	CO	10/4/2005	0.39	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	18	250MW Combined Cycle Combustion Turbine (2A)	A	NOX	10/29/2007	8.58	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	18	250MW Combined Cycle Combustion Turbine (2A)	A	NOX	12/4/2006	8.48	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	18	250MW Combined Cycle Combustion Turbine (2A)	A	NOX	12/2/2003	7.17	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FPl Stack Test Team
FLORIDA POWER &		FORT MYERS POWER						250MW Combined Cycle					PARTS PER MILLION DRY	

LIGHT (PFM)	0710002	PLANT	SD	LEE	A	Y	22	Combustion Turbine (2E)	A	CO	10/10/2005	0.365	GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	22	250MW Combined Cycle Combustion Turbine (2E)	A	CO	11/6/2007	0.46	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	21	250MW Combined Cycle Combustion Turbine (2D)	A	NOX	6/3/2003	8.29	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FPL Test group
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	21	250MW Combined Cycle Combustion Turbine (2D)	A	NOX	12/9/2003	8.13	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FPL Stack Test Team
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	21	250MW Combined Cycle Combustion Turbine (2D)	A	NOX	8/9/2005	10.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	21	250MW Combined Cycle Combustion Turbine (2D)	A	NOX	10/26/2004	8.56	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	21	250MW Combined Cycle Combustion Turbine (2D)	A	NOX	11/29/2006	8.63	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	21	250MW Combined Cycle Combustion Turbine (2D)	A	NOX	10/11/2005	8.16	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	21	250MW Combined Cycle Combustion Turbine (2D)	A	NOX	11/5/2007	8.25	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	VOC	4/10/2003	0.17	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	99= G.E. fired on oil
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	23	250MW Combined Cycle Combustion Turbine (2F)	A	CO	12/3/2003	1.186	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FPL Test Team
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	23	250MW Combined Cycle Combustion Turbine (2F)	A	CO	10/26/2004	1.09	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	23	250MW Combined Cycle Combustion Turbine (2F)	A	CO	11/28/2006	0.19	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	23	250MW Combined Cycle Combustion Turbine (2F)	A	CO	10/11/2005	0.44	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	23	250MW Combined Cycle Combustion Turbine (2F)	A	CO	11/7/2007	0.39	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	22	250MW Combined Cycle Combustion Turbine (2E)	A	CO	12/9/2003	1.13	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FPL Stack Test Team
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	22	250MW Combined Cycle Combustion Turbine (2E)	A	CO	10/25/2004	1.04	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	22	250MW Combined Cycle Combustion Turbine (2E)	A	CO	11/28/2006	0.26	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	NOX	4/28/2003	7.22	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	99=GE. 171.8 MW load
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	NOX	4/28/2003	36.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	99= GE. 179.2 MW load
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	NOX	7/14/2005	7.58	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	NOX	8/10/2005	10	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	NOX	6/29/2004	6.73	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	NOX	6/21/2006	8.19	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	NOX	7/14/2005	9.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	NOX	8/20/2007	9.52	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	peeking mode
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	NOX	8/22/2007	24.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	27	170 MW Simple Cycle Combustion Turbine #1 (3A)	A	NOX	8/20/2007	7.25	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	base load
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	19	250MW Combined Cycle Combustion Turbine (2B)	A	NOX	10/30/2007	8.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	23	250MW Combined Cycle Combustion Turbine (2F)	A	NOX	6/4/2003	8.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FPL Test Group
													PARTS PER	

FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	23	250MW Combined Cycle Combustion Turbine (2F)	A	NOX	12/3/2003	7.51	MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	23	250MW Combined Cycle Combustion Turbine (2F)	A	NOX	10/26/2004	8.92	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	23	250MW Combined Cycle Combustion Turbine (2F)	A	NOX	11/28/2006	8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	23	250MW Combined Cycle Combustion Turbine (2F)	A	NOX	10/11/2005	7.55	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	23	250MW Combined Cycle Combustion Turbine (2F)	A	NOX	11/7/2007	7.74	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	SO2	4/10/2003	0.04	PERCENT SULFUR IN FUEL	99= G.E. so2 % is a measured results, unit firec oil
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	21	250MW Combined Cycle Combustion Turbine (2D)	A	CO	12/9/2003	1.67	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	20	250MW Combined Cycle Combustion Turbine (2C)	A	NOX	12/3/2003	7.86	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FPL Stack Test Team
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	20	250MW Combined Cycle Combustion Turbine (2C)	A	NOX	11/27/2006	8.53	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	20	250MW Combined Cycle Combustion Turbine (2C)	A	NOX	11/10/2005	8.37	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	20	250MW Combined Cycle Combustion Turbine (2C)	A	NOX	10/31/2007	8.34	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	22	250MW Combined Cycle Combustion Turbine (2E)	A	NOX	6/3/2003	8.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FPL Test Group
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	22	250MW Combined Cycle Combustion Turbine (2E)	A	NOX	12/9/2003	7.45	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FPL Stack Test Team
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	22	250MW Combined Cycle Combustion Turbine (2E)	A	NOX	10/25/2004	8.92	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	22	250MW Combined Cycle Combustion Turbine (2E)	A	NOX	11/28/2006	8.38	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	22	250MW Combined Cycle Combustion Turbine (2E)	A	NOX	10/10/2005	8.35	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	22	250MW Combined Cycle Combustion Turbine (2E)	A	NOX	11/6/2007	8.33	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	20	250MW Combined Cycle Combustion Turbine (2C)	A	CO	12/3/2003	1.16	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	20	250MW Combined Cycle Combustion Turbine (2C)	A	CO	11/27/2006	0.13	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	20	250MW Combined Cycle Combustion Turbine (2C)	A	CO	10/5/2005	0.42	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	20	250MW Combined Cycle Combustion Turbine (2C)	A	CO	10/31/2007	0.39	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	19	250MW Combined Cycle Combustion Turbine (2B)	A	NOX	10/3/2003	8.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FPL test team
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	19	250MW Combined Cycle Combustion Turbine (2B)	A	NOX	11/21/2006	8.75	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	19	250MW Combined Cycle Combustion Turbine (2B)	A	NOX	10/4/2005	8.43	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	21	250MW Combined Cycle Combustion Turbine (2D)	A	CO	10/26/2004	1.13	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	21	250MW Combined Cycle Combustion Turbine (2D)	A	CO	11/29/2006	0.28	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	21	250MW Combined Cycle Combustion Turbine (2D)	A	CO	10/11/2005	0.41	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	21	250MW Combined Cycle Combustion Turbine (2D)	A	CO	11/5/2007	0.43	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	19	250MW Combined Cycle Combustion Turbine (2B)	A	CO	12/2/2003	1.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	19	250MW Combined Cycle Combustion Turbine (2B)	A	CO	11/21/2006	0.33	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
													PARTS PER	

FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	19	250MW Combined Cycle Combustion Turbine (2B)	A	CO	10/4/2005	0.39	MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	19	250MW Combined Cycle Combustion Turbine (2B)	A	CO	10/30/2007	0.49	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	18	250MW Combined Cycle Combustion Turbine (2A)	A	NOX	8/9/2005	9.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	18	250MW Combined Cycle Combustion Turbine (2A)	A	NOX	10/4/2005	8.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	18	250MW Combined Cycle Combustion Turbine (2A)	A	CO	12/4/2006	0.13	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	18	250MW Combined Cycle Combustion Turbine (2A)	A	CO	10/29/2007	0.35	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	NOX	6/28/2005	6.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	gas fired
FLORIDA POWER & LIGHT (PFM)	0710002	FORT MYERS POWER PLANT	SD	LEE	A	Y	28	170 MW Simple Cycle Combustion Turbine #2 (3B)	A	NOX	8/16/2007	9.15	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	peaking mode
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H027	6/25/2003	0.0036	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H027	10/8/2007	0.00174	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	DIOX	6/22/2004	7.6	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	DIOX	9/24/2007	0	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test conducted on Unit 2.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	DIOX	10/24/2007	5.27	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	DIOX	6/25/2003	13	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	DIOX	6/30/2005	3.79	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	DIOX	10/8/2007	1.29	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	PB	10/25/2007	0.007	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	PM	10/25/2007	1.33	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H027	6/29/2005	0.000521	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H027	6/22/2004	0.000569	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H106	6/26/2003	97.4	PERCENT REDUCTION IN EMISSIONS	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H021	6/29/2005	0.000008	POUNDS/HOUR	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	NH3	6/28/2005	2.71	PARTS PER MILLION DRY GAS VOLUME	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	NH3	10/23/2007	4.22	PARTS PER MILLION DRY GAS VOLUME	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	NH3	6/28/2005	4	PARTS PER MILLION DRY GAS VOLUME	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H106	6/25/2003	96.9	PERCENT REDUCTION IN EMISSIONS	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H106	6/22/2004	96.5	PERCENT REDUCTION IN EMISSIONS	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	PM	6/22/2004	0.00211	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE	0710119	LEE CO. SOLID WASTE RESOURCE	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	PM	6/26/2003	0.0073	GRAINS PER DRY STANDARD	testar inc.

MGT.		REC. FAC.											CUBIC FOOT @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	PM	6/22/2004	0.000906	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	PM	9/24/2007	0.000039	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	NOX	6/22/2004	156	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	NOX	10/8/2007	137	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H106	6/22/2004	27.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H106	10/8/2007	19.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	CO	9/24/2007	16	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	CO	6/28/2005	9	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	CO	6/22/2004	7.52	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	CO	6/26/2003	9.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	SO2	9/24/2007	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	SO2	6/28/2005	0.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	SO2	6/22/2004	0.501	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	SO2	6/26/2003	0.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	VOC	9/24/2007	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Did not test this year
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	VOC	6/28/2005	0.06	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	FL	6/28/2005	0.167	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H106	10/23/2007	16	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H106	9/24/2007	19	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H106	6/28/2005	17.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H106	6/22/2004	21.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H106	6/26/2003	17.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	VOC	6/28/2005	0.06	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	SO2	10/8/2007	22	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	SO2	6/29/2005	2.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	SO2	6/22/2004	5.93	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	SO2	6/25/2003	2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	CO	10/8/2007	16	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	CO	6/29/2005	13.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar

LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	CO	6/22/2004	6.47	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	CO	6/25/2003	9.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	NOX	10/23/2007	130.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	NOX	9/24/2007	142	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	NOX	6/28/2005	151.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	NOX	6/22/2004	162	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	NOX	6/26/2003	164	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H027	10/23/2007	0.00054	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H027	9/24/2007	0.000635	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H027	6/28/2005	0.000456	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H027	6/22/2004	0.00002	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H027	6/26/2003	0.00992	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H114	10/8/2007	0.0123	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H114	6/29/2005	0.0142	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H114	6/22/2004	0.014	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H114	6/25/2003	0.031	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H114	9/24/2007	0.0118	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H114	6/28/2005	0.0357	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H114	6/22/2004	0.0228	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H114	6/26/2003	0.0259	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	FL	10/25/2007	0.146	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	FL	6/28/2005	0.162	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	CO	10/23/2007	16	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H106	6/29/2005	15.7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H106	6/25/2003	19.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	NOX	6/29/2005	149.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	NOX	6/25/2003	169	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar inc.

LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	PM	6/28/2005	0.000299	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	PM	6/27/2005	0.000345	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	PM	10/8/2007	0.000557	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	PB	9/24/2007	0.000012	POUNDS PER MILLION BTU HEAT INPUT	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	PB	6/28/2005	0.000004	POUNDS PER MILLION BTU HEAT INPUT	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	PB	10/8/2007	0.00005	POUNDS PER MILLION BTU HEAT INPUT	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	SAM	6/27/2005	0.00677	POUNDS PER MILLION BTU HEAT INPUT	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H015	6/28/2005	0	POUNDS PER MILLION BTU HEAT INPUT	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	PB	6/25/2003	0.000052	POUNDS PER MILLION BTU HEAT INPUT	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	PB	6/22/2004	0.000007	POUNDS PER MILLION BTU HEAT INPUT	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	PB	6/29/2005	0	POUNDS PER MILLION BTU HEAT INPUT	testar actual = 0.00000822
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H015	6/29/2005	0	POUNDS PER MILLION BTU HEAT INPUT	testar actual - 0.000000632
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	PB	6/22/2004	0.00003	POUNDS PER MILLION BTU HEAT INPUT	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	PB	6/26/2003	0.000088	POUNDS PER MILLION BTU HEAT INPUT	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	SAM	6/27/2005	0.00678	POUNDS PER MILLION BTU HEAT INPUT	testar
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H021	6/28/2005	0	POUNDS/HOUR	Testar actual < 7.99E-06
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H114	6/26/2003	78.6	PERCENT REDUCTION IN EMISSIONS	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	H114	10/25/2007	89.7	PERCENT REDUCTION IN EMISSIONS	
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	H114	6/25/2003	87.1	PERCENT REDUCTION IN EMISSIONS	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	2	Municipal Waste Combustion Unit #2	A	SO2	6/25/2003	98	PERCENT REDUCTION IN EMISSIONS	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	SO2	6/26/2003	99.8	PERCENT REDUCTION IN EMISSIONS	testar inc.
LEE COUNTY DEPT. OF SOLID WASTE MGT.	0710119	LEE CO. SOLID WASTE RESOURCE REC. FAC.	SD	LEE	A	Y	1	Municipal Waste Combustion Unit #1	A	SO2	10/23/2007	96.7	PERCENT REDUCTION IN EMISSIONS	
BONITA SPRINGS UTILITIES INC	0710236	EAST WATER RECLAMATION FACILITY	SD	LEE	A	Y	1	Rotary Sludge Dryer	A	PM	5/24/2007	0.18	POUNDS/HOUR	
BONITA SPRINGS UTILITIES INC	0710236	EAST WATER RECLAMATION FACILITY	SD	LEE	A	Y	1	Rotary Sludge Dryer	A	H114	6/4/2007	0.0019	POUNDS/DAY	
BONITA SPRINGS UTILITIES INC	0710236	EAST WATER RECLAMATION FACILITY	SD	LEE	A	Y	1	Rotary Sludge Dryer	A	H114	6/4/2007	0.0019	POUNDS/DAY	
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	1	Boiler #1(Phase II Acid Rain Unit)	A	SO2	8/27/2003	0.51	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	4	BOILER #2 (Phase II Acid Rain Unit)	A	PM	7/25/2007	0.0542	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	4	BOILER #2 (Phase II Acid Rain Unit)	A	PM	7/24/2007	0.0524	POUNDS PER MILLION BTU HEAT INPUT	Nominal gross load of 230.1 megawatts
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	4	BOILER #2 (Phase II Acid Rain Unit)	A	PM	8/9/2006	0.0411	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	4	BOILER #2 (Phase II Acid Rain Unit)	A	PM	8/24/2005	0.0856	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	4	BOILER #2 (Phase II Acid Rain Unit)	A	PM	5/26/2004	0.0519	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	4	BOILER #2 (Phase II Acid Rain Unit)	A	SO2	8/27/2003	0.79	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	4	BOILER #2 (Phase II Acid Rain Unit)	A	SO2	5/26/2004	0.82	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	4	BOILER #2 (Phase II Acid Rain Unit)	A	PM	8/27/2003	0.04	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	4	BOILER #2 (Phase II Acid Rain Unit)	A	PM	8/27/2003	0.09	POUNDS PER MILLION BTU HEAT INPUT	Soot Blow
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	4	BOILER #2 (Phase II Acid Rain Unit)	A	PM	5/26/2004	0.0517	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF	0730003	ARVAH B. HOPKINS GENERATING	NWDT	LEON	A	Y	4	BOILER #2 (Phase II Acid	A	PM	8/23/2005	0.0674	POUNDS PER MILLION BTU	

TALLAHASSEE		STATION						Rain Unit)					HEAT INPUT	
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	4	BOILER #2 (Phase II Acid Rain Unit)	A	PM	8/8/2006	0.0472	POUNDS PER MILLION BTU HEAT INPUT	EPA Method 17
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	4	BOILER #2 (Phase II Acid Rain Unit)	A	PM	7/25/2007	0.0542	POUNDS PER MILLION BTU HEAT INPUT	Nominal gross load of 229.1 megawatts
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	1	Boiler #1(Phase II Acid Rain Unit)	A	PM	8/27/2003	0.04	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	1	Boiler #1(Phase II Acid Rain Unit)	A	PM	8/27/2003	0.05	POUNDS PER MILLION BTU HEAT INPUT	Soot Blow
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	31	GE LM6000 Sprint Combustion Turbine HC3 with Inlet Chilling	A	NOX	9/12/2005	4.737	PARTS PER MILLION DRY GAS VOLUME	
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	31	GE LM6000 Sprint Combustion Turbine HC3 with Inlet Chilling	A	SAM	9/17/2005	1.15	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil firing.
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	31	GE LM6000 Sprint Combustion Turbine HC3 with Inlet Chilling	A	SAM	9/17/2005	0.87	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas firing.
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	32	GE LM6000 Sprint Combustion Turbine HC4 with Inlet Chilling	A	SAM	11/18/2005	0.11	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas firing. Air inlet temp = 53.4 degree
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	32	GE LM6000 Sprint Combustion Turbine HC4 with Inlet Chilling	A	NOX	11/18/2005	4.13	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil firing. Inlet air temp = 59.5 degrees F.
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	31	GE LM6000 Sprint Combustion Turbine HC3 with Inlet Chilling	A	NOX	9/19/2007	2.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Spectrum
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	32	GE LM6000 Sprint Combustion Turbine HC4 with Inlet Chilling	A	VOC	11/18/2005	0.35	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas firing. Inlet air temp = 53.4 degrees
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	32	GE LM6000 Sprint Combustion Turbine HC4 with Inlet Chilling	A	VOC	11/18/2005	0.13	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil firing. Inlet air temp = 59.5 degrees F.
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	31	GE LM6000 Sprint Combustion Turbine HC3 with Inlet Chilling	A	CO	9/17/2005	1.01	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas firing.
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	31	GE LM6000 Sprint Combustion Turbine HC3 with Inlet Chilling	A	CO	9/17/2005	0.644	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil firing.
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	31	GE LM6000 Sprint Combustion Turbine HC3 with Inlet Chilling	A	CO	9/12/2006	0.763	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Spectrum. Test metod 10.
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	31	GE LM6000 Sprint Combustion Turbine HC3 with Inlet Chilling	A	CO	9/19/2007	1.68	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Spectrum
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	32	GE LM6000 Sprint Combustion Turbine HC4 with Inlet Chilling	A	CO	11/18/2005	0.52	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas firing. Inlet air temp = 53.4 degrees
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	32	GE LM6000 Sprint Combustion Turbine HC4 with Inlet Chilling	A	CO	11/18/2005	0.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil firing. Inlet temp = 59.5 degrees F.
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	31	GE LM6000 Sprint Combustion Turbine HC3 with Inlet Chilling	A	NOX	9/17/2005	4.59	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas firing. Air inlet = 72 degrees.
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	31	GE LM6000 Sprint Combustion Turbine HC3 with Inlet Chilling	A	NOX	9/17/2005	4.46	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel Oil firing. Inlet air temp = 58 degrees F.
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	32	GE LM6000 Sprint Combustion Turbine HC4 with Inlet Chilling	A	CO	9/12/2006	4.068	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Spectrum. Test method 10.
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	32	GE LM6000 Sprint Combustion Turbine HC4 with Inlet Chilling	A	CO	9/20/2007	4.701	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Spectrum
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	31	GE LM6000 Sprint Combustion Turbine HC3 with Inlet Chilling	A	VOC	9/17/2005	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas firing.
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	31	GE LM6000 Sprint Combustion Turbine HC3 with Inlet Chilling	A	VOC	9/17/2005	0.01	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil firing.
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	32	GE LM6000 Sprint Combustion Turbine HC4 with Inlet Chilling	A	NOX	11/18/2005	4.99	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas firing. Inlet air temp = 53.4 degrees
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	32	GE LM6000 Sprint Combustion Turbine HC4 with Inlet Chilling	A	NOX	9/20/2007	3.932	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Spectrum
CITY OF TALLAHASSEE	0730003	ARVAH B. HOPKINS GENERATING STATION	NWDT	LEON	A	Y	32	GE LM6000 Sprint Combustion Turbine HC4 with Inlet Chilling	A	SAM	11/18/2005	0.153	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Fuel oil firing. Air inlet temp = 59.5
NORTH FLORIDA LUMBER	0770007	NORTH FLORIDA LUMBER	NWDT	LIBERTY	A	Y	2	BOILER #2 850 HP, 42.9 MMBTU/HR WITH WOOD GASIFICATION SYSTE	A	PM	12/5/2007	0.19	POUNDS PER MILLION BTU HEAT INPUT	Heat input average of 29 MMBtu/hr.
NORTH FLORIDA LUMBER	0770007	NORTH FLORIDA LUMBER	NWDT	LIBERTY	A	Y	2	BOILER #2 850 HP, 42.9 MMBTU/HR WITH WOOD GASIFICATION SYSTE	A	PM	10/29/2004	0.184	POUNDS PER MILLION BTU HEAT INPUT	
NORTH FLORIDA LUMBER	0770007	NORTH FLORIDA LUMBER	NWDT	LIBERTY	A	Y	2	BOILER #2 850 HP, 42.9 MMBTU/HR WITH WOOD GASIFICATION SYSTE	A	PM	9/25/2003	0.172	POUNDS PER MILLION BTU HEAT INPUT	
NORTH FLORIDA LUMBER	0770007	NORTH FLORIDA LUMBER	NWDT	LIBERTY	A	Y	2	BOILER #2 850 HP, 42.9 MMBTU/HR WITH WOOD GASIFICATION SYSTE	A	PM	12/28/2006	0.177	POUNDS PER MILLION BTU HEAT INPUT	
NORTH FLORIDA LUMBER	0770007	NORTH FLORIDA LUMBER	NWDT	LIBERTY	A	Y	2	BOILER #2 850 HP, 42.9 MMBTU/HR WITH WOOD	A	PM	10/24/2007	0.313	POUNDS PER MILLION BTU	Re-Test scheduled for 12/5/2007.

								GASIFICATION SYSTE					HEAT INPUT	
CQ BIOPOWER PRODUCERS, LLC	0770009	TELOGIA POWER, LLC	NWDT	LIBERTY	A	Y	1	Carbonaceous Boiler	A	PM	5/1/2006	0.04	POUNDS PER MILLION BTU HEAT INPUT	Power to ESP: 20.5 kpph
CQ BIOPOWER PRODUCERS, LLC	0770009	TELOGIA POWER, LLC	NWDT	LIBERTY	A	Y	1	Carbonaceous Boiler	A	PM	11/2/2006	0.042	POUNDS PER MILLION BTU HEAT INPUT	
CQ BIOPOWER PRODUCERS, LLC	0770009	TELOGIA POWER, LLC	NWDT	LIBERTY	A	Y	1	Carbonaceous Boiler	A	PM	10/8/2003	0.011	POUNDS PER MILLION BTU HEAT INPUT	
CQ BIOPOWER PRODUCERS, LLC	0770009	TELOGIA POWER, LLC	NWDT	LIBERTY	A	Y	1	Carbonaceous Boiler	A	PM	10/16/2004	0.018	POUNDS PER MILLION BTU HEAT INPUT	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	8	Forming bins BH exhaust	A	PM	9/1/2005	0.53	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	CO	9/1/2005	5.4	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	CO	5/12/2006	3.4	POUNDS/HOUR	1530 Degrees F.
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	CO	5/12/2006	9.2	POUNDS/HOUR	1530 degrees F.
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	2	Panel press w/ one RTO	A	VOC	9/1/2005	1.22	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	2	Panel press w/ one RTO	A	VOC	5/9/2006	1.4	POUNDS/HOUR	RTO: 900 degrees F.
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	NOX	5/12/2006	26	POUNDS/HOUR	1530 degrees F.
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	NOX	5/12/2006	22	POUNDS/HOUR	1530 degrees F.
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	NOX	5/11/2006	25	POUNDS/HOUR	1506 degrees F.
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	NOX	5/11/2006	22	POUNDS/HOUR	1506 degrees F.
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	NOX	9/1/2005	21.39	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	NOX	9/1/2005	19.77	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	NOX	5/1/2007	20.17	POUNDS/HOUR	Environmental Monitoring Laboratories; RTO 1551 F
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	NOX	5/1/2007	21.44	POUNDS/HOUR	Environmental Monitoring Laboratories; RTO 1529 F
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	NOX	5/1/2007	21.44	POUNDS/HOUR	Environmental Monitoring Laboratories; RTO 1529 F
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	7	Fuel system pneumatics BH exhaust	A	PM	9/1/2005	0.02	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	2	Panel press w/ one RTO	A	PM	5/9/2006	1.4	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	2	Panel press w/ one RTO	A	PM	9/1/2005	0.83	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	2	Panel press w/ one RTO	A	PM	5/1/2007	0.94	POUNDS/HOUR	Environmental Monitoring Laboratories; RTO 963 F
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	2	Panel press w/ one RTO	A	NOX	5/9/2006	1.2	POUNDS/HOUR	RTO: 900 degrees F.
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	2	Panel press w/ one RTO	A	NOX	9/1/2005	0.79	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	2	Panel press w/ one RTO	A	NOX	5/1/2007	1.34	POUNDS/HOUR	Environmental Monitoring Laboratories; RTO 963 F
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	11	Thermal oil system ESP (bypass stack)	A	NOX	9/1/2005	0.67	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	11	Thermal oil system ESP (bypass stack)	A	NOX	9/1/2005	1.73	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	6	Specialty saw/sander BH exhaust	A	PM	9/1/2005	0.32	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	4	Saw trim/finishing BH exhaust	A	PM	9/1/2005	0.25	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	11	Thermal oil system ESP (bypass stack)	A	CO	9/1/2005	2.1	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	11	Thermal oil system ESP (bypass stack)	A	CO	9/1/2005	0.07	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	3	Screen fines with saw trim transfer BH exhaust	A	PM	9/1/2005	0.43	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	11	Thermal oil system ESP (bypass stack)	A	PM	9/1/2005	0.17	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	11	Thermal oil system ESP (bypass stack)	A	PM	9/1/2005	0.19	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	2	Panel press w/ one RTO	A	VOC	9/1/2005	42.05	POUNDS/HOUR	Inlet side of thermal oxidizer. Percent reductior (42.05 - 0.83) / 42.05 = 98.0
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	2	Panel press w/ one RTO	A	VOC	5/1/2007	0.61	POUNDS/HOUR	Environmental Monitoring Laboratories; RTO 963 F
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	CO	5/11/2006	18	POUNDS/HOUR	1506 degrees F.

GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	CO	5/11/2006	6.1	POUNDS/HOUR	1506 degrees F.
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	CO	9/1/2005	5.11	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	CO	5/1/2007	11.22	POUNDS/HOUR	Environmental Monitoring Laboratories; RTO 1529 F
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	CO	5/1/2007	2	POUNDS/HOUR	Environmental Monitoring Laboratores; RTO - F
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	9	Hammer mill BH exhaust	A	PM	9/1/2005	0.23	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	11	Thermal oil system ESP (bypass stack)	A	VOC	9/1/2005	0.62	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	PM	5/1/2007	7.07	POUNDS/HOUR	Environmental Monitoring Laboratories; RTO 1551 F
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	PM	5/1/2007	7.94	POUNDS/HOUR	Environmental Monitoring Laboratories; RTO 1529 F
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	11	Thermal oil system ESP (bypass stack)	A	VOC	9/1/2005	1.45	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	PM	9/1/2005	5.23	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	PM	5/11/2006	2.6	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	PM	5/12/2006	2.2	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	2	Panel press w/ one RTO	A	CO	5/9/2006	1.9	POUNDS/HOUR	RTO: 900 degrees F.
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	2	Panel press w/ one RTO	A	CO	9/1/2005	0.12	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	2	Panel press w/ one RTO	A	CO	5/1/2007	0	POUNDS/HOUR	Environmental Monitoring Laboritories; RTO 963 F
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	VOC	5/12/2006	1.2	POUNDS/HOUR	1530 degrees F.
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	VOC	5/12/2006	0.6	POUNDS/HOUR	1530 degrees F.
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	VOC	5/11/2006	1.2	POUNDS/HOUR	1506 degrees F.
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	VOC	5/11/2006	1.2	POUNDS/HOUR	1506 degrees F.
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	VOC	9/1/2005	2.52	POUNDS/HOUR	Setpoint: 1508 degrees F for each thermal oxidi
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	VOC	9/1/2005	2.23	POUNDS/HOUR	Setpoint: 1508 degrees F for each thermal oxidi
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	VOC	9/1/2005	227.79	POUNDS/HOUR	Inlet side of RTO A. Percent reduction was (22 2.52) / 227.8 = 98.9%
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	VOC	9/1/2005	224.69	POUNDS/HOUR	Inlet side of RTO B. Percent reduction of VOC (224.7 - 2.23) / 224.7 = 99.0%
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	VOC	5/1/2007	2.24	POUNDS/HOUR	Environmental Monitoring Laboratories; RTO 1551 F
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	VOC	5/1/2007	1.36	POUNDS/HOUR	Environmental Monitoring Laboratories; RTO 1529 F
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	PM	5/12/2006	2.8	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	5	Mat reject/flying saw BH exhaust	A	PM	9/1/2005	0.69	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	PM	5/11/2006	5.1	POUNDS/HOUR	
GA-PACIFIC WOOD PRODUCTS	0770010	GA-PACIFIC WOOD PRODUCTS (HOSFORD OSB)	NWDT	LIBERTY	A	Y	1	Five flake dryers w/ two RTOs	A	PM	9/1/2005	4.45	POUNDS/HOUR	
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	26	New Gas Turbine/Existing HRSG at Cogen Plant	A	CO	3/13/2003	8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Catalyst performed test. Heat input 428 MMBtu Above acutal is only for new turbine. HRSG tes results - 0.6 lb/hr.
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	26	New Gas Turbine/Existing HRSG at Cogen Plant	A	NOX	2/19/2004	22	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	420.95 MMBtu/hr. Catalyst Air Management. HSRG 98.53 MMBtu/hr NOX - 0.003 lb/MMB
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	26	New Gas Turbine/Existing HRSG at Cogen Plant	A	NOX	3/13/2003	19.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Catalyst Performed test. Heat input 428 MMBtu Above acutal is only for the new turbine. HRSC 2.2 lb/hr..
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	26	New Gas Turbine/Existing HRSG at Cogen Plant	A	NOX	2/1/2005	17.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	EPA Method 7E, Catalyst Air Management, Inc 429 MMBtu/hr. HRSG - 0.004 lb/MMBtu. 96.2 MMBtu/hr
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	26	New Gas Turbine/Existing HRSG at Cogen Plant	A	NOX	2/8/2006	23.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	HRSG summary: 0.006 lb/MMBtu NOx; 0.6 lb NOx; 96.5 MMBtu/hr heat input. Catalyst Air Management, Inc.
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	26	New Gas Turbine/Existing HRSG at Cogen Plant	A	NOX	2/7/2008	19.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Catalyst Air Management
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	26	New Gas Turbine/Existing HRSG at Cogen Plant	A	NOX	2/13/2007	18.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	catalyst
TROPICANA								157.4 MMBTU/HR						

MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	15	AUXILIARY BOILER FOR COGEN PLANT	A	NOX	2/13/2007	9.4	POUNDS/HOUR	catalyst
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	15	157.4 MMBTU/HR AUXILIARY BOILER FOR COGEN PLANT	A	NOX	2/7/2006	15.2	POUNDS/HOUR	Fuel: OIL; Catalyst Air Management, Inc.
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	15	157.4 MMBTU/HR AUXILIARY BOILER FOR COGEN PLANT	A	NOX	1/31/2005	9.4	POUNDS/HOUR	Gas testing, EPA Method 7E, Catalyst Air Management, Inc., 154.8 MMBtu/hr
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	15	157.4 MMBTU/HR AUXILIARY BOILER FOR COGEN PLANT	A	NOX	2/7/2006	10.7	POUNDS/HOUR	Fuel: GAS; Catalyst Air Management, Inc.
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	15	157.4 MMBTU/HR AUXILIARY BOILER FOR COGEN PLANT	A	NOX	2/13/2007	12.7	POUNDS/HOUR	catalyst
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	15	157.4 MMBTU/HR AUXILIARY BOILER FOR COGEN PLANT	A	NOX	1/31/2005	14.3	POUNDS/HOUR	Testing on oil, EPA Method 7E, Catalyst, 154.4 MMBtu/hr
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	15	157.4 MMBTU/HR AUXILIARY BOILER FOR COGEN PLANT	A	NOX	2/18/2004	15.8	POUNDS/HOUR	
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	2	CITRUS PEEL DRYER #2 W/WHE	A	PM	3/6/2003	8.89	POUNDS/HOUR	Dryer water spray flow at 112 gpm
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	2	CITRUS PEEL DRYER #2 W/WHE	A	PM	3/31/2005	8.7	POUNDS/HOUR	Total from stack A and stack B. 34.8 TPH
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	2	CITRUS PEEL DRYER #2 W/WHE	A	PM	3/23/2006	2.5	POUNDS/HOUR	
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	2	CITRUS PEEL DRYER #2 W/WHE	A	PM	4/4/2007	3.3	POUNDS/HOUR	southern environmental sciences
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	1	CITRUS PEEL DRYER #1 W/WHE	A	PM	3/9/2004	8.7	POUNDS/HOUR	Scrubber flow rate 233 gpm, a little less than 9(last test (236.7 gpm). Process rate was 46.7 TPI heat input was 55 MMBtu/hr
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	1	CITRUS PEEL DRYER #1 W/WHE	A	PM	2/13/2003	2.4	POUNDS/HOUR	47.83 TPH, 57.8 MMBtu/hr, Carl Stiel perform test, dryer water spray flow at 263 gpm
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	1	CITRUS PEEL DRYER #1 W/WHE	A	PM	4/14/2004	6.9	POUNDS/HOUR	Process rate - 46.5 TPH, scrubber flow rate - 19 gpm, heat input - 59.25 MMBtu/hr Scrubber flo rate must now be at least 171 gpm.
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	1	CITRUS PEEL DRYER #1 W/WHE	A	PM	3/8/2005	3.8	POUNDS/HOUR	34.8 TPH
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	1	CITRUS PEEL DRYER #1 W/WHE	A	PM	3/21/2006	6.6	POUNDS/HOUR	
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	1	CITRUS PEEL DRYER #1 W/WHE	A	PM	4/3/2007	4.6	POUNDS/HOUR	southern environmental sciences
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	3	CITRUS PEEL DRYER #3 W/WHE	A	PM	3/11/2004	4.3	POUNDS/HOUR	Scrubber flow rate 101 gpm. Process rate 46 TI
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	3	CITRUS PEEL DRYER #3 W/WHE	A	PM	2/27/2003	1.37	POUNDS/HOUR	45.1 TPH, Carl Stiel conducted test, dryer wate spray flow at 101 gpm
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	3	CITRUS PEEL DRYER #3 W/WHE	A	PM	3/25/2005	3.2	POUNDS/HOUR	32.5 TPH
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	3	CITRUS PEEL DRYER #3 W/WHE	A	PM	3/22/2006	2.5	POUNDS/HOUR	
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	3	CITRUS PEEL DRYER #3 W/WHE	A	PM	5/2/2007	4.3	POUNDS/HOUR	southern environmental
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	15	157.4 MMBTU/HR AUXILIARY BOILER FOR COGEN PLANT	A	NOX	3/12/2003	14.9	POUNDS/HOUR	Catalyst performed testing. Heat input 147.53 MMBtu/hr.
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	15	157.4 MMBTU/HR AUXILIARY BOILER FOR COGEN PLANT	A	NOX	3/13/2003	9.8	POUNDS/HOUR	Catalyst performed test. Heat input 150.9 MMBtu/hr.
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	2	CITRUS PEEL DRYER #2 W/WHE	A	PM	4/21/2004	9.8	POUNDS/HOUR	Combined emissions from stack A and B. 47 TI 62.2 MMBtu/hr, scrubber flow rate 164 gpm, m be at least 148 gpm
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	2	CITRUS PEEL DRYER #2 W/WHE	A	PM	3/8/2004	10.8	POUNDS/HOUR	
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	15	157.4 MMBTU/HR AUXILIARY BOILER FOR COGEN PLANT	A	NOX	2/18/2004	10.9	POUNDS/HOUR	
TROPICANA MANUFACTURING COMPANY, INC.	0810007	TROPICANA, BRADENTON	SWD	MANATEE	A	Y	15	157.4 MMBTU/HR AUXILIARY BOILER FOR COGEN PLANT	A	NOX	2/6/2008	0.08	POUNDS PER MILLION BTU HEAT INPUT	Fuel: Oil; Catalyst Air Management
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	8	Unit 3D Combustion Turbine (170 MW) with HRSG	A	NOX	5/25/2005	2.24	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	hi load with DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	8	Unit 3D Combustion Turbine (170 MW) with HRSG	A	NH3	5/25/2005	0.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	hi load w/DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	8	Unit 3D Combustion Turbine (170 MW) with HRSG	A	NOX	5/25/2005	2.23	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	hhi load no DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	8	Unit 3D Combustion Turbine (170 MW) with HRSG	A	NH3	6/6/2007	0.028	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	fpl
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	2	Fossil Fuel Steam Generator, Unit 2-Phase II Acid Rain Unit	A	PM	5/25/2004	0.03	POUNDS PER MILLION BTU HEAT INPUT	Steady state testing on fuel oil. Heat input - 755 MMBtu/hr.
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	2	Fossil Fuel Steam Generator, Unit 2-Phase II Acid Rain Unit	A	PM	5/25/2004	0.03	POUNDS PER MILLION BTU HEAT INPUT	Soot blowing while firing fuel oil. Heat input - mmBtu/hr
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	2	Fossil Fuel Steam Generator, Unit 2-Phase II Acid Rain Unit	A	PM	5/3/2005	0.04	POUNDS PER MILLION BTU HEAT INPUT	Fuel oil. 0.95% sulfur. Soot blowing. Heat inpu 7527 mmBtu/hr. Restricts heat input to 8280 MMBtu/hr
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	2	Fossil Fuel Steam Generator, Unit 2-Phase II Acid Rain Unit	A	PM	5/3/2005	0.02	POUNDS PER MILLION BTU HEAT INPUT	Fuel oil. Sulfur content 0.95%. Steady state. He input 7527 MMBtu/hr. Restricts heat inpt to 82 MMBtu/hr.
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	2	Fossil Fuel Steam Generator, Unit 2-Phase II Acid Rain Unit	A	PM	6/6/2006	0.038	POUNDS PER MILLION BTU HEAT INPUT	FPL
FLORIDA POWER &		MANATEE POWER						Fossil Fuel Steam Generator,					POUNDS PER	

LIGHT (PMT)	0810010	PLANT	SWD	MANATEE	A	Y	2	Unit 2-Phase II Acid Rain Unit	A	PM	6/20/2007	0.03	MILLION BTU HEAT INPUT	FPL
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	2	Fossil Fuel Steam Generator, Unit 2-Phase II Acid Rain Unit	A	CO	2/25/2003	0.281	POUNDS PER MILLION BTU HEAT INPUT	Initial Testing on Natural Gas
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	1	Fossil Fuel Steam Generator, Unit 1-Phase II Acid Rain Unit	A	VOC	11/4/2003	0.0011	POUNDS PER MILLION BTU HEAT INPUT	Heat input 5652 mmBTU/hr. Initial testing on natural gas.
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	1	Fossil Fuel Steam Generator, Unit 1-Phase II Acid Rain Unit	A	PM	11/4/2003	0.008	POUNDS PER MILLION BTU HEAT INPUT	Heat input 5676 mmBTU/hr. Initial testing on natural gas.
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	2	Fossil Fuel Steam Generator, Unit 2-Phase II Acid Rain Unit	A	PM	5/20/2003	0.04	POUNDS PER MILLION BTU HEAT INPUT	Steady state while firing with fuel oil. 7651 MMBtu/hr. New heat input limit of 8416.1 MMBtu/hr
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	2	Fossil Fuel Steam Generator, Unit 2-Phase II Acid Rain Unit	A	PM	5/20/2003	0.05	POUNDS PER MILLION BTU HEAT INPUT	Test on fuel oil. Soot Blowing. Heat input 7651 MMBTU/hr. Sets new heat input limit to 8416. MMBtu/hr.
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	2	Fossil Fuel Steam Generator, Unit 2-Phase II Acid Rain Unit	A	PM	2/25/2003	0.003	POUNDS PER MILLION BTU HEAT INPUT	Initial Testing on Natural Gas, 5542 MMBtu/h FP&L Technical Services Emission Test Grou
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	2	Fossil Fuel Steam Generator, Unit 2-Phase II Acid Rain Unit	A	PM	2/25/2003	0.021	POUNDS PER MILLION BTU HEAT INPUT	Soot blowing, 5542 MMBtu/hr, FP&L Technic Services Emission Test Group
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	1	Fossil Fuel Steam Generator, Unit 1-Phase II Acid Rain Unit	A	PM	11/4/2003	0.02	POUNDS PER MILLION BTU HEAT INPUT	Heat input 5676 mmBTU/hr. Initial testing on natural gas.
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	1	Fossil Fuel Steam Generator, Unit 1-Phase II Acid Rain Unit	A	PM	5/4/2004	0.03	POUNDS PER MILLION BTU HEAT INPUT	FP&L Technical Services Testing Group. Testi fuel oil. Steady state.
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	1	Fossil Fuel Steam Generator, Unit 1-Phase II Acid Rain Unit	A	PM	5/4/2004	0.05	POUNDS PER MILLION BTU HEAT INPUT	FP&L Technical Services Test Group. Fuel oil. MMBtu/hr. Soot Blowing.
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	1	Fossil Fuel Steam Generator, Unit 1-Phase II Acid Rain Unit	A	PM	4/26/2005	0.03	POUNDS PER MILLION BTU HEAT INPUT	Fuel oil, steady state. Heat input 7657 MMBtu/ Restricts heat input to 8423 MMBtu/hr
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	1	Fossil Fuel Steam Generator, Unit 1-Phase II Acid Rain Unit	A	PM	4/26/2005	0.06	POUNDS PER MILLION BTU HEAT INPUT	Fuel oil. Soot blowing. Heat input 7657 MMBt Restricts heat input to 8423 MMBtu/hr.
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	1	Fossil Fuel Steam Generator, Unit 1-Phase II Acid Rain Unit	A	PM	4/11/2006	0.05	POUNDS PER MILLION BTU HEAT INPUT	FP&L Technical Services Test Group; fuel oil; blowing.
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	1	Fossil Fuel Steam Generator, Unit 1-Phase II Acid Rain Unit	A	PM	4/11/2006	0.04	POUNDS PER MILLION BTU HEAT INPUT	FP&L Technical Services Test Group; fuel oil; steady-state.
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	1	Fossil Fuel Steam Generator, Unit 1-Phase II Acid Rain Unit	A	PM	6/13/2007	0.03	POUNDS PER MILLION BTU HEAT INPUT	FPL
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	1	Fossil Fuel Steam Generator, Unit 1-Phase II Acid Rain Unit	A	CO	11/4/2003	0.312	POUNDS PER MILLION BTU HEAT INPUT	Heat input 5652 mmBTU/hr. Initial testing on natural gas.
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	2	Fossil Fuel Steam Generator, Unit 2-Phase II Acid Rain Unit	A	VOC	2/25/2003	0.0008	POUNDS PER MILLION BTU HEAT INPUT	Initial Testing on Natural Gas
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	1	Fossil Fuel Steam Generator, Unit 1-Phase II Acid Rain Unit	A	PM	9/9/2003	0.04	POUNDS PER MILLION BTU HEAT INPUT	Heat input - 7740 MMBtu/hr - steady state - oil FP&L Technical Services Emission Test Grou
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	1	Fossil Fuel Steam Generator, Unit 1-Phase II Acid Rain Unit	A	PM	9/9/2003	0.05	POUNDS PER MILLION BTU HEAT INPUT	Heat input - 7740 MMBtu/hr - soot blowing - o FP&L Technical Services Emission Test Grou
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	8	Unit 3D Combustion Turbine (170 MW) with HRSG	A	NH3	6/20/2006	0.039	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Emissions Test Group
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	7	Unit 3C Combustion Turbine (170 MW) with HRSG	A	NOX	6/7/2007	2.31	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	fpl
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	7	Unit 3C Combustion Turbine (170 MW) with HRSG	A	NOX	6/19/2006	2.35	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Emissions Test Group
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	7	Unit 3C Combustion Turbine (170 MW) with HRSG	A	NH3	5/25/2005	0.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	hi load no DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	7	Unit 3C Combustion Turbine (170 MW) with HRSG	A	NH3	6/19/2006	0.07	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Emissions Test Group
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	7	Unit 3C Combustion Turbine (170 MW) with HRSG	A	NH3	6/7/2007	0.033	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	fpl
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	6	Unit 3B Combustion Turbine (170 MW) with HRSG	A	NOX	5/25/2005	2.21	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	high load no DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	6	Unit 3B Combustion Turbine (170 MW) with HRSG	A	NOX	5/25/2005	2.04	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	high load with DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	6	Unit 3B Combustion Turbine (170 MW) with HRSG	A	NOX	6/15/2006	0.97	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Emissions Test Group
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	6	Unit 3B Combustion Turbine (170 MW) with HRSG	A	NOX	6/5/2007	0.0089	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	fpl
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	7	Unit 3C Combustion Turbine (170 MW) with HRSG	A	NOX	5/25/2005	2.24	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	hi load w/DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	8	Unit 3D Combustion Turbine (170 MW) with HRSG	A	NOX	6/20/2006	2.27	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Emissions Test Group
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	8	Unit 3D Combustion Turbine (170 MW) with HRSG	A	NOX	6/6/2007	2.38	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	fpl
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	6	Unit 3B Combustion Turbine (170 MW) with HRSG	A	NH3	5/25/2005	1.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER &		MANATEE POWER						Unit 3B Combustion Turbine					PARTS PER MILLION DRY	

LIGHT (PMT)	0810010	PLANT	SWD	MANATEE	A	Y	6	(170 MW) with HRSG	A	NH3	6/15/2006	0.1	GAS VOLUME @ 15% O2	Emissions Test Group
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	6	Unit 3B Combustion Turbine (170 MW) with HRSG	A	NH3	6/5/2007	0.033	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	fpl
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	5	Unit 3A Combustion Turbine (170 MW) with HRSG	A	NH3	6/14/2006	0.068	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Emissions Test Group
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	5	Unit 3A Combustion Turbine (170 MW) with HRSG	A	NH3	6/6/2007	2.25	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	FPL
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	5	Unit 3A Combustion Turbine (170 MW) with HRSG	A	NOX	5/25/2005	2.25	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	high load with DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	5	Unit 3A Combustion Turbine (170 MW) with HRSG	A	NOX	5/25/2005	2.37	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	high load w/o DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	5	Unit 3A Combustion Turbine (170 MW) with HRSG	A	NOX	6/14/2006	0.068	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Emissions Test Group
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	5	Unit 3A Combustion Turbine (170 MW) with HRSG	A	NOX	6/16/2007	2.71	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	fpl
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	7	Unit 3C Combustion Turbine (170 MW) with HRSG	A	NOX	5/25/2005	2.23	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	hi load no DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	7	Unit 3C Combustion Turbine (170 MW) with HRSG	A	CO	6/7/2007	0.51	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	FPL
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	7	Unit 3C Combustion Turbine (170 MW) with HRSG	A	CO	5/25/2005	1.26	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	hi load w/DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	5	Unit 3A Combustion Turbine (170 MW) with HRSG	A	CO	6/6/2007	0.42	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	FPL
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	5	Unit 3A Combustion Turbine (170 MW) with HRSG	A	CO	5/25/2005	0.98	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	high load w/o DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	6	Unit 3B Combustion Turbine (170 MW) with HRSG	A	VOC	5/25/2005	0.32	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	high load w/o DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	8	Unit 3D Combustion Turbine (170 MW) with HRSG	A	CO	5/25/2005	0.21	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	hi load no DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	8	Unit 3D Combustion Turbine (170 MW) with HRSG	A	CO	5/25/2005	0.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	hi load no DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	8	Unit 3D Combustion Turbine (170 MW) with HRSG	A	CO	6/20/2006	0.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	Emissions Test Group
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	8	Unit 3D Combustion Turbine (170 MW) with HRSG	A	CO	6/6/2007	0.43	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	fpl
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	6	Unit 3B Combustion Turbine (170 MW) with HRSG	A	CO	5/25/2005	0.37	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	high laod w/o DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	6	Unit 3B Combustion Turbine (170 MW) with HRSG	A	CO	5/25/2005	0.65	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	high loas with DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	6	Unit 3B Combustion Turbine (170 MW) with HRSG	A	CO	6/15/2006	0.39	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	Emissions Test Group
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	6	Unit 3B Combustion Turbine (170 MW) with HRSG	A	CO	6/5/2007	0.49	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	FPL
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	5	Unit 3A Combustion Turbine (170 MW) with HRSG	A	VOC	5/25/2005	0.65	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	high load w/o DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	5	Unit 3A Combustion Turbine (170 MW) with HRSG	A	VOC	5/25/2005	0.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	8	Unit 3D Combustion Turbine (170 MW) with HRSG	A	VOC	5/25/2005	0.44	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	hi load no DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	8	Unit 3D Combustion Turbine (170 MW) with HRSG	A	VOC	5/25/2005	0.48	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	hi load w/DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	7	Unit 3C Combustion Turbine (170 MW) with HRSG	A	VOC	5/25/2005	0.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	hi load no DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	7	Unit 3C Combustion Turbine (170 MW) with HRSG	A	VOC	5/25/2005	0.99	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	hi load w/DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	6	Unit 3B Combustion Turbine (170 MW) with HRSG	A	VOC	5/25/2005	0.53	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	high load w/DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	5	Unit 3A Combustion Turbine (170 MW) with HRSG	A	CO	6/14/2006	4.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	Emission Test Group
													PARTS PER	

FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	7	Unit 3C Combustion Turbine (170 MW) with HRSG	A	CO	5/25/2005	0.62	MILLION DRY GAS VOLUME @ 15% O2 ISO	hi load no DB
FLORIDA POWER & LIGHT (PMT)	0810010	MANATEE POWER PLANT	SWD	MANATEE	A	Y	7	Unit 3C Combustion Turbine (170 MW) with HRSG	A	CO	6/19/2006	1.38	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	Emission Test Group
PHOTONIC PRODUCTS GROUP, INC./MRC PMO	0810072	MRC PRECISION METAL OPTICS, INC.	SWD	MANATEE	A	Y	1	BERYLLIUM MACHINE SHOP w/lathe, mill and machining center	A	H021	8/23/2005	0.0151	GRAMS/DAY (24 HOURS)	EPA Method 103. This test was done with only machine operating. It does not satisfy the permi condition.
FLOWERS BAKING COMPANY OF BRADENTON, LLC	0810164	FLOWERS BAKING COMPANY OF BRADENTON, LLC	SWD	MANATEE	A	Y	1	Bread Line (Bread Oven)	A	VOC	2/18/2004	13.61	POUNDS/HOUR	Acetaldehyde emission rate (lb/hr) was 0.420. Testing company was Environmental Sampling Monitoring Services
ALLIED FIBERGLASS INDUSTRIES, INC.	0810203	ALLIED FIBERGLASS INDUSTRIES, INC.	SWD	MANATEE	A	Y	1	Misc. Fiberglass Products Manufacturing	A	H163	2/27/2006	0.0001	TONS/YEAR	velocity test on fans 6 and 7 and paint room fan
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	4	FGTC Engine 1704 - 2000 bhp RICE compressor engine	A	CO	7/10/2003	1.3	GRAMS PER BILLION HORSEPOWER-HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	4	FGTC Engine 1704 - 2000 bhp RICE compressor engine	A	CO	7/26/2005	1.31	GRAMS PER BILLION HORSEPOWER-HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	4	FGTC Engine 1704 - 2000 bhp RICE compressor engine	A	CO	9/24/2004	1.25	GRAMS PER BILLION HORSEPOWER-HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	4	FGTC Engine 1704 - 2000 bhp RICE compressor engine	A	NOX	7/10/2003	6.3	GRAMS PER BILLION HORSEPOWER-HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	4	FGTC Engine 1704 - 2000 bhp RICE compressor engine	A	NOX	7/26/2005	6.32	GRAMS PER BILLION HORSEPOWER-HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	4	FGTC Engine 1704 - 2000 bhp RICE compressor engine	A	NOX	7/25/2007	4.4	GRAMS PER BILLION HORSEPOWER-HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	4	FGTC Engine 1704 - 2000 bhp RICE compressor engine	A	NOX	6/21/2006	4.61	GRAMS PER BILLION HORSEPOWER-HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	4	FGTC Engine 1704 - 2000 bhp RICE compressor engine	A	NOX	9/24/2004	3.68	GRAMS PER BILLION HORSEPOWER-HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	4	FGTC Engine 1704 - 2000 bhp RICE compressor engine	A	CO	7/25/2007	1.2	GRAMS PER BILLION HORSEPOWER-HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	4	FGTC Engine 1704 - 2000 bhp RICE compressor engine	A	CO	6/21/2006	1.2	GRAMS PER BILLION HORSEPOWER-HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	5	FGTC Engine 1705 - 2400 bhp RICE compressor engine	A	NOX	7/25/2007	6.8	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	5	FGTC Engine 1705 - 2400 bhp RICE compressor engine	A	NOX	6/21/2006	3.99	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	5	FGTC Engine 1705 - 2400 bhp RICE compressor engine	A	NOX	7/26/2005	7.2	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	5	FGTC Engine 1705 - 2400 bhp RICE compressor engine	A	NOX	9/23/2004	8.2	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	5	FGTC Engine 1705 - 2400 bhp RICE compressor engine	A	NOX	7/10/2003	4.7	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	8	FGTC Engine 1706 - 15,700 bhp gas turbine compressor engine	A	CO	7/24/2007	1.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	8	FGTC Engine 1706 - 15,700 bhp gas turbine compressor engine	A	CO	9/23/2004	1.26	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Unit tested at 1/2 and full load, passed both
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	8	FGTC Engine 1706 - 15,700 bhp gas turbine compressor engine	A	CO	7/25/2005	9.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	8	FGTC Engine 1706 - 15,700 bhp gas turbine compressor engine	A	CO	6/22/2006	1.27	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	8	FGTC Engine 1706 - 15,700 bhp gas turbine compressor engine	A	NOX	6/10/2003	21.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	8	FGTC Engine 1706 - 15,700 bhp gas turbine compressor engine	A	NOX	1/17/2003	15.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	8	FGTC Engine 1706 - 15,700 bhp gas turbine compressor engine	A	NOX	9/23/2004	18.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	8	FGTC Engine 1706 - 15,700 bhp gas turbine compressor engine	A	NOX	7/25/2005	21.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	8	FGTC Engine 1706 - 15,700 bhp gas turbine compressor engine	A	NOX	6/22/2006	20.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	8	FGTC Engine 1706 - 15,700 bhp gas turbine compressor engine	A	NOX	7/24/2007	15.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	8	FGTC Engine 1706 - 15,700 bhp gas turbine compressor engine	A	CO	1/17/2003	0.85	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	8	FGTC Engine 1706 - 15,700 bhp gas turbine compressor engine	A	CO	6/10/2003	2.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	

FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	5	FGTC Engine 1705 - 2400 bhp RICE compressor engine	A	CO	7/25/2007	9.2	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	5	FGTC Engine 1705 - 2400 bhp RICE compressor engine	A	CO	6/21/2006	10.2	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	5	FGTC Engine 1705 - 2400 bhp RICE compressor engine	A	CO	7/26/2005	11.5	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	5	FGTC Engine 1705 - 2400 bhp RICE compressor engine	A	CO	9/23/2004	11.1	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0830070	FGTC STATION 17, MARION COUNTY	CD	MARION	A	Y	5	FGTC Engine 1705 - 2400 bhp RICE compressor engine	A	CO	7/10/2003	11.6	POUNDS/HOUR	
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	NOX	4/4/2007	1.73	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the test; NOx=0.0063#/MMBT 11.1 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/26/2005	8.69	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: Tst on oil and without DB; NOx= 0.034#/mmbtu=71.40#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/23/2005	2.21	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG without DB; NOx=0.008#/mmbtu=15. #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	NOX	5/15/2007	0.289	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=2080#/hr on oil ; HI=7206 MMBTU
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	NOX	4/26/2006	0.161	POUNDS PER MILLION BTU HEAT INPUT	RN: NG during the test; NOx=906#/hr; HI=5631MMBTU/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	NOX	3/30/2005	0.269	POUNDS PER MILLION BTU HEAT INPUT	RN: unit was tstd on OIL; NOx= 1954#/hr; loa 7270 MMbtu/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	NOX	6/21/2004	0.292	POUNDS PER MILLION BTU HEAT INPUT	RN: oil drng the test;additives seePM tst cmnts NOx=2125#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	PM	6/21/2004	0.04	POUNDS PER MILLION BTU HEAT INPUT	RN: 100% oil during the test; Bycosiin 98014T EESCC910 fuel additives used at injectn rte 17 and 19 gal/nr rspcvly.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	PM	3/30/2005	0.04	POUNDS PER MILLION BTU HEAT INPUT	RN: Oil drng the tst. 7270 vs 9040 MMBTU/H
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	PM	4/27/2006	0.03	POUNDS PER MILLION BTU HEAT INPUT	RN: 100% oil was burned during the test. FPL cndtd stack test.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	PM	5/15/2007	0.03	POUNDS PER MILLION BTU HEAT INPUT	RN: 100% oil with fuel additives (EES SFT-34 and EESO pacitrol) 1:3000 ratio, HI=7206 MMBTU/hr vs 8650
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	PM	4/7/2004	0.06	POUNDS PER MILLION BTU HEAT INPUT	RN: oil during the test;steady state and soot blowing; Fuel additives Bycosin 98014T and E CC910 were used drng the tst at rate 15.06gal/h 19.19gal/hr rsptfly
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	PM	3/25/2003	0.06	POUNDS PER MILLION BTU HEAT INPUT	RN- oil while using Bycosin 98014T & EES C fuel additives at rate of 14 gal/hr & 17.25 Gal/h during the test(1 run on st blwng and 2 runs on state).
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	PM	6/21/2005	0.03	POUNDS PER MILLION BTU HEAT INPUT	RN: 100% oil drng the tst. not within +-10% of capacity.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	PM	4/4/2006	0.04	POUNDS PER MILLION BTU HEAT INPUT	RN: oil drng the test.; HV=7380 MMBTU/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	PM	7/17/2007	0.04	POUNDS PER MILLION BTU HEAT INPUT	RN: 100% oil was fired drng the tst.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	NOX	4/3/2006	0.096	POUNDS PER MILLION BTU HEAT INPUT	RN: NG drng the tst; Nox=570#/hr; HV=5924 MMBTU/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	NOX	7/17/2007	0.278	POUNDS PER MILLION BTU HEAT INPUT	RN: 100% oil drng the tst. NOx=2053#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	NOX	7/16/2007	0.1	POUNDS PER MILLION BTU HEAT INPUT	RN: 100% NG during the tst. NOx=593#/hr (n 10% of 100 % cap).
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	SO2	3/27/2003	0.666	POUNDS PER MILLION BTU HEAT INPUT	RN- metd 6C used ; oil during the test; SO2=48 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	SO2	6/21/2004	0.677	POUNDS PER MILLION BTU HEAT INPUT	RN: oil drng the tst, additives see PM test cmnt SO2=4927 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	SO2	3/30/2005	0.746	POUNDS PER MILLION BTU HEAT INPUT	RN: oil drng the test. SO2= 5421 #/hr; load=72 9040 mmbtu/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	SO2	4/27/2006	0.648	POUNDS PER MILLION BTU HEAT INPUT	RN: oil during the test. SO2=4752#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	SO2	5/15/2007	0.641	POUNDS PER MILLION BTU HEAT INPUT	RN: Oil drng the tst; SO2=4618#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	PM	3/27/2003	0.05	POUNDS PER MILLION BTU HEAT INPUT	RN- oil with edditives Bycosin 98014T(14gal/ and EES CC910 (18 gal/hr)during the test (1ru st blwng and 2-runs on st state).
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	NOX	4/6/2004	0.14	POUNDS PER MILLION BTU HEAT INPUT	RN: NG during the test; NOx=809#/hr; NG= 5,54MMCF/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	NOX	4/7/2004	0.291	POUNDS PER MILLION BTU HEAT INPUT	RN: Oil during the test;NOx=2076#/hr; oil=11 BBL/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	NOX	3/25/2003	0.291	POUNDS PER MILLION BTU HEAT INPUT	RN- oil during the test.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	NOX	3/24/2003	0.103	POUNDS PER MILLION BTU HEAT INPUT	RN-NG during the tst; NOx=591#/hr;Tst load r within +-100%
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	NOX	6/21/2005	0.292	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=2093 #/hr, 79.25 % of the load durin test. (not within 10%).
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	NOX	6/20/2005	0.146	POUNDS PER MILLION BTU HEAT INPUT	RN: NG drng the tst. NOx=893 #/hr ; Load not within 10% (67.29%)
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	NOX	4/4/2006	0.283	POUNDS PER MILLION BTU HEAT INPUT	RN: Oil drng the tst. NOx=2089 #/hr; HV=738 MMBTU/hr

FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	NOX	3/27/2003	0.291	POUNDS PER MILLION BTU HEAT INPUT	RN-oil during the test;NOx=2136#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	NOX	3/26/2003	0.13	POUNDS PER MILLION BTU HEAT INPUT	RN- NG during the test;NOx=740#/hr; testload within +-100% .
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	NOX	8/9/2004	0.152	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=880#/hr , NG drng the tst.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	NOX	3/29/2005	0.181	POUNDS PER MILLION BTU HEAT INPUT	RN: NG during the test ; NOx=1004#/hrLoad d the test 5542 vs 9040 mmbtu/hr.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	NOX	4/27/2006	0.284	POUNDS PER MILLION BTU HEAT INPUT	RN: 100 % oil was burned during the test. NOx=2086#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	2	Fossil Fuel Fired Steam Generator #2(Acid Rain, Phase II)	A	NOX	5/14/2007	0.16	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=920#/hr on NG; about 533 MW and MMBTU/hr av of the 3 runs. NOt +_ of capacit
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/24/2005	2.18	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG with DB drng the tst. NOx=0.008#/MMBTU=17.52 #/tons
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/25/2006	1.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst; NOx=11.11#/hr =0.0063#/MMBTU
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	SO2	4/7/2004	0.688	POUNDS PER MILLION BTU HEAT INPUT	RN: oil during the test;SO2=4910#/hr;Oil=1122BBL/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	SO2	3/25/2003	0.679	POUNDS PER MILLION BTU HEAT INPUT	RN- 100 % oil during the test. SO2=4900#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	SO2	6/21/2005	0.742	POUNDS PER MILLION BTU HEAT INPUT	RN: oil drng the test. SO2+ 5314 #/hr not withi 10% of capcity (79.25%)
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	SO2	4/4/2006	0.669	POUNDS PER MILLION BTU HEAT INPUT	RN: 2006 test; oil drng the tst; SO2=4940 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	1	Fossil Fuel Fired Steam Generator #1(Acid Rain, Phase II)	A	SO2	7/17/2007	0.692	POUNDS PER MILLION BTU HEAT INPUT	RN: 100% oil drng the tst. SO2=5115#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	NH3	4/2/2007	0.028	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the test
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/31/2005	2.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: Tst on oil and without DB
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/28/2005	0.11	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG without DB drng the tst
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	VOC	5/29/2005	0.87	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG with DB drng the tst; VOC=0.001 #/mmbtu=2.31 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	CO	4/2/2007	1.36	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst; CO=5.1 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	CO	5/31/2005	0.51	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: tst on oil and without DB; CO= 0.001#/MMBTU= 2.54 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	CO	5/23/2005	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG without DB drng the tst results showed minus (no CO) for this mode.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	CO	5/24/2005	1.79	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG with DB during the tst.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	CO	5/26/2005	0.11	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: tst on oil and w/DB; CO= 0. 00 #/mmbtu= #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	CO	5/25/2006	1.53	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the test; CO=5.81#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	CO	4/4/2007	1.39	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the test; CO=5.2 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/23/2005	0.06	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG without DB.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/28/2005	0.08	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG without DB drng the test.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/29/2005	0.11	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG with DB drng the test. Note Allw seq a limit are the same for with and wihtout DB for
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/31/2005	1.61	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: Test on OIL and without DB
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/22/2006	0.06	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the test; test method CTM-027 w used.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	NH3	4/3/2007	0.139	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the test;
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	CO	6/11/2003	1.29	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN- 2003 stack test on NG.CO=5.02#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	CO	6/18/2004	1.49	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the test; CO= 5.75 #/hr
													PARTS PER	

FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	CO	5/28/2005	1.1	MILLION DRY GAS VOLUME @ 15% O2	RN: NG without DB; CO=0.002#/MMBTU=4.29#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	CO	5/29/2005	1.87	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG with DB drng the tst; CO=0.004#/MMBTU=8.63 #/HR
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/24/2005	0.13	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG with DB drng the tst.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/26/2005	0.85	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: Tst on oil and without DB
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/24/2006	0.07	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the test
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	NH3	4/3/2007	0.121	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the test, no duct burners.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	CO	5/23/2005	0.27	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN:NG without DB; VOC= 0 #/mmbtu=0.60 #
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	CO	5/24/2005	1.65	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG with DB; CO= 0.004 #/MMBTu; 8.08
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	CO	5/26/2005	0.47	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: tst on oil and without DB; CO=0.001 #/MMBTU=2.21 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	CO	5/24/2006	1.62	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst; CO= 5.99#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	CO	4/3/2007	1.53	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the test; CO= 5.7 #/hr vs 27.5 l
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/26/2005	0.48	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: Tst on oil & w/DB
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/25/2006	0.06	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst;
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	NH3	4/4/2007	0.212	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the test
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/23/2005	2.36	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG without DB; NOX=0.009 #/mmbtu= 1 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/24/2005	2.34	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG with DB ;NOX=0.009 #/mmbtu=18.83#/HR
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/26/2005	9.62	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: Tst on OIL and without DB; NOX= 0.037#/mmbtu=74.25#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/24/2006	1.87	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the test; NOx=11.93#/hr; =0.0069#/MMBTU
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	NOX	4/3/2007	2.11	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: during the RATA -9 runs ave . Need check permit. NOx=13.6#/hr== 0.0078#/MMBTU
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	CO	5/29/2005	1.47	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the test with DB;CO=0.003#/MMBTU=7.07#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/31/2005	8.61	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: oil drng the tst. NOx=0.033#/MMBTU=63.86#/hr (without DB
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/30/2006	1.86	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the test; NOx=11.82 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	NOX	4/3/2007	2.03	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the tst, NOx=0.0075#/MMBTU 13.3 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	VOC	5/23/2005	0.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG without duct burner ;VOC=0.001 #/MMBTU=0.96 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	VOC	5/24/2005	0.98	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG with Duct Burner (DB);VOC=0.001 #/MMBTU=2.70 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	VOC	5/26/2005	0.28	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: Tst on oil and w/DB; VOC=0.0#/mmbtu=(#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	VOC	5/23/2005	0.27	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG without burner ; VOC= 0. #/MMBTU= 0.60 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	VOC	5/24/2005	1.12	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG with DB; VOC= 0.001 #/MMBTU= 3 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	17	Unit 8C - 170 MW gas turbine with gas-fired HRSG	A	VOC	5/26/2005	0.33	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: Tst on oil and without DB; VOC= 0.001##/MMBTU=2.45 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	NOX	6/10/2003	6.96	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN-2003 tst, NOx=46.88#/hr; HV=1713 mmbt and =1834 mmbtu/hr corrected to 35 F.

FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	NOX	6/17/2004	8.11	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the test; NOX= 54.13 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/28/2005	2.36	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst, NOx=0.009 #/MMBTU=15.79#/hr vs 16.3 #/hr (without du burner (DB)).
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/29/2005	2.27	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst with DB;NOx=0.008#/MMBTU=17.95 #/hr vs 23.6 prmt limit.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	6	Combustion Turbine with HRSG (CT 4B)(Acid Rain, Phase II)	A	NOX	9/24/2003	14.03	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: 2003 tsts. NOx=72.8#/hr; NG during the te NOx eqvlnt allwble=177#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	6	Combustion Turbine with HRSG (CT 4B)(Acid Rain, Phase II)	A	NOX	8/5/2004	12.69	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst. NOx=65.2#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	6	Combustion Turbine with HRSG (CT 4B)(Acid Rain, Phase II)	A	NOX	12/6/2004	12.04	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NOx= 69.4 #/hr (40 F test condtns); NG dr the tst.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	6	Combustion Turbine with HRSG (CT 4B)(Acid Rain, Phase II)	A	NOX	10/19/2005	10.42	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tsts at 1805 mmbtu/hr at 40 FNOx= 54.8 #/hr(not within 100+-10% of the capacity).).
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	6	Combustion Turbine with HRSG (CT 4B)(Acid Rain, Phase II)	A	NOX	10/12/2006	10.74	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NOx=57.2#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	6	Combustion Turbine with HRSG (CT 4B)(Acid Rain, Phase II)	A	NOX	10/10/2007	8.87	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst; NOx= 54.34#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/23/2005	0.12	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG without DB drng the tst.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	18	Unit 8D - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/24/2005	0.18	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG with DB drng the tst.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	CO	5/31/2005	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: OIL drng the tst; CO=0 #/hr =0#/MMBTU tsts without DB; Condtd by Air Hygiene International, Inc. all initial tests on oil and Ng(all units # 8.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	CO	5/30/2006	1.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the test. CO=5.94#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	CO	4/3/2007	1.29	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the test. CO=4.9#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	5	Combustion Turbine with HRSG (CT 4A)(Acid Rain, Phase II)	A	NOX	9/25/2003	11.15	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN- 2003 tst; NOx=60.3 #/hr; NG during the te
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	5	Combustion Turbine with HRSG (CT 4A)(Acid Rain, Phase II)	A	NOX	8/4/2004	12.18	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN(NG drng thetst) NOx=62.3#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	5	Combustion Turbine with HRSG (CT 4A)(Acid Rain, Phase II)	A	NOX	12/2/2004	10.89	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst. NOx=69.6#/hr ; ISO cond NOx= 12.19 ppm
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	5	Combustion Turbine with HRSG (CT 4A)(Acid Rain, Phase II)	A	NOX	10/9/2005	9.357	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst, NOx= 51.3#/hr (177#/hr l HI=1750MMBTU/HR at 40 F
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	5	Combustion Turbine with HRSG (CT 4A)(Acid Rain, Phase II)	A	NOX	10/11/2006	12.79	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NOx=70#/hr ; NG drng the tsts.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	NOX	6/11/2003	6.36	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN- 2003 tst,NOx=41.80#/hr HV=1788 MMBTU/HR crtd to 35F; NG drng the tst.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	NOX	6/18/2004	1.49	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the test; NOx=50.91#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/28/2005	2.44	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG and without DB drng the test. NOx= 0.009#/MMBTu=15.68#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/29/2005	2.41	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG with DB . NOx=0.009#/MMBTU=18. #/HR
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/31/2005	8.54	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: oil and without DB; NOx=0.033#/MMBTU=69.68 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	NOX	5/23/2006	1.93	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the test ; NOx=0.0071#/MMBT
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	NOX	4/2/2007	2.17	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the test; NOx=0.0080#/MMBT 14#/hr (during RATA)
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	CO	6/10/2003	1.42	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN-NG drng the tst, CO=5.56#/hr crtd to 35F;HV=1713 and =1834 MMBTU/hrcrtd to 3
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	CO	6/17/2004	1.56	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the test ; CO= 6.04 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	CO	5/28/2005	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG without DB drng the tst. CO=0.00#/MMBTU=0.82#/hr vs 27.5 #/hr limi
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	5	Combustion Turbine with HRSG (CT 4A)(Acid Rain, Phase II)	A	NOX	10/9/2007	11.88	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst; NOX=71.69#/hr

FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	4	Combustion Turbine with HRSG (CT 3B)(Acid Rain, Phase II)	A	NOX	10/23/2003	19.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN-NG drng the test;NOx=108.8#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	4	Combustion Turbine with HRSG (CT 3B)(Acid Rain, Phase II)	A	NOX	8/3/2004	13.35	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst. NOx= 70.1 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	4	Combustion Turbine with HRSG (CT 3B)(Acid Rain, Phase II)	A	NOX	12/1/2004	11.29	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NOX=73.7 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	4	Combustion Turbine with HRSG (CT 3B)(Acid Rain, Phase II)	A	NOX	10/18/2005	11.19	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst; NOx=64.1 vs 177#/hr :1797MMBTU/hr @40F
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	4	Combustion Turbine with HRSG (CT 3B)(Acid Rain, Phase II)	A	NOX	10/10/2006	9.407	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the tst, NOx=53.2#/hr vs 177#/ (lmit on Gas).
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	4	Combustion Turbine with HRSG (CT 3B)(Acid Rain, Phase II)	A	NOX	10/16/2007	11.11	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst; NOX=67.51 @40F
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	VOC	5/28/2005	0.39	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG without DB; VOC=0.001 #/MMBTU=2.48#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	VOC	5/29/2005	0.47	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst with DB, VOC=0.002 #/MMBTU=3.56#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	11	Unit 8A - 170 MW gas turbine with gas-fired HRSG	A	VOC	5/31/2005	0.19	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: Tsts on OIL and without DB; VOC=0.001#/mmbtu=1.39 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	3	Combustion Turbine with HRSG (CT 3A)(Acid Rain, Phase II)	A	NOX	10/9/2003	14.94	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN-NG during the test; NOx=84#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	3	Combustion Turbine with HRSG (CT 3A)(Acid Rain, Phase II)	A	NOX	8/2/2004	13.62	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst. NOx=72.4#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	3	Combustion Turbine with HRSG (CT 3A)(Acid Rain, Phase II)	A	NOX	11/30/2004	13.25	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG Nox=86.8#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	3	Combustion Turbine with HRSG (CT 3A)(Acid Rain, Phase II)	A	NOX	10/17/2005	10.79	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst; NOx= 62.6#/hr vs 177#/h at 1771MMBTU/HR @40F
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	3	Combustion Turbine with HRSG (CT 3A)(Acid Rain, Phase II)	A	NOX	10/9/2006	9.68	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the test ; NOx=55#/hr vs 177(gas
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	3	Combustion Turbine with HRSG (CT 3A)(Acid Rain, Phase II)	A	NOX	10/8/2007	9.31	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG drng the tst; NOx=56.63#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	CO	5/23/2006	1.78	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the test; CO=6.72#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	VOC	5/28/2005	0.68	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG without DB ;VOC=0.001#/mmbtu=1.5 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	VOC	5/31/2005	0.12	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: tst on oil and withiut DB; VOC=0 #/MMB 0.94#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/29/2005	0.17	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG with DB .
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	12	Unit 8B - 170 MW gas turbine with gas-fired HRSG	A	NH3	5/23/2006	0.04	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	RN: NG during the test.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	4	Combustion Turbine with HRSG (CT 3B)(Acid Rain, Phase II)	A	CO	10/16/2007	1.3	PARTS PER MILLION DRY GAS VOLUME	RN: NG drng the tst. CO= 4.29#/hr @ 40 F
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	4	Combustion Turbine with HRSG (CT 3B)(Acid Rain, Phase II)	A	CO	12/1/2004	3.39	PARTS PER MILLION DRY GAS VOLUME	RN: CO= 12.5 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	4	Combustion Turbine with HRSG (CT 3B)(Acid Rain, Phase II)	A	CO	10/10/2006	1.863	PARTS PER MILLION DRY GAS VOLUME	RN: NG drng the tst; CO=6.3#/hr vs 94.3#/hr (l on Gas).
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	4	Combustion Turbine with HRSG (CT 3B)(Acid Rain, Phase II)	A	CO	10/18/2005	1.88	PARTS PER MILLION DRY GAS VOLUME	RN:NG drng the tst; CO= 6.6#/hr vs 94.5#/hr; MMBTU/HR @40F
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	4	Combustion Turbine with HRSG (CT 3B)(Acid Rain, Phase II)	A	CO	8/3/2004	2.55	PARTS PER MILLION DRY GAS VOLUME	RN: NG drng the test; CO=8.5#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	3	Combustion Turbine with HRSG (CT 3A)(Acid Rain, Phase II)	A	CO	10/8/2007	2.5	PARTS PER MILLION DRY GAS VOLUME	RN: NG drng the test; CO= 8.20 #/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	5	Combustion Turbine with HRSG (CT 4A)(Acid Rain, Phase II)	A	CO	10/19/2005	2.5	PARTS PER MILLION DRY GAS VOLUME	RN: NG drng the tst ;CO=8.4 #/hr at 1750mmb at 40 F(not within 100+-10%)
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	5	Combustion Turbine with HRSG (CT 4A)(Acid Rain, Phase II)	A	CO	10/11/2006	2.563	PARTS PER MILLION DRY GAS VOLUME	RN: 100% NG; CO=8.7#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	5	Combustion Turbine with HRSG (CT 4A)(Acid Rain, Phase II)	A	CO	10/9/2007	1.15	PARTS PER MILLION DRY GAS VOLUME	RN: NG drng the tst; CO=3.81#/hr @40F
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	6	Combustion Turbine with HRSG (CT 4B)(Acid Rain, Phase II)	A	CO	9/24/2003	1.37	PARTS PER MILLION DRY GAS VOLUME	RN-NG drng the tst, CO=4.9#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	6	Combustion Turbine with HRSG (CT 4B)(Acid Rain, Phase II)	A	CO	8/5/2004	2.16	PARTS PER MILLION DRY GAS VOLUME	RN: NG drng the test, CO=7.2#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	6	Combustion Turbine with HRSG (CT 4B)(Acid Rain, Phase II)	A	CO	12/6/2004	2.38	PARTS PER MILLION DRY GAS VOLUME	RN: NG drng the tst; CO=8.2 #/hr (40 F test condtns)
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	6	Combustion Turbine with HRSG (CT 4B)(Acid Rain,	A	CO	10/19/2005	2.223	PARTS PER MILLION DRY	RN: NG drng the tst; CO= 7.7#/hr at 1805mmb at 40 F(not within 100+-10% of the load).

								Phase II)					GAS VOLUME	
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	6	Combustion Turbine with HRSG (CT 4B)(Acid Rain, Phase II)	A	CO	10/12/2006	1.77	PARTS PER MILLION DRY GAS VOLUME	RN; CO=6#/hr;HV=1791mmbtu/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	6	Combustion Turbine with HRSG (CT 4B)(Acid Rain, Phase II)	A	CO	10/10/2007	2.02	PARTS PER MILLION DRY GAS VOLUME	RN: NG drng the tst; CO=6.63#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	5	Combustion Turbine with HRSG (CT 4A)(Acid Rain, Phase II)	A	CO	9/25/2003	1.21	PARTS PER MILLION DRY GAS VOLUME	RN-2003 tst;CO=4.13#/hr; NG drng the test.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	5	Combustion Turbine with HRSG (CT 4A)(Acid Rain, Phase II)	A	CO	8/4/2004	2.6	PARTS PER MILLION DRY GAS VOLUME	RN: NG; CO=8.6#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	5	Combustion Turbine with HRSG (CT 4A)(Acid Rain, Phase II)	A	CO	12/2/2004	5.036	PARTS PER MILLION DRY GAS VOLUME	RN: NG during the tst; CO=17.7#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	3	Combustion Turbine with HRSG (CT 3A)(Acid Rain, Phase II)	A	CO	10/9/2003	2	PARTS PER MILLION DRY GAS VOLUME	RN- NG during the test. CO=6.6#/hr
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	3	Combustion Turbine with HRSG (CT 3A)(Acid Rain, Phase II)	A	CO	8/2/2004	2.35	PARTS PER MILLION DRY GAS VOLUME	RN: CO=7.6#/hr on NG .
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	3	Combustion Turbine with HRSG (CT 3A)(Acid Rain, Phase II)	A	CO	11/30/2004	3.72	PARTS PER MILLION DRY GAS VOLUME	RN: CO=14.1 #/hr @ 40Ftest cond.
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	3	Combustion Turbine with HRSG (CT 3A)(Acid Rain, Phase II)	A	CO	10/17/2005	1.93	PARTS PER MILLION DRY GAS VOLUME	RN: NG drng the tst; CO=6.6#/hr vs 94.3#/hr a 1771 MMBTU/HR @ 40 F
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	3	Combustion Turbine with HRSG (CT 3A)(Acid Rain, Phase II)	A	CO	10/9/2006	2.01	PARTS PER MILLION DRY GAS VOLUME	RN: NG drng the test; CO=6.5#/hr vs 94.3#/hr on Gas).
FLORIDA POWER & LIGHT (PMR)	0850001	MARTIN POWER PLANT	SED	MARTIN	A	Y	4	Combustion Turbine with HRSG (CT 3B)(Acid Rain, Phase II)	A	CO	10/23/2003	2.37	PARTS PER MILLION DRY GAS VOLUME	RN- NG drng the test; CO=8.6 #/hr
LOUIS DREYFUS CITRUS, INC.	0850002	LOUIS DREYFUS CITRUS / INDIANTOWN PLANT	SED	MARTIN	A	Y	8	PELLET COOLER #2	A	PM	2/6/2003	0.2052	POUNDS PER HOUR PER TON OF MATERIAL STORED	RN- PM=0.0021 grains /dscf;nozzle diam=0.18 inch.
LOUIS DREYFUS CITRUS, INC.	0850002	LOUIS DREYFUS CITRUS / INDIANTOWN PLANT	SED	MARTIN	A	Y	8	PELLET COOLER #2	A	PM	1/16/2004	0.151	POUNDS PER HOUR PER TON OF MATERIAL STORED	RN: allwble test em is 17.4#/hr . PM may be w by FS after October 2004 if complied with VE<5%;2006 VE has 0% opacity
LOUIS DREYFUS CITRUS, INC.	0850002	LOUIS DREYFUS CITRUS / INDIANTOWN PLANT	SED	MARTIN	A	Y	5	30 T/HR CITRUS PEEL DRYER #2	A	PM	3/27/2007	8.307	POUNDS/HOUR	RN: NG during the test; moisture=44.61% PM=0.0538 grains/dscf ;
LOUIS DREYFUS CITRUS, INC.	0850002	LOUIS DREYFUS CITRUS / INDIANTOWN PLANT	SED	MARTIN	A	Y	5	30 T/HR CITRUS PEEL DRYER #2	A	PM	4/8/2004	14.97	POUNDS/HOUR	RN: retest due to operation over 110 % 1 st test
LOUIS DREYFUS CITRUS, INC.	0850002	LOUIS DREYFUS CITRUS / INDIANTOWN PLANT	SED	MARTIN	A	Y	5	30 T/HR CITRUS PEEL DRYER #2	A	PM	1/29/2004	9.737	POUNDS/HOUR	RN: ATC testing group.
LOUIS DREYFUS CITRUS, INC.	0850002	LOUIS DREYFUS CITRUS / INDIANTOWN PLANT	SED	MARTIN	A	Y	5	30 T/HR CITRUS PEEL DRYER #2	A	PM	1/29/2003	4.761	POUNDS/HOUR	RN: 12 points per run. 60 min per run tstng. PM=0.028 grains/dscf, ISO (90.26,98,97 and 96.57)%.
LOUIS DREYFUS CITRUS, INC.	0850002	LOUIS DREYFUS CITRUS / INDIANTOWN PLANT	SED	MARTIN	A	Y	5	30 T/HR CITRUS PEEL DRYER #2	A	PM	1/27/2005	4.599	POUNDS/HOUR	RN: PM=0.0299 garins/dscf
LOUIS DREYFUS CITRUS, INC.	0850002	LOUIS DREYFUS CITRUS / INDIANTOWN PLANT	SED	MARTIN	A	Y	5	30 T/HR CITRUS PEEL DRYER #2	A	PM	5/9/2006	13.923	POUNDS/HOUR	DG
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	H114	12/10/2003	0.000002	POUNDS PER MILLION BTU HEAT INPUT	RN: ARMS allwd inpt only 6 digits after the dc Hg=1.53E-06 #/MMBTU;Hg= 5.051E-03 #/ hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	PB	12/10/2003	0	POUNDS PER MILLION BTU HEAT INPUT	RN: ARMS does not allwd input result: Pb=4.1 07#/MMBTU; Pb=1.375E-03 #/ hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	H015	12/10/2003	0.000211	POUNDS PER BILLION BTU HEAT INPUT	RN: ARMS does not allwd input result: Ar= 2. 07#/MMBtu; Ar=6.958#/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	NOX	11/17/2007	0.1558	POUNDS PER MILLION BTU HEAT INPUT	RN: NOX= 533.3#/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	PM10	12/8/2003	0.0007	POUNDS PER MILLION BTU HEAT INPUT	RN: it is not clear from the rprt which mthd wa used 201 A or #5 , Discussed with Nick Laryea Will be back. PM10= >2.1884 #/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	7	Aux Boilers (2)	A	NOX	4/25/2007	0.0368	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=6.47#/hr (NOx limit is 30 day rollin ave.);Mtd 7e instead mtd 7 as rqrd was conduct SEE actvty (call) on 6/20/07; not noticed drng t tstng.
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	7	Aux Boilers (2)	A	NOX	8/17/2007	0.0395	POUNDS PER MILLION BTU HEAT INPUT	RN: Propane drng the tst; NOx= 5.55#/hr; HI= 123.600 MMBTU/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	7	Aux Boilers (2)	A	NOX	8/18/2007	0.0387	POUNDS PER MILLION BTU HEAT INPUT	RN: NG drng the test; NOX=6.56#/hr HI=154.2 MMBTU/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	7	Aux Boilers (2)	A	NOX	8/19/2007	0.0347	POUNDS PER MILLION BTU HEAT INPUT	RN: Propane drng the tst. NOx=5.30#/hr HI=124.200 MMBTU/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	7	Aux Boilers (2)	A	NOX	8/20/2007	0.0343	POUNDS PER MILLION BTU HEAT INPUT	RN: NG during the test; NOx=5.56#/hr HI= 15 MMBTU/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	SO2	12/11/2003	0.1116	POUNDS PER MILLION BTU HEAT INPUT	RN: SO2=391.237 #/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	SO2	11/15/2004	0.156	POUNDS PER MILLION BTU HEAT INPUT	RN: basd on Fd; SO2= 478. 2#/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	SO2	12/15/2005	0.142	POUNDS PER MILLION BTU HEAT INPUT	RN: Fc factor; PSO2= 489.7#/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	SO2	12/7/2006	0.1391	POUNDS PER MILLION BTU HEAT INPUT	RN: SO2= 489.2#/hr (0.1391#/MMBTU based Fc) and 0.1372#/mmbtu based on Fd.
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	SO2	11/17/2007	0.1327	POUNDS PER MILLION BTU HEAT INPUT	RN: SO2= 454#/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	PM	12/8/2003	0.0006	POUNDS PER MILLION BTU HEAT INPUT	RN-2003 tst;PM=1.9125 #/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	PM	11/15/2004	0.00083	POUNDS PER MILLION BTU HEAT INPUT	rN: PM based on Fc PM based on Fd=0.00080#/mmbtu, PM=2.40#/hr
INDIANTOWN		INDIANTOWN											POUNDS PER	

COGENERATION, L.P.	0850102	COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	PM	12/15/2005	0.0053	MILLION BTU HEAT INPUT	RN: PM=18.3589 #/Hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	PM	12/7/2006	0.0004	POUNDS PER MILLION BTU HEAT INPUT	RN: PM= <1.3782#/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	PM	11/13/2007	0.0007	POUNDS PER MILLION BTU HEAT INPUT	RN: PM= 2.26 #/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	FL	12/9/2003	0.00002	POUNDS PER MILLION BTU HEAT INPUT	RN: FL=<0.058 #/ hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	7	Aux Boilers (2)	A	CO	4/25/2007	0.0101	POUNDS PER MILLION BTU HEAT INPUT	RN: mtd 10, limit is 30 day rolling av. See com for NOx; CO=1.77#/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	7	Aux Boilers (2)	A	CO	8/18/2007	0.00792	POUNDS PER MILLION BTU HEAT INPUT	RN: NG drng the tst. CO= 1.3 #/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	7	Aux Boilers (2)	A	CO	8/17/2007	0.00306	POUNDS PER MILLION BTU HEAT INPUT	RN: Propane during the test. CO=0.43#/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	7	Aux Boilers (2)	A	CO	8/20/2007	0.0192	POUNDS PER MILLION BTU HEAT INPUT	RN: NG drng the tst. CO=3.12#/hr HI=152.300 MMBTU/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	7	Aux Boilers (2)	A	CO	8/19/2007	0.00175	POUNDS PER MILLION BTU HEAT INPUT	RN: Propane during the tst; CO=0.27#/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	CO	12/11/2003	0.0126	POUNDS PER MILLION BTU HEAT INPUT	RN: CO=44.203 #/ hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	CO	8/25/2006	0.0843	POUNDS PER MILLION BTU HEAT INPUT	RN: CO=338#/hr vs 376 #/hr limit(this is 24 h test due to CO limit av of 24 hr form midnight t midnight). Steam production =53444 KSCF/HF
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	CO	9/6/2007	0.0393	POUNDS PER MILLION BTU HEAT INPUT	RN: CO=138.63#/hr vs 376 #/hr by Coastal Ai Consulting Inc.
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	VOC	12/10/2003	0.0019	POUNDS PER MILLION BTU HEAT INPUT	RN: VOC= < 6.0445 #/hr; results were below t mtd detection limit of 1 ppmwv
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	H021	12/10/2003	0	POUNDS PER MILLION BTU HEAT INPUT	RN: ARMS does not alwd to input Be= 1.539E #/ MMbtu, Be= < 5.086 E-05#/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	NOX	12/7/2006	0.1372	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=482.5#/hr (NOx is based on Fc=0.1372#/mmbtu and = 0.1354 #/MMBTU b on Fd).
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	NOX	11/15/2004	0.164	POUNDS PER MILLION BTU HEAT INPUT	RN : basd on Fd(higher) NOx=503.3 #/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	NOX	12/11/2003	0.158	POUNDS PER MILLION BTU HEAT INPUT	RN: NOx=555.511 #/ hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	NOX	12/15/2005	0.1477	POUNDS PER MILLION BTU HEAT INPUT	RN: Fc factor; NOx= 509.4#/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	SAM	12/9/2003	0.00033	POUNDS PER MILLION BTU HEAT INPUT	RN: H2 SO4= 1.0884 #/hr; Audit was not provi by DEP.
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	7	Aux Boilers (2)	A	VOC	8/19/2007	0.000246	POUNDS/HOUR	RN: Propane drng the tst. VOC=0.04#/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	7	Aux Boilers (2)	A	VOC	8/18/2007	0.00105	POUNDS/HOUR	RN; NG drng the test; VOC= 0.15 #/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	1	Pulverized Coal Main Boiler	A	NH3	12/10/2003	0.0319	PARTS PER MILLION DRY GAS VOLUME	RN: CTM-027 method conducted to determine ammonia, need see which mthd is allwd.
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	7	Aux Boilers (2)	A	VOC	4/25/2007	0.56	POUNDS/HOUR	RN: VOC limit is 12 mo rolling av(draft TV pr will rqr cndtd every 5 yrs)See comnts for NOX CO=0.0032#/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	7	Aux Boilers (2)	A	VOC	8/20/2007	0.00113	POUNDS/HOUR	RN: NG drng the tst. VOC=0.17#/hr
INDIANTOWN COGENERATION, L.P.	0850102	INDIANTOWN COGENERATION PLANT	SED	MARTIN	A	Y	7	Aux Boilers (2)	A	VOC	8/17/2007	0.000605	POUNDS/HOUR	RN: Propane drng the tst ; VOC=0.08#/hr
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	6	8.8 MW DIESEL GENERATOR UNIT 2	A	NOX	8/1/2007	4.97	GRAMS PER HORSEPOWER-HOUR	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	5	8.8 MW DIESEL GENERATOR UNIT 1.	A	NOX	10/11/2007	4.83	GRAMS PER HORSEPOWER-HOUR	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	5	8.8 MW DIESEL GENERATOR UNIT 1.	A	NOX	10/7/2005	4.96	GRAMS PER HORSEPOWER-HOUR	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	5	8.8 MW DIESEL GENERATOR UNIT 1.	A	NOX	8/15/2003	5.1	GRAMS PER HORSEPOWER-HOUR	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	5	8.8 MW DIESEL GENERATOR UNIT 1.	A	NOX	6/24/2004	4.975	GRAMS PER HORSEPOWER-HOUR	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	5	8.8 MW DIESEL GENERATOR UNIT 1.	A	NOX	3/16/2006	5.23	GRAMS PER HORSEPOWER-HOUR	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	11	GE LM 6000 PC SPRINT Combustion Turbine	A	CO	6/23/2006	19	PARTS PER MILLION DRY GAS VOLUME @ 15% O2 ISO	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	6	8.8 MW DIESEL GENERATOR UNIT 2	A	NOX	10/6/2005	4.49	GRAMS PER HORSEPOWER-HOUR	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	6	8.8 MW DIESEL GENERATOR UNIT 2	A	NOX	6/25/2004	4.826	GRAMS PER HORSEPOWER-HOUR	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	6	8.8 MW DIESEL GENERATOR UNIT 2	A	NOX	8/14/2003	5.03	GRAMS PER HORSEPOWER-HOUR	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	6	8.8 MW DIESEL GENERATOR UNIT 2	A	NOX	3/16/2006	4.95	GRAMS PER HORSEPOWER-HOUR	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	11	GE LM 6000 PC SPRINT Combustion Turbine	A	VOC	6/23/2006	0.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	6	8.8 MW DIESEL GENERATOR UNIT 2	A	PM	8/1/2007	0.0957	POUNDS PER MILLION BTU HEAT INPUT	

KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	6	8.8 MW DIESEL GENERATOR UNIT 2	A	PM	6/25/2004	0.0472	POUNDS PER MILLION BTU HEAT INPUT	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	5	8.8 MW DIESEL GENERATOR UNIT 1.	A	PM	10/11/2007	0.0482	POUNDS PER MILLION BTU HEAT INPUT	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	5	8.8 MW DIESEL GENERATOR UNIT 1.	A	PM	10/6/2005	0.0494	POUNDS PER MILLION BTU HEAT INPUT	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	5	8.8 MW DIESEL GENERATOR UNIT 1.	A	PM	8/15/2003	0.0368	POUNDS PER MILLION BTU HEAT INPUT	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	5	8.8 MW DIESEL GENERATOR UNIT 1.	A	PM	6/24/2004	0.0336	POUNDS PER MILLION BTU HEAT INPUT	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	5	8.8 MW DIESEL GENERATOR UNIT 1.	A	PM	3/16/2006	0.0557	POUNDS PER MILLION BTU HEAT INPUT	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	6	8.8 MW DIESEL GENERATOR UNIT 2	A	PM	8/14/2003	0.0332	POUNDS PER MILLION BTU HEAT INPUT	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	6	8.8 MW DIESEL GENERATOR UNIT 2	A	PM	10/6/2005	0.0436	POUNDS PER MILLION BTU HEAT INPUT	
KEYS ENERGY SERVICES	0870003	STOCK ISLAND POWER PLANT	SD	MONROE	A	Y	6	8.8 MW DIESEL GENERATOR UNIT 2	A	PM	3/16/2006	0.0467	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF KEY WEST	0870047	SOUTHERNMOST WASTE TO ENERGY FACILITY	SD	MONROE	I	Y	1	Municipal Solid Waste Combustor, Unit 1	I	PM	12/18/2003	0.0124	GRAINS PER DRY STANDARD CUBIC FOOT @ 12% CO2	
CITY OF KEY WEST	0870047	SOUTHERNMOST WASTE TO ENERGY FACILITY	SD	MONROE	I	Y	2	Municipal Solid Waste Combustor, Unit 2	I	PM	12/20/2003	0.0174	GRAINS PER DRY STANDARD CUBIC FOOT @ 12% CO2	Arlington Environmental Services
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	7	#4 RECY BLR W/ESP & B-W LOW ODOR DESIGN A	A	PM	5/24/2004	0.0056	GRAINS PER DRY STANDARD CUBIC FOOT	env. source samplers
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	7	#4 RECY BLR W/ESP & B-W LOW ODOR DESIGN A	A	PM	6/2/2005	0.0191	GRAINS PER DRY STANDARD CUBIC FOOT	Environmental Source Samplers, Inc., Corneliu NC. (704) 892-4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	7	#4 RECY BLR W/ESP & B-W LOW ODOR DESIGN A	A	PM	5/23/2007	0.01	GRAINS PER DRY STANDARD CUBIC FOOT	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	7	#4 RECY BLR W/ESP & B-W LOW ODOR DESIGN A	A	PM	6/13/2006	0.008	GRAINS PER DRY STANDARD CUBIC FOOT	/Environmental Source Samplers, Inc. 18631-H Northline Dr., Cornelius, NC 28031. (704) 892 8127.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	11	#5 RB-S OR C REC/BOILER-STRAIGHT (S)KRAFT OR CROSS(C) W/ESP P	A	PM	5/24/2004	0.0077	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	11	#5 RB-S OR C REC/BOILER-STRAIGHT (S)KRAFT OR CROSS(C) W/ESP P	A	PM	6/12/2006	0.011	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	/Environmental Source Samplers, Inc. 18631-H Northline Dr., Cornelius, NC 28031. (704) 892 8127.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	21	#4 LIME KILN W/ ESP. ALSO BURNS NCG(TRS) GASES.	A	TRS	5/22/2007	1	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	0.1942 lbs/hr TRS
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	21	#4 LIME KILN W/ ESP. ALSO BURNS NCG(TRS) GASES.	A	TRS	6/15/2006	0.7643	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	/Environmental Source Samplers, Inc. 18631-H Northline Dr., Cornelius, NC 28031. (704) 892 8127.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	21	#4 LIME KILN W/ ESP. ALSO BURNS NCG(TRS) GASES.	A	TRS	5/25/2004	0.0111	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	21	#4 LIME KILN W/ ESP. ALSO BURNS NCG(TRS) GASES.	A	TRS	6/2/2005	0.8514	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	Environmental Source Samplers, Inc., Corneliu NC. (704) 892-4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	21	#4 LIME KILN W/ ESP. ALSO BURNS NCG(TRS) GASES.	A	TRS	5/19/2003	0.6437	PARTS PER MILLION DRY GAS VOLUME @ 10% O2	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	11	#5 RB-S OR C REC/BOILER-STRAIGHT (S)KRAFT OR CROSS(C) W/ESP P	A	PM	5/21/2007	0.0078	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	11	#5 RB-S OR C REC/BOILER-STRAIGHT (S)KRAFT OR CROSS(C) W/ESP P	A	PM	5/31/2005	0.0133	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Environmental Source Samplers, Inc., Corneliu NC. (704) 892-4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	6	#5 PWR BLR (BARK/2.5%S FO) 457/348 MMBTU/H; ESP A	A	H106	7/10/2007	3.616	POUNDS/HOUR	.00625 lb/mmbtu (6.25E-03)
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	20	TALL OIL PLANT W/ PACKED TOWER TYPE WET SCRUBBER	A	TRS	6/30/2004	0.0122	POUNDS PER TON OF PRODUCT	Retest, failed on 5/27/04. Environmental Sourc Samplers, Inc. Cornelius, NC. 704-892-4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	20	TALL OIL PLANT W/ PACKED TOWER TYPE WET SCRUBBER	A	TRS	5/27/2004	0.0649	POUNDS PER TON OF PRODUCT	Production rate = 22.01 TPH Tall Oil / 4 hr bat 2000 lbs = 11,000 lbs/hr. Tester: Environmenta Source Samplers (ESS), 18631-H Northline Dr. Cornelius, NC 28031. Ph# 704--892-4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	24	BROWN STOCK WASHER SYSTEM C LINE	A	TRS	6/16/2006	1.269	PARTS PER MILLION DRY GAS VOLUME	Environmental Source Samplers, Inc. 18631-H Northline Dr., Cornelius, NC (704) 892-4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	33	PULPING SYSTEM (MACT I)	A	HAPS	10/16/2006	0.167	POUNDS PER TON OF PRODUCT	Calculation: 2479 ODTP/day devided by 24 hrs 103.29. 414 Total HAPS lbs/day devided by 24 = 17.25. 17.25 / 103.29 = 0.167 lbs/Ton of proc 98.6 % average "hardpiped" HAP was removed UNOX, as recorded in Allow Seq 001.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	15	#7 PWR BLR 1021MMBTU COAL FIRED W/ESP FOR PM CONTROL AIA P	A	H106	7/11/2007	84.12	POUNDS/HOUR	100% coal.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	11	#5 RB-S OR C REC/BOILER-STRAIGHT (S)KRAFT OR CROSS(C) W/ESP P	A	PM	5/19/2003	16.519	POUNDS/HOUR	Environmental Source Samplers, Inc.
								#5 RB-S OR C						

SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	11	REC/BOILER-STRAIGHT (S)KRAFT OR CROSS(C) W/ESP P	A	PM	5/21/2007	4.914	POUNDS/HOUR	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	11	#5 RB-S OR C REC/BOILER-STRAIGHT (S)KRAFT OR CROSS(C) W/ESP P	A	PM	5/26/2004	12.047	POUNDS/HOUR	Environmental Source Samplers, Inc. Cornelius (704) 892-4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	11	#5 RB-S OR C REC/BOILER-STRAIGHT (S)KRAFT OR CROSS(C) W/ESP P	A	PM	6/12/2006	18.534	POUNDS/HOUR	/Environmental Source Samplers, Inc. 18631-H Northline Dr., Cornelius, NC 28031. (704) 892-8127.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	14	#5 SDT SMELT DISSOLVING TANK W/ WET SCRUBBER P	A	TRS	4/26/2007	0.0148	POUNDS PER TON BLACK LIQUOR SOLIDS	0.0448 lbs/hr. Environmental Source Samplers, 18631-H Northline Dr., Cornelius, NC 28031. (892-8127.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	14	#5 SDT SMELT DISSOLVING TANK W/ WET SCRUBBER P	A	PM	6/12/2006	0.144	POUNDS PER TON BLACK LIQUOR SOLIDS	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	21	#4 LIME KILN W/ ESP. ALSO BURNS NCG(TRS) GASES.	A	PM	5/24/2004	0.0165	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	21	#4 LIME KILN W/ ESP. ALSO BURNS NCG(TRS) GASES.	A	PM	5/19/2003	0.0033	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	21	#4 LIME KILN W/ ESP. ALSO BURNS NCG(TRS) GASES.	A	PM	5/25/2004	0.0165	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	Environmental Source Samplers, Inc. Cornelius (704) 892-4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	21	#4 LIME KILN W/ ESP. ALSO BURNS NCG(TRS) GASES.	A	PM	6/2/2005	0.005	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	Environmental Source Samplers, Inc., Corneliu NC. (704) 892-4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	21	#4 LIME KILN W/ ESP. ALSO BURNS NCG(TRS) GASES.	A	PM	6/15/2006	0.0046	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	/Environmental Source Samplers, Inc. 18631-H Northline Dr., Cornelius, NC 28031. (704) 892-8127.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	21	#4 LIME KILN W/ ESP. ALSO BURNS NCG(TRS) GASES.	A	PM	6/15/2006	0.0046	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	/Environmental Source Samplers, Inc. 18631-H Northline Dr., Cornelius, NC 28031. (704) 892-8127.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	21	#4 LIME KILN W/ ESP. ALSO BURNS NCG(TRS) GASES.	A	PM	5/22/2007	0.0013	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	0.477 lbs/hr PM emission.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	21	#4 LIME KILN W/ ESP. ALSO BURNS NCG(TRS) GASES.	A	PM	5/22/2007	0.0013	GRAINS PER DRY STANDARD CUBIC FOOT @ 10% O2	0.477 lbs/hr PM emissions.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	15	#7 PWR BLR 1021MMBTU COAL FIRED W/ESP FOR PM CONTROL AIA P	A	PM	5/25/2007	0.01	POUNDS PER MILLION BTU HEAT INPUT	100% Coal Fired. 35.8 tons/hr coal feed. 9.370 lbs/hr PM emission.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	15	#7 PWR BLR 1021MMBTU COAL FIRED W/ESP FOR PM CONTROL AIA P	A	PM	7/11/2007	0.003	POUNDS PER MILLION BTU HEAT INPUT	100% coal at 37.2 TPH. ESP mean = 88.4 kW. COMS opacity = 6.7%.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	6	#5 PWR BLR (BARK/2.5%S FO) 457/348 MMBTU/H; ESP A	A	PM	5/19/2003	0.0055	POUNDS PER MILLION BTU HEAT INPUT	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	6	#5 PWR BLR (BARK/2.5%S FO) 457/348 MMBTU/H; ESP A	A	PM	6/1/2005	0.008	POUNDS PER MILLION BTU HEAT INPUT	50.33 T/hr bark feed. Environmental Source Samplers, Inc., Cornelius, NC. (704) 892-4405.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	6	#5 PWR BLR (BARK/2.5%S FO) 457/348 MMBTU/H; ESP A	A	PM	5/25/2004	0.0102	POUNDS PER MILLION BTU HEAT INPUT	Environmental Source Samplers, Inc. Cornelius (704) 892-4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	6	#5 PWR BLR (BARK/2.5%S FO) 457/348 MMBTU/H; ESP A	A	PM	6/14/2006	0.0614	POUNDS PER MILLION BTU HEAT INPUT	47.1 tons/hr bark feed. 110% = 51.8 T/hr bark feed. /Environmental Source Samplers, Inc. 18 H Northline Dr., Cornelius, NC 28031. (704) 8 8127.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	6	#5 PWR BLR (BARK/2.5%S FO) 457/348 MMBTU/H; ESP A	A	PM	6/14/2006	0	POUNDS PER MILLION BTU HEAT INPUT	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	6	#5 PWR BLR (BARK/2.5%S FO) 457/348 MMBTU/H; ESP A	A	PM	5/24/2007	0.011	POUNDS PER MILLION BTU HEAT INPUT	100% Bark fired. 4.382 lbs/hr PM. Process rate 45.32 Tons/hr Bark Feed.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	6	#5 PWR BLR (BARK/2.5%S FO) 457/348 MMBTU/H; ESP A	A	PM	5/24/2007	0.011	POUNDS PER MILLION BTU HEAT INPUT	100% Bark fired. 4.382 lbs/hr PM. Process rate 45.32 Tons/hr Bark Feed.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	6	#5 PWR BLR (BARK/2.5%S FO) 457/348 MMBTU/H; ESP A	A	PM	7/10/2007	0.003	POUNDS PER MILLION BTU HEAT INPUT	Fired on mixture of bark (39.4 TPH) and fuel o (23.4 GPM) during test. ESP power mean = 60.1kW.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	6	#5 PWR BLR (BARK/2.5%S FO) 457/348 MMBTU/H; ESP A	A	H114	7/10/2007	0	POUNDS PER MILLION BTU HEAT INPUT	Actual .0000002 mmbtu
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	6	#5 PWR BLR (BARK/2.5%S FO) 457/348 MMBTU/H; ESP A	A	PM	5/24/2007	0.011	POUNDS PER BILLION BTU HEAT INPUT	100% Bark fired. 4.382 lbs/hr PM. Process rate 45.32 Tons/hr Bark Feed.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	6	#5 PWR BLR (BARK/2.5%S FO) 457/348 MMBTU/H; ESP A	A	PM	6/14/2006	0.0614	POUNDS PER BILLION BTU HEAT INPUT	47.1 tons/hr bark feed. 110% = 51.8 T/hr bark feed. /Environmental Source Samplers, Inc. 18 H Northline Dr., Cornelius, NC 28031. (704) 8 8127.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	13	#4 SMELT DISSOLVING TANK W/VENTURI SCRUBBER	A	PM	5/23/2007	0.0688	POUNDS PER TON BLACK LIQUOR SOLIDS	Process rate = 132,686 lbs/hr BLS. Scrubber wastewater = 52 GPM. Scrubber Water Recirc GPM. Pressure Drop across Scrubber = 14.3 in. H2O
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	13	#4 SMELT DISSOLVING TANK W/VENTURI SCRUBBER	A	PM	6/13/2006	0.2551	POUNDS PER TON BLACK LIQUOR SOLIDS	133,454 lbs BLS/hr fired. /Environmental Sour Samplers, Inc. 18631-H Northline Dr., Corneli NC 28031. (704) 892-8127.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	13	#4 SMELT DISSOLVING TANK W/VENTURI SCRUBBER	A	PM	8/23/2006	0.1676	POUNDS PER TON BLACK LIQUOR SOLIDS	ESS Environmental Source Samplers, Inc. Cornelius, NC. Ph. 704-892-4405.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	13	#4 SMELT DISSOLVING TANK W/VENTURI SCRUBBER	A	PM	7/14/2005	0.1166	POUNDS PER TON BLACK LIQUOR SOLIDS	Retested due to prior test failure. Environmenta Source Samplers, Inc. Cornelius, NC.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	13	#4 SMELT DISSOLVING TANK W/VENTURI SCRUBBER	A	PM	6/2/2005	0.4152	POUNDS PER TON BLACK LIQUOR	126,128 lbs (BLS)/hr. Environmental Source Samplers, Inc., Cornelius, NC. (704) 892-4405

													SOLIDS	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	13	#4 SMELT DISSOLVING TANK W/VENTURI SCRUBBER	A	PM	5/24/2004	0.1853	POUNDS PER TON BLACK LIQUOR SOLIDS	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	14	#5 SDT SMELT DISSOLVING TANK W/ WET SCRUBBER P	A	PM	4/25/2007	0.1281	POUNDS PER TON BLACK LIQUOR SOLIDS	8.990 lbs/hr. Environmental Source Samplers, I
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	14	#5 SDT SMELT DISSOLVING TANK W/ WET SCRUBBER P	A	PM	6/12/2006	0.144	POUNDS PER TON BLACK LIQUOR SOLIDS	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	13	#4 SMELT DISSOLVING TANK W/VENTURI SCRUBBER	A	PM	5/23/2007	4.566	POUNDS/HOUR	Process rate = 132,686 lbs/hr BLS. Scrubber wastewater = 52 GPM. Scrubber Water Recirc GPM. Pressure Drop across Scrubber = 14.3 in. H2O.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	13	#4 SMELT DISSOLVING TANK W/VENTURI SCRUBBER	A	PM	7/10/2006	7.8	POUNDS/HOUR	133,200 BLS lbs/hr. Scrubber pressure drop 12 inches H2O.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	13	#4 SMELT DISSOLVING TANK W/VENTURI SCRUBBER	A	PM	8/23/2006	11.011	POUNDS/HOUR	ESS Environmental Source Samplers, Inc. Cornelius, NC. Ph. 704-892-4405.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	13	#4 SMELT DISSOLVING TANK W/VENTURI SCRUBBER	A	PM	5/19/2003	19.405	POUNDS/HOUR	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	13	#4 SMELT DISSOLVING TANK W/VENTURI SCRUBBER	A	PM	5/24/2004	13.276	POUNDS/HOUR	Environmental Source Samplers, Inc. Cornelius (704) 892-4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	13	#4 SMELT DISSOLVING TANK W/VENTURI SCRUBBER	A	TRS	8/23/2006	0.04	POUNDS/HOUR	ESS Environmental Source Samplers, Inc. Cornelius, NC. Ph. 704-892-4405.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	15	#7 PWR BLR 1021MMBTU COAL FIRED W/ESP FOR PM CONTROL AIA P	A	H114	7/11/2007	0.00295	POUNDS/HOUR	.00000299 lb/mmbtu or (2.99E-06) lb/mmbtu o 2.95E-03 lb/hr.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	14	#5 SDT SMELT DISSOLVING TANK W/ WET SCRUBBER P	A	PM	5/24/2004	9	POUNDS/HOUR	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	14	#5 SDT SMELT DISSOLVING TANK W/ WET SCRUBBER P	A	PM	5/19/2003	1.705	POUNDS/HOUR	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	14	#5 SDT SMELT DISSOLVING TANK W/ WET SCRUBBER P	A	PM	5/24/2004	9	POUNDS/HOUR	Environmental Source Samplers, Inc. Cornelius (704) 892-4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	14	#5 SDT SMELT DISSOLVING TANK W/ WET SCRUBBER P	A	PM	5/31/2005	10.139	POUNDS/HOUR	Environmental Source Samplers, Inc., Corneliu NC. (704) 892-4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	14	#5 SDT SMELT DISSOLVING TANK W/ WET SCRUBBER P	A	PM	6/12/2006	10.297	POUNDS/HOUR	/Environmental Source Samplers, Inc. 18631-H Northline Dr., Cornelius, NC 28031. (704) 892- 8127.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	11	#5 RB-S OR C REC/BOILER-STRAIGHT (S)KRAFT OR CROSS(C) W/ESP P	A	TRS	5/19/2003	0.4029	POUNDS/HOUR	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	6	#5 PWR BLR (BARK/2.5%S FO) 457/348 MMBTU/H; ESP A	A	H114	1/12/2005	0.000486	POUNDS/HOUR	NESHAP for Mercury (40 CFR 61, Subpart E). Used "Ontario-Hydro" Method. Report reviewe Errin Pichard. Annual Testing is still required a Errin Pichard's, July 20, 2005, letter to Smurfit. Environmental Source Samplers, Inc., Corneliu NC tested.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	6	#5 PWR BLR (BARK/2.5%S FO) 457/348 MMBTU/H; ESP A	A	H114	7/10/2007	0.0001	POUNDS/HOUR	
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	33	PULPING SYSTEM (MACT I)	A	HAPS	10/16/2006	98.6	PERCENT REDUCTION IN EMISSIONS	98.6 % average "hardpiped" HAP removed by UNOX. Environmental Source Samplers, Inc. 18631-H Northline Dr., Cornelius, NC 28031. / Enthalpy Analytical, Inc. 2202 Ellis Rd., Durha NC 27703. Ph. 919.850.4392
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	7	#4 RECY BLR W/ESP & B-W LOW ODOR DESIGN A	A	PM	5/19/2003	19.497	POUNDS/HOUR	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	7	#4 RECY BLR W/ESP & B-W LOW ODOR DESIGN A	A	PM	5/24/2004	5.213	POUNDS/HOUR	Environmental Source Samplers, Inc. Cornelius (704) 892-4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	7	#4 RECY BLR W/ESP & B-W LOW ODOR DESIGN A	A	PM	6/13/2006	10.976	POUNDS/HOUR	/Environmental Source Samplers, Inc. 18631-H Northline Dr., Cornelius, NC 28031. (704) 892- 8127.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	7	#4 RECY BLR W/ESP & B-W LOW ODOR DESIGN A	A	PM	5/23/2007	14.856	POUNDS/HOUR	Process rate = 66.3 BLS tons/hr fired.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	15	#7 PWR BLR 1021MMBTU COAL FIRED W/ESP FOR PM CONTROL AIA P	A	PM	5/19/2003	13.699	POUNDS/HOUR	Environmental Source Samplers, Inc.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	15	#7 PWR BLR 1021MMBTU COAL FIRED W/ESP FOR PM CONTROL AIA P	A	PM	6/1/2005	70.429	POUNDS/HOUR	37.37 T/hr coal feed x 2000 x 12,500 btu/lb (permit) / M = 943 MMBTU/hr. Environmental Source Samplers, Inc., Cornelius, NC. (704) 89 4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	15	#7 PWR BLR 1021MMBTU COAL FIRED W/ESP FOR PM CONTROL AIA P	A	PM	5/27/2004	28.863	POUNDS/HOUR	Environmental Source Samplers, Inc. Cornelius (704) 892-4405
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	15	#7 PWR BLR 1021MMBTU COAL FIRED W/ESP FOR PM CONTROL AIA P	A	PM	6/14/2006	25.551	POUNDS/HOUR	/Environmental Source Samplers, Inc. 18631-H Northline Dr., Cornelius, NC 28031. (704) 892- 8127.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	33	PULPING SYSTEM (MACT I)	A	HAPS	10/15/2007	97.88	PERCENT REDUCTION IN EMISSIONS	97.88 % average "hardpiped" HAP removed by UNOX.
SMURFIT-STONE CONTAINER ENTERPRISES, INC	0890003	FERNANDINA BEACH MILL	NED	NASSAU	A	Y	13	#4 SMELT DISSOLVING TANK W/VENTURI SCRUBBER	A	PM	6/13/2006	16.897	POUNDS/HOUR	Failed PM test using Allow Seq 002. /Environmental Source Samplers, Inc. 186 Northline Dr., Cornelius, NC 28031. (704) 892- 8127.
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	22	No. 6 Power Boiler	A	PM	3/30/2007	0.0655	POUNDS PER MILLION BTU HEAT INPUT	Initial Compliance test result.
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	2	#2 PWR BLR COMB BARK & #6 FO; COM STK & VENTURI SCRUBBER W/	A	PM	6/10/2004	29.483	POUNDS/HOUR	
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	2	#2 PWR BLR COMB BARK & #6 FO; COM STK & VENTURI SCRUBBER W/	A	PM	2/13/2003	24.05	POUNDS/HOUR	STCS, INC.
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	2	#2 PWR BLR COMB BARK & #6 FO; COM STK & VENTURI SCRUBBER W/	A	PM	4/22/2003	24.79	POUNDS/HOUR	SOURCE TESTING AND CONSULTING SERVICES, INC., N.C.
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	3	#3 PWR BLR COMB BRK/#6FO 180/167 MMBTUH VENTURI SCRUBBER A1	A	PM	6/10/2004	34.327	POUNDS/HOUR	Wood chips limit is 50.6 lb/hr.

RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	3	#3 PWR BLR COMB BRK/#6FO 180/167 MMBTUH VENTURI SCRUBBER A1	A	PM	6/10/2005	0.0344	POUNDS PER MILLION BTU HEAT INPUT	
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	3	#3 PWR BLR COMB BRK/#6FO 180/167 MMBTUH VENTURI SCRUBBER A1	A	PM	2/10/2003	0.106	POUNDS PER MILLION BTU HEAT INPUT	
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	3	#3 PWR BLR COMB BRK/#6FO 180/167 MMBTUH VENTURI SCRUBBER A1	A	PM	6/10/2004	0.1492	POUNDS PER MILLION BTU HEAT INPUT	
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	3	#3 PWR BLR COMB BRK/#6FO 180/167 MMBTUH VENTURI SCRUBBER A1	A	PM	4/15/2003	0.092	POUNDS PER MILLION BTU HEAT INPUT	SOURCE TESTING AND CONSULTING, IN N.C.
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	22	No. 6 Power Boiler	A	VOC	3/30/2007	0.00077	POUNDS PER MILLION BTU HEAT INPUT	Average VOC emissions =.35 lb/hr.
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	1	#1 PWR BOILER, USING #6 FO; COM STK & VENTURI SCRUB W/ #2 PB	A	PM	6/10/2005	0.03	POUNDS PER MILLION BTU HEAT INPUT	
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	1	#1 PWR BOILER, USING #6 FO; COM STK & VENTURI SCRUB W/ #2 PB	A	PM	6/10/2005	0.0792	POUNDS PER MILLION BTU HEAT INPUT	Source Testing & Consulting Services, Inc.
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	2	#2 PWR BLR COMB BARK & #6 FO; COM STK & VENTURI SCRUBBER W/	A	PM	6/10/2005	0.03	POUNDS PER MILLION BTU HEAT INPUT	
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	1	#1 PWR BOILER, USING #6 FO; COM STK & VENTURI SCRUB W/ #2 PB	A	PM	6/10/2004	13.634	POUNDS/HOUR	
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	6	RECOVERY BLR SULFITE NH3/SSL W/3STG SCRBR & MIST ELIM 0 A	A	PM	4/14/2003	0.452	POUNDS PER TON OF PRODUCT	SOURCE TESTING AND CONSULTING SERVICES, INC., N.C.
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	6	RECOVERY BLR SULFITE NH3/SSL W/3STG SCRBR & MIST ELIM 0 A	A	PM	2/10/2003	0.8006	POUNDS PER TON OF PRODUCT	
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	1	#1 PWR BOILER, USING #6 FO; COM STK & VENTURI SCRUB W/ #2 PB	A	PM	2/13/2003	8.06	POUNDS/HOUR	SOURCE TESTING AND CONSULTING SERVICES, INC., APEX, NC 27502
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	1	#1 PWR BOILER, USING #6 FO; COM STK & VENTURI SCRUB W/ #2 PB	A	PM	4/22/2003	11.4	POUNDS/HOUR	SOURCE TESTING AND CONSULTING SERVICES, INC., N.C.
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	6	RECOVERY BLR SULFITE NH3/SSL W/3STG SCRBR & MIST ELIM 0 A	A	PM	5/24/2003	0.88	POUNDS PER TON OF PRODUCT	
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	6	RECOVERY BLR SULFITE NH3/SSL W/3STG SCRBR & MIST ELIM 0 A	A	PM	6/10/2005	2.5	POUNDS PER TON OF PRODUCT	
RAYONIER PERFORMANCE FIBERS LLC	0890004	RAYONIER FERNANDINA SULFITE MILL	NED	NASSAU	A	Y	6	RECOVERY BLR SULFITE NH3/SSL W/3STG SCRBR & MIST ELIM 0 A	A	PM	3/28/2007	0.0155	GRAINS PER DRY STANDARD CUBIC FOOT	
OKEECHOBEE LANDFILL, INC.	0930104	BERMAN ROAD LANDFILL	SED	OKEECHOBEE	A	Y	3	3000 SCFM ENC FLARE, MODEL 1776 EVAP 3016	A	NMOC	4/15/2003	0.133	PARTS PER MILLION DRY GAS VOLUME	RN- Init.stack tsts in 2003; Hexane (NMOC) : 0.133PPMVD@3%O2 , there is no such unit in base and we input under ppm. They will retest(audits ,etc.) See the DEP Letter July 25, 03.
OKEECHOBEE LANDFILL, INC.	0930104	BERMAN ROAD LANDFILL	SED	OKEECHOBEE	A	Y	3	3000 SCFM ENC FLARE, MODEL 1776 EVAP 3016	A	NMOC	9/24/2003	0.11	PARTS PER MILLION DRY GAS VOLUME AS HEXANE @ 3% O2	RN- retest of the test cndtd on Apr17-19, 2003.
OKEECHOBEE LANDFILL, INC.	0930104	BERMAN ROAD LANDFILL	SED	OKEECHOBEE	A	Y	2	1500 scfm inlet flow enclosed landfill gas flare	I	NMOC	4/16/2003	0.333	PARTS PER MILLION DRY GAS VOLUME AS HEXANE @ 3% O2	RN- 0.333 PPMVD @3%O2, there is no such u and test input under ppm. See comnts for activi
OKEECHOBEE LANDFILL, INC.	0930104	BERMAN ROAD LANDFILL	SED	OKEECHOBEE	A	Y	5	3000 SCFM ENC FLARE, MODEL 1698 EVAP 3004IM	A	NMOC	11/4/2004	0.76	PARTS PER MILLION DRY GAS VOLUME AS HEXANE @ 3% O2	RN: landf. gas;HHV=487 BTU/scf; CO2=33.7 Methane= 45.7% next test within 6 months of t renewal application due date of the permit.
OKEECHOBEE LANDFILL, INC.	0930104	BERMAN ROAD LANDFILL	SED	OKEECHOBEE	A	Y	2	1500 scfm inlet flow enclosed landfill gas flare	I	CO	4/16/2003	0.123	POUNDS PER MILLION BTU HEAT INPUT	RN- initial stack test for 2003 .
OKEECHOBEE LANDFILL, INC.	0930104	BERMAN ROAD LANDFILL	SED	OKEECHOBEE	A	Y	3	3000 SCFM ENC FLARE, MODEL 1776 EVAP 3016	A	CO	8/28/2006	0.025	POUNDS PER MILLION BTU HEAT INPUT	RN:HI=490btu/scf * 2732scfm/60min/hr=2231 BTU/HR
OKEECHOBEE LANDFILL, INC.	0930104	BERMAN ROAD LANDFILL	SED	OKEECHOBEE	A	Y	3	3000 SCFM ENC FLARE, MODEL 1776 EVAP 3016	A	CO	8/28/2006	0.025	POUNDS PER MILLION BTU HEAT INPUT	RN: stack T=1631.6F;moisture 19.3%;O2=10.68%;CO2=9.54%; Fuel flow=27 scfm;Fuel HHV=490 Btu/scf; Methane (577%?
OKEECHOBEE LANDFILL, INC.	0930104	BERMAN ROAD LANDFILL	SED	OKEECHOBEE	A	Y	3	3000 SCFM ENC FLARE, MODEL 1776 EVAP 3016	A	CO	6/28/2005	0.016	POUNDS PER MILLION BTU HEAT INPUT	RN: CO test on flare. T=1500 F; Fuel HHV=49 Btu/scf
OKEECHOBEE LANDFILL, INC.	0930104	BERMAN ROAD LANDFILL	SED	OKEECHOBEE	A	Y	5	3000 SCFM ENC FLARE, MODEL 1698 EVAP 3004IM	A	CO	8/29/2006	0.028	POUNDS PER MILLION BTU HEAT INPUT	RN: Stack T= 1646F; Moisture=24.2%; O2=9.82%;CO2=10.76%;Fuel flow=2012 scfm Fuel HHV=490 btu/scf; Methane =40%
OKEECHOBEE LANDFILL, INC.	0930104	BERMAN ROAD LANDFILL	SED	OKEECHOBEE	A	Y	5	3000 SCFM ENC FLARE, MODEL 1698 EVAP 3004IM	A	CO	11/4/2004	0.027	POUNDS PER MILLION BTU HEAT INPUT	RN: CO=22.23 ppmdv; HHV=487 Btu/scf
OKEECHOBEE LANDFILL, INC.	0930104	BERMAN ROAD LANDFILL	SED	OKEECHOBEE	A	Y	5	3000 SCFM ENC FLARE, MODEL 1698 EVAP 3004IM	A	CO	8/29/2006	0.028	POUNDS PER MILLION BTU HEAT INPUT	RN: HI=490 *2012/60= 16431.3 btu/hr
OKEECHOBEE LANDFILL, INC.	0930104	BERMAN ROAD LANDFILL	SED	OKEECHOBEE	A	Y	3	3000 SCFM ENC FLARE, MODEL 1776 EVAP 3016	A	CO	4/15/2003	0.002	POUNDS PER MILLION BTU HEAT INPUT	RN- initial stack test for 2003.
SONOCO PRODUCTS COMPANY	0950044	SONOCO PRODUCTS/ORLANDO FACILITY	CDOR	ORANGE	A	Y	1	METAL CAN COATER #1 & DRYING OVEN #1	A	VOC	2/7/2006	98.45	PERCENT REDUCTION IN EMISSIONS	The new maximum VOC input rate to the incinerator is 48 pounds per hour. IB
INDUSTRIAL CONTAINER SERVICES - FL, LLC	0950055	DRUM RECONDTIONING FACILITY	CDOR	ORANGE	A	Y	13	Surface Coating and Baking Ovens	A	VOC	8/22/2007	99.98	PERCENT REDUCTION IN EMISSIONS	
KINDER MORGAN ENERGY PARTNERS LP	0950069	CENTRAL FLA PIPELINE	CDOR	ORANGE	A	Y	12	THREE LOADING RACKS #1, #4(T1), #5(T2)	A	VOC	7/16/2003	5.3	MILLIGRAMS PER LITER OF LIQUID LOADED	this is the highest for two flare units
KINDER MORGAN ENERGY PARTNERS LP	0950069	CENTRAL FLA PIPELINE	CDOR	ORANGE	A	Y	12	THREE LOADING RACKS #1, #4(T1), #5(T2)	A	VOC	9/27/2006	4.94	MILLIGRAMS PER LITER OF LIQUID LOADED	Actual results were 1.39 mg/l for rack 1 (north 4.94 mg/l for racks 3, 4 and 5 (south unit)
KINDER MORGAN ENERGY PARTNERS LP	0950069	CENTRAL FLA PIPELINE	CDOR	ORANGE	A	Y	12	THREE LOADING RACKS #1, #4(T1), #5(T2)	A	VOC	7/25/2007	2.82	MILLIGRAMS PER LITER OF LIQUID	JORDAN TECHNOLOGIES, INC. LOUISVIL KY : Actual results were 2.82 mg/l for rack 1 (r unit), 1.11 mg/l for racks 3, 4 and 5 (south unit)

													LOADED	
KINDER MORGAN ENERGY PARTNERS LP	0950069	CENTRAL FLA PIPELINE	CDOR	ORANGE	A	Y	12	THREE LOADING RACKS #1, #4(T1), #5(T2)	A	VOC	4/13/2005	2.05	MILLIGRAMS PER LITER OF LIQUID LOADED	Test performed by Catalyst Air Management, I North Vapor Unit results were 1.83 mg/l. Test c 60 days prior to exp.
KINDER MORGAN ENERGY PARTNERS LP	0950069	CENTRAL FLA PIPELINE	CDOR	ORANGE	A	Y	12	THREE LOADING RACKS #1, #4(T1), #5(T2)	A	VOC	3/17/2004	6.4	MILLIGRAMS PER LITER OF LIQUID LOADED	test conducted by Catalyst Air Management, In
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	112	NECROPSY BLDG: CRAWFORD MODEL CB800 ANIMAL CREMATORY (DAK-1)	A	PM	1/18/2006	0.011	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	@7% O2
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	112	NECROPSY BLDG: CRAWFORD MODEL CB800 ANIMAL CREMATORY (DAK-1)	A	CO	1/19/2006	2.82	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	@7% O2
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	CO	12/18/2007	3.99	POUNDS/HOUR	Spectrum Systems Inc
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	CO	2/4/2003	1.8	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	CO	12/12/2006	1.69	POUNDS/HOUR	Test conducted by Spectrum Systems Inc
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	CO	4/6/2006	4.42	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	CO	1/18/2005	2.89	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	CO	1/27/2004	1.85	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	CO	4/6/2006	4.42	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	80	RCID/EPCOT: 2.5 MW DIESEL GENERATOR (EPCOT DG-2)	A	SO2	1/16/2003	0.041	PERCENT SULFUR IN FUEL	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	NOX	12/18/2007	21.67	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Spectrum, test not required burning oil, NOx te RATA, NOx compliance is by CEM
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	NOX	4/6/2006	26.27	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	NOX	4/6/2006	60.83	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	NOX	4/6/2006	15.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	NOX	4/6/2006	60.83	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	NOX	11/28/2006	20.88	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test performed by Spectrums Systems Inc NO is RATA Limit is 25 ppmvd@15% O2.
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	NOX	1/18/2005	42.37	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	79	RCID/EPCOT: 2.5 MW DIESEL GENERATOR (EPCOT DG-1)	A	SO2	1/16/2003	0.041	PERCENT SULFUR IN FUEL	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	NOX	2/4/2003	45.888	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	NOX	1/27/2004	44.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	SO2	1/27/2004	0.047	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	79	RCID/EPCOT: 2.5 MW DIESEL GENERATOR (EPCOT DG-1)	A	NOX	1/19/2007	74.13	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	SO2	2/4/2003	0.024	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	79	RCID/EPCOT: 2.5 MW DIESEL GENERATOR (EPCOT DG-1)	A	NOX	1/19/2006	78.18	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	79	RCID/EPCOT: 2.5 MW DIESEL GENERATOR (EPCOT DG-1)	A	NOX	1/16/2003	86.39	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	80	RCID/EPCOT: 2.5 MW DIESEL GENERATOR (EPCOT DG-2)	A	NOX	1/19/2006	76.41	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	80	RCID/EPCOT: 2.5 MW DIESEL GENERATOR (EPCOT DG-2)	A	NOX	1/29/2004	88.4	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	80	RCID/EPCOT: 2.5 MW DIESEL GENERATOR (EPCOT DG-2)	A	NOX	1/16/2003	77.72	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	80	RCID/EPCOT: 2.5 MW DIESEL GENERATOR (EPCOT DG-2)	A	NOX	1/20/2005	80.4	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	80	RCID/EPCOT: 2.5 MW DIESEL GENERATOR (EPCOT DG-2)	A	NOX	3/14/2007	74.96	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	79	RCID/EPCOT: 2.5 MW DIESEL GENERATOR (EPCOT DG-1)	A	NOX	1/29/2004	82.93	POUNDS/HOUR	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	NOX	4/6/2006	0.056	POUNDS PER MILLION BTU HEAT INPUT	

WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	NOX	4/6/2006	0.056	POUNDS PER MILLION BTU HEAT INPUT	
WALT DISNEY WORLD COMPANY	0950111	WALT DISNEY WORLD RESORT COMPLEX	CD	ORANGE	A	Y	88	CCCT WITH NATURAL GAS FIRED HRSG (CEP-1)	A	NOX	2/4/2003	0.0858	POUNDS PER MILLION BTU HEAT INPUT	
FP SPIRALKOTE INC	0950125	FP SPIRALKOTE	CDOR	ORANGE	A	Y	11	W & H OLYMPIA-STELLAFLEX 8L PRINTING PRESS	A	VOC	6/27/2006	99.56	PERCENT REDUCTION IN EMISSIONS	
FP SPIRALKOTE INC	0950125	FP SPIRALKOTE	CDOR	ORANGE	A	Y	10	W&H Olympia 746 Flexographic Press (W&H I)	A	VOC	6/27/2006	0.46	POUNDS/HOUR	Reported in lb/hr carbon
FP SPIRALKOTE INC	0950125	FP SPIRALKOTE	CDOR	ORANGE	A	Y	12	Tachys FNC 3000 Press	A	VOC	6/27/2006	2.1	TONS/YEAR	0.48 lb/hr for 8760 hr/yr yields 2.1 TPY
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	SO2	6/27/2007	0	TONS/YEAR	
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	SO2	6/27/2007	0.00274	GRAINS PER DRY STANDARD CUBIC FOOT	Gulf Power Test Team
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	SO2	6/27/2007	0.00274	GRAINS PER DRY STANDARD CUBIC FOOT	Gulr Power Test Team
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	SO2	8/5/2003	0.005	GRAINS PER DRY STANDARD CUBIC FOOT	Test conducted by EPRI
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	SO2	6/14/2005	0.0027	GRAINS PER DRY STANDARD CUBIC FOOT	Test on fuel oil not required
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	SO2	8/4/2003	0.00496	GRAINS PER DRY STANDARD CUBIC FOOT	Test conducted by EPRI
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	CO	7/31/2003	0.474	PARTS PER MILLION DRY GAS VOLUME	Gulf Power Field Services and Sanders Engine RATA Result
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	CO	7/22/2003	0.345	PARTS PER MILLION DRY GAS VOLUME	Gulf Power Field Services and Sanders Engine
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	VOC	8/5/2003	1.68	PARTS PER MILLION DRY GAS VOLUME	
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	VOC	8/5/2003	1.68	PARTS PER MILLION DRY GAS VOLUME	Test conducted by EPRI
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	CO	6/27/2007	2.75	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gulf Power Test Team
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	CO	9/2/2004	0.4302	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gulf Power Test Team
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	CO	6/14/2005	0.345	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test on fuel oil not required
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	NOX	7/31/2003	8.664	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gulf Power Field Services and Sanders Engine
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	NOX	6/27/2007	2.79	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gulf Power Test Team
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	CO	8/4/2003	6.666	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test conducted by EPRI
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	CO	7/31/2003	1.019	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gulf Power Field Services and Sanders Engine Firing Fuel Oil
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	NOX	6/14/2005	2.99	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	test on fuel oil not required
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	VOC	8/4/2003	0.838	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test conducted by EPRI
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	NOX	8/5/2003	3.123	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test conducted by EPRI
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	NOX	6/7/2005	3.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team Southern Company
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	NOX	7/24/2003	7.87	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gulf Power Field Services and Sanders Engine
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	NOX	9/9/2004	2.56	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	conducted by Southern Company test team
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	NOX	6/24/2007	3.11	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gulf Power Test Team
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	NH3	8/5/2003	0.927	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test conducted by EPRI
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	NH3	6/7/2005	0.23	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team Southern Company
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	NH3	6/27/2007	1.09	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gulf Power Test Team
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	CO	8/5/2003	8.266	PARTS PER MILLION DRY GAS VOLUME	Test conducted by EPRI

													@ 15% O2	
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	CO	6/7/2005	0.32	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test Team Southern Company
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	CO	7/24/2003	0.0962	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gulf Power Field Services and Sanders Enginee
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	CO	9/9/2004	0.94	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gulf Power test team
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	CO	6/24/2007	4.64	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gulf Power Tet Team
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	NH3	8/4/2003	0.939	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test conducted by EPRI
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	NH3	6/14/2005	0.35	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test on fuel oil not required
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	NH3	6/27/2007	1.17	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Gulf Power Test Team
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	NOX	8/4/2003	2.73	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Test conducted by EPRI
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	NOX	9/9/2004	0.9472	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	1	468 MW FOSSIL FUEL STEAM GENERATION UNIT #1	A	SO2	4/27/2004	0.034	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	1	468 MW FOSSIL FUEL STEAM GENERATION UNIT #1	A	NOX	4/27/2004	0.487	POUNDS PER MILLION BTU HEAT INPUT	30 day rolling average determined with CEM d
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	1	468 MW FOSSIL FUEL STEAM GENERATION UNIT #1	A	NOX	4/27/2004	0.0487	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	1	468 MW FOSSIL FUEL STEAM GENERATION UNIT #1	A	PM	4/28/2004	0.0068	POUNDS PER MILLION BTU HEAT INPUT	Costal Air Consulting
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	1	468 MW FOSSIL FUEL STEAM GENERATION UNIT #1	A	PM	5/6/2003	0.0026	POUNDS PER MILLION BTU HEAT INPUT	Costal Air Consulting
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	1	468 MW FOSSIL FUEL STEAM GENERATION UNIT #1	A	PM	6/6/2006	0.009	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	1	468 MW FOSSIL FUEL STEAM GENERATION UNIT #1	A	PM	6/6/2006	0.009	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	25	170 MW COMB TURBINE W/FIRED HRSG	A	NOX	7/23/2003	0.0091	POUNDS PER MILLION BTU HEAT INPUT	Gulf Power Field Services and Sanders Enginee
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	2	468 MW FOSSIL FUEL STEAM GENERATION UNIT #2	A	NOX	5/20/2003	0.16	POUNDS PER MILLION BTU HEAT INPUT	Limit is for 30 day rolling average determined l CEM.
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	2	468 MW FOSSIL FUEL STEAM GENERATION UNIT #2	A	NOX	5/4/2004	0.161	POUNDS PER MILLION BTU HEAT INPUT	30 day rolling average determined wiht CEM d
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	2	468 MW FOSSIL FUEL STEAM GENERATION UNIT #2	A	PM	5/20/2003	0.0076	POUNDS PER MILLION BTU HEAT INPUT	Costal Air Consulting
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	2	468 MW FOSSIL FUEL STEAM GENERATION UNIT #2	A	PM	5/4/2004	0.0049	POUNDS PER MILLION BTU HEAT INPUT	Costal Air Consulting
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	2	468 MW FOSSIL FUEL STEAM GENERATION UNIT #2	A	PM	6/14/2006	0.006	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	2	468 MW FOSSIL FUEL STEAM GENERATION UNIT #2	A	PM	6/14/2006	0.006	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	2	468 MW FOSSIL FUEL STEAM GENERATION UNIT #2	A	NOX	5/4/2004	0.161	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	2	468 MW FOSSIL FUEL STEAM GENERATION UNIT #2	A	SO2	5/20/2003	0.16	POUNDS PER MILLION BTU HEAT INPUT	Limit is for 30 day rolling average determined l CEM
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	2	468 MW FOSSIL FUEL STEAM GENERATION UNIT #2	A	SO2	5/4/2004	0.159	POUNDS PER MILLION BTU HEAT INPUT	30 day rolling average determined with CEM s
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	2	468 MW FOSSIL FUEL STEAM GENERATION UNIT #2	A	SO2	5/4/2004	0.159	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	1	468 MW FOSSIL FUEL STEAM GENERATION UNIT #1	A	SO2	4/27/2004	0.34	POUNDS PER MILLION BTU HEAT INPUT	SO2 emission rate determined with CEM data a allowed by the permit
ORLANDO UTILITIES COMMISSION	0950137	STANTON ENERGY CENTER	CD	ORANGE	A	Y	26	170 MW COMB TURBINE W/FIRED HRSG	A	NOX	7/31/2003	0.0115	POUNDS PER MILLION BTU HEAT INPUT	Gulf Power Field Services and Sanders Enginee
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	H114	7/13/2005	0.0123	OTHER (SPECIFY IN COMMENT)	
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	H165	7/13/2005	1.11	OTHER (SPECIFY IN COMMENT)	
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	PM	7/9/2003	0.0021	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Air Testing and Consulting
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	CO	7/19/2007	2.15	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	CUSTOM STACK TEST ANALYSIS, LLC
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	PB	7/13/2005	0.0086	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	

STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	NOX	7/13/2005	128	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	H106	7/19/2007	28.987	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	CUSTOM STACK ANAYLSIS LLC.
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	H106	7/13/2005	44	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	H106	7/19/2006	42.67	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	H106	7/9/2003	26	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing and Consulting
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	SO2	7/13/2005	0.27	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	CO	7/13/2005	5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	PM	7/19/2006	0.0028	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	PM	7/19/2007	0.00369	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	CUSTOM STACK TEST ANALYSIS LLC.
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	CO	7/9/2003	34	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing and Consulting
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	CO	7/19/2006	1.96	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
STERICYCLE INC	0950169	STERICYCLE/APOPKA FACILITY	CDOR	ORANGE	A	Y	1	BIOLOGICAL INCINERATOR (MEDICAL)	A	PM	7/13/2005	0.002	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	6	FTGC Engine 1806 - 7200 bhp gas DLEturbine compressor engine	A	CO	10/30/2007	27.27	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	DeNovo-nv, Inc. The 4 load average is give ab Test was conducted at High, Mid High, Mid Lo and Low loads. The maximum CO occurred at mid low load at 36.19 ppm @ 15% O2
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	6	FTGC Engine 1806 - 7200 bhp gas DLEturbine compressor engine	A	CO	7/16/2007	3.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	DeNovo-nv, Inc.
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	6	FTGC Engine 1806 - 7200 bhp gas DLEturbine compressor engine	A	CO	7/17/2006	1.52	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	6	FTGC Engine 1806 - 7200 bhp gas DLEturbine compressor engine	A	NOX	1/21/2004	16.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	6	FTGC Engine 1806 - 7200 bhp gas DLEturbine compressor engine	A	NOX	11/9/2004	12.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	6	FTGC Engine 1806 - 7200 bhp gas DLEturbine compressor engine	A	NOX	7/17/2006	10.38	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	6	FTGC Engine 1806 - 7200 bhp gas DLEturbine compressor engine	A	NOX	7/16/2007	13.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Denovo-nv, Inc.
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	6	FTGC Engine 1806 - 7200 bhp gas DLEturbine compressor engine	A	NOX	10/30/2007	23.29	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	DENOVO-nv, Inc. Test was conducted under 4 loads the maximum NOx occurred under low lo and was 24.98 ppm @ 15 % O2 ISO. The avera the 4 is given above as the actual.
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	6	FTGC Engine 1806 - 7200 bhp gas DLEturbine compressor engine	A	CO	1/21/2004	1.25	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	6	FTGC Engine 1806 - 7200 bhp gas DLEturbine compressor engine	A	CO	11/9/2004	4.56	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	5	FGTC Engine 1805 - 2700 bhp RICE engine 2 stroke lean burn	A	NOX	8/29/2003	0.983	GRAMS PER BILLION HORSEPOWER	
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	5	FGTC Engine 1805 - 2700 bhp RICE engine 2 stroke lean burn	A	NOX	8/26/2004	0.717	GRAMS PER BILLION HORSEPOWER	
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	5	FGTC Engine 1805 - 2700 bhp RICE engine 2 stroke lean burn	A	NOX	7/11/2005	1.13	GRAMS PER BILLION HORSEPOWER	Units are gram/brake horsepower-hour
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	5	FGTC Engine 1805 - 2700 bhp RICE engine 2 stroke lean burn	A	NOX	7/16/2007	1.78	GRAMS PER BILLION HORSEPOWER	DeNovo-nv, Inc. The Woodlands TX
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	5	FGTC Engine 1805 - 2700 bhp RICE engine 2 stroke lean burn	A	NOX	7/17/2006	1.13	GRAMS PER BILLION HORSEPOWER	Units are grams per horsepower hour; permit li 1.78 g/HP-hr
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	5	FGTC Engine 1805 - 2700 bhp RICE engine 2 stroke lean burn	A	CO	7/16/2007	7	POUNDS/HOUR	Denovo-nv, Inc.
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	5	FGTC Engine 1805 - 2700 bhp RICE engine 2 stroke lean burn	A	CO	8/26/2004	9.02	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	5	FGTC Engine 1805 - 2700 bhp RICE engine 2 stroke lean burn	A	CO	8/29/2003	7.9007	POUNDS/HOUR	
FLORIDA GAS TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	5	FGTC Engine 1805 - 2700 bhp RICE engine 2 stroke lean burn	A	CO	7/11/2005	8.1	POUNDS/HOUR	
FLORIDA GAS								FGTC Engine 1805 - 2700						

TRANSMISSION COMPANY	0950190	FGTC STATION 18, ORANGE COUNTY	CDOR	ORANGE	A	Y	5	bhp RICE engine 2 stroke lean burn	A	CO	7/17/2006	6.23	POUNDS/HOUR	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	2	HRSG and Duct Burner System, Phase II Acid Rain Unit	A	NOX	3/28/2006	0.0476	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	2	HRSG and Duct Burner System, Phase II Acid Rain Unit	A	CO	4/25/2007	0.13	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	2	HRSG and Duct Burner System, Phase II Acid Rain Unit	A	CO	3/30/2005	0.0015	POUNDS PER MILLION BTU HEAT INPUT	G. Bryant and D. MacLarty witnessed the stack
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	2	HRSG and Duct Burner System, Phase II Acid Rain Unit	A	CO	3/12/2003	0.0022	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	2	HRSG and Duct Burner System, Phase II Acid Rain Unit	A	CO	3/23/2004	0.0026	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	2	HRSG and Duct Burner System, Phase II Acid Rain Unit	A	CO	3/28/2006	0.0049	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	2	HRSG and Duct Burner System, Phase II Acid Rain Unit	A	CO	6/7/2007	0.016	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	2	HRSG and Duct Burner System, Phase II Acid Rain Unit	A	NOX	3/12/2003	0.0485	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	2	HRSG and Duct Burner System, Phase II Acid Rain Unit	A	NOX	3/23/2004	0.0504	POUNDS PER MILLION BTU HEAT INPUT	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	2	HRSG and Duct Burner System, Phase II Acid Rain Unit	A	NOX	3/30/2005	0.053	POUNDS PER MILLION BTU HEAT INPUT	G. Bryant and D. MacLarty witnessed the stack
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	1	Combustion Turbine, Phase II Acid Rain Unit	A	NOX	6/7/2007	14.53	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	1	Combustion Turbine, Phase II Acid Rain Unit	A	NOX	3/30/2005	13.21	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	G. Bryant and D. MacLarty witnessed the stack
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	1	Combustion Turbine, Phase II Acid Rain Unit	A	NOX	3/23/2004	12.67	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	1	Combustion Turbine, Phase II Acid Rain Unit	A	NOX	3/12/2003	12.98	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	1	Combustion Turbine, Phase II Acid Rain Unit	A	NOX	3/28/2006	13.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	1	Combustion Turbine, Phase II Acid Rain Unit	A	NOX	4/25/2007	14.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	1	Combustion Turbine, Phase II Acid Rain Unit	A	CO	3/28/2006	0.53	PARTS PER MILLION DRY GAS VOLUME	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	1	Combustion Turbine, Phase II Acid Rain Unit	A	CO	3/12/2003	0.24	PARTS PER MILLION DRY GAS VOLUME	
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	1	Combustion Turbine, Phase II Acid Rain Unit	A	CO	3/30/2005	0.28	PARTS PER MILLION DRY GAS VOLUME	G. Bryant and D. MacLarty witnessed the stack
ORLANDO COGEN LIMITED, L.P.	0950203	ORLANDO COGEN LIMITED, L.P.	CDOR	ORANGE	A	Y	1	Combustion Turbine, Phase II Acid Rain Unit	A	CO	3/23/2004	0.28	PARTS PER MILLION DRY GAS VOLUME	
KISSIMMEE UTILITY AUTHORITY	0970001	KUA - ROY B HANSEL POWER PLANT	CD	OSCEOLA	A	Y	1	49.9 MW COMBINED CYCLE GAS TURBINE	A	SO2	9/11/2006	0.104	POUNDS/HOUR	fuel is natural gas
KISSIMMEE UTILITY AUTHORITY	0970001	KUA - ROY B HANSEL POWER PLANT	CD	OSCEOLA	A	Y	1	49.9 MW COMBINED CYCLE GAS TURBINE	A	NOX	9/10/2007	73.11	POUNDS/HOUR	Lb/hr NOx at full load
KISSIMMEE UTILITY AUTHORITY	0970001	KUA - ROY B HANSEL POWER PLANT	CD	OSCEOLA	A	Y	1	49.9 MW COMBINED CYCLE GAS TURBINE	A	NOX	9/19/2005	95.68	POUNDS/HOUR	
KISSIMMEE UTILITY AUTHORITY	0970001	KUA - ROY B HANSEL POWER PLANT	CD	OSCEOLA	A	Y	1	49.9 MW COMBINED CYCLE GAS TURBINE	A	NOX	9/8/2003	72.1	POUNDS/HOUR	This is a 4 load test. The test result shown is for 100% load
KISSIMMEE UTILITY AUTHORITY	0970001	KUA - ROY B HANSEL POWER PLANT	CD	OSCEOLA	A	Y	1	49.9 MW COMBINED CYCLE GAS TURBINE	A	CO	9/11/2006	65.74	POUNDS/HOUR	
KISSIMMEE UTILITY AUTHORITY	0970001	KUA - ROY B HANSEL POWER PLANT	CD	OSCEOLA	A	Y	1	49.9 MW COMBINED CYCLE GAS TURBINE	A	CO	9/29/2004	38.77	POUNDS/HOUR	
KISSIMMEE UTILITY AUTHORITY	0970001	KUA - ROY B HANSEL POWER PLANT	CD	OSCEOLA	A	Y	1	49.9 MW COMBINED CYCLE GAS TURBINE	A	CO	9/8/2003	46	POUNDS/HOUR	
KISSIMMEE UTILITY AUTHORITY	0970001	KUA - ROY B HANSEL POWER PLANT	CD	OSCEOLA	A	Y	1	49.9 MW COMBINED CYCLE GAS TURBINE	A	CO	9/19/2005	71.81	POUNDS/HOUR	
KISSIMMEE UTILITY AUTHORITY	0970001	KUA - ROY B HANSEL POWER PLANT	CD	OSCEOLA	A	Y	1	49.9 MW COMBINED CYCLE GAS TURBINE	A	CO	9/10/2007	44.63	POUNDS/HOUR	lb/hr CO at full load
KISSIMMEE UTILITY AUTHORITY	0970001	KUA - ROY B HANSEL POWER PLANT	CD	OSCEOLA	A	Y	1	49.9 MW COMBINED CYCLE GAS TURBINE	A	NOX	9/29/2004	61.5	POUNDS/HOUR	This test was conducted at 4 loads. The above r is at full load
KISSIMMEE UTILITY AUTHORITY	0970001	KUA - ROY B HANSEL POWER PLANT	CD	OSCEOLA	A	Y	1	49.9 MW COMBINED CYCLE GAS TURBINE	A	NOX	9/11/2006	85.56	POUNDS/HOUR	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	CO	8/17/2005	1.94	POUNDS/HOUR	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	CO	8/22/2005	0.51	POUNDS/HOUR	CEM Solutions
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	CO	9/23/2004	2.944	POUNDS/HOUR	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	CO	8/24/2005	0.92	POUNDS/HOUR	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	11	Combustion Turbine # 11	A	CO	3/17/2005	2.47	POUNDS/HOUR	CEM Solutions, Inc
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	11	Combustion Turbine # 11	A	CO	8/30/2006	0.09	POUNDS/HOUR	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	CO	8/28/2003	19.11	POUNDS/HOUR	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	CO	8/31/2004	5.228	POUNDS/HOUR	Progress Energy Environmental Test Team

FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	CO	8/23/2006	2.2	POUNDS/HOUR	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	CO	9/9/2003	0.885	POUNDS/HOUR	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	CO	9/14/2005	3.47	POUNDS/HOUR	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	CO	8/26/2003	2.608	POUNDS/HOUR	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	CO	8/23/2006	1.2	POUNDS/HOUR	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	CO	8/25/2004	2.388	POUNDS/HOUR	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	CO	8/30/2005	0.91	POUNDS/HOUR	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	CO	9/11/2003	0.307	PARTS PER MILLION DRY GAS VOLUME	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	CO	9/22/2004	0.002	PARTS PER MILLION DRY GAS VOLUME	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	CO	8/28/2006	6.5	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	CO	8/22/2005	0	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	11	Combustion Turbine # 11	A	SO2	3/17/2005	228	OTHER (SPECIFY IN COMMENT)	Lb/hr SO2, CEM Solutions, Inc.
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	11	Combustion Turbine # 11	A	SO2	3/2/2004	0.18	OTHER (SPECIFY IN COMMENT)	% sulfur by weight
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	11	Combustion Turbine # 11	A	CO	2/4/2003	0.49	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	11	Combustion Turbine # 11	A	CO	3/17/2005	0.64	PARTS PER MILLION DRY GAS VOLUME	CEM Solutions, Inc
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	11	Combustion Turbine # 11	A	CO	3/2/2004	0.87	PARTS PER MILLION DRY GAS VOLUME	Progress Energy Stack Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	11	Combustion Turbine # 11	A	CO	8/30/2006	0.9	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	CO	8/24/2003	0.267	PARTS PER MILLION DRY GAS VOLUME	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	CO	8/31/2004	0.097	PARTS PER MILLION DRY GAS VOLUME	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	CO	8/23/2006	2.2	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	CO	8/16/2005	0	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	SO2	9/23/2004	0.082	OTHER (SPECIFY IN COMMENT)	S g/100SCF, Progress Energy Environmental T Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	CO	9/9/2003	0.44	PARTS PER MILLION DRY GAS VOLUME	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	CO	9/23/2004	1.13	PARTS PER MILLION DRY GAS VOLUME	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	CO	8/22/2005	0	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	CO	8/22/2005	1.1	PARTS PER MILLION DRY GAS VOLUME	CEM Solutions.
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	CO	8/27/2003	0.787	PARTS PER MILLION DRY GAS VOLUME	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	CO	9/21/2004	0.037	PARTS PER MILLION DRY GAS VOLUME	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	CO	8/23/2006	1.2	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	CO	8/16/2005	0.2	PARTS PER MILLION DRY GAS VOLUME	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	SO2	9/13/2004	0.151	OTHER (SPECIFY IN COMMENT)	S g/100scf
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	CO	9/13/2004	0.225	POUNDS/HOUR	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	CO	9/10/2003	4.59	POUNDS/HOUR	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	CO	8/28/2006	6.5	POUNDS/HOUR	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	NOX	8/30/2005	0.006	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	NOX	9/8/2003	21.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	NOX	9/9/2003	37.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER													PARTS PER	

CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	NOX	9/23/2004	37.6	MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	NOX	9/23/2004	19.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	NOX	8/28/2006	0.004	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	NOX	8/28/2006	0.004	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	NOX	8/22/2005	23	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	CEM Solutions. Actual is average of RATA ru Allowables are 24 hour averages. RA was 1.32 which passed. Compliance is by CEM
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	NOX	9/17/2005	40	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	CEM Solutions. Actual is assumed value. Allowables are 24 hour averages. RA was 1.32 which passed. Compliance is by CEM
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	19	P-13: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	9/16/2003	5.48	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	team = FPC test team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	SO2	8/29/2003	0.164	PERCENT SULFUR IN FUEL	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	20	P-14: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	8/18/2005	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	20	P-14: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	8/23/2005	2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	18	P-12: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	9/3/2003	5.77	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	team = FPC test team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	18	P-12: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	9/3/2003	17.29	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	team = FPC test team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	18	P-12: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	9/15/2004	5.45	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	18	P-12: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	8/24/2006	0.002	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	18	P-12: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	8/24/2006	0.002	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	18	P-12: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	8/14/2005	3.67	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	18	P-12: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	8/18/2005	3.67	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	NOX	8/25/2004	24.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	NOX	8/25/2004	41.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	NOX	8/23/2006	0.004	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	NOX	8/23/2006	0.004	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	NOX	8/16/2005	5.52	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	NOX	8/17/2005	5.56	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	SO2	8/27/2003	0.163	PERCENT SULFUR IN FUEL	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	SO2	9/21/2004	0.169	PERCENT SULFUR IN FUEL	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	18	P-12: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	CO	9/3/2003	3.28	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	team = FPC test team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	11	Combustion Turbine # 11	A	SO2	2/4/2003	0.187	PERCENT SULFUR IN FUEL	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	11	Combustion Turbine # 11	A	SO2	3/17/2005	0.13	PERCENT SULFUR IN FUEL	CEM Solutions, Inc
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	SO2	9/9/2003	0.172	PERCENT SULFUR IN FUEL	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	7	Combustion Turbine # 7	A	SO2	9/23/2004	0.162	PERCENT SULFUR IN FUEL	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	11	Combustion Turbine # 11	A	NOX	2/4/2003	35.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy FPC test team
FLORIDA POWER CORPORATION	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	11	Combustion Turbine # 11	A	NOX	3/17/2005	37.37	PARTS PER MILLION DRY GAS VOLUME	CEM Solutions, Inc

D/B/A PROGRESS													@ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	11	Combustion Turbine # 11	A	NOX	3/2/2004	39.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Stack Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	NOX	8/26/2003	24.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	8	Combustion Turbine # 8	A	NOX	8/27/2003	37.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	NOX	8/29/2003	36.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	NOX	8/28/2003	18.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	NOX	8/31/2004	38.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	NOX	8/25/2004	20.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	NOX	8/23/2006	0.003	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	NOX	8/23/2006	0.003	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	NOX	8/16/2005	0.008	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	10	Combustion Turbine # 10	A	NOX	8/16/2005	0.008	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	19	P-13: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	CO	9/16/2003	4.25	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	team = FPC test team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	19	P-13: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	CO	9/15/2004	6.29	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	19	P-13: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	CO	8/31/2006	9.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	19	P-13: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	CO	8/18/2005	1.33	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	20	P-14: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	CO	9/4/2003	8.43	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	team = FPC test team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	20	P-14: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	CO	9/15/2004	9.42	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	20	P-14: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	CO	8/24/2006	3.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	20	P-14: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	CO	8/23/2005	2.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	18	P-12: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	CO	9/15/2004	6.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	18	P-12: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	CO	8/24/2006	6.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	18	P-12: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	CO	8/18/2005	1.61	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	20	P-14: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	9/4/2003	5.18	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	team = FPC test team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	20	P-14: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	9/4/2003	16.22	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	team = FPC test team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	20	P-14: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	9/15/2004	5.29	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	20	P-14: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	8/24/2006	0.002	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	20	P-14: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	8/24/2006	0.002	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	19	P-13: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	9/16/2003	16.65	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	team = FPC test team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	19	P-13: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	9/15/2004	5.87	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION	0970014	INTERCESSION CITY	CD	OSCEOLA	A	Y	19	P-13: Simple cycle combustion turbine 91 MW,	A	NOX	8/31/2006	0.001	PARTS PER MILLION DRY	

D/B/A PROGRESS		PLANT						GE Frame 7EA					GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	19	P-13: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	8/31/2006	0.001	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	19	P-13: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	8/23/2005	2.51	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	19	P-13: Simple cycle combustion turbine 91 MW, GE Frame 7EA	A	NOX	8/18/2005	2.51	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	SO2	9/11/2003	0.179	PERCENT SULFUR IN FUEL	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	SO2	9/22/2004	0.165	PERCENT SULFUR IN FUEL	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	NOX	8/28/2006	0.005	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	NOX	9/13/2004	22.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	NOX	9/22/2004	35.3	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	NOX	9/10/2003	22.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	NOX	9/11/2003	34.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Progress Energy Environmental Test Team
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	NOX	8/24/2006	0.005	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPORATION D/B/A PROGRESS	0970014	INTERCESSION CITY PLANT	CD	OSCEOLA	A	Y	9	Combustion Turbine # 9	A	NOX	8/22/2005	0.006	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	2	Combined Cycle CT Unit: 2, (Phase II Acid Rain Unit)	A	NOX	10/18/2007	6.63	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	NOX	9/15/2006	2.55	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	NOX	9/15/2006	2.55	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	NOX	9/22/2005	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	NOX	8/30/2004	3.03	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	NOX	9/21/2007	3.28	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	NOX	9/30/2003	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Oil was burned less than 400 hours, testing on c was not required
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	NOX	9/10/2003	21.59	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	NOX	8/25/2004	20.53	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	NOX	9/13/2006	22.32	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	2	Combined Cycle CT Unit: 2, (Phase II Acid Rain Unit)	A	CO	9/10/2003	8.18	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Main stack
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	2	Combined Cycle CT Unit: 2, (Phase II Acid Rain Unit)	A	CO	8/25/2004	14.36	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	2	Combined Cycle CT Unit: 2, (Phase II Acid Rain Unit)	A	CO	9/20/2005	10.99	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	2	Combined Cycle CT Unit: 2, (Phase II Acid Rain Unit)	A	CO	9/13/2006	11.31	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	2	Combined Cycle CT Unit: 2, (Phase II Acid Rain Unit)	A	CO	9/12/2007	5.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	NOX	9/12/2003	2.93	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	NOX	9/12/2003	7.39	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Natural gas firing
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	NOX	8/30/2004	3.03	PARTS PER MILLION DRY GAS VOLUME	

@ 15% O2

KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	NOX	9/20/2005	23.15	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	NOX	9/20/2005	22.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	NOX	9/13/2006	22.32	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	NOX	9/11/2007	24.16	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	2	Combined Cycle CT Unit: 2, (Phase II Acid Rain Unit)	A	SO2	9/13/2006	0.015	PERCENT SULFUR IN FUEL	fuel was natural gas
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	2	Combined Cycle CT Unit: 2, (Phase II Acid Rain Unit)	A	SO2	9/12/2007	0.015	PERCENT SULFUR IN FUEL	Testing was conducted burning gas. Test on oil not required. SO2 emissions on gas were below NSPS limit.
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	SO2	9/13/2006	0.015	PERCENT SULFUR IN FUEL	Fuel is natural gas
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	SO2	9/12/2007	0.015	PERCENT SULFUR IN FUEL	Testing was conducted burning gas. Test on oil not required. SO2 emissions on gas were below NSPS limit.
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	NH3	9/21/2007	0.196	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	2	Combined Cycle CT Unit: 2, (Phase II Acid Rain Unit)	A	NOX	9/10/2003	7.77	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Main stack
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	2	Combined Cycle CT Unit: 2, (Phase II Acid Rain Unit)	A	NOX	8/25/2004	7.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	2	Combined Cycle CT Unit: 2, (Phase II Acid Rain Unit)	A	NOX	9/22/2005	9.63	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	2	Combined Cycle CT Unit: 2, (Phase II Acid Rain Unit)	A	NOX	9/13/2006	8.86	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	CO	9/11/2007	12.18	PARTS PER MILLION DRY GAS VOLUME	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	CO	9/20/2005	12.94	PARTS PER MILLION DRY GAS VOLUME	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	CO	9/10/2003	17.15	PARTS PER MILLION DRY GAS VOLUME	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	VOC	9/12/2003	0.23	PARTS PER MILLION DRY GAS VOLUME	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	CO	8/25/2004	20.54	PARTS PER MILLION DRY GAS VOLUME	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	CO	9/12/2003	0.39	PARTS PER MILLION DRY GAS VOLUME	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	CO	9/12/2003	0.68	PARTS PER MILLION DRY GAS VOLUME	Natural gas firing
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	CO	8/30/2004	0.38	PARTS PER MILLION DRY GAS VOLUME	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	CO	9/15/2006	1.01	PARTS PER MILLION DRY GAS VOLUME	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	CO	9/15/2006	1.01	PARTS PER MILLION DRY GAS VOLUME	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	CO	9/22/2005	10.99	PARTS PER MILLION DRY GAS VOLUME	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	CO	8/30/2004	0.38	PARTS PER MILLION DRY GAS VOLUME	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	CO	9/21/2007	0.68	PARTS PER MILLION DRY GAS VOLUME	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	CO	9/13/2006	16.29	PARTS PER MILLION DRY GAS VOLUME	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	NOX	9/29/2003	56	TONS/YEAR	Tons per year calculated from CEM data
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	2	Combined Cycle CT Unit: 2, (Phase II Acid Rain Unit)	A	NOX	9/13/2006	8.86	TONS/YEAR	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	2	Combined Cycle CT Unit: 2, (Phase II Acid Rain Unit)	A	NOX	9/20/2005	9.55	TONS/YEAR	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	2	Combined Cycle CT Unit: 2, (Phase II Acid Rain Unit)	A	NOX	9/29/2003	56	TONS/YEAR	Tons per year calulated from CEM data for unit and both stacks on unit 2
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	NOX	9/13/2006	12.76	TONS/YEAR	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	1	Simple Cycle CT Unit: 1, (Phase II Acid Rain Unit)	A	NOX	8/24/2004	56	TONS/YEAR	
KISSIMMEE UTILITY AUTHORITY	0970043	KUA CANE ISLAND POWER PARK	CD	OSCEOLA	A	Y	3	A 250 MW Combined Cycle Turbine with Supplemental Duct Firg	A	SO2	9/21/2007	0.102	POUNDS/HOUR	
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	3	170 MW Simple Cycle Combustion Turbine	A	CO	6/29/2006	0.09	PARTS PER MILLION DRY GAS VOLUME	
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	3	170 MW Simple Cycle Combustion Turbine	A	CO	6/10/2004	0.15	PARTS PER MILLION DRY GAS VOLUME	GE PG7241FA Combustion Turbine firing natu gas, tested by Costal Air Consulting
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	3	170 MW Simple Cycle Combustion Turbine	A	CO	6/15/2005	0.22	PARTS PER MILLION DRY GAS VOLUME	Costal Air Consulting

RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	1	170 MW Simple Cycle Combustion Turbine	A	CO	6/27/2006	0.02	PARTS PER MILLION DRY GAS VOLUME	
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	1	170 MW Simple Cycle Combustion Turbine	A	CO	6/16/2005	0.27	PARTS PER MILLION DRY GAS VOLUME	Coastal Air Consulting
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	2	170 MW Simple Cycle Combustion Turbine	A	CO	4/22/2003	0.48	PARTS PER MILLION DRY GAS VOLUME	
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	2	170 MW Simple Cycle Combustion Turbine	A	CO	6/14/2005	0.31	PARTS PER MILLION DRY GAS VOLUME	Coastal Air Consulting
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	2	170 MW Simple Cycle Combustion Turbine	A	CO	6/9/2004	0.32	PARTS PER MILLION DRY GAS VOLUME	GE PG7241FA Combustion Turbine firing gas, tested by Costal Air Consulting
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	2	170 MW Simple Cycle Combustion Turbine	A	CO	6/27/2006	0.1	PARTS PER MILLION DRY GAS VOLUME	
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	1	170 MW Simple Cycle Combustion Turbine	A	CO	4/22/2003	0.28	PARTS PER MILLION DRY GAS VOLUME	
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	1	170 MW Simple Cycle Combustion Turbine	A	CO	6/8/2004	0.2	PARTS PER MILLION DRY GAS VOLUME	Costal Air Consulting
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	3	170 MW Simple Cycle Combustion Turbine	A	CO	4/21/2003	0.33	PARTS PER MILLION DRY GAS VOLUME	
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	2	170 MW Simple Cycle Combustion Turbine	A	NOX	6/28/2006	6.44	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	2	170 MW Simple Cycle Combustion Turbine	A	NOX	6/14/2005	6.74	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Caostal Air Consulting
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	1	170 MW Simple Cycle Combustion Turbine	A	NOX	6/8/2004	6.45	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Costal Air Consulting
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	3	170 MW Simple Cycle Combustion Turbine	A	NOX	4/21/2003	6.64	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	3	170 MW Simple Cycle Combustion Turbine	A	NOX	6/15/2005	6.58	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Coastal Air Consulting
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	3	170 MW Simple Cycle Combustion Turbine	A	NOX	6/10/2004	6.02	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE PG7241FA Combustion Turbine firing natu gas, tested by Costal Air Consulting
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	3	170 MW Simple Cycle Combustion Turbine	A	NOX	6/29/2006	5.98	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	1	170 MW Simple Cycle Combustion Turbine	A	NOX	4/22/2003	6.45	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	1	170 MW Simple Cycle Combustion Turbine	A	NOX	6/16/2005	6.65	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	Coastal Air Consulting
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	1	170 MW Simple Cycle Combustion Turbine	A	NOX	6/27/2006	5.65	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	2	170 MW Simple Cycle Combustion Turbine	A	NOX	4/22/2003	7.95	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
RELIANT ENERGY FLORIDA, LLC	0970071	RELIANT ENERGY OSCEOLA	CD	OSCEOLA	A	Y	2	170 MW Simple Cycle Combustion Turbine	A	NOX	6/9/2004	6.48	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	GE PG7241FA Combustion Turbine firing natu gas, tested by Costal Air Consulting
OKEELANTA CORP	0990005	OKEELANTA CORP	SEPB	PALM BEACH	A	Y	14	Boiler 16 - 150,000 lb/hr steam rate (gas/oil)	A	CO	3/16/2004	0.011	POUNDS PER MILLION BTU HEAT INPUT	test on gas
OKEELANTA CORP	0990005	OKEELANTA CORP	SEPB	PALM BEACH	A	Y	14	Boiler 16 - 150,000 lb/hr steam rate (gas/oil)	A	CO	1/30/2003	0.01	POUNDS PER MILLION BTU HEAT INPUT	production limited to 147 mmbtu/hr. heat input
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	1	Boiler 1 - 150,000 lb/hr steam rate	A	NOX	12/10/2004	0.14	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	3	Boiler 3 - 130,000 lb/hr steam rate	A	VOC	11/9/2004	0.176	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	1	Boiler 1 - 150,000 lb/hr steam rate	A	PM	12/5/2003	0.19	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM- 370, delta p-5.22", psig-70
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	1	Boiler 1 - 150,000 lb/hr steam rate	A	PM	12/10/2004	0.2	POUNDS PER MILLION BTU HEAT INPUT	Scrubber GPM-367, delta p-5.3", psig-73
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	1	Boiler 1 - 150,000 lb/hr steam rate	A	VOC	12/5/2003	0.66	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	1	Boiler 1 - 150,000 lb/hr steam rate	A	VOC	12/10/2004	0.6	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	4	Boiler 4 - 125,000 lb/hr steam rate	A	VOC	11/12/2003	0.22	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	4	Boiler 4 - 125,000 lb/hr steam rate	A	VOC	11/12/2004	0.275	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	3	Boiler 3 - 130,000 lb/hr steam rate	A	NOX	11/13/2003	0.133	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	3	Boiler 3 - 130,000 lb/hr steam rate	A	NOX	11/9/2004	0.122	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	3	Boiler 3 - 130,000 lb/hr steam rate	A	PM	11/13/2003	0.171	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	3	Boiler 3 - 130,000 lb/hr steam rate	A	PM	11/9/2004	0.177	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM-345, delta p-5.3", 70psig.

ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	5	Boiler 5 - 115,000 lb/hr steam rate	A	NOX	12/7/2004	0.15	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	5	Boiler 5 - 115,000 lb/hr steam rate	A	CO	12/9/2003	2.91	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	5	Boiler 5 - 115,000 lb/hr steam rate	A	CO	12/7/2004	4	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	3	Boiler 3 - 130,000 lb/hr steam rate	A	VOC	11/13/2003	0.699	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	5	Boiler 5 - 115,000 lb/hr steam rate	A	PM	12/9/2003	0.11	POUNDS PER MILLION BTU HEAT INPUT	scrubber psig-70/72, delta p- 10.38, GPM- 255/
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	5	Boiler 5 - 115,000 lb/hr steam rate	A	PM	12/7/2004	0.13	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM-1019,delta p-7.19,psig-72
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	4	Boiler 4 - 125,000 lb/hr steam rate	A	NOX	11/12/2003	0.205	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	4	Boiler 4 - 125,000 lb/hr steam rate	A	NOX	11/12/2004	0.146	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	1	Boiler 1 - 150,000 lb/hr steam rate	A	NOX	12/5/2003	0.11	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	4	Boiler 4 - 125,000 lb/hr steam rate	A	PM	11/12/2003	0.103	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	4	Boiler 4 - 125,000 lb/hr steam rate	A	PM	11/12/2004	0.182	POUNDS PER MILLION BTU HEAT INPUT	Scrubber GPM- 370, delta p-6", psig-71
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	2	Boiler 2 - 150,000 lb/hr steam rate	A	VOC	12/3/2004	0.31	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	2	Boiler 2 - 150,000 lb/hr steam rate	A	PM	12/3/2004	0.27	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM- 375, delta p-4.3", psig-72
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	5	Boiler 5 - 115,000 lb/hr steam rate	A	VOC	12/9/2003	0.02	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	5	Boiler 5 - 115,000 lb/hr steam rate	A	VOC	12/7/2004	0.22	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	5	Boiler 5 - 115,000 lb/hr steam rate	A	SO2	12/7/2004	0	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	2	Boiler 2 - 150,000 lb/hr steam rate	A	NOX	12/3/2004	0.18	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	2	Boiler 2 - 150,000 lb/hr steam rate	A	NOX	12/3/2003	0.13	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	2	Boiler 2 - 150,000 lb/hr steam rate	A	PM	12/3/2003	0.27	POUNDS PER MILLION BTU HEAT INPUT	
ATLANTIC SUGAR ASSOCIATION	0990016	ATLANTIC SUGAR MILL	SEPB	PALM BEACH	A	Y	2	Boiler 2 - 150,000 lb/hr steam rate	A	VOC	12/3/2003	0.75	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	6	BOILER #6 WITH SCRUBBER PSD	A	NOX	11/17/2006	0.143	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	6	BOILER #6 WITH SCRUBBER PSD	A	NOX	11/17/2004	0.11	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH SCRUBBER	A	SO2	11/22/2004	0	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	6	BOILER #6 WITH SCRUBBER PSD	A	NOX	12/13/2005	0.14	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test.
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH SCRUBBER	A	NOX	11/28/2006	0.12	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	PM	11/9/2006	0.19	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	PM	11/16/2007	0.16	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH SCRUBBER	A	PM	11/20/2003	0.16	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM-732, delta p-17", psig-60
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH SCRUBBER	A	PM	11/22/2004	0.15	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM-1200, delta p-18", psig-60
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH SCRUBBER	A	PM	12/15/2005	0.16	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test.
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH SCRUBBER	A	PM	11/28/2006	0.19	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH SCRUBBER	A	PM	11/8/2007	0.18	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 2 SCRUBBERS AND 2 STACKS	A	PM	12/12/2003	0.19	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM- 800, delta p- 12"/11", psig-65
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 2 SCRUBBERS AND 2 STACKS	A	PM	12/1/2004	0.18	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM-1200, psig-50, delta p-10",10".
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	VOC	11/12/2004	0.38	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	VOC	12/8/2005	0.49	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	VOC	11/9/2006	0.7	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	VOC	11/16/2007	0.4	POUNDS PER MILLION BTU HEAT INPUT	
								BOILER #2 WITH 2					POUNDS PER	

OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	2	SCRUBBERS AND 2 STACKS	A	VOC	12/12/2003	0.23	MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 2 SCRUBBERS AND 2 STACKS	A	VOC	12/1/2004	0.53	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 2 SCRUBBERS AND 2 STACKS	A	VOC	1/10/2006	0.13	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test.
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 2 SCRUBBERS AND 2 STACKS	A	VOC	11/30/2006	0.37	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 2 SCRUBBERS AND 2 STACKS	A	VOC	11/14/2007	0.37	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	5	165,000 LB/HR BAGASSE BOILER # 5 WITH 2 SCRUBBERS & 2 STACKS	A	VOC	11/18/2003	0.09	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	5	165,000 LB/HR BAGASSE BOILER # 5 WITH 2 SCRUBBERS & 2 STACKS	A	VOC	11/10/2004	0.41	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	5	165,000 LB/HR BAGASSE BOILER # 5 WITH 2 SCRUBBERS & 2 STACKS	A	VOC	12/5/2005	0.37	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test.
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	5	165,000 LB/HR BAGASSE BOILER # 5 WITH 2 SCRUBBERS & 2 STACKS	A	VOC	11/14/2006	0.24	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	5	165,000 LB/HR BAGASSE BOILER # 5 WITH 2 SCRUBBERS & 2 STACKS	A	VOC	11/28/2007	0.46	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	6	BOILER #6 WITH SCRUBBER PSD	A	PM	11/12/2003	0.123	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	6	BOILER #6 WITH SCRUBBER PSD	A	PM	11/17/2004	0.137	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	6	BOILER #6 WITH SCRUBBER PSD	A	PM	12/13/2005	0.13	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test.
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	6	BOILER #6 WITH SCRUBBER PSD	A	PM	11/17/2006	0.12	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	5	165,000 LB/HR BAGASSE BOILER # 5 WITH 2 SCRUBBERS & 2 STACKS	A	PM	11/18/2003	0.15	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM-800, delta p-10", 12", psig-75
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	5	165,000 LB/HR BAGASSE BOILER # 5 WITH 2 SCRUBBERS & 2 STACKS	A	PM	11/10/2004	0.17	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	5	165,000 LB/HR BAGASSE BOILER # 5 WITH 2 SCRUBBERS & 2 STACKS	A	PM	12/5/2005	0.16	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	5	165,000 LB/HR BAGASSE BOILER # 5 WITH 2 SCRUBBERS & 2 STACKS	A	PM	11/14/2006	0.162	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	5	165,000 LB/HR BAGASSE BOILER # 5 WITH 2 SCRUBBERS & 2 STACKS	A	PM	11/28/2007	0.171	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH SCRUBBER	A	CO	11/22/2004	3.35	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	NOX	11/12/2003	0.13	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	NOX	11/12/2004	0.25	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	NOX	11/12/2004	0.25	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	NOX	12/8/2005	0.18	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	NOX	11/9/2006	0.21	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	NOX	11/16/2007	0.26	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH SCRUBBER	A	VOC	11/22/2004	0.17	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH SCRUBBER	A	VOC	12/15/2005	0.14	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test.
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH SCRUBBER	A	VOC	11/28/2006	0.2	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	6	BOILER #6 WITH SCRUBBER PSD	A	PM	11/6/2007	0.144	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 2 SCRUBBERS AND 2 STACKS	A	NOX	12/11/2003	0.24	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 2 SCRUBBERS AND 2 STACKS	A	NOX	12/1/2004	0.23	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 2 SCRUBBERS AND 2 STACKS	A	NOX	1/10/2006	0.18	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 2 SCRUBBERS AND 2 STACKS	A	NOX	11/30/2006	0.18	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 2 SCRUBBERS AND 2 STACKS	A	NOX	11/14/2007	0.21	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	VOC	11/12/2003	0.3	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	VOC	11/12/2004	0.38	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 2 SCRUBBERS AND 2 STACKS	A	PM	11/30/2006	0.154	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 2 SCRUBBERS AND 2	A	PM	1/10/2006	0.18	POUNDS PER MILLION BTU	Annual Test

								STACKS					HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 2 SCRUBBERS AND 2 STACKS	A	PM	11/14/2007	0.162	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	5	165,000 LB/HR BAGASSE BOILER # 5 WITH 2 SCRUBBERS & 2 STACKS	A	NOX	11/18/2003	0.2	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	5	165,000 LB/HR BAGASSE BOILER # 5 WITH 2 SCRUBBERS & 2 STACKS	A	NOX	11/10/2004	0.21	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	5	165,000 LB/HR BAGASSE BOILER # 5 WITH 2 SCRUBBERS & 2 STACKS	A	NOX	12/5/2005	0.22	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	5	165,000 LB/HR BAGASSE BOILER # 5 WITH 2 SCRUBBERS & 2 STACKS	A	NOX	11/14/2006	0.28	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	5	165,000 LB/HR BAGASSE BOILER # 5 WITH 2 SCRUBBERS & 2 STACKS	A	NOX	11/28/2007	0.19	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	PM	11/12/2003	0.16	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	PM	11/11/2004	0.2	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	PM	11/12/2004	0.2	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	4	BAGASSE BOILER #4 (UNIT #5), 140,000 LBS/HR STEAM	A	PM	12/8/2005	0.17	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	6	BOILER #6 WITH SCRUBBER PSD	A	VOC	11/17/2004	0.16	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	6	BOILER #6 WITH SCRUBBER PSD	A	VOC	12/13/2005	0.13	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH SCRUBBER	A	NOX	12/15/2005	0.1	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test.
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	6	BOILER #6 WITH SCRUBBER PSD	A	VOC	11/17/2006	0.12	POUNDS PER MILLION BTU HEAT INPUT	
OSCEOLA FARMS	0990019	OSCEOLA FARMS	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH SCRUBBER	A	NOX	11/22/2004	0.14	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	NOX	12/20/2007	0.147	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	NOX	1/22/2004	0.142	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	NOX	1/17/2007	0.126	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	VOC	1/7/2004	0.102	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	VOC	12/15/2004	0.069	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	VOC	1/13/2006	0.09	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test Passed.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	VOC	12/8/2006	0.002	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	VOC	12/8/2006	0.002	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	VOC	12/12/2007	0.008	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	VOC	12/12/2007	0.008	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	CO	2/13/2004	0.71	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	CO	1/19/2005	0.69	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	CO	2/10/2006	1.17	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test Passed.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	CO	1/11/2007	2.32	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	CO	12/10/2007	2.03	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	NOX	1/14/2004	0.359	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	NOX	1/13/2005	0.24	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	NOX	12/7/2005	0.24	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	NOX	1/5/2007	0.29	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	NOX	12/4/2007	0.23	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	PM	1/14/2004	0.124	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM-328, delta p 6.4/7.2, psig=55
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	PM	1/13/2005	0.1	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	PM	12/7/2005	0.07	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test

SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	PM	1/5/2007	0.116	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	PM	12/4/2007	0.117	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	NOX	1/13/2004	0.201	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	NOX	1/27/2005	0.14	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	NOX	1/18/2006	0.09	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test Passed.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	NOX	12/7/2006	0.168	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	NOX	12/19/2007	0.143	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	VOC	1/22/2004	0.447	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	VOC	1/27/2005	0.22	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	VOC	2/21/2004	0.447	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	VOC	1/17/2006	0.11	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test Passed.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	VOC	1/17/2007	0.048	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	VOC	1/17/2007	0.048	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	VOC	12/20/2007	0.053	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	VOC	12/20/2007	0.053	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	VOC	1/13/2004	0.6	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	VOC	1/27/2005	0.24	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	VOC	1/18/2006	0.18	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test Passed.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	VOC	12/7/2006	0.676	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	VOC	12/7/2006	0.676	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	VOC	12/19/2007	0.46	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	VOC	12/19/2007	0.46	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	PM	1/7/2004	0.094	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM- 160, delta p- 7.3
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	PM	12/15/2004	0.115	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	PM	1/13/2006	0.08	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test, Passed at .08 lb/mmbtu.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	PM	12/8/2006	0.105	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	PM	12/12/2007	0.103	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	PM	2/13/2004	0.1	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	NOX	1/16/2004	0.251	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	NOX	1/12/2005	0.24	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	NOX	1/12/2005	0.24	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	NOX	12/9/2005	0.24	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	NOX	1/9/2007	0.24	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	NOX	12/6/2007	0.21	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	PM	1/22/2004	0.152	POUNDS PER MILLION BTU HEAT INPUT	scrubber-151 gpm, delta p- 6.3", psig-50
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	PM	1/27/2005	0.16	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	PM	1/17/2006	0.07	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test Passed.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	PM	1/17/2007	0.111	POUNDS PER MILLION BTU HEAT INPUT	
													POUNDS PER	

SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	PM	12/20/2007	0.107	MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	PM	1/19/2005	0.09	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	PM	1/20/2006	0.07	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test Passed.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	PM	1/11/2007	0.109	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	PM	12/10/2007	0.119	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	PM	1/13/2004	0.113	POUNDS PER MILLION BTU HEAT INPUT	Scrubber GPM-140, delta p-5.4, psig-63%
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	PM	1/27/2005	0.09	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	PM	1/18/2006	0.06	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test Passed.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	PM	12/7/2006	0.134	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	3	BOILER #3 WITH 1 SCRUBBER AND 1 STACK	A	PM	12/19/2007	0.126	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	PM	1/16/2004	0.137	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM- 260, delta p- 7.7/7.8, psig-50
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	PM	1/12/2005	0.15	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	PM	1/12/2005	0.15	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	PM	12/9/2005	0.06	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	PM	1/9/2007	0.076	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	PM	12/6/2007	0.091	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	NOX	1/7/2004	0.139	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	NOX	12/15/2004	0.209	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	NOX	1/13/2006	0.13	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test Passed.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	NOX	12/8/2006	0.18	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	1	BOILER #1 WITH 1 SCRUBBER AND 1 STACK	A	NOX	12/12/2007	0.178	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	12/6/2007	0.27	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	SO2	1/11/2007	0	POUNDS/HOUR	Annual Test Not Required.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	1/5/2007	0.13	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	12/4/2007	0.11	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	12/4/2007	0.11	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	1/16/2004	0.097	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	1/9/2007	0.13	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	1/16/2004	0.097	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	12/9/2005	0.07	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	1/12/2005	0.1	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	1/12/2005	0.1	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	SO2	1/9/2007	0	POUNDS/HOUR	Annual Test Not Required.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	2/13/2004	11	POUNDS/HOUR	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	1/19/2005	78.79	POUNDS/HOUR	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	1/20/2006	31.85	POUNDS/HOUR	Annual Stack Test Passed.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	1/11/2007	66.15	POUNDS/HOUR	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	12/10/2007	110	POUNDS/HOUR	
SUGAR CANE	0990026	SUGAR CANE	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1	A	NOX	1/19/2005	105	POUNDS/HOUR	

GROWERS CO-OP		GROWERS CO-OP						STACK						
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	NOX	1/20/2006	89.83	POUNDS/HOUR	Annual Stack Test Passed.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	NOX	1/11/2007	69.32	POUNDS/HOUR	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	NOX	12/10/2007	100.2	POUNDS/HOUR	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	SO2	1/5/2007	0	POUNDS/HOUR	Annual Test Not Required.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	1/14/2004	0.07	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	1/13/2005	0.1	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	12/7/2005	0.13	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	4	BOILER #4 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	1/5/2007	0.13	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	8	BOILER # 8 WITH 2 SCRUBBERS AND 1 STACK	A	NOX	2/13/2004	93	POUNDS/HOUR	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	1/9/2007	0.13	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	5	BOILER #5 WITH 2 SCRUBBERS AND 1 STACK	A	VOC	12/6/2007	0.27	POUNDS PER MILLION BTU HEAT INPUT	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	NOX	1/27/2005	0.14	GRAMS PER BILLION HORSEPOWER-HOUR	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	NOX	1/17/2006	0.1	GRAMS PER BILLION HORSEPOWER-HOUR	Annual Stack Test Passed.
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	NOX	2/21/2004	0.142	GRAMS PER BILLION HORSEPOWER-HOUR	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	NOX	1/17/2007	0.126	GRAMS PER BILLION HORSEPOWER-HOUR	
SUGAR CANE GROWERS CO-OP	0990026	SUGAR CANE GROWERS CO-OP	SEPB	PALM BEACH	A	Y	2	BOILER #2 WITH 1 SCRUBBER AND 1 STACK	A	NOX	12/20/2007	0.147	GRAMS PER BILLION HORSEPOWER-HOUR	
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	4	Fossil Fuel Steam Generator, Unit 4 -Phase II Acid Rain Unit	A	PM	3/4/2008	0.04	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	4	Fossil Fuel Steam Generator, Unit 4 -Phase II Acid Rain Unit	A	PM	3/4/2008	0.03	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	4	Fossil Fuel Steam Generator, Unit 4 -Phase II Acid Rain Unit	A	PM	4/25/2006	0.06	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test Passed,
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	4	Fossil Fuel Steam Generator, Unit 4 -Phase II Acid Rain Unit	A	PM	3/9/2005	0.04	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	4	Fossil Fuel Steam Generator, Unit 4 -Phase II Acid Rain Unit	A	PM	3/6/2007	0.04	POUNDS PER MILLION BTU HEAT INPUT	Steady State Conditions
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	4	Fossil Fuel Steam Generator, Unit 4 -Phase II Acid Rain Unit	A	PM	3/6/2007	0.05	POUNDS PER MILLION BTU HEAT INPUT	Soot Blowing Conditions
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	4	Fossil Fuel Steam Generator, Unit 4 -Phase II Acid Rain Unit	A	PM	3/9/2005	0.3	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	4	Fossil Fuel Steam Generator, Unit 4 -Phase II Acid Rain Unit	A	PM	7/8/2003	0.04	POUNDS PER MILLION BTU HEAT INPUT	team-FPL
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	3	Fossil Fuel Steam Generator, Unit 3 -Phase II Acid Rain Unit	A	PM	7/7/2003	0.06	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	3	Fossil Fuel Steam Generator, Unit 3 -Phase II Acid Rain Unit	A	PM	3/9/2005	0.04	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	3	Fossil Fuel Steam Generator, Unit 3 -Phase II Acid Rain Unit	A	PM	3/9/2005	0.05	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	3	Fossil Fuel Steam Generator, Unit 3 -Phase II Acid Rain Unit	A	PM	2/21/2006	0.06	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test. Unit 4 will be tested as soon repairs are made to water pump assmbly due to mature corrosion..
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	3	Fossil Fuel Steam Generator, Unit 3 -Phase II Acid Rain Unit	A	PM	2/27/2007	0.03	POUNDS PER MILLION BTU HEAT INPUT	Steady State Conditions
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	3	Fossil Fuel Steam Generator, Unit 3 -Phase II Acid Rain Unit	A	PM	2/27/2007	0.04	POUNDS PER MILLION BTU HEAT INPUT	Soot Blowing Conditions
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	3	Fossil Fuel Steam Generator, Unit 3 -Phase II Acid Rain Unit	A	PM	2/27/2008	0.03	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	3	Fossil Fuel Steam Generator, Unit 3 -Phase II Acid Rain Unit	A	PM	2/27/2008	0.04	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	4	Fossil Fuel Steam Generator, Unit 4 -Phase II Acid Rain Unit	A	PM	3/10/2004	0.042	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	3	Fossil Fuel Steam Generator, Unit 3 -Phase II Acid Rain Unit	A	PM	3/2/2004	0.0538	POUNDS PER MILLION BTU HEAT INPUT	100 Oil
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	3	Fossil Fuel Steam Generator, Unit 3 -Phase II Acid Rain Unit	A	PM	3/2/2004	0.067	POUNDS PER MILLION BTU HEAT INPUT	100 percent on oil.
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	3	Fossil Fuel Steam Generator, Unit 3 -Phase II Acid Rain Unit	A	PM	7/7/2003	0.05	POUNDS PER MILLION BTU HEAT INPUT	team-FPL
FLORIDA POWER &		RIVIERA POWER						Fossil Fuel Steam Generator,					POUNDS PER	

LIGHT (PRV)	0990042	PLANT	SEPB	PALM BEACH	A	Y	4	Unit 4 -Phase II Acid Rain Unit	A	PM	3/10/2004	0.055	MILLION BTU HEAT INPUT	
FLORIDA POWER & LIGHT (PRV)	0990042	RIVIERA POWER PLANT	SEPB	PALM BEACH	A	Y	4	Fossil Fuel Steam Generator, Unit 4 -Phase II Acid Rain Unit	A	PM	7/8/2003	0.05	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF LAKE WORTH UTILITIES	0990045	TOM G. SMITH POWER PLANT	SEPB	PALM BEACH	A	Y	9	FOSSIL FUEL STEAM GENERATOR #3 (Phase II, Acid Rain Unit)	A	NOX	6/9/2003	0.419	POUNDS PER MILLION BTU HEAT INPUT	Normal 9 runs on EU-009, Avg .419000, calibr span test okay.
CITY OF LAKE WORTH UTILITIES	0990045	TOM G. SMITH POWER PLANT	SEPB	PALM BEACH	A	Y	11	COMBINED CYCLE UNIT (GT-2/S-5)	A	NOX	9/30/2005	0.365	POUNDS PER MILLION BTU HEAT INPUT	Test passed. Reviewed by Ajaya Satyal.
CITY OF LAKE WORTH UTILITIES	0990045	TOM G. SMITH POWER PLANT	SEPB	PALM BEACH	A	Y	11	COMBINED CYCLE UNIT (GT-2/S-5)	A	NOX	7/16/2004	0.375	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF LAKE WORTH UTILITIES	0990045	TOM G. SMITH POWER PLANT	SEPB	PALM BEACH	A	Y	11	COMBINED CYCLE UNIT (GT-2/S-5)	A	NOX	8/11/2003	0.33	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF LAKE WORTH UTILITIES	0990045	TOM G. SMITH POWER PLANT	SEPB	PALM BEACH	A	Y	11	COMBINED CYCLE UNIT (GT-2/S-5)	A	NOX	9/7/2006	0.343	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test for NOx passed.
CITY OF LAKE WORTH UTILITIES	0990045	TOM G. SMITH POWER PLANT	SEPB	PALM BEACH	A	Y	11	COMBINED CYCLE UNIT (GT-2/S-5)	A	NOX	9/7/2007	0.379	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF LAKE WORTH UTILITIES	0990045	TOM G. SMITH POWER PLANT	SEPB	PALM BEACH	A	Y	3	2000 KW DIESEL GENERATOR # 3 PEAKING UNIT	A	NOX	2/7/2003	2.25	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF LAKE WORTH UTILITIES	0990045	TOM G. SMITH POWER PLANT	SEPB	PALM BEACH	A	Y	2	2000 KW DIESEL GENERATOR # 2 PEAKING UNIT	A	NOX	12/29/2003	2.06	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF LAKE WORTH UTILITIES	0990045	TOM G. SMITH POWER PLANT	SEPB	PALM BEACH	A	Y	5	2000 KW DIESEL GENERATOR # 5 PEAKING UNIT	A	NOX	8/12/2003	2.2	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF LAKE WORTH UTILITIES	0990045	TOM G. SMITH POWER PLANT	SEPB	PALM BEACH	A	Y	1	2000 KW DIESEL GENERATOR # 1 PEAKING UNIT	A	NOX	8/12/2003	1.74	POUNDS PER MILLION BTU HEAT INPUT	
CITY OF LAKE WORTH UTILITIES	0990045	TOM G. SMITH POWER PLANT	SEPB	PALM BEACH	A	Y	9	FOSSIL FUEL STEAM GENERATOR #3 (Phase II, Acid Rain Unit)	A	SO2	7/1/2003	1.99	PERCENT SULFUR IN FUEL	Qrtrly Sulfur Fuel Analysis Report showed 1.9 Sulfur content.
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	5	BOILER #5 WITH TWO SCRUBBERS	I	NOX	12/8/2004	0.122	POUNDS PER TON OF FEED MATERIAL	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	1	BOILER #1 WITH SCRUBBER	I	NOX	11/9/2006	0.16	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	5	BOILER #5 WITH TWO SCRUBBERS	I	PM	12/8/2004	0.08	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM-850n&s, delta p-11.5N 11S, 62
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	2	BOILER #2 WITH SCRUBBERS	I	PM	12/4/2003	0.101	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM-360, delta p-4'/4', psig-60
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	2	BOILER #2 WITH SCRUBBERS	I	PM	12/2/2004	0.119	POUNDS PER MILLION BTU HEAT INPUT	scrubber delta p-4", GPM-357
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	2	BOILER #2 WITH SCRUBBERS	I	PM	11/17/2005	0.171	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	2	BOILER #2 WITH SCRUBBERS	I	PM	11/8/2006	0.144	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	1	BOILER #1 WITH SCRUBBER	I	VOC	12/5/2003	0.117	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	1	BOILER #1 WITH SCRUBBER	I	VOC	12/3/2004	0.194	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	1	BOILER #1 WITH SCRUBBER	I	VOC	11/17/2005	0.061	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	1	BOILER #1 WITH SCRUBBER	I	VOC	11/9/2006	0.1	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	5	BOILER #5 WITH TWO SCRUBBERS	I	NOX	11/16/2006	0.138	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	3	BOILER #3 WITH SCRUBBER	I	PM	12/3/2003	0.131	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM-240, delta p-7",psig-53
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	3	BOILER #3 WITH SCRUBBER	I	PM	12/1/2004	0.126	POUNDS PER MILLION BTU HEAT INPUT	scrubber gpm-240,delta p-8",psig-64
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	3	BOILER #3 WITH SCRUBBER	I	PM	11/16/2005	0.105	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	3	BOILER #3 WITH SCRUBBER	I	PM	11/8/2006	0.104	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	2	BOILER #2 WITH SCRUBBERS	I	VOC	12/4/2003	0.384	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	2	BOILER #2 WITH SCRUBBERS	I	VOC	12/2/2004	0.704	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	2	BOILER #2 WITH SCRUBBERS	I	VOC	11/17/2005	0.315	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	2	BOILER #2 WITH SCRUBBERS	I	VOC	11/8/2006	0.519	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	7	DIESEL ELECTRIC GENERATOR GENERAL MOTORS MODEL 16-567-B	I	NOX	11/15/2006	2.21	POUNDS PER MILLION BTU HEAT INPUT	Diesel Generator #1. Load=800KW.
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	3	BOILER #3 WITH SCRUBBER	I	NOX	12/3/2003	0.211	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	3	BOILER #3 WITH SCRUBBER	I	NOX	12/1/2004	0.155	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	3	BOILER #3 WITH SCRUBBER	I	NOX	11/16/2005	0.113	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	3	BOILER #3 WITH SCRUBBER	I	NOX	11/8/2006	0.123	POUNDS PER MILLION BTU HEAT INPUT	
													POUNDS PER	

U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	3	BOILER #3 WITH SCRUBBER	I	VOC	12/3/2003	0.24	MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	3	BOILER #3 WITH SCRUBBER	I	VOC	12/1/2004	0.642	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	3	BOILER #3 WITH SCRUBBER	I	VOC	11/16/2005	0.243	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	3	BOILER #3 WITH SCRUBBER	I	VOC	11/8/2006	0.281	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	8	DIESEL ELECTRIC GENERATOR GENERAL MOTORS MODEL 16-567-C	I	NOX	12/12/2003	2.67	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	8	DIESEL ELECTRIC GENERATOR GENERAL MOTORS MODEL 16-567-C	I	NOX	12/9/2004	2.57	POUNDS PER MILLION BTU HEAT INPUT	load-800kw
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	8	DIESEL ELECTRIC GENERATOR GENERAL MOTORS MODEL 16-567-C	I	NOX	11/15/2006	2.15	POUNDS PER MILLION BTU HEAT INPUT	Diesel Generator Unit #2. Load=800KW.
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	7	DIESEL ELECTRIC GENERATOR GENERAL MOTORS MODEL 16-567-B	I	NOX	12/12/2003	2.58	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	7	DIESEL ELECTRIC GENERATOR GENERAL MOTORS MODEL 16-567-B	I	NOX	12/9/2004	2.61	POUNDS PER MILLION BTU HEAT INPUT	load-800kw
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	2	BOILER #2 WITH SCRUBBERS	I	NOX	12/4/2003	0.133	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	2	BOILER #2 WITH SCRUBBERS	I	NOX	12/2/2004	0.22	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	2	BOILER #2 WITH SCRUBBERS	I	NOX	11/17/2005	0.113	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	2	BOILER #2 WITH SCRUBBERS	I	NOX	11/8/2006	0.078	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	1	BOILER #1 WITH SCRUBBER	I	PM	12/5/2003	0.118	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM- 240, delta p- 8.9, psig-60
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	1	BOILER #1 WITH SCRUBBER	I	PM	12/3/2004	0.106	POUNDS PER MILLION BTU HEAT INPUT	scrubber GPM-240, delta p- 8", psig-68.
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	1	BOILER #1 WITH SCRUBBER	I	PM	11/18/2005	0.137	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	1	BOILER #1 WITH SCRUBBER	I	PM	11/9/2006	0.087	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	5	BOILER #5 WITH TWO SCRUBBERS	I	NOX	11/23/2005	0.117	POUNDS PER MILLION BTU HEAT INPUT	Annual Test
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	5	BOILER #5 WITH TWO SCRUBBERS	I	PM	12/10/2003	0.134	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	5	BOILER #5 WITH TWO SCRUBBERS	I	PM	11/23/2005	0.142	POUNDS PER MILLION BTU HEAT INPUT	Annual Test Report Review
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	1	BOILER #1 WITH SCRUBBER	I	NOX	12/3/2004	0.184	POUNDS PER MILLION BTU HEAT INPUT	Scrubber GPM- 240, delta p- 8", psig-68
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	1	BOILER #1 WITH SCRUBBER	I	NOX	12/5/2003	0.173	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	5	BOILER #5 WITH TWO SCRUBBERS	I	PM	11/16/2006	0.107	POUNDS PER MILLION BTU HEAT INPUT	
U.S.SUGAR CORP. BRYANT MILL	0990061	U.S. SUGAR CORP. BRYANT MILL	SEPB	PALM BEACH	I	Y	1	BOILER #1 WITH SCRUBBER	I	NOX	11/18/2005	0.205	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM- w/HRSG	A	H027	3/30/2005	0.01	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Not conducted due to exemption.
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM- w/HRSG	A	DIOX	3/30/2005	1.8	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Not conducted due to exemption.
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM- w/HRSG	A	PM	3/25/2003	0.017	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	air testing and consulting
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM- w/HRSG	A	PM	3/11/2008	0.0095	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM- w/HRSG	A	PM	3/13/2007	0.014	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM- w/HRSG	A	NOX	3/30/2005	88	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM- w/HRSG	A	CO	3/19/2004	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing & Consulting
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM- w/HRSG	A	CO	3/21/2006	8.59	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Stack Test.
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM- w/HRSG	A	CO	3/11/2008	4.54	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
													MILLIGRAMS	

BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	H110	3/30/2005	0.1	PER DRY STANDARD CUBIC METER @ 7% O2	Not conducted due to exemption.
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	H114	3/30/2005	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Not conducted due to exemption.
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	SO2	3/30/2005	5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	H106	3/11/2008	4.54	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	H106	3/13/2007	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	H106	3/21/2006	1.27	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Stack Test.
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	H106	3/30/2005	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	H106	3/19/2004	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	H106	3/25/2003	0.351	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	air testing and consulting
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	CO	3/13/2007	12	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	CO	3/30/2005	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	CO	3/25/2003	1.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	air testing and consulting
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	PM	3/19/2004	0.006	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	scrubber flow-278GPM,stack temp.-106F,scrub amps-61,pH-7.4, test team-ATC
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	PM	3/30/2005	0.013	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	PM	3/21/2006	0.0075	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Stack Test.
BETHESDA MEMORIAL HOSPITAL	0990095	BETHESDA MEMORIAL HOSPITAL	SEPB	PALM BEACH	A	Y	4	MEDICAL WASTE INCINERATION SYSTEM-w/HRSG	A	PM	4/1/2003	0.0087	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	PM	2/4/2003	0.0089	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Arlington Environmental atomizer amps-56.4
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	H027	2/12/2008	0.0024	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	CO	2/23/2006	1.84	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	CO	2/3/2005	0.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	CO	2/2/2004	9.33	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Arlington Environmental Services
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	CO	2/4/2003	11.48	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Arlington Environmental
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	PM	3/1/2007	0.011	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	PM	2/14/2008	0.012	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	PM	2/23/2006	0.017	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	PM	2/2/2004	0.012	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Arlington Environmental Services
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	PM	2/3/2005	0.009	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
													MILLIGRAMS	

BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	H114	2/12/2008	0.0009	PER DRY STANDARD CUBIC METER @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	H110	2/12/2008	0.1604	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	SO2	2/13/2008	0.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	H106	2/14/2008	0.85	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	H106	3/1/2007	1.25	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	H106	2/23/2006	2.65	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	H106	2/3/2005	0.27	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	H106	2/2/2004	0.38	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Arlington Environmental Services
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	H106	2/4/2003	0.37	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Arlington Environmental
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	CO	2/13/2008	3.62	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	CO	3/1/2007	5.97	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	NOX	2/13/2008	106.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
BOCA RATON COMMUNITY HOSPITAL	0990119	BOCA RATON COMMUNITY HOSPITAL	SEPB	PALM BEACH	A	Y	2	BIOLOGICAL INCINERATOR; SIMONDS #AF-3C (730 LB/HR)	A	DIOX	2/15/2008	0.482	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	PB	2/24/2004	0.168	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb= 0.066778#/hr=1.5472E-04#/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	PB	3/1/2004	0.131	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb=0.048127#/hr=1.2069E-04#/mmbtu
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	PB	2/2/2005	0.44	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb= 3.80E-04#/MMBTU vs 4.0E-04 #/MMBTU; load=97.3% of capacity.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	DIOX	3/2/2004	23	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; dixin/furan=1.0E-5#/hr
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	DIOX	1/20/2003	19.0631	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN- mtd 23-dioxin/Furon ; cndtd on 1/14/03,1/ and 1/20/03(last 3rd run)
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	DIOX	2/3/2005	19	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; tstng load =93.75% (wthin -10% of capcity Fancis dlvrd leack check original pages (no lea check in the rprt for 2 units and all runs).
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	DIOX	1/27/2006	7	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: run # 2 post chck @5" instead 17"? D/F=2.638E-06 #/hr
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	DIOX	1/25/2007	6.429	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: test condctd on 1/24-25/07; D/F= 2.622E-(hr
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	DIOX	2/25/2004	22	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:Dioxin/Furan=9.156E-06#/hr
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	DIOX	1/23/2003	16.1249	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	DIOX	1/31/2005	12	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; tstng load =95.73% of capacity.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	DIOX	2/1/2006	5	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: D/F= 2.019E-06#/hr
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	DIOX	1/30/2007	6.5187	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: TST ON1/29-1/30/07; D/F=2.942E-06 #/ l
SOLID WASTE		SOLID WASTE						Municipal Solid Waste					MILLIGRAMS PER DRY	

AUTHORITY OF PBC	0990234	AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Boiler #1	A	PB	1/26/2007	0.14	STANDARD CUBIC METER @ 7% O2	RN: Pb=1.34E-04 #/MMBTU; Pb=0.048708#/l
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	PB	1/27/2006	0.014	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb=1.3E-04 #/ MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	PB	1/15/2003	0.136464	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; Pb=1.2538E-4#/mmbtu
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	PB	1/31/2007	0.382	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; Pb= 3.5E-04#/mmbtu
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	PB	1/21/2003	0.379267	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; Pb=0.0003484#/mmbtu
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	PB	1/31/2005	0.675	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb= 0.000583 vs 0.0004 #/MMBTU; load within -10% of capcity, see Hg.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	PB	2/2/2006	0.257	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Pb=2.3E-04 #/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	PB	3/8/2005	0.092	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PB 2005 retest . Tst load within -10% of capacity. Rvsd tst rprt sbmtd on 7/22/05 Pb=0.092 ;Pb= 8.11E-05#/mmbtu(av of 2 &4 r Run 1 (back half portion of the smple dmged shipment); Run 3 (front half(the probe rinse) dr drng shpmnt)
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H106	1/31/2006	97	PERCENT REDUCTION IN EMISSIONS	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H106	1/23/2003	97.65	PERCENT REDUCTION IN EMISSIONS	RN- outlet conc.=8.93 and input for another sec
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H106	2/1/2005	99.66	PERCENT REDUCTION IN EMISSIONS	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H106	2/26/2004	19.51	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN; HCL=1.54#/SCF
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H106	1/31/2007	9.21	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H106	1/23/2003	8.93	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN- DE=97.65%
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H106	2/1/2005	2.286	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:load within +-10% capacity.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	CO	2/1/2005	33.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	CO	1/16/2003	67.09	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN- (CEMs?)
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	CO	1/30/2006	27.45	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	NOX	2/1/2005	200	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: NOx= 0.329#/MMBTU; tstng load 96.11% capacity.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	PM	1/24/2007	4	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: each run 125 min; PM=0.002 gr/DSCF
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	PM	1/26/2006	5	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM=1.833#/hr; PM=0.00433 #/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	PM	2/3/2005	5	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM=0.002gr/dscf@7%O2; load=98.3% of capacity.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	PM	1/20/2003	7.9632	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN-PM= #/hr? 3 runs were cndtd on 1/15/03,1/16/03 and 1/20/03
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	PM	3/2/2004	5	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: run 3 has Soot blow,PM=1.88 #/hr
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H027	1/26/2007	0.005	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:Cd= 0.001777#/hr= 4.35656E-06#/mmbtu
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H027	1/27/2006	0.018	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd= 0.006577 #/hr ; Cd=1.62475E-05 #/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H027	2/2/2005	0.007	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN Tstng load =97.3% of capacity.
													MILLIGRAMS	

SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H027	1/15/2003	0.00315	PER DRY STANDARD CUBIC METER @ 7% O2	RN-no op rate prvd for any tstcd=2.89794E-06#/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H027	3/1/2004	0.002	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; Cd=0.000716#/hr=1.79466#/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H027	1/31/2007	0.009	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN;Cd=8.29E-06#/mmbtu
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H027	2/2/2006	0.03	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd=0.009384 #/hr; Cd=2.76320E-05#/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H027	1/31/2005	0.0105	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Cd = 9.03#/mmbtu; load within 10% of ca
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H027	3/8/2005	0.001	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN this Cd test (not required but cndtd) and sb in addtn to prvsly subm. tst. Cd=0.0000811#/MMBTU'This is an va of the 2 4 runs. Rvsd rprt Tst cndtd on 3/8/05 ,sbmtd on 7/22/05
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H027	1/21/2003	0.006764	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H027	2/24/2004	0.0021	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; Cd=0.000824#/hr=1.9134#/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H114	1/26/2007	0.006	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; Hg= 5.9E-06#/mmbtu
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H114	1/27/2006	0.0047	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=0.001735 #/hr; Hg=4.35857E-06#/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H114	2/2/2005	0.00743	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN:Hg=6.4E-06# / MMBTU;tstng load 97.31% capacity.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H114	1/15/2003	0.009277	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN(no DE nd and prvd) Hg=8.52341E-6 #/mn
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H114	3/1/2004	0.014	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Mercury=0.005525#/hr =1.36889E-05#/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	PM	1/30/2007	8	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: 125 min per run; PM=0.003 gr/dscf
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	PM	2/1/2006	4	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM= 1.513 #/hr ; PM= 0.0033#/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	PM	1/28/2005	5.33	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: PM=0.002gr/dscf@7%O2; load drng the t =98.95% of capacity
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	NOX	1/31/2006	218.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: NOx=0.380 #/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	NOX	2/1/2005	198	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: NOx=0.348 #/MMBTU; load (96.2%) wit 10% of capacity.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	NOX	1/23/2003	200.99	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN- NOx=.352#/mmbtu
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	SO2	1/29/2007	7.27	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	SO2	1/30/2006	18.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: SO2 reduction =36%?
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	SO2	2/1/2005	14	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN; load within -10% of capacity.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	SO2	1/16/2003	14.07	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN- DE=89.52%(input as sprte tst).
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	NOX	1/29/2007	204.45	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: NOx= 0.359 #/hr
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	NOX	1/30/2006	188.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: NOx= 0.33 #/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	PM	1/24/2003	24.1334	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; PM=0.0106 gr/dscf@7%O2

MILLIGRAMS

SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	PM	2/25/2004	5.32351	PER DRY STANDARD CUBIC METER @ 7% O2	RN; PM=2.143 #/hr=0.005#/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H114	1/31/2007	0.004	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; Hg=3.6E-06#/mmbtu =0.00166#/hr
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H114	2/2/2006	0.00787	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=7.16282E-06 #/MMBTU ; Hg= 0.002 #/hr
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H114	1/31/2005	0.009	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=0.000008 #/MMBTU vs 0.00024; tstn load =95.2% of capacity.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H114	1/21/2003	0.011733	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN; Hg=0.0000107803#/mmbtu
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H114	2/24/2004	0.007592	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	RN: Hg=7.0E-6#/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	SO2	1/29/2007	13.62	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	SO2	1/31/2006	18.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	SO2	2/1/2005	16	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	SO2	1/23/2003	16.88	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN-Dest eff. =83.52 input at 2 nd seqnce.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H106	1/29/2007	11.52	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL=0.04E-02#/mmbtu; Midget impinge were not used because of st pressure (-11" H2O NAOH imp omitted ,and rpcd with one empty.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H106	1/30/2006	17.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:HCL=0.0000014 lbs/scf; large imnrs usd i ofthe rqrd by mtd, one imnr was omtd , may no needed for THC
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H106	2/1/2005	5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:tstng loading=96.11 % of capacity.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H106	1/16/2003	6.66	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN- also tested for DE=98.76% (input as sepa test).no prod. data provided , asked for it.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H106	2/27/2004	17	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: HCL=1.50E-06 #/SCF!
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	NOX	1/29/2007	192.96	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: NOx= 0.339#/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	NOX	1/16/2003	236.74	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN- NOx=0.415#/mmbtu (mtd 7e).
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	CO	2/1/2005	16	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN: sbmtd in the inlet data
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	CO	1/31/2006	17.94	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	CO	1/23/2003	103.82	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN- no prtn rate will be send.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H106	1/31/2006	17.35	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	RN:
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H021	1/27/2006	0	POUNDS PER BILLION BTU HEAT INPUT	RN: Be=0.000034 #/hr; Be= 8.5 E-08 #/MMB method 29 is allowed for this Test only instd o metd 104 by Tal mon sectn.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	VOC	2/1/2005	0.0005	POUNDS PER MILLION BTU HEAT INPUT	RN:pages with correct date are hand delivery o 2/05 for 2 units.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	FL	2/2/2006	0.00014	POUNDS PER MILLION BTU HEAT INPUT	RN:
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	FL	1/27/2006	0.00037	POUNDS PER MILLION BTU HEAT INPUT	RN: audi sample was failed.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	VOC	3/1/2004	0.0086	POUNDS PER MILLION BTU HEAT INPUT	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	VOC	1/16/2003	0.009	POUNDS PER MILLION BTU HEAT INPUT	RN total hydrocarbons as CH4 (VOC n arms)
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	VOC	1/30/2006	0.0011	POUNDS PER MILLION BTU HEAT INPUT	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	H021	2/2/2006	0	POUNDS PER BILLION BTU HEAT INPUT	RN: Be=8.1 E-08 #/MMBTU
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	VOC	1/29/2007	0.0004	POUNDS PER MILLION BTU HEAT INPUT	RN: (method 25A) as CH4
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	VOC	1/29/2007	0.0003	POUNDS PER MILLION BTU HEAT INPUT	RN:

SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	SO2	1/29/2007	80.41	PERCENT REDUCTION IN EMISSIONS	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	SO2	2/1/2005	82.66	PERCENT REDUCTION IN EMISSIONS	RN.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H106	1/29/2007	97.71	PERCENT REDUCTION IN EMISSIONS	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H106	2/1/2005	99	PERCENT REDUCTION IN EMISSIONS	RN: see also test in ppmv
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	SO2	1/16/2003	89.9	PERCENT REDUCTION IN EMISSIONS	RN -outlet conctrn=14.07 ppmvd@7%O2, inpu another allw seqnce.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	SO2	2/1/2005	86	PERCENT REDUCTION IN EMISSIONS	RN ; 2006 stck test show about 36% SO2 reduc If input this intoo ARMS will be as a violation they comply with ppm lmit allwd by the prmt. Change next date to 2007. See SO2 test in Jan 2
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	SO2	1/29/2007	91.72	PERCENT REDUCTION IN EMISSIONS	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H106	1/16/2003	98.76	PERCENT REDUCTION IN EMISSIONS	RN- the HCl=6.66 ppmvd@7%O2<29 (prmt ln were conducted for outlet concentration and DI
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	1	Municipal Solid Waste Boiler #1	A	H106	1/30/2006	97	PERCENT REDUCTION IN EMISSIONS	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	SO2	1/23/2003	83.52	PERCENT REDUCTION IN EMISSIONS	RN rslt better than rqrd.
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	SO2	1/31/2006	81	PERCENT REDUCTION IN EMISSIONS	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	VOC	1/23/2003	0.0095	POUNDS PER MILLION BTU HEAT INPUT	RN
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	VOC	3/24/2004	0.0076	POUNDS PER MILLION BTU HEAT INPUT	RN;
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	VOC	1/31/2006	0.0006	POUNDS PER MILLION BTU HEAT INPUT	RN:
SOLID WASTE AUTHORITY OF PBC	0990234	SOLID WASTE AUTHORITY OF PBC/NCRRF	SED	PALM BEACH	A	Y	2	Municipal Solid waste boiler #2	A	VOC	2/1/2005	0.0004	POUNDS PER MILLION BTU HEAT INPUT	RN
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	PM	2/8/2008	0.0129	POUNDS PER MILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	PM	2/13/2004	0.0068	POUNDS PER MILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	PM	2/15/2007	0.0128	POUNDS PER MILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	PM	2/14/2006	0.0071	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test. PM passed.
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	PM	2/24/2005	0.0126	POUNDS PER MILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	PM	1/22/2003	0.0089	POUNDS PER MILLION BTU HEAT INPUT	6.64 lbs/hr
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	PM10	2/14/2007	0.0137	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	VOC	2/22/2005	0.006	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	VOC	2/13/2007	0.0104	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	H114	2/13/2004	0.000005	POUNDS PER MILLION BTU HEAT INPUT	Actual Emission was .000000624 lbs / mmbtu.
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	H114	1/22/2003	0	POUNDS PER MILLION BTU HEAT INPUT	actual emission=0.000000755lb/mmbtu. Progra won't allow input.
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	H114	2/24/2005	0	POUNDS PER MILLION BTU HEAT INPUT	Actual was .00000026 lbs/mmbtu, but the syste did not allow more that 6 places behind the dec
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	H114	2/14/2006	0.000001	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test Mercury passed less than 1.(E10-6
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	H114	2/15/2007	0.000001	POUNDS PER MILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	H114	2/8/2008	0.000001	POUNDS PER MILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	VOC	1/23/2003	0.00567	POUNDS PER BILLION BTU HEAT INPUT	3.95 lbs/hr.
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	VOC	2/13/2004	0.007	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	VOC	2/8/2008	0.0025	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	VOC	2/15/2007	0.0083	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	VOC	2/14/2006	0.013	POUNDS PER BILLION BTU HEAT INPUT	Annual Stack Test, VOC Passed.
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	VOC	2/24/2005	0.001	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	VOC	1/22/2003	0.00267	POUNDS PER BILLION BTU HEAT INPUT	1.93 lbs/hr
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	VOC	2/13/2004	0.0057	POUNDS PER BILLION BTU HEAT INPUT	

NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	VOC	2/6/2008	0.0016	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	PM	2/13/2004	0.0098	POUNDS PER MILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	PM	1/23/2003	0.0079	POUNDS PER MILLION BTU HEAT INPUT	5.62 lbs/hr.
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	PM	2/24/2005	0.0145	POUNDS PER MILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	PM	2/15/2006	0.01	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test. PM passed.
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	PM	2/14/2007	0.0137	POUNDS PER MILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	PM	2/7/2008	0.013	POUNDS PER MILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	H114	2/16/2006	0.000001	POUNDS PER BILLION BTU HEAT INPUT	Annual Stack Test. Mercury test passed 3.00 E
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	H114	2/22/2005	0	POUNDS PER BILLION BTU HEAT INPUT	Actual emission was calculated as 6.14E-07 lbs/mmBTU
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	H114	1/21/2003	0.000001	POUNDS PER BILLION BTU HEAT INPUT	actual emissions- .0000011 lbs/mmbtu
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	H114	2/13/2004	0.000005	POUNDS PER BILLION BTU HEAT INPUT	Actual Emission was .000000724 lbs/mmbtu.
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	VOC	2/7/2008	0.0022	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	VOC	2/14/2007	0.0219	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	VOC	2/15/2006	0.006	POUNDS PER BILLION BTU HEAT INPUT	Annual Stack Test. VOC passed.
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	VOC	2/24/2005	0.019	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	VOC	2/16/2006	0.01	POUNDS PER BILLION BTU HEAT INPUT	Annual Stack Test. VOC passed.
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	PM10	2/13/2007	0.0148	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	H114	2/7/2008	0.000001	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	H114	2/14/2007	0.000001	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	H114	2/15/2006	0.000001	POUNDS PER BILLION BTU HEAT INPUT	Annual Test Passed. Mercury was 9.11 E10-7.
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	H114	2/24/2005	0.000001	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	H114	1/23/2003	0	POUNDS PER BILLION BTU HEAT INPUT	actual emissions- .000000851 lbs/mmbtu. progr will not accept results
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	2	Cogeneration Boiler B - 760 MMBtu/hr spreader stoker boiler	A	H114	2/13/2004	0.000005	POUNDS PER BILLION BTU HEAT INPUT	Actual Emission was .00000035 lbs/mmbtu.
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	1	Cogeneration Boiler A - 760 MMBtu/hr spreader stoker boiler	A	PM10	2/15/2007	0.012	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	H114	2/6/2008	0.000001	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	H114	2/13/2007	0.000002	POUNDS PER BILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	PM	2/13/2004	0.0078	POUNDS PER MILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	PM	1/21/2003	0.0081	POUNDS PER MILLION BTU HEAT INPUT	5.83 lbs/hr.
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	PM	2/22/2005	0.0123	POUNDS PER MILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	PM	2/16/2006	0.0196	POUNDS PER MILLION BTU HEAT INPUT	Annual Stack Test. PM Passed.
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	PM	2/13/2007	0.0148	POUNDS PER MILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	PM	2/6/2008	0.0152	POUNDS PER MILLION BTU HEAT INPUT	
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	VOC	1/21/2003	0.058	POUNDS PER BILLION BTU HEAT INPUT	42.01 lbs/hr.
NEW HOPE POWER PARTNERSHIP	0990332	OKEELANTA COGENERATION PLANT	SEPB	PALM BEACH	A	Y	3	Cogeneration Boiler C - 760 MMBtu/hr spreader stoker boiler	A	VOC	2/13/2004	0.004	POUNDS PER BILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	1	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 1	A	PM	3/14/2007	0.1	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	1	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 1	A	PM	5/24/2006	0.06	POUNDS PER MILLION BTU HEAT INPUT	#6 oil only
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	1	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 1	A	PM	3/14/2007	0.1	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	1	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 1	A	PM	5/23/2006	0.04	POUNDS PER MILLION BTU HEAT INPUT	#6 oil only
FLORIDA POWER								STEAM TURBINE					POUNDS PER	

CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	1	GENERATOR ANCLOTE UNIT NO. 1	A	PM	7/7/2005	0.045	MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	1	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 1	A	PM	9/24/2004	0.038	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	1	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 1	A	PM	9/16/2003	0.0684	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	1	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 1	A	PM	9/16/2003	0.1171	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	2	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 2	A	PM	10/7/2003	0.0652	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	2	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 2	A	PM	10/7/2003	0.0748	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	2	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 2	A	PM	11/24/2004	0.057	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	2	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 2	A	PM	11/24/2004	0.071	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	2	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 2	A	PM	7/7/2005	0.041	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	2	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 2	A	PM	7/8/2005	0.035	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	2	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 2	A	PM	5/24/2006	0.05	POUNDS PER MILLION BTU HEAT INPUT	# 6 oil only
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	2	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 2	A	PM	5/25/2006	0.08	POUNDS PER MILLION BTU HEAT INPUT	# 6 oil only
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	2	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 2	A	PM	6/21/2007	0.05	POUNDS PER MILLION BTU HEAT INPUT	SOOTBLOWING
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	2	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 2	A	PM	6/21/2007	0.05	POUNDS PER MILLION BTU HEAT INPUT	NON-SOOTBLOWING
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	1	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 1	A	PM	9/25/2004	0.041	POUNDS PER MILLION BTU HEAT INPUT	4605mmbtu/hr
FLORIDA POWER CORPDBAPROGRESS ENERGY FL	1010017	ANCLOTE POWER PLANT	SWD	PASCO	A	Y	1	STEAM TURBINE GENERATOR ANCLOTE UNIT NO. 1	A	PM	7/6/2005	0.051	POUNDS PER MILLION BTU HEAT INPUT	
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H021	4/17/2007	0.000028	POUNDS PER BILLION BTU HEAT INPUT	testar, units really sent in as lb/MMBtu
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	FL	4/17/2007	0.0001	POUNDS PER MILLION BTU HEAT INPUT	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	FL	4/22/2005	0.000113	POUNDS PER MILLION BTU HEAT INPUT	Actual results reported as <0.000113 lb/MMBtu Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	FL	4/22/2004	0.000132	POUNDS PER MILLION BTU HEAT INPUT	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	FL	4/11/2003	0.00013	POUNDS PER MILLION BTU HEAT INPUT	Actual emissions reported as <.00013 lb/MMB Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	FL	4/22/2005	0.000123	POUNDS PER MILLION BTU HEAT INPUT	Actual result reported as <0.000123. Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	FL	4/10/2006	0.000125	POUNDS PER MILLION BTU HEAT INPUT	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	FL	4/17/2007	0.00011	POUNDS PER MILLION BTU HEAT INPUT	
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	NOX	4/17/2007	0.322	POUNDS PER MILLION BTU HEAT INPUT	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	FL	4/22/2004	0.000128	POUNDS PER MILLION BTU HEAT INPUT	Test team: Testar. Result actually reported as <0.000128
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	PB	4/17/2006	0.000005	POUNDS PER MILLION BTU HEAT INPUT	Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	VOC	4/17/2007	0.0012	POUNDS PER MILLION BTU HEAT INPUT	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	FL	4/22/2004	0.000134	POUNDS PER MILLION BTU HEAT INPUT	Test team: Testar. Result actually reported as <0.000134.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	FL	4/11/2003	0.000125	POUNDS PER MILLION BTU HEAT INPUT	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	FL	4/22/2005	0.000117	POUNDS PER MILLION BTU HEAT INPUT	Actual results reported as <0.000117 lb/MMBtu Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	FL	4/11/2006	0.000124	POUNDS PER MILLION BTU HEAT INPUT	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	FL	4/17/2007	0.00011	POUNDS PER MILLION BTU HEAT INPUT	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	FL	4/11/2003	0.000124	POUNDS PER MILLION BTU HEAT INPUT	Actual emissions reported as <0.000124 lb/MM Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	FL	4/11/2006	0.000125	POUNDS PER MILLION BTU HEAT INPUT	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	VOC	4/17/2007	0.0013	POUNDS PER MILLION BTU HEAT INPUT	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H021	4/17/2006	0.000027	POUNDS PER BILLION BTU HEAT INPUT	units really come in as lb/MMBtu
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H021	4/17/2007	0.000026	POUNDS PER BILLION BTU HEAT INPUT	testar, units really sent in as lb/MMBtu
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE	SWD	PASCO	A	Y	1	Municipal waste Combustor	A	VOC	4/17/2007	0.0009	POUNDS PER MILLION BTU	testar

		RECOVERY FACILITY						Unit #1					HEAT INPUT	
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H114	4/22/2005	94.3	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H114	4/22/2004	93.2	PERCENT REDUCTION IN EMISSIONS	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	SO2	4/22/2005	100	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	SO2	4/17/2007	95.8	PERCENT REDUCTION IN EMISSIONS	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	SO2	4/22/2004	97.1	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	SO2	4/11/2003	95.8	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	SO2	4/22/2005	98.7	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H106	4/22/2004	97.7	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H106	4/11/2003	99.3	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H106	4/22/2005	99.1	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H106	4/17/2007	97.7	PERCENT REDUCTION IN EMISSIONS	Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H106	4/22/2004	97.9	PERCENT REDUCTION IN EMISSIONS	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H106	4/11/2003	99	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H106	4/22/2005	98.7	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	SO2	4/22/2004	100	PERCENT REDUCTION IN EMISSIONS	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	SO2	4/11/2003	95.3	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H114	4/11/2003	97.3	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H114	4/22/2004	86.6	PERCENT REDUCTION IN EMISSIONS	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H114	4/17/2007	88.1	PERCENT REDUCTION IN EMISSIONS	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H114	4/11/2006	86.9	PERCENT REDUCTION IN EMISSIONS	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H114	4/11/2003	95.5	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H114	4/22/2005	91.9	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	PM	4/11/2006	0.00105	GRAINS PER DRY STANDARD CUBIC FOOT	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	PM	4/11/2006	0.0016	GRAINS PER DRY STANDARD CUBIC FOOT	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	PM	4/17/2007	0.0014	GRAINS PER DRY STANDARD CUBIC FOOT	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H027	4/17/2007	0.0003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H027	4/11/2006	0.00116	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H027	4/22/2005	0.000872	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H027	4/11/2003	0.00058	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H027	4/22/2004	0.000292	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	PB	4/11/2006	0.00461	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	PB	4/22/2005	0.0162	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	PB	4/11/2003	0.0106	MILLIGRAMS PER DRY STANDARD CUBIC METER	Test team: Testar

													@ 7% O2	
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	PB	4/22/2004	0.0122	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	PM	4/22/2005	5.74	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	PM	4/11/2003	3.74	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	PM	4/22/2004	1.25	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H114	4/11/2006	0.01104	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H114	4/22/2005	0.00449	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H114	4/11/2003	0.00332	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H114	4/22/2004	0.0132	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	PM	4/17/2007	2.15	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	PM	4/22/2005	4.75	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	PM	4/11/2003	1.71	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	PM	4/22/2004	1.29	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H027	4/15/2007	0.00055	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H027	4/11/2006	0.0005	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H027	4/22/2005	0.0013	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H027	4/11/2003	0.00064	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H027	4/22/2004	0.00036	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	PB	4/17/2007	0.00094	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	PB	4/11/2006	0.00934	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	PB	4/22/2005	0.00907	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	PB	4/11/2003	0.00432	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	PB	4/22/2004	0.00247	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	NOX	4/17/2007	185	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	NOX	4/11/2006	194	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	NOX	4/22/2005	187	PARTS PER MILLION DRY GAS VOLUME	Test team: Testar

		RECOVERY FACILITY											@ 7% O2	
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	NOX	4/11/2003	182	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	NOX	4/22/2004	187	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	CO	4/17/2007	15	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	CO	4/11/2006	9	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	CO	4/22/2005	11	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	CO	4/11/2003	15	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	CO	4/22/2004	16	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	CO	4/11/2006	7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	CO	4/22/2005	10	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	CO	4/11/2003	11	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	CO	4/22/2004	13	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	NOX	4/11/2006	187	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	NOX	4/22/2005	188	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	NOX	4/11/2003	184	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	NOX	4/22/2004	189	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	CO	4/16/2007	10	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	NOX	4/17/2007	191	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	NOX	4/11/2006	191	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	NOX	4/22/2005	189	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	NOX	4/11/2003	188	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	NOX	4/22/2004	191	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	CO	4/17/2007	9	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	CO	4/22/2005	7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	CO	4/11/2003	13	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	CO	4/22/2004	13	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	SO2	4/16/2007	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H106	4/17/2007	11.7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H106	4/10/2006	10.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H106	4/22/2005	7.95	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE	SWD	PASCO	A	Y	3	Municipal Waste Combustor	A	SO2	4/17/2007	2	PARTS PER MILLION DRY	testar

		RECOVERY FACILITY						Unit #3					GAS VOLUME @ 7% O2	
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H106	4/11/2006	13.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testsar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H106	4/22/2005	6.62	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H106	4/11/2003	5.12	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H106	4/22/2004	11.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	SO2	4/22/2005	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	SO2	4/11/2003	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	SO2	4/22/2004	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H106	4/17/2007	13.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H106	4/11/2006	12.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H106	4/22/2005	9.98	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H106	4/11/2003	4.95	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H106	4/22/2004	8.74	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	SO2	4/11/2006	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	SO2	4/22/2005	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	SO2	4/11/2003	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	SO2	4/22/2004	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	SO2	4/11/2006	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	SO2	4/22/2005	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	SO2	4/11/2003	2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	SO2	4/22/2004	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H106	4/11/2003	6.04	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H106	4/22/2004	11.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H114	4/16/2007	18	MICROGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H021	4/22/2005	0	POUNDS/HOUR	Actual results reported as <0.0000000314 lb/hr team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H021	4/11/2006	0	POUNDS/HOUR	actual emissions are .0000000323 but won't acc testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H106	4/22/2004	98.5	PERCENT REDUCTION IN EMISSIONS	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H106	4/11/2003	99	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H106	4/22/2005	98.5	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H021	4/22/2004	0	POUNDS/HOUR	Test team: Testar. Actual result reported as <3. 08.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H021	4/11/2003	0.000005	POUNDS/HOUR	Actual emissions reported as <0.0000000321 lb/MMBtu. Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H021	4/22/2005	0	POUNDS/HOUR	Actual result was <0.0000000331. Test team: T

PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H021	4/11/2006	0.000005	POUNDS/HOUR	Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H021	4/22/2004	0	POUNDS/HOUR	Test team: Testar. Actual reported result <3.48
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H021	4/11/2003	0.000005	POUNDS/HOUR	Actual result <.00000522 lb/hr and <0.0000000 lb/MMBtu. Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	SO2	4/22/2004	97.1	PERCENT REDUCTION IN EMISSIONS	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H114	4/11/2003	96.9	PERCENT REDUCTION IN EMISSIONS	
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H114	4/22/2004	86.5	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	SO2	4/11/2006	94	PERCENT REDUCTION IN EMISSIONS	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	SO2	4/11/2003	95.2	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	SO2	4/22/2005	99	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H114	4/22/2005	95.9	PERCENT REDUCTION IN EMISSIONS	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	H114	4/11/2006	87	PERCENT REDUCTION IN EMISSIONS	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H021	4/22/2004	0	POUNDS/HOUR	Test team: Testar. Actual result reported as <3. 08.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H021	4/11/2003	0.000005	POUNDS/HOUR	Actual emissions <0.00000484 lb/hr and <0.0000000314 lb/MMBtu. Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H021	4/22/2005	0	POUNDS/HOUR	Actual result reported as <0.0000000318 lb/hr. team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H021	4/11/2006	0	POUNDS/HOUR	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H114	4/22/2004	0.00659	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H114	4/11/2003	0.00411	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	PM	4/17/2007	3.58	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	PM	4/10/2006	0.782	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	PM	4/22/2005	6	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	PM	4/11/2003	4.67	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	PM	4/22/2004	1.39	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H114	4/11/2006	0.0179	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H114	4/17/2007	0.0105	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H114	4/22/2005	0.00492	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	DIOX	4/11/2003	4.52	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar. Other unit tested in 2004.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	DIOX	4/11/2006	3.69	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	DIOX	4/22/2004	5.62	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	DIOX	4/17/2007	0.987	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	1	Municipal waste Combustor Unit #1	A	DIOX	4/22/2005	0.684	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar

PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	PB	4/17/2007	0.00232	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	PB	4/11/2006	0.01593	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	PB	4/22/2005	0.00666	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	PB	4/11/2003	0.0107	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	PB	4/22/2004	0.00523	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H027	4/17/2007	0.00018	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H027	4/11/2006	0.0009	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H027	4/22/2005	0.000967	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H027	4/11/2003	0.00031	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	3	Municipal Waste Combustor Unit #3	A	H027	4/22/2004	0.000278	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar.
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H114	4/22/2005	0.0082	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H114	4/11/2003	0.00506	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar
PASCO COUNTY	1010056	PASCO COUNTY RESOURCE RECOVERY FACILITY	SWD	PASCO	A	Y	2	Municipal Waste Combustor Unit #2	A	H114	4/22/2004	0.0123	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Test team: Testar.
PASCO COGEN LIMITED	1010071	PASCO COGEN LIMITED	SWD	PASCO	A	Y	2	COMBUSTION TURBINE (CT) WITH HRSG AND DBS	A	NOX	6/1/2007	21.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
PASCO COGEN LIMITED	1010071	PASCO COGEN LIMITED	SWD	PASCO	A	Y	2	COMBUSTION TURBINE (CT) WITH HRSG AND DBS	A	NOX	7/13/2006	24.64	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
PASCO COGEN LIMITED	1010071	PASCO COGEN LIMITED	SWD	PASCO	A	Y	2	COMBUSTION TURBINE (CT) WITH HRSG AND DBS	A	NOX	7/31/2003	24.32	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
PASCO COGEN LIMITED	1010071	PASCO COGEN LIMITED	SWD	PASCO	A	Y	2	COMBUSTION TURBINE (CT) WITH HRSG AND DBS	A	NOX	4/23/2004	23.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
PASCO COGEN LIMITED	1010071	PASCO COGEN LIMITED	SWD	PASCO	A	Y	2	COMBUSTION TURBINE (CT) WITH HRSG AND DBS	A	NOX	8/10/2005	24.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
PASCO COGEN LIMITED	1010071	PASCO COGEN LIMITED	SWD	PASCO	A	Y	1	COMBUSTION TURBINE (CT) WITH HRSG AND DBS	A	NOX	4/22/2004	24.4	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
PASCO COGEN LIMITED	1010071	PASCO COGEN LIMITED	SWD	PASCO	A	Y	1	COMBUSTION TURBINE (CT) WITH HRSG AND DBS	A	NOX	8/1/2003	24.47	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
PASCO COGEN LIMITED	1010071	PASCO COGEN LIMITED	SWD	PASCO	A	Y	1	COMBUSTION TURBINE (CT) WITH HRSG AND DBS	A	NOX	8/10/2005	23.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
PASCO COGEN LIMITED	1010071	PASCO COGEN LIMITED	SWD	PASCO	A	Y	1	COMBUSTION TURBINE (CT) WITH HRSG AND DBS	A	NOX	7/14/2006	23.85	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
PASCO COGEN LIMITED	1010071	PASCO COGEN LIMITED	SWD	PASCO	A	Y	1	COMBUSTION TURBINE (CT) WITH HRSG AND DBS	A	NOX	1/4/2007	24.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	REPLACEMENT ENGINE TEST BASE LOA
PASCO COGEN LIMITED	1010071	PASCO COGEN LIMITED	SWD	PASCO	A	Y	1	COMBUSTION TURBINE (CT) WITH HRSG AND DBS	A	NOX	6/1/2007	21.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	C T AND DUCT BURNER
PASCO COGEN LIMITED	1010071	PASCO COGEN LIMITED	SWD	PASCO	A	Y	1	COMBUSTION TURBINE (CT) WITH HRSG AND DBS	A	NOX	10/5/2007	24.8	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
PASCO COGEN LIMITED	1010071	PASCO COGEN LIMITED	SWD	PASCO	A	Y	1	COMBUSTION TURBINE (CT) WITH HRSG AND DBS	A	CO	1/4/2007	22.5	PARTS PER MILLION DRY GAS VOLUME	BASE LOAD TEST OF REPLACEMENT ENGINE
PASCO COGEN LIMITED	1010071	PASCO COGEN LIMITED	SWD	PASCO	A	Y	1	COMBUSTION TURBINE (CT) WITH HRSG AND DBS	A	CO	4/22/2004	25.2	PARTS PER MILLION DRY GAS VOLUME	
PASCO COGEN	1010071	PASCO COGEN	SWD	PASCO	A	Y	2	COMBUSTION TURBINE (CT) WITH HRSG AND	A	CO	4/23/2004	26.3	PARTS PER MILLION DRY	

LIMITED		LIMITED						DBS					GAS VOLUME	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	4/11/2007	0.26	PARTS PER MILLION DRY GAS VOLUME	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/2/2003	0.29	PARTS PER MILLION DRY GAS VOLUME	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/5/2003	0.2	PARTS PER MILLION DRY GAS VOLUME	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/16/2005	0.07	PARTS PER MILLION DRY GAS VOLUME	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/26/2004	0.3	PARTS PER MILLION DRY GAS VOLUME	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/11/2006	0.36	PARTS PER MILLION DRY GAS VOLUME	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	4/11/2007	0.17	PARTS PER MILLION DRY GAS VOLUME	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	6/4/2003	0.23	PARTS PER MILLION DRY GAS VOLUME	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/27/2004	0.2	PARTS PER MILLION DRY GAS VOLUME	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/10/2006	0.21	PARTS PER MILLION DRY GAS VOLUME	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	4/11/2007	0.31	PARTS PER MILLION DRY GAS VOLUME	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/8/2006	0.25	PARTS PER MILLION DRY GAS VOLUME	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/17/2005	0.17	PARTS PER MILLION DRY GAS VOLUME	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	CO	5/24/2004	0.14	PARTS PER MILLION DRY GAS VOLUME	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	4/11/2007	7.17	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/27/2004	7.64	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	4/11/2007	6.68	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/4/2003	6.75	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	2	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/10/2006	7.03	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	4/11/2007	0	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/24/2004	7.5	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/2/2003	6.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	6/5/2003	6.54	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/16/2005	6.66	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/26/2004	7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/11/2006	6.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	3	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	4/12/2007	7.04	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/17/2005	7.05	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
SHADY HILLS POWER COMPANY, L.L.C.	1010373	SHADY HILLS GENERATING STATION	SWD	PASCO	A	Y	1	A 170 MW Gas Simple Cycle Combustion Turbine	A	NOX	5/8/2006	6.85	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	2	No.2 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	5/23/2007	0.076	POUNDS PER MILLION BTU HEAT INPUT	The consultant company was CEM Solutions. j
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	2	No.2 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	5/23/2005	0.0436	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	2	No.2 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	8/27/2003	0.248	POUNDS PER MILLION BTU HEAT INPUT	Testing team was Environmental Source Sampl Inc. 18631-H Northline Drive, Cornelius North Carolina 28031. JAR
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	2	No.2 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	8/27/2003	0.066	POUNDS PER MILLION BTU HEAT INPUT	Testing team was Environmental Source Sampl Inc. 18631-H Northline Drive, Cornelius North Carolina 28031. JAR
FLORIDA POWER CORPDBAPROGRESS	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	2	No.2 Unit, FFSG (Phase II	A	PM	5/23/2005	0.0794	POUNDS PER MILLION BTU	

ENERGY FLA								Acid Rain Unit)					HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	2	No.2 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	6/2/2004	0.239	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	2	No.2 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	5/23/2007	0.055	POUNDS PER MILLION BTU HEAT INPUT	The consultant company was CEM Solutions. J
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	2	No.2 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	8/8/2006	0.037	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	2	No.2 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	8/8/2006	0.045	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	2	No.2 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	6/2/2004	0.0397	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	3	No.3 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	5/16/2007	0.0435	POUNDS PER MILLION BTU HEAT INPUT	In compliance. jar
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	3	No.3 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	5/26/2005	0.0332	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	3	No.3 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	8/28/2003	0.0804	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	1	No.1 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	5/26/2005	0.0203	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	1	No.1 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	6/1/2004	0.0303	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	1	No.1 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	6/1/2004	0.041	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	1	No.1 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	8/9/2006	0.026	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	1	No.1 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	8/9/2006	0.035	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	1	No.1 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	8/9/2006	0.033	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	1	No.1 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	5/30/2007	0.01	POUNDS PER MILLION BTU HEAT INPUT	Normal Mode(test team-CEMs Solutions)
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	1	No.1 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	5/30/2007	0.01	POUNDS PER MILLION BTU HEAT INPUT	In compliance ATR(Test Team- CEMs Solutio
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	3	No.3 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	8/28/2003	0.1726	POUNDS PER MILLION BTU HEAT INPUT	In Com PLiance. JAR
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	1	No.1 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	8/26/2003	0.0502	POUNDS PER MILLION BTU HEAT INPUT	In Compliance. JAR
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	1	No.1 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	8/26/2003	0.0642	POUNDS PER MILLION BTU HEAT INPUT	In Compliance. JAR
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	1	No.1 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	5/26/2005	0.0236	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	3	No.3 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	5/24/2005	0.08687	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	3	No.3 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	6/3/2004	0.255	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	3	No.3 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	9/25/2006	0.01	POUNDS PER MILLION BTU HEAT INPUT	In compliance
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	3	No.3 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	9/25/2006	0.0499	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	3	No.3 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	6/3/2004	0.0798	POUNDS PER MILLION BTU HEAT INPUT	
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	3	No.3 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	8/8/2006	0.0499	POUNDS PER MILLION BTU HEAT INPUT	In compliance
FLORIDA POWER CORPDBAPROGRESS ENERGY FLA	1030011	BARTOW PLANT	SWPN	PINELLAS	A	Y	3	No.3 Unit, FFSG (Phase II Acid Rain Unit)	A	PM	5/16/2007	0.0561	POUNDS PER MILLION BTU HEAT INPUT	In compliance. jar
HONEYWELL INTERNATIONAL	1030019	HONEYWELL, CLEARWATER	SWPN	PINELLAS	A	Y	1	PLANT 1 - BERYLLIUM OPERATIONS	A	H021	3/13/2007	0.000735	GRAMS/DAY (24 HOURS)	99.99% under the limit[jm]
HONEYWELL INTERNATIONAL	1030019	HONEYWELL, CLEARWATER	SWPN	PINELLAS	A	Y	1	PLANT 1 - BERYLLIUM OPERATIONS	A	H021	2/27/2005	0.0028	GRAMS/DAY (24 HOURS)	
HONEYWELL INTERNATIONAL	1030019	HONEYWELL, CLEARWATER	SWPN	PINELLAS	A	Y	1	PLANT 1 - BERYLLIUM OPERATIONS	A	H021	2/27/2003	0.003	GRAMS/DAY (24 HOURS)	
HONEYWELL INTERNATIONAL	1030019	HONEYWELL, CLEARWATER	SWPN	PINELLAS	A	Y	1	PLANT 1 - BERYLLIUM OPERATIONS	A	H021	3/2/2004	0.0029	GRAMS/DAY (24 HOURS)	
HONEYWELL INTERNATIONAL	1030019	HONEYWELL, CLEARWATER	SWPN	PINELLAS	A	Y	1	PLANT 1 - BERYLLIUM OPERATIONS	A	H021	2/21/2006	0.0029	GRAMS/DAY (24 HOURS)	
CITY OF LARGO - WWTP	1030060	CITY OF LARGO WASTEWATER TREATMENT PLANT	SWPN	PINELLAS	A	Y	1	SLUDGE DRYING TRAINS 1 & 2 WITH COMMON THERMAL OXIDIZER	A	H114	5/10/2003	29.38	GRAMS/DAY (24 HOURS)	
CITY OF LARGO - WWTP	1030060	CITY OF LARGO WASTEWATER TREATMENT PLANT	SWPN	PINELLAS	A	Y	3	PELLETIZING BUILDING WITH WET SCRUBBER ODOR CONTROL SYSTEM	A	H114	5/13/2003	29.38	GRAMS/DAY (24 HOURS)	In Compliance. JAR
CITY OF LARGO - WWTP	1030060	CITY OF LARGO WASTEWATER TREATMENT PLANT	SWPN	PINELLAS	A	Y	1	SLUDGE DRYING TRAINS 1 & 2 WITH COMMON THERMAL OXIDIZER	A	PM	5/13/2003	0.00171	GRAINS PER DRY STANDARD CUBIC FOOT	In Compliance. JAR
CITY OF LARGO - WWTP	1030060	CITY OF LARGO WASTEWATER TREATMENT PLANT	SWPN	PINELLAS	A	Y	1	SLUDGE DRYING TRAINS 1 & 2 WITH COMMON THERMAL OXIDIZER	A	VOC	5/13/2003	0.085	POUNDS/HOUR	
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	H106	9/18/2007	0.0011	POUNDS/HOUR	Air testing & Consulting. JAR
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	H106	9/19/2006	0.024	POUNDS/HOUR	In compliance. JAR Testing Team: ATC Air Te & Consulting

BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	H106	9/23/2004	0.117	POUNDS/HOUR	
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	H106	9/20/2005	0.0212	POUNDS/HOUR	Air Testing & Consulting was the consultant.
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	PM	9/23/2004	0.0099	GRAINS PER DRY STANDARD CUBIC FOOT	
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	PM	9/19/2006	0.0062	GRAINS PER DRY STANDARD CUBIC FOOT	In compliance. JAR Testing Team: ATC Air Te & Consulting
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	CO	9/20/2005	2.33	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing & Consulting was the consultant.
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	CO	9/18/2007	6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	In compliance. JAR
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	H027	9/20/2005	0.0028	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Air Testing & Consulting was the consultant.
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	PB	9/20/2005	0.0667	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Air Testing & Consulting was the consultant.
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	SO2	9/20/2005	2.32	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing & Consulting was the consultant.
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	CO	9/19/2006	19.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	In compliance. JAR Testing Team: ATC Air Te & Consulting
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	CO	9/23/2004	1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing & Consulting. JAR
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	PM	9/20/2005	0.0045	GRAINS PER DRY STANDARD CUBIC FOOT	Air Testing & Consulting was the consultant.
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	PM	9/18/2007	0.006	GRAINS PER DRY STANDARD CUBIC FOOT	Air Testing & Consulting; In compliance. JAR
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	NOX	9/20/2005	141	PARTS PER MILLION DRY GAS VOLUME	Air Testing & Consulting was the consultant.
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	H114	9/20/2005	0.00181	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Air Testing & Consulting was the consultant.
BAYFRONT-ST. ANTHONY'S HEALTH CARE	1030095	BAYFRONT MEDICAL CENTER	SWPN	PINELLAS	A	Y	2	MEDICAL WASTE INCINERATOR. 1500 POUNDS PER HOUR.	A	DIOX	9/20/2005	0.442	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Air Testing & Consulting was the consultant.
MI METALS, INC./METAL INDUSTRIES, INC.	1030114	MI METALS - OLDSMAR	SWPN	PINELLAS	A	Y	1	Secondary Aluminum Production: Mode A & Mode B	A	DIOX	3/11/2003	0	POUNDS/HOUR	Actual results were 0.00000003
MI METALS, INC./METAL INDUSTRIES, INC.	1030114	MI METALS - OLDSMAR	SWPN	PINELLAS	A	Y	1	Secondary Aluminum Production: Mode A & Mode B	A	DIOX	9/24/2003	0.000001	POUNDS/HOUR	
MI METALS, INC./METAL INDUSTRIES, INC.	1030114	MI METALS - OLDSMAR	SWPN	PINELLAS	A	Y	1	Secondary Aluminum Production: Mode A & Mode B	A	PM	8/15/2003	0.065	POUNDS/HOUR	Average of three one-hour runs ranged from 0.(0.11 lbs./hour. Test ran on 8/13/03, 14 and - 15
MI METALS, INC./METAL INDUSTRIES, INC.	1030114	MI METALS - OLDSMAR	SWPN	PINELLAS	A	Y	1	Secondary Aluminum Production: Mode A & Mode B	A	PM	3/13/2003	2.57	POUNDS/HOUR	% Isokinetic on first of three one hour runs was 61%. Accepted results. mvh
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	4/28/2004	95	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	4/25/2003	91	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	4/27/2004	97	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	4/25/2003	95	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	4/21/2005	95	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	4/27/2006	98	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H021	4/27/2007	0.000029	POUNDS/HOUR	clean air
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	4/25/2003	78	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	4/29/2004	81.3	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	4/25/2003	85	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	4/27/2004	86.6	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	4/25/2003	98	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	4/29/2004	89.9	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO.	1030117	PINELLAS CO. RESOURCE	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor	A	H114	4/25/2003	94	PERCENT REDUCTION IN	

COMMISSIONERS		RECOVERY FACILITY						& Auxiliary burners-Unit #1					EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	4/21/2005	99	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	4/25/2003	96	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	4/21/2005	98	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	4/28/2004	97	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	4/27/2006	98	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	4/25/2003	98	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	4/21/2005	99	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	4/27/2004	99	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H021	4/25/2003	0.00001	POUNDS/HOUR	Actual result reported as <0.00001 lb/hr
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H021	4/21/2005	0.000009	POUNDS/HOUR	Actual results reported as <0.0000097 lb/hr
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H021	4/27/2004	0.00001	POUNDS/HOUR	Actual results reported as <0.00001 lb/hr
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	4/29/2004	71	PERCENT REDUCTION IN EMISSIONS	Passes because rule requires meeting either mg/dscm standard or removal standard, not bot
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	4/27/2006	92	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	4/25/2003	99	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	4/21/2005	99	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	4/29/2004	97	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	4/21/2005	95	PERCENT REDUCTION IN EMISSIONS	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	FL	4/21/2005	0.0105	POUNDS/HOUR	Actual results reported as <0.0105 lb/hr
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	4/25/2003	0.0067	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	4/21/2005	0.0016	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H027	4/21/2005	0.00043	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	4/21/2005	0.0056	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	DIOX	4/27/2004	0.83	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	DIOX	4/27/2006	2	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	DIOX	4/27/2007	0.44	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	clean air
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	4/28/2004	0.0039	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	4/21/2005	0.0051	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	4/25/2003	0.0056	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PB	4/27/2007	0.012	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	clean air
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PB	4/27/2004	0.0017	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PB	4/21/2005	0.028	MILLIGRAMS PER DRY STANDARD CUBIC METER	

													@ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PB	4/25/2003	0.004	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	4/27/2007	0.0018	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	clean air
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	4/27/2004	0.0024	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	DIOX	4/21/2005	1.1	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	DIOX	4/25/2003	0.36	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	DIOX	4/25/2006	0.0077	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PM	4/27/2007	2.9	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	clean air
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PM	4/27/2006	3.6	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PM	4/28/2004	1.6	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PM	4/21/2005	1.4	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PM	4/25/2003	2	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	4/27/2007	0.0016	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	clean air
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H114	4/27/2006	0.011	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H114	4/25/2003	0.0057	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H027	4/27/2006	0.00072	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H027	4/27/2007	0.0013	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	clean air
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H027	4/29/2004	0.00012	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Results actually reported as <0.00012 mg/dscm
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H027	4/25/2003	0.00091	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H114	4/29/2004	0.035	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	8	ASH CONDITIONING BUILDING	A	PM	7/28/2005	0.002	GRAINS PER DRY STANDARD CUBIC FOOT	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	4/27/2006	13	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	4/27/2004	7.1	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	SO2	4/25/2003	8.2	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	4/29/2004	10.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	SO2	4/25/2003	9.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO.		PINELLAS CO.											PARTS PER	

BOARD OF CO. COMMISSIONERS	1030117	RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	NOX	4/29/2004	188	MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	NOX	4/25/2003	189.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	4/27/2007	6.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	clean air
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	4/27/2004	7.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	4/21/2005	7.9	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H106	4/25/2003	13	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	NOX	4/27/2004	171.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	NOX	4/25/2003	196	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H027	4/27/2004	0.00012	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Actual result reported as <0.00012 mg/dscm
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H027	4/21/2005	0.0033	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H027	4/25/2003	0.00072	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H027	4/27/2007	0.00018	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	clean air
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H027	4/27/2006	0.0015	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H027	4/28/2004	0.0005	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H027	4/21/2005	0.00025	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H027	4/25/2003	0.00096	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PB	4/27/2006	0.011	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PB	4/27/2007	0.0057	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	clean air
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PB	4/27/2006	0.00242	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PB	4/29/2004	0.00042	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PB	4/21/2005	0.0035	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PB	4/25/2003	0.0094	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	4/29/2004	0.75	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	Results actually reported as <0.75 mg/dscm
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	4/21/2005	0.91	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	4/25/2003	4.7	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PM	4/27/2007	7.4	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	clean air

PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PM	4/27/2006	2.6	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PM	4/27/2004	0.96	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PM	4/21/2005	7.4	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	PM	4/25/2003	3	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	H027	4/27/2007	0.0013	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	clean air
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	4/27/2007	4.4	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	clean air
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	PM	4/27/2006	2.6	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PB	4/28/2004	0.0078	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PB	4/21/2005	0.003	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PB	4/25/2003	0.0055	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	CO	4/27/2004	13.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	CO	4/25/2003	10.8	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	NOX	4/29/2004	180.9	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	NOX	4/25/2003	187.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	CO	4/28/2004	13.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	PB	4/27/2007	0.0016	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	clean air
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	CO	4/25/2003	12.7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	4/27/2007	9	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	clean air
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	4/27/2006	16	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	4/29/2004	18	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	4/21/2005	6.6	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	1	Municipal Waste Combustor & Auxiliary burners-Unit #1	A	H106	4/25/2003	5.4	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	4/29/2004	9.5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	3	Municipal Waste Combustor & Auxiliary burners-Unit #3	A	SO2	4/25/2003	1.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	4/27/2007	13	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	clean air
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	4/28/2004	15	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	CO	4/25/2003	13.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO.		PINELLAS CO.						Municipal Waste Combustor					PARTS PER MILLION DRY	

BOARD OF CO. COMMISSIONERS	1030117	RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	& Auxiliary burners-Unit #2	A	CO	4/29/2004	19.4	GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	4/21/2005	13	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	2	Municipal Waste Combustor & Auxiliary burners-Unit #2	A	H106	4/25/2003	22	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
PINELLAS CO. BOARD OF CO. COMMISSIONERS	1030117	PINELLAS CO. RESOURCE RECOVERY FACILITY	SWD	PINELLAS	A	Y	5	METALS RECOVERY SYSTEM	A	PM	7/28/2005	0.005	GRAINS PER DRY STANDARD CUBIC FOOT	
SCHNELLER LLC	1030118	SCHNELLER LLC	SWPN	PINELLAS	A	Y	3	COATING LINE WITH THERMAL INCINERATOR	A	VOC	5/3/2006	1.39	POUNDS/HOUR	In compliance. Ammended process rate of 255. lbs VOC/hr, at 1240 F. ET.
SCHNELLER LLC	1030118	SCHNELLER LLC	SWPN	PINELLAS	A	Y	3	COATING LINE WITH THERMAL INCINERATOR	A	VOC	10/18/2005	1.7	POUNDS/HOUR	Environmental Sciences Group
SCHNELLER LLC	1030118	SCHNELLER LLC	SWPN	PINELLAS	A	Y	3	COATING LINE WITH THERMAL INCINERATOR	A	VOC	4/30/2003	1.17	POUNDS/HOUR	IN Compliance [wrf]
FILM TECHNOLOGIES INT, INC	1030119	FILM TECHNOLOGIES INT, INC	SWPN	PINELLAS	A	Y	2	COATING LINE NO. 2 WITH CATALYTIC INCINERATOR	A	VOC	1/28/2004	0.79	POUNDS PER GALLON OF COATING, EXCLUDING WATER	
FILM TECHNOLOGIES INT, INC	1030119	FILM TECHNOLOGIES INT, INC	SWPN	PINELLAS	A	Y	1	COATING LINE NO. 1, WITH CATALYTIC INCINERATOR & MIXING ROOM	A	VOC	1/10/2007	0.693	OTHER (SPECIFY IN COMMENT)	
FILM TECHNOLOGIES INT, INC	1030119	FILM TECHNOLOGIES INT, INC	SWPN	PINELLAS	A	Y	2	COATING LINE NO. 2 WITH CATALYTIC INCINERATOR	A	VOC	2/5/2003	0.396	OTHER (SPECIFY IN COMMENT)	Source considered in compliance JAR
FILM TECHNOLOGIES INT, INC	1030119	FILM TECHNOLOGIES INT, INC	SWPN	PINELLAS	A	Y	2	COATING LINE NO. 2 WITH CATALYTIC INCINERATOR	A	VOC	1/28/2004	0.62	OTHER (SPECIFY IN COMMENT)	Units for Actual Emissions are lbs/Gallon of Sc ET
FILM TECHNOLOGIES INT, INC	1030119	FILM TECHNOLOGIES INT, INC	SWPN	PINELLAS	A	Y	2	COATING LINE NO. 2 WITH CATALYTIC INCINERATOR	A	VOC	2/2/2005	0.46	OTHER (SPECIFY IN COMMENT)	0.46 lbs VOC/Gal solid applied.ET.
FILM TECHNOLOGIES INT, INC	1030119	FILM TECHNOLOGIES INT, INC	SWPN	PINELLAS	A	Y	2	COATING LINE NO. 2 WITH CATALYTIC INCINERATOR	A	VOC	4/5/2006	0.985	OTHER (SPECIFY IN COMMENT)	lbs VOC/gallon of solids applied. et
FILM TECHNOLOGIES INT, INC	1030119	FILM TECHNOLOGIES INT, INC	SWPN	PINELLAS	A	Y	2	COATING LINE NO. 2 WITH CATALYTIC INCINERATOR	A	VOC	1/10/2007	0.376	OTHER (SPECIFY IN COMMENT)	
FILM TECHNOLOGIES INT, INC	1030119	FILM TECHNOLOGIES INT, INC	SWPN	PINELLAS	A	Y	1	COATING LINE NO. 1, WITH CATALYTIC INCINERATOR & MIXING ROOM	A	VOC	2/4/2003	2.33	OTHER (SPECIFY IN COMMENT)	
FILM TECHNOLOGIES INT, INC	1030119	FILM TECHNOLOGIES INT, INC	SWPN	PINELLAS	A	Y	1	COATING LINE NO. 1, WITH CATALYTIC INCINERATOR & MIXING ROOM	A	VOC	1/27/2004	0.82	OTHER (SPECIFY IN COMMENT)	Units for Test Actual are pounds VOC emitted gallon of Solids. JAR
FILM TECHNOLOGIES INT, INC	1030119	FILM TECHNOLOGIES INT, INC	SWPN	PINELLAS	A	Y	1	COATING LINE NO. 1, WITH CATALYTIC INCINERATOR & MIXING ROOM	A	VOC	2/3/2005	0.65	OTHER (SPECIFY IN COMMENT)	0.65 lbs VOC/Gal solid applied. ET.
FILM TECHNOLOGIES INT, INC	1030119	FILM TECHNOLOGIES INT, INC	SWPN	PINELLAS	A	Y	1	COATING LINE NO. 1, WITH CATALYTIC INCINERATOR & MIXING ROOM	A	VOC	4/14/2006	0.985	OTHER (SPECIFY IN COMMENT)	lbs VOC/gallon of solids applied. et
BLUE HAWAIIAN PRODUCTS, INC.	1030162	BLUE HAWAIIAN PRODUCTS, INC. - LARGO PLT	SWPN	PINELLAS	A	Y	1	REINFORCED PLASTIC COMPOSITES PRODUCTION FACILITY	A	VOC	5/30/2005	0	TONS/YEAR	Velocity Flow test Method 2A Minimum requi velocity 47.9 ft/sec Received Past Due sljperfo and observed slj
BLUE HAWAIIAN PRODUCTS, INC.	1030162	BLUE HAWAIIAN PRODUCTS, INC. - LARGO PLT	SWPN	PINELLAS	A	Y	1	REINFORCED PLASTIC COMPOSITES PRODUCTION FACILITY	A	H163	5/23/2006	0	TONS/MONTH	Permit Flow rate requirement = 47.89 ft/second test results for North stack = 53.55 ft/second 17 ACFM South stack = 57.26 ft/second 19205 A passed slj This was attached to CA activity ST 8/1/2006.
MEDLINE INDUSTRIES, INC.	1030197	MEDLINE INDUSTRIES, INC.	SWPN	PINELLAS	A	Y	1	ETHYLENE OXIDE STERILIZATION UNIT	A	H092	11/15/2006	0.000012	POUNDS/DAY	
MEDLINE INDUSTRIES, INC.	1030197	MEDLINE INDUSTRIES, INC.	SWPN	PINELLAS	A	Y	1	ETHYLENE OXIDE STERILIZATION UNIT	A	H092	12/11/2003	0.153	POUNDS/DAY	Air Testing and Consulting
MEDLINE INDUSTRIES, INC.	1030197	MEDLINE INDUSTRIES, INC.	SWPN	PINELLAS	A	Y	1	ETHYLENE OXIDE STERILIZATION UNIT	A	H092	11/30/2004	0.1074	POUNDS/DAY	operating at 128 lb load
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	PM	1/22/2003	0.001	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	In compliance for PM. [wrm]
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	PM	1/22/2003	0.001	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	PM	3/11/2004	0.0037	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Air Testing & Consulting, INC. 813-651-0878
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	PM	9/27/2006	0.006	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	In compliance. JAR
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	H106	3/11/2004	5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing & Consulting, Inc. 813-651-0878
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	H106	2/9/2005	9	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Testing delayed for maintenance; revised next t date. [wrm]
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	H106	9/27/2006	11	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	In compliance. 9/27/06 11/3/06 JAR
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	NOX	9/27/2006	215	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	In compliance. JAR
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	H027	9/5/2006	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	In compliance. JAR Testing Team: ATC Air Te & Consulting
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE	I	SO2	9/27/2006	7	PARTS PER MILLION DRY GAS VOLUME	In compliance. JASR

								INCINERATOR					@ 7% O2	
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	SO2	9/5/2006	7	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	In compliance. JAR Testing Team: ATC Air Te & Consulting
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	CO	9/27/2006	11	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	CO	9/27/2006	11	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	in compliance. JAR
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	CO	9/5/2006	11	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	In compliance. JAR Testing Team: ATC Air Te & Consulting
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	CO	2/9/2005	5	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Revised next test date. GP notification expires 12/20/07. [wrm]
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	CO	3/11/2004	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Air Testing & Consulting , Inc. 813-651-0878
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	CO	1/22/2003	0	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	CO emissions were measured as zero. In compl with CO. [wrm]
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	H114	9/27/2006	0.01	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	H114	9/5/2006	0.01	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	In compliance. JAR Testing Team: ATC Air Te & Consulting
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	PB	9/27/2006	0.03	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	In compliance. jAR
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	PB	9/5/2006	0.03	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	In compliance. JAR Testing Team: ATC Air Te & Consulting
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	H027	9/27/2006	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	H027	9/5/2006	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	In compliance. JAR Testing Team: ATC Air Te & Consulting
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	H027	9/5/2006	0	MILLIGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	In compliance. JAR Testing Team: ATC Air Te & Consulting
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	NOX	9/5/2006	215.3	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	In compliance. JAR Testing Team: ATC Air Te & Consulting
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	H106	9/5/2006	11	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	In compliance. JAR Testing Team: ATC Air Te & Consulting
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	H106	1/22/2003	183	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Exceeded 50 ppmv ELS in permit. wrm
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	H106	2/13/2003	31.48	PARTS PER MILLION DRY GAS VOLUME @ 7% O2	Retest put the source back in compliance. Enforcement case in process. wrm
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	PM	9/5/2006	0.0062	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	In compliance. JAR Testing Team: ATC Air Te & Consulting
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	PM	2/9/2005	0.005	GRAINS PER DRY STANDARD CUBIC FOOT @ 7% O2	Testing delayed for maintenance; revised next t date. [wrm]
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	DIOX	9/27/2006	2.1	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	In compliance. JAR
MEDICO ENVIRONMENTAL SERVICES, INC.	1030210	MEDICO ENVIRONMENTAL SERVICES, INC.	SWPN	PINELLAS	I	Y	1	SIMONDS MFG, MODEL 4F7D; 2350 #/HR MEDICAL WASTE INCINERATOR	I	DIOX	9/5/2006	76	NANOGRAMS PER DRY STANDARD CUBIC METER @ 7% O2	In compliance. JAR Testing Team: ATC Air Te & Consulting
PINELLAS COUNTY GOVERNMENT	1030234	SOUTH CROSS BAYOU WATER RECLAMATION FAC	SWD	PINELLAS	A	Y	6	Sewage Sludge Dryer	A	H114	5/7/2003	2.79	GRAMS/DAY (24 HOURS)	
PINELLAS COUNTY GOVERNMENT	1030234	SOUTH CROSS BAYOU WATER RECLAMATION FAC	SWD	PINELLAS	A	Y	6	Sewage Sludge Dryer	A	PM	5/7/2003	0.709	POUNDS/HOUR	
CITROSUCO NORTH AMERICA, INC.	1050001	CITROSUCO NORTH AMERICA, INC.	SWD	POLK	A	Y	6	PEEL DRYER NO 2	A	PM	2/26/2008	4.939	POUNDS/HOUR	ATC. Process rate: 43.4 tph
CITROSUCO NORTH AMERICA, INC.	1050001	CITROSUCO NORTH AMERICA, INC.	SWD	POLK	A	Y	6	PEEL DRYER NO 2	A	PM	2/20/2007	8.8	POUNDS/HOUR	ATC
CITROSUCO NORTH AMERICA, INC.	1050001	CITROSUCO NORTH AMERICA, INC.	SWD	POLK	A	Y	6	PEEL DRYER NO 2	A	PM	2/2/2005	10.9	POUNDS/HOUR	
CITROSUCO NORTH AMERICA, INC.	1050001	CITROSUCO NORTH AMERICA, INC.	SWD	POLK	A	Y	6	PEEL DRYER NO 2	A	PM	4/24/2003	7.4	POUNDS/HOUR	production rate: 43.3 tph (sets max. rate to 47.(tph)
CITROSUCO NORTH AMERICA, INC.	1050001	CITROSUCO NORTH AMERICA, INC.	SWD	POLK	A	Y	6	PEEL DRYER NO 2	A	PM	2/20/2004	10.1	POUNDS/HOUR	
CITROSUCO NORTH AMERICA, INC.	1050001	CITROSUCO NORTH AMERICA, INC.	SWD	POLK	A	Y	6	PEEL DRYER NO 2	A	PM	2/18/2005	10.862	POUNDS/HOUR	Process Rate 36.8 TPH
CITROSUCO NORTH		CITROSUCO NORTH												

AMERICA, INC.	1050001	AMERICA, INC.	SWD	POLK	A	Y	6	PEEL DRYER NO 2	A	PM	2/15/2006	8.1	POUNDS/HOUR	
CITROSUCO NORTH AMERICA, INC.	1050001	CITROSUCO NORTH AMERICA, INC.	SWD	POLK	A	Y	6	PEEL DRYER NO 2	A	PM	3/19/2003	5	POUNDS/HOUR	
CITROSUCO NORTH AMERICA, INC.	1050001	CITROSUCO NORTH AMERICA, INC.	SWD	POLK	A	Y	7	PEEL DRYER NO 3	A	PM	3/19/2003	9.41	POUNDS/HOUR	
CITROSUCO NORTH AMERICA, INC.	1050001	CITROSUCO NORTH AMERICA, INC.	SWD	POLK	A	Y	7	PEEL DRYER NO 3	A	PM	4/24/2003	15.3	POUNDS/HOUR	process rate: 47.5 tph
CITROSUCO NORTH AMERICA, INC.	1050001	CITROSUCO NORTH AMERICA, INC.	SWD	POLK	A	Y	7	PEEL DRYER NO 3	A	PM	2/19/2004	9	POUNDS/HOUR	
CITROSUCO NORTH AMERICA, INC.	1050001	CITROSUCO NORTH AMERICA, INC.	SWD	POLK	A	Y	7	PEEL DRYER NO 3	A	PM	2/18/2005	14.449	POUNDS/HOUR	Process Rate 37.4 TPH
CITROSUCO NORTH AMERICA, INC.	1050001	CITROSUCO NORTH AMERICA, INC.	SWD	POLK	A	Y	7	PEEL DRYER NO 3	A	PM	2/2/2005	14.5	POUNDS/HOUR	
CITROSUCO NORTH AMERICA, INC.	1050001	CITROSUCO NORTH AMERICA, INC.	SWD	POLK	A	Y	7	PEEL DRYER NO 3	A	PM	2/15/2006	10.7	POUNDS/HOUR	
CITROSUCO NORTH AMERICA, INC.	1050001	CITROSUCO NORTH AMERICA, INC.	SWD	POLK	A	Y	7	PEEL DRYER NO 3	A	PM	2/20/2007	7.4	POUNDS/HOUR	ATC
CITROSUCO NORTH AMERICA, INC.	1050001	CITROSUCO NORTH AMERICA, INC.	SWD	POLK	A	Y	7	PEEL DRYER NO 3	A	PM	3/6/2008	12.92	POUNDS/HOUR	ATC. Process rate: 46.9 tph
CITRUS WORLD, INC.	1050002	CITRUS WORLD, INC.	SWD	POLK	A	Y	7	CITRUS PEEL DRYER WITH WASTE-HEAT EVAPORATOR #1	A	PM	4/14/2005	8.63	POUNDS/HOUR	
CITRUS WORLD, INC.	1050002	CITRUS WORLD, INC.	SWD	POLK	A	Y	7	CITRUS PEEL DRYER WITH WASTE-HEAT EVAPORATOR #1	A	PM	4/15/2004	9.4921	POUNDS/HOUR	
CITRUS WORLD, INC.	1050002	CITRUS WORLD, INC.	SWD	POLK	A	Y	13	CITRUS PEEL DRYER WITH WASTE-HEAT EVAPORATOR #3	A	PM	4/23/2004	9.254	POUNDS/HOUR	
CITRUS WORLD, INC.	1050002	CITRUS WORLD, INC.	SWD	POLK	A	Y	13	CITRUS PEEL DRYER WITH WASTE-HEAT EVAPORATOR #3	A	PM	4/12/2005	6.6	POUNDS/HOUR	
CITRUS WORLD, INC.	1050002	CITRUS WORLD, INC.	SWD	POLK	A	Y	7	CITRUS PEEL DRYER WITH WASTE-HEAT EVAPORATOR #1	A	PM	4/15/2003	15.5	POUNDS/HOUR	31.01 tph
CITRUS WORLD, INC.	1050002	CITRUS WORLD, INC.	SWD	POLK	A	Y	13	CITRUS PEEL DRYER WITH WASTE-HEAT EVAPORATOR #3	A	PM	4/16/2003	19.3	POUNDS/HOUR	55.74 tph
CITRUS WORLD, INC.	1050002	CITRUS WORLD, INC.	SWD	POLK	A	Y	27	GAS TURBINE NO. 2 W/WH BOILER	A	NOX	4/13/2005	8.9	PARTS PER MILLION DRY GAS VOLUME	
CITRUS WORLD, INC.	1050002	CITRUS WORLD, INC.	SWD	POLK	A	Y	27	GAS TURBINE NO. 2 W/WH BOILER	A	NOX	4/6/2006	9.12	PARTS PER MILLION DRY GAS VOLUME	Coastal Air Consulting
CITRUS WORLD, INC.	1050002	CITRUS WORLD, INC.	SWD	POLK	A	Y	12	NATURAL GAS TURBINE @ 51.1MMBTU/HR (APPROX. 66 DEG. F)	A	NOX	4/5/2006	30.5	TONS/YEAR	Coastal Air Consulting
CITRUS WORLD, INC.	1050002	CITRUS WORLD, INC.	SWD	POLK	A	Y	1	CITRUS PEEL DRYER WITH WASTE-HEAT EVAPORATOR #2	A	PM	4/13/2005	12.13	POUNDS/HOUR	
CITRUS WORLD, INC.	1050002	CITRUS WORLD, INC.	SWD	POLK	A	Y	1	CITRUS PEEL DRYER WITH WASTE-HEAT EVAPORATOR #2	A	PM	4/17/2003	14.55	POUNDS/HOUR	47.74 tph
CITRUS WORLD, INC.	1050002	CITRUS WORLD, INC.	SWD	POLK	A	Y	1	CITRUS PEEL DRYER WITH WASTE-HEAT EVAPORATOR #2	A	PM	4/22/2004	7.7683	POUNDS/HOUR	
CITRUS WORLD, INC.	1050002	CITRUS WORLD, INC.	SWD	POLK	A	Y	12	NATURAL GAS TURBINE @ 51.1MMBTU/HR (APPROX. 66 DEG. F)	A	NOX	4/13/2005	0.033	POUNDS PER MILLION BTU HEAT INPUT	
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER PLANT	SWD	POLK	A	Y	4	Steam Generator # 7 (Phase II Acid Rain unit)	A	PM	9/30/2006	0.000001	POUNDS PER MILLION BTU HEAT INPUT	not operated
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER PLANT	SWD	POLK	A	Y	4	Steam Generator # 7 (Phase II Acid Rain unit)	A	PM	9/30/2006	0.000001	POUNDS PER MILLION BTU HEAT INPUT	not operated
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER PLANT	SWD	POLK	A	Y	4	Steam Generator # 7 (Phase II Acid Rain unit)	A	PM	6/12/2003	0.095	POUNDS PER MILLION BTU HEAT INPUT	
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER PLANT	SWD	POLK	A	Y	3	Fossil Fuel Fired Steam Generator # 6	A	PM	9/30/2006	0.00001	POUNDS PER MILLION BTU HEAT INPUT	not operated
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER PLANT	SWD	POLK	A	Y	3	Fossil Fuel Fired Steam Generator # 6	A	PM	9/30/2006	0.00001	POUNDS PER MILLION BTU HEAT INPUT	not operated
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER PLANT	SWD	POLK	A	Y	4	Steam Generator # 7 (Phase II Acid Rain unit)	A	PM	6/12/2003	0.105	POUNDS PER MILLION BTU HEAT INPUT	
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER PLANT	SWD	POLK	A	Y	8	Simple and Combined Cycle CTs (Phase II Acid Rain unit)	A	CO	2/8/2008	3.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	TESTED ON OIL NAT. GAS CO = 21.4 PPM
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER PLANT	SWD	POLK	A	Y	8	Simple and Combined Cycle CTs (Phase II Acid Rain unit)	A	CO	11/29/2005	11.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER PLANT	SWD	POLK	A	Y	8	Simple and Combined Cycle CTs (Phase II Acid Rain unit)	A	CO	11/29/2005	1.9	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER PLANT	SWD	POLK	A	Y	8	Simple and Combined Cycle CTs (Phase II Acid Rain unit)	A	NOX	12/2/2003	18.1	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER PLANT	SWD	POLK	A	Y	8	Simple and Combined Cycle CTs (Phase II Acid Rain unit)	A	NOX	1/30/2003	17.6	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	NATURAL GAS
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER PLANT	SWD	POLK	A	Y	8	Simple and Combined Cycle CTs (Phase II Acid Rain unit)	A	NOX	1/31/2003	33	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	OIL FUEL
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER PLANT	SWD	POLK	A	Y	8	Simple and Combined Cycle CTs (Phase II Acid Rain unit)	A	NOX	12/7/2004	13.7	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER PLANT	SWD	POLK	A	Y	8	Simple and Combined Cycle CTs (Phase II Acid Rain unit)	A	NOX	2/7/2005	31.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	test run at peak load operation on oil...base loac results same
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER PLANT	SWD	POLK	A	Y	8	Simple and Combined Cycle CTs (Phase II Acid Rain unit)	A	NOX	2/7/2005	18.2	PARTS PER MILLION DRY GAS VOLUME @ 15% O2	tested at peak load on gas...base load 15.8 ppm
LAKELAND ELECTRIC	1050003	CHARLES LARSEN MEMORIAL POWER	SWD	POLK	A	Y	8	Simple and Combined Cycle CTs (Phase II Acid Rain	A	NOX	11/29/2005	32.1	PARTS PER MILLION DRY GAS VOLUME	